

How To Use Free-Surface Flows in OpenFOAM v. 4.1

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Training level: Intermediate

Session type: Lecture with examples

Software stack: OpenFOAM v.4.1

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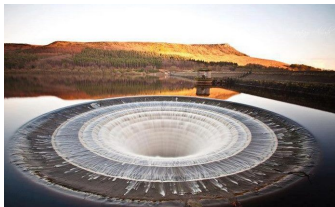
Plan of training course

1. Introduction
2. Key points of training course
3. interFoam solver: how it works
 - ▶ Governing equations
 - ▶ Volume of Fluid method
 - ▶ Solution process
 - ▶ Boundary conditions
4. Basic case: Spillway tutorial
 - ▶ Problem statement
 - ▶ Physical properties setup
 - ▶ Mesh generation
 - ▶ Boundary conditions setup
 - ▶ Numerical schemes and time advancement settings.
 - ▶ Running.
 - ▶ Results
5. Additional case: RT tutorial
 - ▶ Problem statement
 - ▶ Settings in OpenFOAM.
 - ▶ Running.
 - ▶ Results. Comparison with linear theory.
6. Conclusions and discussion

Introduction

Applicability

- printing;
- engines;
- ecological cases;
- dams, spillways;
- etc.



Complexities

- large deformations of the interface;
- creation of different subregions (droplets, bubbles. . .);
- solution should:
 - ▶ be stable;
 - ▶ have small diffusivity in the interface region;
 - ▶ satisfy to conservation laws;
 - ▶ be correct in different scales;
 - ▶ require not so much resources for computations.

Key points of training course

- Look how the solver for free-surface flows works
- Study how to set boundary conditions in different versions of OpenFOAM
- Look to all stages of modeling of free-surface flows in OpenFOAM v. 4.1: from mesh generation to post-processing

Boundary conditions are critically important in the successful modeling. There are strong differences between OpenFoam 2.2.x and 2.3.0+.

The main tool: an interFoam solver in OF v. 4.1.
We will study it with Spillway tutorial: the turbulent flow of fluid

Part I

Theoretical part

interFoam: how it works

Structure of theoretical part

1. Governing equations
2. Volume of Fluid method
3. Block scheme of interFoam
4. Pressure-velocity coupling
5. Boundary conditions (most common types):
 - ▶ walls and inlets;
 - ▶ outlets and open boundaries;
 - ▶ planes of symmetry.

Governing equations for incompressible flow

- Continuity equation:

$$\nabla \cdot \mathbf{U} = 0;$$

- Navier — Stokes equations:

$$\frac{\partial(\rho \mathbf{U})}{\partial t} + \nabla \cdot (\rho \mathbf{U} \otimes \mathbf{U}) = -\nabla p + \nabla \cdot \hat{\tau} + \rho \mathbf{g},$$

where $\hat{\tau} = \mu(\nabla \mathbf{U}^T + \nabla \mathbf{U})$ is the viscous stress tensor;

- boundary conditions on the interface:

$$[-p\mathbf{I} + \hat{\tau}] \cdot \mathbf{n} = \sigma \kappa \mathbf{n}, \quad [\mathbf{U}] = 0;$$

- initial and boundary conditions on the flow region boundaries (different types — walls, inlets, outlets, open boundaries and other).

Volume of Fluid method

Add a volume fraction function:

$$\alpha_1 = \begin{cases} 1 & \text{if cell full of liquid;} \\ 0 & \text{if cell full of gas;} \\ (0; 1) & \text{if cell is placed on the interface;} \end{cases}$$

For two phases

$$\alpha_1 + \alpha_2 = 1.$$

Solve a transport equation for this function:

$$\frac{\partial \alpha_1}{\partial t} + \nabla \cdot (\mathbf{U} \alpha_1) + \nabla \cdot (\mathbf{U}_R \alpha_1 \alpha_2) = 0,$$

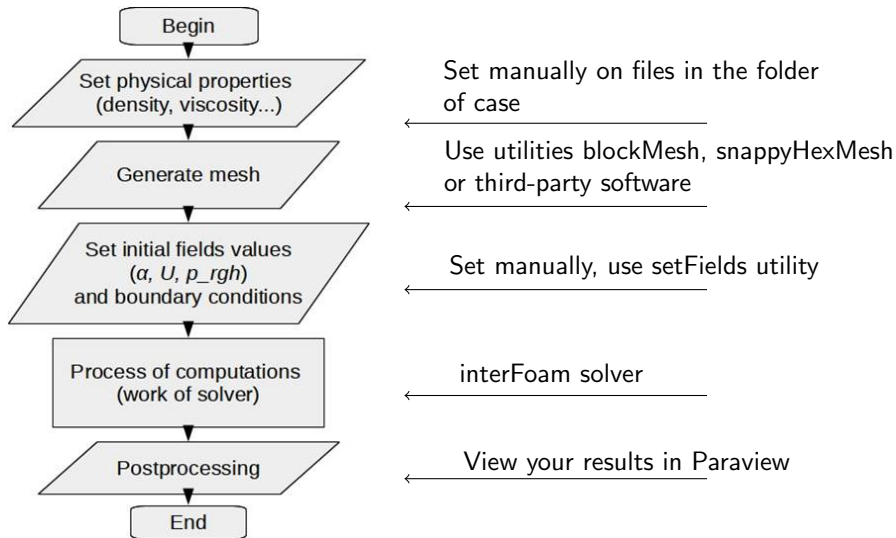
where $\mathbf{U} = \alpha_1 \mathbf{U}_1 + \alpha_2 \mathbf{U}_2$ — velocity of mixture;

$\mathbf{U}_R = \mathbf{U}_1 - \mathbf{U}_2$ — velocity field suitable to compress the interface.

0	0	0	0	0	0
0	0	0	0	0	0
0	0	0	0	0	0
0.8	0.9	0.5	0	0	0
1	1	1	0.2	0	0
1	1	1	0.2	0	0

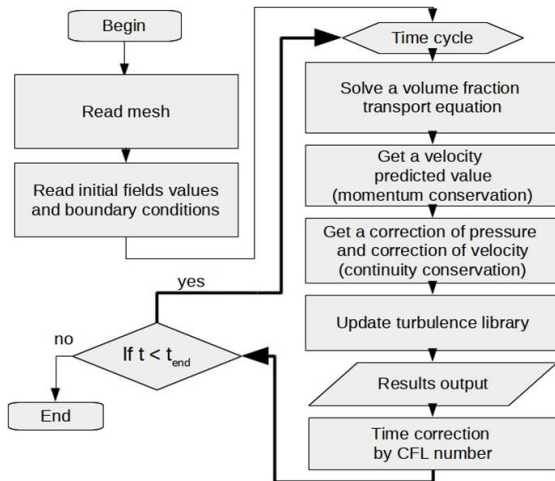
Approximation: **Finite Volume Method**

Solution process



interFoam solver

Block scheme



see `alphaEqn.H`¹

←

see `UEqn.H`

←

see `pEqn.H`

←

Location: `OpenFoam-4.1/applications/solvers/multiphase/interFoam`

¹see slide 8

interFoam solver

Modified Navier — Stokes equations

Surface tension forces are approximated as an additional term \mathbf{F}_σ in Navier — Stokes equation²:

$$\frac{\partial(\rho\mathbf{U})}{\partial t} + \nabla \cdot (\rho\mathbf{U} \otimes \mathbf{U}) = -\nabla p + \nabla \cdot \hat{\tau} + \rho\mathbf{g} + \mathbf{F}_\sigma.$$

Use modified pressure:

$$p^* = p - \rho(\mathbf{g} \cdot \mathbf{r}).$$

Its gradient:

$$\nabla p^* = \nabla p - (\nabla \rho)(\mathbf{g} \cdot \mathbf{r}) - \rho\mathbf{g}.$$

Approximation of surface tension forces — by volume fraction gradient:

$$\mathbf{F}_\sigma \approx \sigma \kappa \nabla \alpha_1.$$

²see slide 7

interFoam solver I

Pressure-velocity coupling

Use velocity as sum of prediction and correction parts:

$$\mathbf{U} = \mathbf{U}^* + \mathbf{U}'.$$
 (1)

Semi-discrete form of momentum equation:

$$A\mathbf{U} = H - \nabla p^* - (\nabla \rho)(\mathbf{g} \cdot \mathbf{r}) + \mathbf{F}_\sigma.$$

Here A is the diagonal part of initial matrix system,
 H is the non-diagonal part of matrix + r.h.s. without diagonal part of initial matrix system, pressure gradient and terms for gravity and surface tension.

We can write comparing with the velocity splitting (1):

$$\mathbf{U}^* = A^{-1}H;$$

$$\mathbf{U}' = -A^{-1}\nabla p^* - A^{-1}(\nabla \rho)(\mathbf{g} \cdot \mathbf{r}) + A^{-1}\mathbf{F}_\sigma.$$

interFoam solver II

Pressure-velocity coupling

Continuity equation in the discrete form:

$$\int_V \nabla \cdot \mathbf{U} dV = \int_S \mathbf{U} \cdot \mathbf{n} dS \approx \sum_f \underbrace{\mathbf{U}_f \cdot \mathbf{S}_f}_{\varphi_f} = 0, \quad (2)$$

consequently,

$$\boxed{\sum_f \varphi_f = 0.} \quad (3)$$

Let's calculate fluxes through one face f :

$$\underbrace{\mathbf{U}_f \cdot \mathbf{S}_f}_{\varphi} = \underbrace{\mathbf{U}_f^* \cdot \mathbf{S}_f}_{\varphi_{H/A}} - \underbrace{(A^{-1})_f (\nabla p^*)_f \cdot \mathbf{S}_f}_{D_p} - \underbrace{(A^{-1}(\nabla \rho)(\mathbf{g} \cdot \mathbf{r}))_f \cdot \mathbf{S}_f + (A^{-1} \mathbf{F}_\sigma)_f}_{\varphi_g}. \quad (4)$$

interFoam solver III

Pressure-velocity coupling

Create a **pressure equation** which is derived from continuity equation (3):

$$\sum_f (\varphi_{H/A} + \varphi_g) = \sum_f D_p (\nabla p^*)_f \cdot \mathbf{S}_f.$$

Pressure gradient:

$$(\nabla p^*)_f = \frac{\varphi_{H/A} + \varphi_g - \varphi}{D_p \cdot \mathbf{S}_f}. \quad (5)$$

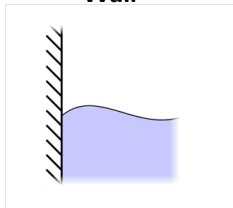
In the source code:

```
phiHbyA = phiHbyA + phig;  
snGrad(p_rgh) = (phiHbyA - phi) / (rAUf * Sf).
```

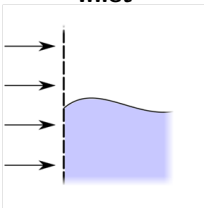
interFoam solver

Types of boundary conditions

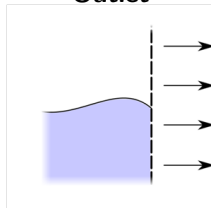
Wall



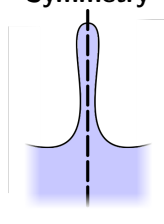
Inlet



Outlet



Symmetry



Note

For incompressible fluids it is important to calculate correctly the pressure gradient. Absolute value of pressure is calculated up to a constant. So, it is enough to know the pressure reference value only in one point.

Location: `OpenFoam-4.1/src/finiteVolume/fields/fvPatchFields`

interFoam solver I

Walls & inlets

Boundary condition for **volume fraction**:

$$\alpha = 0 \text{ or } \alpha = 1 \text{ (fixedValue) — for inlets;}$$
$$\nabla \alpha = 0 \text{ (zeroGradient) — for walls.}$$

Boundary condition for **velocity**:

$$\mathbf{U} = \{U_x; U_y; U_z\} \text{ (fixedValue).}$$

Note

Capillary effects are neglected; to account for these effects — special boundary conditions for volume fraction must be imposed.

Boundary conditions for **pressure** are critically important here.

Let's consider the correct boundary condition and changes in OpenFOAM v.2.3.0+.

interFoam solver II

Walls & inlets

On boundaries for walls and inlets:

$$\mathbf{U} = \{U_x; U_y; U_z\}, \quad \mathbf{U}^* = \{U_x; U_y; U_z\} \Rightarrow \mathbf{U}' = \{0; 0; 0\}.$$

According to BC for volume fraction:

$$\mathbf{F}_\sigma \approx \sigma \kappa \nabla \alpha_1 = 0 \text{ on the boundary.}$$

So, according to expression for volumetric flux (4):

$$-D_p(\nabla p^*)_f \cdot \mathbf{S}_f - (A^{-1}(\nabla \rho)(\mathbf{g} \cdot \mathbf{r}))_f \cdot \mathbf{S}_f = 0,$$

and, therefore, we can derive boundary condition for pressure:

$$(\nabla p^*)_f = -((\nabla \rho)(\mathbf{g} \cdot \mathbf{r}))_f.$$

interFoam solver III

Walls & inlets

Implementation in OpenFOAM

In OpenFOAM v.2.2.x — `buoyantPressure`: this expression is in the source code of boundary condition.

In OpenFOAM v.2.3.0+ — `fixedFluxPressure`: boundary condition is satisfied automatically by pressure gradient (5), calculating in the solver's source code.

interFoam solver I

Outlets

Boundary condition for **volume fraction**:

$$\nabla \alpha = 0 \text{ (zeroGradient)}.$$

Boundary condition for **velocity**:

$$\nabla \mathbf{U} = 0 \text{ (zeroGradient)}.$$

Boundary condition for **pressure**:

- reference level of pressure — if there are no pressure boundary conditions in any another boundary (typically means “atmosphere”):

$$p_p^* = p_0 - \frac{U^2}{2} \text{ (totalPressure)},$$

where p_0 — total pressure, U — velocity magnitude.

interFoam solver II

Outlets

In the source code we use:

$$p = p0 - 0.5*(1 - \text{pos}(\phi))*\text{magSqr}(U).$$

Here `pos()` is the boolean function which equals to 1 when the flow leaves the domain, i.e. `phi>0`.

- `zeroGradient` — if you have some another boundary with derived reference level of pressure.

In case of **symmetry** just use `slip` boundary condition for all variables.

Note

Calculations of patch boundary field on the symmetry planes are performed using the Householder projection on the patch.

Part II

Practical part

Basic case: Spillway tutorial

Stages of simulation

1. Geometry: make STL-surface to draw the dam (in SALOME).
2. Liquid/gas properties: write density, kinematic viscosity ...
3. Mesh generation:
 - ▶ blockMesh: create a basic mesh box;
 - ▶ snappyHexMesh: refine mesh near the dam surface;
 - ▶ extrudeMesh: make a 2D-mesh for fast calculations.
4. Boundary conditions: define it with files in 0.org folder.
5. Set fields: set initial liquid phase volume fraction.
6. Numerical settings:
 - ▶ describe interpolation of terms;
 - ▶ describe solvers for SLAE;
 - ▶ setup turbulence models.
7. Time settings: set the end time, CFL-number ...
8. Running: an interFoam command.
9. Post-processing: open file <filename>.foam in Paraview.

Problem statement

Input data

Water:

density: 1000 kg/m^3 ;

dynamic viscosity:
 $10^{-3} \text{ Pa} \cdot \text{s}$.

Air:

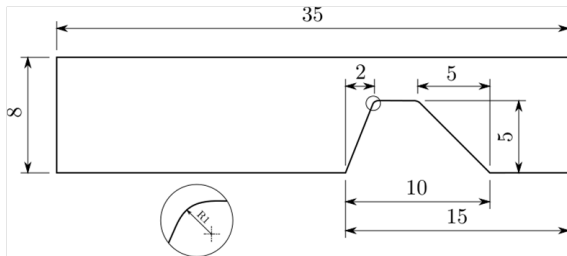
density: 1 kg/m^3 ;

dynamic viscosity:
 $1.48 \cdot 10^{-5} \text{ Pa} \cdot \text{s}$.

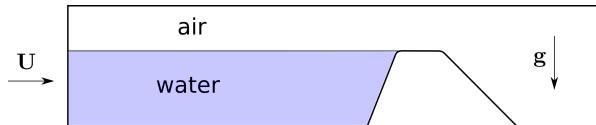
Surface tension
 coefficient: 0.07 N/m .

Inlet velocity: 0.6 m/s .

Geometry



Scheme



Physical properties I

See: folder \constant

File **transportProperties:**

- Set phases:

```
phases (water air);
```

- Set density and kinematic viscosity for each phase:

```
water
{
    transportModel    Newtonian;
    nu                nu [ 0 2 -1 0 0 0 0 ] 1e-06;
    rho               rho [ 1 -3 0 0 0 0 0 ] 1000;
}

air
{
    transportModel    Newtonian;
    nu                nu [ 0 2 -1 0 0 0 0 ] 1.48e-05;
    rho               rho [ 1 -3 0 0 0 0 0 ] 1;
}
```


Physical properties II

- Set surface tension:

```
sigma          sigma [ 1 0 -2 0 0 0 0 ] 0.07;
```

File **g**: set the value and direction of gravity

```
dimensions      [0 1 -2 0 0 0 0];  
value           (0 0 -9.81);
```

File **turbulenceProperties**: set the turbulence model

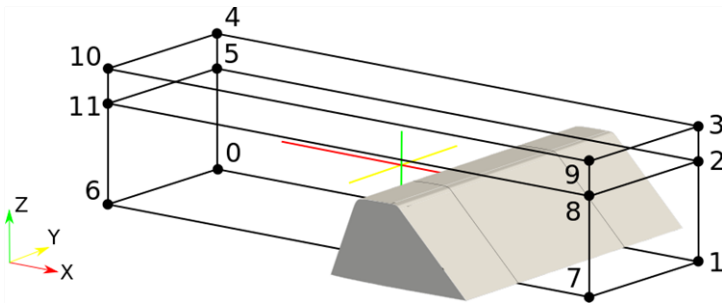
```
simulationType  RAS;  
  
RAS  
{  
    RASModel      k0megaSST;  
  
    turbulence     on;  
  
    printCoeffs    on;  
}
```

blockMesh I

Create basic coarse mesh in the flow region and mark the boundaries.

See: constant/polyMesh/blockMeshDict

Command: blockMesh



Exercise: check results in Paraview.

You should see the rectangular region with the coarse mesh

blockMesh II

- Set scale: `convertToMeters 1;`

- Set vertices:

```
vertices
(
  (-20 -0.45 0 )
  ( 15 -0.45 0 )
  ( 15 -0.45 6 )
  ( 15 -0.45 8 )
  (-20 -0.45 8 )
  (-20 -0.45 6 )
  (-20 -0.55 0 )
  ( 15 -0.55 0 )
  ( 15 -0.55 6 )
  ( 15 -0.55 8 )
  (-20 -0.55 8 )
  (-20 -0.55 6 )
);
```

- Create two boxes:

```
blocks
(
  hex (0 1 2 5 6 7 8 11) (70 12 1) simpleGrading (1 1 1)
  hex (5 2 3 4 11 8 9 10) (70 4 1) simpleGrading (1 1 1)
);
```

blockMesh III

- Define boundaries:

```
boundary
(
    inletAir
    {
        type patch;
        faces
        (
            (4 5 11 10)
        );
    }

    inletWater
    {
        type patch;
        faces
        (
            (5 0 6 11)
        );
    }
}
```

```
outlet
{
    type patch;
    faces
    (
        (1 2 8 7)
        (2 3 9 8)
    );
}

atmosphere
{
    type patch;
    faces
    (
        (3 4 10 9)
    );
}

bottomWall
{
    type wall;
    faces
    (
        (0 1 7 6)
    );
}
```

```
front
{
    type empty;
    faces
    (
        (1 0 5 2)
        (2 5 4 3)
    );
}

back
{
    type empty;
    faces
    (
        (6 7 8 11)
        (11 8 9 10)
    );
}

);
```

snappyHexMesh I

See: `constant/system/snappyHexMeshDict`

Command: `snappyHexMesh -overwrite`

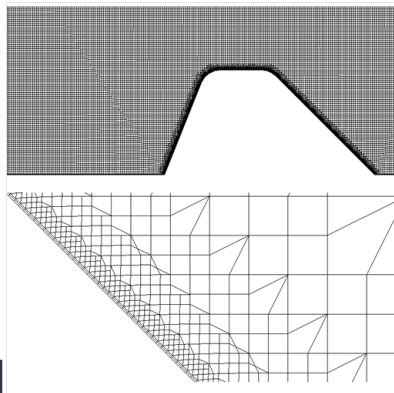
Stage 1. Refine mesh near the surface of the dam.

Three stages of meshing:

- refinement (see `CastellatedMeshControl` section);
- smoothing (see `SnapControls` section);
- set of layers (see `addLayersControls` section).

Use STL-surface to do it (see `constant/triSurface`):

```
dam.stl
{
    type triSurfaceMesh;
    name dam;
}
```



snappyHexMesh II

Stage 2. Add two refinement regions where the surface of water will flow. Use two boxes and plane to do it:

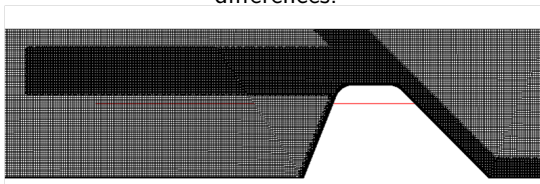
```
surface
{
    type searchableBox;
    min ( -15 -1 4.5 );
    max ( 4 0 7 );
}
```

```
aroundDam
{
    type searchablePlane;
    planeType pointAndNormal;

    pointAndNormalDict
    {
        basePoint ( 7.5 -0.5 2.5 );
        normalVector ( 1 0 1 );
    };
}
```

```
outlet
{
    type searchableBox;
    min ( 10 -1 0 );
    max ( 15 0 1 );
}
```

Exercise: try to run snappyHexMesh with different studies of remeshing. Watch differences.



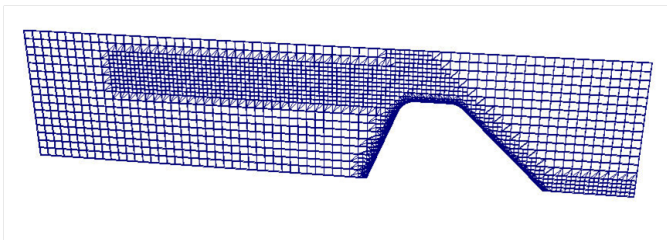
extrudeMesh

See: `constant/system/extrudeMeshDict`

Command: `extrudeMesh`

`blockMesh` and `snappyHexMesh` made 3D-mesh.

`extrudeMesh` creates a 2D-mesh from the surface (in our case — from patch).



Exercise: run `checkMesh` utility before running `extrudeMesh` and after it.
Compare numbers of cells.

Boundary conditions

See: folder 0.org/. Change needed files and copy it to folder 0/.

Name	α	k	ω	p^*	\mathbf{U}
inletAir	fixedValue 0	fixedValue 2.16e-4	fixedValue 0.1470	fixedFlux Pressure	fixedValue (0 0 0)
inletWater	fixedValue 1	fixedValue 2.16e-4	fixedValue 0.1470	fixedFlux Pressure	fixedValue (0.6 0 0)
outlet	zero Gradient	zero Gradient	zero Gradient	fixedFlux Pressure	zero Gradient
walls	kqRWall Function	omegaWall Function	zero Gradient	fixedFlux Pressure	fixedValue (0 0 0) pressure Inlet Outlet Velocity
atmosphere	inletOutlet	inletOutlet 2.16e-4	inletOutlet 0.1470	total Pressure	
front,back, defaultFaces	empty	empty	empty	empty	empty

setFields

Set an initial distribution of fields (`alpha.water`) in regions.
Files in `0/` folder were modified.

```
defaultFieldValues
(
    volScalarFieldValue alpha.water 0
);

regions
(
    boxToCell
    {
        box (-20 -1 0) (3 1 5);
        fieldValues
        (
            volScalarFieldValue alpha.water 1
        );
    }
);
```



Numerical schemes and time settings. Running simulation

See `system/controlDict` to create time settings:

- time interval,
- CFL number,
- write interval,
- time precision.

Settings for numerical schemes (use default settings): see `system/fvSchemes` and `system/fvSolution`.

Start application by `interFoam` command.

Scripts

Sequence of all commands is placed into script file `./Allrun`.

Clean results: `./Allclean`.

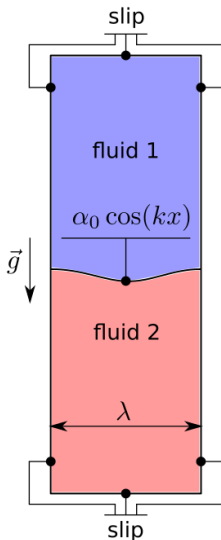
Results

Part II

Practical part

Additional case: Rayleigh — Taylor instability

Problem statement



Input data

Fluid 1:

density: 1.255 kg/m^3 ;

dynamic viscosity: $3.13 \cdot 10^{-3} \text{ Pa}\cdot\text{s}$.

Fluid 2:

density: 0.032 kg/m^3 ;

dynamic viscosity: $3.13 \cdot 10^{-3} \text{ Pa}\cdot\text{s}$.

Surface tension coefficient: 0.01 N/m .

Interface form: $\alpha_0 = 0.05 \text{ m}$, $k = 2\pi$.

Wave length: $\lambda = 1 \text{ m}$.

Linear theory

Instability conditions

1. Initial perturbation: $\alpha > 0$, $\alpha \ll \lambda$.
2. Surface tension coefficient: $\sigma < \sigma_c$, $\sigma_c = \frac{\Delta \rho g}{k^2}$.
3. Dynamic viscosities: $\mu_1 = \mu_2 = \mu$.

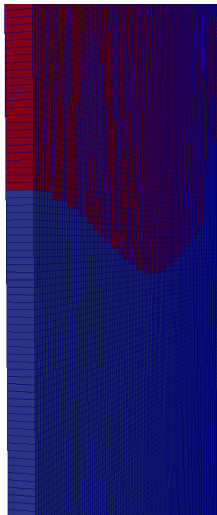
Law for growth of amplitude instability

$$\alpha(t) = \alpha_0 \cosh(\Gamma t),$$

where Γ — growth rate (1/s), A — Atwood number (non-dimensional):

$$\Gamma = \sqrt{kg \left(A - \frac{k^2 \sigma}{g(\rho_1 + \rho_2)} \right)}; \quad A = \frac{\rho_2 - \rho_1}{\rho_2 + \rho_1}.$$

OpenFOAM case



General settings

Mesh: one block, uniform mesh, no refinement.

Boundary conditions: slip for all variables.

Transport properties: set density and kinematic viscosity for two fluids.

Turbulence properties: laminar flow.

Numerical settings: standard interFoam settings.

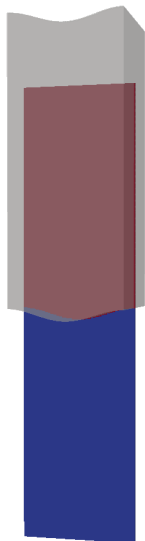
How to set up the interface

Different ways to set up the initial perturbation:

1. use STL surface in standard setFields utility;
2. use funkySetFields utility from swak4Foam library.

OpenFOAM case

setFields



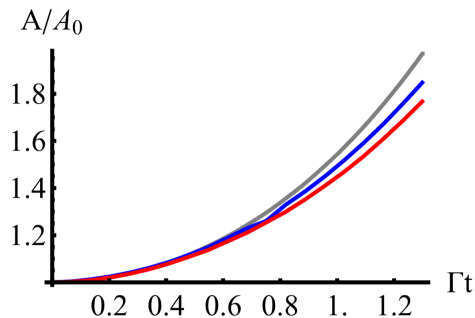
Source code for STL in setFields

```
regions
(
    surfaceToCell
    {
        file            "liquid.stl";
        useSurfaceOrientation false; // use closed surface inside/outside
                                   // test (ignores includeCut,
                                   // outsidePoints)
        outsidePoints    ((1e-4 0 -1.04)); // definition of outside
        includeCut        true;             // cells cut by surface
        includeInside     true;             // cells not on outside of surf
        includeOutside    false;           // cells on outside of surf
        nearDistance      -1;              // cells with centre near surf
                                   // (set to -1 if not used)
        curvature         -100;            // cells within nearDistance
                                   // and near surf curvature
                                   // (set to -100 if not used)

        fieldValues
        (
            volScalarFieldValue alpha.liquid 1
            volVectorFieldValue U            (0 0 0)
        );
    }
);
```

STL surface should be placed in the case folder.

Results



Gray color — linear theory

Blue color — Gerris³

Red color — OpenFOAM

³open-source code for free-surface flows, see

http://gfs.sourceforge.net/wiki/index.php/Main_Page

Summary

- We looked how `interFoam` works (look in the source code).
- We learned how to set boundary conditions for free-surface flows.
- We studied how to solve cases for free-surface flows step-by-step on the basic example — Spillway tutorial.
- We get the first experience in linear theory of hydrodynamic instabilities and run the additional case — RT instability

Let's talk about training track.
Questions?