

# REVIEW AND ANALYSIS OF “A MICROCLIMATE GREENHOUSE MULTIVARIABLE CONTROL: A GUIDE TO USE HARDWARE IN THE LOOP SIMULATION”

Aaron Rosenberg

ECE 763

4/19/2023

G. Cevallos, J. Pinzon, and O. Camacho, “A microclimate greenhouse multivariable control: A guide to use hardware in the Loop Simulation,”  
2022 IEEE International Conference on Automation/XXV Congress of the Chilean Association of Automatic Control (ICA-ACCA), 2022.

# STATEMENT OF INTEREST

- Groundwork for home project
  - Maintain growth of tropical plants
  - Goal is to eventually grow food plants
- Benefits of greenhouses
  - Controlled environment (temperature/humidity)
  - Protected environment (weather/pests/animals)
  - Ability to grow out of season/conditions



Picture of inside of greenhouse [2]

# BACKGROUND INFORMATION

How does **Temperature** affect plants? [4]

- Plant vigor
- Leaf size
- Leaf expansion rate
- Time to fruit development

How does **Humidity** affect plants? [4]

- Transpiration
  - Calcium uptake
  - Hormonal Distribution

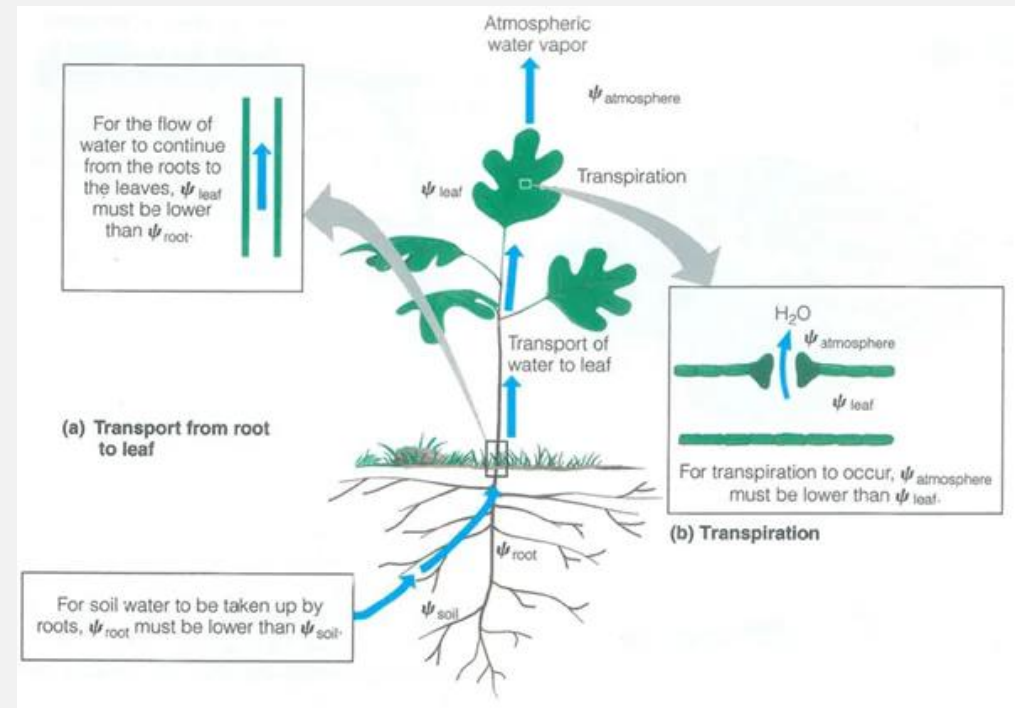


Diagram of plant transpiration process [3]

# TEMPERATURE/HUMIDITY RANGES FOR PLANTS

Rule of thumb for most horticultural crops [4]:

- Temperature ranging from 70 °F - 79°F (21°C - 26°C) during the day, with temperatures ~10°F (5.5°C) lower at night.
- Relative humidity between 55% and 95%



Monstera Deliciosa

<https://commons.wikimedia.org/w/index.php?curid=7094>

Plant	Ideal Temperature °F	Ideal Temperature °C	Ideal Relative Humidity
Monstera Deliciosa	65 - 90	18.33 - 32.22	60% - 80%
Golden Pothos	65 - 85	18.33 - 29.44	50% - 70%
Syngonium Wendlandii	59 - 86	15 - 30	60% - 80%
Poblano	70 - 85	21 - 29.44	70% - 80%
Serrano	71 - 85	22 - 29.44	70% - 80%
Tomato	70 - 79	21 - 26	80% - 90%

# TEMPERATURE AND HUMIDITY

## RELATIVE HUMIDITY

$$RH = \frac{\text{amount of water vapor in air}}{\text{max capacity of water vapor in air}} * 100$$

- Temperature dependent
- Inversely proportional

## ABSOLUTE HUMIDITY

$$AH = \frac{\text{mass of water vapor present}}{\text{unit volume of air}}$$

- Temperature independent\*

## SPECIFIC HUMIDITY

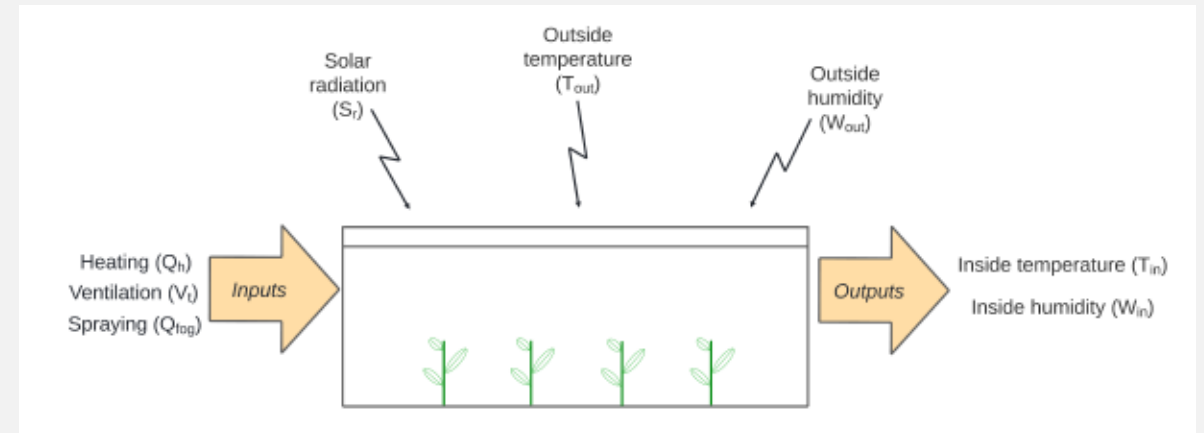
$$SH = \frac{\text{mass of water vapor present}}{\text{mass of dry air}}$$

- Temperature independent

\*As long as the volume is kept constant

# DESCRIPTION OF PHYSICAL SYSTEM

- Maintain the inside temperature and inside humidity at desired set point
  - Non-linear, coupled system
  - MIMO system; 3 input, 2 output, 3 disturbance inputs
  - Implement controller on Arduino and simulate control of greenhouse microclimate



Greenhouse Model Inputs, Outputs, and Disturbances [1]

# MATHEMATICAL MODEL

$$\frac{dT_{in}}{dt} = \frac{Q_h}{\rho V C_p} + \frac{S_i}{\rho V C_p} - \frac{\gamma Q_{fog}}{\rho V C_p} - (T_{in} - T_{out}) \left[ \frac{V_t}{V} + \frac{UA}{\rho V C_p} \right] \quad (1)$$

$$\frac{dW_{in}}{dt} = \frac{Q_{fog}}{\rho V} + \frac{E}{\rho V} - \frac{V_t(W_{in} - W_{out})}{\rho V} \quad (2)$$

## Outputs

$T_{in}$  = Inside Temperature (°C) =  $x_1$

$W_{in}$  = Inside Humidity (g/m<sup>3</sup>) =  $x_2$

## Inputs

$V_t$  = Ventilation rate (m<sup>3</sup>/s) =  $u_1$

$Q_{fog}$  = Water capacity of fog system (g/s) =  $u_2$

$Q_h$  = Heat provided by heater (Watts) =  $u_3$

## Disturbances

$T_{out}$  = Outside Temperature (°C) =  $d_1$

$W_{out}$  = Outside Humidity (g/m<sup>3</sup>) =  $d_2$

$S_r$  = Intercepted solar radiant energy (Watts/m<sup>2</sup>) =  $d_3$

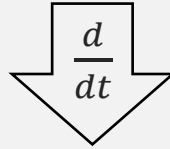
TABLE I  
CONSTANTS AND VARIABLES IN THE EQUILIBRIUM POINT. [11]

Constant	Value	Variable	Value
$V$	4000 m <sup>3</sup>	$\overline{S_r}$	300 W/m <sup>2</sup>
$U$	25 W/(m <sup>2</sup> · K)	$\overline{T_{out}}$	25 °C
$A$	1000 m <sup>2</sup>	$\overline{W_{out}}$	4 g/m <sup>3</sup>
$\rho$	1.2 kg/m <sup>3</sup>	$\overline{V_t}$	10 m <sup>3</sup> /s
$C_p$	1006 J/(kg · K)	$\overline{Q_{fog}}$	18 g/s
$\gamma$	2257 J/g	-	-

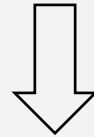
# DERIVATION OF MATHEMATICAL MODEL

**Specific Heat Capacity** – the amount of heat required to change the temperature of a mass by 1°C

$$Q = mC\Delta T$$



$$\dot{Q} = mC\dot{T}$$



$$\dot{T} = \frac{\dot{Q}}{mC} \quad (3)$$

Check Units:

$$J = kg * \frac{J}{kgK} * K$$

Check Units:

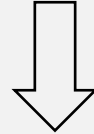
$$watts = \frac{J}{s} = kg * \frac{J}{kgK} * \frac{K}{s}$$



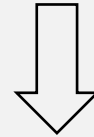
# DERIVATION OF MATHEMATICAL MODEL

**Conduction – transfer of heat due to temperature gradient**

$$\dot{Q} = -UA(T_{in} - T_{out})$$



$$mC\dot{T} = \dot{Q} = -UA(T_{in} - T_{out})$$



$$\dot{T} = \frac{-UA(T_{in} - T_{out})}{mC} \quad (4)$$

Check Units:

$$\text{watts} = \frac{J}{s} = \frac{W}{m^2 K} * m^2 * K$$

## EQUATION (1) REVISITED

$$\frac{dT_{in}}{dt} = \underbrace{\frac{Q_h}{\rho V C_p}}_{\text{Heater Term}} + \underbrace{\frac{S_i}{\rho V C_p}}_{\text{Solar Term}} - \underbrace{\frac{\gamma Q_{fog}}{\rho V C_p}}_{\text{Fog Term}} - (T_{in} - T_{out}) \left[ \underbrace{\frac{V_t}{V}}_{\text{Ventilation Term}} + \underbrace{\frac{UA}{\rho V C_p}}_{\text{Conduction Term}} \right]$$

Additional Discussion:

1. Solar Term
  - a. Derived from Eq. (3)
  - b. Heat added to system through solar radiation, watts
2. Fog Term
  - a. Derived from Eq. (3)
  - b. Heat removed from system due to addition of water vapor
3. Ventilation Term
  - a. Temperature change due to venting out air

## EVAPOTRANSPIRATION RATE, E

$$E = \alpha \frac{S_i}{\gamma} - \beta_T W_{in} \quad (5)$$

Check Units:

$$\frac{g}{s} = \frac{\frac{W}{m^2} * m^2}{\frac{J}{g}} - \frac{g}{s}$$

Where:

$$S_i = S_r * A$$

$\alpha$  – coefficient to account for leaf shading and leaf area index

$\beta$  – coefficient to account for thermodynamic constants

$\gamma$  – latent heat of vaporization

## EQUATION (2) REVISITED

$$\frac{dW_{in}}{dt} = \underbrace{\frac{Q_{fog}}{\rho V}}_{\text{Fog Term}} + \underbrace{\frac{E}{\rho V}}_{\text{Transpiration Term}} - \underbrace{\frac{V_t(W_{in} - W_{out})}{\rho V}}_{\text{Venting Term}}$$

Additional Discussion:

1. Fog Term
  - a. Mass of water vapor added to system due to fogging
2. Transpiration Term
  - a. Mass of water vapor added to system through transpiration
3. Ventilation Term
  - a. Mass of water vapor removed from system through venting

# LINEARIZED MODEL

$$P_{n(s)} = \begin{pmatrix} G_{11(s)} & G_{12(s)} \\ G_{21(s)} & G_{22(s)} \end{pmatrix}.$$
$$P_{n(s)} = \begin{pmatrix} \frac{-0.212 \cdot e^{-147.625s}}{126.892s+1} & \frac{-0.061 \cdot e^{-147.625s}}{130.829s+1} \\ \frac{-0.281 \cdot e^{-147.625s}}{435.488s+1} & \frac{0.100 \cdot e^{-147.625s}}{480.172s+1} \end{pmatrix}$$

- Authors linearized non-linear model using non-linear system identification techniques
- Delay calculated from average of delays from reference source
- Delay added to account for sensor delay in real system

Transfer Functions:

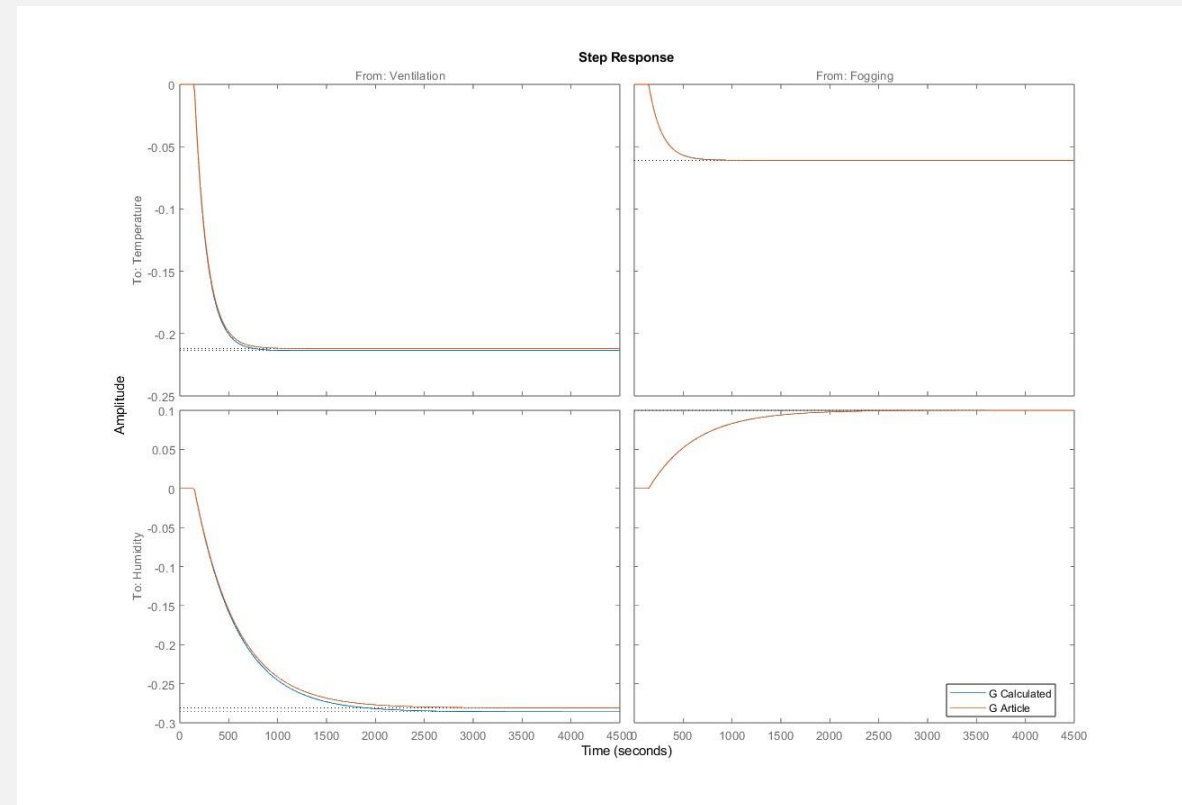
- $G_{11}$  is Temperature response due to ventilation
- $G_{12}$  is Temperature response due to fogging
- $G_{21}$  is Humidity response due to ventilation
- $G_{22}$  is Humidity response due to fogging

# COMPARISON TO ECE763 LINEARIZATION

$$A = \begin{bmatrix} \frac{\partial F}{\partial x_1} & \frac{\partial F}{\partial x_2} \\ \frac{\partial G}{\partial x_1} & \frac{\partial G}{\partial x_2} \end{bmatrix}$$

$$B = \begin{bmatrix} \frac{\partial F}{\partial u_1} & \frac{\partial F}{\partial u_2} \\ \frac{\partial G}{\partial u_1} & \frac{\partial G}{\partial u_2} \end{bmatrix}$$

$$C = \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix} \quad (6)$$



# RELATIVE GAIN ARRAY (RGA)

$$RGA(G) = \Lambda(G) \triangleq G .* (G^{-1})^T \quad (7)$$

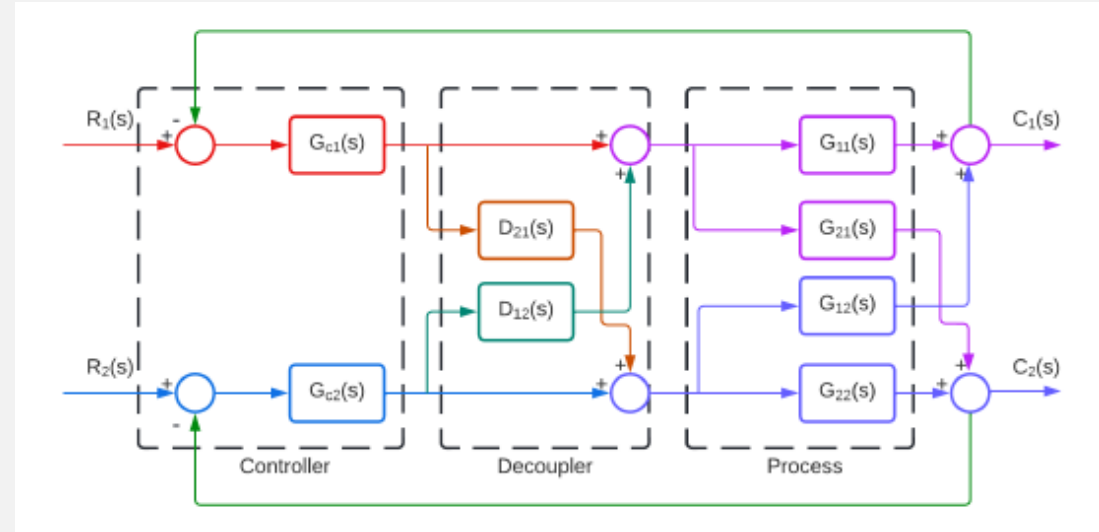
- Ratio of the open loop gain to the closed loop gain for each transfer function,  $\forall \omega$  [7]
- “Measures” the amount of interaction between inputs and outputs
- All columns in the RGA sum to 1, all rows in the RGA sum to 1
- Entries  $\approx 1$  indicate strong interactions between input/output
- Entries  $\approx 0.5$  indicate strong coupling in system between inputs and outputs
- Negative entries indicate interactions in the opposite direction  $\rightarrow$  instability

$$\Lambda = \begin{pmatrix} -0.212 & -0.061 \\ -0.281 & 0.100 \end{pmatrix} \left[ \begin{pmatrix} -0.212 & -0.061 \\ -0.281 & 0.100 \end{pmatrix}^{-1} \right]^T$$
$$\Lambda = \begin{pmatrix} 0.553 & 0.447 \\ 0.447 & 0.553 \end{pmatrix}.$$

# DECENTRALIZED CONTROL

- Simplest approach for multivariable controller design [7]
- Diagonal controller
- Design controllers separately, to control a single output

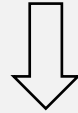
$$K = \begin{bmatrix} k_1 & \cdots & 0 \\ \vdots & \ddots & \vdots \\ 0 & \cdots & k_n \end{bmatrix}$$



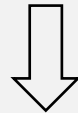


# DECOUPLER DESIGN

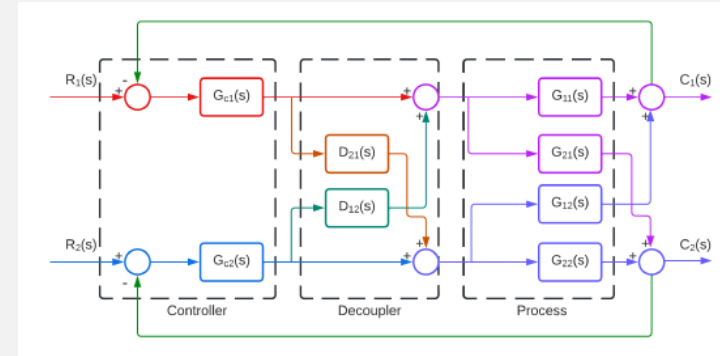
$$G^* = GW_1 = \begin{bmatrix} G_{11} & G_{12} \\ G_{21} & G_{22} \end{bmatrix} * \begin{bmatrix} 1 & D_{12} \\ D_{21} & 1 \end{bmatrix}$$



$$G^* = \begin{bmatrix} G_{11} + G_{12}D_{21} & G_{11}D_{12} + G_{12} \\ G_{21} + G_{22}D_{21} & G_{21}D_{12} + G_{22} \end{bmatrix},$$



$$G^* = \begin{bmatrix} G_{11} - \frac{G_{12}G_{21}}{G_{22}} & 0 \\ 0 & G_{22} - \frac{G_{21}G_{12}}{G_{11}} \end{bmatrix} \quad (9)$$



$$D_{12} = -\frac{G_{12}}{G_{11}} \quad D_{21} = -\frac{G_{21}}{G_{22}} \quad (8)$$

## DECOUPLER DESIGN

$$D_{12(s)} = -\frac{G_{12(s)}}{G_{11(s)}} = -0.287.$$

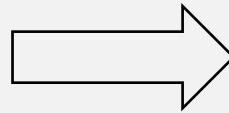
$$D_{21(s)} = -\frac{G_{21(s)}}{G_{22(s)}} = 2.813.$$

$$\Lambda(G^*) = \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix}$$

# CONTROLLER DESIGN

$$G_{c1(s)} = -2.027 \left[ \frac{(126.892)s + 1}{(126.892)s} \right]$$

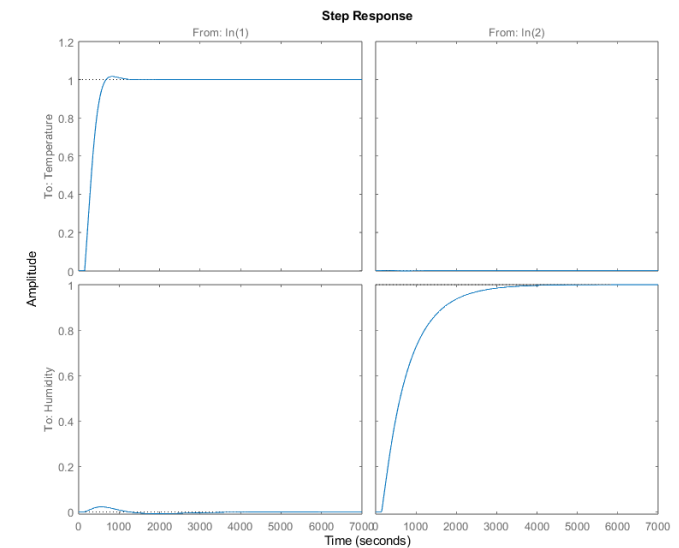
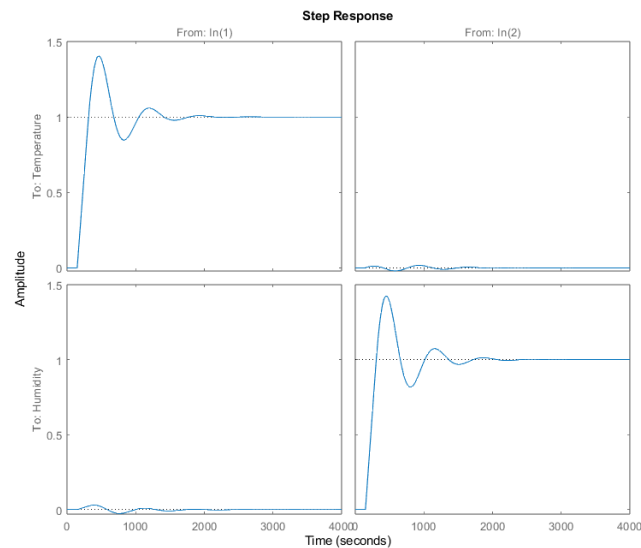
$$G_{c2(s)} = 16.263 \left[ \frac{(480.172)s + 1}{(480.172)s} \right]$$



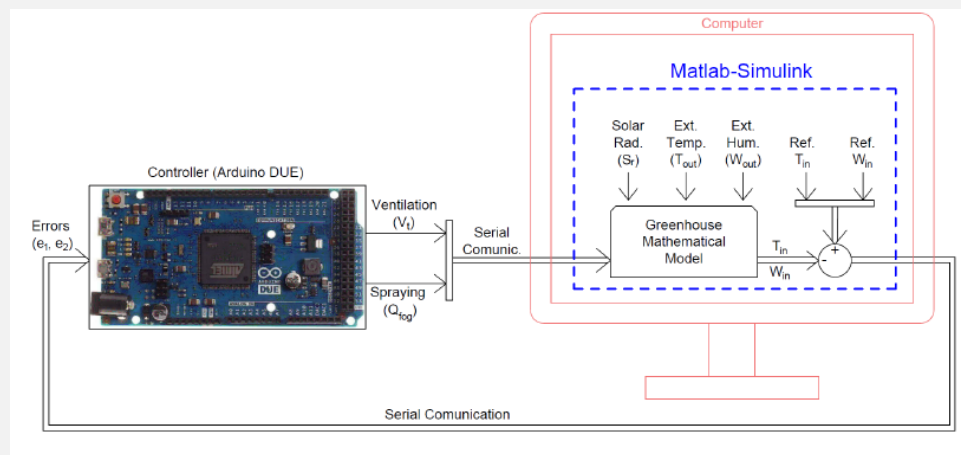
$$G_{c1(s)} = -1.014 \left[ \frac{(126.892)s + 1}{(126.892)s} \right]$$

$$G_{c2(s)} = 3.253 \left[ \frac{(480.172)s + 1}{(480.172)s} \right]$$

Reduce gain  
to improve  
control  
performance



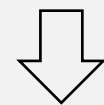
# CONVERSION TO DISCRETE TIME



“Tustin Approximation” [8]

$$z = e^{sT_s} \approx \frac{1 + sT_s/2}{1 - sT_s/2} \quad (10)$$

$$H_d(z) = H(s'), \quad s' = \frac{2}{T_s} \frac{z - 1}{z + 1} \quad (11)$$



$$G_{c1(z)} = -1.092 \cdot \left( \frac{z - 0.856}{z - 1} \right)$$

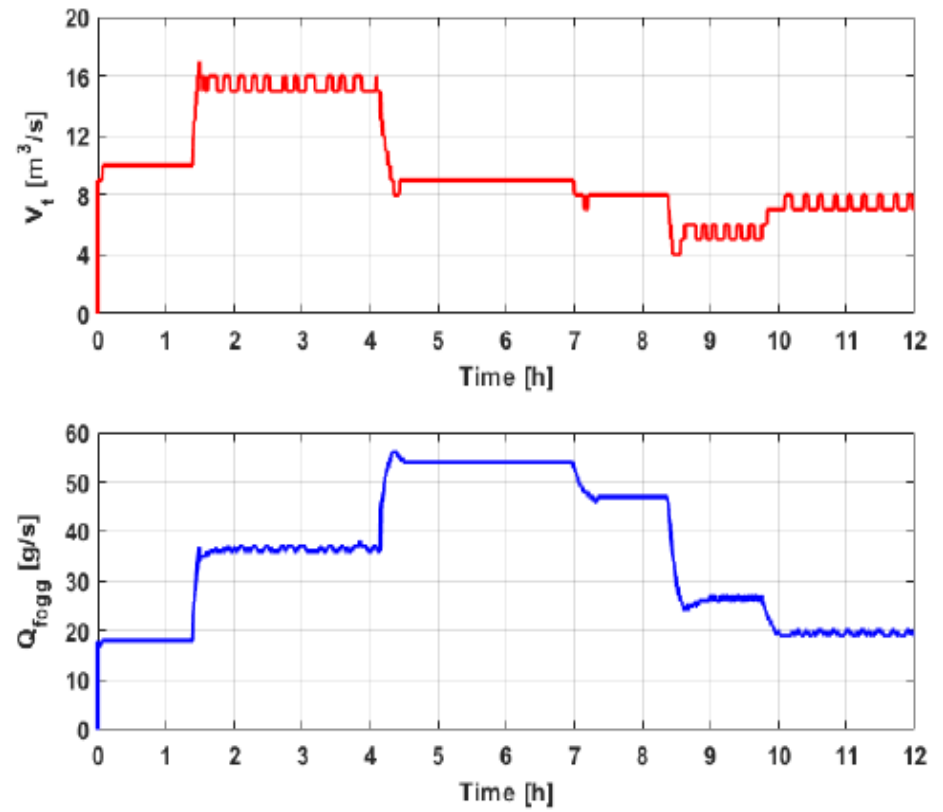
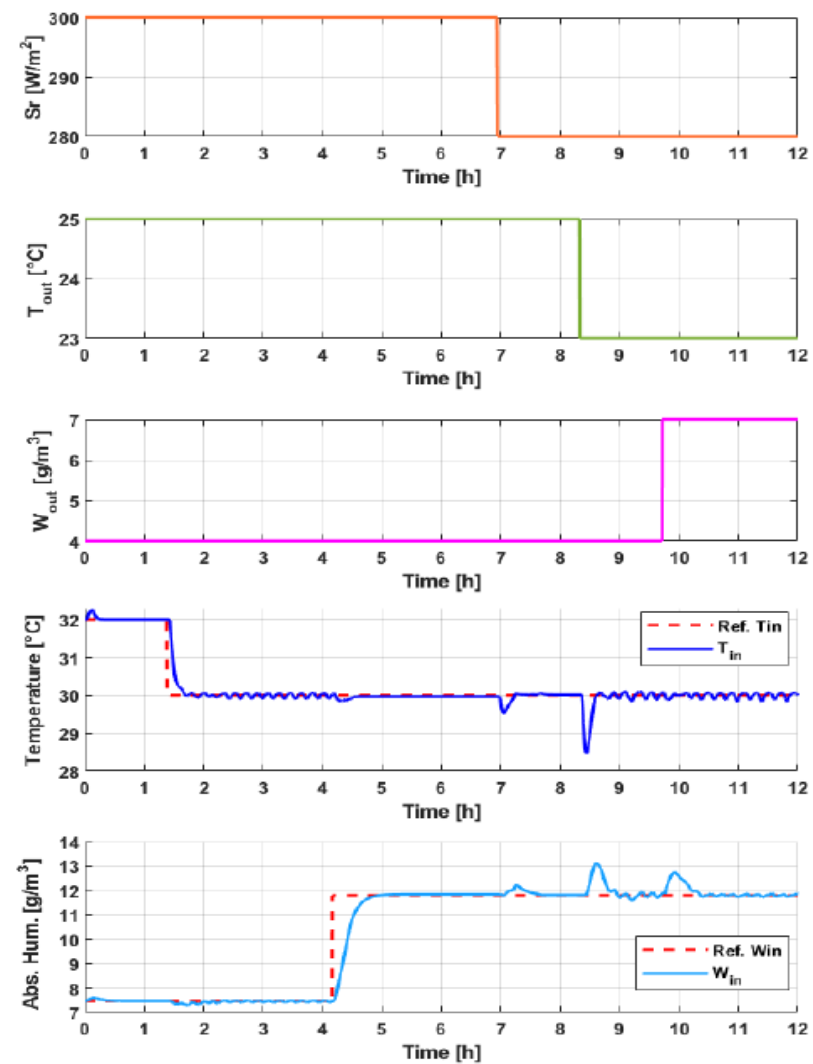
$$G_{c2(z)} = 3.320 \cdot \left( \frac{z - 0.960}{z - 1} \right)$$



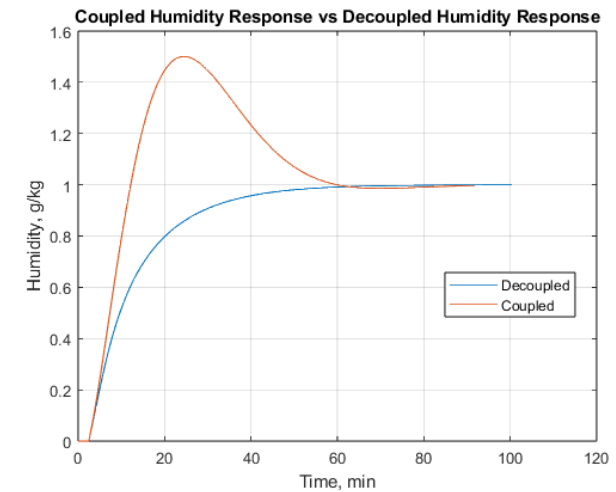
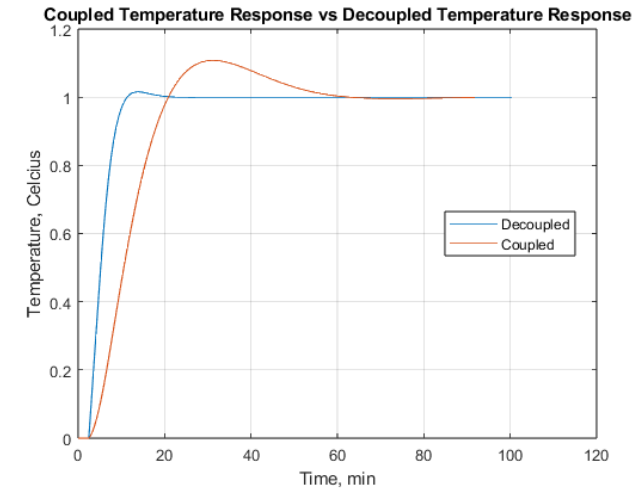
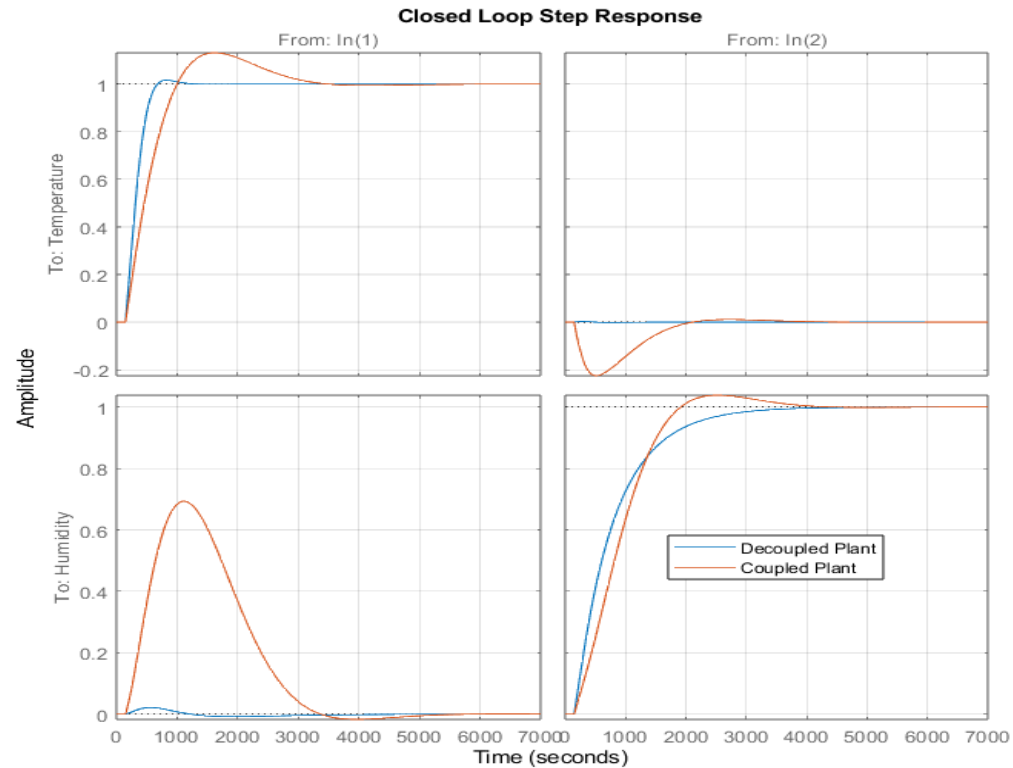
$$u_{1(k)} = u_{1(k-1)} - (1.092)e_{1(k)} + (1.092)(0.856)e_{1(k-1)}$$

$$u_{2(k)} = u_{2(k-1)} + (3.320)e_{2(k)} - (3.320)(0.960)e_{2(k-1)}$$

# ARTICLE RESULTS



# SYSTEM INSIGHTS: DECOUPLING VS COUPLING

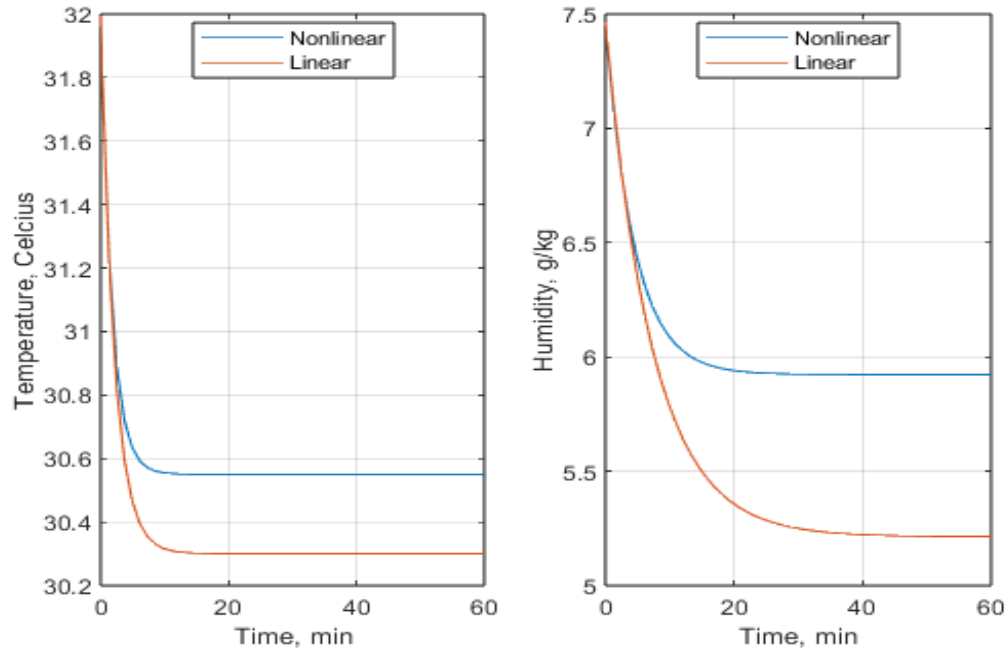


# SYSTEM INSIGHTS: VALIDITY OF LINEAR MODEL

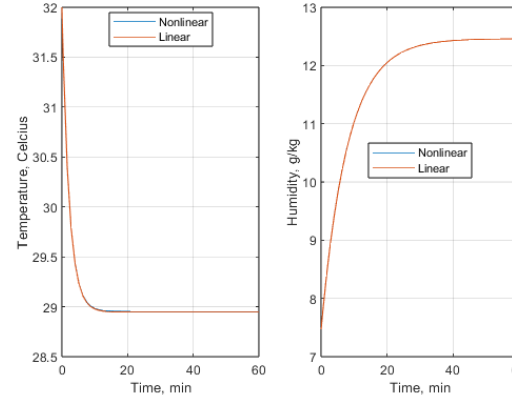
Linear model matches nonlinear system well for most variables over realistic ranges

Linear model breaks down under very little change in venting ( $\pm 1 \text{ m}^3/\text{s}$ )

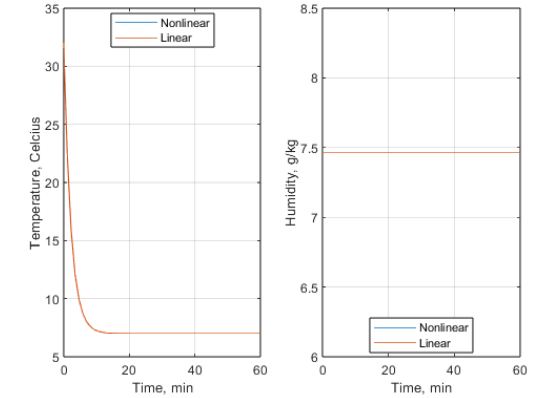
Maximum Venting Action



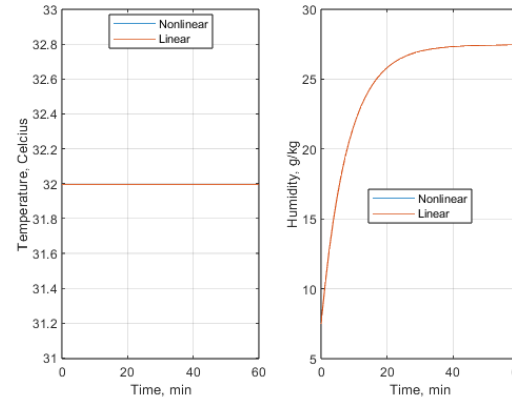
Maximum Fogging Action



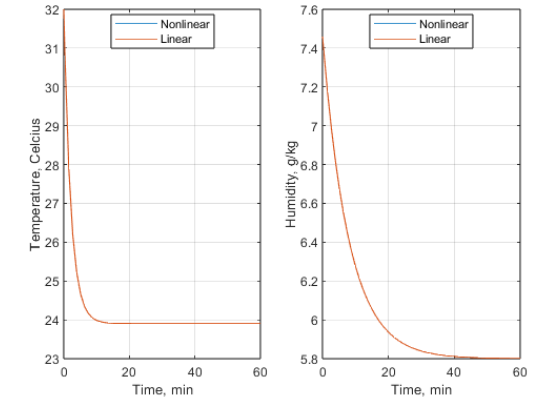
Maximum Outside Temperature Disturbance



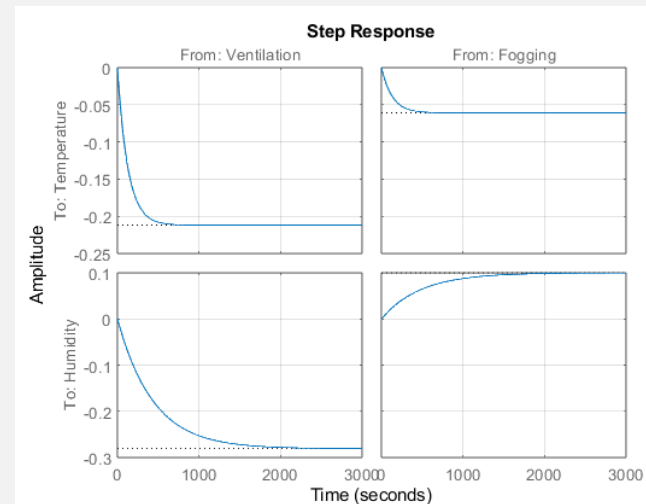
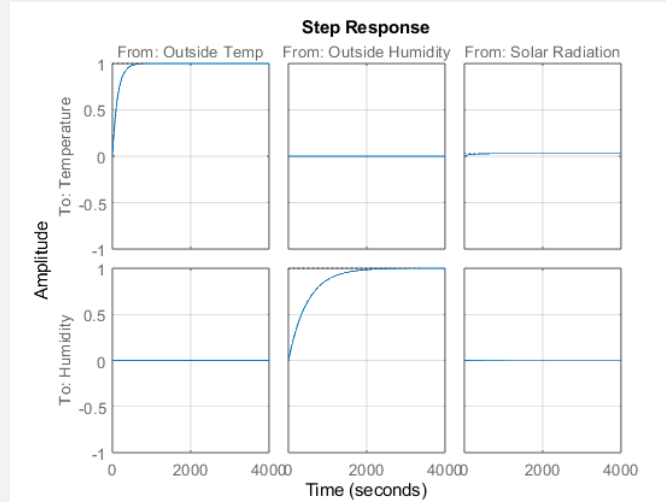
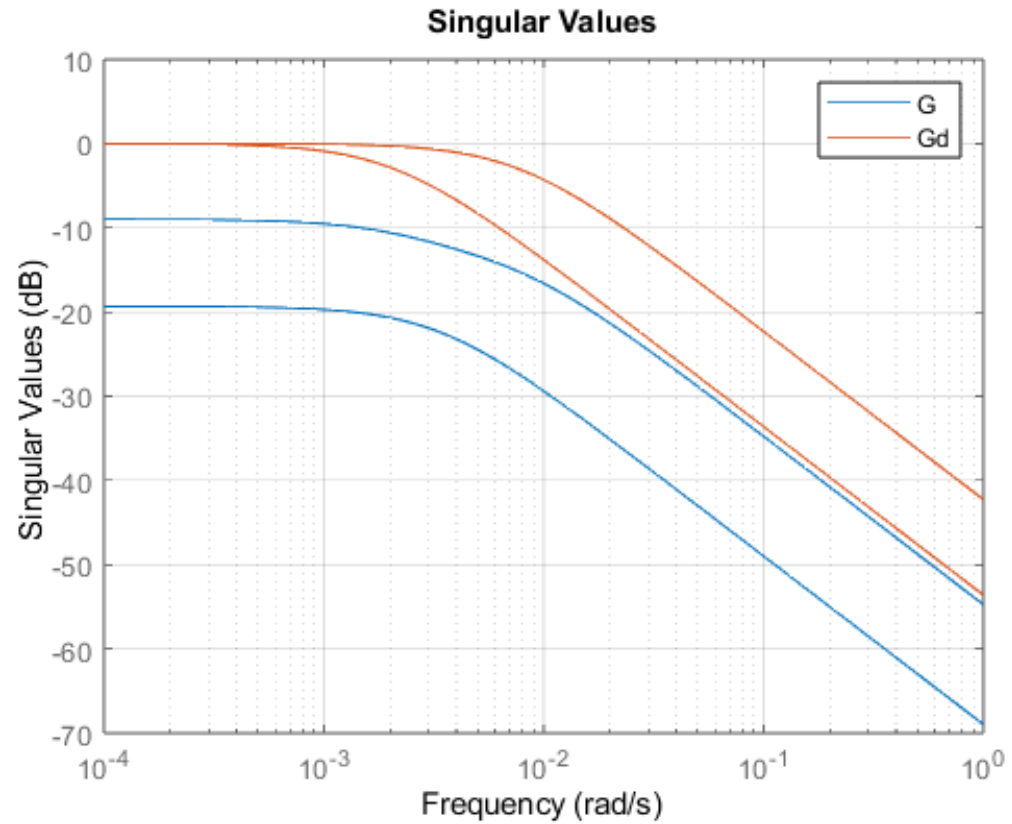
Maximum Outside Humidity Disturbance



Maximum Solar Radiation Disturbance



# SYSTEM INSIGHTS: DISTURBANCE RESPONSES





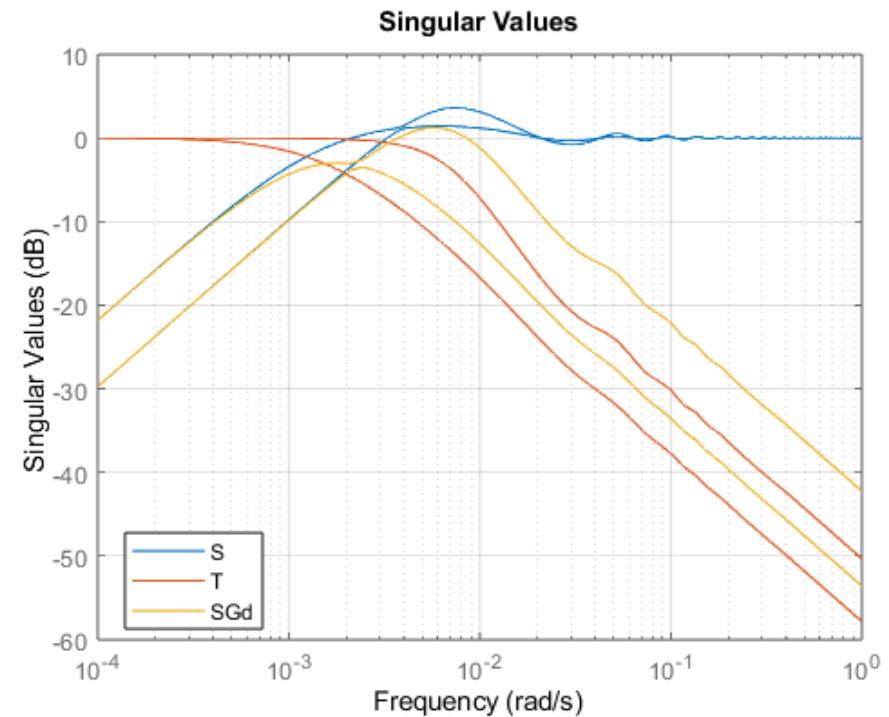
## SYSTEM INSIGHTS: S,T, AND SG<sub>D</sub>

$$\bar{\sigma}(T) \approx 1 \text{ for } \omega < 0.001 \frac{\text{rad}}{\text{s}}$$

- Good tracking at steady state
- Good noise rejection

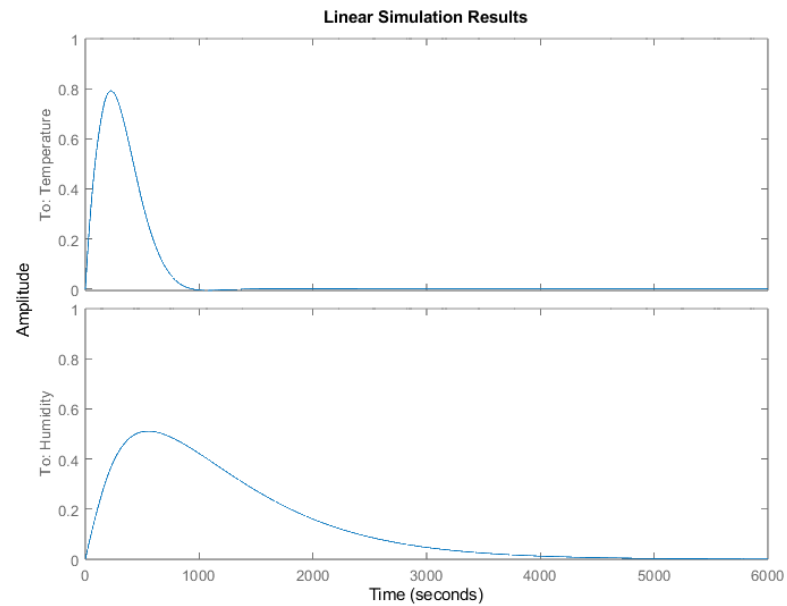
$$\bar{\sigma}(SG_d) > 3\text{dB}, 0.002 < \omega < 0.012$$

- Bad disturbance rejection in this range

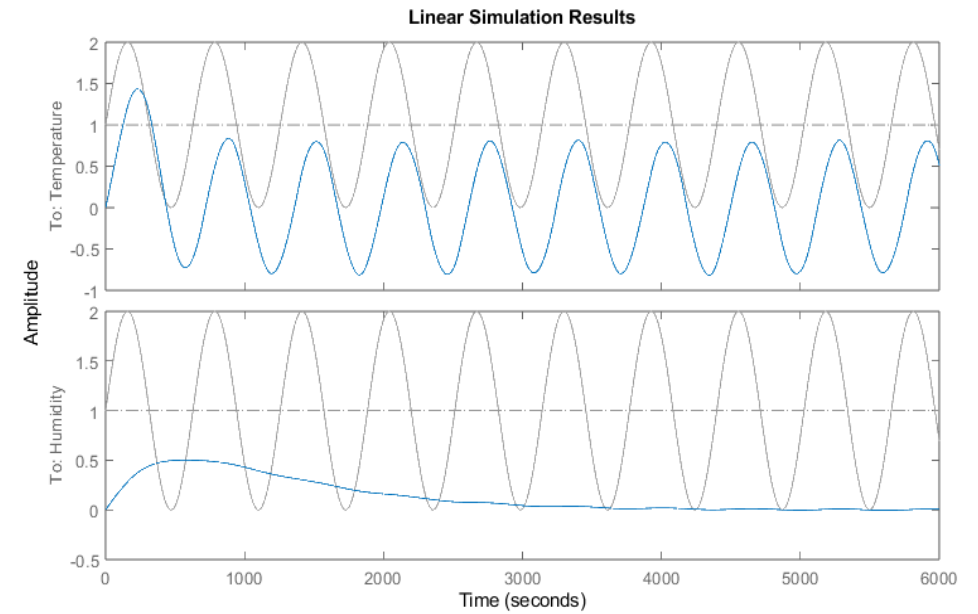


# DISTURBANCE REJECTION

Outside Temperature Step Response ( $\omega=0$ )



Outside Temperature Response ( $\omega=0.01$ )



# REFERENCES

- [1] G. Cevallos, J. Pinzon, and O. Camacho, "A microclimate greenhouse multivariable control: A guide to use hardware in the Loop Simulation," *2022 IEEE International Conference on Automation/XXV Congress of the Chilean Association of Automatic Control (ICA-ACCA)*, 2022.
- [2] *Energy Producing Greenhouse: Organic Photovoltaics Integrated Greenhouse*. 2023.
- [3] S. Trimble. *Transpiration in Plants: Its Importance and Applications*. 2022.
- [4] *Environmental Control Systems*. [Online]. Available: <https://cals.arizona.edu/hydroponictomatoes/system.htm>. [Accessed: 30-Mar-2023].
- [5] S. J. Lilly, "Chapter 11: Plant Health Care," in *Arborists' Certification Study Guide*, P. Currid, Ed. Atlanta, GA: International Society of Arboriculture, 2010, p. 180.
- [6] G. Acquaah, *Horticulture: Principles and Practices*. Upper Saddle River, NJ: Pearson Education, Inc., 2009.
- [7] S. Skogestad and I. Postlethwaite, *Multivariable Feedback Control: Analysis and Design*. Chichester: Wiley, 2005.
- [8] "Continuous-Discrete Conversion Methods," *Continuous-Discrete Conversion Methods - MATLAB & Simulink*. [Online]. Available: <https://www.mathworks.com/help/ident/ug/continuous-discrete-conversion-methods.html#bs78nig-8>. [Accessed: 15-Apr-2023].