

1D EJECTOR SIMULATION TOOL

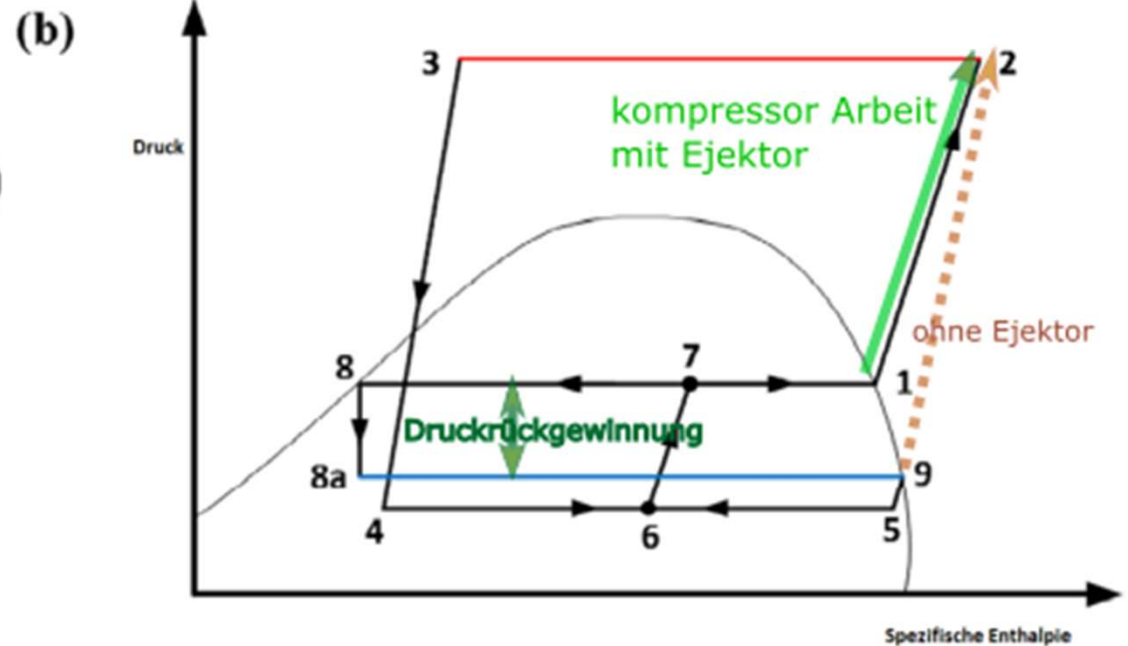
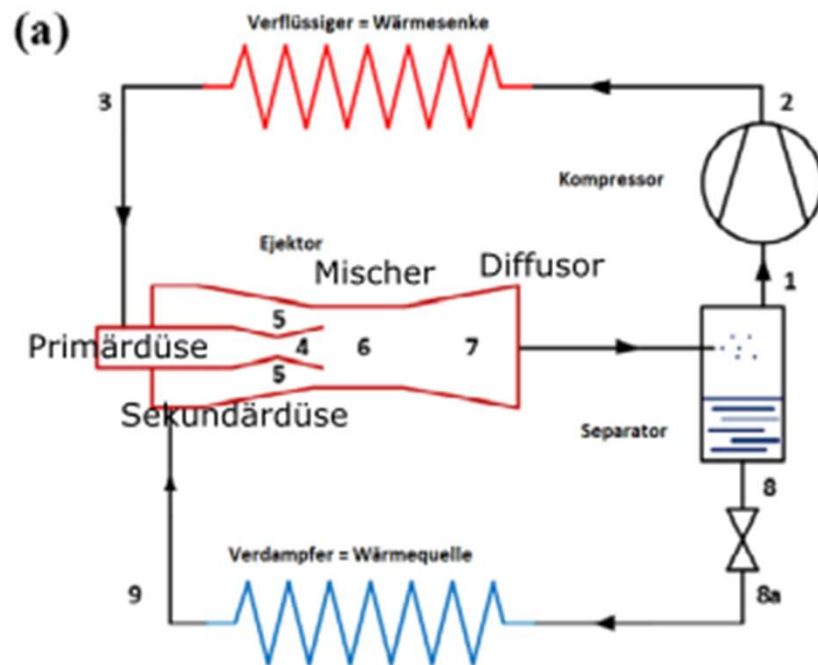
ONE DIMENSIONAL EJECTOR DESIGN FOR HEAT PUMPS

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EJECTORS FOR HEAT PUMPS



$$\text{Pressure recovery ratio} = \frac{p_7}{p_9}$$

higher Pressure
recovery



Compressor
less work



Better COP

Experiment: difficult and expensive.
 New Geometrie → new Fabrication
 Sensors influence the Fluid Flow
 Therefore need for **Simulation**

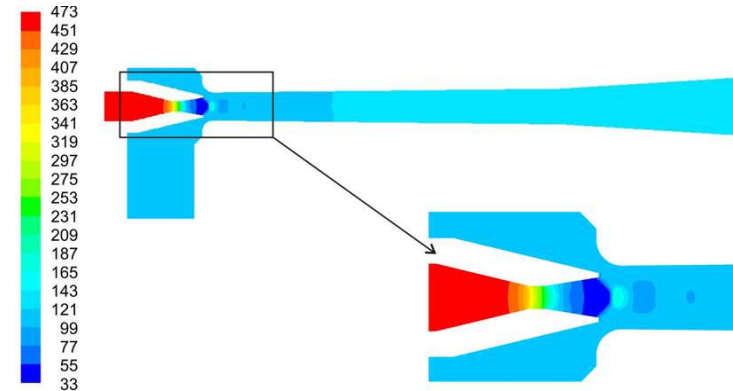
CFD SIMULATION

Advantage:

- Precision: Turbulence etc,
- Equilibrium and Non Equilibrium models.
- Axialsymmetry : 3D → 2D.

Disadvantage:

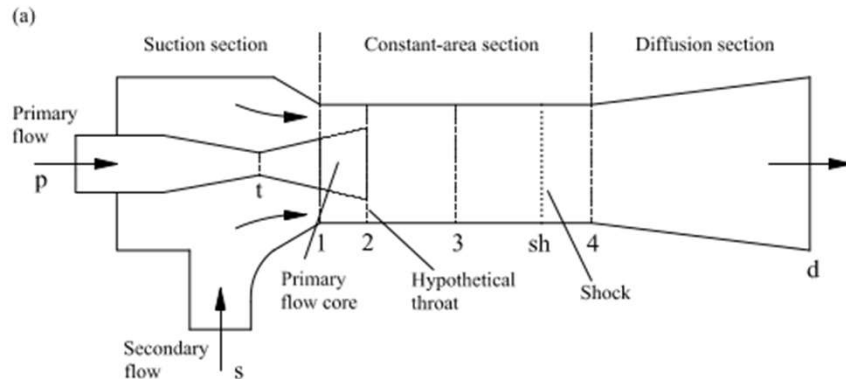
- Disadvantage: Time: Hours / Days
- Often problems with convergence
- Great Know-how + Experience from the Engineer is needed



From Smolka et al. 2013

Need for fast, simple to use Simulation tool
 For Ejector design and optimization

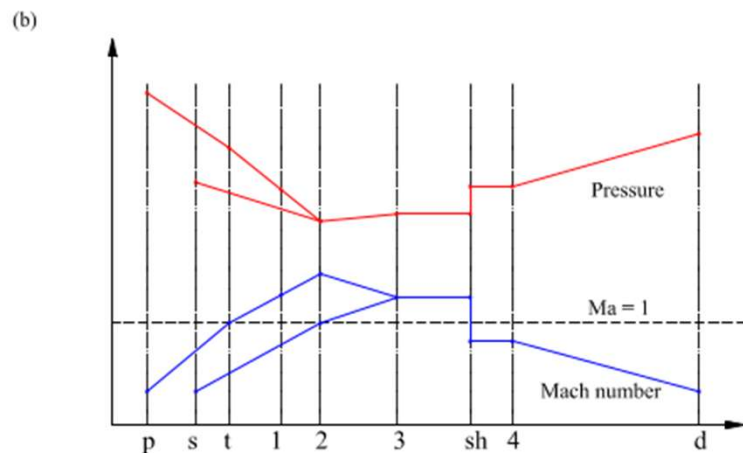
ONE DIMENSIONAL MODELS



Assumption of *Munday-Bagster*: no mixing before the hypothetical throat

Solving the equations for

- Mass conservation
- Momentum equation
- Energy Conservation
- Thermodynamics: Equilibrium, one or two phase flow with Homogeneous Equilibrium models..



Choking :

The Primary mass flow reaches a maximum value → Primary nozzle works like a supersonic Laval-Nozzle.

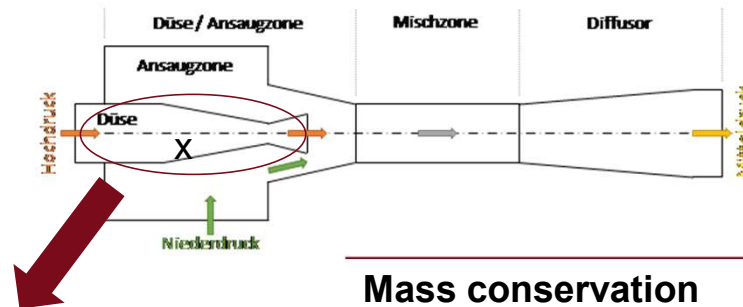
Double Chocking:

The secondary nozzle mass flow also reaches critical maximum value

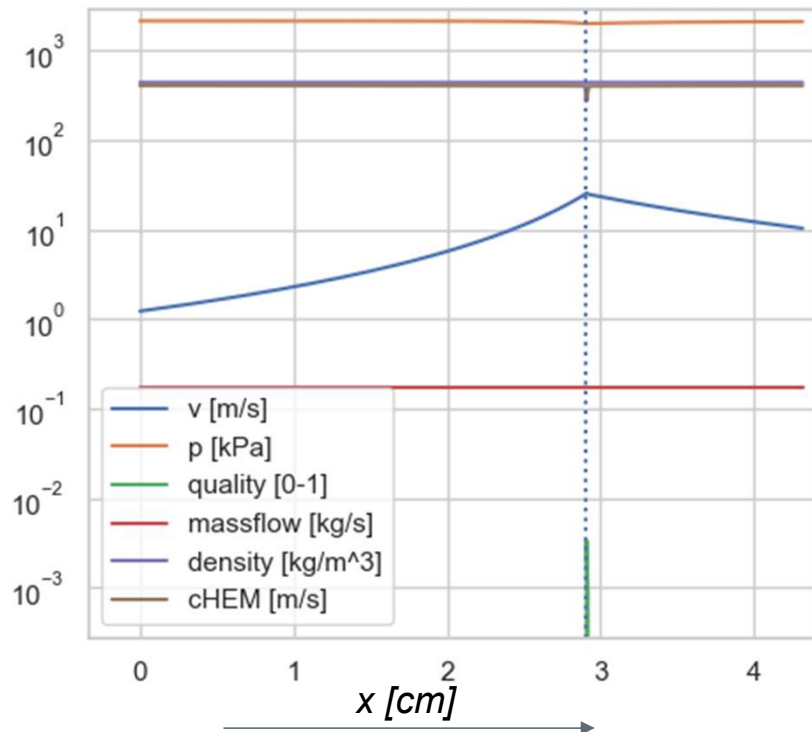
Single Choking:

- The secondary mass flow below the critical maximum value.
- The mass flow will be governed by the pressure ratio.

MOTIVE NOZZLE 1D MODELL



Subkritische Strömung. Reibungsfaktor = 0.01



Mass conservation

$$\dot{M} = \rho A v = const.$$

Momentum

$$-f \sqrt{\frac{\pi}{A}} \frac{\dot{M}}{A} v(x) = \frac{\dot{M}}{A} \frac{dv}{dx} + \frac{dp}{dx}$$

Energy

$$0 = v(x) \frac{dv}{dx} + \frac{dh}{dx}$$

Homogeneous Equilibrium (HEM)

Density from RefProp library

$$\rho(x) = RP_{\rho}(p(x), h(x))$$

Assumption:

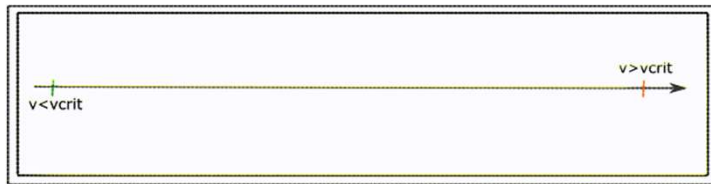
- Viscosity neglected
- Friction with Faktor f (Darcy Weisbach Eq.)
- Turbulence neglected
- Homogeneous Fluid after the phase transition

Solution:

- Initial value problem: from the speed by the prim nozzle inlet
→ Equation System of Differences (Forward differencial)
- Self made adaptive Solution method

MOTIVE NOZZLE II: CHOKING: CRITICAL MASS FLOW

Finding the critical Mass flow with
Bisection method:

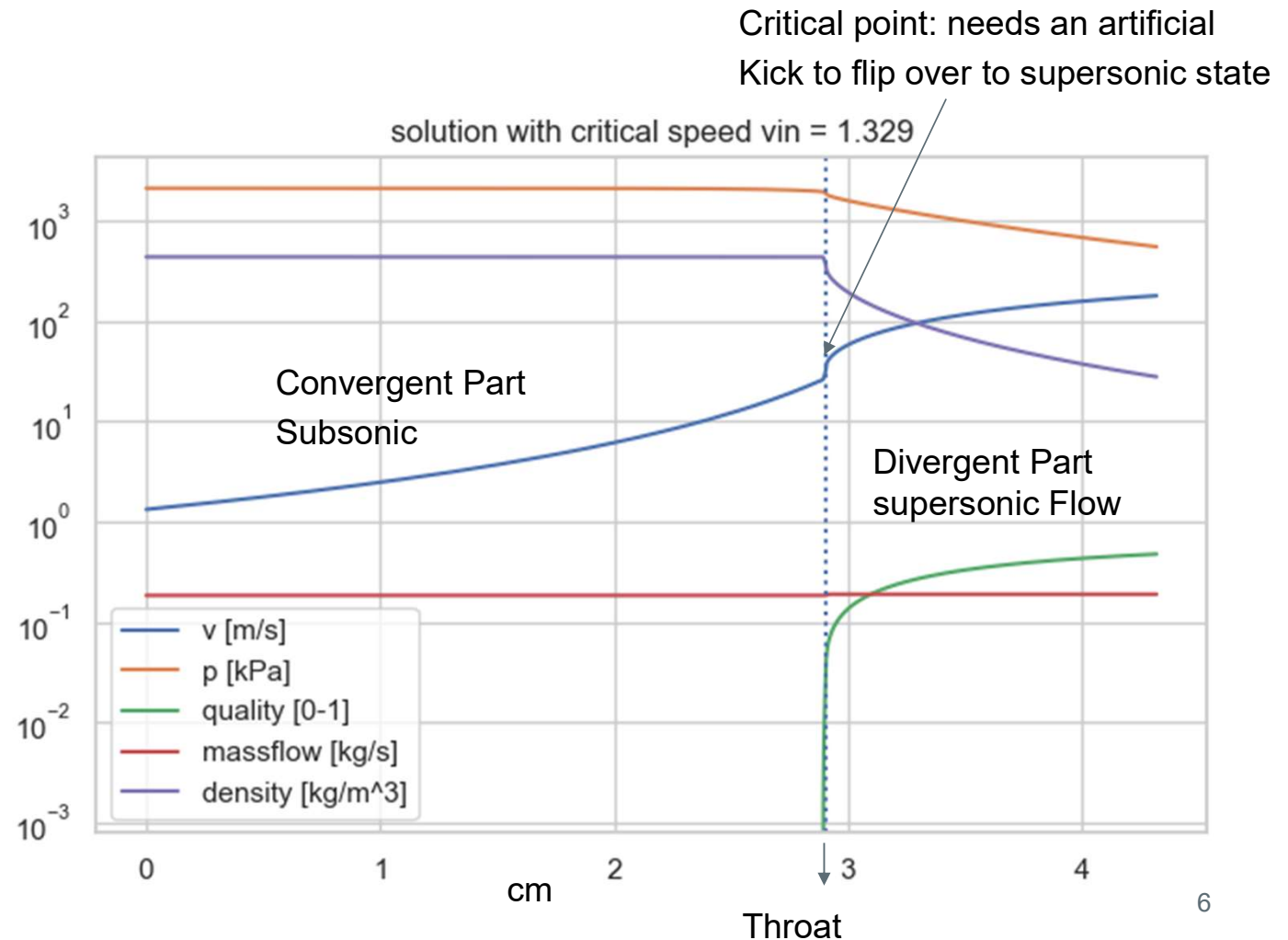


Experiment : Primary nozzle of a Butan
Ejector from *Schlemminger et al. 2019*

$P = 21.4 \text{ bar}$, $T = 114 \text{ }^{\circ}\text{C}$

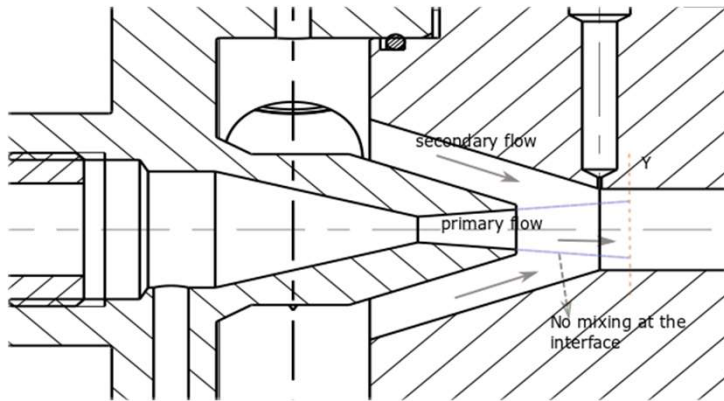
Primary nozzle Mass flow:

Simulation	Experiment
0.184 kg/sec	0.127 kg/sec



PRE-MIXER (OLD)

0-DIMENSIONAL EQUATIONS



Munday-Bagster Hypothesis:

- No mixing until cross section Y

Critical Operating mode (Double Choking mode):

Secondary flow reaches the speed of sound by Y:

$$v_{SY} = \text{RP}_c(p_Y, h_{SY}) \text{ (RefProp)}$$

\dot{m}_S is calculated from that.

Subcritical Operating mode(single Choking mode):

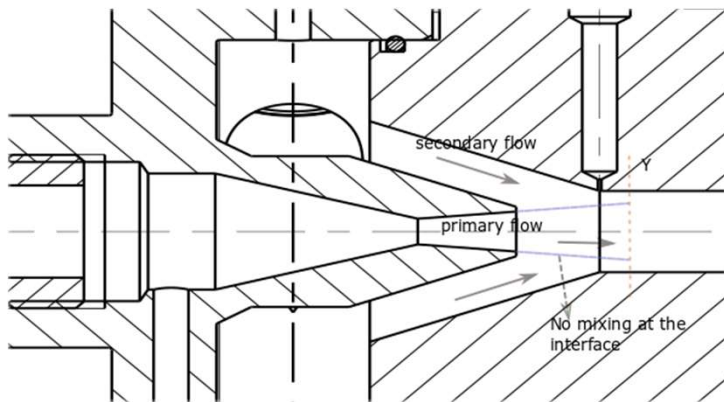
\dot{m}_S is an external Parameter

Conservation	Primary (Motive) Flow	Secondary (Suction-) Flow
Mass	$\dot{m}_P = \rho_{pY} v_{pY} A_{pY}$	$\dot{m}_S = \rho_{SY} v_{SY} A_{SY}$
Energy	$h_o + \frac{v_o^2}{2} = h_{pY} + \frac{v_{pY}^2}{2}$	$h_{St} = h_{SY} + \frac{v_{SY}^2}{2}$
Entropy	$s_{po} = \text{RP}_s(p_{pY}, h_{pY})$	$s_{St} = \text{RP}_s(p_{SY}, h_{SY})$
Density	$\rho_{pY} = \text{RP}_\rho(p_{pY}, h_{pY})$	$\rho_{SY} = \text{RP}_\rho(p_{SY}, h_{SY})$
Cross section	$A_m = A_{SY} + A_{pY}$	

Pressure balance: $p_Y = p_{pY} = p_{SY}$



PRE-MIXING UPDATE

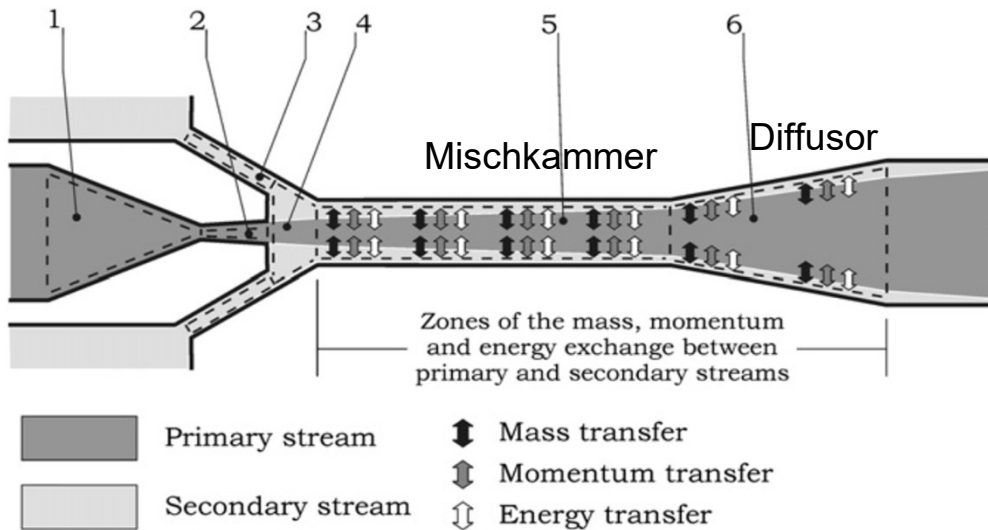


- **Subcritical Operating mode**(single Choking mode):

From the solution of the equations we get $(p_Y, v_{pY}, A_{pY}, v_{sY}, h_{sY})$ and **also \dot{m}_S !**

Conservation	Primary (Motive) Flow	Secondary (Suction-) Flow
Mass	$\dot{m}_P = \rho_{pY} v_{pY} A_{pY}$	$\dot{m}_S = \rho_{sY} v_{sY} A_{sY}$
Energy	$h_o + \frac{v_o^2}{2} = h_{pY} + \frac{v_{pY}^2}{2}$	$h_{St} = h_{sY} + \frac{v_{sY}^2}{2}$
Entropy	$s_{po} = RP_s(p_{pY}, h_{pY})$	$s_{St} = RP_s(p_{sY}, h_{sY})$
Momentum	$\int_{x_{Si}}^Y \rho A v \frac{dv}{dx} dx = - \int_{x_{Si}}^Y A(x) \frac{dp}{dx} dx$	
Density	$\rho_{pY} = RP_\rho(p_{pY}, h_{pY})$	$\rho_{sY} = RP_\rho(p_{sY}, h_{sY})$
Cross section	$A_m = A_{sY} + A_{pY}$	
Pressure	$p_Y = p_{pY} = p_{sY}$	

MIXER AND DIFFUSER



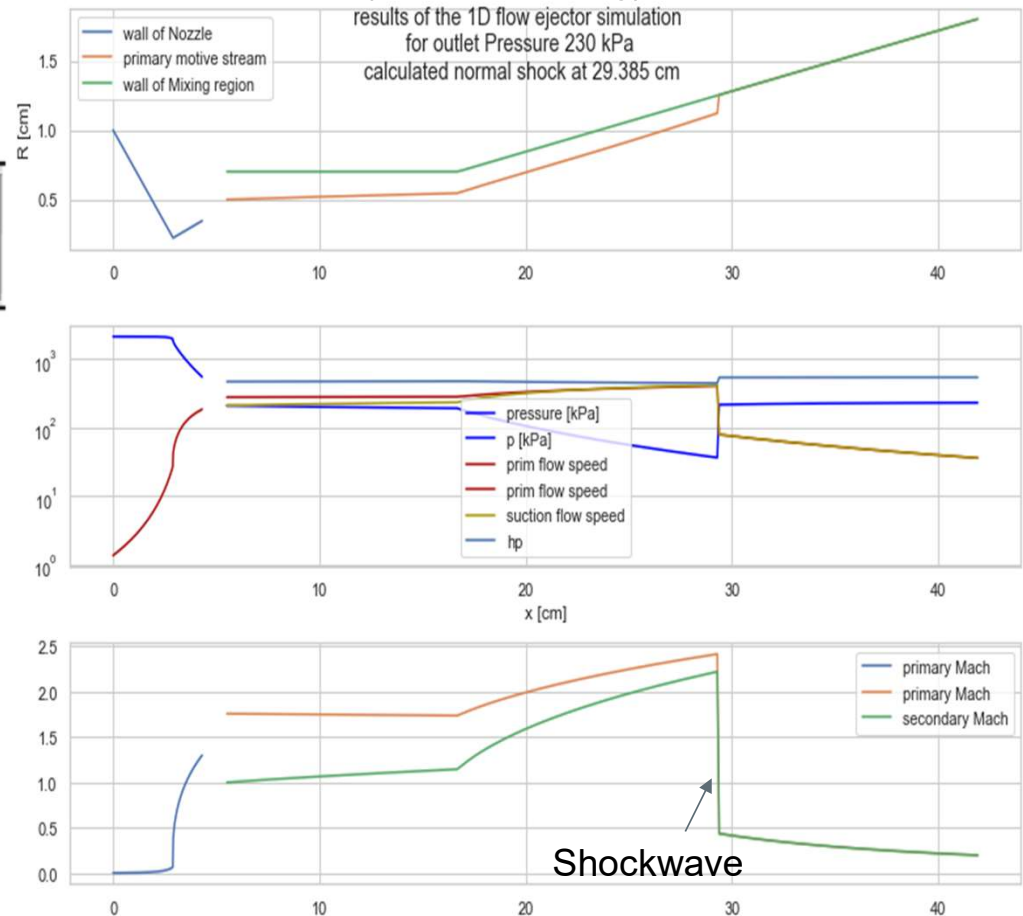
Assumptions after *Banasiak and Hafner (2011)*:

Coaxial Flow in the Mixer:

Mass, Momentum and Energy equations

Coefficients for the Mass and Momentum exchange

Critical Operation(Double choking)



Outlet Pressure



Normal Shock Wave
Position

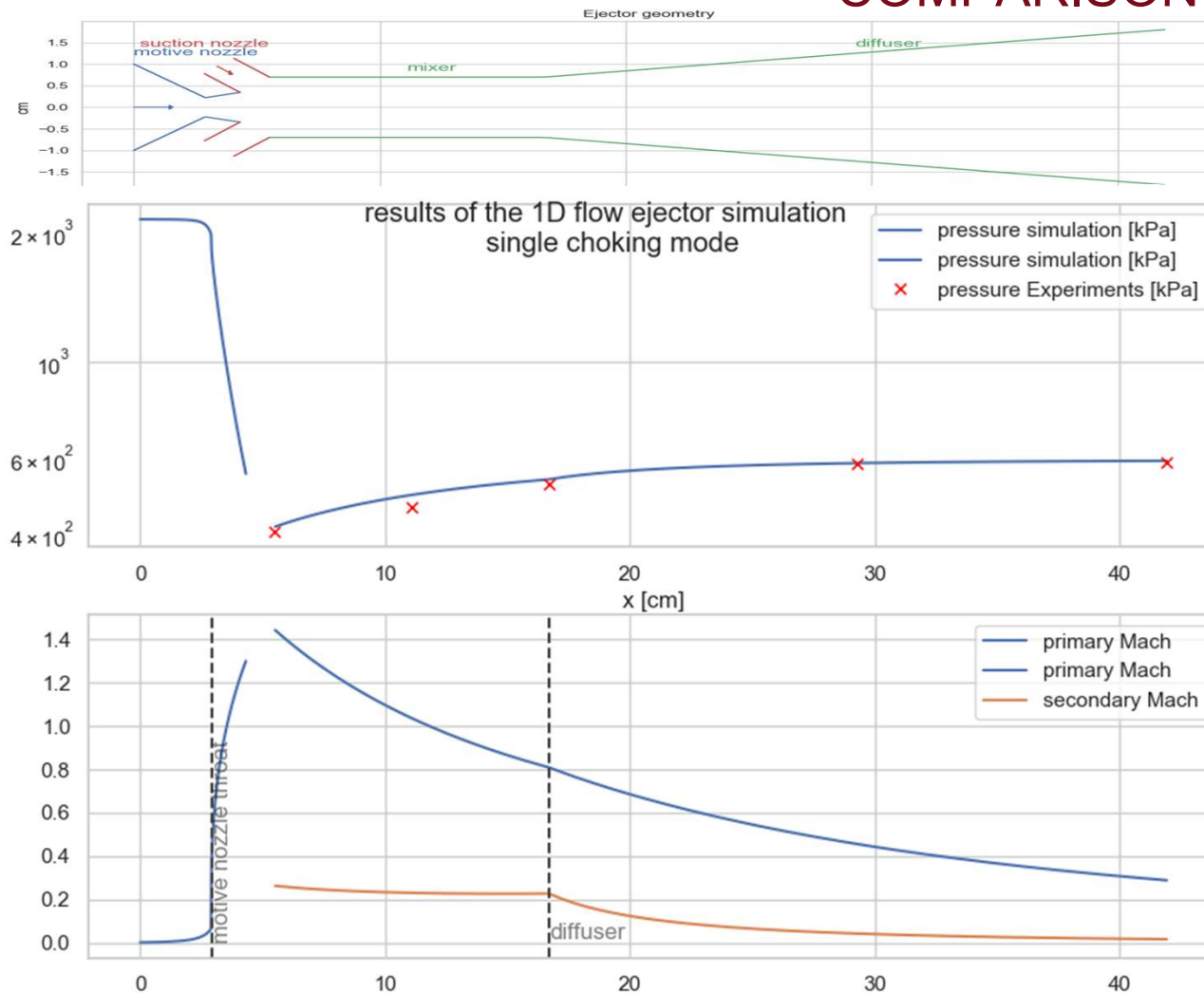
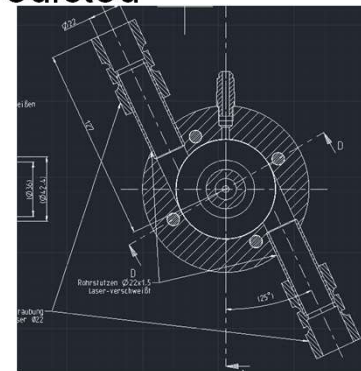
COMPARISON WITH EXPERIMENT

- Experiment: Butan Ejector (Single Choking)

Schlemminger et al 2019

→ good agreement of the pressure values.

→ 7-50% deviation of predicted mass flow rates



MFR g/s	Experiment	Our 1D Simulation
Motive Nozzle	127 g/s	190 g/s
Suction Nozzle	58 g/s	54 g/s

SUMMARY

- I have developed : 1D Ejector Simulation tool.
- Soon will be freely available on Github (open-source!)
- Geometry, Thermodynamic state, refrigerant flexible variable.
- Simulation takes only 20-40 seconds (on 1 CPU core)
- Python Package (run on every Operating System, and every server, you can connect it to any other post-processing tool)
- First experimental validation performed.

Outlook and open points:

- Further Tests/Comparisons with Experiments/CFD simulation needed. (Parameter Settings)
- Integration into Heat Pump Models (Dymola, Modelica)
- Graphical User Interface
- More precise calculation (Viscosity, Non-Equilibrium models, etc.)
- Still potential for speed up (currently runs on 1 CPU core)

THANKS FOR WATCHING/LISTENING!

Dr Adam Buruzs, 06.10.2022.

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