

## 1. User Inputs

- Gold head grade (grams/tonne)
- Particle size distributions
  - P50 value (microns)
  - P10 value (microns)
  - P80 value (microns)
- Ore mineralogy (% for each)
  - Pyrite
  - Arsenopyrite
  - Chalcopyrite
  - Sphalerite
  - Galena
  - Calcite
  - Siderite
  - Quartz
  - Feldspars
  - Montmorillonite
  - Kaolinite
- Throughput: tph or tpd
- Reagents:
  - CN(kg/t),
  - Lime(kg/t),
  - Collector A(g/t),
  - Collector B(g/t),
  - Frother(mL/t)

## 2. Ore Classification

- Program analyzes minerals to determine ore type
  - Uses minerals >10% for sulfides
  - Minerals >5% for carbonates
  - Silicates + clays >90% for gangues

## 3. Flowsheet Selection

- Database retrieves relevant flowsheet based on:
  - Ore type
  - Grade & size ranges
  - Key mineral makeup

#### 4. Process Models

##### A. Cyanidation

Rate of Gold Dissolution:

$$d[\text{Au}]/dt = k[\text{Au}][\text{CN}^-]$$

Where:

$$k = A \cdot \exp(-E_a/RT)$$

Arrhenius Equation:

$$k = A \cdot \exp(-E_a/RT)$$

Carbon Adsorption:

Langmuir Equation:

$$q = (q_{\max} \cdot b \cdot C) / (1 + b \cdot C)$$

##### B. Flotation

Collection Efficiency:

$$\alpha = 1 / (1 + \exp((E_b/kT)))$$

DLVO Theory:

$$E_b = E_{vdw} + E_{edl}$$

$$E_{vdw} = -A \cdot (H_1 \cdot H_2 / (H_1 + H_2))$$

$$E_{edl} = (2 \cdot \pi \cdot \epsilon_0 \cdot \epsilon_r \cdot \zeta_1 \cdot \zeta_2) \cdot \exp(-\kappa \cdot H) / (1 + \kappa \cdot H)$$

Let me ensure I properly disclose all parameters for the DLVO equations:

For the  $E_{vdw}$  term:

$$-A \cdot (H_1 \cdot H_2 / (H_1 + H_2))$$

The Hamaker constant (A) can range from  $10^{-20}$  to  $10^{-20}$  Joules.

Particle size ( $H_1$ ) is usually 1-100  $\mu\text{m}$ .

Bubble size ( $H_2$ ) is typically 50-200  $\mu\text{m}$ .

For the  $E_{edl}$  term:

$$(2 \cdot \pi \cdot \epsilon_0 \cdot \epsilon_r \cdot \zeta_1 \cdot \zeta_2) \cdot \exp(-\kappa \cdot H) / (1 + \kappa \cdot H)$$

The permittivity of free space ( $\epsilon_0$ ) is a constant at  $8.85 \times 10^{-12} \text{ C}^2/\text{N}\cdot\text{m}^2$ .

The relative permittivity ( $\epsilon_r$ ) of process water ranges from 2-10.

Zeta potentials ( $\zeta_1$  and  $\zeta_2$ ) on particle and bubble surfaces usually fall between  $\pm 10$ -100 mV.

The inverse Debye length ( $\kappa$ ) is commonly  $10^8$ - $10^{10} \text{ m}^{-1}$ .

The separation distance (H) in colloid systems is on the nanoscale, around 1-1000 nm.

Rate Equation:

$$dC/dt = k(C - C^*)$$

You're right, to fully disclose how C is modeled I should state the formulas and constants.

In the flotation rate equation:

$$dC/dt = k(C - C^*)$$

C represents the concentration of valuable metal/mineral in the flotation concentrate at any given time.

If plant data on concentrate grade (C values) over time is provided, the model uses that directly.

If no time-based C data is available, the model calculates C implicitly using the integrated rate law formula:

$$C = C^* - (C^* - C_0)e^{-kt}$$

Where:

$C_0$  = initial concentration in pulp/feed

$C^*$  = equilibrium/maximum concentration (65-90% of the head grade.)

k = rate constant from Arrhenius equation

t = time.

The rate constant k is calculated using the Arrhenius equation:

$$k = A \cdot \exp(-E_a/RT)$$

Where:

A = pre-exponential factor, typically 1011 m<sup>3</sup>/g-min

E<sub>a</sub> = activation energy, usually 50 kJ/mol

R = universal gas constant, 8.314 J/mol-K

T = temperature in Kelvin

### C. Gravity

Particle Settling:

$$v = g \cdot (\rho_p - \rho_f) / 18 \cdot \mu \cdot d^2$$

The variables are:

v = terminal settling velocity

g = acceleration due to gravity, 9.81 m/s<sup>2</sup>

ρ<sub>p</sub> = particle density, 2500 - 4000 kg/m<sup>3</sup>

ρ<sub>f</sub> = fluid density, approximately 1000 kg/m<sup>3</sup>

μ = fluid viscosity, ranging from 0.0005-0.005 Pa·s

d = particle diameter

### D. Heap/CIL/CIP

Leaching:

Same as cyanidation above

Dynamic Tank Model:

$$dV/dt = F_{in} - F_{out}$$

$$dC/dt = (F_{in}C_{in} - F_{out}C_{out})/V + R - kC$$

You're quite right, I should disclose all parameters for the dynamic tank model equations as well. Here are the constants and ranges:

Dynamic Tank Model:

$$dV/dt = F_{in} - F_{out}$$

F<sub>in</sub> = Inlet flow rate (m<sup>3</sup>/hr)

Range: Depends on tank size, usually 0.5-50 m<sup>3</sup>/min or 50-5000 m<sup>3</sup>/hr

**F<sub>out</sub>** = Outlet flow rate

Calculated from volume and residence time (5-60 min typical)

$$dC/dt = (F_{in}C_{in} - F_{out}C_{out})/V + R - kC$$

**C<sub>in</sub>** = metal concentration entering tank (g/L)

Ranges: 0.1-10 g/L

**C<sub>out</sub>** = metal concentration leaving tank (g/L)

Calculated based on recovery performance

**V** = volume in tank (m<sup>3</sup>)

Ranges: 10-1000 m<sup>3</sup>

**R** = metal recovery/extraction rate (g/L-hr)

Estimated using leach kinetics rate equations

**k** = metal dissolution/desorption rate constant (1/hr)

Ranges: 0.001-0.1 1/hr

**Carbon Contact:**

Forward:  $k_1 C Q$

$k_1$  range: 0.005 - 0.015 L/g-min

Reverse:  $k_{-1} Q$

$k_{-1}$  range: 0.0025 - 0.0075 1/min

For carbon saturation  $Q$ :

$$Q = Q_0 * e^{(-k_3 * t)}$$

$Q_0$  range: 50 - 150 mg metal/g carbon

$k_3$  range: 0.0005 - 0.0015 1/min

$t$  is time elapsed.

The  $C$  concentration in the dynamic tank model is calculated from:

$$C = C^* - (C^* - C_0)e^{-kt}$$

C0 range: Head grade +/- 20%

C\* range: 70-95% of C0

k from Arrhenius equation:  $A=10^{11}$ ,  $E_a=30-80$  kJ/mol

## 5. Initial Recovery Prediction comprehensive technical list of all inputs, formulas, parameters and constants

Formulas:

Comminution:

- Bond Work Index (kWh/t) =  $13.048 \cdot (P_{80})^{-0.4915}$

Gravity Recovery Formula:

-  $R_g(\%) = 100 \cdot (1 - e^{-kt})$

Where:

k = specific rate constant (hr<sup>-1</sup>) derived from batch tests

Range: 0.1-1 hr<sup>-1</sup> for free gold

Particle size dependent

t = residence time in gravity circuit (hrs)

Typical range: 0.25-1 hrs

Flotation Recovery Formula:

-  $R_f(\%) = 100 \cdot (1 - e^{-kt})$

Where:

k = flotation rate constant

Range: 0.02-0.5 hr<sup>-1</sup>

t = flotation cell residence time (mins)

Range: 20-60 mins

Leach Recovery Formula:

-  $R_l(\%) = 100 \cdot (1 - e^{-kt})$

Where:

k = rate constant from leach kinetic tests

t = residence time in leach circuit (hrs)

Range: 12-72 hrs

Carbon Adsorption Formula:

-  $q = k \cdot C \cdot t$

Where:

k = rate constant (L/g/hr)

Dependent on: Particle size, pH, temp

Range: 0.01-1 L/g/hr

C = gold concentration in pulp (g/L)

t = contact time in CIL/CIP (hrs)

Range: 6-24 hrs

Overall Recovery:

-  $R_t = R_g + R_f + R_l - R_g \cdot R_f - R_g \cdot R_l - R_f \cdot R_l + R_g \cdot R_f \cdot R_l$

Constants:

- Gravity recovery limits = 95-98%
- Leach residence times = 6-72 hrs
- Equipment throughputs in tph
- Bond Work Index ranges by ore type = 10-18 kWh/t
- Carbon loading capacities = 25-50 g Au/t
- Reagent consumptions per tonne of ore

Parameters:

- Rate constants (k) from batch tests = 0.01-1 hr<sup>-1</sup>
- Process water requirements in m<sup>3</sup>/hr
- Energy inputs by unit operation

Let me know if you require any additional information! Metallurgical modeling is central to optimization.

## 6. Total Recovery Projection

- Monte Carlo simulations varying inputs 1000 times
- Returns mean, standard deviation, confidence intervals

## 7. Optimization Simulation

- Adjusts parameters over ranges to maximize recovery