$\frac{m}{M}RT\ln\frac{V_2}{V_1}$

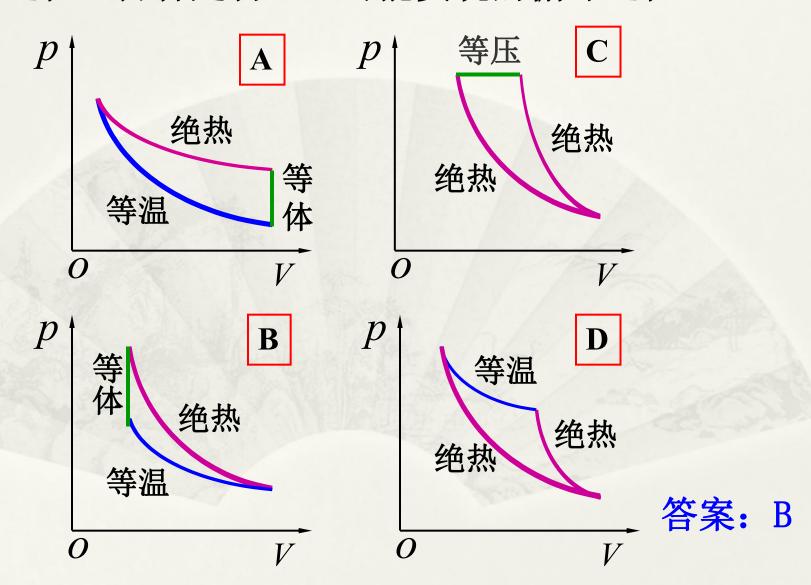
 $(P_1V_1\ln\frac{P_1}{P_2})$

等温

 $\frac{m}{M}RT\ln\frac{V_2}{V_1}$

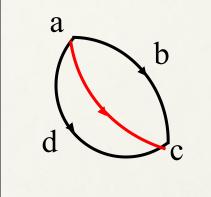
 $(P_1V_1\ln\frac{P_1}{P_2})$

例1、以下四图是某人设计的理想气体的四种循环过程,哪种是物理上可能实现的循环过程?



问: abc过程和adc过程是吸热还是放热

答:
$$\therefore a \to c$$
 $(dQ = 0)$
 $A > 0$
 $A = -\Delta E$





$$abc$$
过程: $Q' = A' + \Delta E$ $\Delta E = -A$ $A' > A$ $Q' = (A' - A) > 0$ (吸热)

$$adc$$
过程: $Q'' = A'' + \Delta E$

$$\Delta E = -A$$

$$A'' < A$$

$$Q' = (A'' - A) < 0$$
 (放热)

[例3] 1mo1单原子理想气体,由状态a(p₁, V₁)先等压加热至体积增大1倍,再等体加热至压力增大1倍,最后再经绝热膨胀,使其温度降至初始温度,如图所示,试求:

- (1) 状态d的体积Vd;
- (2)整个过程对外所做的功;
- (3)整个过程吸收的热量.

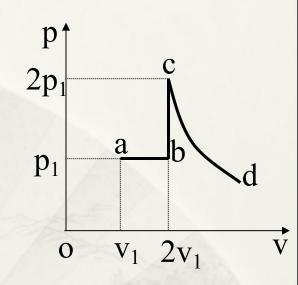


解:(1)由绝热过程方程: $T_cV_c^{\gamma-1} = T_dV_d^{\gamma-1}$

得:
$$V_d = \left(\frac{T_c}{T_d}\right)^{\frac{1}{\gamma-1}} V_c = 15.8 V_1$$

根据题意:
$$T_d = T_a = \frac{p_1 V_1}{R}$$

$$T_c = \frac{p_c V_c}{R} = \frac{4 p_1 V_1}{R} = 4 T_a$$



$$V_c = 2V_1$$

$$\gamma = \frac{5}{3}$$

(2)整个过程对外所做的功;

$$A = A_{ab} + A_{bc} + A_{cd}$$

其中:
$$A_{ab} = p_1(V_b - V_a) = p_1V_1$$

$$A_{bc} = 0$$

$$A_{cd} = -\Delta E_{cd} = C_V (T_c - T_d) = C_V (4T_a - T_a)$$
$$= \frac{3}{2} R \cdot 3T_a = \frac{9}{2} p_1 V_1$$

得:
$$A = \frac{11}{2} P_1 V_1$$

(3)整个过程吸收的热量.

方法一:
$$Q = Q_{ab} + Q_{bc} + Q_{cd} = \frac{11}{2} P_1 V_1$$

$$Q_{ab} = C_p (T_b - T_a) = \frac{5}{2} R(T_b - T_a)$$

$$= \frac{5}{2}(p_b V_b - p_a V_a) = \frac{5}{2}p_1 V_1$$

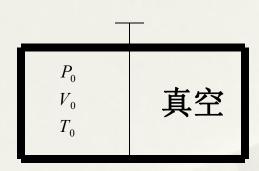
$$Q_{bc} = C_V(T_c - T_b) = \frac{3}{2}R(T_c - T_b) = \frac{3}{2}(p_c V_c - p_b V_b) = 3p_1 V_1$$

$$Q_{cd} = 0$$

方法二:对abcd整个应用热力学第一定律 $Q=\Delta E+A$

$$T_a = T_d, \Delta E = 0 \quad \therefore Q = A = \frac{11}{2} p_1 V_1$$

二、非静态绝热过程——绝热自由膨胀





$$V_0^{\gamma - 1} T_0 = (2V_0)^{\gamma - 1} T \to T$$

$$P_0 V_0^{\gamma} = P (2V_0)^{\gamma} \to P$$

 $2V_0$

$$P_0 V_0^{\gamma} = P \ (2V_0)^{\gamma} \to P$$

$$\begin{array}{c} \therefore (E - E_0) + A = 0 \\ \hline \longrightarrow A = 0 \end{array}$$

$$E = E_0 \qquad (T = T_0)$$

始末两态满足
$$\frac{P_0V_0}{T_0} = \frac{P_0(2V_0)}{T}$$
 \longrightarrow $P = \frac{1}{2}P_0$

三、多方过程

$$pV^n = C$$

一般情况1< n < γ, 多方过程可近似代表 气体内进行的实际过程。

*多方过程的功

$$A = \int_{V_1}^{V_2} P dV$$

$$PV^n = P_1 V_1^n$$

$$A = P_1 V_1^n \int_{V_1}^{V_2} \frac{dV}{V^n} = \frac{P_1 V_1 - P_2 V_2}{n-1}$$

$$= \frac{P_1 V_1 - P_2 V_2}{n - 1}$$

*摩尔热容

$$A = \frac{P_1 V_1 - P_2 V_2}{n - 1} = -\frac{1}{n - 1} \left[\frac{m}{M} R(T_2 - T_1) \right]$$

$$\Delta E = \frac{m}{M} C_V (T_2 - T_1)$$

$$Q = A + \Delta E = \frac{m}{M} \left[C_V - \frac{R}{n-1} \right] (T_2 - T_1) = \frac{m}{M} C_{mol} \Delta T$$

$$C_{mol} = C_V - \frac{R}{n-1} = \frac{n-\gamma}{n-1} C_V$$

等容过程: $n = \infty$, $C_{mol} = C_V$

等温过程: $n=1, C_{mol}=\infty$

等压过程: $n=0, C_{mol}=\gamma C_V=C_P$ 绝热过程: $n=\gamma, C_{mol}=0$

$$Q = \frac{m}{M} C_{mol} \Delta T$$

$$C_{mol} < 0$$

$$\therefore$$
当 $1 < n < \gamma$ 时, $C_{mol} < 0$ $\begin{cases} T \uparrow Q < 0 & 放热 \\ T \downarrow Q > 0 & 吸热 \end{cases}$

当
$$n > \gamma$$
或 $n < 1$ 时 $\mathbf{C}_{mol} > 0$ $\begin{cases} T \uparrow Q > 0 & \mathbf{W} \\ T \downarrow Q < 0 & \mathbf{M} \end{cases}$

$$C_{mol} > 0$$

$$T \downarrow Q$$

[例4] 一摩尔的单原子理想气体,从初态 (P_1, V_2)

出发,经过某一过程 $PV^2 = C$,体积膨胀到 $V_2 = 2V_1$ 。

- ①.试写出气体温度与压强间的表达式;
- ②当气体膨胀时,其温度是升高还是降低;



- ③.在此过程中气体摩尔热容 C_{mol} 为何值;
- (4).气体分子的平均动能将如何变化。

解:(1).
$$PV^2 = P(\frac{m}{M}\frac{RT}{P})^2 = \frac{m^2}{M^2}R^2\frac{T^2}{P} = C$$
 :. $PT^{-2} = C'$

$$(2). : PV^2 = C$$

$$PT^{-2} = C'$$

$$VT = C'' : V \uparrow, T \downarrow$$

③.在此过程中气体摩尔热容 C_{mol} 为何值;

解法一:

$$C_{mol} = \frac{n - \gamma}{n - 1} C_V$$

$$n=2, \qquad C_V=\frac{3}{2}R$$

$$\gamma = \frac{C_P}{C_V} = \frac{i+2}{i} = \frac{5}{3}$$

得:
$$C_{mol} = \frac{1}{2}R$$

解法二:

$$C_{mol} = \frac{Q}{T_2 - T_1} = \frac{\Delta E + A}{T_2 - T_1}$$

$$\Delta E = \frac{i}{2}R \ (T_2 - T_1) = \frac{3}{2}R \ (T_2 - T_1)$$

$$A = \frac{P_1V_1 - P_2V_2}{n - 1} = -R \ (T_2 - T_1)$$

得:
$$C_{mol} = \frac{1}{2}R$$

(4).气体分子的平均动能将如何变化。

7.5 循环过程 卡诺循环

一 循环过程

系统经过一系列变化状态过程后,又回到原来的状态的过程叫热力学循环过程.

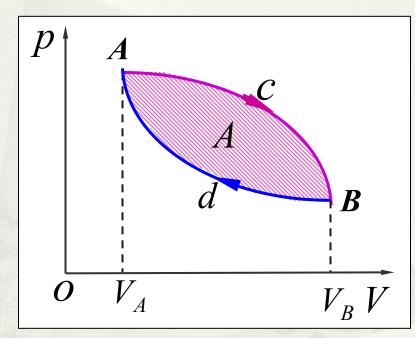
特征
$$\Delta E = 0$$

热力学第一定律 Q = A

$$A_{\mu}$$
 $\overline{Q}_1 - Q_2 = Q$

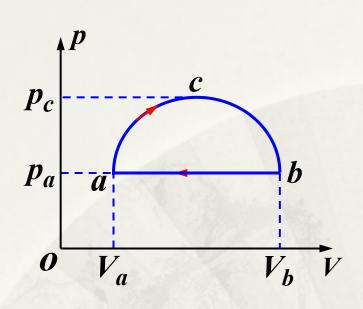
总吸热 $\longrightarrow Q_1$

总放热 $\longrightarrow Q_2$ (取绝对值)



例1

 $p_c = 2p_a$,循环过程中净吸热为



(A)
$$Q = \frac{m}{M} C_p (T_b - T_a)$$

(B)
$$Q < \frac{m}{M}C_p(T_b - T_a)$$

(C)
$$Q > \frac{m}{M} C_p (T_b - T_a)$$

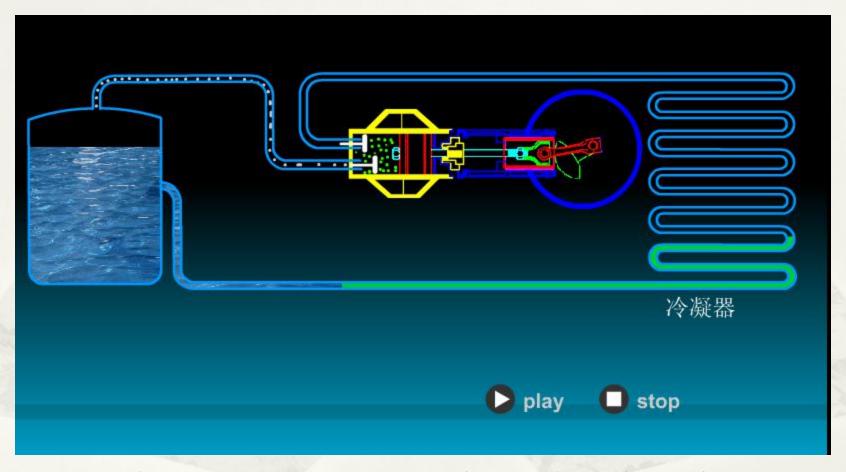
(D) 不能确定

净吸热 Q =

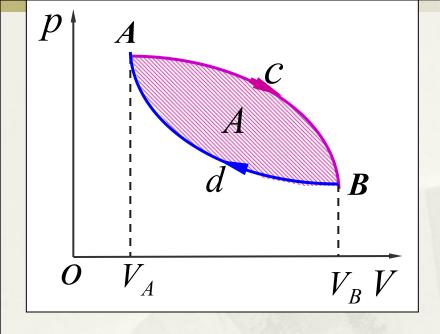
$$a \rightarrow b$$
 过程吸热
$$\frac{m}{M}C_p(T_b - T_a) = \frac{i+2}{2}P_a(V_b - V_a)$$

二 热机和热机效率

热机: 持续地将热量转变为功的机器.

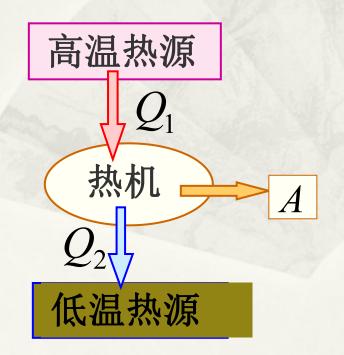


工作物质(工质): 热机中被用来吸收热量并对外做功的物质.



热机(正循环)A > 0

热机效率

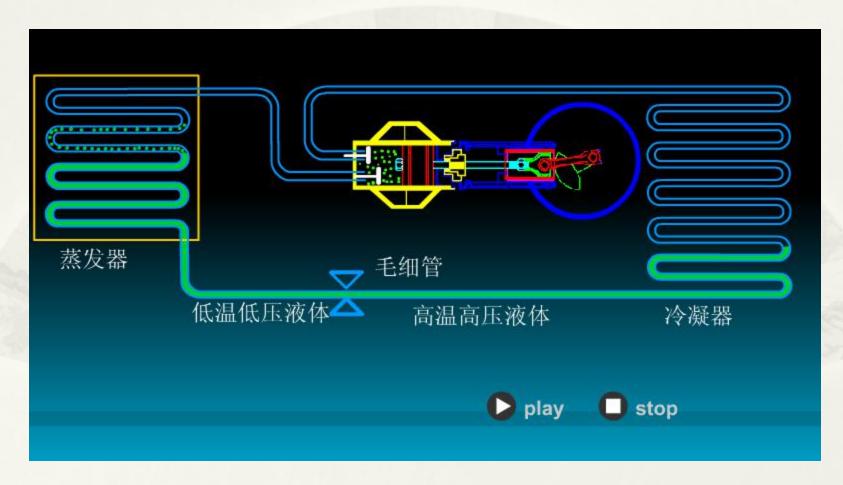


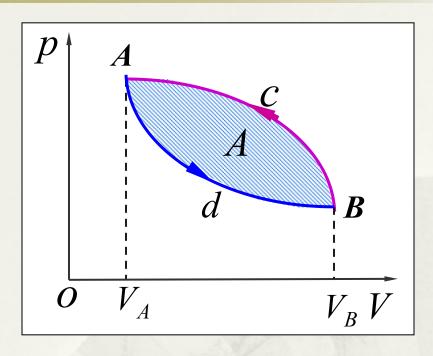
$$\eta = \frac{A}{Q_1} = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1}$$

三 致冷机和致冷系数

制冷机:

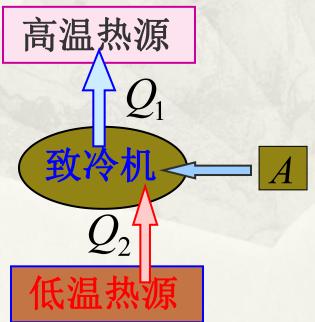
冰箱循环示意图





致冷机(逆循环) A < 0

致冷机致冷系数



$$\omega = \frac{Q_2}{|\mathbf{A}|} = \frac{Q_2}{Q_1 - Q_2}$$

[例2] 1mol 氢气作如图所示的循环过程计算此循环之效率。

解:
$$A = (P_a - P_d)(V_b - V_a)$$

$$Q_{\mathfrak{B}} = Q_{ab} + Q_{da}$$

$$= C_P(T_b - T_a) + C_V(T_a - T_d)$$

$$\begin{array}{c|c}
p(\text{atm}) & Q_{ab} \\
\hline
2 & Q_{da} & Q_{bc} \\
\hline
1 & Q_{cd} & C
\end{array}$$

[例3] 1mol 氧气作如图所示的循环。

求: 循环效率

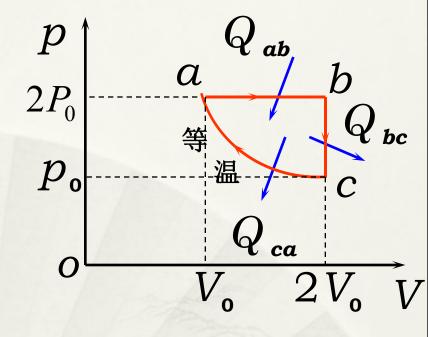
解:

$$Q_{ab} = C_P (T_b - T_a)$$

$$Q_{bc} = C_V (T_c - T_b)$$

$$Q_{ca} = RT_c \ln \frac{V_0}{2V_0}$$

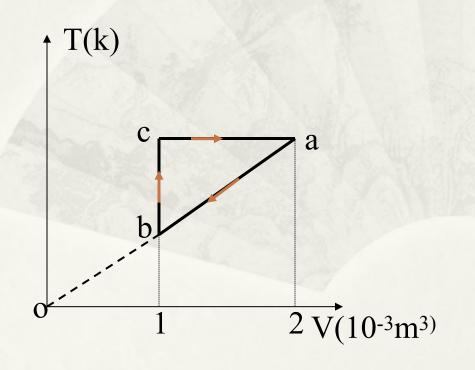
$$\eta = 1 - \frac{Q_{\dot{m}}}{Q_{\dot{m}}} = 1 - \frac{|Q_{bc} + Q_{ca}|}{Q_{ab}}$$

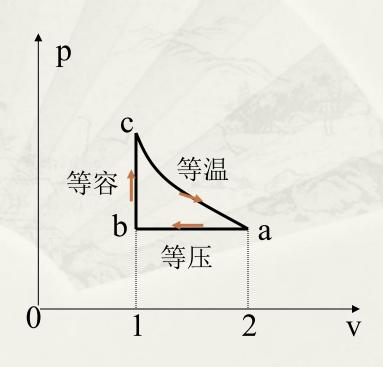


$$(T_b = 2T_c = 2T_a)$$

[例4] 1mol单原子分子理想气体的 循环过程 如图所示,其中 $T_c = 600 K$ 。试求:

- ①.ab、bc、ca各过程系统吸收的热量,
- (2).经一循环系统所作的净 功,
- ③ 循环的效率。





①.ab、bc、ca各过程系统吸收的热量

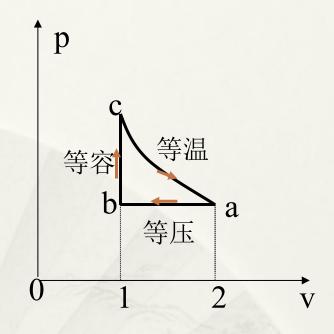
$$Q_{ab} = C_P(T_b - T_a)$$

$$\frac{V_a}{V_b} = \frac{T_a}{T_b} = \frac{T_c}{T_b} = 2$$

$$T_c = T_a = 600k$$

$$C_P = \frac{i+2}{2}R = \frac{5}{2}R$$

Q_{ab} 放热



$$Q_{bc} = C_V (T_c - T_b)$$

$$C_V = \frac{3}{2}R$$

$$T_c = 600k, T_b = 300k$$

 Q_{bc} 吸热

$$Q_{ca} = RT_c \ln \frac{V_a}{V_c}$$

吸热

(2).经一循环系统所作的净功

解一:

$$A_{\not\ni} = A_{ca} - |A_{ab}| = Q_{ca} - R (T_a - T_b)$$

解二:

$$A$$
 $_{\mathcal{P}}$ $=$ Q $_{\mathcal{W}}$ Q $_{\mathcal{W}}$

③ 循环的效率。

$$\eta = \frac{A}{Q_{\text{W}}}$$

