SVKM's D. J. Sanghvi College of Engineering

Program: B.Tech in Mechanical Academic Year: 2022 Duration: 3 hours

Engineering Date: 07.01.2023

Time: 10:30 am to 01:30 pm

Subject: Heat Transfer (Semester V)

Marks: 75

Instructions: Candidates should read carefully the instructions printed on the question paper and on the cover page of the Answer Book, which is provided for their use.

- (1) This question paper contains three pages.
- (2) All Questions are Compulsory.
- (3) All questions carry equal marks.
- (4) Answer to each new question is to be started on a fresh page.
- (5) Figures in the brackets on the right indicate full marks.
- (6) Assume suitable data wherever required, but justify it.
- (7) Draw the neat labelled diagrams, wherever necessary.

Question		Max.			
No.	l N				
Q1 (a)	Explain the term critical insulation thickness. Derive an expression for the critical radius of insulation for a sphere.				
Q1 (b)	 i. A thermopane (thermally insulated glass) window that is 0.6 m long by 0.3 m wide comprises two 8 mm thick pieces of glass sandwiching an 8 mm thick stagnant air space. The thermal conductivity of glass is 1.4 W/m K and that of air is 0.025 W/m K. The window separates room air at 20°C from outside ambient air at -10°C. The convection coefficients associated with the inner (room side) and the outer (ambient) surfaces are 10 W/m²K and 80 W/m²K respectively. (a) Determine the heat loss through the window, and the two surface temperatures. (b) What would be the heat loss if the window had a single glass of 8 mm thickness instead of a thermopane? OR ii. A composite cylinder consists of 100 mm radius steel pipe of 25 mm thickness over which two layers of insulation 30 mm and 35 mm are 	[10]			
02()	laid. The conductivities are 25 W/mK, 0.25 W/mK and 0.65 W/mK. The inside is exposed to convection at 300°C with h = 65 W/m ² K. The outside is exposed to air at 30°C with h = 15 W/m ² K. Determine the heat loss per meter length. Also find the interface temperatures.	[07]			
Q2 (a)	For transient heat conduction, with negligible internal resistance with usual notations show that, $\frac{\theta}{\theta_i} = e^{(B_i \times F_0)}$.				
Q2 (b)	i. A metal rod is attached horizontally to a large tank at a temperature of 200°C. The rod has 1 cm diameter, 30 cm length and thermal conductivity of 65 W/mK. The rod dissipates heat by convection into the ambient air at 20°C with heat transfer coefficient of 15 W/m²K. What is the temperature of the rod at 10 cm and 20 cm from the tank? Assuming the rod as a long fin, Calculate the heat transfer rate, the fin efficiency and effectiveness.	[08]			

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	OR	[80]	
	ii. The handle of a ladle used for pouring molten lead at 328°C is 30 cm long. Originally the handle was made of 1.3 cm by 2.0 cm mild steel bar stock. To reduce the grip temperature, it is proposed to form a hollow handle of 1.5 mm thick mild steel tubing to the same rectangular shape. The average heat-transfer coefficient over the handle surface is 17 W/m ² K, when the ambient air temperature is 28°C. The thermal conductivity of mild steel is 43 W/m ² K. Determine the reduction in the temperature of the grip, stating the assumptions made.		
Q3 (a)	Using Buckingham's π method, derive an expression for heat transfer	[07]	
	coefficient in free convection in terms of Nusselt number, Grashof number and Prandtl number.		
Q3 (b)	i. A refrigerated truck is moving at a speed of 85 km/h where ambient temperature is 50°C. The body of the truck is of rectangular shape of size 10 m (Length), 4 m(Width) and 3 m(Height). Assume the boundary layer is turbulent and the wall surface temperature is at 10°C. Neglect heat transfer from vertical front and backside of truck and flow of air is parallel to 10 m long side. Calculate heat loss from the four surfaces. For turbulent flow over flat surfaces: Nu = 0.036 Re ^{0.8} × Pr ^{0.33} Average properties of air at 30°C: ρ = 1.165 kg/m³, Cp = 1.005 kJ/kgK, ν = 16 ×10 ⁻⁶ m²/s, Pr = 0.701	[80]	
	 ii. A hot, square plate, 50 cm × 50 cm, at 100°C is exposed to atmospheric air at 20°C. Find the heat loss from both the surfaces of the plate: (i) if the plate is kept vertical (ii) if the plate is kept horizontal. Properties of air at mean temperature of 60°C are given below: ρ = 1.06 kg/m³, k = 0.028 W/mK, v = 18.97 × 10⁻⁶ m²/s, Cp = 1.008 kJ/kgK. Following empirical relations can be used: Case (i): Nu = 0.13 × (Gr Pr)^{1/3} Case (ii): Nu = 0.71 × (Gr Pr)^{1/4} for the upper surface, and Nu = 0.35 × (Gr Pr)^{1/4} for the lower surface. 	[08]	
Q4 (a)	Nu = $0.35 \times (Gr Pr)^{1/4}$ for the lower surface. A spherical liquid oxygen tank, 0.3 m in diameter is enclosed concentrically in a spherical container of 0.4 m diameter and the space in between is evacuated. The tank surface is at $-183^{\circ}C$ and has an emissivity of 0.2. The container surface is at $25^{\circ}C$ and has an emissivity of 0.25. Determine the net radiant heat transfer rate.		
Q4 (b)	 i. State and explain Kirchhoff's law of radiation. ii. Write a short note on properties of view factor. iii. State Wein's law of displacement and prove that monochromatic emissive power of a black body is maximum when λmT = constant. 	[05] [05] [05]	
Q5 (a)	A chemical (Cp = 3.3 kJ/kgK) following at the rate of 20000 kg/hr enters a parallel flow heat exchanger at 120°C. The flow rate of cooling water (Cp = 4.186 kJ/kg K) is 50000 kg/h with an inlet temperature of 20°C. The heat-transfer surface area is 10 m² and the overall heat transfer coefficient is 1050 W/m²K. Calculate the (a) effectiveness of the heat exchanger, and (b) outlet temperatures of water and chemical.	[07]	

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Q5 (b)	i.	Derive an expression for the LMTD of a counter flow type heat	[08]
		exchanger. Also list the assumptions made in the analysis.	
		OR	
	ii.	Starting from basics, derive an equation for the effectiveness of a parallel-flow heat exchanger in terms of NTU and capacity ratio.	[08]

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