

定常与非定常传热

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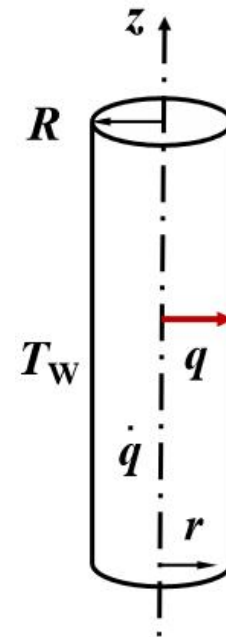
第十一讲. 定常与非定常传热

- 1. 通电导线内的温度分布**
- 2. 半无限大平壁非定常导热**
- 3. 小球非定常传热**

1. 通电导线内的温度分布

柱坐标系下的对流传热微分方程：

$$\frac{\partial T}{\partial t} + u_r \frac{\partial T}{\partial r} + \frac{u_\theta}{r} \frac{\partial T}{\partial \theta} + u_z \frac{\partial T}{\partial z} = a \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial T}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 T}{\partial \theta^2} + \frac{\partial^2 T}{\partial z^2} \right] + \frac{\dot{q}}{\rho C_p}$$



定常: $\frac{\partial T}{\partial t} = 0$

导线内: $\begin{cases} u_r = 0 \\ u_\theta = 0 \\ u_z = 0 \end{cases} \quad \begin{cases} \frac{\partial T}{\partial r} \neq 0 \\ \frac{\partial T}{\partial \theta} = 0 \\ \frac{\partial T}{\partial z} = 0 \end{cases} \quad \begin{cases} \frac{\partial^2 T}{\partial \theta^2} = 0 \\ \frac{\partial^2 T}{\partial z^2} = 0 \end{cases}$

有内热源: $\dot{q} \neq 0$

简化对流传热微分方程

$$\frac{1}{r} \frac{d}{dr} \left(r \frac{dT}{dr} \right) = -\frac{\dot{q}}{k}$$

边界条件:

$$\begin{cases} r=0, & \frac{dT}{dr}=0 \\ r=R, & T=T_w \end{cases}$$

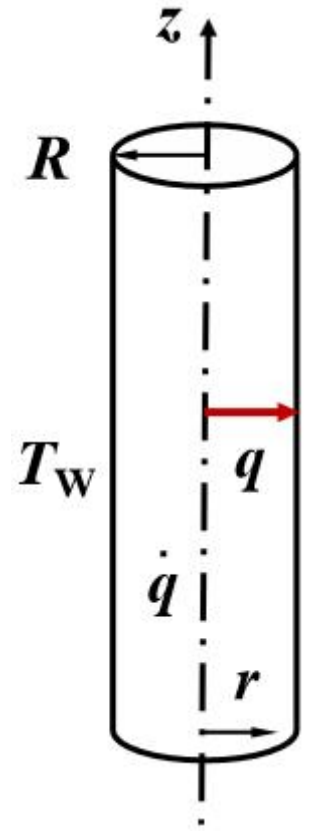
积分得:

$$r \frac{dT}{dr} = -\frac{\dot{q}}{2k} r^2 + C_1$$

$$\because r=0, \quad \frac{dT}{dr}=0; \quad \therefore C_1=0$$

通电导线内的温度分布:

$$T = T_w + \frac{\dot{q}}{4k} (R^2 - r^2)$$



过余温度分布: $T - T_w = \frac{\dot{q}}{4k} (R^2 - r^2)$

$r = 0, \quad T = T_0$ 最大温升: $T_0 - T_w = \frac{\dot{q}}{4k} R^2$

无量纲温度分布: $\frac{T - T_w}{T_0 - T_w} = 1 - \frac{r^2}{R^2}$

截面平均温度: $T_{av} = \frac{\int_0^R T 2\pi r dr}{\pi R^2} = T_w + \frac{\dot{q}}{8k} R^2$

平均温度与最大温升关系: $\frac{T_{av} - T_w}{T_0 - T_w} = \frac{1}{2}$

问题探讨

其与管内层流规律类似?

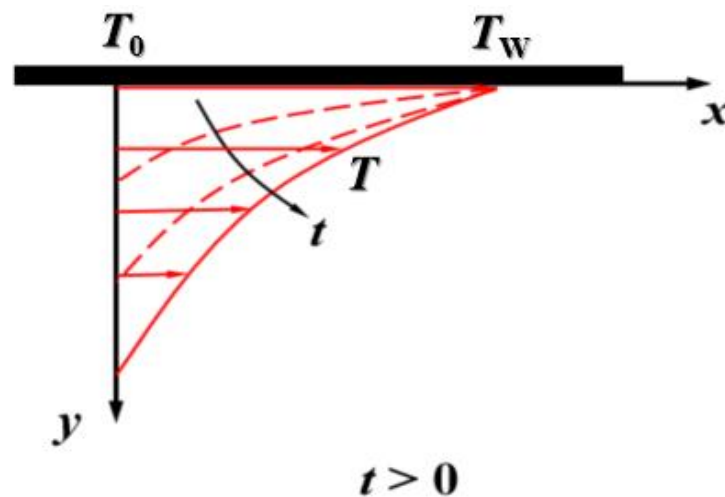
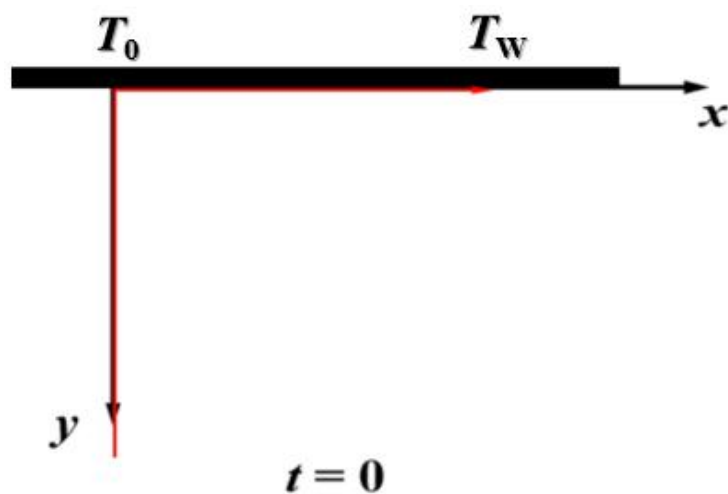
课后思考

1. 电热棒、管式固定床反应器、核燃料棒的温度分布规律？



2. 半无限大平壁非定常导热

一半无限大平壁，初始温度为 T_0 ，突然壁面温度变为 T_W ，并维持不变。平壁内的温度分布 T 随时间也发生变化。

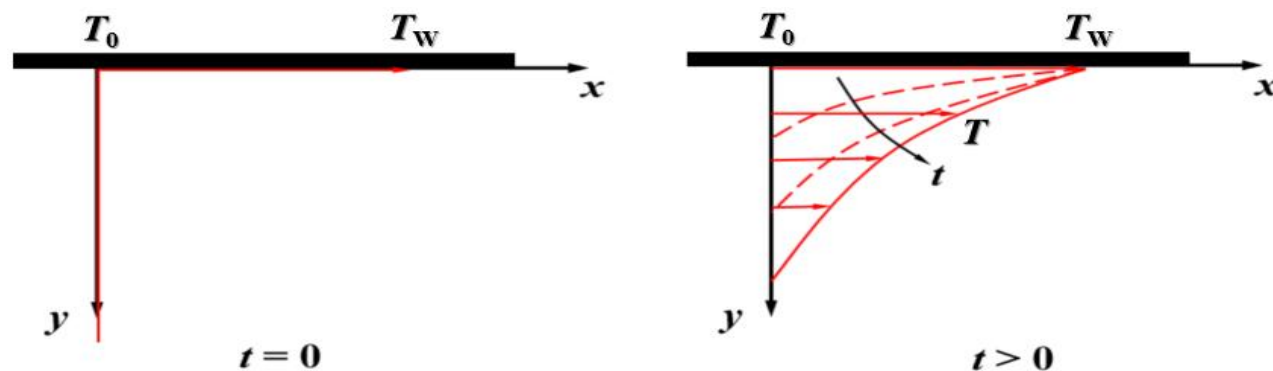


导热微分方程：

$$\rho C_p \frac{\partial T}{\partial t} = k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) + \dot{q}$$

课后自学

1.类似静止流体中的平板启动，推导半无限大平壁非定常导热数学模型为：



$$\frac{d^2 T}{d\eta^2} + 2\eta \frac{dT}{d\eta} = 0$$

边界条件：

$$\begin{cases} \eta = 0, T = T_w \\ \eta \rightarrow \infty, T = T_0 \end{cases}$$

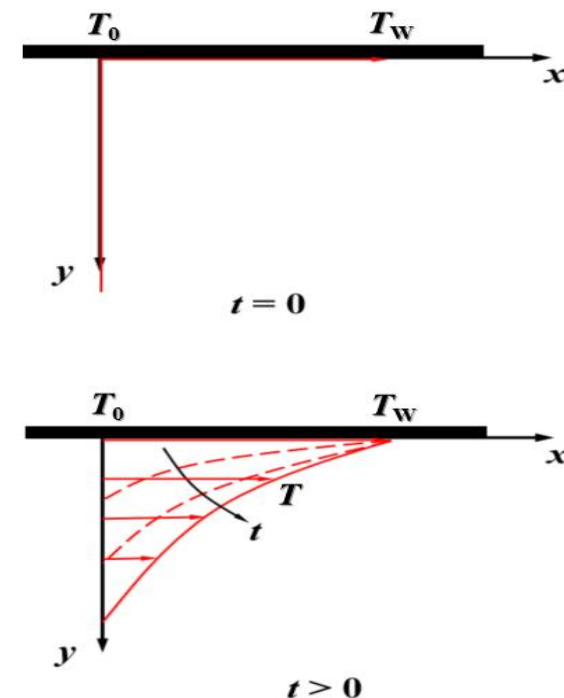
非定常: $\frac{\partial T}{\partial t} \neq 0$

一维导热:

$$\begin{cases} \frac{\partial T}{\partial x} = 0 \\ \frac{\partial T}{\partial y} \neq 0 \\ \frac{\partial T}{\partial z} = 0 \end{cases} \quad \begin{cases} \frac{\partial^2 T}{\partial x^2} = 0 \\ \frac{\partial^2 T}{\partial y^2} \neq 0 \\ \frac{\partial^2 T}{\partial z^2} = 0 \end{cases}$$

无内热源: $\dot{q} = 0$

$$\rho C_p \frac{\partial T}{\partial t} = k \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right) + \dot{q}$$

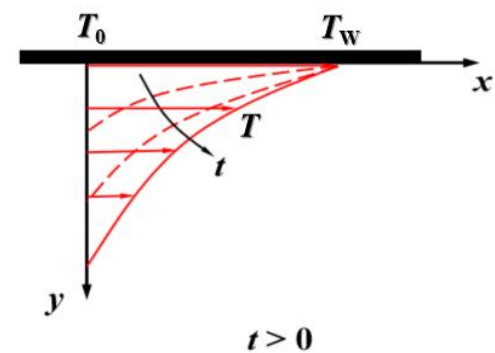
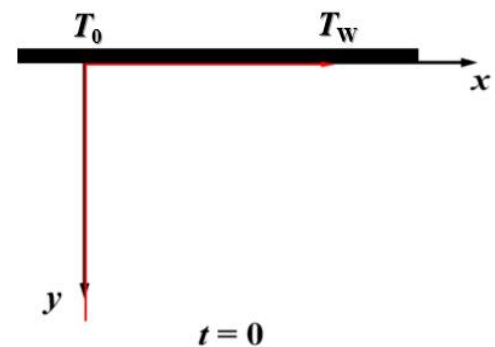


简化导热微分方程，可得：

$$\frac{\partial T}{\partial t} = a \frac{\partial^2 T}{\partial y^2}$$

初始条件： $t = 0, T = T_0$

边界条件： $t > 0, \begin{cases} y = 0, T = T_w \\ y \rightarrow \infty, T = T_0 \end{cases}$



方程为一维非定常偏微分方程：
$$\frac{\partial T}{\partial t} = a \frac{\partial^2 T}{\partial y^2}$$

令 $\eta = \frac{y}{\sqrt{4at}}$ 则
$$\frac{\partial T}{\partial t} = \frac{\partial T}{\partial \eta} \frac{\partial \eta}{\partial t} = -\frac{\eta}{2t} \frac{\partial T}{\partial \eta}$$

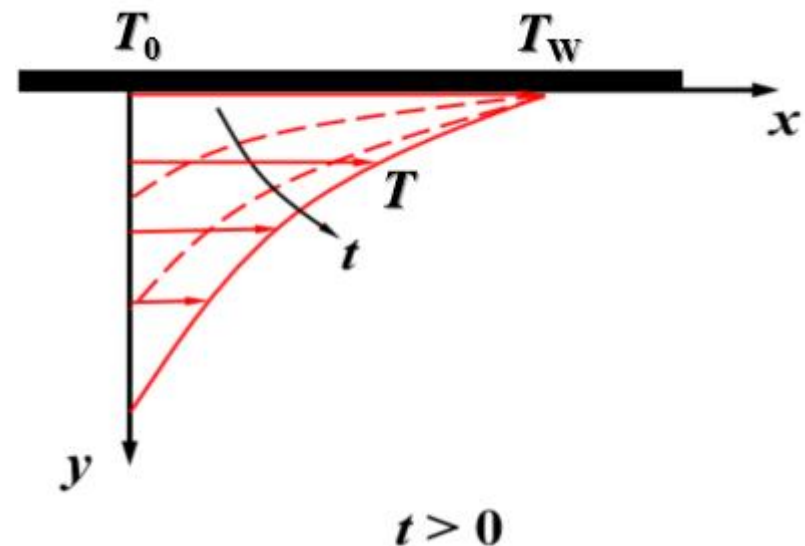
$$\frac{\partial T}{\partial y} = \frac{\partial T}{\partial \eta} \frac{\partial \eta}{\partial y} = \frac{1}{\sqrt{4at}} \frac{\partial T}{\partial \eta}$$

$$\frac{\partial^2 T}{\partial y^2} = \frac{1}{\sqrt{4at}} \frac{\partial}{\partial \eta} \frac{\partial T}{\partial \eta} \frac{\partial \eta}{\partial y} = \frac{1}{4at} \frac{\partial^2 T}{\partial \eta^2}$$

代入原方程可得：
$$\frac{d^2 T}{d\eta^2} + 2\eta \frac{dT}{d\eta} = 0$$

$$\frac{d^2 T}{d\eta^2} + 2\eta \frac{dT}{d\eta} = 0$$

边界条件：
$$\begin{cases} \eta = 0, & T = T_w \\ \eta \rightarrow \infty, & T = T_0 \end{cases}$$



解方程得温度分布：

$$\frac{T - T_w}{T_0 - T_w} = \frac{2}{\sqrt{\pi}} \int_0^\eta e^{-\eta^2} d\eta = \operatorname{erf}(\eta)$$

$$\frac{T - T_w}{T_0 - T_w} = \operatorname{erf}(\eta) \quad \text{高斯误差函数} \quad \eta = \frac{y}{\sqrt{4at}}$$

t 时刻壁面处的导热通量:

$$q_{t,y=0} = -k \frac{\partial T}{\partial y} \bigg|_{y=0} = -k \left(\frac{\partial T}{\partial \eta} \frac{\partial \eta}{\partial y} \right) \bigg|_{y=0} = \frac{k(T_w - T_0)}{\sqrt{\pi a t}}$$

$0 \sim t$ 时间内通过单位面积壁面的导热量:

$$Q = \int_0^t q_{t,y=0} dt = \int_0^t \frac{k(T_w - T_0)}{\sqrt{\pi a t}} dt = 2k(T_w - T_0) \sqrt{\frac{t}{\pi a}}$$

大地升温

若温度5°C的大地，已知：大地 $a = 4.65 \times 10^{-7} \text{ m}^2/\text{s}$ ，表面突然升至37°C。试求：

- (1). 1小时后地表面下0.05m处的温度？
- (2). $[0, t]$ 与 $[t, 2t]$ 内单位面积传热量之比。

解：(1). $\eta = \frac{y}{\sqrt{4at}} = 0.61$ 查表 $\text{erf}(\eta) \approx 0.612 = \frac{T - T_w}{T_0 - T_w}$ $T = 17.4^\circ\text{C}$

$$(2). \frac{Q_2}{Q_1} = \frac{2k(T_w - T_0) \frac{\sqrt{2t} - \sqrt{t}}{\sqrt{\pi a}}}{2k(T_w - T_0) \sqrt{\frac{t}{\pi a}}} = \sqrt{2} - 1 = 41.4\%$$

3. 小球非定常传热

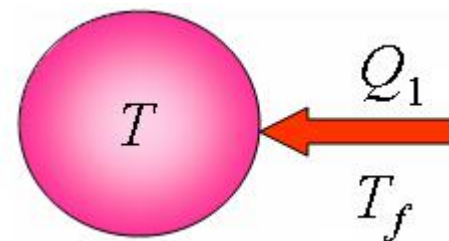
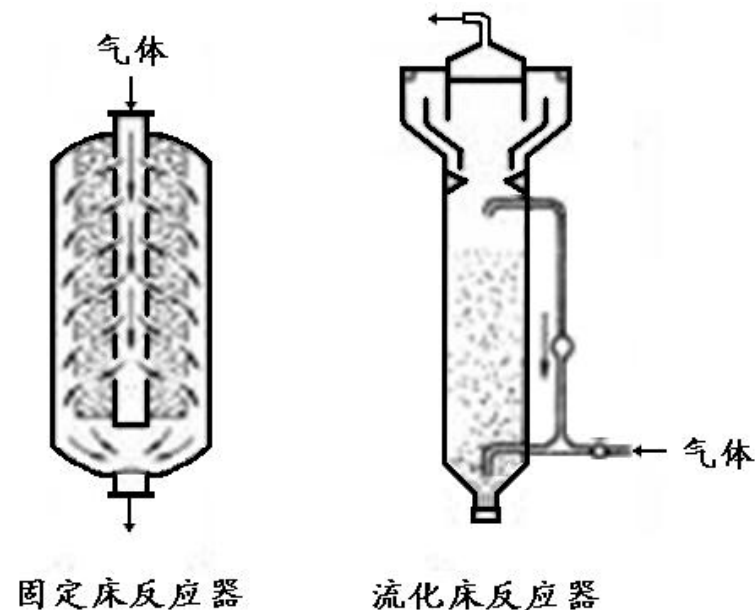
传热原理

反应器中的球形催化剂颗粒体积 V , 表面积 A , 初始温度 T_0 , 通入温度为 T_f 的热气流, 颗粒温度将随时间升高。

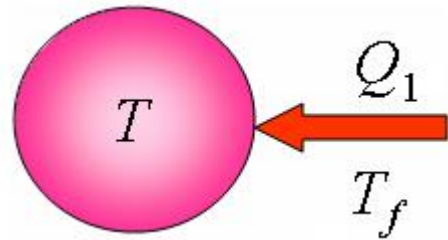
简化: 忽略颗粒内部导热热阻, 集总参数法。

毕奥数 $Bi < 0.1$

$$Bi = \frac{\frac{V}{A}/k}{1/h} = \frac{\text{内部导热热阻}}{\text{外部对流热阻}}$$



球坐标系下的对流传热微分方程：



$$\frac{\partial T}{\partial t} + u_r \frac{\partial T}{\partial r} + \frac{u_\theta}{r} \frac{\partial T}{\partial \theta} + \frac{u_\phi}{r \sin \theta} \frac{\partial T}{\partial \phi}$$
$$= a \left[\frac{1}{r^2} \frac{\partial}{\partial r} \left(r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial T}{\partial \theta} \right) + \frac{1}{r^2 \sin^2 \theta} \frac{\partial^2 T}{\partial \phi^2} \right] + \frac{\dot{q}}{\rho C_p}$$

简化得：

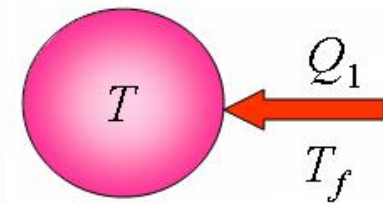
$$\frac{dT}{dt} = \frac{\dot{q}}{\rho C_p}$$

式中：

$$\dot{q} = \frac{hA(T_f - T)}{V}$$

$$\frac{dT}{dt} = \frac{hA(T_f - T)}{\rho C_p V}$$

$$\frac{dT}{dt} = \frac{hA(T_f - T)}{\rho C_p V}$$



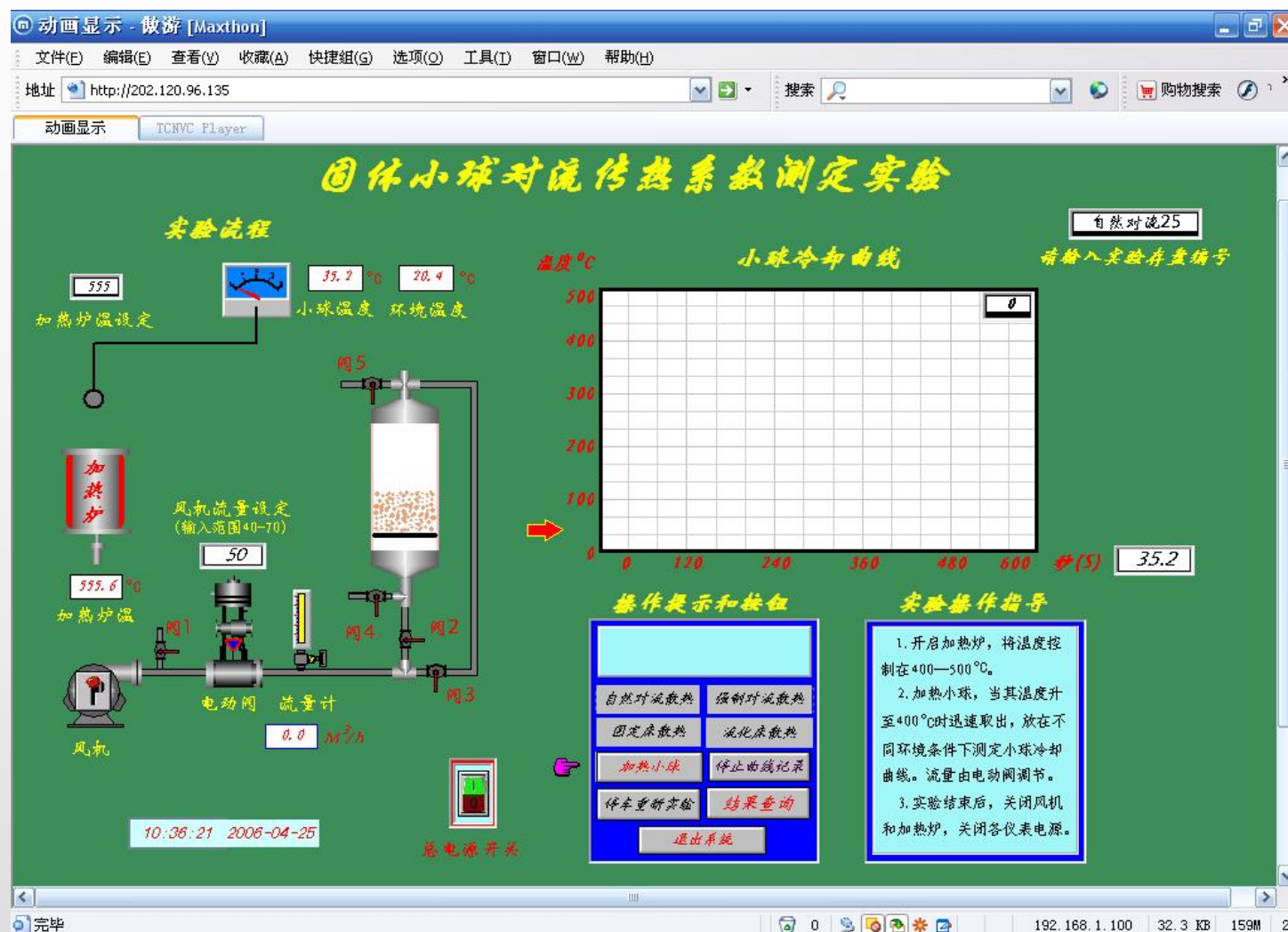
$$\int_{T_0 - T_f}^{T - T_f} \frac{d(T - T_f)}{T - T_f} = -\frac{hA}{\rho C_p V} \int_0^t dt$$

温度随时间变化关系：

$$\frac{T - T_f}{T_0 - T_f} = e^{-\frac{hA}{\rho C_p V} \cdot t}$$

小球传热专业实验

① 控制界面

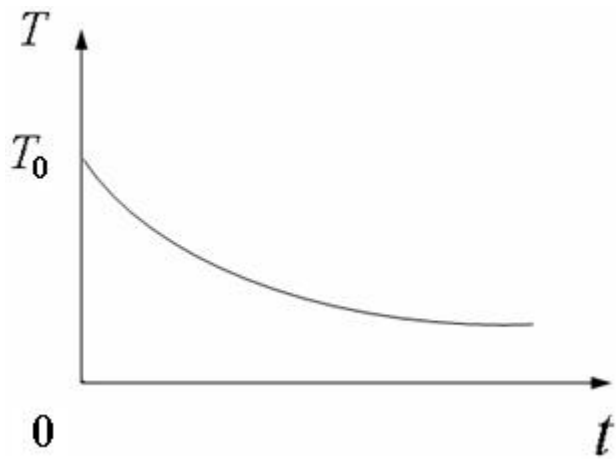


② 实验装置



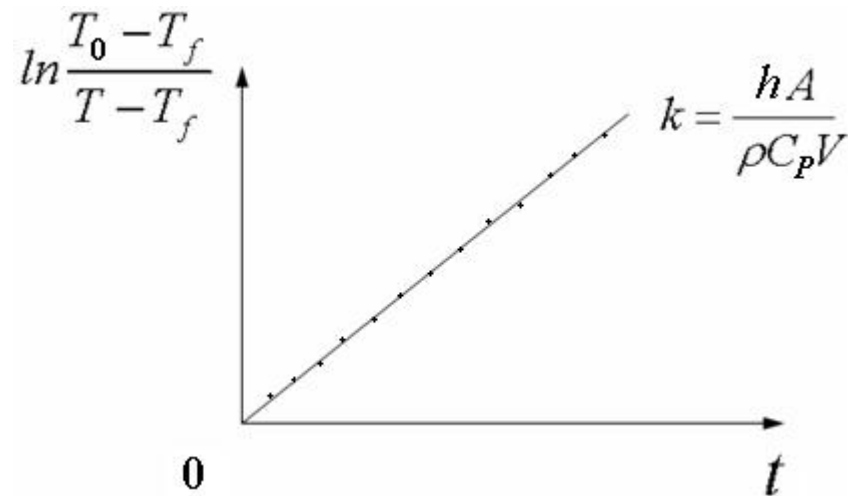
③ 实验结果讨论

小球温度随时间的变化关系



$$\frac{T - T_f}{T_0 - T_f} = e^{-\frac{hA}{\rho C_p V} \cdot t}$$

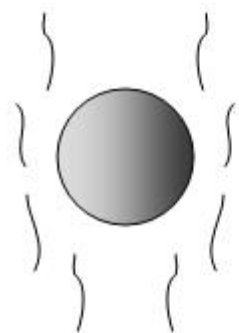
数据处理



$$\ln \frac{T_0 - T_f}{T - T_f} = -\frac{hA}{\rho C_p V} \cdot t$$

单个颗粒

自然对流



密度差引起流动

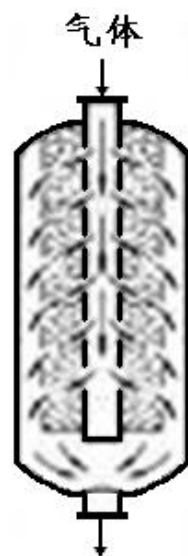


流体流速 U

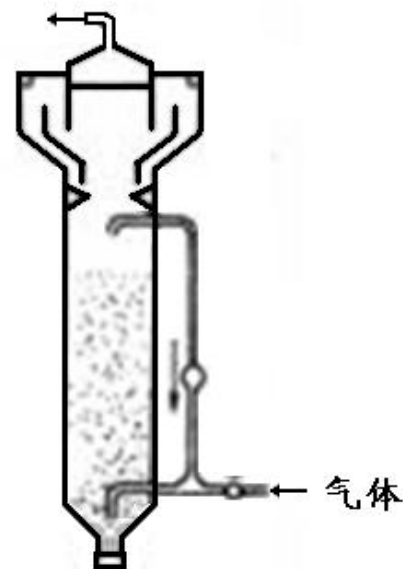
强制对流

颗粒群

固定床



固定床反应器



流化床反应器

流化床

课后思考

1. 热电偶测温原理？

2. 热电偶支架是不锈钢管，用焊接将其与小球连接，试分析对实验结果有何影响。

