
DWSIM - Process Simulation, Modeling and Optimization User Guide

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DWSIM - Process Simulation, Modeling and Optimization

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1 Introduction

This document gives a detailed description about how to setup, run, modify and view results of a basic process simulation in DWSIM. The document is organized according to the sequence of execution of a simulation. Each step/task is explained with the help of images and descriptions of the associated windows.

For details about the models used for calculation of thermodynamic, transport and thermal properties, please read the **Technical Manual**. Detailed Unit Operations and Utilities' descriptions can be found in the context-sensitive help available inside the application by through the 'F1' key.

Visit DWSIM's Wiki for more up-to-date information about DWSIM, including general usage tips and tricks.

2 Welcome screen

When DWSIM is opened, the welcome screen is shown (Figure 1):



Figure 1: DWSIM's welcome screen.

The welcome screen provides the user with shortcuts to open existing simulations, create new ones, create new compound creator and data regression cases and open the samples folder. The "Close Window" button closes the window and shows the main DWSIM interface.

The following items are displayed on DWSIM's main window:

- **Menu bar**, with buttons to open/save/create simulations, component creator and data regression cases, configure the active simulation, general preferences, launch tools, configure the child windows view mode, etc.;
- **Button strip**, to open, save and create new steady-state simulations, component creator and data regression cases.

There are various ways to access the most commonly operations with simulation files and component creator/data regression cases - open, save and create. In the next sections you will be guided through some necessary steps to create and configure a steady-state simulation, a compound creator and/or a data regression case.

3 Simulation

3.1 User Interface

The "Create a new steady-state simulation" button in the welcome window can be used to create a new simulation. After the simulation is created, the **configuration window** (Figure 3) is shown. The simulation configuration interface consists in a tabbed window:

- **Compounds** - Add or remove compounds to/from the simulation and petroleum fractions (pseudocomponents) utilities.
- **Basis** - Property Package configuration, phase equilibrium flash algorithm selection and other advanced thermodynamic model settings.
- **System of Units** - Management of Systems of Units.
- **Miscellaneous** - Simulation info (title, author and description), number formatting and password settings.
- **Property Tables** - Definition of objects properties to be shown on flowsheet floating tables.

3.2 Configuration

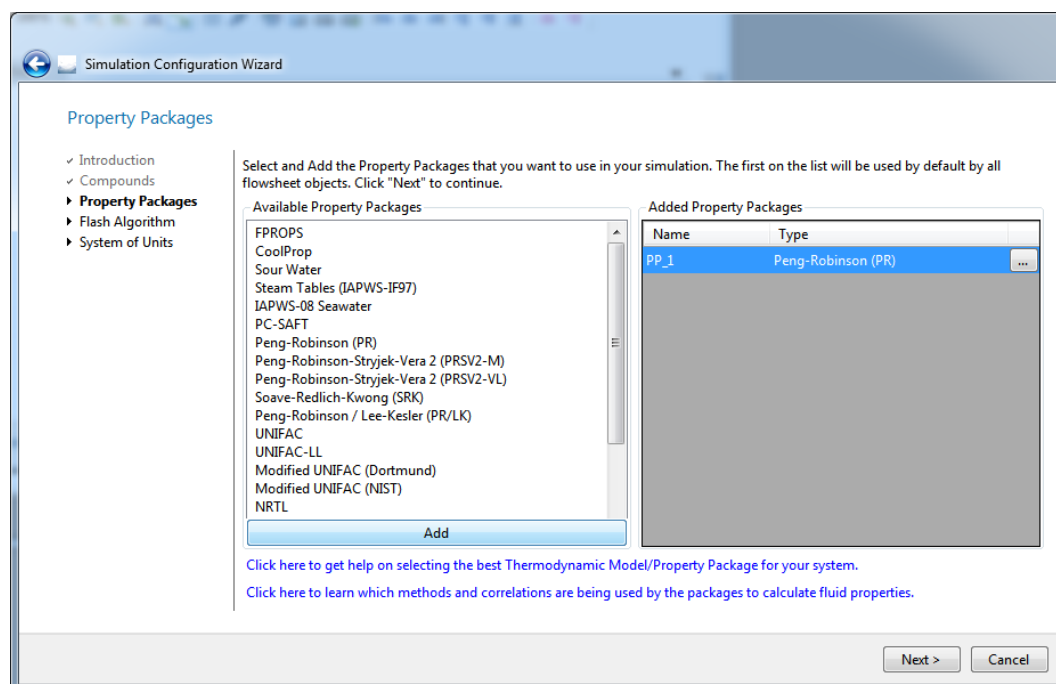


Figure 2: Simulation Configuration Wizard.

Since DWSIM 3.3, a new Simulation Configuration Wizard (Figure 2) is opened as soon as a new simulation is created, and will display the interfaces described in the following sections in a more streamlined way. The older simulation configuration window can be accessed anytime during the simulation or through a button located in the first page of the config wizard.

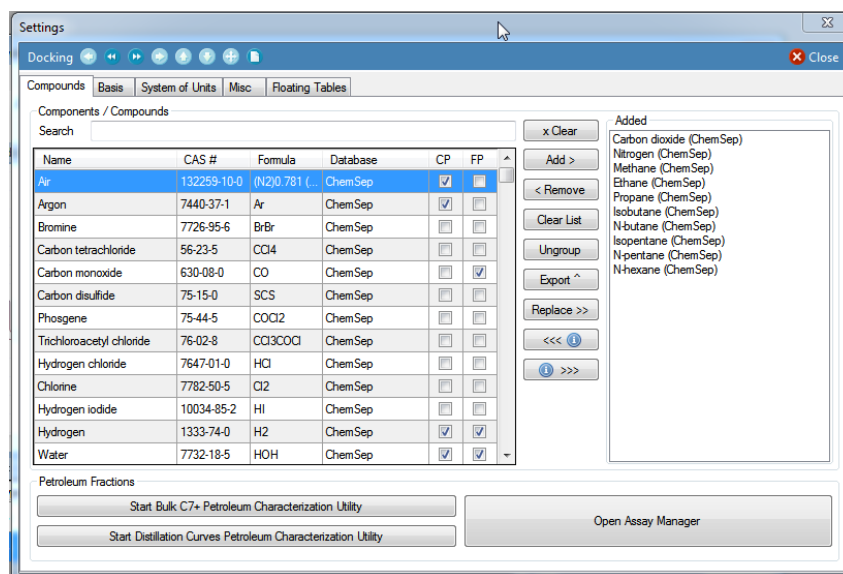


Figure 3: Simulation configuration window.

The simulation configuration window (Figure 3) is the interface where all the functions for configuration and personalization of a simulation in DWSIM can be found. In this window, the user can manage the simulation components, the property package (thermodynamic model), units system and number format, among other options.



The simulation configuration window can be accessed anytime when a simulation is opened in DWSIM. The changes made through it have immediate effect on the simulation.

3.2.1 Components/Compounds

There are two essential information required by DWSIM in order to correctly start a simulation. The first refers to the available **components** (or **compounds**). There are three types of components which can be managed in DWSIM - the first type are the components present in the database. The second, **hypotheticals**, and the third, **pseudocomponents**, are components which can be added by the user through the **Compound Creator** or the **Petroleum Characterization** utilities. These user-created components will be available in the end of the component list inside the "Components" tab for inclusion or removal from the simulation as required.



View the section 3.8 for information about the compound creation utilities.

3.2.2 Basis

Property Packages The Property Package consists in a set of methods and models for the calculation of physical and chemical properties of material streams in the simulation. It is composed of a thermodynamic model - an equation of state or a hybrid model - and methods

for property calculation, like the surface tension of the liquid phase. The figure 4 shows the interface for configuration of the property package.

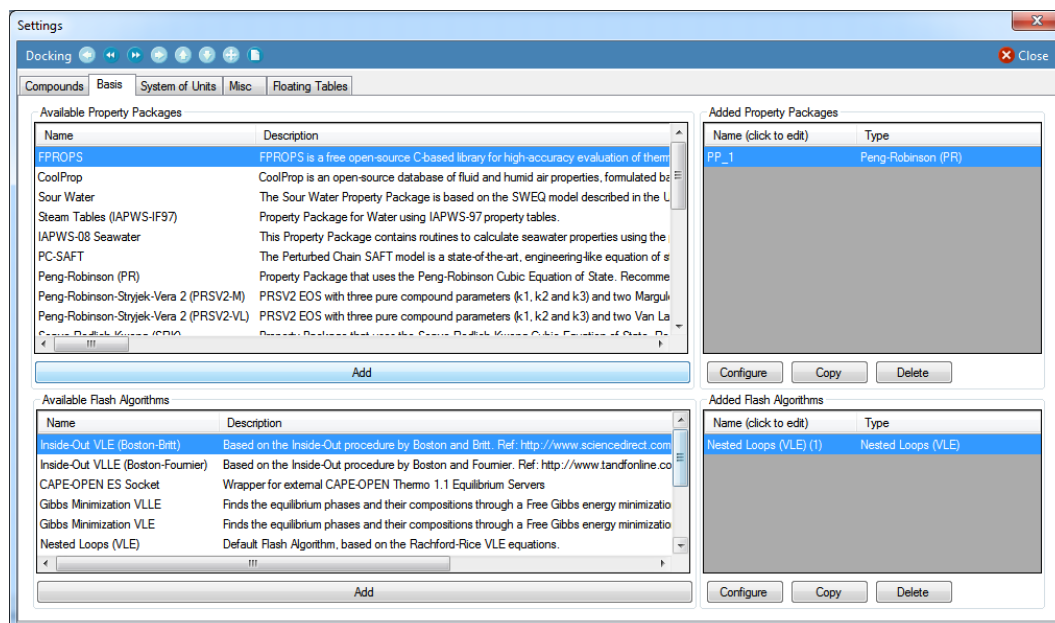


Figure 4: Property Package configuration interface.

If the selected property package has any editable property, the "Configure" button becomes clickable and the user can click on it to show the property package configuration window.

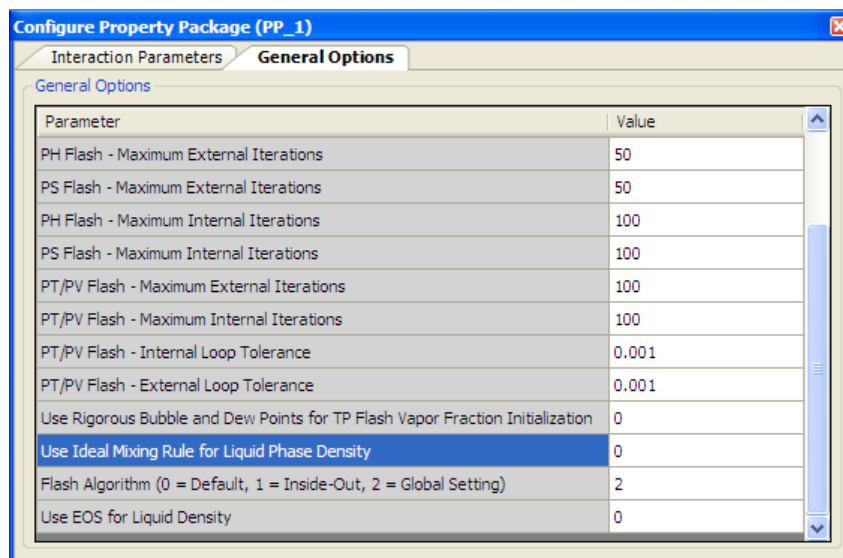


Figure 5: Property package configuration window (1).

Property Package configuration options

→ Use Ideal Mixing Rule for Liquid Phase Density

If the liquid phase has small amounts of supercritical components, the default calculation method may fail. If that is the case, change this option to 1 to force an ideal mixing rule for the

liquid density (use a molar weighted average of individual component liquid densities).

Additional Property Package configuration options Some Property Packages have extra configuration options in order to allow a deeper control of the thermodynamic calculations for the user. They are:

→ *Use EOS for Liquid Density*

This option forces the calculation of the liquid densities based on the compressibility factor given by the EOS. When disabled, DWSIM will use the Rackett correlation to calculate the liquid density. Please note that this also affects the calculation of partial molar volumes, and, consequently, component liquid volumetric fractions and flow rates.

Use 0 to disable, 1 to enable this option.

→ *Use Peneloux Volume Translation correction*

This option is available for PR and SRK Property Packages. It enables correction of EOS-calculated densities by the inclusion of a correction factor named *volume translation coefficient*. This option will be effective only if the *Use EOS for Liquid Density* option is enabled.

Use 0 to disable, 1 to enable this option.

→ *Use Experimental Liquid Density Data*

This option affects ChemSep database compounds only. It forces usage of experimental coefficients present in the database to calculate liquid phase densities.

Use 0 to disable, 1 to enable this option.

→ *Use Experimental Liquid Thermal Conductivity Data*

This option affects ChemSep database compounds only. It forces usage of experimental coefficients present in the database to calculate liquid thermal conductivities.

Use 0 to disable, 1 to enable this option.

→ *Enthalpy/Entropy/Cp calculation method (Activity Coefficient Property Packages only)*

Defines the Enthalpy, Entropy and Heat Capacity calculation model (0 = Lee-Kesler, 1 = Ideal, 2 = Excess).

→ *Ignore maximum salinity limit (IAPWS-08 Seawater Property Package only)*

Ignores the maximum supported salinity value (0.12 kg/kg) for calculations and doesn't display any warnings. Use 0 to disable, 1 to enable this option. If enabled, the calculated salinity will be send directly to the property calculation routines without further check. If disabled, the maximum value of 0.12 will be used if the calculated salinity is higher, and a warning message will be displayed in the flowsheet log window.

Flash Algorithms The Flash Algorithms in DWSIM are the components responsible for determining a particular set of phases at thermodynamic equilibrium, their amounts (and the amounts of the compounds on each phase) at the specified conditions like Temperature, Pressure, Total Enthalpy and Total Entropy. Some Flash Algorithms are capable of predicting equilibrium between one vapor and one liquid phase, while others support another co-existing liquid

and/or solid phase. As the amount of phases considered in equilibrium increases, the calculation time/complexity also increases while the results' reliability decreases. Some flash algorithms are more capable/reliable than others, depending on the mixture for which the flash calculation request is being requested. DWSIM features a selection of flash algorithms that are capable of calculating VLE, VLLE and SLE. They are:

1. **Nested Loops (VLE)**: recommended for the vast majority of VLE systems;
2. **Nested Loops (VLLE)**: recommended for systems where the liquid phase may be unstable (will split in two liquid phases with different compositions);
3. **Inside-Out (VLE/VLLE)**: recommended for petroleum simulations with many pseudo-components. The 3-phase option must be used when a second liquid phase is expected (i.e. free water);
4. **Gibbs Minimization (VLE/VLLE)**: recommended for difficult chemical systems;
5. **Nested Loops for Eutectic Solid Systems (SLE-E)**: Calculates Solid-Liquid Equilibria for eutectic systems considering the solid phase as being ideal.
6. **Nested Loops for Solid Solution Systems (SLE-SS)**: Calculates Solid-Liquid Equilibria for solid solution systems considering the solid phase as being ideal.
7. **Nested Loops (3-phase immiscible VLLE)**: For systems with an immiscible second liquid phase (VLLE). The first compound selected in the key compound list will be the immiscible one.

You can configure the added Flash Algorithms by selecting the item to configure and clicking on the "Configure" button on the "Added Flash Algorithms" section.

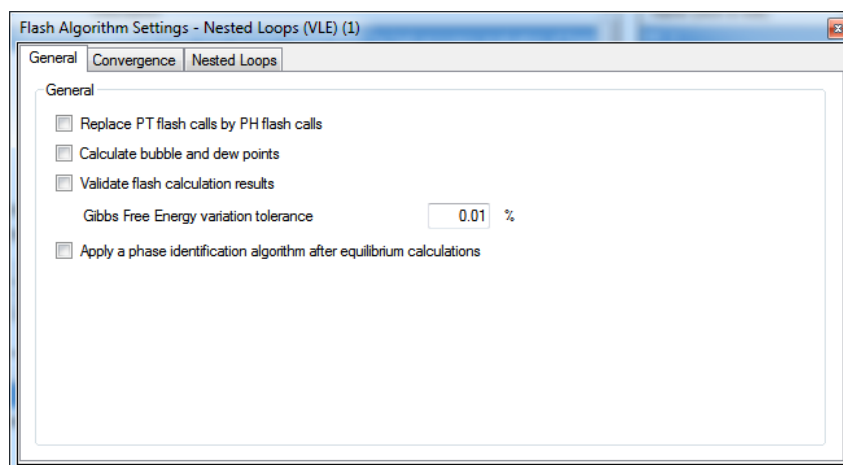


Figure 6: Property Package configuration interface.

➔ *Force Pressure-Enthalpy (PH) Flash calculations*

If enabled, all requests by unit operations for PT Flashes will be replaced by PH ones. This option must be activated if you are working with only one component (steam simulation, for example), otherwise you won't have partial vaporization/liquefaction in valves, compressors and expanders.

→ *Calculate Bubble and Dew points at stream conditions*

Check this box if you want the DWSIM to calculate bubble and dew points at conditions specified on each material stream. The calculated values will be shown only if the stream is at VLE equilibrium. The calculations are not exactly fast, so use this option with caution and only if needed.

→ *Validate Equilibrium Flash Calculation Results*

If enabled, DWSIM will check the mixture Gibbs energy before and after the equilibrium flash calculation. If the gibbs energy *increases* after the calculation (it should always *decrease* when there is a phase split), an error message will be shown and the flowsheet calculation will be aborted.

→ *Apply a Phase Identification Algorithm after Equilibrium Calculations*

Check this to apply an identification algorithm to each phase after the equilibrium calculation is finished. This can be useful for supercritical compounds which behave as liquid at high pressures and temperatures, or special mixtures which exhibit LLE behavior at low temperatures, incorrectly identified as VLE by the flash algorithms.

This procedure is enabled by default and will override the flash result regarding phase identification. For instance, the result of a flash calculation may give an all-vapor solution and, after the phase identification algorithm is applied, the phase may, in fact, behave as liquid. In this case, DWSIM will show this phase as liquid in the Material Stream property window.

Visit DWSIM's wiki for more information about the phase identification algorithm.

→ *Stability Test*

When a flash algorithm with a three-phase capability is selected, DWSIM needs to know which components are most likely to be present in a second liquid phase. You can do that by selecting the ones you think that will be in a higher amount - that is, the key components for the second liquid phase. That doesn't necessarily impose that the other, unselected components cannot be present in the second liquid phase - only the equilibrium calculation will tell you that.

The search severity setting controls how much effort DWSIM should put into searching for a second liquid phase. In the *Low* setting, only one trial phase is created with a mixture of the key components and the convergence tolerance is somewhat high. In the *High* setting, DWSIM will include additional trial phases, one for each key component and do additional checks using incipient phases' gibbs energy, with the smallest convergence tolerance value (1E-06).

Multiple Property Packages & Flash Algorithms DWSIM allows multiple Property Packages and Flash Algorithms to be added to a single simulation, which can be associated to each unit operation and material stream on an individual basis. Each property package and flash algorithm has its own settings, even if two or more packages/algorithms are of the same type.

3.2.3 Systems of Units

Three basic units systems are present in DWSIM: **SI System** (selected by default), **CGS System** and **English (Imperial) System**. The simulation's units system can be viewed/modified in the "Units System" section of the "Options" tab in the simulation configuration window (Figure 7).

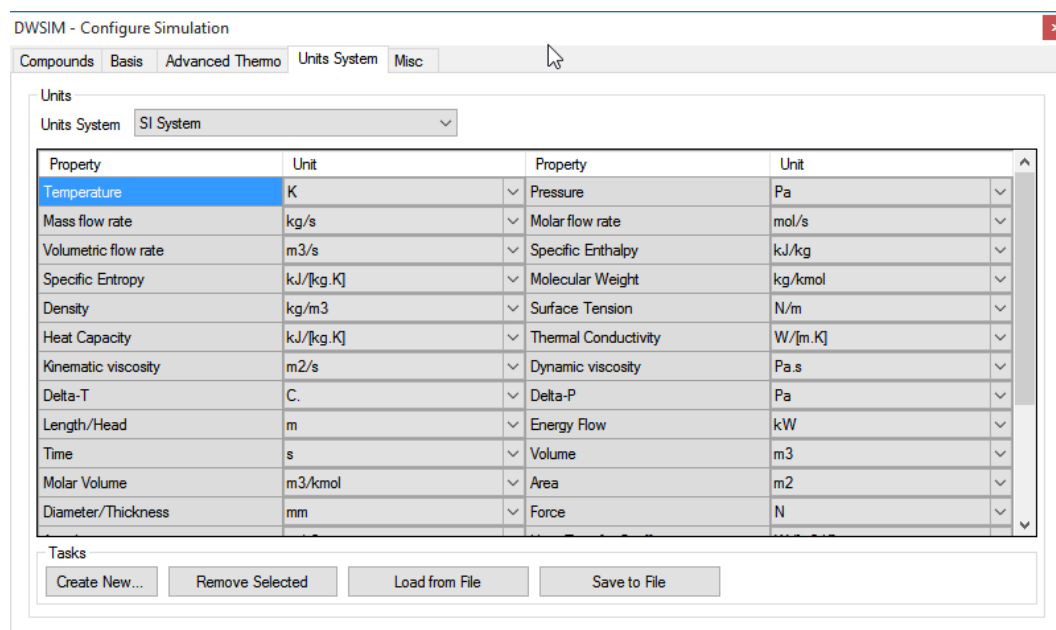


Figure 7: Units system configuration interface.

There are buttons available on this interface to create custom units systems and save/load them. It is worth remembering that the units systems can also be modified at any time during the simulation - the changes are applied immediately.

3.2.4 Miscellaneous

In the "Misc" section it is possible to define the number formatting in the simulation (Figure 8). In the "Description" group box it is possible to edit some information about the active simulation (title, author and description). You can also define a password to prevent the simulation of being opened by anyone, but this feature only works with the Compressed XML simulation file format (*.dwxmz).

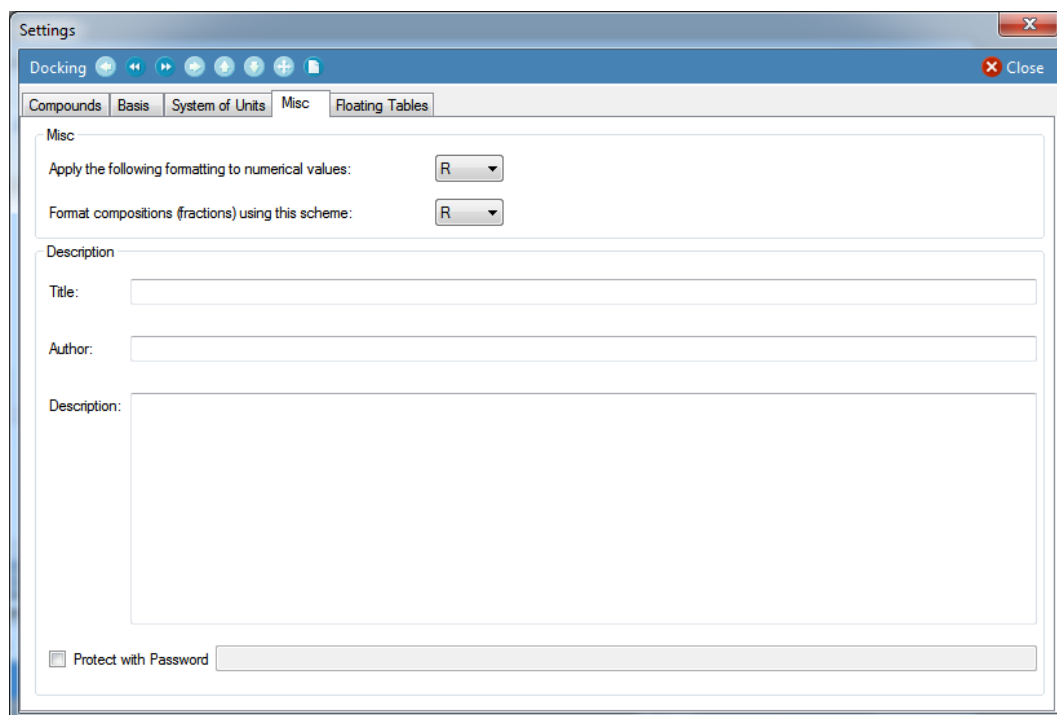


Figure 8: Misc settings interface.

3.2.5 Property Tables

In the "Property Tables" section you can define which properties are going to be shown for each object type when you hover the mouse over the objects on the flowsheet. The property list is saved in a per-simulation basis.

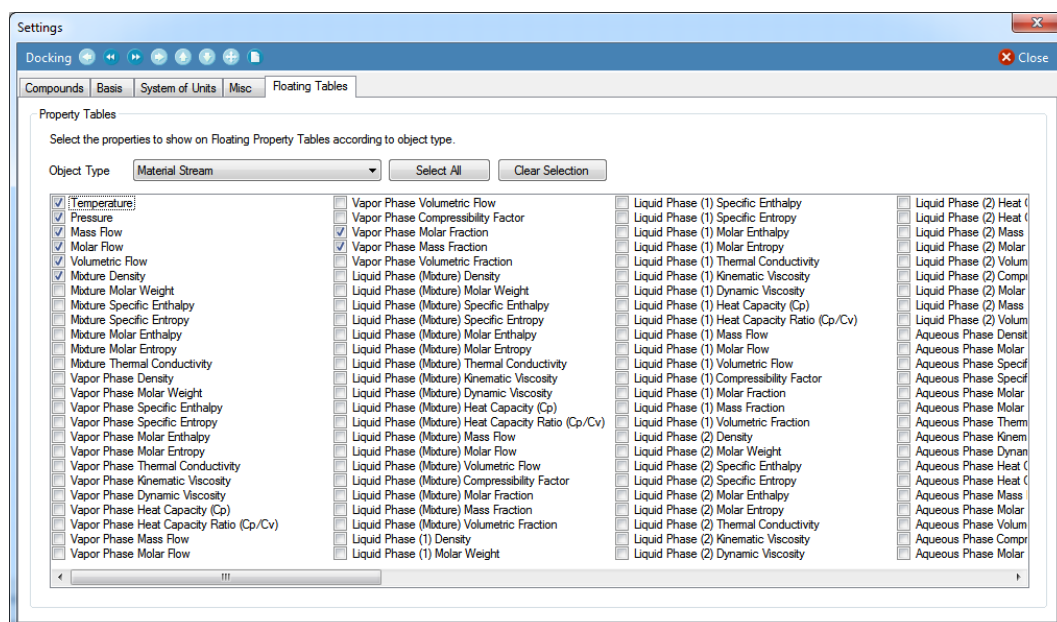


Figure 9: Property Tables settings interface.

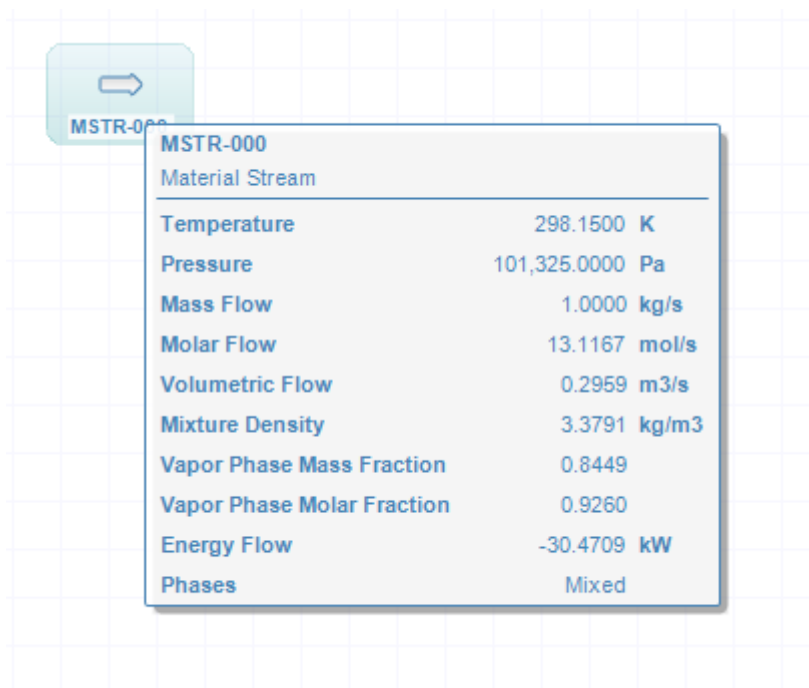


Figure 10: Selected properties on the previous image are shown on the flowsheet for the Material Streams.

3.3 Process modeling (Flowsheeting)

After configuring the simulation, the user is taken to the main simulation window (Figure 11). In this window we can highlight the following areas:

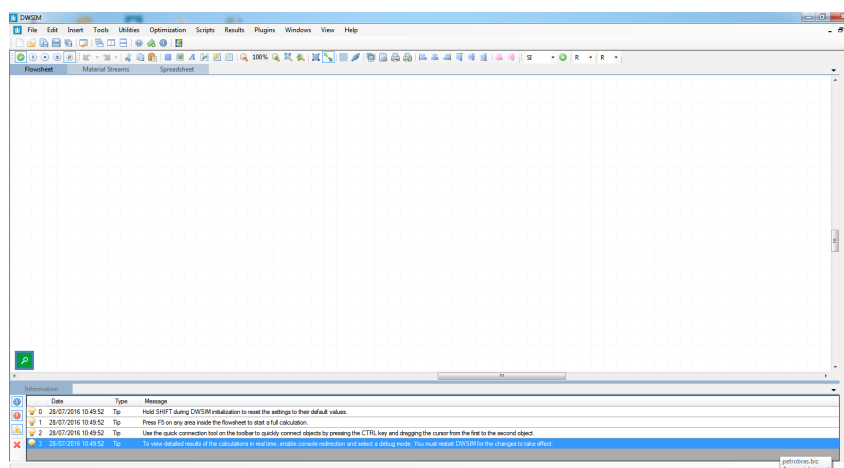


Figure 11: DWSIM simulation window.

- **Menu bars** (left-right / up-down): edit flowsheet objects, results viewer, image and text insertion, zoom controls and flowsheet printing; unit ops and streams insertion buttons;
- **Object Palette** window: shows objects which can be added by dragging them into the PFD;

- ➔ **Material Streams** window: lists the material streams in the flowsheet and their calculated properties;
- ➔ **Flowsheet** window: process flowsheet building and editing area;
- ➔ **Information** window: general information about the active simulation;
- ➔ **Spreadsheet** window: shows the spreadsheet, a utility to do math operations with data provided by the objects in the current simulation;

When running DWSIM on a Windows platform, the simulation windows can be freely repositioned, with the arrangement information being saved together with the rest of simulation data. To reposition a window, the user should click with the left mouse button in the window's top bar and drag it to the desired place. A preview of how the window will be is shown in blue (Figure 12).

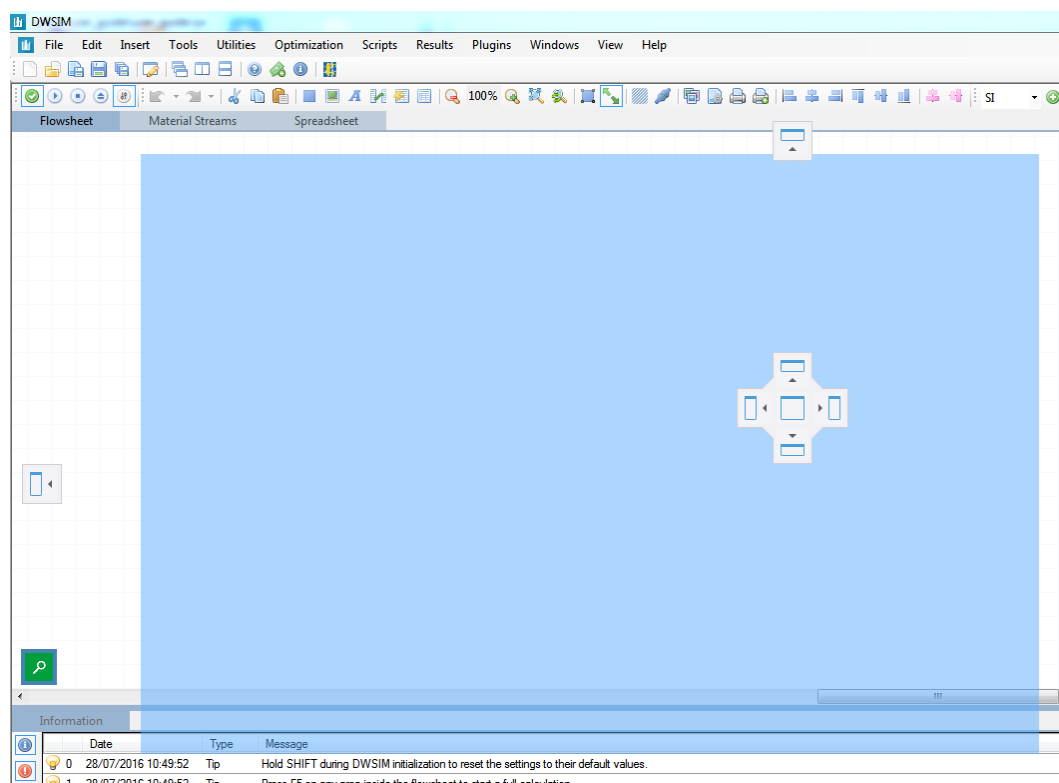


Figure 12: Window repositioning.

When running DWSIM on Mono, use the context menus (right-click with the mouse on the window caption bar) on each window to reposition/dock its contents.

3.3.1 Inserting Flowsheet Objects

To add an object to the flowsheet, you can:

- ➔ Use the **Insert > Flowsheet Object** menu item (keyboard shortcut: Ctrl+A):

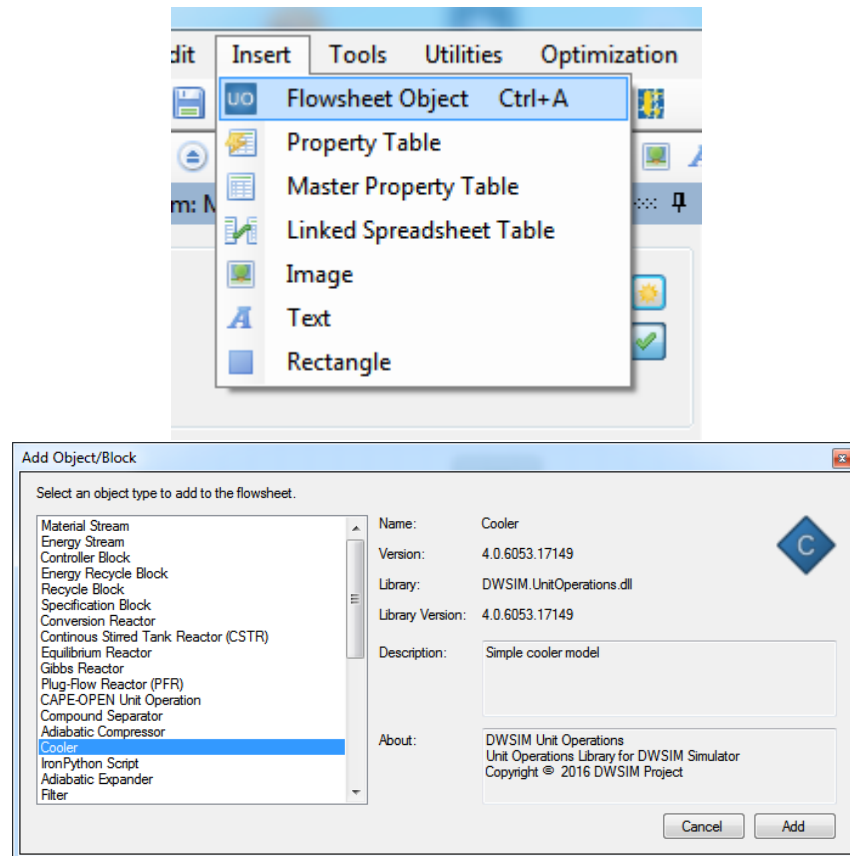


Figure 13: Inserting an object to the flowsheet.

- Drag an item from the **Object Palette** window located on the far right of the main window (auto-hidden by default):

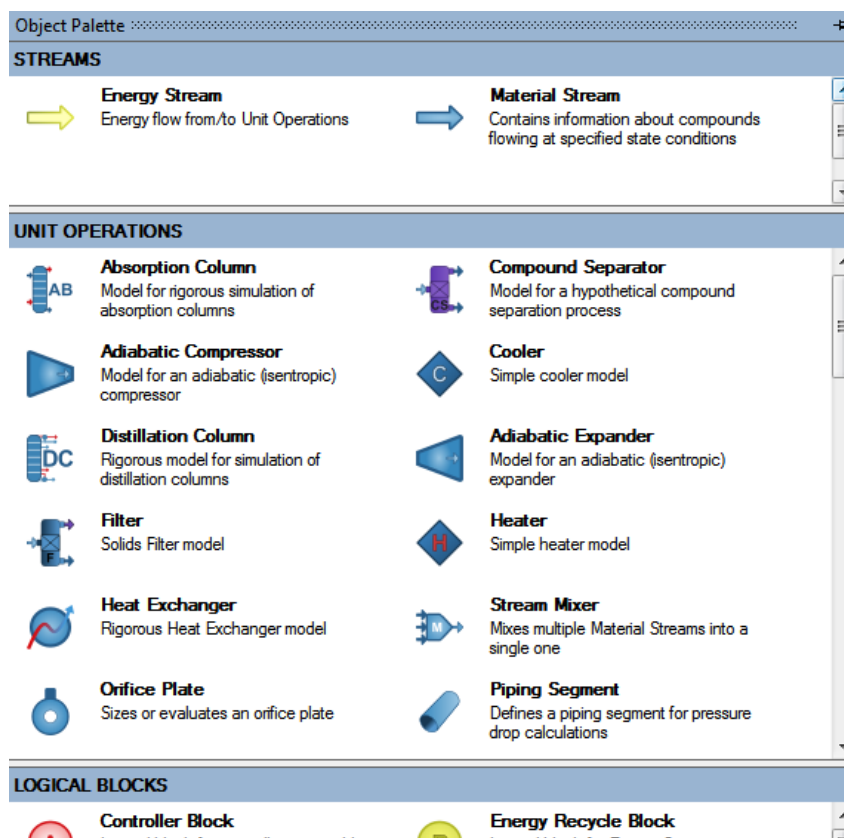


Figure 14: Inserting an object to the flowsheet by dragging from the Object Palette window.

The elements of a simulation (objects) which can be added to the flowsheet are:

- **Material Stream**: used to represent matter which enters and leaves the limits of the simulation and passes through the unit operations. The user should define their conditions and composition in order for DWSIM to calculate their properties accordingly;
- **Energy Stream**: used to represent energy which enters and leaves the limits of the simulation and passes through the unit operations;
- **Mixer**: used to mix up to three material streams into one, while executing all the mass and energy balances;
- **Splitter**: mass balance unit operation - divides a material stream into two or three other streams;
- **Valve**: works like a fixed pressure drop for the process, where the outlet material stream properties are calculated beginning from the principle that the expansion is an isenthalpic process;
- **Pipe**: simulates a fluid flow process (mono or two-phase). The pipe implementation in DWSIM provides the user with various configuration options, including heat transfer to environment or even to the soil in buried pipes. Two correlations for pressure drop calculations are available: Beggs & Brill and Lockhart & Martinelli. Both reduce to Darcy equation in the case of single-phase flow;

- **Pump**: used to provide energy to a liquid stream in the form of pressure. The process is isenthalpic, and the non-idealities are considered according to the pump efficiency, which is defined by the user;
- **Tank**: in the current version of DWSIM, the tank works like a fixed pressure drop for the process;
- **Separator Vessel**: used to separate the vapor and liquid phases of a stream into two other distinct streams;
- **Compressor**: used to provide energy to a vapor stream in the form of pressure. The ideal process is isentropic (constant entropy) and the non-idealities are considered according to the compressor efficiency, which is defined by the user;
- **Expander**: the expander is used to extract energy from a high-pressure vapor stream. The ideal process is isentropic (constant entropy) and the non-idealities are considered according to the expander efficiency, which is defined by the user;
- **Heater**: simulates a stream heating process;
- **Cooler**: simulates a stream cooling process;
- **Conversion Reactor**: simulates a reactor where conversion reactions occur;
- **Equilibrium Reactor**: simulates a reactor where equilibrium reactions occur;
- **PFR**: simulates a Plug Flow Reactor (PFR);
- **CSTR**: simulates a Continuous-Stirred Tank Reactor (CSTR);
- **Shortcut Column**: simulates a simple distillation column with approximate results using shortcut calculations;
- **Distillation Column**: simulates a distillation column using rigorous thermodynamic models;
- **Absorption Column**: simulates an absorption column using rigorous thermodynamic models;
- **Refluxed Absorber**: simulates a refluxed absorber column using rigorous thermodynamic models;
- **Reboiled Absorber**: simulates a reboiled absorber column using rigorous thermodynamic models.
- **Heat Exchanger**: simulates a countercurrent heat exchanger using rigorous thermodynamic models.
- **Orifice Plate**: model to simulate an orifice plate, used for flow metering.
- **Component Separator**: model to simulate a generic process for component separation.
- **Custom Unit Operation**: an user-defined model based on IronPython/IronRuby scripts.

- **CAPE-OPEN Unit Operation:** External CAPE-OPEN Unit Operation socket for adding CO Unit Operations in DWSIM.
- **Spreadsheet Unit Operation:** Unit Operation where the model is defined and calculated in Spreadsheet (XLS/XLSX/ODS) files.
- **Solids Separator:** model to simulate a generic process for solid compound separation.
- **Continuous Cake Filter:** continuous cake filter model for solids separation.

Additionally, the following logical operations are available in DWSIM:

- **Adjust:** used to make a variable to be equal to a user-defined value by changing the value of other (independent) variable;
- **Specification:** used to make a variable to be equal to a value that is a function of other variable, from other stream;
- **Recycle:** used to mix downstream material with upstream material in a flowsheet,
- **Energy Recycle:** used to mix downstream energy with upstream energy in a flowsheet.

Figure 15 shows a material stream added to the flowsheet by one of the method described above. It can be observed that the stream is selected and that its property editor is shown as a panel on the left part of the main window.

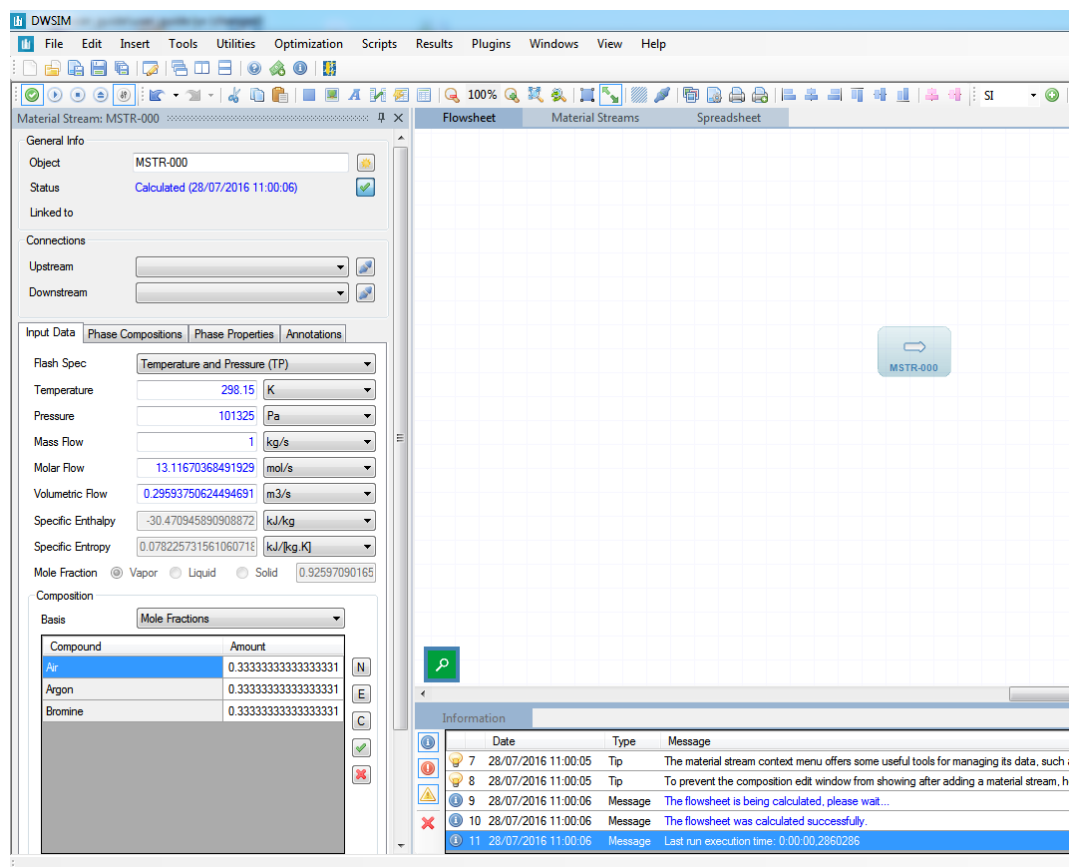


Figure 15: A material stream in the flowsheet.

Connecting objects The material streams represent mass flowing between unit operations. There are two different ways in which a material stream can be connected to a unit operation (or *vice-versa*):

- Through the context menu activated with a right mouse button click over the object (Figure 16);

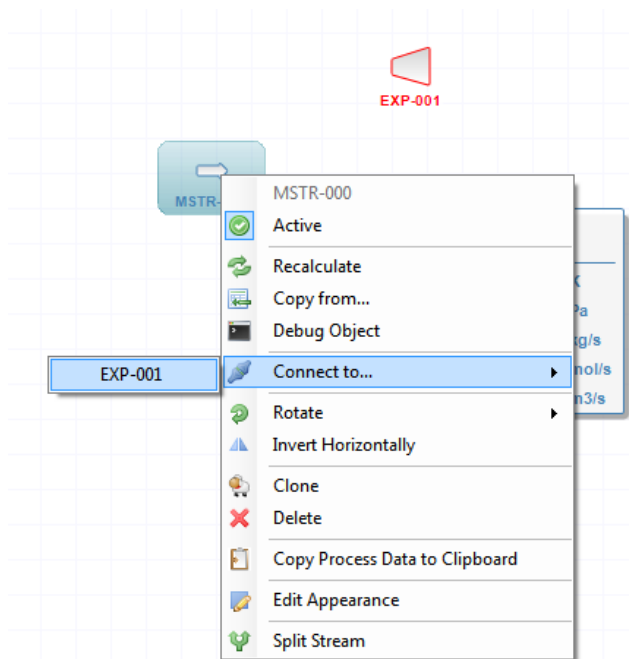


Figure 16: Selected object context menu.

- Through the property editor window - Connections section.

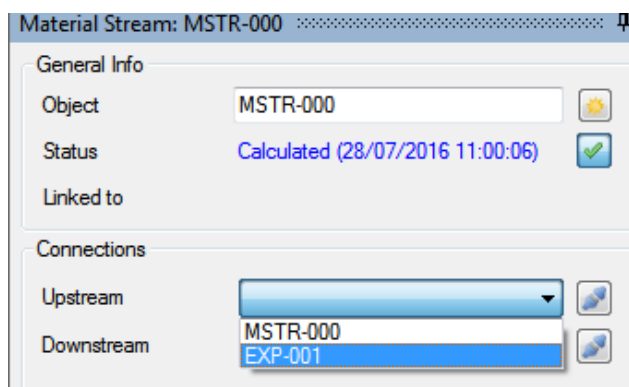


Figure 17: Connection selection menu.

- Through the "Create and Connect" buttons on the object editors. When you click on these buttons, DWSIM will automatically create and connect streams to the associated ports on the selected object.

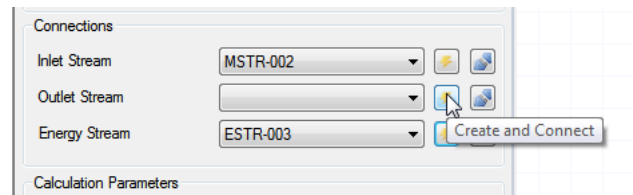


Figure 18: Create and Connect tool.

An expander system with its connections is shown on Figure 19.

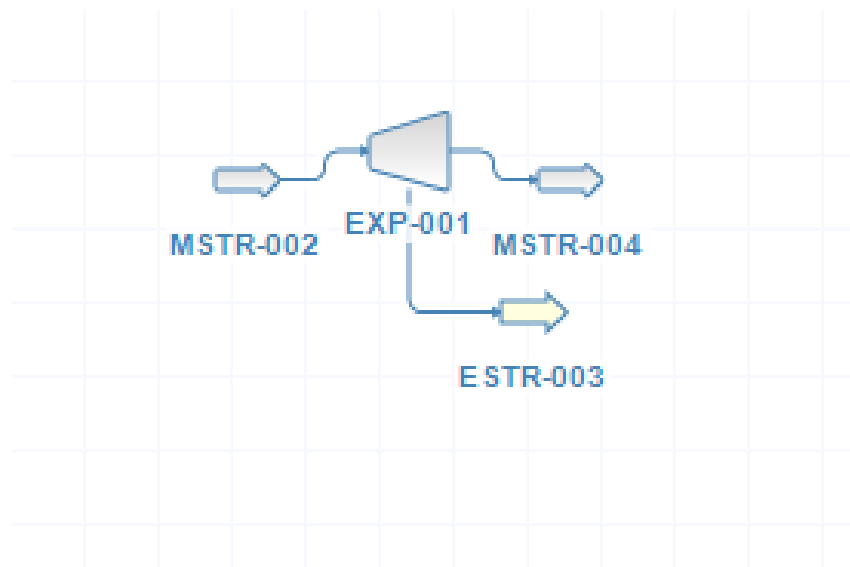


Figure 19: Expander with all connections correctly configured.

Disconnecting objects Tools to disconnect objects from each other can be found on the same locations as the connecting ones.

Removing objects from the flowsheet The selected object can be removed from the flowsheet by pressing the DEL keyboard button or by using the context menu - "Delete" item (Figure 16).

3.3.2 Process data management

Entering process data The objects' process data (temperature, pressure, flow, composition and/or other parameters) can be entered in the property editor window (Figure 20). Properties that cannot be edited (read-only) are grayed-out.

The screenshot shows the 'General Info' and 'Input Data' tabs of the DWSIM editor. The 'General Info' tab displays the object name 'in1_LNG', its status 'Calculated (01/01/0001 00:00:00)', and its connections (Upstream: empty, Downstream: HX_01). The 'Input Data' tab is active, showing various input properties for a 'Flash Spec' set to 'Temperature and Pressure (TP)'. The properties include Temperature (133.15 K), Pressure (30000000 Pa), Mass Flow (0.111111 kg/s), Molar Flow (5.53552 mol/s), Volumetric Flow (0.000236 m3/s), Specific Enthalpy (-760.606907 kJ/kg), and Specific Entropy (-5.082017 kJ/[kg.K]). The 'Mole Fraction' section shows 'Vapor' selected. The 'Composition' section shows a table of compounds and their amounts.

Compound	Amount
Carbon dioxide	0
Nitrogen	0.002038
Methane	0.833668
Ethane	0.046315
Propane	0.11483
Isobutane	0.003057
N-butane	0
Isopentane	9.3E-05
N-pentane	0

Figure 20: Viewing object properties in the editor window.

Most properties can be edited directly by typing a value in the textbox and pressing ENTER. DWSIM will then commit the new property value and trigger the calculator.

This screenshot shows the 'Input Data' tab with the 'Temperature' property selected for editing. The value '300' is entered in the textbox, and the unit 'K' is selected from the dropdown menu. The other properties (Pressure, Mass Flow) remain unchanged.

Figure 21: Direct editing of a property.

You can also use the inline units converter to convert the value of a property from the desired units to the current selected units. Type the value of the property on the textbox and

select the unit to convert from at the combobox on the right. DWSIM will then convert the value from the selected units on the combobox to the actual units of the simulation system of units.

Figure 22: Converting 50 C to the current temperature units (K).

Figure 23: Converted temperature value (323.15 K).

If all object properties were correctly defined, it will be calculated by DWSIM and its flowsheet representation will have a blue border instead of a red one, indicating that the object was calculated successfully (Figure 24).

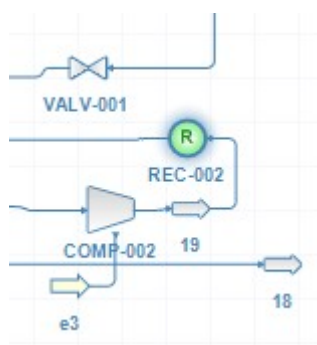


Figure 24: Calculated objects.

3.3.3 Undo/Redo actions

DWSIM supports Undo and Redo for certain actions, like:

- ➔ Changing a property of an object (model and graphic object properties)

- Connecting, disconnecting objects
- Adding and removing objects
- Adding and removing compounds
- Adding, removing and editing Property Packages

To undo or redo an action, click on the "Edit" menu item and then on the corresponding menu items (Figure 26). You can also access a list of actions to undo or redo through the arrow buttons located in the menu strip, near to the "Flowsheet" label (Figure 25).

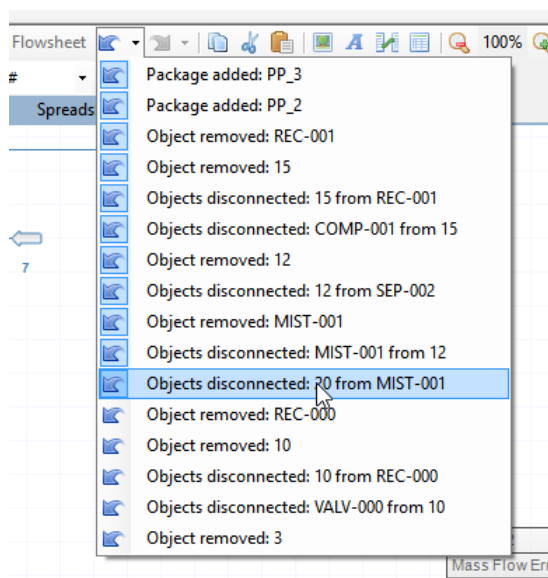


Figure 25: Undo action list.

The "Edit" menu also contains some handy tools for handling flowsheet objects, as well as simulation and application configuration menu items (Figure 26).

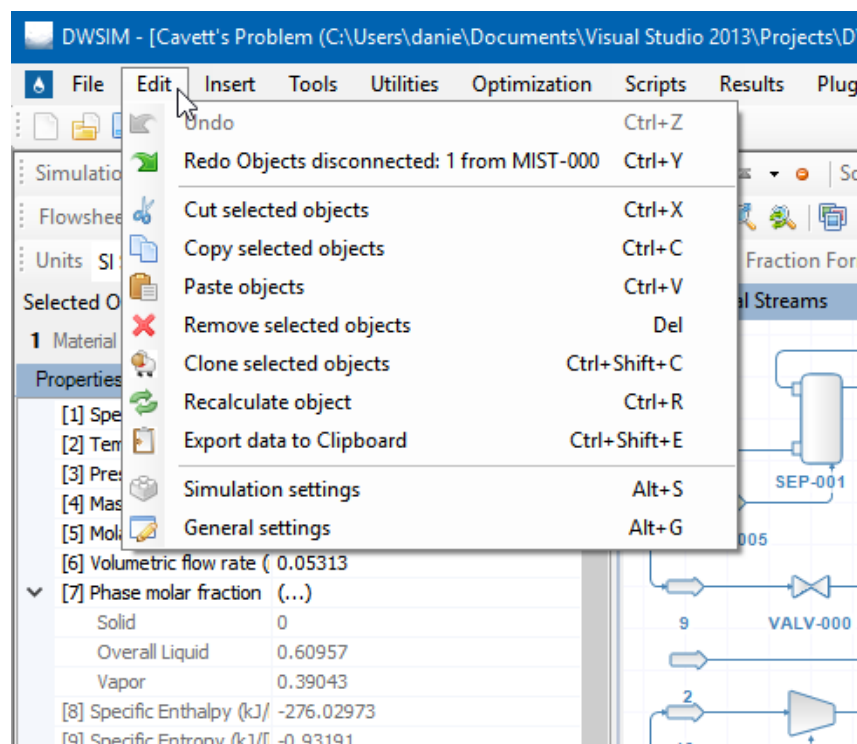


Figure 26: Edit menu.



3.3.4 Cut/Copy/Paste objects

DWSIM also supports cutting, copying and pasting flowsheet objects inside a flowsheet or between different flowsheets. When copying objects between flowsheets, DWSIM may also copy compounds and property packages from one flowsheet to another. Cut/Copy/Paste behavior is an application setting and can be set in the General Settings menu (Section 6.4).

3.3.5 Simulation

DWSIM is a sequential modular process simulator, that is, all calculations are made in a per-module basis, according to the connections between the objects. The calculator checks if an object has all of its properties defined and, if yes, passes the data for the downstream object and calculates it, repeating the process in a loop until it reaches an object that doesn't have any of its downstream connections attached to any object. This way, the entire flowsheet can be calculated as many times as necessary without having to "tell" DWSIM which object must be calculated. In fact, this is done indirectly if the user define all the properties and make all connections between objects correctly.

DWSIM's calculation starts when the user edits a property which defines an object. For example, editing a stream mass flow when its temperature, pressure and composition are already well-defined activates DWSIM's calculator.

It is possible to control DWSIM's calculator by using its button bar (Figure 27). Clicking on the  button activates or deactivates the calculator. The  button performs a full flowsheet recalculation. DWSIM's calculator is enabled by default - if it is disabled, modifying of a property is accepted, but **does not** recalculate the object nor the ones that are downstream



in the flowsheet. The  button stops the any ongoing calculation. The  button removes all items which may still be present in the calculator queue, waiting to be processed.



Figure 27: DWSIM's calculator control bar.

As DWSIM's calculator does its job, messages are added to the "Information" window. These messages tell the user if the object was calculated successfully or if there was an error while calculating it, among others (Figure 28).

		Date	Type	Message
	7	8/7/2008 11:21:53	Warning	COMP-000: No energy stream associated with the compressor.
	6	8/7/2008 11:13:59	Message	File C:\Documents and Settings\DANIEL\Desktop loaded successfully.

Figure 28: A DWSIM's calculator message.

3.3.6 Results

Results can be viewed in reports, generated (Figures 29 and 30) for printing. Report data can also be saved to ODT, ODS, XLS, TXT or XML files.

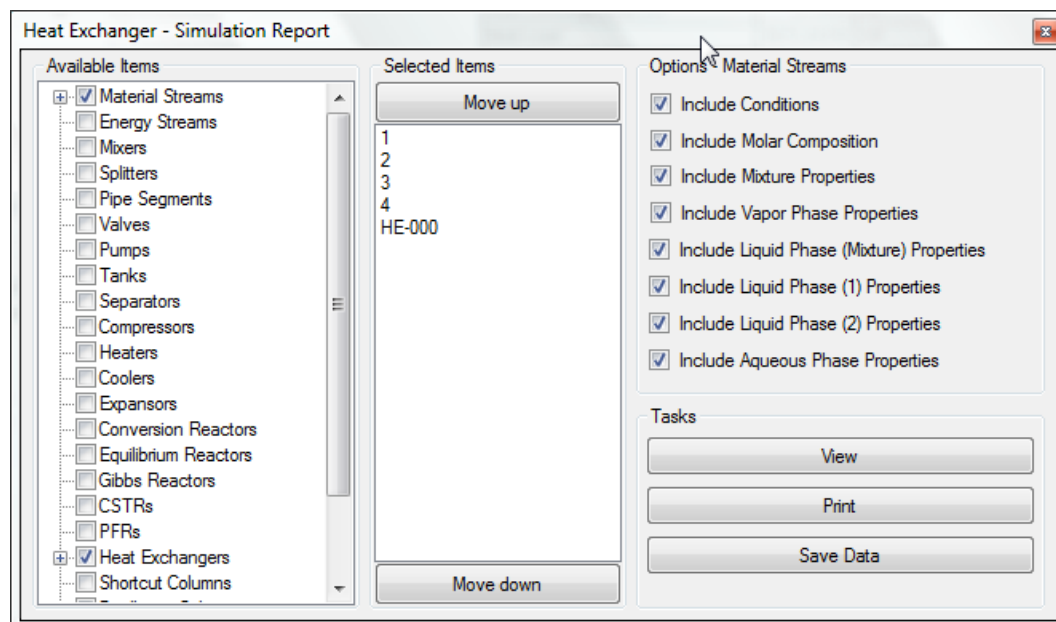


Figure 29: Results report configuration.

Relatório da Simulação
DWSIM v1.2

Detalhes
Título: Teste 1
Comentários: Simulação-teste para o Guia do Usuário do DWSIM

Corrente de Matéria: MAT-000

	Mistura	Vapor	Líquido
Definições			
Temperatura (K)	300,0	-	-
Pressão (Pa)	101325,0	-	-
Vazão mássica (kg/s)	25,0	25,0	0,0
Vazão molar (mol/s)	1084,29293	1084,29293	0,0
Vazão volumétrica (m3/s)	26,69078	26,69078	0,0
Composição em Frações Molares			
Metano (C1)	0,5	0,5	0
Etano (C2)	0,5	0,5	0
Propriedades			
Fração Molar (-)	0,0	1,0	0,0
Fração Mássica (-)	0,0	1,0	0,0
Entalpia Específica (kJ/kg)	2,02486	2,02486	0,0
Entropia Específica (kJ/(kg.K))	0,28737	0,28737	0,0
Massa Molar (kg/kmol)	23,0565	23,0565	0,0
Massa Específica (kg/m3)	0,93665	0,93665	0,0

Figure 30: Results report.

3.4 Sensitivity Analysis

You can use the Sensitivity Analysis Utility in order to study the influence of up to 2 variables into other dependent flowsheet variables. The changes in variables are defined by a value range and a number of equally spaced points within this range. For example, you can analyze the influence of temperature and pressure in the enthalpy of a mixture, from 200 to 400 K and from 100 to 1000 kPa, nine points for temperature and 5 points for pressure, totaling 45 points on which the enthalpy will be calculated at different temperatures and pressures. This also means that the flowsheet will be recalculated 45 times (!), so be careful with the number of points you choose as the calculation time can be prohibitive.

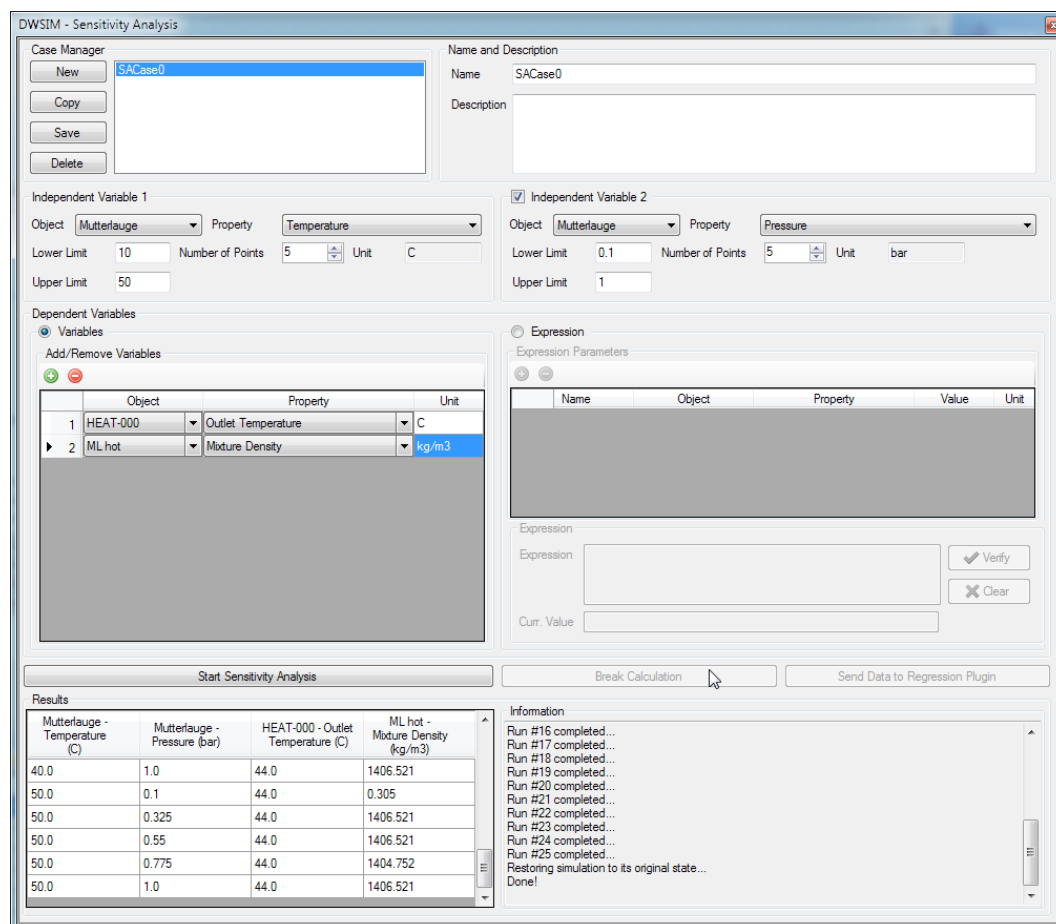


Figure 31: Sensitivity Analysis Utility (1).

The sensitivity analysis utility is based on case studies. In a single simulation one can define a number of cases, each one with its own variables, ranges and results. These cases will be saved together with the simulation, and cannot be exported to other ones. The results are shown in a table, so the data can be copied and pasted into another specialized data analysis software or sent directly to the data regression plugin.

3.5 Flowsheet Optimization

The new Optimizer in DWSIM handles single and multivariate optimization problems with or without bound constraints. The objective function can be either a variable in the flowsheet or an expression as a function of as many variables as you need.

The interface is very similar to Sensitivity Analysis's one. One can define a number of cases, each one with its own variables, ranges and results. These cases will be saved together with the current simulation, and cannot be exported to other simulations.

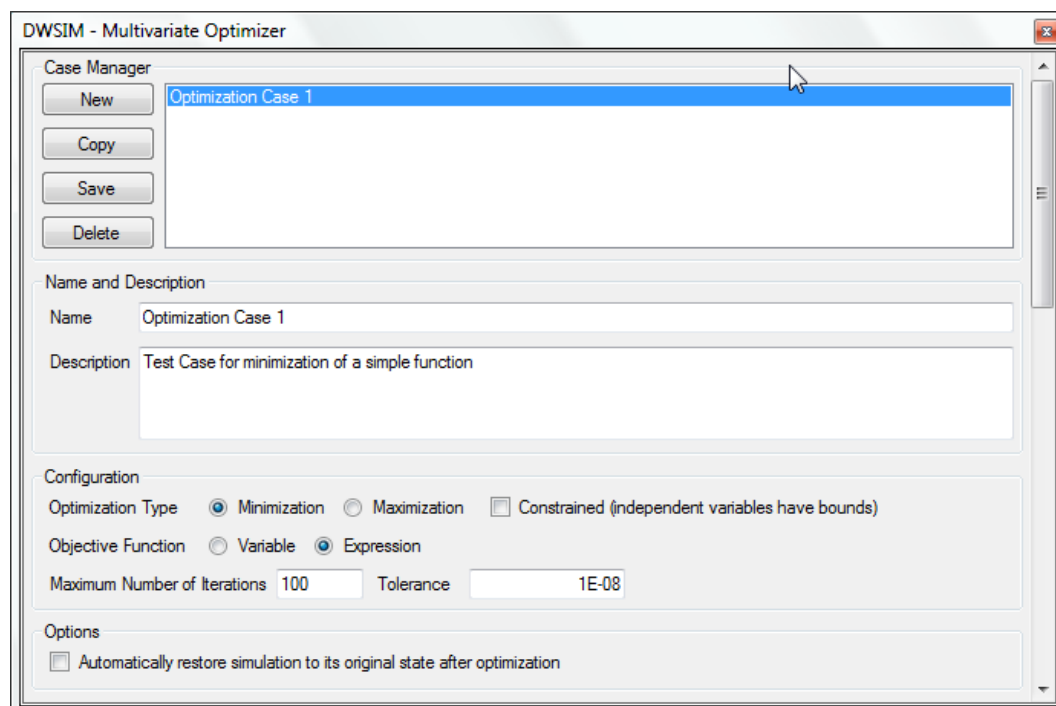


Figure 32: Multivariate Optimization Utility (1).

There are some options to choose from in DWSIM's Multivariate Optimizer. It is possible to select the type of the optimization (minimization or maximization of the objective function), choose if the independent variables will have lower and/or upper bounds and if the objective function will be a flowsheet variable or an expression based on flowsheet variables. One can also define a maximum number for the iterations and a tolerance for the variation of the calculated value for the objective function - if the variation is less than the defined value, the flowsheet is considered optimized and the process stops. There is also an option to choose if the flowsheet will be returned to its original state after optimization, so the results will be shown only in the current window, and the flowsheet initial configuration will remain intact.

In order to define variables to be used in the optimization process, a variable can be added by clicking on the "+" button. With the variable row added to the list, one chooses an object, then the desired property and the type of variable (IND for independent, AUX for auxiliary or DEP for dependent variables). If necessary, one can define a lower and/or upper limit for the IND variables, according to the current unit system. The variable name is the one which will be used in the expression.

DWSIM only considers bounds for independent variables. Also, if the objective function is a DEP variable, and you defined multiple DEP variables, only the first will be used. AUX variables are used in the context of an expression only. To remove a variable, a row must be selected by clicking at the row header before pressing the "-" button.

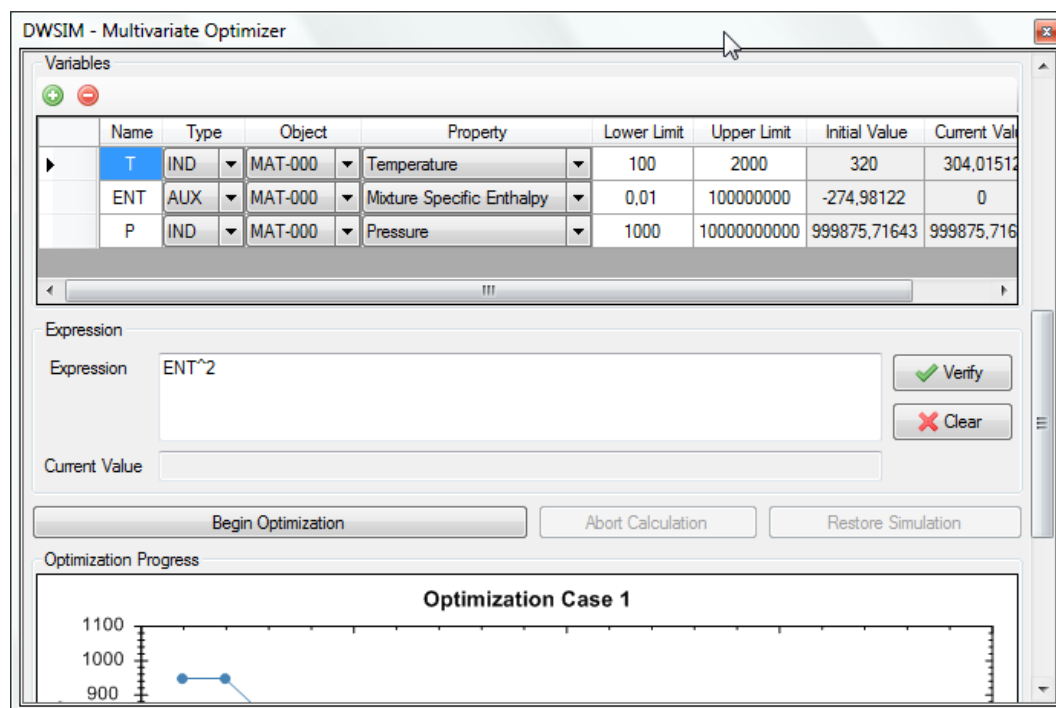


Figure 33: Multivariate Optimization Utility (2).

With all the variables defined and the case configured, the optimization can be carried out by clicking on the appropriate button - the button will become disabled. After some time, if the optimization converges, the button will become active again, indicating that the optimization process is over.

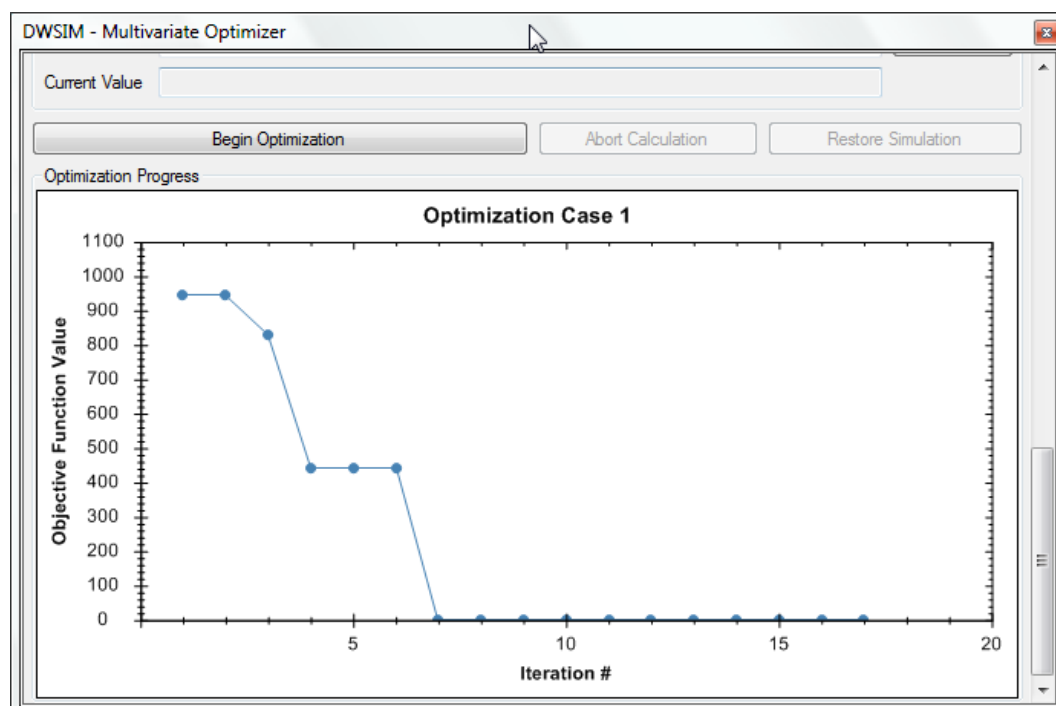


Figure 34: Multivariate Optimization Utility (3).

3.6 Utilities

DWSIM includes some utilities which provides the user with more information about the process being simulated.

Utilities can be added and attached to Flowsheet objects (**Utilities > Add Utility** menu item). After being attached, they will be saved together with simulation data and restored upon reopening. Some data from the attached utilities will be available to be displayed on property tables and used on sensitivity analysis and optimization studies.

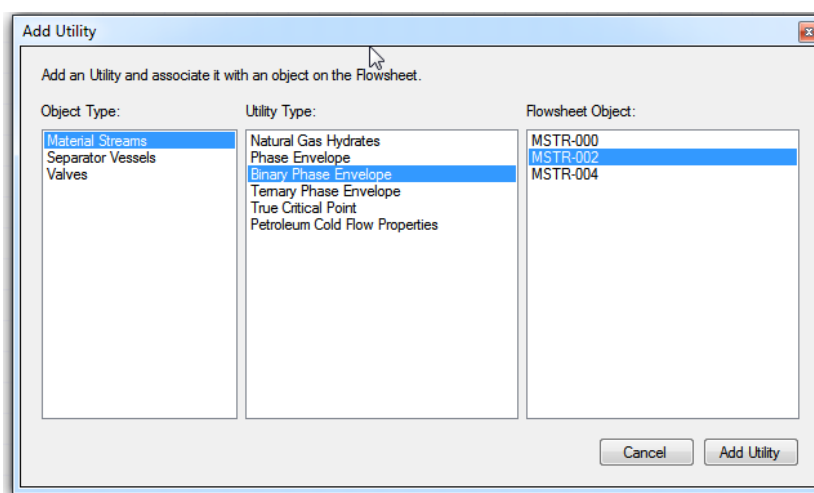


Figure 35: Attaching Utilities through the "Add Utility" window.

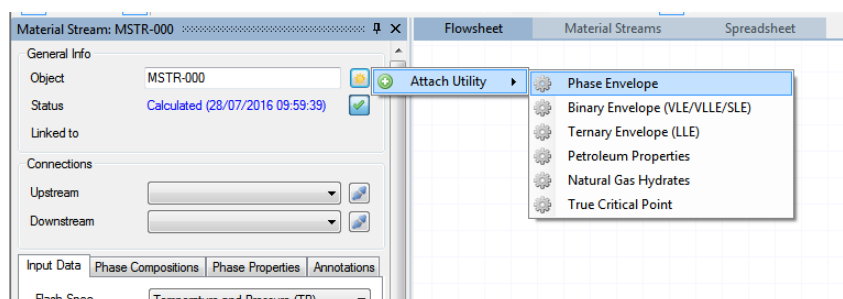


Figure 36: Attaching Utilities through the object editors.

Added/Attached Utilities will be visible on the context menu located on the object editors, on the right of the Object's Name textbox.

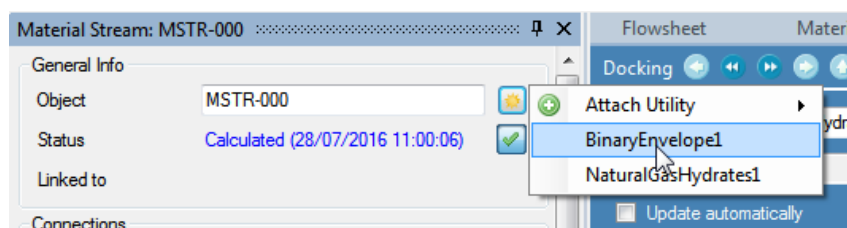
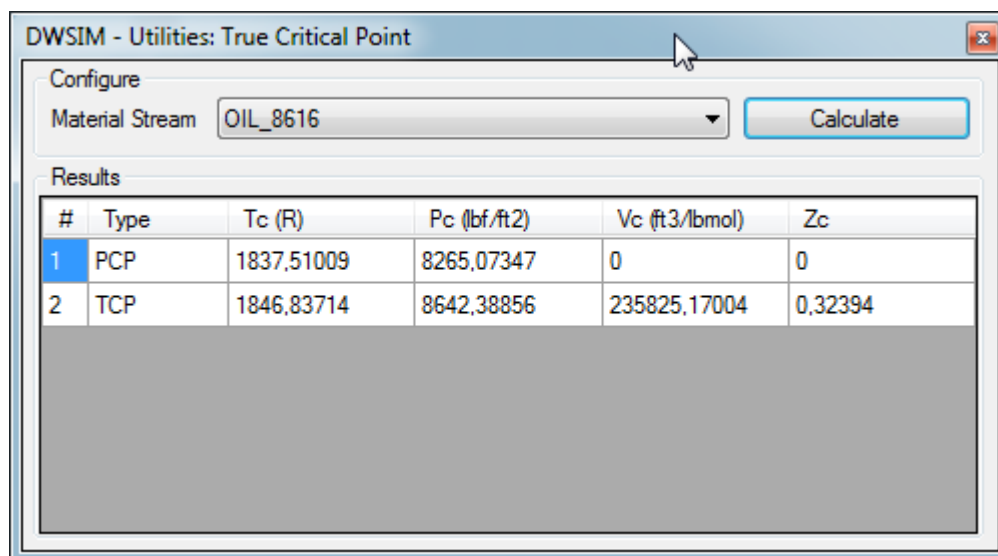


Figure 37: Accessing attached Utilities.

→ **True Critical Point** - utility to calculate the true critical point of a mixture (Figure 38).



DWSIM - Utilities: True Critical Point

Configure

Material Stream: OIL_8616

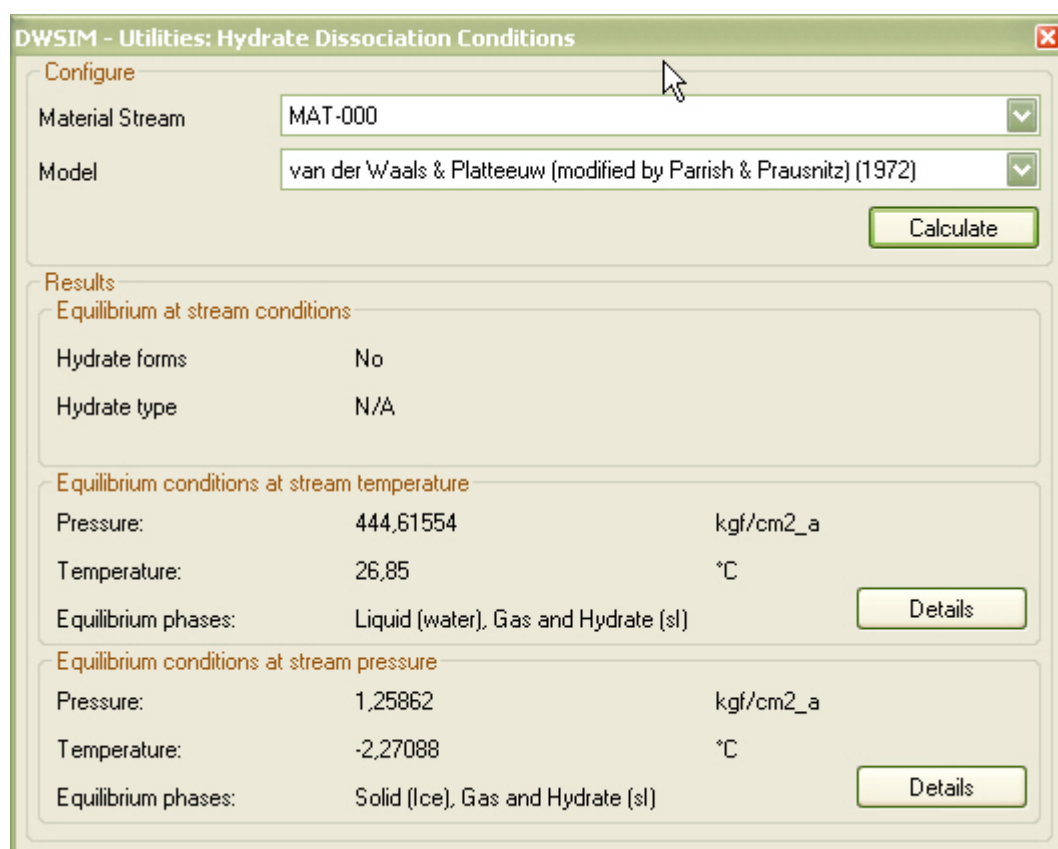
Calculate

Results

#	Type	Tc (R)	Pc (lbf/ft2)	Vc (ft3/lbmol)	Zc
1	PCP	1837,51009	8265,07347	0	0
2	TCP	1846,83714	8642,38856	235825,17004	0,32394

Figure 38: Utilities - True Critical Point.

→ **Hydrate Equilibrium/Dissociation Utility** - calculation of the equilibrium conditions for natural gas hydrates (Figure 39);



DWSIM - Utilities: Hydrate Dissociation Conditions

Configure

Material Stream: MAT-000

Model: van der Waals & Platteeuw (modified by Parrish & Prausnitz) (1972)

Calculate

Results

Equilibrium at stream conditions

Hydrate forms: No

Hydrate type: N/A

Equilibrium conditions at stream temperature

Pressure: 444,61554 kgf/cm2_a

Temperature: 26,85 °C

Equilibrium phases: Liquid (water), Gas and Hydrate (sl) Details

Equilibrium conditions at stream pressure

Pressure: 1,25862 kgf/cm2_a

Temperature: -2,27088 °C

Equilibrium phases: Solid (Ice), Gas and Hydrate (sl) Details

Figure 39: Utilities - Hydrate Calculations.

→ **Phase Envelope** - Material stream phase equilibria envelope calculation (Figure 40);

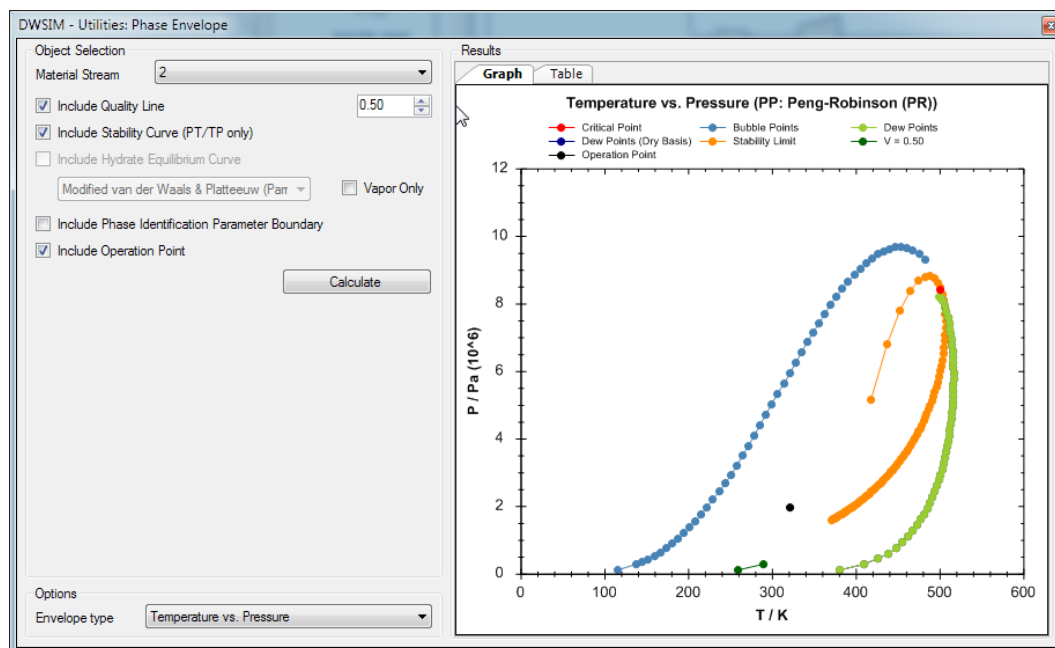


Figure 40: Utilities - Phase Envelope.

→ **Binary Envelope** - special envelopes for binary mixtures (Figure 41).

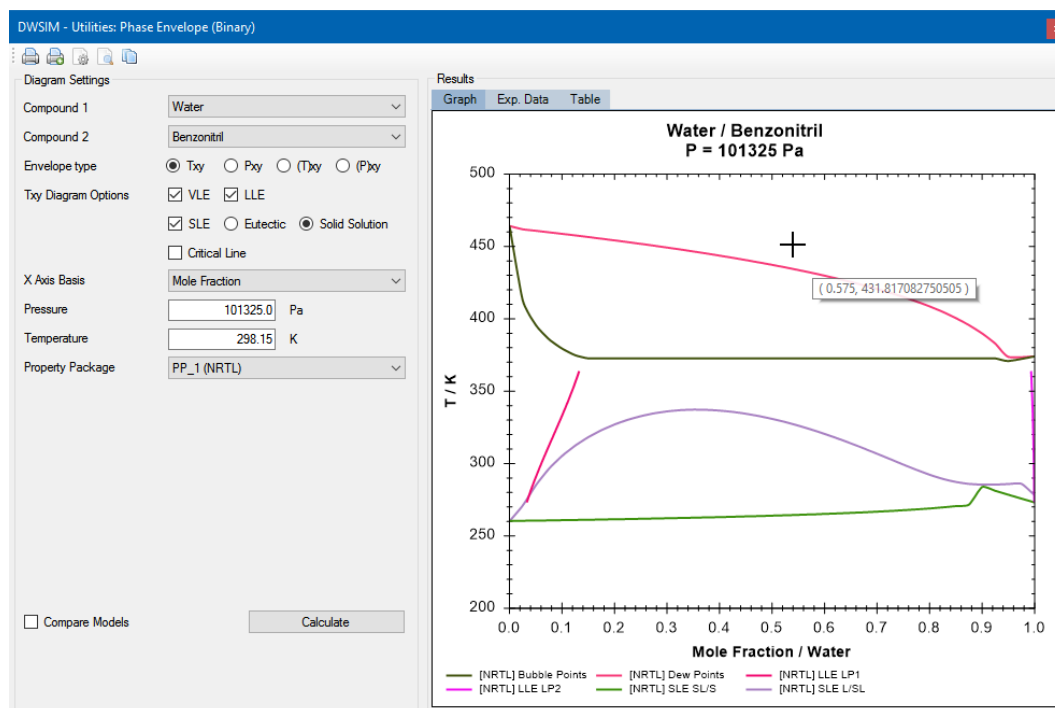


Figure 41: Utilities - Binary Envelope.

→ **Petroleum Cold Flow Properties** - special properties of petroleum fractions, like cetane index, flash point, refraction index, etc. (Figure 42).

Property	Value	Unit
True Vapor Pressure @ 37,8 °C	1044,81154	Pa
Reid Vapor Pressure @ 37,8 °C	526,7964	Pa
Viscosity @ 37,8 °C	0,00067	Pa.s
Viscosity @ 98,9 °C	0,0006	Pa.s
Flash Point (Closed Cup)	323,27997	K
Pour Point	229,55037	K
Cloud Point	203,38739	K
Freezing Point	210,55127	K
Refraction Index @ 20 °C	1,45351	
Cetane Index	37,09667	

Figure 42: Utilities - Petroleum Cold Flow Properties.

Utilities calculate their properties for one object only, which is selected inside their own windows. In the majority of cases, this object must be calculated in order to be available for selection in the utility window.



Please view DWSIM's Technical Manual for more details about the models and methods used by the Utilities.

3.7 Chemical Reactions

DWSIM classifies chemical reactions in three different types: Conversion, where the conversion of a reagent can be specified as a function of temperature; Equilibrium, where the reaction is characterized by an equilibrium constant K, and Kinetic, where the reaction is led by a velocity expression which is a function of concentration of reagents and/or products.



Please view DWSIM's Technical Manual and Equipment and Utilities Guide for more details about chemical reactions and reactors, respectively.

Chemical reactions in DWSIM are managed through the **Chemical Reactions Manager** (**Tools > Reactions Manager** menu item) (Figure 43):

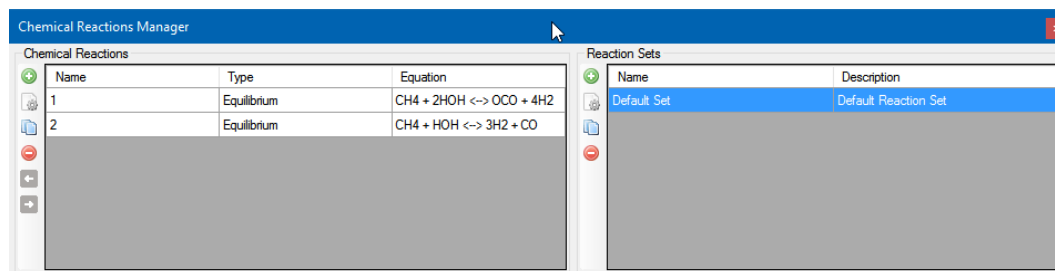


Figure 43: Chemical Reactions Manager.

The user can define various reactions which are grouped in *Reaction Sets*. These reaction sets list all chemical reactions, and the user must activate only those he wants to become available for one or more reactors (since the reactor's parameter is the **reaction set** and not the chemical reactions themselves). In the reaction set configuration window it is also possible to define the reaction ordering. Equal indexes define parallel reactions (Figure 44):

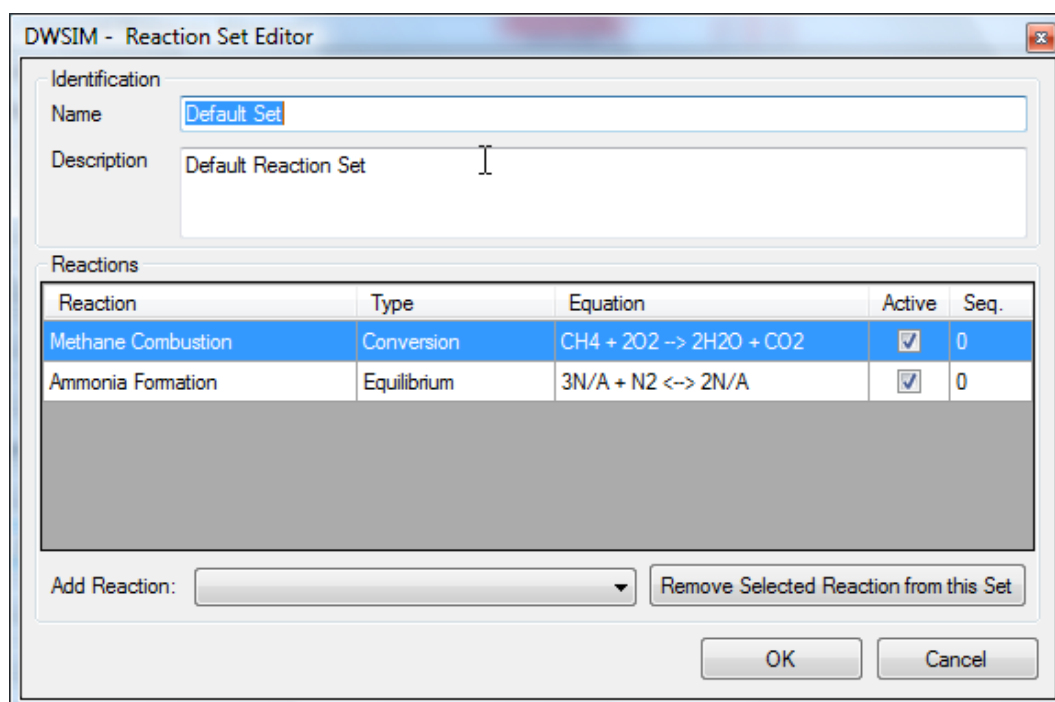


Figure 44: Reaction Set editor.

When the reactions and their respective reaction sets are correctly defined, the last will be available for selection in the property window of a reactor in the simulation. The reactor will then look for active reactions inside the selected set (Figure 45):

Object	RC-000	
Type	Reator de Conversão	
Status	Calculated	
<div> <div>Properties</div> <div>Format Object</div> <div>▼</div> </div>		
<div> <div>1. Connections</div> <div> <div>Input Stream</div> <div>1</div> </div> <div> <div>Vapor outlet</div> <div>2</div> </div> <div> <div>Liquid outlet</div> <div>3</div> </div> <div> <div>Energy Stream</div> <div>e1</div> </div> </div>		
<div> <div>2. Parameters of calculation</div> <div> <div>Reaction Set</div> <div>Default Set</div> </div> <div> <div>Operation Mode</div> <div>Isothermic</div> </div> <div> <div>Pressure drop (Pa)</div> <div>0,0</div> </div> </div>		
<div> <div>3. Results</div> <div> <div>Delta T (K)</div> <div>0,0</div> </div> <div> <div>Heat Load (kW)</div> <div>-3841071,32356</div> </div> </div>		
<div> <div>Reactions and Conversions (%)</div> <div>(...)</div> <div> <div>Methane Combustion</div> <div>90,3</div> </div> </div>		
<div> <div>Property Package</div> </div>		
<div> <div>Reactions and Conversions (%)</div> <div>Show active reactions and their conversions, in percent (%).</div> </div>		

Figure 45: Reaction set in a reactor's property window.

3.8 Characterization of Petroleum Fractions

DWSIM provides two tools for characterization of petroleum fractions ("Simulation Settings" > "Tools" > "Petroleum Characterization"). One of them characterizes C7+ fractions from bulk properties (Figure 46). The other characterizes the oil from an ASTM or TBP distillation curve (Figure 47).

In both tools, the characterization is done through the creation of various components with different boiling points (pseudocomponents) which together represent the assay as a whole.

- **Characterization from bulk properties** The method itself requires a minimum of information to generate the pseudocomponents, though the more data the user provides, the better

will be the results (Figure 46). It is recommended that the user provides the specific gravity of the C7+ fraction at least. Viscosity data is also very important.

DWSIM - Bulk C7+ Petroleum Characterization

General Options

Input Data

Molecular Weight (MW) kg/kmol

Specific Gravity (d60/60) 0,87 [adimensional]

Avg. Boiling Temperature K

Viscosity data (leave blank to calculate)

T1 37,78 °C Visc 1 cSt

T2 98,89 °C Visc 2 cSt

Pseudocomponents 10

Properties

Name	Molar Fraction	NBP (K)	SG	MW (kg/kmol)	Tc (K)	Pc (Pa)	Ac. Factor
PSE_6491_2	0,1	430,57251	0,77497	129,94632	618,25856	2530230,32513	0,37296
PSE_6491_3	0,1	500,9978	0,81593	176,79062	690,99271	2016624,06851	0,47662
PSE_6491_4	0,1	551,17542	0,84061	217,03795	740,01856	1724984,07188	0,55751
PSE_6491_5	0,1	597,69994	0,86098	260,64929	783,70248	1499466,04091	0,63883
PSE_6491_6	0,1	644,70208	0,87962	312,24068	826,31569	1307894,75544	0,72834
PSE_6491_7	0,1	695,01427	0,89786	377,99601	870,44868	1136179,01316	0,83402
PSE_6491_8	0,1	751,84282	0,91681	469,53874	918,71932	976137,35063	0,96845
PSE_6491_9	0,1	820,24094	0,93797	614,91426	975,0268	821876,09522	1,15726

Stream Name OIL_4565

Figure 46: C7+ petroleum fraction characterization utility.

- **Characterization from distillation curves** This tool gets data from an ASTM or TBP distillation curve to generate pseudocomponents. It is also possible to include viscosity, molecular weight and specific gravity curves to enhance the characterization.

The interface has a wizard-like style, with various customization options (Figure 47):

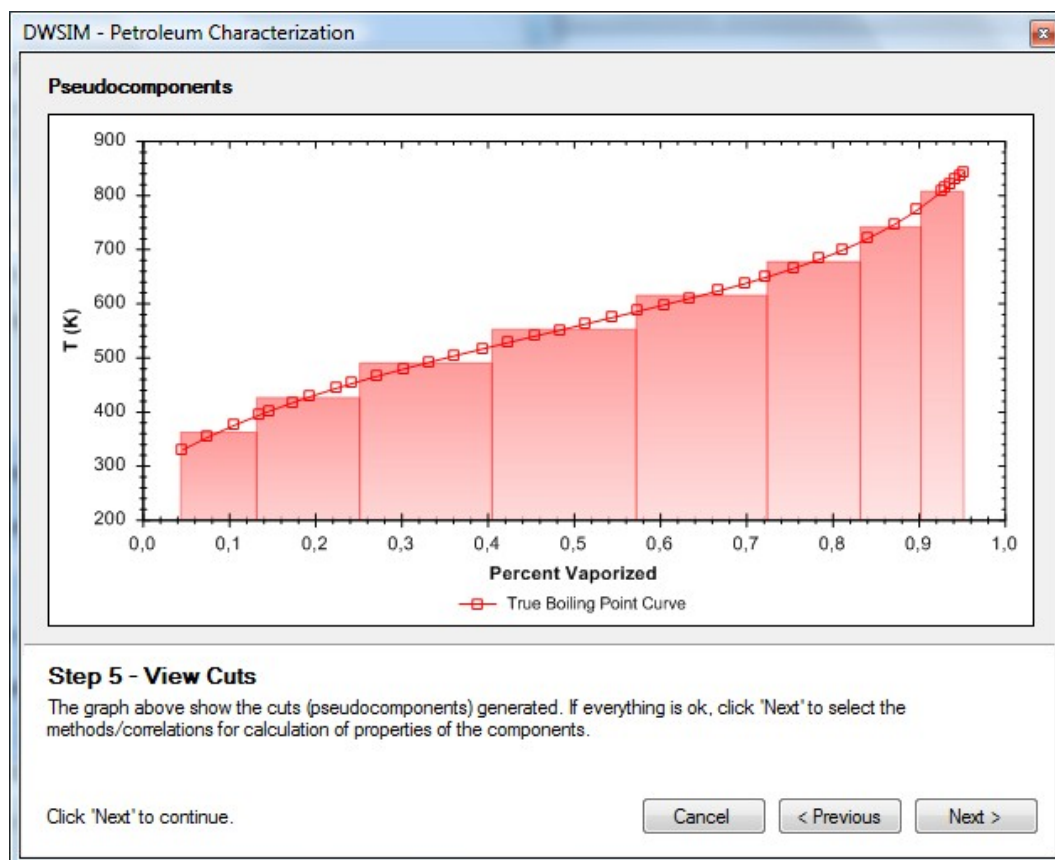


Figure 47: Characterizing petroleum from distillation curves.

After the pseudocomponents are created, a material stream with a defined composition is also created, which represents the characterized petroleum fraction.



The hypo and pseudocomponents are available for use only in the simulation in which they were generated, even if there is more than one opened simulation in DWSIM. Nevertheless, the user can export these components to a file and import them into another simulation.

4 Compound Creator

4.1 Component/Compound Databases

4.1.1 Databases/Datasets

The compounds available for use in simulations are grouped in *databases/datasets*. DWSIM comes with one database with the most common compounds used in the petroleum industry plus some alcohols and inert gases. DWSIM also includes a database with more than 400 compounds from *ChemSep™ LITE*.

User-Defined Databases in DWSIM can be managed through a window which can be opened from the Main Menu > Settings > General Settings (Figure 48):

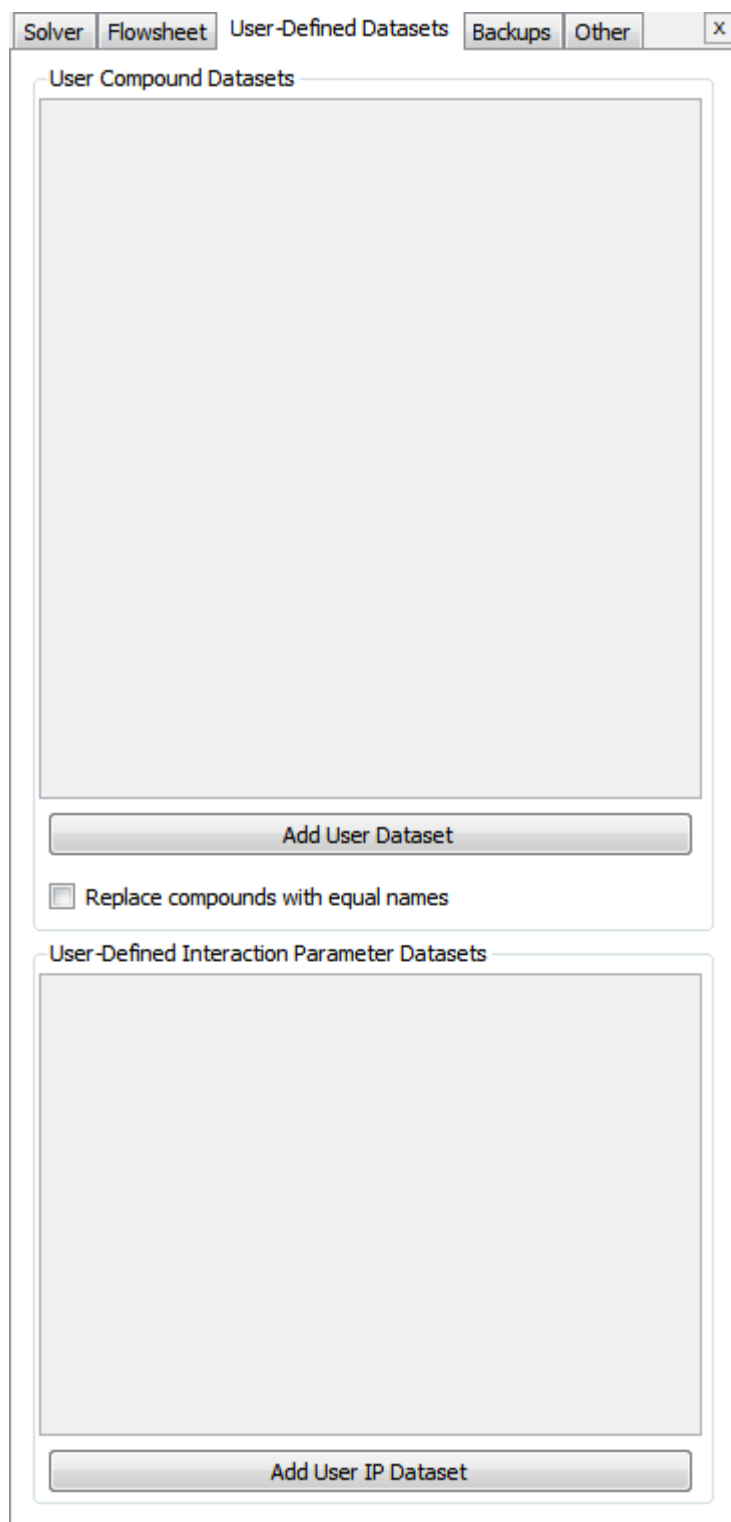


Figure 48: Database manager.

On this window the user can add and/or remove modified databases (created from the

Components tab in the **Simulation Settings** window).

User databases can be created and managed through the **Compound Creator Utility**, which unifies the Quick Component Creator and Hypothetical Component utilities into a single, easy-to-use tool.

4.2 About the Compound Creator Utility

The Compound Creator puts together the features found in the Hypothetical and Quick Compound Creator, allowing the user to save his compounds into a database that can be loaded later globally in DWSIM, that is, your compounds can be used in all simulations, not only in the one that they were created. The Compound Creator also allows you to save and load your compound creation study/case for later use.

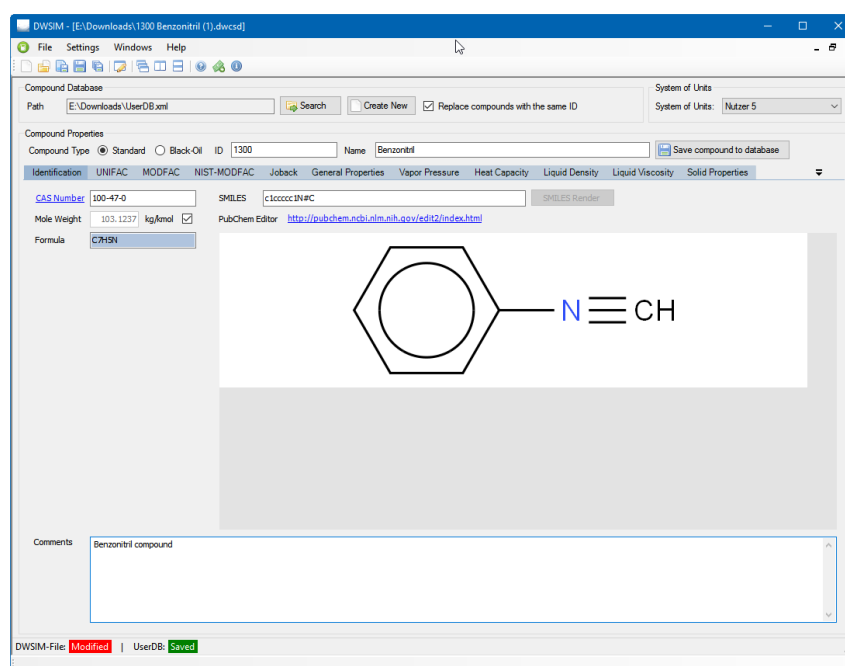


Figure 49: Compound Creator Utility.

5 Data Regression

DWSIM can regress experimental binary VLE/LLE/SLE data in order to calculate interaction parameters for a variety of thermodynamic models. This way you can calculate interaction parameters for compounds in DWSIM and ChemSep databases that do not have them or calculate parameters between known compounds and one that you just created using the Compound Creator utility.

5.1 About the Data Regression Utility

The Data Regression Utility supports regression of experimental binary data for determination of interaction parameters for the following models:

→ PC-SAFT

- Peng-Robinson
- Peng-Robinson-Stryjek-Vera 2
- Soave-Redlich-Kwong
- UNIQUAC
- NRTL
- Lee-Kesler-Plöcker

The following data sets are supported:

- VLE Temperature and molar fractions (T_{xy})
- VLE Pressure and molar fractions (P_{xy})
- VLE Temperature, Pressure and molar fractions (TP_{xy})
- LLE Temperature and molar fractions (T_{xx})
- LLE Pressure and molar fractions (P_{xx})
- LLE Temperature, Pressure and molar fractions (TP_{xx})
- SLE Temperatures and mole fractions (TT_x)

The Data Regression Utility also possesses some handy additional features like:

- Calculation of initial values for the binaries using UNIFAC/MODFAC structure information
- Calculation of missing experimental data using known models/binaries for determination of parameters for other models
- Optimization method selection
- Objective Function selection (Least Squares of temperature/pressure plus vapor fractions)

The Data Regression Utility also supports loading and saving of a regression study/case for later use.

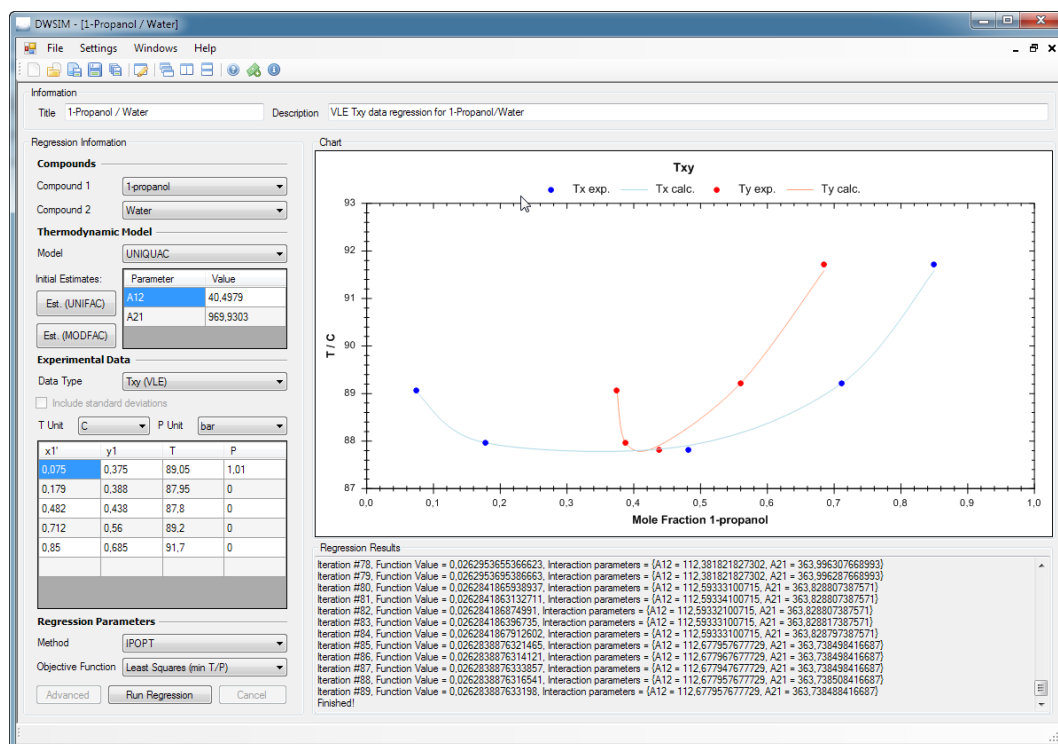


Figure 50: Data Regression Utility.

6 General Settings

The application settings can be accessed through the **Edit > General Settings** menu item (Figure 51):

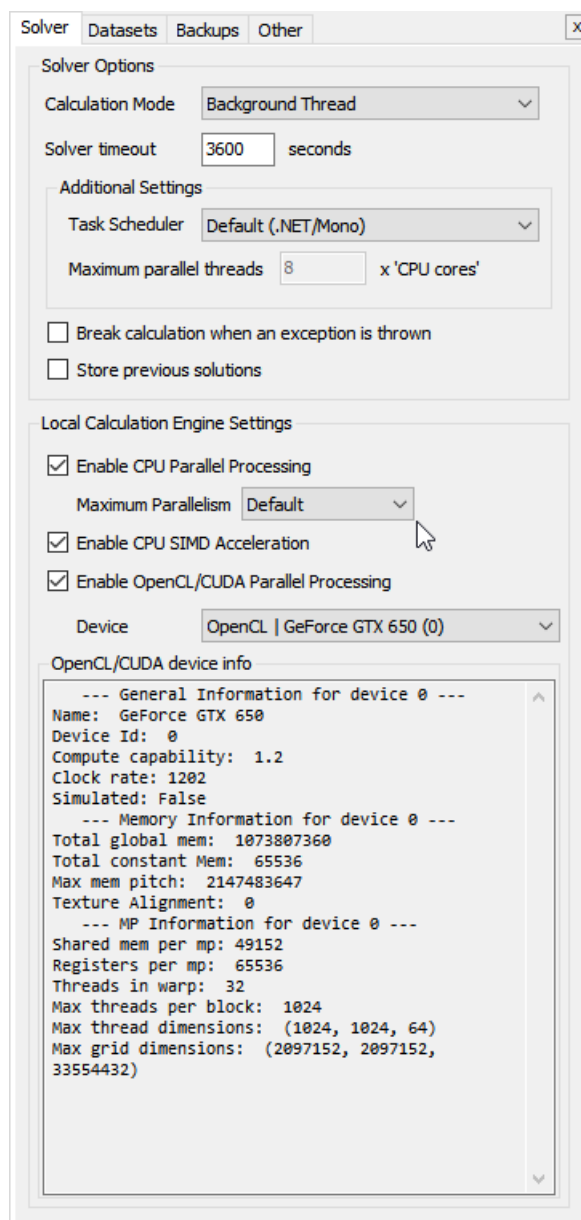


Figure 51: General Settings section.

6.1 Solver

The Solver configuration tab display a group of settings to control the behavior of DWSIM's solver. Check the Wiki article [Solver Configuration](#) for more details.

6.2 Datasets

In the database tab, you have options to remove, add and edit user-defined compound and interaction parameter datasets.

6.3 Backup

The Backup tab has options to control the frequency of the backup file saving. You can also configure the option to save an existing file with another name instead of overwriting it.

6.4 Other

6.4.1 Messages

- **Show tips**: displays context-sensitive tips on the flowsheet information (log) window.
- **Show "What's New"**: displays a window with information about what's new on the running version.
- **Checks for updates**: DWSIM will check for updated installers on startup.
- **Enable automatic updates**: DWSIM will be automatically updated without user intervention. When an update package is available, DWSIM will download and apply it, restarting after the process is finished.

6.4.2 Debug mode

- **Debug level**: controls the amount of information written to the flowsheet information (log) window when solving the simulation.
- **Redirect console output**: redirects the output of the console to the console window inside DWSIM.

6.4.3 UI Language

- **Language**: sets the UI language. Requires a restart.

6.5 Flowsheet

6.5.1 Cut/Copy/Paste Flowsheet Objects

- **Compounds**: controls how compounds are handled during cut/copy/paste operations.
- **Property Packages**: controls how Property Packages are handled during cut/copy/paste operations.

6.5.2 Undo/Redo

- **Recalculate flowsheet**: defines if the flowsheet is to be recalculated after undo/redo operations.

6.5.3 Object Editors

- **Enable multiple editors**: allows displaying of multiple object editors at once.
- **Close editors on deselecting**: closes the editors once the object being edited is deselected.
- **Default initial placement**: default location for displaying the object editors.