How to use free-surface flows in OpenFOAM® 3.0

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Training type: Intermediate

Session type: Lecture with examples

Software stack: OpenFOAM 3.0.x

Plan of training course

- Introduction
- Key points of training course
- interFoam solver: how it works
 - Governing equations
 - Volume of Fluid method
 - Solution process
 - Boundary conditions
- Spillway tutorial
 - Model setup
 - blockMesh utility
 - snappyHexMesh utility
 - Boundary conditions setup
 - Numerical and time settings. Running.
 - Results
- Conclusions and discussion



Introduction

Applicability:

- printing;
- engines;
- ecological cases;
- dams, spillways;
- etc.

Complexities:

- large deformations of the interface;
- creation of different subregions (droplets, bubbles...);
- solution should:
 - be stable;
 - have small diffusivity in the interface region;
 - satisfy to conservation laws;
 - be correct in different scales (example droplet impact to the liquid layer);
 - require not so much resources for computations.



Key points of training course

The main key points of training track:

Look how a solver for free-surface flows works.

Study how to set boundary conditions in different versions of OpenFOAM.

Boundary conditions are critically important in the successful modeling.

There are strong differences between OpenFoam 2.2.x and 2.3.0+.

Another key point:

Look to all stages of modeling of free-surface flows

in OpenFOAM v.3.0.0:

from mesh generation to post-processing

The main tool: an interFoam solver in OF v. 3.0.0.

We will study it with **Spillway tutorial**: the turbulent flow of fluid.

Part I

Theoretical part

interFoam: how it works

Structure of theoretical part

- 1. Governing equations.
- 2. Volume of Fluid method.
- Block scheme of interFoam.
- 4. Pressure-velocity coupling.
- 5. Boundary conditions (most common types):
 - 1. walls and inlets;
 - 2. outlets;
 - 3. open boundaries.

Governing equations for incompressible flow

Continuity equation:

$$\nabla \cdot \vec{U} = 0;$$

Navier — Stokes equations:

$$\frac{\partial \rho \vec{U}}{\partial t} + \nabla \cdot (\rho \vec{U} \otimes \vec{U}) = -\nabla p + \nabla \cdot \hat{\tau} + \rho \vec{g};$$

where $\hat{\tau} = \mu(\nabla \vec{U} + \nabla \vec{U}^T)$ — viscous stress tensor;

boundary conditions on the interface:

$$[-p\mathbf{I} + \hat{\tau}] \cdot \vec{n} = \sigma \kappa \vec{n}; \qquad [\vec{U}] = 0.$$

 initial and boundary conditions on the flow region boundaries (different types — walls, inlets, outlets, open boundaries).

Volume of Fluid

Add a volume fraction function:

$$\alpha_1 = \begin{cases} 1 \text{ if cell full of liquid;} \\ 0 \text{ if cell full of gas;} \\ (0; 1) \text{ if cell is on the interface.} \end{cases}$$

For two phases

$$\alpha_1 + \alpha_2 = 1.$$

Solve a transport equation for this function:

$$\frac{\partial \alpha_1}{\partial t} + \nabla \cdot (\vec{U}\alpha_1) + \nabla \cdot (\vec{U}_R \alpha_1 \alpha_2) = 0,$$

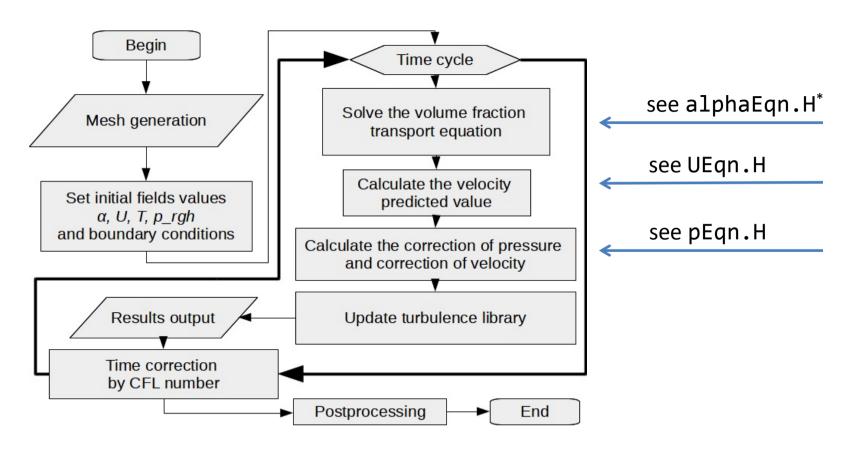
where $\vec{U} = \alpha_1 \vec{U}_1 + \alpha_2 \vec{U}_2$ — mixture velocity;

$$ec{U}_R = ec{U}_1 - ec{U}_2$$
 — velocity field suitable to compress the interface.

0	0	0		0	0	0
0	0	0		0	0	0
0	0	0		0	0	0
0.8	0.9	0.5		0	0	0
1	1	1	4).2	0	0
1	1	1	Ø).2	0	0

Approximation: Finite Volume Method

Solution process



Location: OpenFoam-3.0.0/applications/solvers/multiphase/interFoam

Modified Navier — Stokes equations

Surface tension forces considered as an additional term $\rho \vec{F}$ in Navier — Stokes equation*:

$$\frac{\partial \rho \vec{U}}{\partial t} + \nabla \cdot (\rho \vec{U} \otimes \vec{U}) = -\nabla p + \nabla \cdot \hat{\tau} + \rho \vec{g} + \rho \vec{F}.$$

Use modified pressure:

$$p^* = p - \rho(\vec{q} \cdot \vec{r}).$$

Its gradient:

$$\nabla p^* = \underline{\nabla p} - (\nabla \rho)(\vec{g} \cdot \vec{r}) - \rho \vec{g}.$$

Navier — Stokes equations in terms of modified pressure:

$$\frac{\partial \rho \vec{U}}{\partial t} + \nabla \cdot (\rho \vec{U} \otimes \vec{U}) - \nabla \cdot \hat{\tau} = -\nabla p^* - (\nabla \rho)(\vec{g} \cdot \vec{r}) + \rho \vec{F}.$$

Approximation of surface tension forces — by **volume fraction gradient**:

$$\vec{F} \approx \sigma \kappa \nabla \alpha_1.$$

Pressure-velocity coupling

Use velocity as sum of prediction and correction parts:

$$\vec{U} = \vec{U}^* + \vec{U}'. \tag{*}$$

Semi-discrete form of momentum equation:

$$A\vec{U} = H - \nabla p - (\nabla \rho)(\vec{g} \cdot \vec{r}) + \rho \vec{F}.$$

Here A is the diagonal part of initial matrix system,

 ${\cal H}$ is the non-diagonal part of matrix + r.h.s. without pressure gradient and terms for gravity and surface tension.

We can write comparing with the velocity splitting (*):

$$\vec{U}^* = A^{-1}H,$$

$$\vec{U}' = -A^{-1}\nabla p^* - A^{-1}(\nabla \rho)(\vec{g} \cdot \vec{r}) + A^{-1}\rho \vec{F}.$$

Continuity equation in the discrete form:

$$\int_{V} \nabla \cdot \vec{U} \, dV = \int_{S} \vec{U} \cdot \vec{n} \, dS \approx \sum_{f} \underbrace{\vec{U}_{f} \cdot \vec{S}_{f}}_{\phi_{f}} = 0 \Rightarrow \sum_{f} \phi_{f} = 0.$$
 (**)

Pressure-velocity coupling

Let's calculate fluxes through one face f by Finite Volume method:

$$\underbrace{\vec{U}_f \cdot \vec{S}_f}_{\phi} = \underbrace{(\vec{U}^*)_f \cdot \vec{S}_f}_{\phi_{H/A}} - \underbrace{(A^{-1})_f}_{Dp} (\nabla p^*)_f \cdot \vec{S}_f - \underbrace{(A^{-1})_f (\nabla p^*)_f \cdot \vec{S}_f}_{Dp} \cdot \underbrace{\vec{C}_f}_{Dp} + \underbrace{(A^{-1})_f (\nabla p)(\vec{g} \cdot \vec{r})_f \cdot \vec{S}_f}_{\phi_g} \cdot \underbrace{(A^{-1})_f (\nabla p)(\vec{r})_f \cdot \vec{S}_f}_{\phi_g} \cdot \underbrace{(A$$

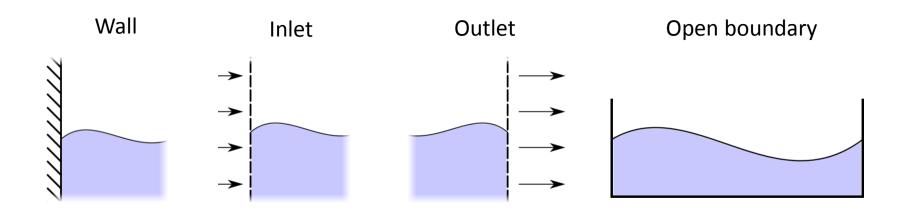
Create a **pressure equation** which is derived by continuity equation (**):

$$\sum_{f} (\phi_{H/A} + \phi_g)_f = \sum_{f} Dp(\nabla p^*)_f \cdot \vec{S}_f.$$

Pressure gradient:

$$(\nabla p^*)_f = \frac{\phi_{H/A} + \phi_g - \phi}{Dp \cdot \vec{S}_f}.$$
 (****)

Types of boundary conditions



Note

For incompressible fluids it is important to calculate correctly the pressure gradient. Absolute value of pressure is calculated with precision to a constant. So, it is enough to know the pressure "null value" only in one point.

Location: OpenFoam-3.0.0/src/finiteVolume/fields/fvPatchFields

Walls & inlets

Boundary condition for **volume fraction**:

$$\alpha = 0$$
 or $\alpha = 1$ (fixedValue).

Boundary condition for velocity:

$$\vec{U} = \{U_x \, U_y \, U_z\}$$
 (fixedValue).

Note

Capillary effects are neglected; for them — special boundary conditions for volume fraction.

Boundary conditions for **pressure** are critically important here. Let's consider the correct boundary condition and changes in OpenFOAM v.2.3.0+.

At the end of practical part — videos with the flow where BC are right or wrong.

Walls & inlets

On boundaries for walls and inlets:

$$\vec{U} = \{U_x \, U_y \, U_z\}, \quad \vec{U}^* = \{U_x \, U_y \, U_z\} \quad \Rightarrow \quad \vec{U}' = \{0 \, 0 \, 0\}.$$

According to BC for volume fraction:

$$\vec{F} \approx \sigma \kappa \nabla \alpha_1 = 0$$
 on the boundary.

So, according to expression for volumetric flux (***):

$$-Dp(\nabla p^*)_f \cdot \vec{S}_f - (A^{-1}(\nabla \rho)(\vec{g} \cdot \vec{r}))_f \cdot \vec{S}_f = 0.$$

and, therefore, we can derive boundary condition for pressure:

$$(\nabla p^*)_f = -(\nabla \rho)(\vec{g} \cdot \vec{r})_f.$$

Implementation in OpenFOAM

In *OpenFOAM v.2.2.x* — **buoyantPressure**: this expression is in the source code of boundary condition.

In *OpenFOAM v.2.3.0+* — **fixedFluxPressure**: boundary condition is satisfied automatically by pressure gradient (****) calculating in the solver's source code.

Open boundaries

Boundary condition for volume fraction:

$$\nabla \alpha_1 = 0$$
 (zeroGradient).

Boundary condition for **velocity** — pressureInletOutletVelocity:

- positive flux (out of cell): apply zero-gradient condition;
- negative flux (into cell): derive from the flux in the patch-normal direction and the tangential patch velocity (optionally).

Boundary condition for **pressure** — derive the "null level" of pressure according to Bernoulli's principle:

$$p_p^* = p_0 - rac{U^2}{2}$$
 (totalPressure),

where p_0 — total pressure, U — velocity magnitude.

According to BC for velocity in the source code we use:

$$p = p0 - 0.5*(1 - pos(phi))*magSqr(U).$$

Here pos() is the boolean function which equals to 1 when the flux phi>0.

Outlets

Boundary condition for **volume fraction**:

$$\nabla \alpha_1 = 0$$
 (zeroGradient).

Boundary condition for **velocity**:

$$\nabla \vec{U} = 0$$
 (zeroGradient).

Boundary condition for **pressure**:

- "null level" of pressure if there are no pressure boundary conditions in any another boundary (totalPressure);
- zeroGradient if you have some another boundary (for example, open boundary) with derived "null level" of pressure.

Part II

Practical part: hands-on training

Spillway tutorial

Stages of solution

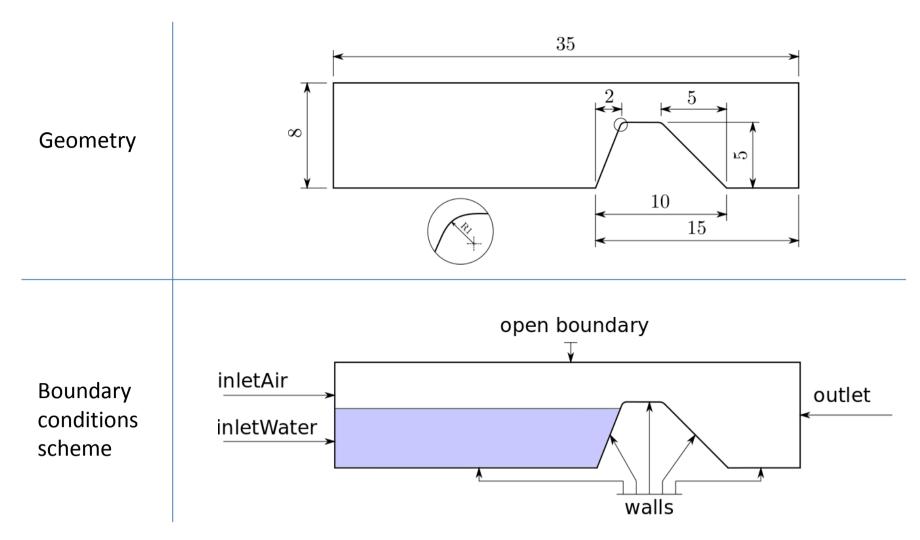
- **1. Geometry**: make STL-surface to draw the dam (in SALOME).
- **2. Liquid/gas properties**: write density, kinematic viscosity...
- **3.** Mesh generation:
 - a) blockMesh: create a "0" level of mesh;
 - b) snappyHexMesh: refine mesh near the dam surface;
 - c) extrudeMesh: make a 2D-mesh for fast calculations.
- **4. Boundary conditions**: describe it into files in "0.org" folder.
- **5. Set fields**: put initial liquid regions into the flow region.
- **6.** Numerical settings:
 - a) describe interpolation of terms;
 - describe solvers for SLAE;
 - c) describe turbulence models.
- **7. Time settings**: write end time, CFL-number...
- **8. Running**: an interFoam command.
- **9. Post-processing**: open file <filename>.foam in Paraview.
- 10. Enjoy!

```
alpha.water
    nut
    omeda
    p rah
0.org (4)
    alpha.water
    nut
    omega
    p rgh
constant
    polyMesh
        blockMeshDict(3a)
    triSurface

    dam.stl(1)

    a
    transportProperties (2)
    turbulenceProperties (6c)
    controlDict(7)
    extrudeMeshDict (3c)
    fvSolution (6b)
    setFieldsDict (5)
    snappyHexMeshDict (3b)
spillway 3p0.foam
```

Model setup

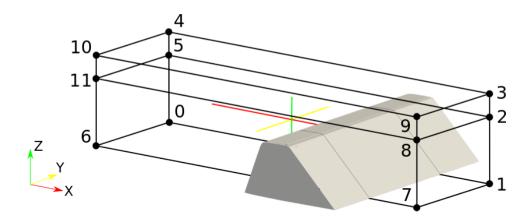


blockMesh utility

Create mesh of "0" level in the flow region and mark the boundaries.

See: constant/polyMesh/blockMeshDict

Command: blockMesh



Exercise: inspect results in Paraview.

You should see the rectangular region with the coarse mesh.

blockMesh utility

(1) Create vertices and two boxes:

```
convertToMeters 1:
vertices
    (-20 - 0.45 0)
     15 -0.45 0
     15 -0.45 6
    15 -0.45 8
    (-20 -0.45 8
    (-20 - 0.45 6)
    (-20 -0.55 0
     15 -0.55 0
     15 -0.55 6
     15 -0.55 8
    (-20 - 0.55 8)
    (-20 - 0.55 6)
blocks
    hex (0 1 2 5 6 7 8 11) (70 12 1) simpleGrading (1 1 1)
    hex (5 2 3 4 11 8 9 10) (70 4 1) simpleGrading (1 1 1)
edges
```

blockMesh utility

(2) Describe boundaries:

```
outlet
    type patch;
    faces
        (1287)
        (2398)
    );
atmosphere
    type patch;
    faces
        (3 4 10 9)
    );
bottomWall
    type wall;
    faces
        (0\ 1\ 7\ 6)
```

```
front
    type empty;
    faces
        (1052)
        (2543)
    );
back
    type empty;
    faces
        (6 7 8 11)
        (11 8 9 10)
    );
```

snappyHexMesh utility

See: constant/system/snappyHexMeshDict

Command: snappyHexMesh -overwrite

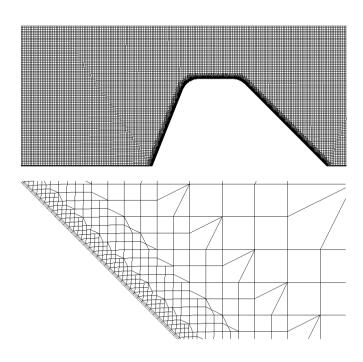
(1) Refine mesh near the surface of the dam.

Three studies of remeshing:

- refinement (see CastellatedMeshControl section);
- smoothing (see SnapControls section);
- set of layers (see addLayersControls section).

Use STL-surface to do it (it is in constant/triSurface):

```
dam.stl
{
    type triSurfaceMesh;
    name dam;
}
```



snappyHexMesh utility

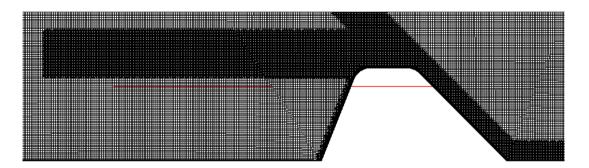
(2) Add two refinement regions where the surface of water will flow.

Use two boxes and plane to do it:

```
surface
{
    type searchableBox;
    min ( -15 -1 4.5 );
    max ( 4 0 7 );
}
```

```
outlet
{
    type searchableBox;
    min ( 10 -1 0 );
    max ( 15 0 1 );
}
```

Exercise: try to run snappyHexMesh with different studies of remeshing. Watch differences.

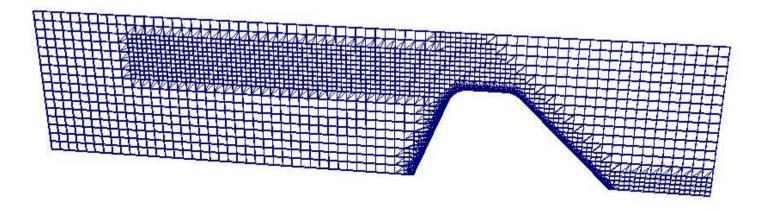


extrudeMesh utility

See: constant/system/extrudeMeshDict

Command: extrudeMesh

blockMesh and snappyHexMesh made 3D-mesh. extrudeMesh make your mesh two-dimensional.



Exercise: run checkMesh utility before running extrudeMesh and after it. Compare numbers of cells.

Boundary conditions

See: the folder 0.org/. Change needed files and copy it to folder 0/.

	α_1	k	ω	p^*	$ec{U}$	
in lat A in	fixedValue	fixedValue fixedValue		five dEl Dracere	fixedValue	
inletAir	0	2.16e-4	0.1470	fixedFluxPressure	(0 0 0)	
inletWater	fixedValue	fixedValue	fixedValue	fine dEl Due se	fixedValue	
	1	2.16e-4	0.1470	fixedFluxPressure	(0.600)	
outlet	zeroGradient	zeroGradient	zeroGradient	fixedFluxPressure	zeroGradient	
walls	C	Landon Marian		fine del monaccione	fixedValue	
	zeroGradient	kqRWallFunction	omegaWallFunction	fixedFluxPressure	(0 0 0)	
atmosphere	in lat Outlat	inletOutlet	inletOutlet	total Duoces une		
	inletOutlet	2.16e-4	0.1470	totalPressure	pressureInletOutletVelocity	
front, back,	omntv	omntu	omntv	omntu	omntv	
defaultFaces	empty	empty	empty	empty	empty	

Note

Files in 0/ folder are modified after using setFields utility.

We use the copy 0.org/ for comfortable changing of boundary conditions.

setFields utility

Set an initial distribution of fields (alpha.water) in regions. Files in 0/ folder were modified.

```
defaultFieldValues
(
    volScalarFieldValue alpha.water 0
);
regions
(
    boxToCell
    {
       box (-20 -1 0) (3 1 5);
        fieldValues
        (
            volScalarFieldValue alpha.water 1
        );
    }
);
```



Numerical and time settings. Running

See system/controlDict to create time settings:

- time interval,
- CFL number,
- write interval,
- time precision.

Settings for numerical schemes (use default settings): see system/fvSchemes and system/fvSolution.

Start application by interFoam command.

Sequence of all commands is placed into script file ./Allrun.

Clean results: ./Allclean.

Results

See videos in the folder of training track!

Summary

- We looked how interFoam works inside (in the source code).
- We talked about correct boundary conditions for free-surface flows.
- We studied how to solve cases for free-surface flows on example — Spillway tutorial.

Let's talk about training track.
Some questions?