

Table 2-50 Chemical Reactions and Heats of Combustion Involved in the Incomplete Combustion of Pure Combustible Materials

Heat of combustion,* Btu per	lb	gross	Reaction	Combustible material	Reaction	lb-mole	gross	cu ft†
691.0	16.245	260.580	$\text{C} + \frac{1}{2}\text{O}_2 = \text{CO}$	Carbon to carbon monoxide	$\text{CH}_4 + \frac{1}{2}\text{O}_2 = \text{CO} + 2\text{H}_2\text{O}$	1	16.245	†
41.0	856	14,380	$\text{CH}_4 + \frac{1}{2}\text{O}_2 = \text{CO} + 2\text{H}_2$	Methane to CO and water	$\text{CH}_4 + \text{O}_2 = \text{CO} + 2\text{H}_2$	1	856	41.0
369.8	10.812	173,440	$\text{CH}_4 + \text{O}_2 = \text{HCHO} + \text{H}_2\text{O}$	Methane to formaldehyde	$\text{CH}_4 + \text{O}_2 = \text{HCHO} + \text{H}_2\text{O}$	1	10.812	369.8
711.8	17.849	270,280	$\text{CH}_4 + \frac{3}{2}\text{O}_2 = \text{HCOOH} + \text{H}_2\text{O}$	Methane to formic acid	$\text{CH}_4 + \frac{3}{2}\text{O}_2 = \text{HCOOH} + \text{H}_2\text{O}$	1	17.849	711.8
144.8	3.385	54,300	$\text{CH}_4 + \frac{1}{2}\text{O}_2 = \text{CH}_3\text{OH}$	Methane to methyl alcohol	$\text{CH}_4 + \frac{1}{2}\text{O}_2 = \text{CH}_3\text{OH}$	1	3.385	144.8
1148.4	14.181	426,390	$\text{C}_2\text{H}_6 + \frac{5}{2}\text{O}_2 = 2\text{CO} + 3\text{H}_2\text{O}$	Ethane to CO	$\text{C}_2\text{H}_6 + \frac{5}{2}\text{O}_2 = 2\text{CO} + 3\text{H}_2\text{O}$	1	14.181	1148.4
432.0	5.655	170,030	$\text{C}_2\text{H}_6 + \text{O}_2 = \text{CH}_3\text{CHO} + \text{H}_2\text{O}$	Ethane to acetaldehyde	$\text{C}_2\text{H}_6 + \text{O}_2 = \text{CH}_3\text{CHO} + \text{H}_2\text{O}$	1	5.655	432.0
192.0	2.159	64,900	$\text{C}_2\text{H}_6 + \frac{1}{2}\text{O}_2 = \text{C}_2\text{H}_5\text{OH}$	Ethane to ethyl alcohol	$\text{C}_2\text{H}_6 + \frac{1}{2}\text{O}_2 = \text{C}_2\text{H}_5\text{OH}$	1	2.159	192.0

* Calculated by subtracting the heat of combustion of the unburned product of reaction from the heat of reaction to complete combustion.
† All volumes corrected to 60 F, 30-in. Hg dry.
‡ See Table 2-59.

the temperature and pressure of the gas, composition of the gas, and amount of heat lost thru the compressor walls.

Atomic or Nuclear Energy.† The energy released in a nuclear pile appears as the kinetic energy of the fragments of the fission of uranium and thorium atoms. The fragments are charged electrically and give off a portion of their energy to the negative particles of each of the atoms thru which they travel. Their kinetic energy is dissipated in speeding up the atoms surrounding them and is converted to heat.

It is this heat which is utilized in generating power from nuclear reactions.

Combustion Reactions

Combustion data presented in Tables 2-59, 2-63, and 2-89 are based on perfect combustion. In practical applications, excess air is usually present, and therefore complete combustion is the more appropriate term. Gas appliance performance standards as established in American Standard Ap-
proval Requirements, ASHRAE Committee Z21, permit slight but stated departures from "complete combustion." For most appliances, the limit of carbon monoxide which may be present in the dry, air-free flue products is 0.04 per cent. Some types of appliances have limits which vary slightly above or below this figure because of low input rates, intermittent operation, and general operating conditions. These limits for flue gas composition ensure that the maximum amounts of CO which may develop in room air from the use of unvented gas appliances will be far below levels which might be harmful to the occupants. Vented appliances are subject to similar CO limits because of the possibility that the venting system might fail to function properly.

Incomplete or Partial Combustion. In certain industrial operations incomplete or partial combustion of the gas fuel is required; the resultant products of combustion are primarily carbon monoxide and hydrogen.

Table 2-60 presents representative chemical reactions of carbon, methane, and ethane when they are burned *incompletely*, as well as their respective calculated heats of combustion. Other hydrocarbons would react in the partial combustion process in a manner similar to methane and ethane. Products of incomplete combustion of carbon monoxide or hydrogen are not found by ordinary methods of analysis. Reactions in the combustion of hydrogen²⁸ involve

Table 2-61 Products of Incomplete Combustion^a of Three Gases With Limited Air Supply, Self-Supporting Flame, and No External Heat

Heating value of gas, Btu per cu ft	Specific gravity of gas for complete combustion	Aeration (100 per cent required for complete combustion on dry, air-free basis, per cent)	Products of combustion on dry, air-free basis, per cent	Oxal analysis:	Carbon dioxide	Unsaturated hydrocarbons	Carbon monoxide	Hydrogen	Methane	Nitrogen (100 minus sum of above)	Total	Chemical analysis:	Formaldehyde	Acetaldehyde	Clyoxal	Formic acid	Methyl alcohol	Combined nitrogen	Total
3207	0.404	534	49.5%	67.5%	3.4	0.1	9.6	9.9	76.7	67.9	100.0	0.0133	0.00302	0.00008	0.00005	0.00282	0.00106	0.00046	0.01816
49.0%	2.0	3207	49.0%	67.5%	4.6	0.3	13.5	9.6	76.7	67.9	100.0	0.0842	0.0052	0.0023	0.0028	< .006	0.00106	0.00499	0.11956

Table 2-59 Chemical Reactions and Heats of Combustion of Pure Combustible Materials

No.	Combustible material	Reaction	lb-mole	gross	net ^b	gross	net ^b	cu ft	lb of vapor (except C & S)	gross	net ^b	Heat of combustion, Btu per
1	Carbon (graphite)	$\text{C} + 0.5\text{O}_2 = \text{CO}$	1	47,460	3,950	174,000	14,500	3,950	3,950	174,000	14,500	174,000
2	Carbon (coke)	$\text{C} + \text{O}_2 = \text{CO}_2$	1	169,860	14,093	169,860	14,093	14,093	14,093	169,860	14,093	169,860
3	Graphite	$\text{C} + 0.5\text{O}_2 = \text{CO}$	1	47,460	3,950	174,000	14,500	3,950	3,950	174,000	14,500	174,000
4	Carbon monoxide	$\text{CO} + 0.5\text{O}_2 = \text{CO}_2$	1	122,400	4,347	122,400	4,347	4,347	4,347	122,400	4,347	122,400
5	Hydrogen	$\text{H}_2 + 0.5\text{O}_2 = \text{H}_2\text{O}$	1	61,095	51,623	61,095	51,623	51,623	51,623	61,095	51,623	61,095

Heat of combustion (except No. 1)
[perfect combustion (except No. 1)]

6	Methane	$\text{CH}_4 + 2\text{O}_2 = \text{CO}_2 + 2\text{H}_2\text{O}$	1	382,980	23,875	1012,324	911,454	59,755	59.0	382,980	23,875	1012,324
7	Ethane	$\text{C}_2\text{H}_6 + 3.5\text{O}_2 = 2\text{CO}_2 + 3\text{H}_2\text{O}$	1	671,190	22,323	1773,424	1622,104	74,010	41.3	671,190	22,323	1773,424
8	Propane	$\text{C}_3\text{H}_8 + 5\text{O}_2 = 3\text{CO}_2 + 4\text{H}_2\text{O}$	1	955,430	21,669	2523,824	2322,014	91,740	35.91	955,430	21,669	2523,824
9	n-Butane	$\text{C}_4\text{H}_{10} + 6.5\text{O}_2 = 4\text{CO}_2 + 5\text{H}_2\text{O}$	1	1,239,130	21,321	3270,694	3018,484	103,787	30.77	1,239,130	21,321	3270,694
10	iso-Butane	$\text{C}_4\text{H}_{10} + 6.5\text{O}_2 = 4\text{CO}_2 + 5\text{H}_2\text{O}$	1	1,236,230	21,271	3261,174	3008,964	100,176	29.77	1,236,230	21,271	3261,174
11	n-Pentane	$\text{C}_5\text{H}_{12} + 8\text{O}_2 = 5\text{CO}_2 + 6\text{H}_2\text{O}$	1	1,521,880	21,095	4019,654	3717,154	105,822	26.35	1,521,880	21,095	4019,654
12	iso-Pentane	$\text{C}_5\text{H}_{12} + 8\text{O}_2 = 5\text{CO}_2 + 6\text{H}_2\text{O}$	1	1,518,410	21,047	4010,714	3708,014	104,863	26.17	1,518,410	21,047	4010,714
13	Neopentane	$\text{C}_5\text{H}_{12} + 8\text{O}_2 = 5\text{CO}_2 + 6\text{H}_2\text{O}$	1	1,513,440	20,978	3994	3692	104,603	26.19	1,513,440	20,978	3994
14	n-Hexane	$\text{C}_6\text{H}_{14} + 9.5\text{O}_2 = 6\text{CO}_2 + 7\text{H}_2\text{O}$	1	1,803,600	20,931	4760	4407	108,806	22.82	1,803,600	20,931	4760
15	Neohexane	$\text{C}_6\text{H}_{14} + 9.5\text{O}_2 = 6\text{CO}_2 + 7\text{H}_2\text{O}$	1	1,800,620	20,966	4768,274	4415,234	108,806	22.82	1,800,620	20,966	4768,274
16	n-Heptane	$\text{C}_7\text{H}_{16} + 11\text{O}_2 = 7\text{CO}_2 + 8\text{H}_2\text{O}$	1	2,089,530	20,554	5459	5056	108,907	19.95	2,089,530	20,554	5459
17	Triptane	$\text{C}_7\text{H}_{16} + 11\text{O}_2 = 7\text{CO}_2 + 8\text{H}_2\text{O}$	1	2,086,520	20,524	5445	5042	108,907	19.95	2,086,520	20,524	5445
18	n-Octane	$\text{C}_8\text{H}_{18} + 12.5\text{O}_2 = 8\text{CO}_2 + 9\text{H}_2\text{O}$	1	2,375,400	20,796	6249	5795	111,240	17.77	2,375,400	20,796	6249
19	iso-Octane	$\text{C}_8\text{H}_{18} + 12.5\text{O}_2 = 8\text{CO}_2 + 9\text{H}_2\text{O}$	1	2,372,430	20,770	6249	5795	111,240	17.77	2,372,430	20,770	6249
20	Ethylene	$\text{C}_2\text{H}_4 + 3\text{O}_2 = 2\text{CO}_2 + 2\text{H}_2\text{O}$	1	606,910	21,636	1603,754	1502,874	71,504	44.33	606,910	21,636	1603,754
21	Propylene	$\text{C}_3\text{H}_6 + 4.5\text{O}_2 = 3\text{CO}_2 + 3\text{H}_2\text{O}$	1	888,640	21,048	2339,704	2188,404	87,390	37.41	888,640	21,048	2339,704
22	Butylene (n-Butene)	$\text{C}_4\text{H}_8 + 6\text{O}_2 = 4\text{CO}_2 + 4\text{H}_2\text{O}$	1	1,169,950	20,854	3084	2885	102,106	33.27	1,169,950	20,854	3084
23	iso-Butene	$\text{C}_4\text{H}_8 + 6\text{O}_2 = 4\text{CO}_2 + 4\text{H}_2\text{O}$	1	1,163,390	20,737	3069	2868	102,106	33.27	1,163,390	20,737	3069
24	n-Pentene	$\text{C}_5\text{H}_{10} + 7.5\text{O}_2 = 5\text{CO}_2 + 5\text{H}_2\text{O}$	1	1,453,050	20,720	3837	3585	102,106	33.27	1,453,050	20,720	3837
25	Benzene	$\text{C}_6\text{H}_6 + 7.5\text{O}_2 = 6\text{CO}_2 + 3\text{H}_2\text{O}$	1	1,420,300	18,184	3751,684	3600,524	129,724	34.63	1,420,300	18,184	3751,684
26	Toluene	$\text{C}_7\text{H}_8 + 9\text{O}_2 = 7\text{CO}_2 + 4\text{H}_2\text{O}$	1	1,704,530	18,501	4486,444	4284,814	129,003	28.68	1,704,530	18,501	4486,444
27	p-Xylene	$\text{C}_8\text{H}_{10} + 10.5\text{O}_2 = 8\text{CO}_2 + 5\text{H}_2\text{O}$	1	1,978,040	18,633	5223	4971	127,988	24.50	1,978,040	18,633	5223

* All values corrected to 60 F, 30 in. Hg dry. For gases saturated with water vapor at 60 F, deduct 1.74 per cent of the Btu value.
† Addition from net to gross heating value determined by adding 19,095 Btu per lb-mole of water in the products of combustion. Keenan, J. H., and Keyes, F. G. *Thermodynamic Properties of Steam*. New York, Wiley, 1936.
‡ "Actual" volume of gas at 60 F and 760 mm formed upon vaporization; considered deviation from perfect gas laws. Matteson, R., and Hanna, U. S. "Physical Constants of Low Boiling-Point Hydrocarbons." *Oil & Gas J.* 41: 33-7, 1942.
§ Mason, D. M., and Eakin, E. B. "Proposed Standard Method for Calculating Heating Value and Specific Gravity from Gas Composition." *A.G.A. Proc.* 1961: C6P-61-11.
|| A.G.A. *Combustion*, 3rd ed., rev. New York, A.G.A., 1938.
¶ Does not readily react in air; reaction takes place in pure oxygen. In presence of platinum catalyst: $4\text{NH}_3 + 5\text{O}_2 = 4\text{NO} + 6\text{H}_2\text{O}$.
|| Calculated from *Handbook of Chemistry and Physics*, 28th ed., p. 1436-44. Cleveland, Ohio, Chemical Rubber Co., 1945.
|| Shulman, L., ed. *Gaseous Fuels*, 2nd ed., p. 273. New York, New York, A.G.A., 1954.
|| Btu per lb-mole divided by 380.

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