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On the lattice Boltzmann method and its application to turbulent, multiphase flows of various fluids including cryogens: A review ⊕⊘

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ABSTRACT

Cryogenic fluids are used in a myriad of different applications not limited to green fuels, medical devices, spacecraft, and cryoelectronics. In this review, we elaborate on these applications and synthesize recent lattice Boltzmann methods (LBMs) including collision operators, boundary conditions, grid-refinement techniques, and multiphase models that have enabled the simulation of turbulence, thermodynamic phase change, and non-isothermal effects in a wide array of fluids, including cryogens. The LBM has reached a mature state over the last three decades and become a strong alternative to the conventional Navier–Stokes equations for simulating complex, rarefied, thermal, multiphase fluid systems. Moreover, the method's scalability boosts the efficiency of large-scale fluid flow computations on parallel clusters, including heterogeneous clusters with graphics card-based accelerators. Despite this maturity, the LBM has only recently experienced limited use in the study of cryogenic fluid systems. Therefore, it is fitting to emphasize the usefulness of the LBM for simulating computationally prohibitive, complex cryogenic flows. We expect that the method will be employed more extensively in the future owing to its simple representation of molecular interaction and consequently thermodynamic changes of state, surface tension effects, non-ideal effects, and boundary treatments, among others.

I. INTRODUCTION

In recent years, cryogenic (ultra-cold) fluids have become more prevalent in various technologies and industries. By liquefying gaseous fuels such as liquefied natural gas (LNG) and liquid hydrogen (LH_2), relatively high volumetric energy densities are achievable for use in rocket propulsion systems, nuclear magnetic resonance equipment, refrigeration, and cryoelectronics for space applications,[1] among several other applications. The high capital cost of constructing physical prototypes as well as conducting large-scale physical experiments can slow the development of new technologies. As a result, computational modeling and simulation are becoming increasingly important as a lower-cost pathway for obtaining new physical insights at a fraction of the cost of physical experimentation.

LNG and LH_2 have been proposed as alternatives to fossil fuels such as diesel and heavy fuel oil with reduced adverse environmental effects.[2,3] However, their cryogenic nature poses a unique set of physical challenges to engineering design. These include phenomena such as non-isothermal cavitation in turbomachinery, diffusion in miscible species, fuel weathering, and phase roll-over. The weathering event refers to the long-term preferential evaporation of the lightest molecules in a LNG mixture which in turn changes its composition and thermophysical properties. As a mixture weathers, it stratifies in layers of its constituent components where the upper layers become more dense from evaporation of light molecules at the free surface, and the lower layers experience superheating under the hydrostatic pressure. Eventually the increasing buoyancy between the phases results in their relocation and dangerous surges in pressure caused by evaporation of "metastable," superheated LNG.[4]

The physics of cryogenic fluids are especially important when investigating accidental spills of cryogens, which can occur in collisions between marine carriers transporting $\mathcal{O}(10^5)$ m^3 of LNG, as well as loss of mechanical integrity in flanged connections in loading arms, accidental disconnection of hoses, fracture of brittled material, and overfilling or over-pressurization of fuel storage tanks, and may lead to

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undesirable outcomes.[5] The vapor production rate following accidental spills is primarily driven by the heat transfer processes from the substrate and the environment to the cryogen. Nevertheless, the heat transfer physics involves mechanisms that are non-linear and coupled.[6] The level of complexity renders detailed modeling in numerical simulations elusive, even considering the vast amount of effort that has been invested for several decades. The majority of modeling efforts of cryogenic fluid flows have been based on continuum conservation laws especially in cavitation research.[7] The review of Yeoh and Zhang[8] gives a partial view into some of the lower-order, empirical models that are popularly employed as source-terms in the Navier–Stokes equations. Whereas the boiling physics of water are well covered, correlated, and understood in literature,[9–13] boiling of more exotic substances such as superfluids,[14] refrigerants and cryogens, boiling systems in microgravity environments,[15] and non-ideal mixtures with multiple species still demand further study. For example, the thermophysical properties of LNG, which is a zeotropic mixture, are highly dependent on its chemical composition and have significant effects on the boiling heat transfer in various boiling regimes.[16] This also applies to mixtures of liquid nitrogen (LN_2), liquid oxygen (LO_2), and liquid air.[17,18]

In space applications, the use of cryogens is absolutely essential for scientific instruments that require very low operating temperatures $\mathcal{O}(50–100)$ mK.[1] The reconnaissance "Helios" and meteorological "Meteosat"[19] satellites are equipped with infrared detectors operating at 85 K. Telecommunication satellites use superconductors to reduce size, weight, and cost, and to process radio-frequencies.[20] Gravity gradiometers operate at very low temperatures to be accurate.[21] Moreover, gaseous fuels for propulsion are most efficiently stored in their liquid form, and for future interplanetary missions, life-support systems may depend on cryogens—e.g., in fuel cells for electricity production.[22] Finally, when photo-voltaic cells cannot accommodate surges in power demand, energy can be stored in intense magnetic fields generated by superconducting magnets.[1] The required cooling power for these devices are currently provided by various mechanical coolers, e.g., Brayton, Joule–Thomson, and Stirling variants, or passive coolers such as liquid/solid cryostats and deep-space radiators.[1] Also, devices such as adiabatic demagnetization-refrigerators and dilution coolers can provide very low temperatures ($\ll 1$ K).[1] From a heat transfer perspective, current challenges in space-cryogenics include the low heat-engine isentropic efficiencies (in the range of 2%–5%), designing cryogenic heat pipes, pressure transducers, flow meters, and thermometry, predicting the effects of vibrations and micro- and zero-gravity, and more.[1]

In the above examples, the employed cryogenic fluids may involve non-isothermal conditions and the corresponding change in the fluid's thermophysical properties, miscibility of multiple liquid species, cryogenic cavitation, turbulence, compressibility, and concurrent evaporation, condensation, and freezing phase-change. Some notable challenges in the study of these phenomena with continuum conservation laws are the development of accurate and computationally inexpensive interface-tracking schemes, and the modeling of phase transitions that are naturally stochastic whereas there is not inherent stochasticity in the Navier–Stokes equations. The mesoscopic lattice Boltzmann method (LBM) has developed into a mature and efficient alternative to traditional Navier–Stokes solvers since its incipience from the lattice-gas automata formulated by Hardy *et al.*[23] and is especially known for its ability to compute multiphase flows. In comparison with Navier–Stokes solvers, LBMs represent fluid flow from a discrete, mesoscopic perspective, rather than a macroscopic continuum. There are advantages and disadvantages to both methods, but the most prominent advantage of the LBM is its superior scalability, and notable disadvantages are high memory requirements and a lack of physical interpretation in many of the discretized lattice Boltzmann equations (LBEs). The method has been used in a range of new applications in phase transitions, turbulence modeling, and micro- and nano-fluidics. The reviews of Aidun and Clausen,[24] Arumuga Perumal and Dass,[25] Chen and Doolen,[26] and Li *et al.*[27] assessed the developments in the lattice Boltzmann method for simulating rarefied multiphase flows and heat transfer. However, there is still a need for a more exhaustive synthesis of LBM works on cryogenic flows. Accordingly, our review focuses on cryogenic fluid systems broadly, as well as LBMs that can be used for the analysis of the previously mentioned effects in cryogenic flows.

This review is structured as follows: Sec. II brings an introduction to the Boltzmann equation, Sec. III presents approaches for modeling the collision between distributions of particles, and Sec. IV refers to some relevant boundary treatments. In Sec. V, techniques for adaptive mesh refinement are presented, in Sec. VI multiphase models for treating phase change and interfacial transport are presented, and high-order schemes are discussed in Sec. VII. Section VIII reviews selected cryogenic fluid systems analyzed with LBMs. Our review is concluded in Sec. X in which we suggest possible directions for future work.

II. THE BOLTZMANN EQUATION

Rarefied gas flows can be described as flows where the statistical distance between molecules following collisions, termed the mean free path (MFP), becomes significant compared to the characteristic geometric length scale of the flow.[28] In this scenario, the flow cannot be described by continuum models based on the Navier–Stokes equations which consider macroscopic properties of fluids. In assessing rarefied flows, the Knudsen number is often used to compare the MFB, λ, with the characteristic length scale, L: $Kn = \lambda/L$. At large Knudsen numbers, relatively few collisions occur and the number of molecules in a control volume is relatively small. As a result, the properties of the fluid can vary significantly. Referring to the Maxwell–Boltzmann distribution, the event that a large number of molecules will obtain velocities in the highest and lowest quantiles of the distribution inside a control volume may produce a significant perturbation in the properties of the fluid in that control volume, and thereby may initiate the creation of a new thermodynamic phase.

At high Kn, the interaction between solid substrates and molecules significantly affects the flow's evolution. As it is not feasible to resolve the motion of all particles, we instead rely on statistical mechanics to describe the average macroscopic thermophysical properties from the appropriate microscale parameters. This is where the Boltzmann equation can describe the exact dynamics of discrete particles in a flow from a particle-number-velocity distribution f,[26–29]

$$\frac{\partial f}{\partial t} + \mathbf{c} \cdot \nabla f = \Omega. \tag{1}$$

Herein, $\mathbf{c}$ is the particle velocity and f is the probability density function representing the proportion of particles with a particular $\mathbf{c}(\mathbf{x}, t)$ at location $\mathbf{x} = [x_\alpha, x_\beta, x_\gamma]$ and time t. The probability density function f is dependent on the time evolution of the particle following its trajectory, which is inferred through the local particle collision tensor, Ω. Ω encompasses all physical phenomena that defines its behavior in relation to the thermodynamic equilibrium state. For example, immediately after an mth particle collides with a lth particle that has a probability density $f^{(l)}$ of colliding with the mth particle, Ω changes $f^{(m)}$ by an amount $^{(m)} = \mathscr{G} - \mathscr{L}$.[28] $\mathscr{G}$ describes the gain in particle-m momentum expressed by the probability of a particle-j colliding with the mth within the ranges $[\mathbf{x}^{(m)}, \mathbf{x}^{(m)} + \delta\mathbf{x}^{(m)}]$, $[\mathbf{c}^{(m)}, \mathbf{c}^{(m)} + \delta\mathbf{c}^{(m)}]$, $[\mathbf{x}^{(l)}, \mathbf{x}^{(l)} + \delta\mathbf{x}^{(l)}]$, $[\mathbf{c}^{(l)}, \mathbf{c}^{(l)} + \delta\mathbf{c}^{(l)}]$, and $[t, t + \delta_t]$ as a function of the particle surface area, and $\mathbf{x}^{(m)}$, $\mathbf{x}^{(l)}$, $\mathbf{c}^{(m)}$, $\mathbf{c}^{(l)}$, and t. In a similar fashion, the loss term $\mathscr{L}$ describes the loss in momentum of the m-th particle. The discretized lattice Boltzmann equation (2) (LBE) can be written into a streaming process (left-hand side) and a collision process (right-hand side),

$$f_i(\mathbf{x} + \delta\mathbf{x}, t + \delta_t) - f_i(\mathbf{x}, t) = \Omega. \tag{2}$$

The collision process is correlated with an offset between the non-equilibrium and equilibrium distributions and a tensor containing characteristic relaxation coefficients, which represent the ("streaming") time between individual collisions. The solution of the equation is performed along i streaming directions—including the zeroth representing no streaming—as exemplified in Fig. 1 for a D2Q5 lattice model, and computed in a discrete manner according to the algorithm in Fig. 2.

The Hermite or Taylor expansions bridge the mesoscale to the continuum limit to achieve the Navier–Stokes equations. The macroscopic flow variables such as density, velocity, and temperature, respectively, ρ, $\mathbf{U}$, T, are correlated with the sums of the statistical particle distributions for mass and momentum (f) and energy (g), in the n total streaming directions (for double distribution functions only)—the formulation varies between LBMs
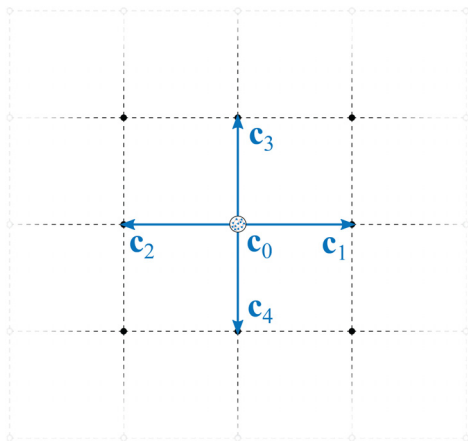

FIG. 1. Illustration of the five streaming paths (including no streaming in $\mathbf{c}_0$) in the D2Q5 lattice model.
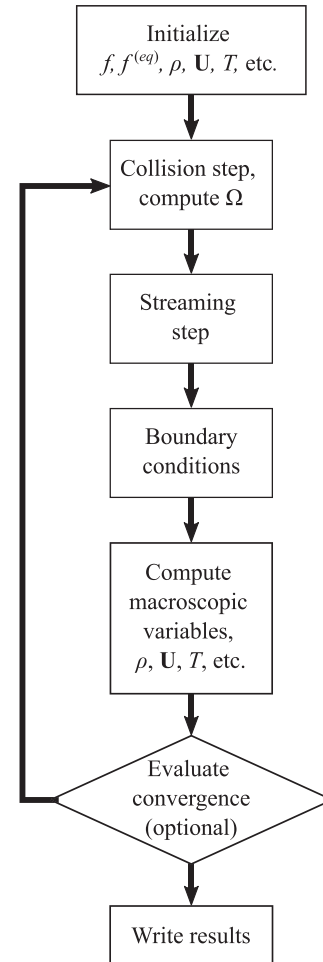

FIG. 2. General solution procedure for an LBM.

$$\rho = \sum_{i=1}^{n} f_i, \tag{3}$$

$$\rho\mathbf{U} = \sum_{i=1}^{n} f_i \mathbf{c}_i, \tag{4}$$

$$T = \sum_{i=1}^{n} g_i, \tag{5}$$

where body forces $\mathbf{F}$ are also present, the true continuum velocity is $\mathbf{U} = \mathbf{u} + \mathbf{F}\delta_t/2\rho$, where $\mathbf{u} = \frac{1}{\rho}\sum_{i}^{n} f_i \mathbf{c}_i$. The physics describing the particle interactions in multiphase flows is imposed through models using equations-of-state, free energy, interaction energies, and others. The physics describing the phase transitions in multiphase flows can be categorized into explicit and implicit methods.[30] In explicit methods, phase interfaces are tracked in time and space, and in implicit methods—such as the model of Shan and Chen (SC)[31]—interfaces are produced by calculating intermolecular action between adjacent

populations of molecules. In implicit methods, the phase transitions are spatially continuous across several lattices. This is advantageous for modeling the behavior of cryogens in environments where the temperature is not strongly dissimilar to the critical temperature requiring a high accuracy in predicting interfacial phase-change.[30]

III. COLLISION OPERATORS

Core to the lattice Boltzmann method is the way with which the thermodynamic state of a medium is altered toward one in equilibrium with a Maxwellian distribution $f^{(eq)}$ of velocities. The inequilibrated distribution f, which in the continuum limit corresponds to a temperature, changes with a rate that is dictated by the intermolecular collisions. The effects of these collisions are reflected by a collision operator Ω that relaxes the distribution function toward an equilibrium state. In the simplest form the evolution of f is represented by a single relaxation time τ in the continuous Boltzmann equation:[32]

$$\Omega_i = -\frac{1}{\tau}\left(f_i - f_i^{(eq)}\right). \qquad (6)$$

However, with the collisions represented by a single relaxation time, some multi-speed lattice models with this Bhatnagar–Gross–Krook (BGK) model[33] suffers from some limitations, e.g., the Prandtl number is fixed at unity.[32] Consequently, numerous formulations of the collision operator have been proposed since Bhatnagar et al.,[33] not limited to multiple relaxation time (MRT) schemes and models based on entropy that also provide numerical stability at high Reynolds numbers.

To ensure stability in the simulation of turbulent cryogen flows, more sophisticated collision models with multiple relaxation times beyond the single relaxation-time BGK variant have been used. Recently, models were formulated by Mazloomi et al.,[34,35] and Pareschi et al.[36] Pareschi et al. presented a two-way coupled conjugate heat transfer (CHT) model applied at the fluid–solid boundary [presented as Grad's boundary condition (BC) in Sec. IV], with a two-population entropic LBM to simulate the bulk fluid kinetics. The model was validated for cases with turbulent Reynolds numbers and complex boundaries. Since the original formulation of the entropic-class LBM by Karlin et al.,[37] the method was considered an important milestone in the development of the LBM. It enjoyed the attention due to its unconditional stability at high Reynolds number flows in immersed complex geometries as the sub-grid physics were modeled. However, this comes at higher computational cost owing to the solution of non-linear equations for entropy. In the methods of Karlin et al.,[37] equilibrium population distributions were obtained by minimizing the entropy operator

$$S = \sum_{i=1}^{n}\left[f_i \ln\left(\frac{f_i}{w_i}\right)\right], \qquad (7)$$

where w_i is the ith direction-dependent weight from the particular DnQm n-dimensional lattice model with m streaming directions. In order to accommodate turbulent flows, Pareschi et al.[36] employed the multi-relaxation Karlin–Boesch–Chikatamarla (KBC) entropic LBM[38,39] in which the double distribution functions are chosen so as to minimize S,

$$f_i(\mathbf{x} + \mathbf{c}_i \cdot \delta_t, t + \delta_t) - f_i(\mathbf{x}, t)$$
$$= \omega_f\left(f_i^{(eq)} - f_i\right) + (\omega_f - \omega_{1f})\left(f_i^{\star} - f_i^{(eq)}\right), \qquad (8)$$

$$g_i(\mathbf{x} + \mathbf{c}_i \cdot \delta_t, t + \delta_t) - g_i(\mathbf{x}, t)$$
$$= \omega_f\left(g_i^{(eq)} - g_i\right) + (\omega_f - \omega_{1f})\left(g_i^{\star} - g_i^{(eq)}\right). \qquad (9)$$

In these kinetic equations, pseudo-equilibrium distributions—denoted by "$\star$"—were adopted to allow for variable Prandtl numbers that otherwise are fixed to 1 in collision models with single relaxation times. The relaxation parameters ω_f and ω_{1f}, where subscript "f" denotes fluid (there are also parameters defined for the solid domains), allow for variable kinematic viscosity ν and thermal diffusivity α via

$$Pr = \frac{\nu}{\alpha} = \frac{(2 - \omega_f)\omega_{1f}}{(2 - \omega_{1f})\omega_f}. \qquad (10)$$

The collision operators in Eqs. (8) and (9) replaced the conventional BGK collision model, which is deficient at relatively high Reynolds numbers due to numerical instabilities inducing deleterious divergence. Nevertheless, because of the simplicity and computational efficiency, the BGK collision model remains the workhorse of most LBM-implementations.[39]

Owing to the BGK popularity, the LBM was conjectured to be unsuitable for simulating high Reynolds number flows. A number of recent studies have shown this to be incorrect, as in addition to the use of the entropic LBM,[40,41] recent studies[42–46] have simulated turbulent flows with MRT collision operators—all outlined in Table I. Whereas the BGK collision model adopts a single fixed rate $1/\tau$ for f, in the MRT collision model all moments are relaxed by individual rates[42] from relaxation ($\mathbf{S}$) and transformation ($\mathbf{M}$) matrices,[47]

$$\Omega_i = -\mathbf{M}^{-1}\mathbf{S}\mathbf{M}\left(f_i - f_i^{(eq)}\right)\Delta t. \qquad (11)$$

From the basic notion that the moments in an LBM—i.e., the lower-order density (zeroth), momentum (first), momentum flux (second), and those of higher order—relax toward their equilibrium states at dissimilar rates[42] brings to reason how representing the turbulence energy-cascade with a single rate can be deleterious and produce non-trivial errors. Whereas the low-order moments are inferrable from the fluid properties,[46] the higher-order moments are non-interpretable and are normally fixed at a constant value.[42] Being able to fine-tune each of the rates adaptively during runtime is paramount to eliminating numerical dispersion.

Other methods for relaxing the higher-order moments than with entropy as in the KBC model have been formulated. Li et al.[42] recently introduced a "measurement functional" that adjusts the higher-order moment relaxation rates on-the-fly. Other turbulence-studies using MRTs such as those of Wu et al.,[44] Zecevic et al.[46] showed good agreement with the Navier–Stokes equations from other direct numerical simulations[49,50] (DNS), in terms of turbulence-energy budgets. With more sophisticated formulations of the relaxation rates in MRT schemes and entropic extensions, stable simulations of turbulent flows are becoming a part of the repertoire of the LBM.
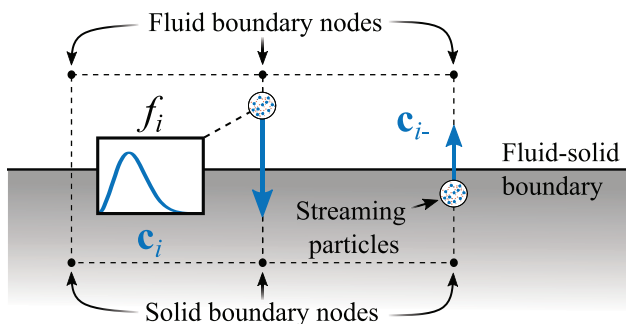
IV. BOUNDARY CONDITIONS

Boundary treatments define how the streaming fluid particles interact with molecules in solids. Several boundary condition (BC) models have been proposed, and are frequently published. The most commonly used BC models are standard bounce-back (SBB),[51–55] which are simple but normally achieve only first-order accuracy. The

TABLE I. Selected numerical experiments with the LBM of various turbulent flows since 2018. Collision models employed: entropic,[40,41] MRT,[42–46] and BGK.[48] Nomenclature: cylinder/sphere diameter D, time-averaged root mean square velocity $\bar{U}_{\mathrm{rms}}$, Taylor microscale λ, continuous phase kinematic viscosity ν_c, friction velocity U_τ, channel height h, plate/filament/channel length l, minimum and maximum stroke ϕ, flapping frequency f, span-wise length of a wing l_w, mean wing-chord $\bar{c}$, and lid velocity U_{lid}.

References	Cases	Reynolds nos.
Morrison and Leder[40]	(a) Wall-mounted cylinder	(a) $Re_D = \frac{U_\infty D}{\nu} = 2 \times 10^2$
	(b) Sediment transport around cylinder	(b) $Re_D = 1.7 \times 10^4$
Feuchter et al.[41]	Wall-mounted cylinder	$Re_D = 3.2 \times 10^4$
Li et al.[42]	(a) Tornado	(a) 8×10^4
	(b) Falling box	(b) 10^5
	(c) Plank drop	(c) 1.4×10^5
	(d) Turbulent jet	(d) 2×10^4
Zhong and Komrakova[43]	Liq. droplet breakup	$Re_\lambda = \frac{\bar{U}_{\mathrm{rms}}\lambda}{\nu_c} = \{56.7, 57.1, 57.1\}$
Wu et al.[44]	Channel flows	$Re_\tau = \frac{U_\tau}{\nu}\frac{h}{2} = (180, 395, 640)$
Xu et al.[45]	(a) Vertical plate	(a) $Re_l = \frac{U_\infty l}{\nu} = 126$
	(b) Stationary/oscillating cylinders	(b) $Re_D = \{100, 185\}$
	(c) Flapping foils	(c) $Re_c = \frac{U_\infty c}{\nu} A\{1, 1.1, 10\} \times 10^3$
	(d) Flexible filaments	(d) $Re_{l,f} = \{200, 10^3, 7.8 \times 10^3, 9 \times 10^3\}$
	(e) Wavy wall	(e) $Re_h = 2.4 \times 10^3$
	(f) Stationary sphere	(f) $Re_D = \{1, 2.5, 3, 5\} \times 10^2$
	(g) Hovering dragonfly	(g) $Re = \frac{2(\phi_{\max} - \phi_{\min})fl_w\bar{c}}{\nu} = 2.495 \times 10^3$
Zecevic et al.[46]	Channel flow	$Re_l = 180$
Hegele et al.[48]	Cavity flow	$Re = \frac{U_{\mathrm{lid}} l}{\nu} = 5 \times 10^4$

SBB condition infers the boundary effects by traversing particles through links crossing the solid–fluid boundary, as depicted in Fig. 3. Interpolated bounce-back (IBB) and halfway bounce-back—an SBB subclass[32]—conditions achieve up to second-order accuracy, but are difficult to implement due to a strong dependence on grid resolution.[56] Other popular BCs include immersed-boundary methods (IBM)[57–59] and non-equilibrium extrapolation schemes.[60] In addition, treatments for curved, complex boundaries[61–63] are often published and it is noted that the numerical stability of simulations—especially with turbulence—is affected by the boundary condition implementation.

FIG. 3. Illustration of the standard bounce-back scheme. When the fluid–solid boundary is halfway between the FBN and the first fluid-immersed lattice, the method is second-order accurate.[53]

In the SBB condition, the fluid at a fluid boundary node (FBN) is bounced back with an adjustment of momentum so that the post-streaming state at a link at $\{\mathbf{x}, t + \delta_t\}$ is[24,51]

$$f_i(\mathbf{x}, t + \delta_t) = f_{i^-}(\mathbf{x}, t^+) + 2\mathbf{U}_b \cdot \frac{\rho w_i}{c_s^2} \cdot \mathbf{c}_i. \tag{12}$$

Here, i^- denotes the opposite direction of i and t^+ a time immediately post-collision but pre-streaming. $\mathbf{U}_b$ is the *in situ* boundary velocity, ρ the fluid density, w_i the weights according to the DnQm lattice definitions, c_s the speed of sound, and $\mathbf{c}_i$ the particle velocity in the ith direction. The transfer of momentum to the solid boundary $\mathcal{F}_{i^-}$ is then

$$\mathcal{F}_{i^-}(\mathbf{x}_b, t) = -2\mathbf{c}_i \left[f_{i^-}(\mathbf{x}, t^+) + \frac{\rho w_i}{c_s^2} \mathbf{U}_b \cdot \mathbf{c}_i \right]. \tag{13}$$

This momentum transfer constitutes the macroscopic pressure exerted on the wall.

Rigorous conjugate heat transfer (CHT) algorithms are particularly critical for pool boiling simulations, as the evaporation rate of the spilled cryogen is dependent on thermal conduction in the solid substrate.[64] Moreover, it is also relevant to cryogenic spill scenarios on liquid substrates, including seawater, where continuous convective heat transfer from water into the spilled cryogen may lead to solidification of the seawater as ice. A stable CHT model is essential to model such spill scenarios. Grad's boundary condition—employed for entropic LBMs by Chikatamarla et al.,[65] Dorschner et al.,[66] and Pareschi et al.[36]—is a stable CHT treatment useful for cases where spatial gradients in the boundary velocity and temperature are non-negligible.[36] The virtues of the scheme are a higher accuracy and broader stability

in contrast to the interpolated bounce-back scheme (which is already a second-order scheme). Furthermore, it can be used to model either two-fluid interfaces or solid–fluid boundaries and is suitable for high Reynolds numbers.
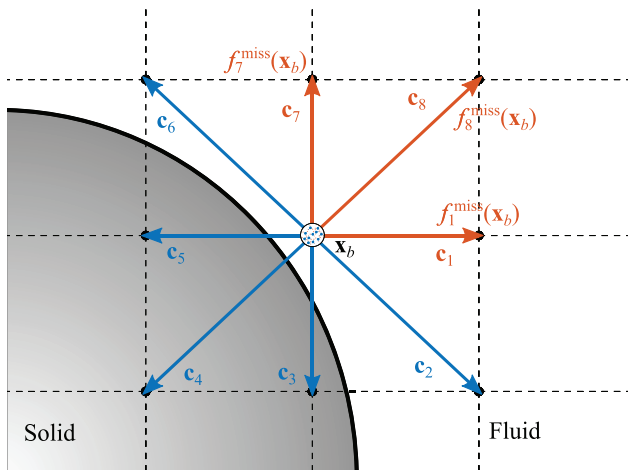
To illustrate Grad's boundary condition, consider the post-propagation particle distributions streaming away from the solid into the fluid depicted in Fig. 4. The particle distributions at the arbitrary lattice-proximate location $\mathbf{x}_b$ at time t are unknown due to the missing information yielded after collision with the solid–fluid boundary. In order to complete the advection process of the LBM, the "missing populations" $f_i^{\text{miss}}(\mathbf{x}_b, t)$ and $g_i^{\text{miss}}(\mathbf{x}_b, t)$ (denoted Grad's distribution) were determined by Dorschner et al.[66] as

$$\begin{aligned} f_i^{\text{miss}}(\mathbf{x}_b, t) &= f_i^{(eq)} + f_i^{(1)}, \\ g_i^{\text{miss}}(\mathbf{x}_b, t) &= g_i^{(eq)} + g_i^{(1)}. \end{aligned} \tag{14}$$

Grad's distribution comprises the equilibrium distributions and two first-order populations denoted with superscript "(1)." The equilibrium populations are calculated as in the work of Pareschi et al.,[36] where the population for the f-lattice is a function of the macroscopic velocity, density, and temperature, and for the g-lattice the equilibrium state is defined by the internal energy. The non-equilibrium population set F_i for the bulk and boundary distributions results in the moments for the boundary node with coordinate $\mathbf{x}_b$,

$$F_i = w_i \left[M_0 + \frac{M_\alpha c_{i,\alpha}}{T_0} + \frac{(M_{\alpha\beta} - M_0 \, \delta_{\alpha\beta} \, T_0)(c_{i,\alpha} \cdot c_{i,\beta} - T_0 \, \delta_{\alpha\beta})}{2 \, T_0^2} \right], \tag{15}$$

where M_0, $\mathbf{M}_\alpha$, and $\mathbf{M}_{\alpha\beta}$ are the zeroth-, first-, and higher-order moments (listed in Table II). These are determined from the pressure tensor $\mathbf{P}_{\alpha\beta}^{(1)}$ (16), the arbitrary high-order tensor $\mathbf{R}_{\alpha\beta}^{(1),f}$ (17), the heat flux in the fluid (convection) $q_\alpha^{(1),f}$ (18), and the heat flux in the solid (conduction) $q_\alpha^{(1),s}$ (19). The notation ∂_α is shorthand for $\partial/\partial\mathbf{x}_\alpha$.

TABLE II. The first-order moments components employed in Grad's boundary distribution (14). Reproduced with permission from Pareschi et al., Phys. Rev. E **94**, 013305 (2016). Copyright 2016 American Physical Society.

Population F_i (15)	$M_0^{(1)}$	$\mathbf{M}_\alpha^{(1)}$	$\mathbf{M}_{\alpha\beta}^{(1)}$
$f_i^{(1),f}$	0	0	$\mathbf{P}_{\alpha\beta}^{(1)}$
$g_i^{(1),f}$	0	$q_\alpha^{(1),f}$	$\mathbf{R}_{\alpha\beta}^{(1),f}$
$g_i^{\star(1),s}$	0	$2\nu_\beta\mathbf{P}_{\alpha\beta}^{(1),s}$	0
$g_i^{(1),s}$	0	$q_\alpha^{(1),s}$	0

$$\mathbf{P}_{\alpha\beta}^{(1)} = \sum_{i=1}^{n} \mathbf{c}_{i,\alpha} \cdot \mathbf{c}_{i,\beta} f_i^{(1)} = -\frac{1}{\omega_f} \rho T_0 \mathbf{S}_{\alpha\beta}, \tag{16}$$
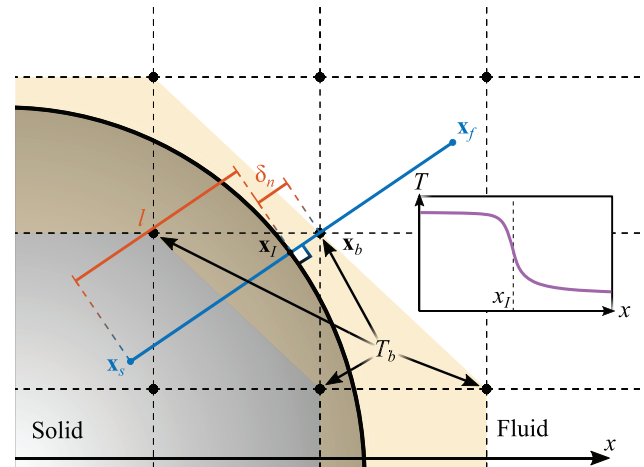
$$\mathbf{R}_{\alpha\beta}^{(1),f} = -\frac{2}{\omega_{1f}} \rho \, T_0 \left[c_\nu (\mathbf{U}_\alpha \cdot \partial_\beta T + \mathbf{U}_\beta \cdot \partial_\alpha T) + \mathbf{S}_{\alpha\beta}(2T_0 + c_\nu T) \right], \tag{17}$$

$$q_\alpha^{(1),f} = -\frac{2}{\omega_{1f}} \cdot \rho \, c_\nu \, T_0 \, \boldsymbol{\partial}_\alpha T + 2 \, \mathbf{U}_\beta \mathbf{P}_{\alpha\beta}^{(1)}, \tag{18}$$

$$q_\alpha^{(1),s} = -\frac{2}{\omega_{1,s}} \rho_s \, c_\nu^s \, T_0 \, \boldsymbol{\partial}_\alpha T. \tag{19}$$

In order to determine the temperature field surrounding the solid–fluid interface, Pareschi et al.[36] computed the interface location $\mathbf{x}_I$, which is the projection of the boundary node $\mathbf{x}_b$ onto the interface, as depicted in Fig. 5, as well as the spatial gradients in Eqs. (17)–(19). At the interface, the conduction continuity applies in the wall-normal η-direction

$$-k_s \frac{\partial T}{\partial \eta}\bigg|_{\mathbf{x}_{I,s}} = -k_f \frac{\partial T}{\partial \eta}\bigg|_{\mathbf{x}_{I,f}}. \tag{20}$$

FIG. 4. Population velocities in a D2Q9 lattice where the missing populations are $f_{\{1,7,8\}}^{\text{miss}}$, $g_{\{1,7,8\}}^{\text{miss}}$. Reproduced with permission from Dorschner et al., J. Comput. Phys. **295**, 340–354 (2015). Copyright 2015 Elsevier.

FIG. 5. Area of interest in a CHT problem where the Dirichlet and Neumann conditions do not apply. The value for $T(\mathbf{x}_I)$ in the shaded yellow region is attainable through interpolation between the target temperature at the $\mathbf{x}_b$ and an arbitrary temperature in the solid $[T(\mathbf{x}_s)]$ and fluid $[T(\mathbf{x}_f)]$. Reproduced with permission from Pareschi et al., Phys. Rev. E **94**, 013305 (2016). Copyright 2016 American Physical Society.

Upon discretization of the above gradient, the balance below was achieved:

$$k_s \frac{T(\mathbf{x}_s) - T(\mathbf{x}_I)}{l} = k_f \frac{T(\mathbf{x}_I) - T(\mathbf{x}_f)}{l}, \quad (21)$$

$$T(\mathbf{x}_I) = \frac{k_s\, T(\mathbf{x}_s) + k_f\, T(\mathbf{x}_f)}{k_s + k_f}, \quad (22)$$

where l is defined in Fig. 5. Thus, with known fields of $T(\mathbf{x}_s)$ and $T(\mathbf{x}_f)$, $T(\mathbf{x}_I)$ can be computed. By interpolation, the target temperature at the boundary node $T(\mathbf{x}_b)$ can be calculated, and the temperature field in between nodes was calculated by linear interpolation as

$$T(\mathbf{x}_b)|_{\mathbf{x}_{b,f}} = T(\mathbf{x}_I) + \frac{\delta_\eta}{l}\left[T(\mathbf{x}_f) - T(\mathbf{x}_I)\right], \quad (23)$$

$$T(\mathbf{x}_b)|_{\mathbf{x}_{b,s}} = T(\mathbf{x}_I) + \frac{\delta_\eta}{l}\left[T(\mathbf{x}_s) - T(\mathbf{x}_I)\right]. \quad (24)$$

With the known temperature field, all the information needed to employ Grad's BC (14) is available. Pareschi *et al.*[36] used the procedure to compute the turbulent heat transfer around a wall-mounted cube immersed in air and successfully achieved a stable solution. We note that using a conjugate heat transfer BC enables the heat conduction in the solid substrate to be accounted for to accurately simulate the solid–fluid heat flux. Lately, a number of other studies[67–70] also implemented CHTs.

Cahn[71] previously showed that liquids completely wet a surface at some characteristic wetting temperature and that cooling and heating can cause a wetting transition between partial and full wetting states, i.e., the contact angle of a fluid is temperature dependent. Such a transition has also been observed in cryogens.[72–77] The wetting temperature is, however, exceptionally prone to thermal hysteresis,[77–81] and so the conjugate heat transfer and the temperature profile in a solid–fluid pair may impact the contact angle history. It has previously been remarked that the heterogeneous nucleation rate in cryogens is more susceptible to surface treatments than in water.[82] An eventual contribution from the surface topology to the interfacial tensions at a triple contact line may alter a fluid's contact angle, so it is relevant to review BCs that can account for surface energy.

Wen *et al.*[83] used a very simple, yet effective, chemical-potential based boundary scheme to evaluate the evolution of the non-ideal force [also described in Eq. (65)],

$$\mathbf{F}(\mathbf{x}) = -\rho\nabla\mu + \nabla\cdot\mathbf{P}_{\alpha\beta}^{(0)}. \quad (25)$$

Owing to its clear physical interpretation, the chemical potential is a more eloquent way of representing surface hydrophobicity and philicity, rather than through density, as is done in the pseudo-potential LBM.[31,84–86] The BC is concerned with the first layers of fluid boundary nodes (FBNs) adjacent to a solid–fluid interface and that of the neighboring solid boundary nodes (SBNs). In the FBNs, the populations still stream and collide, and distributions that rebound from the solid are approximated following the bounce-back scheme. The SBNs are treated with a Dirichlet-like condition where they are assigned a fixed chemical potential suggestive of the surface energy properties of the solid, so that the chemical potential is never computed in the SBNs. This affects the non-ideal forces—used in various equations of state (EOS)—for the nodes in proximity to the interface. The density

gradient was estimated through a weighted average for the SBN density,

$$\bar{\rho}(\mathbf{x},0) = \frac{2}{3}\rho(\mathbf{x},1) + \frac{1}{6}\rho(\mathbf{x}-1,1) + \frac{1}{6}\rho(\mathbf{x}+1,1). \quad (26)$$

Figure 6 depicts the implementation of the chemical-potential BC, with the nodes in the yellow shaded region being used to compute the average.

As spilled cryogens undergo phase transitions, a triple contact line will exist that demarcates the liquid, vapor, and solid phases, illustrated in Fig. 7. The angle of the liquid/vapor interface incident to the contact line (contact angle, denoted θ) impacts the nucleation rates and heat transfer at the solid boundary as liquids with higher contact angles are less likely to fill cavities and retain vapor phases therein. Contact angle hysteresis occurs when changes in θ do not move the triple contact line; denoting angles that advance the triple contact line as θ_A and those that recede it as θ_R, the hysteresis range corresponds to $\theta_R \le \theta \le \theta_A$. Contact angle hysteresis has been modeled through wettability BCs in density-based contact angle schemes[86,87] and pseudo-potential-based contact angle schemes.[84,85,88] Yang *et al.*[89] implemented a contact angle hysteresis BC which established the geometric relation for the Neumann triangle depicted in Fig. 7 as

$$\tan\left(\frac{\pi}{2} - \theta\right) = \frac{\overline{AC}}{\overline{AB}} = -\frac{\dfrac{\partial\rho}{\partial z}}{\sqrt{\left(\dfrac{\partial\rho}{\partial x}\right)^2 + \left(\dfrac{\partial\rho}{\partial y}\right)^2}}. \quad (27)$$

Approximating the derivatives as difference quotients yields the density at the surface of the substrate ($z = 0$) as

$$\rho_{i,j,0} = \rho_{i,j,2} + \tan\left(\frac{\pi}{2} - \theta\right)\sqrt{(\rho_{i+1,j,1} - \rho_{i-1,j,1})^2 + (\rho_{i,j+1,1} - \rho_{i,j-1,1})^2}, \quad (28)$$

where i, j, k indices represented lattice nodes in the direction of the three coordinate unit vectors for x, y, z (not in terms of the lattice model). The hysteresis window expressed in terms of density, $\rho_R \le \rho_{i,j,1} \le \rho_A$, where $\rho_{i,j,1}$ pertains to the first layer nodes atop the solid surface, is obtained by evaluating Eq. (28) with θ_A, θ_R. This means that the thermophysical properties of the fluid contained inside the triple contact line can vary between ρ_R and ρ_A without changing the bubble/droplet base diameter. The formulas above present a simple way to realize the hysteresis window as Yang *et al.*[89] did in their pseudo-potential LBM. The implications of contact angle hysteresis on evaporation heat transfer in cryogens on surfaces with non-uniform
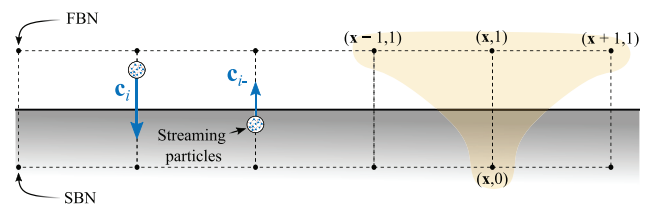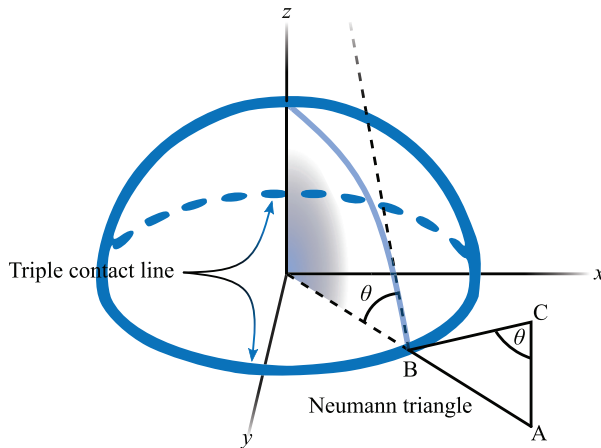

FIG. 6. Lattice structure based on the chemical-potential boundary condition of Wen *et al.*[84]

FIG. 7. Schematic of the geometric relationship which applies to the triple contact line at the periphery of a droplet or bubble, in which vapor, solid, and liquid interact. Reproduced with permission from Yang *et al.*, J. Colloid and Interface Sci. **566**, 327–337 (2020). Copyright 2020 Elsevier.

roughness, temperature, etc., may prove to be non-trivial considering that it was shown that a majority of the heat transfer takes place in and around the triple contact line and the bubble meniscus.[90] However, how strongly evaporation is affected by the hysteresis window is not clear in the literature and requires further investigation.

For thermal LBMs such as the Watari–Tsutahara–Gonella model,[91,92] the diffuse reflection boundary condition[93] proved useful for simulating rarefied flows where the slip condition applies, as well as temperature jumps, for example across shocks as investigated in the works of Traudt and Schlechtriem.[94] The BC draws inspiration from the diffuse reflection concept for gases originally proposed by Maxwell[95] and considers the solid–fluid interaction as analogous to how incident light reflects in a diffuse rather than specular manner with the strongest intensity of photons in the wall normal direction.

V. GRID-REFINEMENT TECHNIQUES

An avenue for attaining high accuracy LBM solutions at reduced computational cost is the use of multi-block (MB)[96–99] and adaptive-mesh refinement (AMR)[100–102] techniques. Ma *et al.*[103] exploited the advantages of both frameworks by developing a hybrid MB–AMR technique which combines the MB simplicity and AMR flexibility. This hybrid method belongs to the non-conformal grid approach which may result in discontinuities in the flow variables incident at the refinement interfaces. Such a framework is useful for simulating cryogenic spills on water considering that the moving surface of the water phase favors the use of AMR. In spills on solid substrates, a MB approach is useful for dividing regions of different surface energies in the lateral plane, and in the vertical plane, resolving the length scales of bubbles as they ascend, and grow/shrink in size, in the liquid column. Even though the MB–AMR technique of Ma *et al.*[103]—among others[104,105]—was purposed for neutron transport in nuclear reactors, the general algorithm can be modified to scalar/momentum transport. The indicator ϵ for the local mesh resolution was formulated in terms of the gradient of the neutron scalar flux $\nabla\Phi_s$ in block b on node s as

$$\varepsilon_{s,b} = |\nabla\Phi_s|\Delta h_b^{3/2}, \tag{29}$$

where the mesh step Δh_b varies as the MB-AMR is performed. In order to determine if a particular block should be refined or merged, standard deviation of the indicator γ_b was computed and compared to the standard deviation of the entire domain $\bar\gamma$, defined, respectively, as

$$\gamma_b = \sqrt{\frac{\sum\limits_{s\in b}\varepsilon_{s,b}^2}{N_b}}, \tag{30}$$

$$\bar\gamma = \sqrt{\frac{\sum\limits_{b}\sum\limits_{s\in b}\varepsilon_{s,b}^2}{\sum\limits_{b}N_b}}. \tag{31}$$

The overall processes of refinement and merging are depicted in Fig. 8. The lattice is initialized at the coarsest refinement level (level 1) and is subsequently resolved to higher levels (levels 2, 3, …, N). The lattice in block b is refined if $\gamma_b > \bar\gamma$ and lattice-nodes are merged if $\gamma_b < 0.1\bar\gamma$. The mesh step between finer and coarser levels is successively halved so that $\Delta x_f = \Delta x_c/2$. The simplicity in the AMR is owed to the correlation between the refinement levels by the rule that no adjacent blocks can have a resolution-level difference greater than one, which eliminates the complex tree-structured data that are inherent in conventional AMR codes.[103] In refinement "uncommon" or hanging nodes are created, and their distributions are approximated with fourth-order accuracy through a cubic interpolation scheme. During merging, a common node simply inherits the population distribution from the local node in the higher-level lattice.

Recently, several large-scale implementations of MB–AMRs have been published, revolving around simulations of lid-driven cavities, human vocal-chord flows[106] microfluidic particle separation, additive
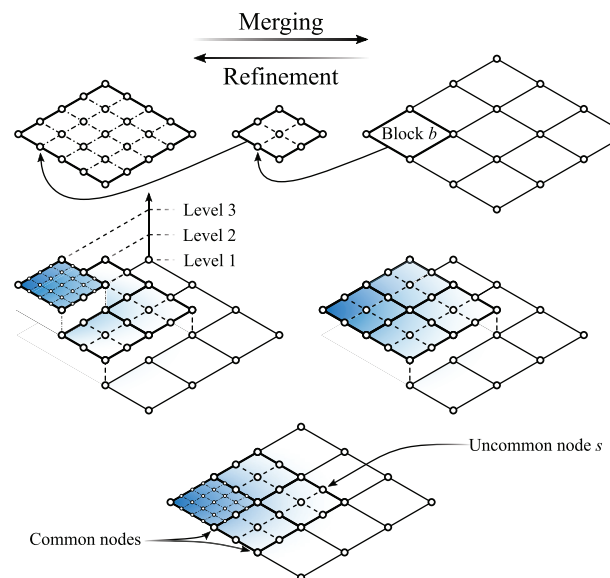
FIG. 8. Schematic of the MB-AMR technique of Ma *et al.*[103] Reproduced with permission from Ma *et al.*, Nucl. Sci. Eng. **193**, 1219–1237 (2019). Copyright 2019 Taylor & Francis.

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manufacturing, porous flows,[107] wind farm wakes,[108] bubble breakup,[109] and Rayleigh–Taylor instabilities.[110] A focus on parallelism and acceleration using graphics processing units (GPUs) has emerged where MB-AMR schemes have been parallelized, both on homogeneous[106,108–110] and heterogeneous architectures.[107,111,112] These types of AMRs are popularly coined "para-AMRs."[110,113] Schornbaum and Rüde[106] demonstrated the peta-scale computing scalability with a MB–AMR scheme on a lattice with 13.8×10^9 nodes. On accelerators, Bauer et al.,[107] Hsu et al.,[111] and Onodera et al.[112] successfully partitioned block-structured AMRs with notable speedups and reduced communication costs via communication reduced multi-time step algorithms.[112]

VI. MULTIPHASE MODELS

Fluid systems with multiple miscible or immiscible components require special treatment. In the last decade, there were noteworthy advances in the color-gradient, pseudo-potential, free-energy, and phase-field LBMs.

A. Color-gradient LBMs

The color-gradient LBM was introduced by Gunstensen et al.[114] based on the two-component lattice-gas model of Rothman and Keller,[115] which applies to immiscible fluids. The color-gradient LBM applies red and blue particle distribution functions f_i^R and f_i^B, representing the velocity distributions of two fluids. The inherent disadvantages of the method are a lack of Galilean invariance, susceptibility to spurious currents, and that phase separation requires source term models. Moreover, the accuracy significantly decays at high Reynolds numbers and density ratios, which have to be compensated for with closure models. Lishchuk et al.[116] modeled surface tension at a two-fluid interface through a continuum surface force (CSF) equation which significantly reduced, but not completely eliminated, the occurrence of spurious currents. Latva-Kokko and Rothman[117] proposed a diffusion method for creating symmetric distributions of particles around the interface to mitigate problems with lattice-pinning, which occurs when a lattice close to an interface experiences inadequate transport of either blue or red particles, so that the interface is artificially "pinned" to the lattice. Newer variants of recoloring schemes have since then eliminated these problems. For example, Ba et al.[118] successfully removed spurious currents and improved accuracy at high Reynolds numbers and density ratios by decomposing the k-colored collision parameter Ω_i^k that constitutes the momentum loss or gain in the ith direction. The decomposition yields three components: a multiple-relaxation-time operator $(\Omega_i^k)^{(1)}$ that improves stability, a perturbation operator $(\Omega_i^k)^{(2)}$ that computes high-curvature interfacial forces while eliminating spurious currents, and a recoloring operator $(\Omega_i^k)^{(3)}$ for inferring a discrete immiscible fluid boundary,

$$\Omega_i^k = \left(\Omega_i^k\right)^{(3)} \cdot \left[\left(\Omega_i^k\right)^{(1)} + \left(\Omega_i^k\right)^{(2)}\right]. \quad (32)$$

The multiple-relaxation-time operator $(\Omega_i^k)^{(1)}$ in Eq. (33) projects the color-specific distribution function f_i^k from the discrete space to the moment space, i.e., the continuum so that $\mathbf{m}_i^k = \sum_j M_{ij} f_j^k$ is a matrix including stress tensor components, densities, and other thermophysical properties,

$$\left(\Omega_i^k\right)^{(1)} = \sum_j (\mathbf{M}^{-1}\mathbf{S})_{ij}\left(m_j^k - m_j^{k,(eq)}\right) + \sum_j (\mathbf{M}^{-1})_{ij} C_j^k. \quad (33)$$

$\mathbf{S}$ is a diagonal matrix related to fluid viscosity, C_j^k is a source term which recovers the Navier–Stokes equations through the Chapman–Enskog expansion, and F_s is an interfacial tension force. $f_i^{k'}$ is the post-perturbation distribution function and $f_i^{k''}$ is the post-segregation distribution function. The perturbation operator[119] $(\Omega_i^k)^{(2)}$ in Eq. (34) generates interfacial tension using a continuum surface force (CSF) model (35), such as those of Halliday et al.[120] and Lishchuk et al.,[116] through the curvature $K = -[\mathbf{I} - \mathbf{n} \cdot \mathbf{n}] \cdot \nabla \cdot \mathbf{n}$, interfacial tension σ, and the phase field function $\rho^N = (\rho^R - \rho^B)/(\rho^R + \rho^B)$,[114,121]

$$\left(\Omega_i^k\right)^{(2)} = A^k w_i \left(1 - \frac{\omega^k}{2}\right)[3(\mathbf{c}_i - \mathbf{U}) + 9(\mathbf{c}_i \cdot \mathbf{U})\mathbf{c}_i] \cdot F_s, \quad (34)$$

$$F_s = -\frac{1}{2}\sigma K \nabla \rho^N. \quad (35)$$

Employing this operator and the CSF effectively reduces the occurrence of spurious currents and the anisotropy of the interface.

The recoloring operators formulated by Latva-Kokko and Rothman,[117] defined as

$$\left(\Omega_i^R\right)^{(3)}(f_i') \equiv f_i^{R''} = \frac{\rho^R}{\rho}f_i' + \beta w_i \frac{\rho^R \rho^B}{\rho}\cos(\varphi_i)|\mathbf{c}_i| \quad (36)$$

and

$$\left(\Omega_i^B\right)^{(3)}(f_i') \equiv f_i^{B''} = \frac{\rho^B}{\rho}f_i' + \beta w_i \frac{\rho^B \rho^R}{\rho}\cos(\varphi_i)|\mathbf{c}_i|, \quad (37)$$

ensure efficient phase segregation and a reasonably sharp interface. ϕ_i is the angle between the color gradient $\nabla \rho^N$ and $\mathbf{c}_i$ and β is an interface-thickness parameter $\in [0, 1]$.

It is noted that even though the combined use of Eq. (34) and the CSF scheme does not accurately recover the kinematic condition, it was successfully used to predict multispecies flows in bubble coalescence,[122] droplet formation,[123] and deformation under shearing.[124]

Recently, Wen et al.[125] proposed a Galilean invariant 3D color-gradient LBM with improved stability for immiscible two-phase flows. The first 3D color-gradient LBM was conceived by Tölke[126] with a D3Q19 lattice. Chapman–Enskog analysis of the LBM indicated that the following error terms in k-fluid velocity ΔU_α^k were produced in the hydrodynamic momentum equations:[127]

$$\Delta U_\alpha^k = \partial_\beta \left\{ \left(\tau - \frac{1}{2}\right)\left[\frac{1}{3}c^2 - \left(c_s^k\right)^2\right] \right.$$
$$\left. \cdot \left[U_\beta^k \partial_\alpha \rho^k + U_\alpha \partial_\beta \rho^k + \partial_\gamma \left(\rho^k U_\gamma\right)\delta_{\alpha\beta}\right] \right\}, \quad (38)$$

where $c = \delta_x/\delta_t$ is the lattice speed. In fluids with equal densities, Eq. (38) will disappear, but for dissimilar densities, Galilean invariance is lost and may impair the numerical accuracy. Wen et al. used an improved equilibrium distribution function $f_i^{k,(eq)}$ with a MRT collision operator to eliminate the error and ensure Galilean invariance. When a circular droplet was simulated in a uniform flow field with a LBM without Galilean invariance, the droplet morphed

into an elliptic shape, while it retained its circular shape with Galilean invariance.[125,128,129] Another contribution is from Lee and Ahn[130] who used a combined color-gradient-LBM and smoothed-profile-method framework to simulate spinodal decompositions and wetting of solid particles in two-fluid systems.

B. Pseudo-potential LBMs

The pseudo-potential LBM, also known as the interparticle-potential model, Shan–Chen (SC), or Shan–Doolen model, is the simplest and most popular of the Boltzmann frameworks.[31,131] The primary advantage in using the pseudo-potential LBM is that it automatically resolves, tracks and develops phase separation, without interface-tracking closure algorithms. This is due to the particle–particle interaction (for single species systems) being described by a simple force equation.[131] However, Kang et al.,[87] Chin,[132] Kang et al.,[133] and Zhang et al.[134] have reported issues with the scheme not being exclusively immiscible and not creating sharp interfaces. This is in the nature of the SC model which is a diffuse-interface model—the density is non-discrete across tens of lattices. Given that the interfaces are not tracked, the grid resolution must be uniform, which increases the requirement for the total number of lattices to adequately resolve interfaces.[30] Moreover, the particle–particle interaction must be relatively strong to maintain an interface which may incur stability issues.[135] For a multispecies, multiphase fluid system consisting of m components, the SC lattice Boltzmann equation (LBE) is written routinely with a relaxation scheme, for the k'th species, as[32,131]

$$f_i^k(\mathbf{x} + \delta\mathbf{x}, t + \delta_t) - f_i^k(\mathbf{x}, t) = -\frac{1}{\tau^k}\left(f_i^k - f_i^{k,(eq)}\right), \quad (39)$$

where $k \in \{1, \ldots, m\}$. In order to determine the streaming process, the equilibrium population for the kth species was formulated as an arbitrary function E of the component density $\rho^k = \sum_i f_i^k$, equilibrium velocity $\mathbf{c}_i^{k,(eq)}$, and the lattice configuration; $f_i^{k,(eq)} = E_i(\rho^k, \mathbf{c}_i^{k,(eq)})$. The equilibrium velocity distribution was used for determining $f_i^{k,(eq)}$. The velocity distribution, Eq. (40), is dependent on the mixture velocity $\mathbf{U}$ defined by $\rho\mathbf{U} = \sum_k \rho^k \mathbf{U}^k = \sum_k \sum_i \mathbf{c}_i \cdot f_i^k$, where $\rho = \sum_k \rho^k$ is the mixture density:

$$\mathbf{c}_i^{k,(eq)}(\mathbf{x}) = \mathbf{U}(\mathbf{x}) + \tau^k \delta_t \frac{\mathbf{F}^k}{\rho^k}. \quad (40)$$

For m phases, $\mathscr{G}$ makes up the $m \times m$ symmetric interaction matrix $\mathbf{G}^{k-\bar{k}}$ in Eq. (42). The intensity and direction of the interaction force is inferred through $\mathscr{G}^{k-\bar{k}}$ so that the negative and positive signs create attractive and repulsive forces, respectively.

The non-monotonic force $\mathbf{F}^k$, Eq. (41)—responsible for phase-change—is inferred from the interaction between the phase k and its adjacent lattice phase $\bar{k}$ from the effective densities ρ_{eff} and $\mathscr{G}^{k-\bar{k}}$ as

$$\mathbf{F}^k(\mathbf{x}) = -\rho_{\text{eff}}^k(\mathbf{x}) \sum_{\bar{k}} \mathscr{G}^{k-\bar{k}} \sum_i \rho_{\text{eff}}^{\bar{k}}(\mathbf{x} + \mathbf{c}_i \delta_t) \cdot \mathbf{c}_i, \quad (41)$$

where Green's function $\mathscr{G}^{k-\bar{k}}$ is defined by Kwok[136] and Shan and Chen[31,131] as

$$\mathscr{G}^{k-\bar{k}} = \begin{cases} 0 & |\mathbf{x} - \mathbf{x}'| > |\delta\mathbf{x}|, \\ \mathscr{G}^{k-\bar{k}} & |\mathbf{x} - \mathbf{x}'| = |\delta\mathbf{x}|. \end{cases} \quad (42)$$

The Boltzmann equation is coupled with this interaction force to adjust the particle velocities. The added benefit of this particular method is that it is stable at high density ratios $\rho_l/\rho_v \sim 10^3$ and relatively high Reynolds numbers, as compared to other LBMs. It has been applied to many fluid dynamics problems. Green's function can be used to represent fluid-fluid interactions as well as fluid–solid interactions such as wettability.[137] Recently, Reyhanian et al.[138] formulated the force in terms of the Korteweg stresses to represent phase transitions and surface tension in miscible and immiscible species.

Yang et al.[89] recently examined droplet morphology by invoking contact angle hysteresis—that is, the difference between the minimum (receding) and maximum (advancing) contact angles of a droplet on a surface—through a modified multi-relaxation time (MRT) pseudo-potential LBM with tunable surface tension. With $\bar{f}_i = f_i - \delta_t \bar{F}_i/2$ and $\Lambda_{ij} = (\mathbf{M}^{-1}\mathbf{SM})_{ij}$, the relaxed LBE in the physical space is

$$\bar{f}_i(\mathbf{x} + \delta\mathbf{x}, t + \delta_t) = \bar{f}_i(\mathbf{x}, t) - \Lambda_{ij}\left[\bar{f}_j - f_j^{(eq)}\right]\bigg|_{(\mathbf{x},t)} + \left(\boldsymbol{\delta}_{\alpha\beta} - \frac{\Lambda_{ij}}{2}\right)\bar{F}_i(\mathbf{x}, t)\delta_t, \quad (43)$$

where the forcing terms are computed as below, with the total force $\mathbf{F} = \mathbf{F}_\Psi + \mathbf{F}_g$ including the pseudo-potential interaction force $\mathbf{F}_\Psi$ and body forces $\mathbf{F}_g$ (also known as Guo's force model[32,139]). The relaxation rates in Λ are normally calculated through the thermophysical properties of the working fluid. For example, in isothermal cases such as that of Orr et al.,[30] the relaxation frequency was modeled through the kinematic viscosity ν,

$$\omega = \frac{2}{6\nu + 1}. \quad (44)$$

Writing the collision process from Eq. (43) to the moment space through the linear transformation matrix $\mathbf{M}$ yielded

$$\bar{\mathbf{m}}^\star = \bar{\mathbf{m}} - \mathbf{S}(\bar{\mathbf{m}} - \bar{\mathbf{m}}^{(eq)}) + \left(\boldsymbol{\delta}_{\alpha\beta} - \frac{\mathbf{S}}{2}\right)\delta_t \mathbf{F}. \quad (45)$$

Here, the superscript "$\star$" denotes the state at $(\mathbf{x}, t)$, and $\bar{\mathbf{m}} = \mathbf{M}\bar{f}, \bar{\mathbf{m}}^{(eq)} = \mathbf{M}f^{eq}$ and $\mathbf{F} = \mathbf{M}\bar{\mathbf{F}}$. Following the collision process, the streaming process prescribes $\bar{f}_i(\mathbf{x} + \mathbf{c}_i\delta_t, t + \delta_t) = \bar{f}_i^\star$, where $\bar{f}^\star = \mathbf{M}^{-1}\bar{\mathbf{m}}^\star$. The flow properties in the macro perspective were then $\rho = \sum_i \bar{f}_i$ and $\rho\mathbf{U} = \sum_i \bar{f}_i\mathbf{c}_i + \frac{\delta_t\mathbf{F}}{2}$. In order to simulate advancing and receding contact angles, the collision process was adjusted to

$$\text{Eq.}(45) + \delta_t \cdot \mathbf{C}. \quad (46)$$

Yang et al. used the correction term $\delta_t \cdot \mathbf{C}$ for which the D3Q19 lattice model was modeled with inspiration from Li and Luo[140] as

$$\mathbf{C} = \bigg[0, \frac{76}{5}s_\nu(Q_{xx} + Q_{yy} + Q_{zz}), 0, 0, 0, 0, 0, 0, 0,$$
$$-s_\nu(2Q_{xx} - Q_{yy} - Q_{zz}), 0, -s_\nu(Q_{yy} - Q_{zz}), 0,$$
$$s_\nu Q_{xy}, -s_\nu Q_{yz}, -s_\nu Q_{xz}, 0, 0, 0\bigg]^{-1},$$

where the tensor $\mathbf{Q}$ with the surface tension adjustment parameter κ is

$$\mathbf{Q} = \kappa \frac{G}{2} \psi(\mathbf{x}) \sum_i w(|\mathbf{c}_i|^2)[\psi(\mathbf{x} + \mathbf{c}_i \delta_t) - \psi(\mathbf{x})]\mathbf{c}_i \cdot \mathbf{c}_i. \quad (47)$$

This reformulation of the pseudo-potential framework gave rise to simulation of advancing and receding contact angles in hysteresis windows.

The pseudo-potential LBM has become the popular choice for simulating pool boiling processes due to the natural interface treatment without the need for interface tracking algorithms. Recently Zhou et al.[141] used a two-population (often referred to as double-distribution function) pseudo-potential LBM similar to the one described above with the Peng–Robinson EOS to simulate the nucleate heat transfer on square micropillar surfaces,[141] and square, circular, trapezoidal and inverted trapezoidal cavities.[142] Zhou et al.[142] found that arranging a grid of micropillars created nucleation sites between pairs of four pillars, whereas a smooth surface at the same thermophysical state would not experience nucleation. The nucleate heat transfer reported for the cavity boiling cases is all attributed to microlayer evaporation. Other studies on pool boiling also exist,[143–145] but to the authors' knowledge, not concerning cryogenic fluids. Other authors have used the pseudo-potential model for simulating droplet dynamics,[146] and cavitation.[147–150] The study of Ezzatneshan and Vaseghnia[147] revolved around cryogens and will be elaborated in Sec. VIII.

The accuracy of the two-population pseudo-potential models in predicting heat transfer have rarely been documented. Hu et al.[151] provided a comprehensive evaluation of the accuracy in the most widely used thermal models for correlating the macroscopic variables, including, T, to the equilibrium populations $f_i^{(eq)}$ and $g_i^{(eq)}$. These are the internal-energy-based (ITLB), temperature-based (TTLB), and simplified temperature-based (STTLB) thermal lattice Boltzmann models, respectively, defined as

$$\text{ITLB}: \quad g_i^{(eq)} = C_p \, T f_i^{(eq)}, \quad (48)$$

$$\text{TTLB}: g_i^{(eq)} = \frac{T f_i^{(eq)}}{\rho}, \quad (49)$$

$$\text{STTLB}: g_i^{(eq)} = w_i \, T(\mathbf{x}, t) \left[1 + \frac{\mathbf{c}_i \cdot \mathbf{c}^{(eq)}}{c_s^2} \right]. \quad (50)$$

Hu et al. compared the thermal lattice Boltzmann (LB) models to a finite-difference simulation of natural convection in a cavity and static phase change in a 1D channel. They found that the thermal LB models contained non-trivial errors. Unfortunately, no experimental validation was performed; the numerical simulations were merely compared to the numerical heat transfer model coupled with the $k - \varepsilon$ turbulence model of Barakos et al.[152] Thus, no clear benchmark was provided to establish the true physical errors in the simulations.

As an alternative to the pseudo-potential LBM with phase-change, Reyhanian et al.[138,153] recently formulated a kinetic theory that uses "peculiar" velocities (51), which comprise both the thermodynamic velocity and the velocity of a translating reference frame, in the streaming and collision processes,

$$\mathbf{v}_i = \sqrt{\frac{P}{\rho T}} \mathbf{c}_i + \mathbf{U}. \quad (51)$$

For thermal models in which not only hydrodynamic behavior is important, but other thermophysical phenomena such as phase-

change are relevant, thermodynamic consistency implies that the model possesses a well-defined temperature and specific entropy across the simulated physical regimes.[154,155] Naturally, this relies on the accurate coupling and concurrent evolution of hydrodynamic and thermodynamic behavior. As a consequence, thermodynamic consistency is often associated with a correct implementation of equations of state (EOS). The kinetic theory of Reyhanian et al. was thermodynamically consistent and eliminated issues related to non-satisfaction of Galilean invariance and allowed for very stable simulations of compressible flows as well as phase-change processes, without the requirement of models to compensate for latent heat transfer—such as the one by Ma et al.[145]

C. Free-energy LBMs

Proposed by Orlandini et al.,[156] Swift et al.,[157] and Swift et al.,[158] the free-energy LBM is purely rooted in thermodynamics, so that the particle collision parameter is based on the free energy functional Ψ. For one component non-ideal fluids, the Helmholtz free energy Ψ, Eq. (52), is written as a function of the bulk free energy ψ, and the free energy correlated with surface tension,[32,157–159] $\psi_\kappa = \kappa/2(\nabla\rho(\mathbf{x}))^2$,

$$\Psi(\mathbf{x}) = \int \left[\psi(T(\mathbf{x}), \rho(\mathbf{x})) + \frac{\kappa}{2}(\nabla\rho(\mathbf{x}))^2 \right] d\mathbf{x}. \quad (52)$$

The capillary coefficient κ gives rise to a changing energy balance and interfacial tension in areas of high density gradients near triple junctions. From the van der Waals EOS, the non-local pressure is[157]

$$p(\mathbf{x}) = \rho \frac{\delta\Psi}{\delta\rho} - \Psi = p_0 - \kappa\rho\nabla^2\rho - \frac{\kappa}{2}|\nabla\rho|^2, \quad (53)$$

where

$$p_0 = \rho \cdot \nabla\Psi(\rho) - \Psi(\mathbf{x}). \quad (54)$$

The thermodynamic pressure tensor $\tilde{\mathbf{P}}(\mathbf{x})$ is then correlated with the mixed partial derivative of the density and the surface tension as[157]

$$\tilde{\mathbf{P}}_{\alpha\beta}(\mathbf{x}) = p(\mathbf{x})\delta_{\alpha\beta} + \kappa \frac{\partial\rho}{\partial x_\alpha} \frac{\partial\rho}{\partial x_\beta}. \quad (55)$$

It is noted that $\tilde{\mathbf{P}}_{\alpha\beta}$ excludes the shear stress tensor, so that the tensor representing the total pressure is $\mathbf{P} = \tilde{\mathbf{P}}_{\alpha\beta} + \tau_{\alpha\beta}$. Then the LBE for the BGK collision model is[157]

$$f_i(\mathbf{x} + \mathbf{c}_i\delta_t, t + \delta_t) - f_i(\mathbf{x}, t) = -\frac{1}{\tau}\left[f_i - f_i^{(eq)}(\rho, \mathbf{c}, \nabla\rho)\right], \quad (56)$$

where $f_i^{(eq)}$ is formulated so as to be thermodynamically consistent and upon performing a Chapman–Enskog expansion, will recover the macroscopic equations in the hydrodynamic limit with insignificant error,[157]

$$\sum_i f_i^{(eq)} = \rho, \quad \sum_i f_i^{(eq)} \mathbf{c}_{\alpha,i} = \rho\mathbf{U}_\alpha,$$
$$\sum_i \mathbf{c}_{\alpha,i} \cdot \mathbf{c}_{\beta,i} f_i^{(eq)} = \tilde{\mathbf{P}} + \rho\mathbf{U}_\alpha \cdot \mathbf{U}_\beta. \quad (57)$$

For binary fluid systems, Swift et al.[158] introduced a free energy form based on two lattice populations f_i and g_i,

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$$\Psi = \sum \left[\psi(\rho, T, \varphi) + \frac{\kappa}{2} |\nabla \rho|^2 + \frac{\kappa}{2} |\nabla \varphi|^2 \right] d\mathbf{x}, \qquad (58)$$

where the bulk free energy density ψ is defined as a functional of the density and the sum of the higher order moment, $\varphi = \sum_i g_i^{(eq)}$, including the binary interaction strength G,[158]

$$\psi = \frac{RT}{2}(\rho - \varphi) \ln \left(\frac{\rho - \varphi}{2} \right)$$
$$+ \frac{G}{4} \rho \left(1 - \frac{\varphi^2}{\rho^2} \right) - \rho RT + \frac{RT}{2}(\rho + \varphi) \ln \left(\frac{\rho + \varphi}{2} \right). \qquad (59)$$

In order to reproduce the Navier–Stokes equations the following constraints for g_i must be obeyed:[158]

$$\sum_i g_i^{(eq)} = \varphi, \qquad \sum_i \mathbf{c}_i g_i^{(eq)} = \varphi \mathbf{U},$$
$$\sum_i \mathbf{c}_i \mathbf{c}_i g_i^{(eq)} = M_i \Delta\mu \boldsymbol{\delta}_{\alpha\beta} + \varphi \mathbf{U}_\alpha \cdot \mathbf{U}_\beta. \qquad (60)$$

Herein, M_i is the fluid "mobility" yet to be introduced in Eq. (70). From the free energy density defined in Eq. (59), the chemical potential between the pertinent components $\Delta\mu$ and the pressure tensor $\tilde{\mathbf{P}}_{\alpha\beta}$ are derived as[158]

$$\Delta\mu = -\frac{G\varphi}{2\rho} + \frac{RT}{2} \ln \left(\frac{1 + \varphi/\rho}{1 - \varphi/\rho} \right) - \kappa \nabla^2 \varphi \qquad (61)$$

and

$$\tilde{\mathbf{P}}_{\alpha\beta}(\mathbf{x}) = p(\mathbf{x})\boldsymbol{\delta}_{\alpha\beta} + \kappa \frac{\partial\rho}{\partial x_\alpha} \frac{\partial\rho}{\partial x_\beta} + \kappa \frac{\partial\varphi}{\partial x_\alpha} \frac{\partial\varphi}{\partial x_\beta}. \qquad (62)$$

The non-local pressure is then determined as[158]

$$p(\mathbf{x}) = \rho RT - \kappa(\rho\nabla^2\rho + \varphi\nabla^2\varphi) - \frac{\kappa}{2}\left(|\nabla\rho|^2 + |\nabla\varphi|^2\right). \qquad (63)$$

As with the original color-gradient method, the original free-energy LBM lacked Galilean invariance. However, a handful of studies have for certain DnQm lattice models mitigated the adverse effects from the variance property. Notably, Inamuro et al.,[128] Kalarakis et al.,[129] Swift et al.,[158] Zheng et al.[160,161] improved the triangular lattice Frisch, Hasslacher, and Pomeau (FHP)[162]-model and the D2Q9, D2Q5 lattice models. Similarly to Swift et al., Wen et al.[83] recently modified a chemical-potential based free-energy LBM through manipulation of the pressure tensor $\mathbf{P}_{\alpha\beta}$. Instead of only exerting Eq. (55) on the momentum through Eq. (57), a non-ideal force was constructed and augmented by an ideal gas pressure tensor $\mathbf{P}_{\alpha\beta}^{(0)} = c_s^2 \rho \cdot \boldsymbol{\delta}_{\alpha\beta}$ coupled with the Redlich–Kwong and the Peng–Robinson EOS, yielding

$$\nabla\mathbf{P}_{\alpha\beta} = \rho\nabla\mu, \qquad (64)$$

$$\mathbf{F}(\mathbf{x}) = -\nabla\mathbf{P}_{\alpha\beta} + \nabla\mathbf{P}_{\alpha\beta}^{(0)}$$
$$\updownarrow \qquad (65)$$
$$\mathbf{F}(\mathbf{x}) = -\rho\nabla\mu + \nabla\mathbf{P}_{\alpha\beta}^{(0)}.$$

This formulation is thermodynamically consistent and Galilean invariant,[163] with the force computed through chemical potentials. Because the pressure tensor is not computed directly via Eq. (55), as was done in previous studies,[128,129,158,160,161] computational efficiency improved and lower spurious currents were present. Zheng et al.,[161] Inamuro

et al.[164] modified the model to extend the applicability to high-density ratios, while Wen et al. also developed a chemical potential BC to simulate the wettability of solid surfaces.

Recently, Wöhrwag et al.[165] proposed a thermodynamically consistent hybrid free-energy "entropic" LBM for ternary, immiscible fluids with large density ratios of the order $\mathcal{O}(10^3)$, which subsequently was extended by Bala et al.[166] to wetting boundaries incident at solid walls with varying geometric and forcing schemes. The title implies that the collision of particles is correlated with the production of entropy when a particular fluid tends toward a thermodynamic equilibrium state. Approaches prior to Wöhrwag et al.[165] were thermodynamically inconsistent,[31,167] and could not handle significant density ratios.[168,169] Moreover, the entropic LBM proposed by Wöhrwag et al.[165] accommodated a broad spectrum of interfacial and surface tension ratios enabling the simulation of partial wetting states in Neumann triangles in liquid lenses, through full wetting with complete fluid encapsulation. The interfacial tension in the model was flexibly tuned by simulating a liquid lens and varying the Neumann angles until the existence curves predicted by the model matched theoretical solutions. Wöhrwag et al.[165] included double-well potentials to model two or more fluids, whether gaseous or liquid. The potentials were analogous to those introduced in the original free-energy model proposed by Swift et al.[158]

A study of the optimal EOS for the entropic LBM was also carried out by Wöhrwag et al.[165] A Helmholtz free-energy volumetric functional Ψ was formulated that decomposed the free energy into bulk and interfacial contributions,

$$\Psi = \int \psi_B + \psi_I \, dV. \qquad (66)$$

The bulk free energy ψ_B was defined as the sum of potentials for one gas and two liquids, expressed as

$$\psi_B = \frac{\lambda_1}{2} \left[\psi_{EOS}(\rho) - \psi_0 \right] \quad \text{(gas)}$$
$$+ \underbrace{\frac{\lambda_2}{2} \cdot C_{l,1}^2 (1 - C_{l,1})^2}_{\text{liquid 1}} + \underbrace{\frac{\lambda_3}{2} \cdot C_{l,2}^2 (1 - C_{l,2})^2}_{\text{liquid 2}}, \qquad (67)$$

where the potentials for the liquids were of the double-well form. A thorough study on the bulk free energy with various EOS was performed by Boyer and Lapuerta[170] with the Cahn–Hillard model. Their results were for three liquid potentials. Similarly to the original free-energy formulation of Swift et al.[158] and Swift et al.,[157] interfacial forces were modeled as

$$\psi_I = \frac{\kappa_1}{2}(\nabla\rho)^2 + \frac{\kappa_2}{2}(\nabla C_{l,1})^2 + \frac{\kappa_3}{2}(\nabla C_{l,2})^2, \qquad (68)$$

where λ and κ were relaxation parameters, C_l the liquid concentration, and ψ_0 the reference state free energy. The free energy ψ_{EOS} was predicted by the Carnahan–Starling (CS) EOS,[135]

$$\psi_{EOS} = \rho \left[C - a\rho - \frac{8RT(-6 + b\rho)}{(-4 + b\rho)^2} + RT\log(\rho) \right], \qquad (69)$$

in which C, a, and b are fluid-critical constants.

Wöhrwag et al.[165] noted that the Peng–Robinson and van der Waals EOS also can be implemented relatively effortlessly. Yuan and

Schaefer[135] evaluated existence curves for various EOS including the CS, Peng–Robinson, van der Waals, Shan–Chen, Redlich–Kwong, Redlich–Kwong–Soave and compared them to the Maxwell construction. Yuan and Schaefer[135] noted that the CS EOS is more generic as it has no free parameters, which may lead to inferior predictive accuracy for some fluids in comparison with other EOS, despite being defined from coexistence data. For cryogenic liquid oxygen, Orr et al.[30] reported that the CS EOS over-predicted pressure. So, the accuracy of the Shan–Chen LBM is subject to the ability of the EOS in reproducing empirical data—it is important to validate an EOS for the specific fluid to be simulated to ensure sufficient solution accuracy. The fourth-order polynomial bulk free energy from Boyer and Lapuerta[170] was used to determine the chemical potentials $\mu_\rho = \delta\Psi/\delta\rho|_{T,\phi}$, $\mu_\phi = \delta\Psi/\delta\phi|_{T,\rho}$ and the pressure tensor $\nabla P = \rho\nabla\mu_\rho + \phi\nabla\mu_\phi$. In order to solve the equations of motion at a solid–fluid boundary, the Cahn–Hillard wall-collision model (70) was employed,

$$\frac{\partial\phi_i}{\partial t} + \nabla\cdot(\phi_i\mathbf{U}) = M_i\nabla^2\mu_{\phi_i}. \tag{70}$$

The authors assumed a value for the fluid mobility M constant when it is in reality tightly coupled with the velocity field.[171] The interparticle collisions were solved routinely via the popular BGK collision operator.

D. Phase-field LBMs

Representing interfaces in ternary fluid systems is an elusive task requiring computationally intensive interface-tracking models. The most common interface theories that are used in LBM are the Cahn–Hillard [Eq. (70)] and Allen–Cahn models.[172,173] The Allen–Cahn model includes second-order derivatives which makes it more efficient, although the use of a fourth-order approximation of the diffusion term makes it susceptible to divergence.[174,175] The Cahn–Hillard model's advantage is its conservative features in comparison with the original Allen–Cahn model, although recent efforts have produced conservative versions.[176]

One of the latest phase-field LBMs was formulated by Abadi et al.[171] The authors extended the tracking algorithm of Geier et al.[177] for a two-fluid interface to ternary fluid systems by deriving the equilibrium state volume fraction $|\phi_i|^{(eq)}$ in Eq. (71) from the Euler–Lagrange (EL) differential in Eq. (72). The EL differential equation correlates the bulk free energy Φ, the capillary force term ψ, and the chemical potential in the ith phase fraction ϕ_i, which were introduced by Boyer and Lapuerta[170]

$$|\phi_i|^{(eq)} = \frac{4}{\xi}\cdot|\phi_i(1-\phi_i)|, \tag{71}$$

$$\frac{\partial\Phi}{\partial\phi_i} - \nabla\cdot\frac{\partial\psi}{\partial\phi_i} - \mu_{\phi_i} = 0. \tag{72}$$

The advection of phase i was subsequently modeled through the following conservation equation:

$$\frac{\partial\phi_i}{\partial t} + \nabla\cdot(\mathbf{U}\phi_i) = \nabla M_i\cdot\left(\nabla\phi_i - \mathbf{n}_i|\nabla\phi_i|^{(eq)} + \frac{1}{3}\sum_{i=1}^{3}\mathbf{n}_i|\nabla\phi_i|^{(eq)}\right). \tag{73}$$

The mobility of a phase M_i—a measure of the efficacy with which one phase diffuses into a neighboring phase, as a function of boundary

curvature and interfacial tension—is tightly coupled to the phase-field distribution of mass, as well as momentum transfer. Significant effort was invested in formulating mobility relations.[178–181] The mobility is especially dependent on density and the phase-field, augmenting non-linearities. Closure is achieved through a ternary formulation of the interface-tracking LBE formulated by Geier et al.,[177] Fakhari et al.,[182] with a D2Q9 lattice configuration. Moreover, hydrodynamic stability is enforced through an LBE which accommodates high density and viscosity ratios, which reduced spurious currents to below 10^{-7} lattice units. Sadeghi and Shadloo[183] used this phase-field LBM with the Cahn–Hillard interface-tracking model to simulate single and multi-mode film boiling in agreement with the Berenson[9] and Klimenko[184] correlations. In addition to this, the method has been used to simulate a wide array of problems. Ma et al.[185] proposed a spectral-difference phase-field LBM for incompressible two-fluid systems and used it to simulate rigid-body rotation of Zalesak's disk, layered Poiseuille flows, bubble deformation caused by shear, Rayleigh–Taylor instabilities, and bubble coalescence. Kalantarpour et al.[186] employed a ternary phase-field LBM to simulate static and dynamic bubble interaction at a liquid-liquid interface, Rayleigh–Taylor instabilities, as well as coalescence of a gas bubble rising in a column of water with an oil phase. Fields of bubbles in turbulent water-air pipe flows were simulated in the direct numerical simulations of Sitompul et al.[187] The phase-field LBM has also been accelerated to GPUs by Alpak et al.[188] to investigate transient binary flows in capillary tubes as well as flows in various geological formations. Moreover, the LBM is often used to simulate the convection and growth of dendritic networks of solidifying alloys.[113,189,190]

VII. HIGH-ORDER SCHEMES FOR STABLE SIMULATION OF COMPLEX FLOWS

The LBM has been criticized for its high cost in memory, inconvenient implementation of boundary conditions of higher order accuracy, and stability issues at high Reynolds numbers.[191–193] As discussed in this review, endeavors to mitigate these drawbacks were made with various numerical implementations, such as the entropic LBM that significantly improved numerical stability. Recently, stability has been vastly improved through approaches that focus on decoupling the streaming process from the pertinent lattice. However, the recovery of high-order moments implies the manipulation of complicated expansion terms that sacrifices the simplicity of the LBM. Chen et al.[194] contributed to the framework of simplified and highly stable lattice Boltzmann methods (SHSLBMs),[195–198] with a highly accurate, simplified lattice Boltzmann method (HSLBM). By employing Lagrange interpolation between equispaced "ghost-nodes" as seen in Fig. 9 with a streaming distance of 1/5 of the lattice spacing, the authors' HSLBM retained third-order accuracy in space while consuming less memory and computational time than the SHSLBM, while also being more stable. Moreover, a linear extrapolation scheme, also with third-order accuracy was proposed for determining populations at the boundaries. The non-equilibrium distribution functions were interpolated at the streaming nodes from the surrounding mesh points from the 2D Lagrange formulation with polynomials a_m and b_n. To distinguish from the i-streaming direction notation, the rectangular coordinate system has the dimension $\mathbf{x} = [x^{(\alpha)}, x^{(\beta)}]$ with indices m and n,
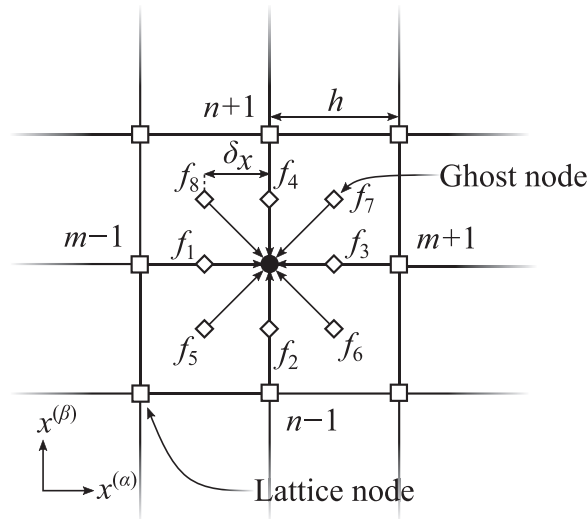
FIG. 9. HSLBM interpolation ghost nodes with a D2Q9 model. Reproduced with the permission from Chen *et al.*, Phys. Fluids **30**, 103605 (2018). Copyright 2018 AIP Publishing LLC.

$$\mathcal{L}(\mathbf{x}) = \sum_{m=1}^{M} \sum_{n=1}^{N} \mathcal{L}(\mathbf{x}(m,n)) a_m(x^{(\alpha)}) b_n(x^{(\beta)}), \quad (74)$$

$$a_m = \prod_{l=1, l \neq m}^{M} \frac{x^{(\alpha)} - x_l^{(\alpha)}}{x_m^{(\alpha)} - x_l^{(\alpha)}}, \quad (75)$$

$$b_n = \prod_{l=1, l \neq n}^{N} \frac{x^{(\beta)} - x_l^{(\beta)}}{x_n^{(\beta)} - x_l^{(\beta)}}. \quad (76)$$

A predictor–corrector scheme was adopted to obtain the macroscopic field-variables at each time step. In contrast to conventional LBMs where the distribution functions are updated in the streaming process, the HSLBM updates the macroscopic variables prior to obtaining the equilibrium distributions. This lowers the cost in virtual memory and simplifies the implementation of physical boundary conditions. The eventual numerical diffusion associated with evolution of the equilibrium distributions was recently addressed with strategies for its suppression[199] and the same method was extended to non-Newtonian fluids[200] and immersed-boundary treatments.[201]

The method has proven useful for simulating complex nanofluidic systems. Ma and Yang[202] utilized the method to simulate the natural convection from heated fins, in water–Ag–TiO$_2$ nanofluids. Li et al.[203] combined the simplified framework with the phase-field LBM to investigate multiphase ferro-hydrodynamics in ferrofluids to detail the coalescence of bubbles immersed in ferrofluid, subjected to a magnetic field. Other studies similarly investigated various configurations of ferrofluid flow problems.[204,205] It has also been formulated in terms of the finite-volume method to compute various laminar and turbulent flows.[206,207]

VIII. LBM APPLICATIONS IN CRYOGENIC FLUID SYSTEMS

This section highlights applications of the LBM to cryogenic fluid systems. The studies that have used LBMs to simulate cryogenic

phase-change, summarized in Table III, are few despite the success with which LBM has been applied to other fluids. In the earlier days of the LBM maturity, Tatsumi and Nishijima[14] used the color-gradient LBM to investigate the stability of superconductivity in a wire submerged in liquid Helium (LHe$_2$). In more recent years, Orr et al.[30] reported their development of a pseudo-potential LBM for spacecraft propellant slosh simulation in microgravity environments.

In space, low Bond numbers $Bo = \left(\rho g L_c^2 / \sigma \right)$ are useful for characterizing the hydrodynamic behavior of multiphase cryogenic flows—such as the oxidizer liquid oxygen (LO$_2$) simulated by Orr et al.[30]—due to the low gravitational acceleration relative to capillary forces. It was crucial to be able to alter gravitational effects, so they incorporate body forces into the LBE following the exact difference method (EDM) of Kupershtokh.[213] This method applies body forces simultaneously to the advection step and the equilibrium population where the subsequent shift in velocity due to the forcing is computed as $\Delta \mathbf{U} = \bar{\mathcal{F}} / \rho$, where $\bar{\mathcal{F}}$ is the momentum density, which equates to g if the gravitational field is uniform. The lattice velocity distributions are shifted to a modified velocity $\mathbf{U}^\star$ which is subsequently used to compute the collision process. The authors reported that the equilibrium populations must be updated at least twice during collision. The $(n+1)$-th time step was equated to the below, where (pc) is the post-collision state:

$$f[n+1] = (\mathbf{I} - \mathbf{M}^{-1}\mathbf{SM}) \times \left(f^{(pc)}[n] - f^{(eq)}(\mathbf{x}, \mathbf{U}, \rho) \right) + f^{(eq)}(\mathbf{x}, \mathbf{U}^\star, \rho). \quad (77)$$

With the discretized LBE $f_i(\mathbf{x} + \delta\mathbf{x}, t + \delta_t) = f_i(\mathbf{x}, t) - \boldsymbol{\Lambda}[f_i(\mathbf{x}, t) - f_i^{(eq)}(\mathbf{x}, \mathbf{U}, \rho)]$, the collision matrix $\boldsymbol{\Lambda}$ expands to

$$\boldsymbol{\Lambda}_{\alpha\beta} = \boldsymbol{\Lambda}_0 + \omega_{\alpha\beta}\Delta\boldsymbol{\Lambda}_{\alpha\beta} = \mathbf{M}^{-1}(\mathbf{S}_0 + \Delta\mathbf{S}_{\alpha\beta})\mathbf{M}, \quad (78)$$

where $\mathbf{S}_0$ is the hydrodynamic part of the relaxation matrix. The matrix $\Delta\boldsymbol{\Lambda}_{\alpha\beta}$ only relaxed the diagonal and off-diagonal entries of the pressure tensor $\mathbf{P}_{\alpha\alpha}$ and $\mathbf{P}_{\alpha\beta}$, respectively. With $\Delta f[n] = f^{(pc)}[n] - f^{(eq)}(\mathbf{x}, \mathbf{U}^\star, \rho)$, the collision equation for the MRT scheme with body forcing is

$$f[n+1] = (\mathbf{I} - \boldsymbol{\Lambda}_0)\Delta f[n] + f^{(eq)}(\mathbf{x}, \mathbf{U}^\star, \rho) - \omega_{\alpha\beta}\Delta\boldsymbol{\Lambda}_{\alpha\beta}\Delta f[n]. \quad (79)$$

Crucial to the simulation of spacecraft dynamics is the total force acting on the entire fluid domain, which was computed as the difference between body forces and internal forces (in terms of momentum density),

$$\bar{\mathcal{F}}_d[n] = \sum_{\alpha\beta} \bar{\mathcal{F}}_{\alpha\beta} - \left(\sum_{\alpha\beta} \rho_{\alpha\beta} U_{\alpha\beta}[n] - \sum_{\alpha\beta} \rho_{\alpha\beta} U_{\alpha\beta}[n-1] \right). \quad (80)$$

Orr et al.[30] used the above approach to compute the lateral sloshing of LO$_2$ in an asymmetrical tank with a gravitational field of $g = 0.001g_0$ at 15° in relation to the axial direction. Their 2D solution at $t = 9.8$ s is depicted in Fig. 10, which shows the velocity field in lattice units. For spacecraft dynamics in microgravity environments, convection caused by gradients in interfacial tension is characterized through the Bond number, $Bo = \rho g L_c^2 / \sigma$. The primary mode oscillated with a frequency of $\mathcal{O}(10^{-2})$ Hz with a modest lateral force of $\mathcal{O}(10^{-4})$ N. The simulation showed strong advective patterns in the

TABLE III. Overview of published works on cryogenic fluids using LBMs: (a)—Tatsumi and Nishijima (2003),[14] (b)—Izumi *et al.* (2004),[208] (c)—Imre *et al.* (2008),[209] (d)—Orr *et al.* (2015),[30] (e)—Traudt and Schlechtriem (2019),[94] and (f)—Ezzatneshan and Vaseghnia (2020).[147]

Study	LBM	Cases	Conditions
(a)	Color gradient	Natural convection around superconducting wire	Subcooled, LHe$_2$, thermal response, and convective stability to varying transport currents, dynamic viscosity $\mu = 5 \times 10^{-6}$ Pa s
(b)	Pseudo-potential	Heterogeneous nucleation	Continuation of "(a)" with phase transition
(c)	Pseudo-potential	Spinodal estimation	Lennard–Jones Argon at 128 K, liquid film in vapor, gravitation-free, accompanied by molecular dynamics simulations
(d)	Pseudo-potential	Varying wetting (i)	(i): LO$_2$, corner geometry, negative (hydrophobic), neutral, and positive (hydrophilic) wall interaction potentials, contact angle $\theta < \pi/2$
		Lateral sloshing in tank, frequency analysis (ii)	(ii): LO$_2$, surface tension $\sigma = 0.0122$ N/m, Bond/Eötvös number $Bo = \Delta\rho g L^2/\sigma \sim 20$, acc. $g = 0.001 \cdot g_0$
(e)	Finite-difference, multi-speed	Lid-driven cavity (i)	(i) Gaseous nitrogen at 114 K and 0.306 MPa, laminar, incompressible flow, $Re < 5000$, ideal-gas model
		Riemann shock tube (ii)	(ii) Supercritical/gaseous oxygen, $\rho_{t=0} \in [43.6, 170] (\text{kg/m}^3)$, $T_{t=0} \in [139, 170]$ (K), $Ma \in [1.118, 1.139]$, ideal-gas model
		Saturated film boiling (iii)	(iii): LO 2, $T_{t=0} = T_{\text{sat}} = 139$ K, $\rho = 723$ kg/m^3, 1.2 MPa, $\Delta T \in [5, 62]$
(f)	Pseudo-potential	Validation study (i)	(i): H$_2$O , LN$_2$, LH$_2$ droplets suspended in vapor, verification with Laplace law and the Maxwell construction, validation from NIST.[210]
		Heterogeneous cavitation-bubble nucleation (ii)	(ii): H$_2$O, LN$_2$, LH$_2$, $\rho_l/\rho_v \in [13, 112]$, phase transition inception with the energy-barrier equation,[211] verification from the Rayleigh–Plesset equation[212]
		Cav.-bubble collapse near solid surface (iii)	(iii): H$_2$O, LN$_2$, LH$_2$, collapse time sensitivity to varying bubble-to-wall distance and contact angle $\theta = \{30°, 90°, 150°\}$

vapor phase in the form of rotational structures emanating from the triple junctions at the tank walls. The interface behavior at the triple junctions suggests that the wettability of the wall produces an apparent attractive effect at the pertaining low Bond number of the problem.

Traudt and Schlechtriem[94] used a van der Waals-based finite-difference LBM to simulate transient two-phase flow of cryogenic propellants in rocket engine feed systems, including test cases on single LO$_2$ bubble evaporation and the Riemann shock problem. Their model showed the capability to resolve shocks and supersonic flow, which are also relevant to modeling the gas dynamics involved in rapid phase transitions that may occur during high ΔT film boiling. In the design of rocket engines and their propellant feeding systems, the complexity of valve configurations and timing upon startup incur high costs in prototyping, as the integrity of the engine is highly prone to damage from the timing of said valves. The fuel and oxidizer are most often cryogenic and cavitate when the valves open and also experience heterogeneous nucleation when contacting the solid engine parts. Moreover, after cooling the rocket nozzle and being pressurized in turbopumps, the cryogens may become supercritical. Thus, numerical methods for simulating the transient startup processes are required to be stable at high Reynolds numbers, compressible, sub- and supercritical multiphase flows of non-ideal fluids, in complex geometries.

Traudt and Schlechtriem[94] used the multi-speed model of Watari and Tsutahara[91] which has proven to be accurate for supersonic flow simulations,[214] with an extension for simulating non-ideal van der Waals fluids.[92] The real-gas model of Gonnella *et al.*[92] implemented a force term similar to the pseudo-potential LBM that emulates the interaction forces between molecules to simulate phase transitions and continuous density gradients across interfaces. Since the lattice speeds are lattice-speed independent, a finite difference discretization was used with a van-Leer limiter in the flux $\ddot{F}$ at the halfway distance $j \pm 1/2$ to the neighboring node j,

$$f_i(n+1) = f_i(n) - \frac{c_k \delta_t}{w_i \delta_x}\left[\ddot{F}j + 1/2 - \ddot{F}j - 1/2\right]_{(n)}$$
$$- \frac{\delta_t}{\tau}\left[f_i(n) - f_i^{(eq)}\right]_{(n)} - \delta_t \cdot F_i, \quad (81)$$

where

$$\ddot{F}j + 1/2 = f_i + \frac{1}{2}\left(1 - \frac{c_k \delta_t}{w_i \delta_x}\right)\left[f_i^{j+1} - f_i\right]_{(n)}\tilde{\Psi}(\Theta), \quad (82)$$

and Θ_i^j is a smoothness function and $\tilde{\Psi}$ is a flux delimiter,

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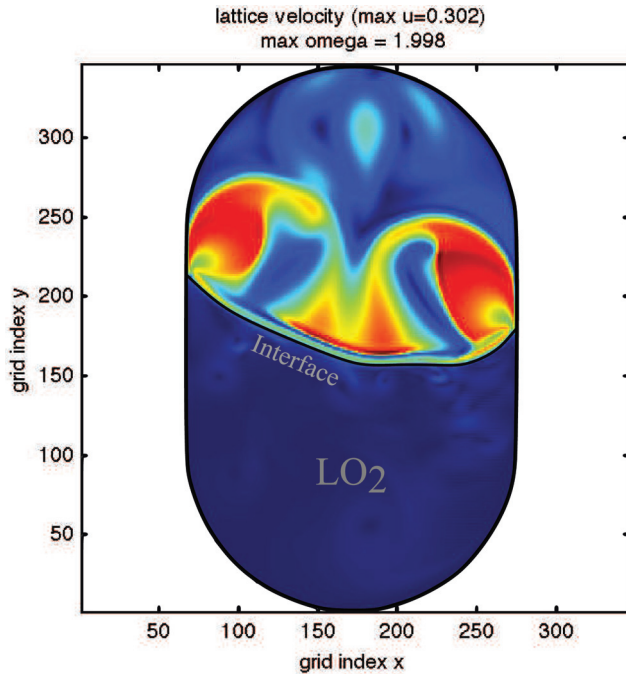
FIG. 10. Instantaneous velocity contour of LO_2 propellant undergoing lateral sloshing in a tank. Solution from an isothermal simulation with the pseudo-potential method. Reproduced with the permission from Orr *et al.*, in American Astronautical Society (AAS) Guidance, Navigation, and Control Conference (National Aeronautics and Space Administration, Breckenridge, CO, USA, 2015).[30] Copyright 2015 National Aeronautics and Space Administration.

$$\Theta_i^j = \frac{f_i^j - f_i^{j-1}}{f_i^{j+1} - f_i^j}, \tag{83}$$

$$\tilde{\Psi} = \begin{cases} 0 & \Theta_i^j \leq 0 \\ \dfrac{2\Theta_i^j}{1 + \Theta_i^j} & \Theta_i^j > 0. \end{cases} \tag{84}$$

The multi-speed model produced no error through the Chapman–Enskog expansion and improved stability in multiphase, compressible flows. The van der Waals EOS contains derivatives that Traudt and Schlechtriem[94] computed with a fourth-order accuracy through a nine-point discretization. The authors' simulations comprised a Riemann shock problem with LO_2. In comparison with the analytical solution of Wagner,[215] predictions for the velocities, pressures, temperatures, and densities for four different simulations incurred <1% error. Traudt and Schlechtriem[94] also simulated the film boiling of LO_2 with good agreement with experiments.

The comparative study of Peng *et al.*[216] found that of the velocity shifting method (VSM), exact difference method (EDM) and Guo's force schemes, the VSM and EDM allowed for the highest density ratios. Thus, Ezzatneshan and Vaseghnia[147] employed the VSM and EDM in a pseudo-potential LBM for studying the nucleation and collapse of cavitation bubbles in water, LN_2, and LH_2. In the VSM, the hydrodynamic velocity is shifted by the sum of the pertinent body forces (e.g., interaction, gravitational, fluid–solid) **F** so that the velocity used in the equilibrium distribution is

$$\mathbf{U}^{(eq)} = \mathbf{U} + \frac{\tau \mathbf{F}}{\rho}, \tag{85}$$

and the real velocity field is redefined as

$$\tilde{\mathbf{U}} = \mathbf{U} + \frac{\mathbf{F}\delta_t}{2\rho}. \tag{86}$$

In the EDM, the body forces are directly added to the RHS of the LBE,

$$f_i(\mathbf{x} + \mathbf{c}_i\delta_t, t + \delta_t) - f_i(\mathbf{x}, t) = -\frac{\delta_t}{\tau}\left[f_i(\mathbf{x}, t) - f_i^{(eq)}(\rho, \mathbf{U})\right] + f_i^{(eq)}(\rho, \mathbf{U}, \Delta\mathbf{U}) - f_i^{(eq)}(\rho, \mathbf{U}), \tag{87}$$

where $\Delta\mathbf{U} = \mathbf{F}\delta_t/\rho$. Ezzatneshan and Vaseghnia conducted a sensitivity analysis of the bubble nucleation/collapse dynamics with varying vapor-to-liquid pressure differences $\Delta P = P_l - P_v$ via the "energy-barrier equation"

$$\Delta E = 4\pi R^2 \sigma + \frac{4}{3}\pi R^3 \Delta P, \tag{88}$$

which relates the total system energy to the cavity radius R and the surface tension σ. The inequality of this equation leads to phase transition, but the equality preserves any liquid-vapor pair in an equilibrium state where a critical pressure difference $\Delta P_c = -\sigma/R$ (the Laplace law) is unique for a fluid—i.e., $\Delta P_c = \{-0.009\,028\,5, -0.006\,335\,9, -0.009\,028\,5\}$ (lattice-units) for H_2O, LN_2, and LH_2, respectively.[147] The authors were able to verify the growth dynamics from the Rayleigh–Plesset equation[212] and investigated the nucleation of a cavity in a liquid filled with microbubbles, as well as the collapse of a cavity near a solid wall with varying wettability and wall-to-cavity distance. The authors found that the collapse of the water cavity, in comparison with the cryogens, was more aggressive (as indicated in Fig. 11), in agreement with the experiments of Dular and
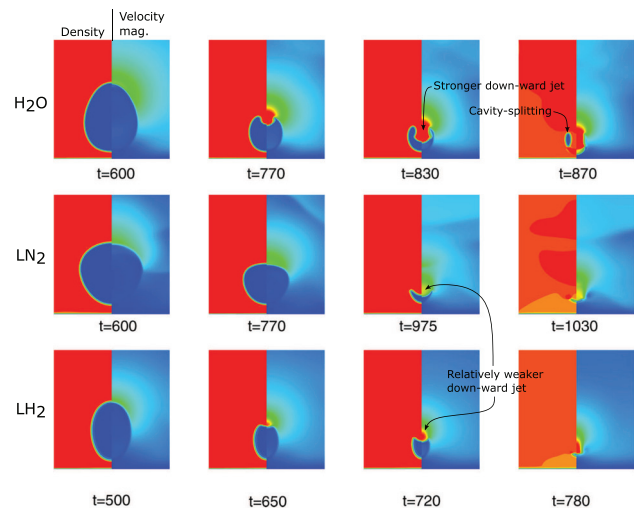
FIG. 11. Collapse of H_2O, LN_2, and LH_2 cavities near a solid wall by Ezzatneshan and Vaseghnia.[147] Reproduced with permission from Ezzatneshan and Vaseghnia, Phys. Rev. E **102**, 053309 (2020). Copyright 2020 American Physical Society.

Petkovšek.[217] The distinct collapsing behavior was owed to the implementation of the acentric factor in the authors LBM which is a measure of the molecular structure and polarity in a fluid, where a low acentricity is associated with spherical molecules with low polarity.[218]

A stable liquid is bounded by its equilibrium curve between its freezing and boiling points, but outside of this in the metastable region the liquid will become unstable and prefer a new thermodynamic state. However, beyond the equilibrium with either superheating or subcooling substances can exist in their liquid state under certain conditions—i.e., if no impurities exist and the system is not disturbed by external forces.[219] However, the metastable region is similarly bounded by stability limits in either of the directions of superheating and subcooling, beyond which vapors and liquids cannot exist.[209] Such a limit is termed a "spinodal" and these are impossible to determine experimentally[209]—a full elimination of impurities and disturbances in a given substance is impractical to achieve. Accordingly, Imre et al.[209] simulated a liquid film surrounded by vapor in a zero-gravity environment, with a pseudo-potential LBM (and a molecular-dynamics simulation). They found that the employed equation of state[31] in the LBM—extended deep into the metastable extremes—was able to reproduce the liquid spinodal for argon, derived from experimental results for interfacial thickness and surface tension. The authors' simulations are useful for further development of EOS applicable to metastable systems.

Modeling accidental spills of cryogenic fluids on water is relevant to shipping of LNG and its use as a marine fuel. Accurate models of cryogenic spills require elucidating the heat transfer characteristics of the ice formed in water following contact with the cryogenic LNG, as well as a better understanding of how water turbulence affects the freezing rate and overall heat transfer between the two fluids. Recently, Li et al.[220] proposed a pseudo-potential LBM with a concurrent evaporation, condensation, and freezing phase-change model based on enthalpy. The authors employed two populations for momentum and energy, Eqs. (89) and (92), to resolve the velocity, pressure, and temperature fields,

$$f_i(n+1) - f_i(n) = -\frac{1-B}{\tau_f}\left[f_i - f_i^{(eq)}\right] + B\Omega_i^s + (1-B)\Delta f_i. \quad (89)$$

$\Omega_i^s = f_{i^-} - f_i + f_i^{(eq)}(\rho, \mathbf{U}_s), -f_i^{(eq)}(\rho, \mathbf{U})$ is a bounce-back collision term for the non-equilibrium part of f with $\mathbf{U}_s$ being the velocity of the solid. The f-population was weighted by B which relaxes the collision process as a function of the relaxation time τ_f and the solid volume fraction f_s,

$$B = \frac{f_s(\tau_f - 1/2)}{1/2 - f_s + \tau_f}. \quad (90)$$

The solid volume fraction is unity for an iced phase and zero for liquid, and $0 < f_s < 1$ for multiple phases including vapor, and was determined based on enthalpy,[137]

$$f_s = \begin{cases} 0 & H > H_l \\ \dfrac{H - H_s}{H_l - H_s} & H_s < H < H_l \\ 1 & H < H_s. \end{cases} \quad (91)$$

The population corresponding to energy is a function of two source terms ϕ_{vl} and ϕ_{ls}

$$g_i(n+1) - g_i(n) = -\frac{1}{\tau_T}\left[g_i - g_i^{(eq)}\right] + \delta_t w_i(\phi_{vl} + \phi_{ls}). \quad (92)$$

The generic algorithm computed the freezing phase change by computing ϕ_{vl} and ϕ_{ls} prior to the collision step, and enthalpy and f_s after computing the macroscopic variables. In terms of Fourier number, $Fo = \alpha_s t / l_0^2$, Li et al.[220] simulated a cryogenic spot with water vapor undergoing condensation and freezing phase change.

The phase morphology predicted by Li et al.[220] for a droplet solidifying on a vertical substrate is depicted in Fig. 12. In agreement with Yang et al.,[89] Li et al.[220] noted that surface wettability affects the morphology of liquid droplets but not the growth of ice under concurrent evaporation, condensation, and freezing phase-change. The wettability was inferred through the body forces $\mathbf{F} = \mathbf{F}_\Psi + \mathbf{F}_s + \mathbf{F}_g$ with $\mathbf{F}_s$ representing fluid–solid interaction. Preceding this work, Sun et al.[137] developed a LBM for modeling the freezing phase-change heat transfer within a droplet as well as surface frost formation on a horizontal surface from air humidity. To resolve the frost layer, they adopted porous media permeability theory so that the fluid streams according to $f_i'(\mathbf{x} + \delta\mathbf{x}, t + \delta_t) = f_i(\mathbf{x}, t)$ when $f_s = 0$, the populations remained stationary when $f_s = 1$, and if $0 < f_s < 1$ the populations contained a solid–fluid mixture and only a fraction of f_i streams with a modified streaming equation,

$$f_i'(\mathbf{x} + \delta\mathbf{x}, t + \delta_t) = (1 - f_s)f_i(\mathbf{x}, t) + f_s f_i(\mathbf{x} + \delta\mathbf{x}). \quad (93)$$

In addition, Zhao et al.[221] simulated the impact dynamics of a droplet on freezing surfaces. The importance of concurrent evaporation, condensation, and freezing phase-change in cryogenic spills is
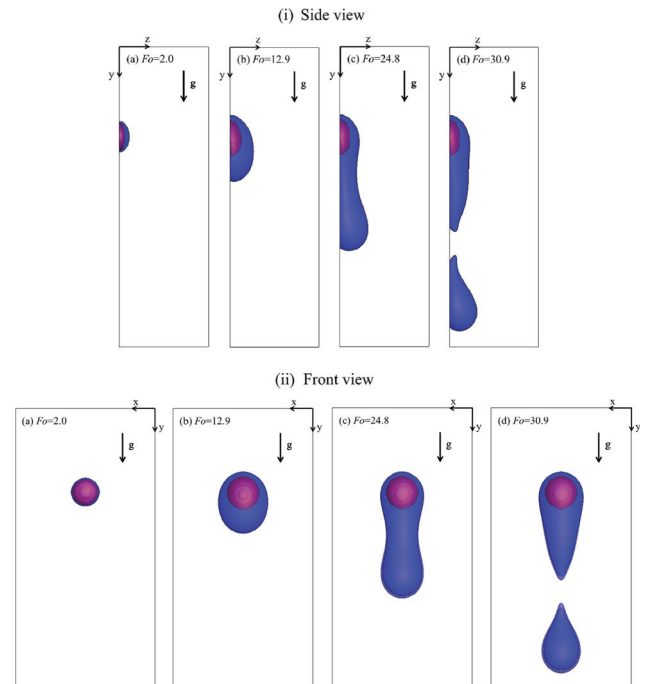
FIG. 12. Freezing droplet morphology as reported in the paper by Li et al.[220] The ice phase is purple and the liquid phase blue. Reproduced with permission from Li et al., Int. J. Heat Mass Transfer **114**, 628–639 (2017). Copyright 2017 Elsevier.

exemplified in the fact that the cryogen comes in contact with water in ocean spills in which an ice film will interact with both the ambient humid air and water phases. Furthermore, the subsequent dispersion of the cold vapor triggers the condensation of the unsaturated vapor in the air.

IX. DISCUSSION

Throughout this paper, we have presented lattice Boltzmann methods relevant to many fluid and flow configurations, despite cryogens being our main area of research. The limited number of studies discussed in Sec. VIII shows that application of LBMs to cryogens is still in its infancy, and requires further development. In particular, the authors' aim is to conduct massively parallel simulations of accidental spills of cryogens (especially liquefied natural gas and hydrogen) on solid substrates as well as on water to elucidate the fundamental nature of the pertinent fluid dynamics as well as inform our industrial partners and their work with storage and transport of LNG and LH_2.

There are several challenges in formulating the relevant numerics for the physics that constitute this problem. The interaction between nucleation sites in the nucleate boiling regime on solid substrates will require the simulation of clusters of sites. This contrasts the studies reviewed herein, that only considered the evolution of bubbles from a single nucleation site. Furthermore, wetting transitions have been observed in cryogens,[72–77] meaning that they are susceptible to thermal hysteresis. As the ability for a fluid to nucleate is proportional to its ability to spread on a solid surface, knowledge of the contact angle dynamics is important to accurately predict nucleation rates. In contrast to water which is polar, cryogens exhibit weak self-mutual molecular interactions that can be represented by van der Waals forces.[222] In order to infer a rigorous thermal dependence, future research can investigate the formulation of explicit temperature dependence in, e.g., the pseudo-potential LBM. The contact angle of cryogens, which virtually is zero,[82] results in non-isothermal phase-change and thereby a non-trivial dependence on a thermal condition in the molecular interaction potentials. A parametric investigation of contact angle hysteresis in cryogens does not exist on the basis of the presently reviewed content, although analytical approximations do exist.[223,224] Additionally, as cryogens are especially sensitive to surface treatments,[82] an elucidation of their effects on the contact angle will also be valuable for finding methods for controlling the onset of boiling and critical heat flux, which is relevant to minimizing boiloff in storage applications.

Successful simulations of cryogenic spills will include concurrent turbulence, freezing and boiling phase change, contact angle hysteresis, various free-surface perturbations, Rayleigh–Taylor instabilities and splashing, and conjugate solid–fluid heat transfer. As exemplified so far, each of these fundamental phenomena have been simulated separately, and the associated publications provide a road-map for the design of more complicated multi-physics simulations of realistic spill scenarios. To our knowledge, no investigations have attempted to encompass all of these simultaneously in a single framework. We expect that this will constitute an enormous challenge. Given the span of scales in cryogenic spill problems both in terms of the turbulence cascade and the evolution of embryonic nuclei to detached, fully developed bubbles, direct numerical simulations will be appropriate for our planned work. The associated computational demand will necessitate high-performance computing resources. The presented para-AMRs

(Sec. V) and methodologies for GPU-acceleration[42,44,107,111,112] may prove beneficial.

This review can also pave the way for investigations of other problems, where the above-mentioned phenomena also occur. The majority of the reviewed LBMs revolved around immiscible species. LNG, which is a multi-component mixture, experiences species stratification over time, potentially resulting in adverse roll-over phenomena. Accurate modeling of these requires LBM frameworks with the capability of simulating ternary mixtures with cross-diffusing species, which requires more development. Recently, a couple of studies have developed miscible extensions in the phase-field LBM[225] and through forcing terms,[226] for which the latter can be extended to all of the LBMs reported herein. In diffuse interfaces where diffusion is so slow that large interfacial concentration gradients exist for extended durations, Korteweg stresses, or "effective interfacial tension" arise,[227] which can drive viscous fingering instabilities.[228] Elucidating if this can trigger roll-over in LNG is another avenue for research. In favor of this, the Korteweg stress has recently been incorporated in a kinetic theory.[138]

In space-craft propulsion—specifically compressors—cryogenic fluids can reach their supercritical states. In such applications equations-of-state that can cover the sub- and supercritical regimes in cryogens are important. A further review of equations of state that can cover this range and are applicable to cryogens would be valuable. In turbomachinery used in pumping applications for cryogen storage and transport, cryogens can undergo cavitation. Previous studies have investigated cavitation[147–150] as well as compressible flows of cryogens[94] and other fluids.[138]

In addition, the review has included several LBMs with applications of other fluid systems as a by-product, not limited to nanofluids, porous flows, biological flows, neutron transport, among others, that can hopefully inspire readers studying other topics than cryogenic fluids.

X. CONCLUSION AND FUTURE WORK

We have identified some key applications in which cryogenic fluids such as liquefied natural gas (LNG), hydrogen (LH_2), and helium (LHe_2), are used—propulsion systems in trucking, marine carriers, and spacecraft, as well as medical devices and scientific equipment in spacecraft, among others. Ultracold LNG and LH_2 have much higher densities compared to their gaseous states making them more cost-efficient during marine transport. However, in their cryogenic state, their interaction with standard-state conditions is associated with non-isothermal phase-change mechanisms—turbulent cavitation in turbomachinery, "rapid phase transition" in spills on hot liquid and solid substrates, contact angle hysteresis, and turbulent free-surfaces in spills on water, with concurrent freezing, condensation, and evaporation phase-change. To assess the ability to simulate such applications, we reviewed lattice Boltzmann methods (LBMs) for stable simulation at high Reynolds numbers including collision operators, boundary conditions, adaptive-mesh refinement, multiphase models, and high-order discretization schemes. As a consequence of these reviewed models having revolved around other fluids than cryogens, the reader will find the scope of this paper to be relatively broad, but our main purpose is to illustrate their capabilities and applicability to cryogenic fluid systems. Conclusively, we showed that there exist few LBM studies that have been dedicated to cryogenic flows, but that the LBM has

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been extended to simulate many of the phenomena and mechanisms that are found in the physics of cryogenic fluids.

We synthesized the various collision operators that are currently in use, namely single-relaxation and multi-relaxation time (MRT) schemes and entropic stabilizers. The correct implementation of these affects the numerical stability, accuracy, and ability to simulate turbulent flows. Within the last three years significant process was made in formulating MRTs and entropic extensions that can reliably simulate rich turbulent flow fields inspired by many applications. A particular class of LBMs, "simplified and highly stable lattice Boltzmann methods" have proven to significantly reduce memory consumption and enhance computational efficiency and stability. However, these methods should be used with care as they can be diffusive, which may not be appropriate for turbulent flow simulations.

Recent developments in multiphase LBMs have permitted simulating contact angle hysteresis, varying surface chemical potentials—for emulating surface hydrophibicity/philicity—and conjugate heat transfer in fluid–solid couples. We reviewed methods for inferring tunable surface tension, phase transitions, and non-ideal fluid behavior—namely via color-gradient, pseudo-potential, free-energy, and phase-field LBMs. Historically, the LBM has experienced issues with spurious current in interfaces with high curvature, but the aforementioned schemes have all been developed with trivial currents.

Only six studies have employed LBMs specifically for modeling cryogenic fluid systems despite the multiphase-capabilities of the LBM. Available studies have been limited to the color-gradient and pseudo-potential approaches for modeling multiphase flows in cryogenic conditions. The main applications have been fuel-storage for spacecraft, shocks, cavitation, and pool-boiling. With the extreme temperatures in cryogens, we also reviewed models for freezing-phase change relevant to spills on water.

Our primary interest and active area of research is employing our own LBM codes to simulate spill and subsequent pool boiling in various cryogens on both solid and liquid substrates, in order to develop lower-order empirical models for use in larger-scale problems and to provide fundamental insight into the evolution of phase change dynamics in especially the nucleate and transitional regimes.[229,230] Significant challenges exist with developing accurate, deterministic closure models in the hydrodynamic limit and minimizing the inherent computational costs. Especially the baroclinic nature of cryogens has emerged in our previous works.[230] The review provides a roadmap for extending an in-house LBM that has been used for studies on turbulence,[231] porous media flows,[232,233] and microfluidics[234] to allow computationally efficient, large-scale simulations of cryogenic flows.

AUTHORS' CONTRIBUTIONS

K.J.P. conducted the literature survey and composed the manuscript. J.R.B. conceptualized the study and reviewed the manuscript.

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DATA AVAILABILITY

Data sharing is not applicable to this article as no new data were created or analyzed in this study.

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