

1) Quick summary — when to use which

- LMTD method — use when inlet & outlet temperatures of both streams are known. It gives the mean temperature driving force and is suitable for single-pass shell-and-tube exchangers behaving like true counter- or parallel-flow.
- NTU (effectiveness) method — use when one outlet temperature is unknown or for complex flow arrangements with multiple passes. It's more general and handles different configurations better.

2) Important formulas

Heat duty (energy balance): $Q = \dot{m}_h C_p (\bar{T}_{h,in} - \bar{T}_{h,out}) = \dot{m}_c C_p (\bar{T}_{c,out} - \bar{T}_{c,in})$

LMTD method:

$$\Delta T_{lm} = (\Delta T_1 - \Delta T_2) / \ln(\Delta T_1 / \Delta T_2)$$

where for counterflow: $\Delta T_1 = \bar{T}_{h,in} - \bar{T}_{c,out}$, $\Delta T_2 = \bar{T}_{h,out} - \bar{T}_{c,in}$

$$UA = Q / \Delta T_{lm}$$

NTU/Effectiveness method:

$$Ch = \dot{m}_h C_p, Cc = \dot{m}_c C_p, C_{min} = \min(Ch, Cc), Cr = C_{min} / C_{max}$$

$$NTU = UA / C_{min}$$

$$\text{For counterflow: } \epsilon = [1 - \exp(-NTU(1-Cr))] / [1 - Cr \exp(-NTU(1-Cr))]$$

$$Q = \epsilon C_{min} (\bar{T}_{h,in} - \bar{T}_{c,in})$$

3) Worked numerical example

Given:

Hot stream: $\dot{m}_h = 1.5 \text{ kg/s}$, $C_p = 2000 \text{ J/kg}\cdot\text{K}$, $\bar{T}_{h,in} = 150^\circ\text{C}$, $\bar{T}_{h,out} = 100^\circ\text{C}$

Cold stream: $\dot{m}_c = 2.0 \text{ kg/s}$, $C_p = 4180 \text{ J/kg}\cdot\text{K}$, $\bar{T}_{c,in} = 30^\circ\text{C}$

A) $Q = 1.5 \times 2000 \times (150 - 100) = 150,000 \text{ W}$

B) $\bar{T}_{c,out} = 30 + 150000 / (2 \times 4180) = 47.94^\circ\text{C}$

C) $\Delta T_1 = 150 - 47.94 = 102.06^\circ\text{C}$; $\Delta T_2 = 100 - 30 = 70^\circ\text{C}$

$\Delta T_{lm} = (102.06 - 70) / \ln(102.06 / 70) = 85.02^\circ\text{C}$

D) $UA = Q / \Delta T_{lm} = 150000 / 85.02 = 1764 \text{ W/K}$

E) $NTU = UA / C_{min} = 1764 / 3000 = 0.588$; $\epsilon = 0.417$; $Q = 0.417 \times 360000 = 150,000 \text{ W}$
(consistent).

4) Notes for shell-and-tube exchangers

- Real exchangers often use a correction factor F for multi-pass or crossflow geometry:
 $\Delta T_{lm(actual)} = F \times \Delta T_{lm(ideal)}$.
- F is based on parameters $R = (\bar{T}_{h,in} - \bar{T}_{h,out}) / (\bar{T}_{c,out} - \bar{T}_{c,in})$ and $P = (\bar{T}_{c,out} - \bar{T}_{c,in}) / (\bar{T}_{h,in} - \bar{T}_{h,out})$.
- Typical overall heat-transfer coefficient (U): 200–1000 W/m²K depending on fluids and fouling.
- NTU method avoids correction charts and works well for complex shell-pass arrangements.

5) Practical checklist for design/calculation

1. Determine knowns: inlet/outlet temps or flow rates.
2. Choose method: LMTD if both outlets known; NTU if one outlet unknown.
3. Calculate heat duty (Q) via energy balance.
4. Compute LMTD (apply F if needed) and get $UA = Q / \Delta T_{lm}$.
5. Estimate U and compute $A = UA / U$.
6. Use NTU method to verify effectiveness.
7. Iterate if parameters (U , flow, geometry) change.