

## Location and shape of phase boundary

One component (pure) system

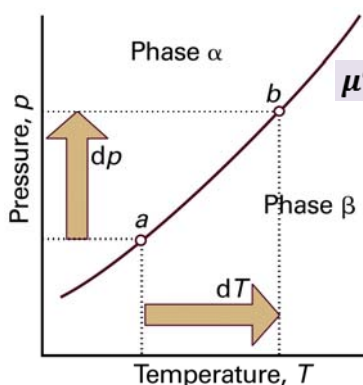


Figure 4-12  
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At point 'a'

$$\mu^\alpha(T, p) = \mu^\alpha(T, p)$$

At point 'b'

$$\mu^\alpha(T + dT, p + dp) = \mu^\beta(T + dT, p + dp)$$

$$\mu^\alpha(T, p) + d\mu^\alpha = \mu^\beta(T, p) + d\mu^\beta$$

$$d\mu^\alpha = d\mu^\beta$$

$$d\mu^i = -S_m^i dT + V_m^i dp$$

$$-S_m^\alpha dT + V_m^\alpha dp = -S_m^\beta dT + V_m^\beta dp$$

$$\frac{dp}{dT} = \frac{(S_m^\alpha - S_m^\beta)}{(V_m^\alpha - V_m^\beta)}$$

$$\frac{dp}{dT} = \frac{\Delta S_{\beta \rightarrow \alpha}}{\Delta V_{\beta \rightarrow \alpha}}$$

The Clapeyron Equation

$$\frac{dp}{dT} = \frac{\Delta S_{trans}}{\Delta V_{trans}}$$

Applies to any phase equilibrium of any pure substance

## Solid to Liquid Phase Boundary

If  $T_1$  is melting point at  $p_1$ , and  $T_2$  at  $p_2$

$$\frac{dp}{dT} = \frac{\Delta S_{trs}}{\Delta V_{trs}} = \frac{\Delta H_{fus}}{T \Delta V_{fus}}$$

$$\int_{p_1}^{p_2} dp = \frac{\Delta H_{fus}}{\Delta V_{fus}} \int_{T_1}^{T_2} \frac{dT}{T}$$

$$\Delta p = \frac{\Delta H_{fus}}{\Delta V_{fus}} \ln \frac{T_2}{T_1}$$

for,  $T_2 \approx T_1$ ,  $\ln \frac{T_2}{T_1} = \ln(1 + \frac{T_2 - T_1}{T_1}) \approx \frac{T_2 - T_1}{T_1} = \frac{\Delta T}{T_1}$

$$\Delta p = \frac{\Delta H_{fus}}{T_1 \Delta V_{fus}} \Delta T$$

$$\Delta T = \frac{T_1 \Delta V_{fus}}{\Delta H_{fus}} \Delta p$$

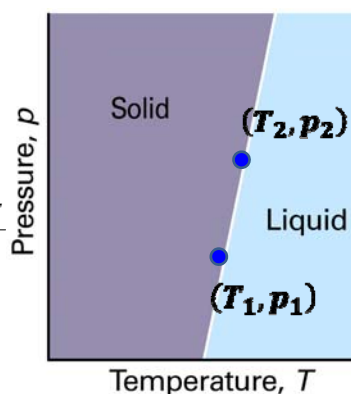


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Melting point varies linearly with pressure

**Liquid to Vapor Phase Boundary**

$$\frac{dp}{dT} = \frac{\Delta S_{trs}}{\Delta V_{trs}} = \frac{\Delta H_{vap}}{T \Delta V_{vap}}$$

$$\Delta V_{vap} = V_m(g) - V_m(l) \cong V_m(g) = RT/p \text{ (for ideal gas)}$$

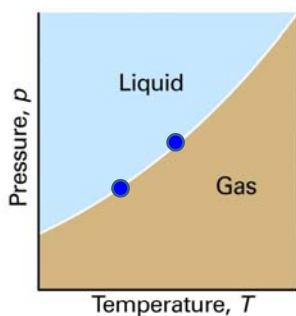


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$$\frac{d \ln p}{dT} = \frac{\Delta H_{vap}}{RT^2}$$

$$\frac{dp}{dT} = \frac{\Delta H_{vap}}{TV_m} = \frac{\Delta H_{vap}}{T(RT)/p}$$

$$\frac{dp}{p} \frac{1}{dT} = \frac{\Delta H_{vap}}{RT^2} \quad (\text{for ideal gas})$$

$$\frac{d \ln p}{dT} = \frac{\Delta H_{vap}}{RT^2}$$

$$\int_{\ln p_1}^{\ln p_2} d \ln p = \frac{\Delta H_{vap}}{R} \int_{T_1}^{T_2} \frac{dT}{T^2}$$

$$\ln \frac{p_2}{p_1} = -\frac{\Delta H_{vap}}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right)$$

**Clausius -Clapeyron Equation**

**Solid to Vapor Phase Boundary**

$$\frac{dp}{dT} = \frac{\Delta S_{trs}}{\Delta V_{trs}} = \frac{\Delta H_{sub}}{T \Delta V_{sub}}$$

$$\Delta V_{sub} = V_m(g) - V_m(s) \cong V_m(g) = RT/p \text{ (for ideal gas)}$$

$$\frac{d \ln p}{dT} = \frac{\Delta H_{sub}}{RT^2}$$

$$\ln \frac{p_2}{p_1} = -\frac{\Delta H_{sub}}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right)$$

$$p_2 = p_1 \exp(-\xi),$$

$$\xi = \frac{\Delta H_{sub}}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right)$$

$$= \frac{\Delta H_{fus} + \Delta H_{vap}}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right)$$

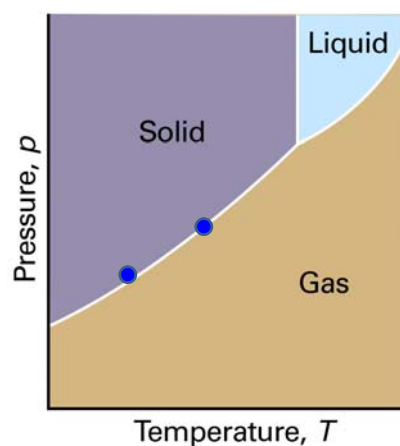


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## Location and shape of phase boundary

### One component (pure) system

#### Clausius -Clapeyron Equation

$$\frac{dp}{dT} = \frac{\Delta S_{\text{trs}}}{\Delta V_{\text{trs}}}$$

Solid to Liquid Phase Boundary

$$\frac{dp}{dT} = \frac{\Delta S_{\text{trs}}}{\Delta V_{\text{trs}}} = \frac{\Delta H_{\text{fus}}}{T_{\text{fus}} \Delta V_{\text{fus}}}$$

Liquid to Vapor Phase Boundary

$$\frac{dp}{dT} = \frac{\Delta H_{\text{vap}}}{TV_m} = \frac{\Delta H_{\text{vap}}}{T(RT)/p}$$

#### Clausius -Clapeyron Equation

$$\frac{d \ln p}{dT} = \frac{\Delta H_{\text{vap}}}{RT^2}$$

For Solid to Vapor

$$\frac{d \ln p}{dT} = \frac{\Delta H_{\text{sub}}}{RT^2} = \frac{\Delta H_{\text{fus}} + \Delta H_{\text{vap}}}{RT^2}$$

## Problem

Ice melts at 273 K at 1.0 bar.

$$\Delta H_{\text{fus}} = +6.008 \text{ kJ mol}^{-1} \quad \Delta V_{\text{fus}} = -1.613 \text{ m}^3 \text{ mol}^{-1}$$

The blade is 30 cm long and 0.03 cm wide. What is the pressure exerted by each blade on ice by a 50 kg skater?

Area of each blade in contact with ice =  $9 \times 10^{-5} \text{ m}^2$

Assume, weight on each leg = 25 kg

$$\begin{aligned} \text{Pressure on each blade} &= \frac{(25.0 \text{ kg}) \times (9.8 \text{ m s}^{-2})}{(9 \times 10^{-5} \text{ m}^2)} \\ &= 27.2 \times 10^5 \text{ J m}^{-3} \end{aligned}$$

$$\Delta T = \frac{T_1 \Delta V_{\text{fus}}}{\Delta H_{\text{fus}}} \Delta p$$

$$\Delta T = -1.92 \text{ K}$$



Ice skating shoe

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## Temperature Dependence of Chemical Potential

$$dG = Vdp - SdT$$

$$d\mu = V_m dP - S_m dT$$

$$\left(\frac{\partial \mu}{\partial T}\right)_P = -S_m$$

$$S_m(\text{solid}) < S_m(\text{liquid}) \ll S_m(\text{gas})$$

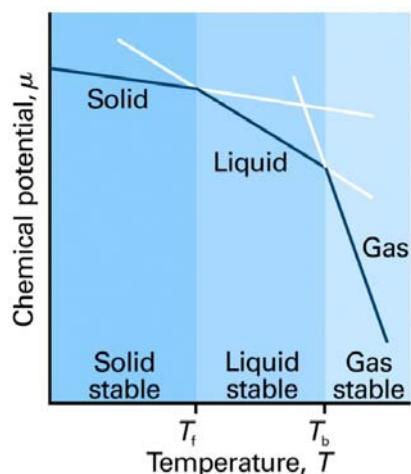


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## (isothermal) Pressure dependence of Chemical Potential

$$\left(\frac{\partial G}{\partial p}\right)_T = V \quad \int_{G_1}^{G_2} dG = \int_{p_1}^{p_2} V dp \quad G_2 = G_1 + \int_{p_1}^{p_2} V dp$$

for one component system,  $\mu_2(T) = \mu_1(T) + \int_{p_1}^{p_2} V_m dp$

Case 1: liquid or solid;  $V$  weakly dependent on  $p$

$$\mu_2(T) = \mu_1(T) + V_m(p_2 - p_1) \quad \text{for one component system}$$

Case 2: ideal gas;  $V$  is dependent on  $p$ ,

$$\mu_2(T) = \mu_1(T) + RT \ln \frac{p_2}{p_1}$$

$$\mu(T) = \mu^\circ(T) + RT \ln \frac{p}{p^\circ}$$

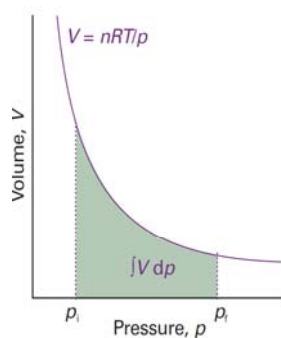
$$\mu(T) = \mu^\circ(T) + RT \ln p$$

$\mu^\circ$  = standard chemical potential, the chemical potential of the pure gas at 1 bar at temp  $T$ .

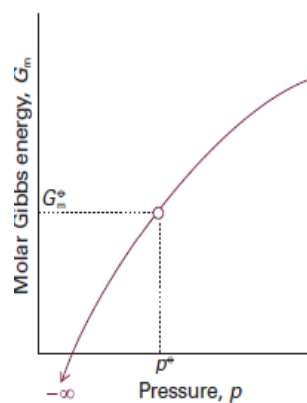
$p$  expressed in bar.

### Chemical Potential of an ideal gas

$$\mu_2 = \mu_1 + \int_{p_1}^{p_2} V_m dp$$



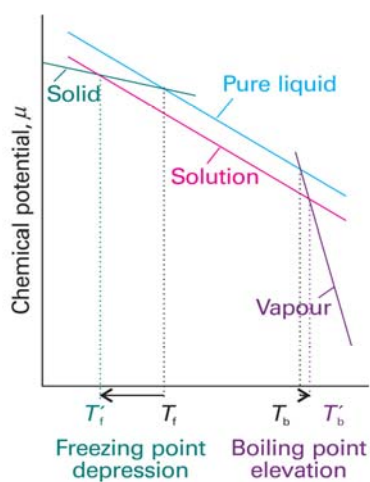
$$\mu(T) = \mu^o(T) + RT \ln \frac{p}{p^o}$$



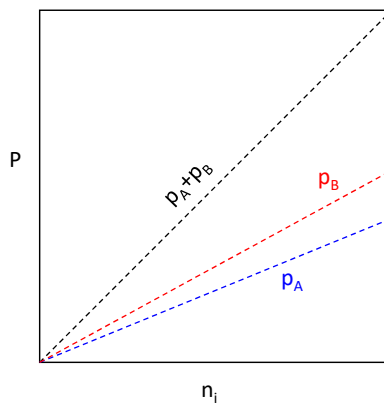
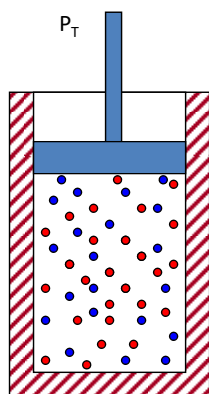
### Effect of solute on boiling and melting points of solvent

$$\mu_A = \mu_A^* + RT \ln x_A$$

$$\mu_A = \mu_A^* + RT \ln a_A$$



## Mixtures of ideal gases



$$P = p_A + p_B$$

**Dalton's Law of partial pressures**

If the gases are "ideal", then:

$$p_A = x_A P$$

$$p_B = x_B P$$

where:

$$x_A = \frac{n_A}{n}$$

$$x_B = \frac{n_B}{n}$$

## The Gibbs Energy of Mixing of Ideal Gases

$$\mu_i(T) = \mu_i^o(T) + RT \ln p_i \quad p_i = \text{partial pressure of } i^{\text{th}} \text{ gas in bar.}$$

Before mixing:

$$G_{\text{before mixing}} = \sum_i n_i (\mu_i^o(T) + RT \ln p)$$

After mixing:

$$\begin{aligned} G_{\text{mixture}} &= \sum_i n_i \mu_i = \sum_i n_i (\mu_i^o(T) + RT \ln p_i) \\ &= \sum_i n_i (\mu_i^o(T) + RT \ln x_i p) \end{aligned}$$

Dalton's law of partial pressure,  $p_i = x_i p$

$$\Delta G_{\text{mix}} = nRT \sum_i x_i \ln x_i$$

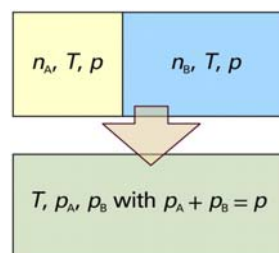


Figure 1.8  
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Gibbs free energy of mixing of ideal gases is always negative, and hence spontaneous

## The Enthalpy of Mixing of Ideal Gases

$$\Delta G_{mix} = nRT \sum_i x_i \ln x_i$$

$$\Delta S_{mix} = - \left( \frac{\partial (\Delta G_{mix})}{\partial T} \right)_{p,n} = -nR \sum_i x_i \ln x_i$$

$$\Delta H_{mix} = \Delta G_{mix} + T\Delta S_{mix} = 0$$

Ideal gases show no intermolecular interactions and hence change in enthalpy is zero

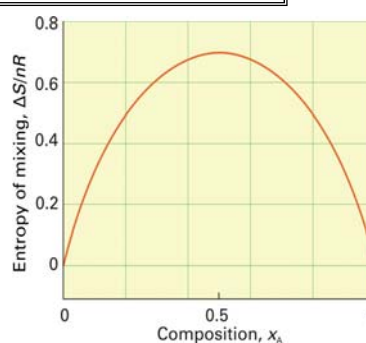
## Gas mixtures

Perfect gases mix spontaneously in all proportions

$$\Delta S_{mix} = - \left( \frac{\partial (\Delta G_{mix})}{\partial T} \right)_{p,n}$$

$$\Delta V_{mix} = \left( \frac{\partial (\Delta G_{mix})}{\partial p} \right)_{T,n}$$

$$\Delta H_{mix} = \Delta G_{mix} + T\Delta S_{mix}$$



$$\Delta G_{mix} = nRT \{x_A \ln x_A + x_B \ln x_B\}$$

$$\Delta G = \Delta H - T\Delta S$$

$$\Delta S_{mix} = -nR \{x_A \ln x_A + x_B \ln x_B\}$$

$$\Delta H_{mix} = 0$$

## Equilibrium: Overview

### Describing Chemical Equilibrium

- Chemical Equilibrium – A Dynamic Equilibrium (the link to Chemical Kinetics)
- The Equilibrium Constant
- Heterogeneous Equilibria; solvents in homogeneous equilibria

### Using the Equilibrium Constant

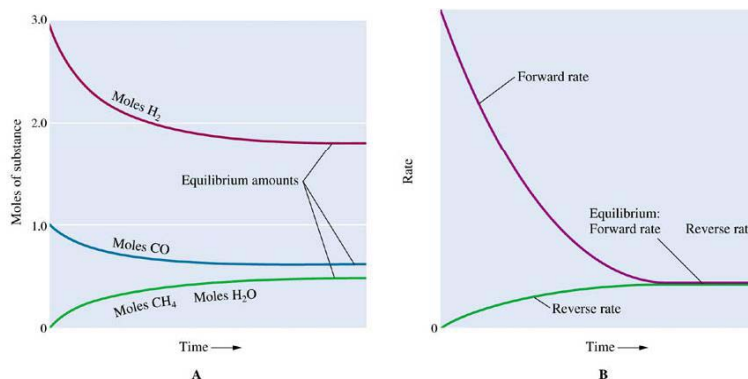
- Qualitatively Interpreting the Equilibrium Constant
- Predicting the direction of a Reaction
- Calculating Equilibrium Concentrations

### Changing Reaction Conditions: Le Châtelier's Principle

- Removing Products or Adding Reactants
- Changing the Pressure or Temperature
- Effect of a Catalyst

## Chemical Equilibrium – A Dynamic Equilibrium

- Upon addition of reactants and/or products, reaction occurs until a constant amount of reactants and products are present = **equilibrium**
- Equilibrium is dynamic since product is constantly made (forward reaction), but at the same rate it is consumed (reverse reaction)

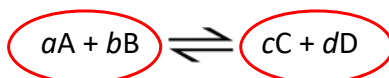




### Chemical Equilibrium – A Dynamic Equilibrium



$$K = \frac{[\text{NO}_2]^2}{[\text{N}_2\text{O}_4]} = 4.63 \times 10^{-3}$$



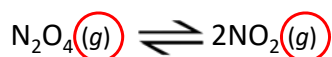
$$K = \frac{[\text{C}]^c[\text{D}]^d}{[\text{A}]^a[\text{B}]^b}$$

**Law of Mass Action**

### Equilibrium Will

$K \gg 1$	Lie to the right	Favour products
$K \ll 1$	Lie to the left	Favour reactants

**Homogenous equilibrium** applies to reactions in which all reacting species **are in the same phase**



$$K_c = \frac{[\text{NO}_2]^2}{[\text{N}_2\text{O}_4]}$$

$$K_p = \frac{P_{\text{NO}_2}^2}{P_{\text{N}_2\text{O}_4}}$$

In most cases

$$K_c \neq K_p$$



$$K_p = K_c(RT)^{\Delta n}$$

$$\begin{aligned} \Delta n &= \text{moles of gaseous products} - \text{moles of gaseous reactants} \\ &= (c + d) - (a + b) \end{aligned}$$

### Chemical Equilibrium



$$\Delta G_r^0 = \sum_{\text{pdts}} \nu \Delta G_f^0 - \sum_{\text{reactants}} \nu \Delta G_f^0$$

$$\Delta G_r^0 = c \Delta_f G_C^0 + d \Delta_f G_D^0 - a \Delta_f G_A^0 - b \Delta_f G_B^0$$

If  $\Delta_r G^0 > 0$  then the reaction will not go as written (the reverse reaction will go); if  $\Delta_r G^0 < 0$  then the reaction will go as written.

$\Delta G_r^0$  can also be written in terms of chemical potentials of the components.  
All components are in their standard states

$$\Delta G_r^0 = c \mu_C^0 + d \mu_D^0 - a \mu_A^0 - b \mu_B^0$$

$\Delta G_r^0 \neq 0$       **Chemical reactions are not equilibrium processes**

### Chemical Equilibrium

#### Criterion for equilibrium at constant p and T

$$dG_{p,T} \leq 0$$

$$dG_{p,T} = \sum_i \mu_i dn_i \leq 0$$

Let the reaction proceed by an amount  $dn$  ( $dn > 0$ )

$$dn_C = c dn$$

$$dn_D = d dn$$

$$dn_A = -a dn$$

$$dn_B = -b dn$$

$$dG_{p,T} = c \mu_C dn + d \mu_D dn - a \mu_A dn - b \mu_B dn$$

$$= (c \mu_C + d \mu_D - a \mu_A - b \mu_B) dn$$

$$dG_{p,T} = \Delta G_r dn \leq 0$$

$$\Delta G_r = c \mu_C + d \mu_D - a \mu_A - b \mu_B$$

### Chemical Equilibrium

$$\Delta G_r^0 = c\mu_C^0 + d\mu_D^0 - a\mu_A^0 - b\mu_B^0$$

If the components are not in their standard states:

$$\Delta G_r = c\mu_C + d\mu_D - a\mu_A - b\mu_B$$

Write a general form of the chemical potential of component  $i$  in terms of the activity  $a_i$  – choose system e.g. ideal / real gas etc.

$$\mu_i = \mu_i^0 + RT \ln a_i$$

$$\Delta G_r = \Delta G_r^0 + RT (\ln a_C^c + \ln a_D^d - \ln a_A^a - \ln a_B^b)$$

$$\Delta G_r = \Delta G_r^0 + RT \ln \frac{a_C^c a_D^d}{a_A^a a_B^b}$$

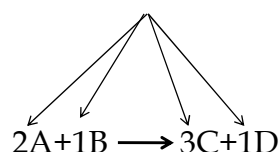
$$\Delta G_r = \Delta G_r^0 + RT \ln Q$$

### Chemical Equilibrium

$$\Delta G_r = \sum_i \nu_i \mu_i$$

$$\Delta G_r = 3\mu_C + \mu_D - 2\mu_A - \mu_B$$

Stoichiometric numbers  $\nu_i$



$$\Delta G_r = \sum_i \nu_i (\mu_i^0 + RT \ln a_i) = \sum_i \nu_i \mu_i^0 + RT \sum_i \nu_i \ln a_i$$

$$= \Delta G_r^0 + RT \ln \prod_i a_i^{\nu_i}$$

$$\Delta G_r^0 = \sum_i \nu_i \mu_i^0 = \sum_{\text{pds}} \nu \Delta G_f^0 - \sum_{\text{reactants}} \nu \Delta G_f^0$$

$$= \Delta G_r^0 + RT \ln Q$$

$$Q = \prod_i a_i^{\nu_i}$$

## Chemical Equilibrium

$$\Delta G_r = \Delta G_r^0 + RT \ln \prod_i a_i^{v_i} = \Delta G_r^0 + RT \ln Q \quad \boxed{Q = \prod_i a_i^{v_i}}$$

At equilibrium:

$$K = \left[ \prod_i a_i^{v_i} \right]_{\text{equilibrium}} \quad \text{Thermodynamic equilibrium constant}$$

$$\Delta G_r = 0 = \Delta G_r^0 + RT \ln K$$

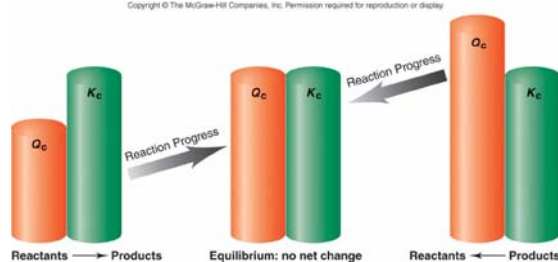
Practically  $a_i$  approximated by  
numerical values of molalities / by  
molar concentration / numerical  
values of partial pressures

$$\begin{aligned} \Delta G_r &= 0 = \Delta G_r^0 + RT \ln K_a \\ \Delta G_r^0 &= -RT \ln K_a \\ K_a &= \exp \frac{\Delta G^0}{RT} \\ K_a &= \exp \frac{\Delta H^0 - T\Delta S^0}{RT} \\ K_a &= \exp \frac{\Delta H^0}{RT} \exp \frac{\Delta S^0}{R} \end{aligned}$$

## Applications of Equilibrium Constants

### Predicting the Direction of Reaction

- If  $Q > K$  then the reverse reaction must occur to reach equilibrium
- If  $Q < K$  then the forward reaction must occur to reach equilibrium



**TABLE 18.4** Relation Between  $\Delta G^\circ$  and  $K$  as Predicted by the Equation  $\Delta G^\circ = -RT \ln K$

$K$	$\ln K$	$\Delta G^\circ$	Comments
$> 1$	Positive	Negative	Products are favored over reactants at equilibrium.
$= 1$	0	0	Products and reactants are equally favored at equilibrium.
$< 1$	Negative	Positive	Reactants are favored over products at equilibrium.