模型预测控制 Model Predictive Control

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Implementation in MATLAB

Lecture 5

Coding MPC from zero in MATLAB

MPC toolbox in MATLAB

At first place, let's predict!!

Suppose that, the plant is given by

$$x(k+1) = Ax(k) + Bu(k), \qquad x \in \mathbb{R}^n, \ u \in \mathbb{R}^p,$$

where $x \in \mathbb{R}^n$, $u \in \mathbb{R}^p$ are state and control input, respectively.

- The matrices A, B are known with proper dimensions. (A,B) is controllable/stabilizable.
- The state sequence can be predicted by

$$X(k) = Fx(k) + \Phi U(k), \qquad F = \begin{bmatrix} A \\ A^2 \\ \vdots \\ A^N \end{bmatrix}, \quad \Phi = \begin{bmatrix} B & 0 \\ AB & B & 0 \\ \vdots \\ A^{N-1}B & A^{N-2}B & \cdots & B \end{bmatrix},$$

$$F = \begin{bmatrix} A \\ A^2 \\ \vdots \\ A^N \end{bmatrix},$$

$$\Phi = \begin{bmatrix} B & 0 \\ AB & B & 0 \\ \vdots & & & \\ A^{N-1}B & A^{N-2}B & \cdots & B \end{bmatrix}.$$

For example

$$A = \begin{bmatrix} 1.1 & 2 \\ 0 & 0.95 \end{bmatrix}, \quad B = \begin{bmatrix} 0 \\ 0.079 \end{bmatrix}$$



Weighting matrices and the terminal weight

• Infinite horizon cost function:

$$J(k) = \sum_{i=1}^{\infty} ||x(i|k)||_{Q}^{2} + ||u(i-1|k)||_{R}^{2}$$

$$= ||x(N|k)||_{P}^{2} + ||u(N-1|k)||_{R}^{2} + \sum_{i=1}^{N-1} ||x(i|k)||_{Q}^{2} + ||u(i-1|k)||_{R}^{2}$$

$$= X^{T}(k)QX(k) + U(k)^{T}RU(k)$$

$$\begin{aligned} \mathcal{Q} &= \operatorname{diag}[Q, Q, \cdots, Q, P] \\ \mathcal{R} &= \operatorname{diag}[R, R, \cdots, \cdots, R] \\ \\ P &- (A - BK)^T P (A - BK) = Q + K^T RK \end{aligned}$$

Weighting matrices and the terminal weight (cont'd)

Solve the discrete-time Lyapunov equation to get the terminal weight

$$Q = \text{diag}[Q, Q, \dots, Q, P]$$

$$P - (A - BK)^T P(A - BK) = Q + K^T RK$$

%solve lyapunov equation

Ak = A-B*K;

Qk = Q+K'*R*K;

 $P \equiv dlyap(Ak', Qk)$

Description

X = dlyap(A,Q) solves the discrete-time Lyapunov equation $AXA^T - X + Q = 0$, where A and Q are n-by-n matrices.

The solution X is symmetric when Q is symmetric, and positive definite when Q is positive definite and A has all its eigenvalues inside the unit disk.



For unconstrained MPC, simply calculate the linear feedback gain

$$u^*(k) = -\left[I_{p \times p} \ 0 \ \cdots \ 0\right] (\Phi^T \mathcal{Q} \Phi + \mathcal{R})^{-1} \Phi^T \mathcal{Q} F x(k) = -K_{mpc} x(k)$$



For constrained MPC, continue to construct the optimization

Constrained optimization

%optimization U = quadprog(Phi'*QQ*Phi+RR, x(:,i)'*F'*QQ*Phi, Ain, bin, [], [], lb, ub, u0);

$$U^*(k) = \arg\min_{U(k)} J(k)$$

$$= \arg\min_{U(k)} \left[x^T(k)F^T Q F x(k) + 2x^T(k)F^T Q \Phi U(k) + U^T(k)(\Phi^T Q \Phi + \mathcal{R})U(k) \right],$$

s.t.
$$Gx(i \mid k) + Hu(i \mid k) \le 1$$
, $\forall i = 0, 1, \cdots, N-1$.
$$x(N \mid k) \in \mathcal{X}_f \subset \Omega$$
.

x = quadprog(H,f,A,b,Aeq,beq,lb,ub,x0) 从向量 x0 开始求解上述问题。如果不存在边界,请设置 lb = [] 和 ub = []。一些 quadprog 算法会忽略 x0;请参阅 x0。

注意

x0 是 'active-set' 算法的必需参数。

说明

具有线性约束的二次目标函数的求解器。

quadprog 求由下式指定的问题的最小值

$$\min_{x} \frac{1}{2} x^{T} H x + f^{T} x \text{ such that } \begin{cases} A \cdot x \leq b, \\ Aeq \cdot x = beq, \\ lb \leq x \leq ub. \end{cases}$$

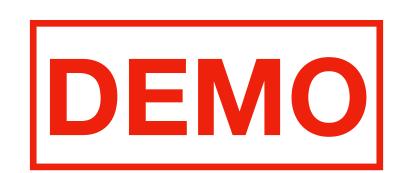
H、A和Aeq是矩阵,f、b、beq、lb、ub和x是向量。

Implementation of terminal constraints

Terminal state:

$$x(N|k) = [0, 0, \dots, I_{n \times n}]X(k)$$

= $[0, 0, \dots, I_{n \times n}][Fx(k) + \Phi U(k)]$



For example

$$x(N|k) \le 1$$

$$[0, 0, \dots, I_{n \times n}] [Fx(k) + \Phi U(k)] \le 1$$

$$[A^{N-1}b, A^{N-2}b, \dots, b] U(k) \le 1 - A^N x(k)$$

```
%terminal inequality constraint
bin1 = [u1_terminal_upper; u2_terminal_upper]-A^Nc*x(:,i);
bin2 =- [u1_terminal_lower; u2_terminal_lower]+A^Nc*x(:,i);
bin = [bin1; bin2];
Ain = [Phi(2*Nc-1:2*Nc,:); -Phi(2*Nc-1:2*Nc,:)];
```

- Prediction: calculate F and Φ , such that $X(k) = Fx(k) + \Phi U(k)$
- Weighting matrices: calculate *P*
 - find K such that |eig(A BK)| < 0
 - solve discrete-time Lyapunov equation to obtain P
- Constraints
 - state constraints and control constraints
 - terminal constraints

What if the plant is nonlinear??

$$[X^*(k), U^*(k)] = \arg\min_{X(k), U(k)} \left[\|x(N+1 \mid k)\|_P^2 + \|u(N \mid k)\|_R^2 + \sum_{i=1}^N \|x(i \mid k)\|_Q^2 + \|u(i-1 \mid k)\|_R^2 \right]$$

s.t.
$$Gx(i|k) + Hu(i|k) \le 1$$
, $\forall i = 0,1,\dots, N-1$, $x(0|k) = x(k)$, $x(i+1|k) = f\left(x(i|k), u(i|k)\right)$, $\forall i = 0,1,\dots, N-1$, $x(N|k) \in \mathcal{X}_f \subset \Omega$.

- Both state sequence and control sequence are selected as decision variables satisfying
 - state and control constraints
 - initial equality constraint
 - dynamic equality constraint (state equation)
 - terminal constraints

Let's try a nonlinear example

$$x(k+1) = f(x(k), u(k))$$

$$f(x(k), u(k)) = \begin{bmatrix} 1.1x_1(k) + \sin(x_2(k)) \\ 0.12x_1^2(k) + x_2(k) + 0.079u(k) \end{bmatrix}$$

s.t.
$$-4 \le u \le 4$$

```
%This is the nonlinear function for MPC demo

function xplus = nonlinear_func(x, u)

xplus = zeros(2,1);

xplus(1) = 1.1*x(1) + sin(x(2));

xplus(2) = 0.12* x(1)^2 + x(2) + 0.079*u;

end
```

Let's try a nonlinear example (cont'd)

$$J(k) = \sum_{i=1}^{N} \|x(i \mid k)\|_{Q}^{2} + \|u(i-1 \mid k)\|_{R}^{2},$$

s.t.
$$-4 \le u \le 4$$
 $x(0|k) = x(k)$ $x(N|k) = 0$

```
%This is the objective function for MPC demo
\Box function f = objfun(xx)
  global N;
  global dimx;
  global dimu;
  global dimy;
 X = xx(1: N*dimx);
                                                    %Predictive state series
  U = xx(N*dimx+1: N*dimx+N*dimu);
                                                  %Predictive control series
 f = 0;
  %weighting matrix
  Q = eye(dimx);
 R = 0.1;
  %Cost function
\Box for i = 1: N
    f = f + (X((i-1)*dimx+1: i*dimx)'*Q*X((i-1)*dimx+1: i*dimx)) ...
       + (U((i-1)*dimu+1: i*dimu)'*R* U((i-1)*dimu+1: i*dimu));
  end
  end
```

Let's try a nonlinear example (cont'd)

%Run optimization

xi = fmincon(@objFun, xi, Aueq, bueq, Aeq, beq, lb, ub, @nonlinear_constraints, options);

%Receding horizon implementation.

%Only the first step of predicive control is implemented.

u(:,k) = xi(N*dimx+1: N*dimx + dimu);

%model

 $x(:, k+1) = nonlinear_func(x(:, k), u(:, k));$



说明

非线性规划求解器。

求以下问题的最小值:

$$\min_{x} f(x) \text{ such that } \begin{cases} c(x) \leq 0 \\ ceq(x) = 0 \\ A \cdot x \leq b \\ Aeq \cdot x = beq \\ lb \leq x \leq ub, \end{cases}$$

b 和 beq 是向量,A 和 Aeq 是矩阵,c(x) 和 ceq(x) 是返回向量的函数,f(x) 是返回标量的函数。f(x)、c(x) 和 ceq(x) 可以是非线性函数。

MPC toolbox in MATLAB

Plant

Continuous-time —> Discrete-time

Create an MPC object

```
%plant Ts = 0.2; \qquad \text{%sampling time for discretization} \\ A = [0 \ 1; \ 1 \ 1]; \\ B = [0; \ 1]; \\ C = [1 \ 0]; \\ D = 0; \\ plant = c2d(ss(A,B,C,D), \ Ts); \\ \label{eq:main_sampling}
```

%mpc controller based on prediction of plant mpcObj = mpc(plant);

mpcobj = mpc(plant, ts, P, M, W, MV, OV, DV) specifies the following controller properties. If any of these values are omitted or empty, the default values apply.

- P sets the PredictionHorizon property.
- M sets the ControlHorizon property.
- W sets the Weights property.
- MV sets the ManipulatedVariables property.
- OV sets the OutputVariables property.
- DV sets the DisturbanceVariables property.

MPC toolbox in MATLAB

```
>> mpcObj
 MPC object (created on 08-Jun-2022 14:28:43):
 Sampling time: 0.2 (seconds)
 Prediction Horizon: 5
 Control Horizon: 5
 Plant Model:
     1 manipulated variable(s) --> 2 states
                                |--> 1 measured output(s)
     0 measured disturbance(s) --> 1 inputs
                                |--> 0 unmeasured output(s)
     0 unmeasured disturbance(s) --> 1 outputs |
 Disturbance and Noise Models:
      Output disturbance model: default (type "getoutdist(mpcObj)" for details)
      Measurement noise model: default (unity gain after scaling)
 Weights:
      ManipulatedVariables: 1
   ManipulatedVariablesRate: 0
         OutputVariables: 10
                ECR: 100000
 State Estimation: Default Kalman Filter (type "getEstimator(mpcObj)" for details)
 Constraints:
 -4 \le MV1(t+0) \le 4, MV1/rate is unconstrained, -\ln t \le MO1(t+1) \le \ln t
 -4 \le MV1(t+1) \le 4
                                       -Inf <= MO1(t+2) <= Inf
                                      -Inf \ll MO1(t+3) \ll Inf
 -4 <= MV1(t+2) <= 4
                                       -Inf \le MO1(t+4) \le Inf
 -4 \le MV1(t+3) \le 4
 -4 \le MV1(t+4) \le 4
                                          0 \le MO1(t+5) \le 0
: >>
```

```
%control constraints
mpcObj.MV(1).Min = -4;
mpcObj.MV(1).Max = 4;

%control horizon
mpcObj.ControlHorizon = 5;
mpcObj.PredictionHorizon = mpcObj.ControlHorizon;

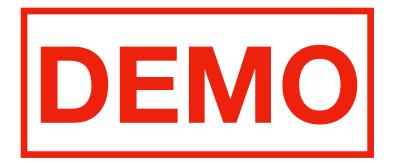
%Weights
mpcObj.Weights.ManipulatedVariables = 1;
mpcObj.Weights.ManipulatedVariablesRate = 0;
mpcObj.Weights.OutputVariables = 10;

%Terminal constraints
Y = struct('Weight',[],'Min',[-0],'Max',[0]);
U = struct('Weight',[],'Min',[],'Max',[]);
setterminal(mpcObj, Y, U);
```

- Parameters of MPC can be set manually.
 - Constraints, terminal constraints,
 - Control/predictive horizon, weights...

MPC toolbox in MATLAB

Run MPC using "mpcmove"



```
%Ref
  r = 0;
  t = 0: Ts : 5;
  N = length(t);
  y = zeros(N,1);
  xsys = zeros(N, 2);
  u = zeros(N,1);
\neg for i = 1:N
     % simulated plant and predictive model are identical
     y(i) = plant.C*x.Plant;
    xsys(i, :) = x.Plant;
     %Run mpc
     u(i) = mpcmove(mpcObj, x, y(i), r);
  end
```

Nonlinear MPC using MPC toolbox

Nonlinear MPC

R2020b

As in traditional linear MPC, nonlinear MPC calculates control actions at each control interval using a combination of model-based prediction and constrained optimization. The key differences are:

- The prediction model can be nonlinear and include time-varying parameters.
- The equality and inequality constraints can be nonlinear.
- The scalar cost function to be minimized can be a nonquadratic (linear or nonlinear) function of the decision variables.

Using nonlinear MPC, you can:

- Simulate closed-loop control of nonlinear plants under nonlinear costs and constraints.
- Plan optimal trajectories by solving an open-loop constrained nonlinear optimization problem.

Nonlinear MPC using MPC toolbox

$$x(k+1) = f(x(k), u(k))$$

$$f(x(k), u(k)) = \begin{bmatrix} 1.1x_1(k) + \sin(x_2(k)) \\ 0.12x_1^2(k) + x_2(k) + 0.079u(k) \end{bmatrix}$$

s.t.
$$-4 \le u \le 4$$

```
%This is the nonlinear function for MPC demo

function xplus = nonlinear_func(x, u)

xplus = zeros(2,1);

xplus(1) = 1.1*x(1) + sin(x(2));

xplus(2) = 0.12* x(1)^2 + x(2) + 0.079*u;

end
```

```
%Define a nonlinear mpc object

nx = 2;

ny = 2;

nu = 1;

nlobj = nlmpc(nx, ny, nu);

%State equation of the nonlinear plant

nlobj.Model.StateFcn = "nonlinear_func";

%It is not discretized from continuous-time model.

nlobj.Model.IsContinuousTime = false;
```

Nonlinear MPC using toolbox

- Parameters of the nonlinear MPC can be set manually.
 - Constraints, terminal constraints,
 - Control/predictive horizon, weights...

```
%Control horizon and predictive horizon
nlobj.PredictionHorizon = 10;
nlobj.ControlHorizon = 10;

%Control constraints
nlobj.MV = struct('Min',{-4},'Max',{4});

%Weight of output/state
nlobj.Weights.OutputVariables = [1 1];

%Weight of control input
nlobj.Weights.ManipulatedVariables = [0.1];
```

```
%Terminal constraint
  Optimization.CustomEqConFcn = "myEqConFunction";
  %This is to specify the terminal equality constraint
function ceq = myEqConFunction(X,U,data,params)
  p = data.PredictionHorizon;
 ceq = [X(p+1,1) - 0;
      X(p+1,2) - 0;
  end
```

Run the nonlinear MPC

```
%Run
for i = 1:N
  % simulated plant and predictive model are identical
  %Run mpc
  u(i) = nlmpcmove(nlobj, x(:, i), lastMV);
  lastMV = u(i);
  %Run nonlinear plant
  x(:, i+1) = nonlinear_func(x(:, i), u(i));
end
```

Description

mv = nlmpcmove(nlmpcobj,x,lastmv) computes the optimal manipulated variable control action for the current time. To simulate closed-loop nonlinear MPC control, call nlmpcmove repeatedly.



- Explicit MPC avoids online computations in "Implicit" MPC.
- Explicit MPC is simply "switches" among affine functions of states.

$$U^{*}(k) = \begin{bmatrix} u^{*}(0 \mid k) \\ u^{*}(1 \mid k) \\ \vdots \\ u^{*}(N-1 \mid k) \end{bmatrix} \qquad u^{*}(0 \mid k) = \begin{cases} F_{1}x + g_{1}, & \text{if } H_{1}x \leq K_{1}, \\ F_{2}x + g_{2}, & \text{if } H_{2}x \leq K_{2}, \\ \vdots \\ F_{M}x + g_{M}, & \text{if } H_{M}x \leq K_{M}. \end{cases}$$

Constrained optimization to be solved:

$$U^* = \arg\min_{U} \left[\frac{1}{2} x^T Q x + 2 x^T F^T U + \frac{1}{2} U^T Y U \right],$$

$$s.t. \quad GU \le W + Sx$$

Optimization by using active-set algorithm

$$\text{Active} \qquad G_i U^*(x_0) = W_i + S_i x_0$$
 For some $x_0 \in \mathcal{X}$
$$\text{Inactive} \qquad G_j U^*(x_0) \leq W_j + S_j x_0$$

Optimization with Lagrangian multiplier

$$U^* = \arg\min_{U} \left[\frac{1}{2} x^T Q x + 2 x^T F^T U + \frac{1}{2} U^T Y U + \lambda (\tilde{G}z - \tilde{W} - \tilde{S}x) \right],$$

$$\frac{\partial J}{\partial U} = 0 \quad \Rightarrow \quad QU + Fx + \tilde{G}^T \tilde{\lambda} = 0 \quad \Rightarrow \quad U = Q^{-1} (Fx + \tilde{G}^T \tilde{\lambda})$$

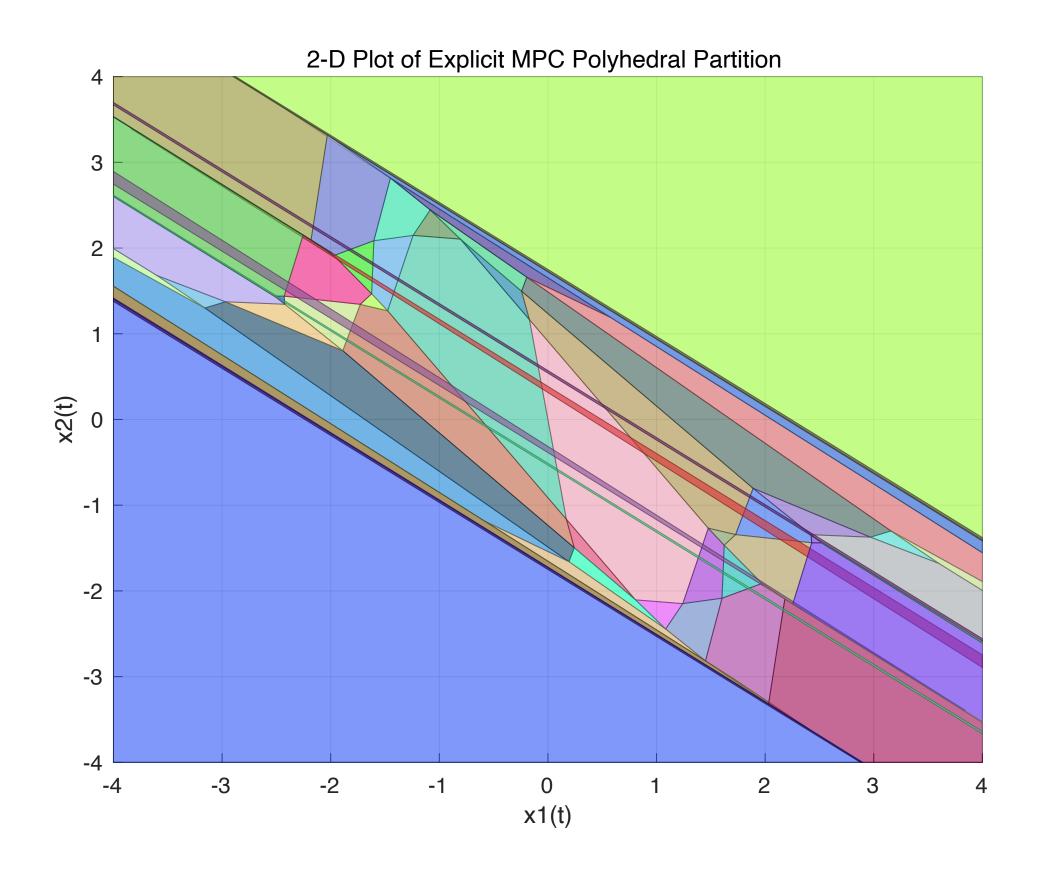
$$\frac{\partial J}{\partial \lambda} = 0 \qquad \Rightarrow \qquad \tilde{G}U - \tilde{W} - \tilde{S}x = 0$$

$$\Rightarrow \qquad \tilde{\lambda}(x) = -(\tilde{G}Q^{-1}\tilde{G}^T)^{-1}(\tilde{W} + (\tilde{S} + \tilde{G}Q^{-1}F)x)$$

Affine function of x

$$U(x) = Q^{-1} \left[(\tilde{G}Q^{-1}\tilde{G}^T)^{-1} (\tilde{W} + (\tilde{S} + \tilde{G}Q^{-1}F)x) - Fx \right]$$

$$u^{*}(0 \mid k) = \begin{cases} F_{1}x + g_{1}, & \text{if } H_{1}x \leq K_{1}, \\ F_{2}x + g_{2}, & \text{if } H_{2}x \leq K_{2}, \\ \vdots & & \\ F_{M}x + g_{M}, & \text{if } H_{M}x \leq K_{M}. \end{cases}$$

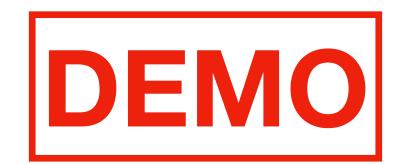


```
% This file is to generate explicit MPC
range = generateExplicitRange(mpcObj);
%There are 3 states???
%2 states, and 1 disturbance, as shown by mpcstate(mpcObj)
range.State.Min = [-4;-4;-1];
range.State.Max = [4; 4; 1];
range.Reference.Min = -4;
range.Reference.Max = 4;
range.ManipulatedVariable.Min = -4;
range.ManipulatedVariable.Max = 4;
mpcobjExplicit = generateExplicitMPC(mpcObj, range);
mpcobjExplicit = simplify(mpcobjExplicit, 'exact');
display(mpcobjExplicit);
```

```
for i = 1:N
  % simulated plant and predictive model are identical
  yExplicit(i) = plant.C*xExplicit.Plant;

  xsysExplicit(i, :) = xExplicit.Plant;

%Run mpc
  uExplicit(i) = mpcmoveExplicit(mpcobjExplicit, xExplicit, yExplicit(i), r);
end
```



Summary

Coding MPC in MATLAB

- Linear MPC: constrained quadratic optimization
- Nonlinear MPC: dynamic equality constraints

MPC toolbox

- Linear MPC
- Nonlinear MPC: more freedom to include nonlinear cost and nonlinear constraints
- Explicit MPC: avoid online computation, "switching" affine functions of states