

## Why Numerical Methods?

→ To avoid rigorous mathematics (Basically)

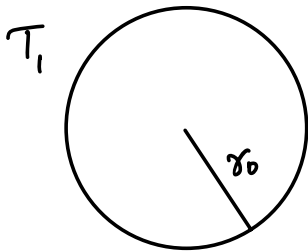
By now, we know &

- ① To make ODE
- ② Expressing B.C.
- ③ Solving diff eqn & applying B.C.

Ex: for 1D steady Cond<sup>n</sup> :

Sphere

$$\frac{1}{r^2} \frac{d}{dr} \left( r^2 \frac{dT}{dr} \right) + \frac{\dot{e}}{k} = 0$$



$$\text{B.C. } \frac{dT}{dr} = 0 \quad \& \quad T(r_0) = T_i$$

⇒ Using this if we solve,

⇒

Analytical Sol<sup>n</sup>,

$$\Rightarrow T(r) = T_i + \frac{\dot{e}}{6k} (r_0^2 - r^2)$$

By this we can also find, rate of  
Heat transfer ( $\dot{Q}$ ) = ? now.

⇒ Fourier's law,

$$\dot{Q}(r) = -kA \frac{dT}{dr} = \frac{4\pi r^3 \dot{e}}{3} \quad \text{Simple!}$$

\* Complexities comes with complex geometries where analytical sol<sup>n</sup> is very getting difficult

+ Even simple geometries can be complex if thermal cond<sup>n</sup> are not sufficiently simple.

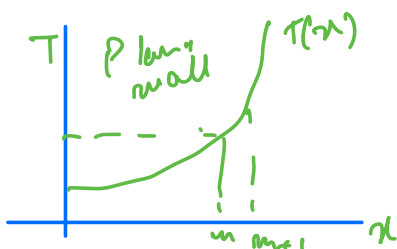
# ES0-208 ⇒ finite Difference Method

forward
Central
Backward

Proof

$$\frac{dT}{dx} \approx \frac{T_m - T_{m-1}}{\Delta x}$$

$$\frac{d^2T}{dx^2} = \frac{\frac{dT}{dx}|_m - \frac{dT}{dx}|_{m-1}}{\Delta x}$$



\* for 1D heat transfer plane

finite difference form<sup>n</sup>.

$$\Rightarrow \left\{ \frac{T_{m-1} - 2T_m + T_{m+1}}{\Delta x^2} + \frac{\dot{e}_m}{k} = 0 \right\}$$

need?

Heat Conduction eq<sup>n</sup> involves this term.

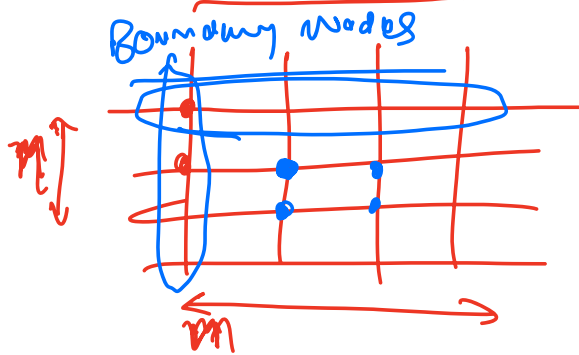
Diff eq<sup>n</sup> is  $\frac{d^2 T}{dx^2} + \frac{\dot{e}}{k} = 0$

$$\rho C_p \frac{\partial T}{\partial t} = \frac{\partial}{\partial x} \left( k \frac{\partial T}{\partial x} \right) - \dot{e}, \dot{e}$$

Extending to 2D, 3D —

$$\frac{T_{m+1,n} - 2T_{m,n} + T_{m-1,n}}{\Delta x^2} + \frac{(\quad)}{\Delta y^2} + \frac{\dot{e}_{m,n}}{k} = 0$$

\* Nodes Used ?



x divided in m region  
y divided in n region

$$\text{Total nodes} \Rightarrow (m+1)(n+1)$$

Finite diff  
applied to

$$(m-1)(n-1) \text{ nodes}$$

To overcome these B.C., we will be using energy conservation method.

$$* \text{Rate of } ( \text{Cond} + \text{Gen} = \text{Change in Energy} )$$

### \* Example

Large Uranium plate of thickness  $L = 4 \text{ cm}$

$$k = 28 \frac{\text{W}}{\text{m} \cdot \text{K}}$$

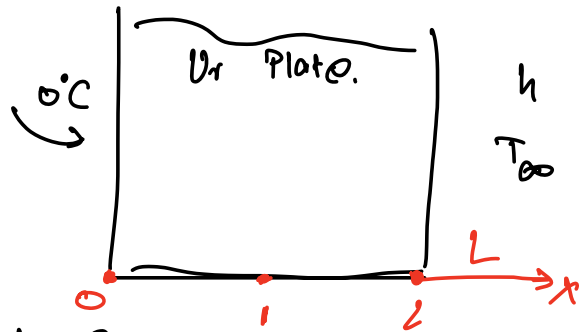
$$\dot{e} = 5 \times 10^6 \frac{\text{W}}{\text{m} \cdot \text{K}}$$

$$h = 45 \frac{\text{W}}{\text{m}^2 \cdot \text{K}}$$

3 Nodes (equal spaced)

estimate exposed surface temp. ?

@ S. State



$$\Delta x = ?$$

$$\frac{L}{m-1} = 0.02 \text{ m}$$

$$T_0 = 0^\circ \text{C} \quad (\text{B.C.})$$

$$T_1, T_2 = ? \Rightarrow \text{unknown nodal Temp}$$

$\Rightarrow$  apply finite diff method

$$m=1 \Rightarrow \frac{T_0 - 2T_1 + T_2}{\Delta x^2} + \frac{\dot{e}_1}{k} = 0 \Rightarrow \textcircled{1}$$

# NODE - 2 B.C  $\Rightarrow$  Energy conservation.

$$hA(T_{\infty} - T_2) + kA \frac{(T_1 - T_2)}{\Delta x} + \dot{Q}_2(A \frac{\Delta x}{2}) = 0$$

solve for  $T_1$  &  $T_2$

$\hookrightarrow$  (2)