

Mathematics

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1 Calculus

1.1 Differentiation

- 2 Series**
- 3 Multivariable Calculus**
- 4 Linear Algebra**
- 5 Differential Equations**
- 6 Partial Differential Equations**

7 Vector Calculus

7.1 Operators

7.1.1 Grad

7.1.2 Div

7.1.3 Curl

7.1.4 Laplacian

7.2 Integral Theorems

7.2.1 Divergence Theorem

7.2.2 Stokes's Theorem

8 Fluid Mechanics

8.1 Kinematics

8.1.1 Coordinates

Lagrangian $\underline{x}(\underline{a}, t)$: The *motion of individual particles* is studied; the position \underline{x} of a particle at time t is related to its position at a reference point in time \underline{a} (typically at $t = 0$).

Eulerian (\underline{x}, t) : The *'flow field'* is considered as a whole and the state of a fluid is described in terms of the values at a fixed location \underline{x} and at a fixed time t .

8.1.2 Velocity

In Cartesian coordinates the velocity of a fluid particle at position $\underline{x}(x, y, z)$ is given by:

$$\underline{u}(x, y, z) = u(x, y, z)\hat{i} + v(x, y, z)\hat{j} + w(x, y, z)\hat{k}$$

8.1.3 Stagnation Points

Stagnation points occur when the velocity vector \underline{u} is equal to $\underline{0}$

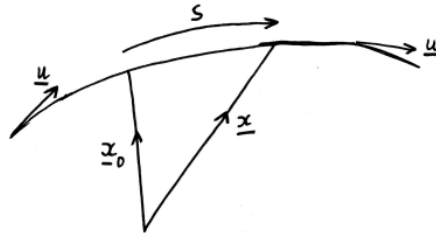
$$u = 0$$

$$v = 0$$

$$w = 0$$

8.1.4 Streamlines

A streamline is a curve C drawn at one point in time such that the fluid velocity vector \underline{u} is tangent to C at every point along C .



$$\frac{d\underline{x}}{ds} = \underline{u}$$

$$\frac{dx}{ds} = u, \frac{dy}{ds} = v, \frac{dz}{ds} = w$$

$$\boxed{\frac{dx}{u} = \frac{dy}{v} = \frac{dz}{w} (= ds)}$$

8.1.5 Particle Paths

Particle path is obtained by solving the initial value problem:

$$\frac{d\underline{x}}{dt} = \underline{u}(\underline{x}, t), \underline{x} = x_0 \text{ at } t = 0$$

$$\frac{dx}{dt} = u, x(0) = x_0$$

$$\frac{dy}{dt} = v, y(0) = y_0$$

$$\frac{dz}{dt} = w, z(0) = z_0$$

8.1.6 Steady Flow

Steady Flow: The flow velocity vector \underline{u} is independent of time t

Unsteady Flow: \underline{u} depends on t ; the pattern of streamlines changes with t

8.1.7 Convective Derivative

The convective derivative tells us how a property changes *as it moves with a flow*.

General

$$\boxed{\frac{D*}{Dt} = \frac{\partial*}{\partial t} + (\underline{u} \cdot \nabla)* = \frac{\partial*}{\partial t} + u \frac{\partial*}{\partial x} + v \frac{\partial*}{\partial y} + w \frac{\partial*}{\partial z}}$$

Scalar

$$\boxed{\frac{D\rho}{Dt} = \frac{\partial\rho}{\partial t} + (\underline{u} \cdot \nabla)\rho = \frac{\partial\rho}{\partial t} + u \frac{\partial\rho}{\partial x} + v \frac{\partial\rho}{\partial y} + w \frac{\partial\rho}{\partial z}}$$

Vector

$$\boxed{\frac{D\underline{u}}{Dt} = \frac{\partial\underline{u}}{\partial t} + (\underline{u} \cdot \nabla)\underline{u} = \frac{\partial\underline{u}}{\partial t} + u \frac{\partial\underline{u}}{\partial x} + v \frac{\partial\underline{u}}{\partial y} + w \frac{\partial\underline{u}}{\partial z}}$$

8.1.8 Vorticity

Vorticity $\underline{\omega}$ is a measure of the local rotation of fluid particles in flow.

$$\underline{\omega} = \nabla \times \underline{u}$$

$$\nabla \times \underline{u} = \begin{vmatrix} \underline{i} & \underline{j} & \underline{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ u & v & w \end{vmatrix}$$

Irrotational Flow:

$$\underline{\omega} = \underline{0}$$

8.1.9 Incompressible Flow

$$\nabla \cdot \underline{u} = 0$$

When this is true the convective derivative of the fluid density is zero:

$$\frac{D\rho}{Dt} = 0$$

8.1.10 Velocity Potential

For an irrotational flow the velocity can be described as the gradient of a scalar field known as the *Velocity Potential*.

$$\nabla \times \underline{u} = 0$$

The curl of the gradient of a scalar field is zero:

$$\nabla \times (\nabla \phi) = 0$$

$$\underline{u} = \nabla \phi$$

If the flow is also incompressible

$$\nabla \cdot \underline{u} = 0$$

$$\nabla \cdot (\nabla \phi) = 0$$

Therefore the velocity potential of an irrotational, incompressible flow satisfies

Laplace's Equation:

$$\nabla^2 \phi = 0$$

8.1.11 Equipotential Surfaces

Lines/surfaces of constant ϕ are *equipotentials*.

The velocity potential can be considered a surface:

$$\phi(x, y, z) = c$$

Let \underline{a} be tangent to the surface, the derivative of ϕ in the direction of \underline{a} :

$$\underline{a} \cdot \nabla \phi = 0$$

Because the derivative of a constant c is zero: $\nabla \phi$ is normal to the surface.

$$\underline{\hat{n}} = \frac{\nabla \phi}{|\nabla \phi|}$$

8.1.12 The Stream Function

Considering incompressible two dimensional flow:

$$\begin{aligned} \nabla \cdot \underline{u} &= 0 \\ \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} &= 0 \end{aligned}$$

We can introduce the stream function $\psi(x, y, t)$ such that:

$$u = \frac{\partial \psi}{\partial y}, v = -\frac{\partial \psi}{\partial x}$$

This satisfies the previous equations:

$$\frac{\partial^2 \psi}{\partial x \partial y} - \frac{\partial^2 \psi}{\partial y \partial x} = 0$$

Vorticity of an incompressible two dimensional flow:

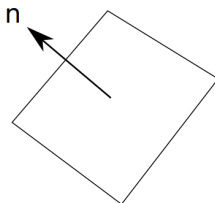
$$\begin{aligned} \underline{\omega} &= \nabla \times \underline{u} \\ \underline{\omega} &= \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \\ \underline{\omega} &= -\frac{\partial^2 \psi}{\partial^2 x} - \frac{\partial^2 \psi}{\partial^2 y} \\ \underline{\omega} &= -\nabla^2 \psi \end{aligned}$$

8.2 Pressure in a Fluid

8.2.1 Pressure and Force

Let the normal vector \underline{n} be pointing into the fluid.

$$\partial \underline{F} = -\partial F \underline{n}$$



∂F is the force exerted over a small area ∂S

$$p = \lim_{\partial S \rightarrow 0} \left(\frac{\partial F}{\partial S} \right)$$

$$\underline{F} = - \int \int_S p \underline{n} dS$$

8.2.2 Equations of State

Ideal Gas Law

$$pV = nRT$$

$$\frac{pV}{T} = nR$$

$$V \propto 1/\rho$$

$$\frac{p}{\rho T} = \text{constant}$$

Isothermal Gas

For a gas at constant temperature T

Boyle's Law:

$$p \propto \rho$$

$$p\rho^{-1} = p_0\rho_0^{-1}$$

Adiabatic Gas

Quick fluctuations in pressure (such as in sound waves) are described by the adiabatic law.

$$p\rho^{-\gamma} = c$$

Where γ is the *Polytropic Index*

8.2.3 Hydrostatics

The force due to the pressure of the fluid

$$\underline{F} = - \int \int_S p \underline{n} dS$$

Applying the divergence theorem for a scalar:

$$\underline{F} = - \int \int_V \nabla p dV$$

Calculating the weight of the fluid region:

$$\underline{W} = \int \int_V \rho \underline{g} dV$$

Since the fluid is stationary, the total force on the fluid is zero

$$\underline{W} + \underline{F} = 0$$

$$\int \int \int_V \rho \underline{g} dV - \int \int \int_V \nabla p dV = 0$$

$$\int \int \int_V (\rho \underline{g} - \nabla p) dV = 0$$

Therefore:

$$\rho \underline{g} = \nabla p$$

$$g = -g\hat{k}$$

$$\frac{\partial p}{\partial z} = -\rho g$$

Integrating gives:

$$p = p_a - \rho g z$$

8.2.4 Buoyancy

Buoyancy is the force exerted on a submerged body due to the pressure of the surrounding static fluid.

$$\underline{B} = - \int \int_S p \underline{n} dS$$

Applying the divergence theorem for a scalar:

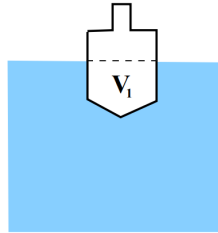
$$\underline{B} = - \int \int \int_V \nabla p dV$$

$$\nabla p = \rho \underline{g}, \underline{g} = -g\hat{k}$$

$$\underline{B} = \hat{k} g \int \int \int_V \rho dV$$

$$\underline{B} = \rho V g \hat{k} = m_w g \hat{k}$$

Archimedes' Principle – the buoyancy force on a body is equal in magnitude to the weight of fluid that is displaced by the body.



$$V_1 = \text{Volume of displaced water,}$$

$$\rho_w = \text{Density of water,}$$

$$m_B = \text{Mass of the body}$$

At equilibrium:

$$\underline{B} + \underline{W} = 0$$

$$\rho_w V_1 g \hat{k} - m_B g \hat{k} = 0$$

$$m_B = \rho_w V_1$$

Center of Mass (Gravity): A theoretical point in the body where the body's total mass (weight) is thought to be concentrated.

Center of Buoyancy: The centre of mass of the displaced water

A floating body is stable if its centre of gravity is below its centre of buoyancy.

8.2.5 Oscillation of a Floating Body

When a floating body is submerged below its equilibrium depth d it begins to oscillate.

Consider a cylindrical body with mass m , circular area A , equilibrium depth d :

$$\begin{aligned} mz''(t) &= \rho_w g(d - z(t))A - mg \\ &= -\rho_w g z(t)A \\ &= mg \frac{z(t)}{d} \end{aligned}$$

Therefore you can form the differential equation:

$$\begin{aligned} z''(t) &= \frac{g}{d} z(t) \\ z(0) &= -z_0 \end{aligned}$$

The solution:

$$z(t) = -z_0 \cos(\sqrt{\frac{g}{d}}t)$$

8.3 Flow Dynamics

8.3.1 Reynolds Transport Theorem

$$\frac{d}{dt} \int_{\Omega(t)} F(\underline{x}, t) dV = \lim_{\Delta t \rightarrow 0} [\int_{\Omega(t+\Delta t)} F(\underline{x}, t + \Delta t) dV - \int_{\Omega(t)} F(\underline{x}, t) dV]$$

Using the Taylor series expansion:

$$\frac{d}{dt} \int_{\Omega(t)} F(\underline{x}, t) dV = \lim_{\Delta t \rightarrow 0} [\int_{\Omega(t+\Delta t)} F(\underline{x}, t) + \frac{\partial F}{\partial t}(\underline{x}, t) \Delta t + O(\Delta t)^2 dV - \int_{\Omega(t)} F(\underline{x}, t) dV]$$

Let $\Delta\Omega$ be the difference between the regions $\Omega(t)$ and $\Omega(t + \Delta t)$:

$$\frac{d}{dt} \int_{\Omega(t)} F(\underline{x}, t) dV = \lim_{\Delta t \rightarrow 0} [\int_{\Delta\Omega} F(\underline{x}, t) dV + \int_{\Omega(t+\Delta t)} \frac{\partial F}{\partial t}(\underline{x}, t) \Delta t + O(\Delta t)^2 dV]$$

Letting U_n be the normal velocity to the boundary $\partial\Omega$

$$\frac{d}{dt} \int_{\Omega(t)} F(\underline{x}, t) dV = \lim_{\Delta t \rightarrow 0} [\int_{\partial\Omega} F(\underline{x}, t) U_n(\underline{x}, t) \Delta t dS] + \lim_{\Delta t \rightarrow \infty} [\int_{\Omega(t+\Delta t)} \frac{\partial F}{\partial t}(\underline{x}, t) \Delta t dV]$$

$$\boxed{\frac{d}{dt} \int_{\Omega(t)} F(\underline{x}, t) dV = \int_{\partial\Omega} F(\underline{x}, t) U_n(\underline{x}, t) dS + \int_{\Omega(t)} \frac{\partial F}{\partial t}(\underline{x}, t) dV}$$

Leibniz's Integral Rule: The rule can be derived from considering a one dimensional case of *Reynold's Transport Theorem*.

$$\boxed{\frac{d}{dt} \int_{a(t)}^{b(t)} F(x, t) dx = \int_{a(t)}^{b(t)} \frac{\partial F}{\partial t}(x, t) dx + F(b(t), t) \frac{db}{dt} - F(a(t), t) \frac{da}{dt}}$$

8.3.2 Conservation of Mass

8.4 Tow-dimensional Flow

8.5 Vorticity Dynamics

8.6 Free Surface Waves

9 Numerical Methods