**Results**

For this experiment, pressure measurements at two separate points (P1 and P2), compressor shaft RPM measurements (N), and force measurements (Scale Reading) were collected for three separate back plate configurations. The static pressure and temperature of the room were also recorded, for use in finding the density of the air in Oliver Hall. Each pressure measurement (besides the static pressure of Oliver Hall) was recorded in inches of water, with the former being a measurement of the pressure difference between the atmosphere and the larger of the two tube diameters within the compressor, and the latter being a measurement of the pressure difference between the smaller of the two tube diameters within the compressor and the first pressure reading.

With these values collected, the shaft horse power of the compressor was calculated through the use of Equation (1) below:

(1)

This value, whose units were in horse power, was then converted to W through the use of Equation (2) below:

(2)

Once this was completed, the pressure values, which were recorded in inches of water, were converted to Pascals through the use of Equation (3) below:

(3)

Where is the density of water (1000 kg/m3), h is the height of the water in meters, and g is the acceleration of gravity (9.81 m/s2).

With all of these values calculated, the flow rate through the compressor was then found. This was accomplished by assuming a different Reynold’s Number for each RPM increment in each trial. Based on this Reynold’s Number, a coefficient of drag was calculated for each trial based on Equation (4) below:

(4)

Where β is given as 0.5 and L2, the location of PT2 is 0.5. The results of this work are listed in Table (1) on the following page.

This value was then used to calculate the volume flow rate through the compressor, as described in Equation (5) below:

(5)

Where A2 is the smallest area within the compressor, which was found to be 0.041 m2.

The Power Output of the compressor (Po) was then found by multiplying Q by P2. With all of these values calculated, the coefficients associated with the flow through the compressor were then found through the use of Equations (6-9) below:

Power Coefficient:

Pressure Coefficient:

Flow Coefficient:

Reynold’s Number:

(6-9)

Where µ is the kinematic viscosity of air, for which a value of 1.983 x 10-5 kg/ms was used. Once the Re of each trial was found, the initial Re used to calculated CD was changed until the two Re’s were reasonably close for each case (Within 1000 of each other). The final efficiency for each trial (η) was then found by dividing the output power by the input power.

Tables 4-1 through 4-3 list all of the data collected, used, and collected over the course of the experiment.

**Table 4-1. Shaft RPM, Force, Power, and Compressor Pressures**

|  |  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- | --- |
| **Test No** | **N (RPM)** | **Back Plate Location (in)** | **Scale Reading** | **HP** | **PT1 (m)** | **PT2 (m)** |
| 1 | 631 | 3 | 0.5 | 0.078875 | 0.0089 | 0.0000 |
| 2 | 1204 | 3 | 1.75 | 0.52675 | 0.0356 | 0.0000 |
| 3 | 1823 | 3 | 3.9 | 1.777425 | 0.0978 | 0.0000 |
| 4 | 625 | 2 | 0.5 | 0.078125 | 0.0089 | 0.0025 |
| 5 | 1227 | 2 | 1.6 | 0.4908 | 0.0394 | 0.0127 |
| 6 | 1809 | 2 | 3.6 | 1.6281 | 0.0991 | 0.0330 |
| 7 | 625 | 1 | 0.1 | 0.015625 | 0.0089 | 0.0051 |
| 8 | 1286 | 1 | 1.3 | 0.41795 | 0.0432 | 0.0203 |
| 9 | 1812 | 1 | 2.5 | 1.1325 | 0.0914 | 0.0419 |

**Table 4-2. Room Pressure and Temperature, Density, Kinematic Viscosity, and Airflow Parameters**

|  |  |
| --- | --- |
| **Parameter** | **Value** |
| **Temp (K)** | 294.1 |
| **Static Pressure (Pa)** | 100250 |
| **Air Density (kg/m^3)** | 1.1877 |
| **Water Density (kg/m^3)** | 1000 |
| **μ (kg/m s)** | 0.00001983 |
| **A2 (m^2)** | 0.041 |
| **β** | 0.5 |
| **Re (N~600)** | 210000 |
| **Re2 (N~1200)** | 430000 |
| **Re3 (N~1800)** | 690000 |
| **Cd (N~600)** | 0.630 |
| **Cd2 (N~1200)** | 0.618 |
| **Cd3 (N~1800)** | 0.613 |

**Table 4-3. Airflow Coefficients for Each Back Plate Configuration**

|  |  |  |  |  |  |
| --- | --- | --- | --- | --- | --- |
| **Test No** | **Cw** | **Cp** | **Cq** | **Re** | **η** |
| 1 | 0.000375 | 0.0805 | 0.051 | 216041 | 0 |
| 2 | 0.000361 | 0.0884 | 0.053 | 423520 | 0 |
| 3 | 0.000351 | 0.1060 | 0.057 | 697223 | 0 |
| 4 | 0.000383 | 0.0820 | 0.052 | 216041 | 0.139 |
| 5 | 0.000318 | 0.0942 | 0.054 | 445632 | 0.227 |
| 6 | 0.000329 | 0.1091 | 0.058 | 701736 | 0.281 |
| 7 | 0.000077 | 0.0820 | 0.052 | 216041 | 1.385 |
| 8 | 0.000235 | 0.0941 | 0.054 | 466697 | 0.447 |
| 9 | 0.000228 | 0.1004 | 0.056 | 674206 | 0.492 |

**Discussion of Results**

Based on the data listed in Tables 4-1 through 4-3, several different parameters were plotted with respect to Re for each back plate configuration. The first parameter that was plotted was that of the compressor efficiency, as shown in Figure 5-1 below:

**Figure 5-1. Compression Efficiency vs. Re for Each Back Plate Configuration**

As can be seen in the above figure, as Re increases, so does the efficiency of the compressor. This is likely due to the reduced effect of viscosity at higher Re’s, meaning that the flow through the compressor is behaving more isentropic ally, and thus, more efficiently.

However, some discrepancies can be observed, mainly, for the lowest Re value on the X = 2 Inches plot, the efficiency actually exceeds 100%. This result most certainly arose from the mis-recording of the scale force associated with said trial (0.1 lbs for Trial 7, in comparison to 0.5 lbs for Trials 1 and 4). If this experiment were run again and a more accurate force measurement were made, the trend for the 2 inch case would have likely followed that of the 1 inch case.

A final flow characteristic to make note of from this figure is the behavior of the compressor when the back plate was located at 3 inches. In this configuration, the efficiency was zero in each trial. This indicates that absolutely no compression was occurring and that the compressor was essentially acting as an airflow accelerator.

The next parameter that was plotted was that of the power coefficient, as shown in Figure 5-2 below:

**Figure 5-2. Power Coefficient vs. Re for Each Back Plate Configuration**

As can be observed from the figure, the power coefficient for each case tended to decrease slightly as Re increased, with the disclaimer that the first point in the 1 inch case be ignored due to the points raised in the previous paragraphs of this analysis. With this point being ignored, a decrease in the power coefficient over the Re range falls in line with the principal that for increased Re, viscosity effects decrease, meaning that the compressor has to do less work to accelerate the same amount of fluid, thus leading to the observed decrease in the power coefficient.