

1) Quick summary — when to use which

- LMTD method — use when inlet & outlet temperatures of both streams are known. It gives the mean temperature driving force and is suitable for single-pass shell-and-tube exchangers behaving like true counter- or parallel-flow.
- NTU (effectiveness) method — use when one outlet temperature is unknown or for complex flow arrangements with multiple passes. It's more general and handles different configurations better.

2) Important formulas

Heat duty (energy balance): $Q = \dot{m}_h C_{p,h} (T_{h,in} - T_{h,out}) = \dot{m}_c C_{p,c} (T_{c,out} - T_{c,in})$

LMTD method:

$$\Delta T_{lm} = (\Delta T_1 - \Delta T_2) / \ln(\Delta T_1 / \Delta T_2)$$

where for counterflow: $\Delta T_1 = T_{h,in} - T_{c,out}$, $\Delta T_2 = T_{h,out} - T_{c,in}$

$$UA = Q / \Delta T_{lm}$$

NTU/Effectiveness method:

$$C_h = \dot{m}_h C_{p,h}, C_c = \dot{m}_c C_{p,c}, C_{min} = \min(C_h, C_c), Cr = C_{min} / C_{max}$$

$$NTU = UA / C_{min}$$

$$\text{For counterflow: } \varepsilon = [1 - \exp(-NTU(1-Cr))] / [1 - Cr \exp(-NTU(1-Cr))]$$

$$Q = \varepsilon C_{min} (T_{h,in} - T_{c,in})$$

3) Worked numerical example

Given:

Hot stream: $\dot{m}_h = 1.5 \text{ kg/s}$, $C_{p,h} = 2000 \text{ J/kg}\cdot\text{K}$, $T_{h,in} = 150^\circ\text{C}$, $T_{h,out} = 100^\circ\text{C}$

Cold stream: $\dot{m}_c = 2.0 \text{ kg/s}$, $C_{p,c} = 4180 \text{ J/kg}\cdot\text{K}$, $T_{c,in} = 30^\circ\text{C}$

$$\text{A) } Q = 1.5 \times 2000 \times (150 - 100) = 150,000 \text{ W}$$

$$\text{B) } T_{c,out} = 30 + 150,000 / (2 \times 4180) = 47.94^\circ\text{C}$$

$$\text{C) } \Delta T_1 = 150 - 47.94 = 102.06^\circ\text{C}; \Delta T_2 = 100 - 30 = 70^\circ\text{C}$$

$$\Delta T_{lm} = (102.06 - 70) / \ln(102.06 / 70) = 85.02^\circ\text{C}$$

$$\text{D) } UA = Q / \Delta T_{lm} = 150,000 / 85.02 = 1764 \text{ W/K}$$

$$\text{E) } NTU = UA / C_{min} = 1764 / 3000 = 0.588; \varepsilon = 0.417; Q = 0.417 \times 360,000 = 150,000 \text{ W (consistent).}$$

4) Notes for shell-and-tube exchangers

- Real exchangers often use a correction factor F for multi-pass or crossflow geometry:
 $\Delta T_{lm}(\text{actual}) = F \times \Delta T_{lm}(\text{ideal})$.
- F is based on parameters $R = (T_{h,in} - T_{h,out}) / (T_{c,out} - T_{c,in})$ and $P = (T_{c,out} - T_{c,in}) / (T_{h,in} - T_{c,in})$.
- Typical overall heat-transfer coefficient (U): 200–1000 W/m²K depending on fluids and fouling.
- NTU method avoids correction charts and works well for complex shell-pass arrangements.

5) Practical checklist for design/calculation

1. Determine knowns: inlet/outlet temps or flow rates.
2. Choose method: LMTD if both outlets known; NTU if one outlet unknown.
3. Calculate heat duty (Q) via energy balance.
4. Compute LMTD (apply F if needed) and get $UA = Q / \Delta T_{lm}$.
5. Estimate U and compute $A = UA / U$.
6. Use NTU method to verify effectiveness.
7. Iterate if parameters (U , flow, geometry) change.