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1. Prelab

a. Viscosity calculations:

For calculating mixed viscosity, use Refutas method

Calculate VBN for each component

$$VBN_i = 14.534 \times \ln \left(\ln \left(\frac{\eta}{\text{density}} + 0.8 \right) \right) + 10.975$$

$$VBN_f = \sum x_i \times VBN_i$$

$$\frac{\eta}{\text{density}} = e^{e^{\frac{VBN_f - 10.975}{14.534}}} - 0.8$$

Room temp: 19 deg.C as of 24-02-26

Water viscosity: 1.0266 mPa*s

Glycerol viscosity: 1551.5 mPa*s (from calculator)

Target viscosity glycerol 1: 2.0532 mPa*s

Target G2: 4.1064 mPa*s

Refutus method too complicated as it needs density variables which fluctuate with temperature: switching to Exponential Power-Form Model (Cheng, 2008) method with calculator online

From calculator: for 2.0533mPa*s, 79.87% water 20.13% glycerol

For 4.1075: 36.1% glycerol 63.9% water

Dilution calculation with glycerol 5um beads:

Conc. 0.5% weight by volume

5 beads per 1440x1080 pixels x 0.06845um per pixel

= 5 beads per 98.568 x 73.926 um x 5um

G of beads

2.5um rad per bead = 65.45 um^3

/1000^3= 65.45*10^-9 mm^3

/1000 = 65.45*10^-12 cm^3 (ml)

X1.05g/ml = 687.225*10^-13 g/bead

Volume of image = 36433um^3 /1000^3 /1000 = 3.6434*10^-8 ml

Beads per ml = 5/3.6434*10^-8 ml = 1.3723*10^8 beads/ml

g/bead * bead/ml = g/ml = 0.009431

0.005g/1ml initial

Initial/final conc. = 1.886X concentration

Solution: switch to 50X from 100X, 4X the image area

Dilution calculation with glycerol 3um beads:

1.5um rad = 14.137um^3

=...148.4385*10^-13 g/bead

Beads per ml = 10/3.6434*10^-8 ml = 2.7447*10^8 beads/ml

g/bead * bead/ml = g/ml = 0.000407

Original = 0.005

Dilution: 1.2285X

Dilution calculation with glycerol 1um beads:

0.5um rad per bead = 0.5236 um^3

... = 5.4978*10^-13 g/bead

Beads per ml = 10/3.6434*10^-8 ml = 2.7447*10^8 beads/ml

g/bead * bead/ml = g/ml = 0.00015089

Original = 0.005

Initial/final conc. = 33.137X

Correction: FOV is 82.5um depth

Volume of image: 6.055*10^5um^3

/1000^4 = 6.055*10^-7ml

Beads/ml = 10/6.055*10^-7ml = 1.6515*10^7

3um beads:

Beads/ml*148.4385*10^-13 g/bead= 0.00024515

Dilution Factor: 0.005/0.00024515 = 20.39567612X

1. Stokes-Einstein relation:

$$\langle r^2 \rangle = 2dt \cdot D$$

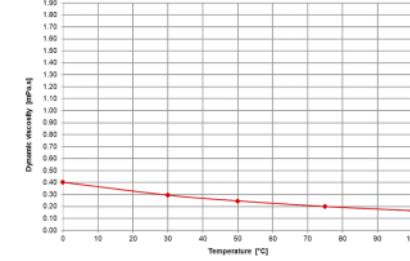
Theoretical Viscosity

$$\eta_d = A \cdot e^{-\frac{E_a}{RT}}$$

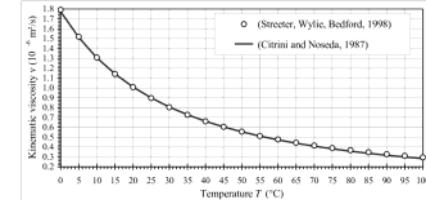
*these constants vary with temperature so a table must be used:

*Do acetone instead of methanol, 0.3mPa

Acetone Viscosity vs temp



Water Viscosity vs temp



Temp. (°C)	Density ρ , kg/m³	Viscosity η_v , dynes/cm.s	Viscosity η_v , mPa.s	Kinematic viscosity η_k , mm²/s	Uncertainty $\Delta \eta$	Relative uncertainty $\Delta \eta / \eta_k$, %	Deviation $\delta \eta$, %
10	668.7261	1306.9	1306.9	1.307	0.009	-0.09	-0.02
15	668.1296	1138.2	1138.2	1.139	0.0015	-0.13	-0.08
20	668.2306	1000.3	1000.3	1.002	0.0025	-0.22	-0.05
25	668.2303	866.3	866.3	0.862	0.0031	-0.26	-0.14
30	668.4710	797.5	797.5	0.796	0.0030	-0.49	-0.20
35	668.4710	717.7	717.7	0.717	0.0028	-0.55	-0.13
40	668.2473	685.3	685.3	0.685	0.0051	-0.39	-0.15
45	668.2473	650.1	650.1	0.650	0.0041	-0.31	-0.11
50	668.2473	547.1	547.1	0.547	0.0033	-0.20	-0.11
55	668.73	504.2	504.2	0.504	0.0016	-0.31	-0.13
60	668.73	447.1	447.1	0.447	0.0011	-0.23	-0.13
65	668.73	404.4	404.4	0.404	0.0011	-0.23	-0.13
70	668.73	365.9	365.9	0.365	0.0012	-0.25	-0.13
75	668.73	335.9	335.9	0.335	0.0012	-0.25	-0.13
80	668.73	310.9	310.9	0.310	0.0012	-0.25	-0.13
85	668.73	290.9	290.9	0.290	0.0012	-0.25	-0.13
90	668.73	270.9	270.9	0.270	0.0012	-0.25	-0.13
95	668.73	250.9	250.9	0.250	0.0012	-0.25	-0.13
100	672.01	230.9	230.9	0.230	0.0012	-0.25	-0.13

$\Delta = (2.2718 \pm 0.00071) \times 10^6 \text{ Pa} \cdot \text{s}$
 $\eta = (6.67 \pm 0.52) \times 10^{-6} \text{ m}^2/\text{s}$

1. Stokes-Einstein relation:

$$\langle r^2 \rangle = 2dt \cdot D$$

$$D = \frac{k_B \cdot T}{6\pi \cdot \eta \cdot R}, m^3 s^{-3}$$

$$k_B = Boltz. Cst. = 1.380649 \cdot 10^{-23} m^2 kg \cdot s^{-2} K^{-1}$$

η = viscosity, $Pa \cdot s$ or $kg \cdot s \cdot m^{-2}$

R = bead radius, m

Concentration effects:

- Increased effective fluid viscosity
- Fused particles have effectively increased radius, more drag and therefore less brownian motion
- Wall effects increase viscosity from liquid shearing effects

Einstines Viscosity Equation (for suspension)

$$\eta = \eta_0(1 + 2.5\phi)$$

η = apparent viscosity, η_0 = original viscosity (of mixed fluid)

$$\phi = \text{partical fraction volume} = \left(\frac{V_{\text{bead}} \cdot n_{\text{bead}}}{V_{\text{solution}}} \right)$$

For higher concentrations, use Batchelor equation:

$$\eta = \eta_0(1 + 2.5\phi + 6.2\phi^2)$$

Concentration should be chosen where particles do not clump or fuse, so increased radius effects can be ignored.

Wall Interactions:

Use Faxén's Laws.

$$D_{||} = D_0 \cdot [1 - 9/16 \cdot (R/h) + 1/8 \cdot (R/h)^3 - 45/256 \cdot (R/h)^4 - 1/16 \cdot (R/h)^5 \dots]$$

Volume of slide: est. 50um

Max particle size: 5um

Minimum wall effect for 5um: $D = D_0 * (1 - 0.1138)$

2. Objectives:

- Make different bead samples, 7 different slides varying concentration, viscosity, particle size 3 times.
- Record 3 avi videos of beads for each slide (21 videos)
- Repeat samples to get consistent data (14 mixtures/slides, 42 videos)
- Data analysis during spare time
- Uncertainties in data if we have sufficient lab time

3. Procedure

*actual framerate 66.019fps

Target slides:

Slide	Mix/Visc. (% glycerol)	Bead Size (um)	Conc (beads/FOV)
1	0	3um	10
2	20	1um	10
3	20	3um	10
4	20	5um	10
5	20	3um	5
6	20	3um	20
7	36	3um	10

Dilution factors:

Slide	Factor	Percent Stock
1	20.3956	4.90%
2		
3		
4		
5		
6		
7		

Notes:

- Once we used a field depth of 82.5micrometers (tape depth), the amount of beads improved a lot (previously there were 200 beads in the field of view)
- Probably 2X as diluted as above calculation

To Do

- Lookup actual FOV of microscope
- Try using nailpolish instead of tape
- Make sure slide is symetrical so particles don't drift to escape
- Find a spot on slide where concentration of beads is correct so we can analyze the other effects

0.000	29	100	4	11	12	13	14	15	16	17	18	19	20	21	22	23	24	25	26	27	28	29	30
666.07	543.1	343	547	553	553	553	553	553	553	553	553	553	553	553	553	553	553	553	553	553	553	553	553
553.29	430.3	247	430	430	430	430	430	430	430	430	430	430	430	430	430	430	430	430	430	430	430	430	430
553.24	665.4	497	655	655	655	655	655	655	655	655	655	655	655	655	655	655	655	655	655	655	655	655	655
553.09	635.4	884	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643
553.11	655.9	882	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643	643

$A = (2.2716 \pm 0.0007) \times 10^6 \mu\text{Pa}\cdot\text{s}$
 $B = (6.7 \pm 0.32) \times 10^{-6} \text{ m}^2$

Glycerol Viscosity vs temp

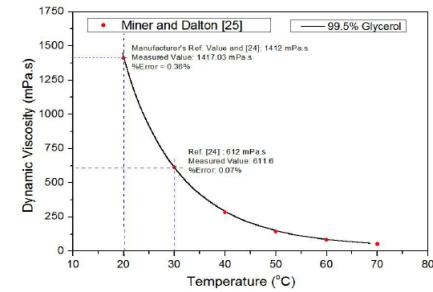


TABLE V. Viscosity of various glycerol solutions

Glycerol (%)	0	20	30	40	50	60	70	80	90	95	100
0.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
1.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
2.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
3.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
4.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
5.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
6.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
7.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
8.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
9.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
10.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
11.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
12.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
13.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
14.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
15.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
16.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
17.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
18.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
19.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
20.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
21.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
22.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
23.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
24.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
25.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
26.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
27.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
28.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
29.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-
30.000	1.7052	1.364	1.095	0.800	0.6000	0.5124	0.4658	0.4141	0.3562	0.3093	-

- Finish collecting rest of slides, analyzing motion, comparing results and matching with formula