



Name : .....

Roll No. : .....

Invigilator's Signature : .....

**CS / B.TECH(CHE)(N) / SEM-5 / CHE-501 / 2012-13**

**2012**

**SEPARATION PROCESS-I**

*Time Allotted : 3 Hours*

*Full Marks : 70*

*The figures in the margin indicate full marks.*

*Candidates are required to give their answers in their own words  
as far as practicable.*

*Graph sheet (mm) will be supplied by the Institute on demand.*

**GROUP – A**

**( Multiple Choice Type Questions )**

1. Choose the correct alternatives for any *ten* of the following :  $10 \times 1 = 10$ 
  - i) The absorption factor along with its most economical value is given as
    - a) Ratio of slope of equilibrium line to operating line;  
1.2 to 2
    - b) Ratio of slope of operating line to equilibrium line;  
0.5 to 1
    - c) Ratio of slope of operating line to equilibrium line;  
1.25 to 2
    - d) Ratio of slope of operating line to equilibrium line;  
0 to 1.



- ii) NTU is numerically equal to Number of Theoretical plates only when operating line
  - a) lies below the equilibrium curve
  - b) lies above the equilibrium curve
  - c) and the equilibrium lines are straight and parallel
  - d) is far from the equilibrium line.
- iii) In physical terms, Schmidt number means
  - a) Thermal diffusivity/mass diffusivity
  - b) Thermal diffusivity/momentum diffusivity
  - c) Momentum diffusivity/mass diffusivity
  - d) Mass diffusivity/thermal diffusivity.
- iv) Distillation process belongs to the which one of the following phases in contact ?
  - a) Solid—liquid
  - b) Solid—gas
  - c) Liquid—liquid
  - d) Vapour—liquid.
- v) Steam distillation is used to separate
  - a) azeotropes
  - b) high boiling substances from non-volatile impurities
  - c) heat sensitive materials
  - d) mixtures of low relative volatility.



- vi) Physical adsorption is
- an irreversible phenomenon
  - a reversible phenomenon
  - accompanied by evolution of heat
  - both (b) and (c).
- vii) A feed mixture of distillation contains 25% liquid and rest is vapour.  $q$  value of the mixture is
- 3
  - 0
  - $\frac{1}{4}$
  - $\frac{3}{4}$ .
- viii) Wetted wall tower experiments determines
- molar diffusivity
  - volumetric coefficient
  - mass transfer coefficient
  - none of these.
- ix) At the azeotropic composition of a binary mixture, the relative volatility is
- 0
  - 1
  - $< 1$
  - $\infty$ .
- x) With lowering of equilibrium pressure, at a given temperature the amount of adsorbate on the adsorbent
- increases
  - decreases
  - remains same
  - either (a) or (b) depends on the system.



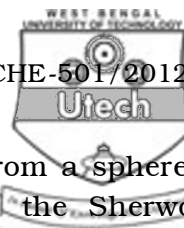
- xi) Minimum number of theoretical plates are required in distillation process in case of
- a) Total Reflux
  - b) Infinite Reflux
  - c) Minimum Reflux
  - d) Both (a) and (b).
- xii) The length of the unused bed (LUB) is more if the mass transfer zone is
- a) wide
  - b) narrow
  - c) asymmetric
  - d) symmetric.

**GROUP – B**

**( Short Answer Type Questions )**

Answer any *three* of the following.  $3 \times 5 = 15$

2. Show that for a binary gas mixture, the diffusivity of *A* in *B* equals the diffusivity of *B* in *A*. 5
3. Show that according to film theory, mass transfer coefficient is proportional to diffusivity and according to penetration theory, mass transfer coefficient is proportional to the square root of diffusivity. 5



4. Prove that for equimolar counter-diffusion from a sphere to a surrounding stationary infinite medium, the Sherwood number based on the diameter of the sphere is equal to 2. 5
5. Hydrogen gas at 2 atm pressure and 250 C flows through a neoprene rubber with internal dia and outer dia of 25 mm and 50 mm respectively. The solubility of hydrogen is reported as  $0.053 \text{ m}^3 \text{ S.T.P./m}^3 \text{ atm}$  and the diffusivity of hydrogen gas through rubber is  $0.0000018 \text{ cm}^2/\text{sec}$ . Estimate the loss of hydrogen by diffusion per metre length of pipe. 5
6. How is the height of overall gas phase transfer unit  $H_{OG}$  related to the height of gas film transfer unit  $H_G$  and the height of liquid film transfer unit  $H_L$  if the equilibrium relationship is given by  $y^* = mx$  and gas flow rate and liquid flow rates are given by  $G_m$  and  $L_m$  ? 5

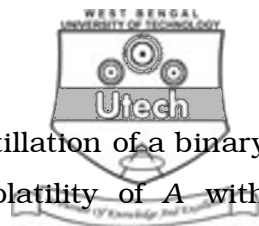
### GROUP – C

#### ( Long Answer Type Questions )

Answer any *three* of the following.  $3 \times 15 = 45$

7. A spherical gas bulb of volume 500 c.c. contains air- $\text{NH}_3$  mixture in the volume ratio 4 : 1 at  $40^\circ \text{ C}$  and 1 atm pressure. It is exposed to the atmosphere at the same temperature and pressure through a tapered capillary of length 5 cm. The diameter at the left hand side is 2 mm, and that at the right hand side, which is exposed to atmosphere, is 1 mm. If the gas bulb is left open as such, find the  $\text{NH}_3$  concentration in the bulb after 15 minutes.  $D_{AB}$  for air- $\text{NH}_3$  at  $0^\circ \text{ C}$  and 1 atm pressure is  $0.198 \times 10^{-4} \text{ m}^2/\text{s}$ . State all the assumptions made for solving the problem.

12 + 3



8. a) Derive Rayleigh equation of batch distillation of a binary mixture  $A$  and  $B$  where relative volatility of  $A$  with respect to  $B$  is  $\alpha$ . Explain azeotropic distillation.

- b) The Antoine constants for benzene and toluene are as follows :

$$\text{For benzene : } A = 6.906, B = 1211.03, C = 220.79$$

$$\text{For toluene : } A = 6.95, B = 1343.9, C = 219.37$$

The equation is as follows :

$$\log P^\circ = A - B / (t + C) \text{ where } P^\circ = \text{mm Hg and } t \text{ is in } ^\circ\text{C}$$

Determine vapour composition of a mixture in equilibrium with a liquid mixture of 0.5 mole fraction benzene and 0.5 mole fraction of toluene at 338 K. Will the liquid vaporize at  $101.3 \text{ kN/m}^2$  ?

- c) The liquid of 50 mole %  $n$ -heptane (more volatile) and 50 mole %  $n$ -octane were subjected to a differential distillation at atmospheric pressure, with 60 mole % of the liquid distilled. Compute the composition of the composited distillate and the residue graphically [ Graph paper (mm) will be required ].

The equilibrium data are given below :

$x :$	0.5	0.46	0.42	0.38	0.34	0.32
$y^*$	0.689	0.648	0.608	0.567	0.523	0.497

5 + 5 + 5



9. A liquid mixture of benzene-toluene is to be distilled in a fractionating tower at 101.3 kPa pressure. The feed of 100 kmol/h is liquid, containing 45 mol % of benzene and the rest is toluene enters at 327.6 K. A distillate containing 95 mol % of benzene and the bottoms containing 10 mol % of benzene are to be obtained. The reflux ratio is 4 : 1. The average heat capacity of the feed is 159 kJ/kmolK and the average latent heat is 32099 kJ/kmol. Calculate the amount of distillate, bottoms and the number of theoretical trays needed. Equilibrium data for this system are given below (at 101.325 kPa ) :

$x_A :$	1.00	0.78	0.58	0.41	0.26	0.13	0.00
$y_A$	1.00	0.90	0.78	0.63	0.46	0.26	0.00

10. State basic assumptions for Langmuir type adsorption. Derive mathematical expression for Langmuir isotherm. Discuss the graphical method of determining usual parameters of the isotherm. 3 + 7 + 5
11. a) What are the desirable properties of an adsorbent ? Give examples of commonly used adsorbent.
- b) Write short notes on Breakthrough curve in adsorption.
- c) Show that Freundlich isotherm is a special case of Langmuir isotherm. 5 + 5 + 5

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