



Cairo University - Faculty Of Engineering
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Control Engineering - Spring 2025



Two-Ttank System

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Part 1: Dynamic Equations and Block Diagram

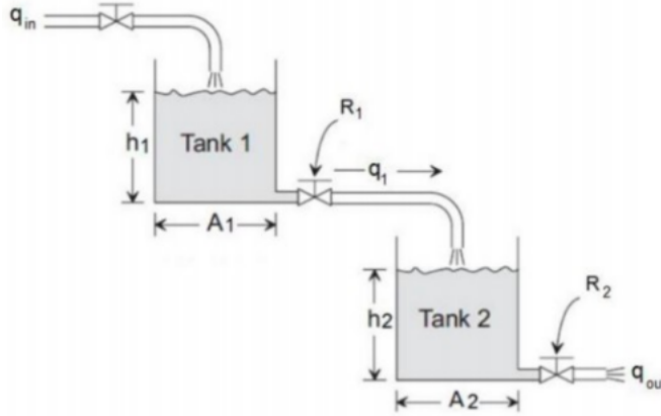


Figure 1: Two-tank System

Dynamic Equations

For Tank 1:

$$q_{in}(t) - q_1(t) = A_1 \frac{dh_1}{dt} \quad \longrightarrow \quad Q_{in}(S) - Q_1(S) = A_1 S H_1(S) \quad (1)$$

$$q_1(t) = \frac{h_1(t) - h_2(t)}{R_1} \quad \longrightarrow \quad Q_1(S) = \frac{H_1(S) - H_2(S)}{R_1} \quad (2)$$

Substituting (2) into (1):

$$\frac{dh_1}{dt} = \frac{1}{A_1} \left(q_{in}(t) - \frac{h_1(t) - h_2(t)}{R_1} \right) \quad \longrightarrow \quad H_1(S) = \frac{1}{SA_1} \left(Q_{in}(S) - \frac{H_1(S) - H_2(S)}{R_1} \right) \quad (3)$$

For Tank 2:

$$q_1(t) - q_2(t) = A_2 \frac{dh_2}{dt} \quad \longrightarrow \quad Q_1(S) - Q_2(S) = A_2 S H_2(S) \quad (4)$$

Output flow:

$$q_2(t) = \frac{h_2(t)}{R_2} \quad \longrightarrow \quad Q_2(S) = \frac{H_2(S)}{R_2} \quad (5)$$

Substituting (5) into (4):

$$\frac{dh_2}{dt} = \frac{1}{A_2} \left(\frac{h_1(t) - h_2(t)}{R_1} - \frac{h_2(t)}{R_2} \right) \quad \longrightarrow \quad H_2(S) = \frac{1}{SA_2} \left(\frac{H_1(S) - H_2(S)}{R_1} - \frac{H_2(S)}{R_2} \right) \quad (6)$$

$$Q_2(S) = Q_{in}(S) - A_1 S H_1(S) - A_2 S H_2(S)$$

$$Q_2(S) = Q_{in}(S) - A_1 S [Q_1(S) R_1 + H_2(S)] - A_2 S [R_2 Q_2(S)]$$

$$Q_2(S) = Q_{in}(S) - A_1 S Q_2(S) R_1 - A_1 A_2 S^2 H_2(S) R_1 - A_1 S R_2 Q_2(S) - A_2 S R_2 Q_2(S)$$

$$Q_2(S) = Q_{in}(S) - A_1 S Q_2(S) R_1 - A_1 A_2 S^2 [R_1 Q_2(S)] R_1 - A_1 S R_2 Q_2(S) - A_2 S R_2 Q_2(S)$$

$$Q_2(S) [1 + A_1 S R_1 + A_1 A_2 S^2 R_1 R_2 + A_1 S R_2 + A_2 S R_2] = Q_{in}(S)$$

Block Diagram Representation

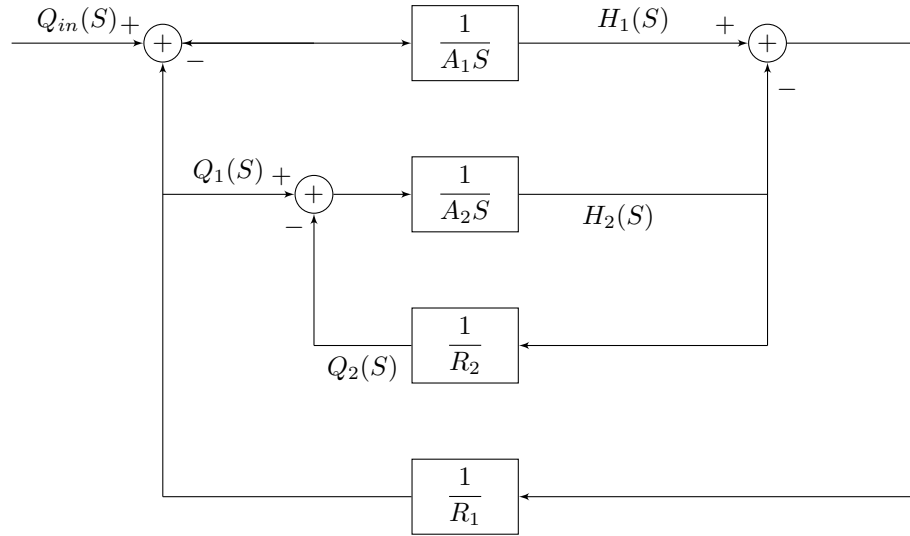


Figure 2: Block diagram of the system

Simulation

Obtaining Transfer Functions using MATLAB

System Parameters: $A_1 = 5m^2$, $A_2 = 4m^2$, $R_1 = 3s/m^2$, $R_2 = 5s/m^2$

Using Matlab, we get the following results:

$$\frac{H_2(S)}{Q_{in}(S)} = \frac{5}{300S^2 + 60S + 1}$$

$$\frac{H_1(S)}{Q_{in}(S)} = \frac{60S + 8}{300S^2 + 60S + 1}$$

$$\frac{Q_1(S)}{Q_{in}(S)} = \frac{20S + 1}{300S^2 + 60S + 1}$$

$$\frac{Q_2(S)}{Q_{in}(S)} = \frac{1}{300S^2 + 60S + 1}$$

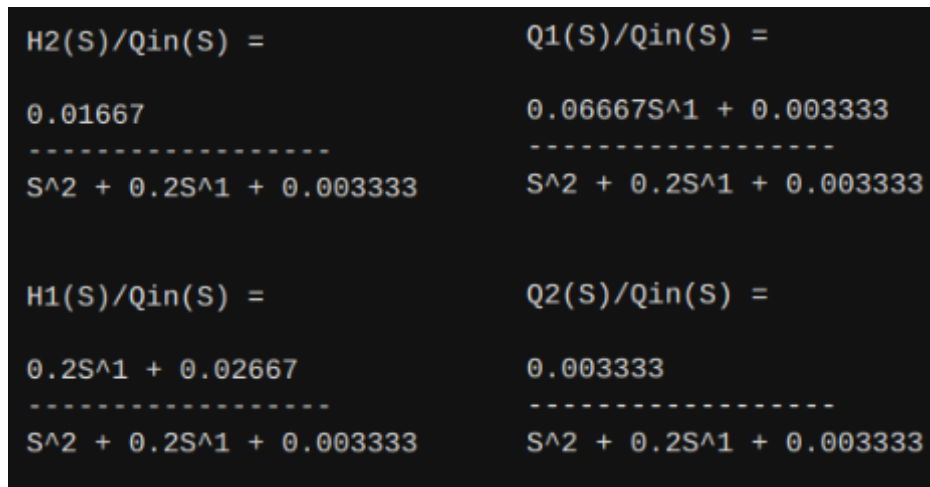


Figure 3: Transfer Functions

Studying Stability

Studying the stability of the system by analyzing the denominator of TF: $300S^2 + 60S + 1 = 0$
We find that the system has 2 poles:

$$P_0 = -0.18165, \quad P_1 = -0.01835$$

We can see that both of them lie on the left half of the plane, which means that the system is stable. We also checked it using the `isstable()` function in MATLAB.

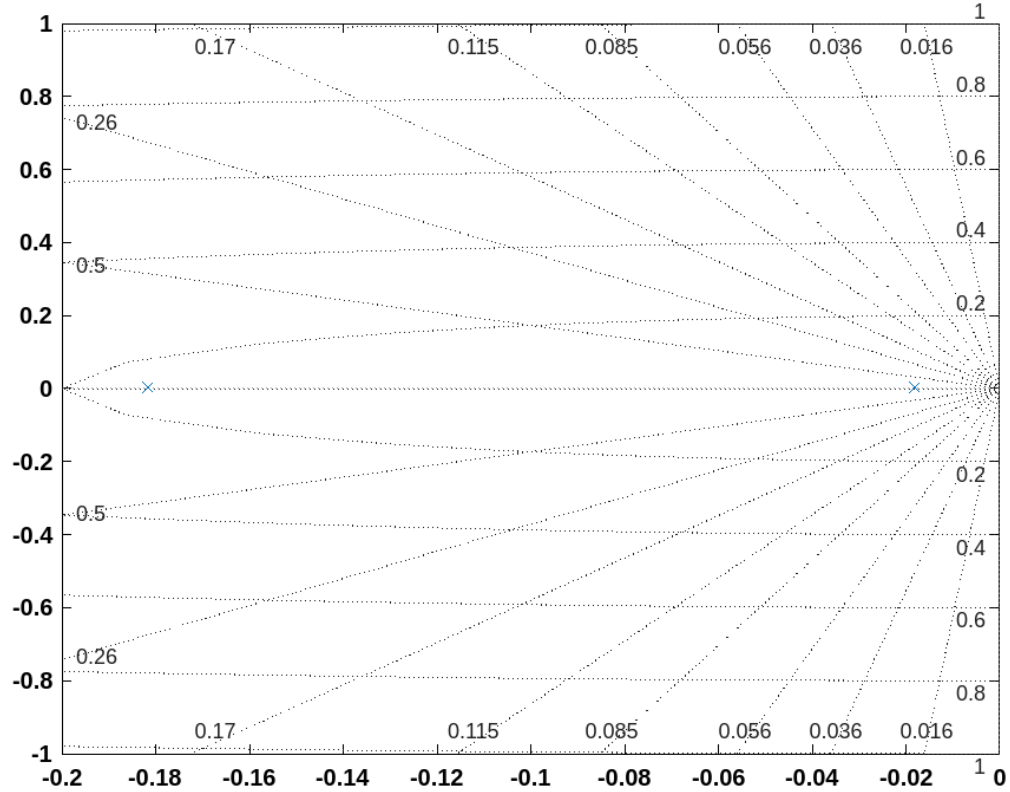


Figure 4: Pole-Zero map of the system

Simulating with $Q_{in} = 1m/s$

After simulating we get the following results

```
Steady-state values:
h1 = 7.9992 m
h2 = 4.9994 m
Q1 = 0.9999 m^3/s
Q2 = 0.9999 m^3/s
```

Figure 5: Steady State Values for System Outputs

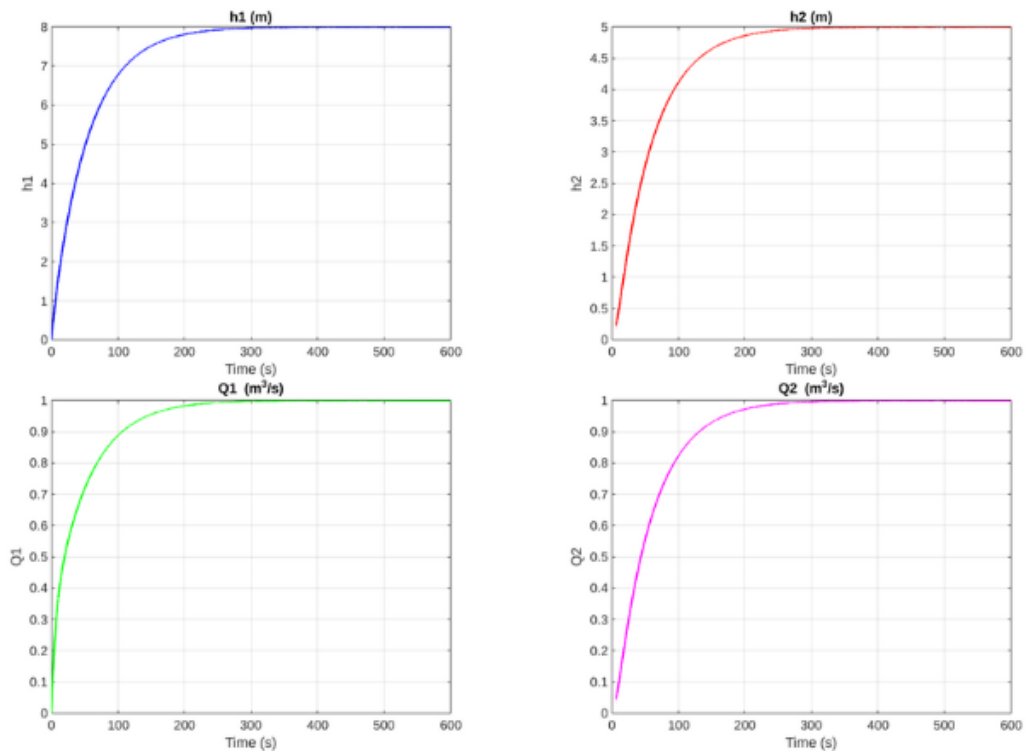


Figure 6: Time Responses for System Outputs

Theoretically

$$h_1(t \approx \infty) = \lim_{S \rightarrow 0} SH_1(S) \approx 8 \text{ m}$$

$$h_2(t \approx \infty) = \lim_{S \rightarrow 0} SH_2(S) \approx 5 \text{ m}$$

$$q_1(t \approx \infty) = \lim_{S \rightarrow 0} SQ_1(S) \approx 1 \text{ m}^3/s$$

$$q_2(t \approx \infty) = \lim_{S \rightarrow 0} SQ_2(S) \approx 1 \text{ m}^3/s$$

Part 2: Feedback Modification and Stability Check

Representation of the feedback modification block diagram

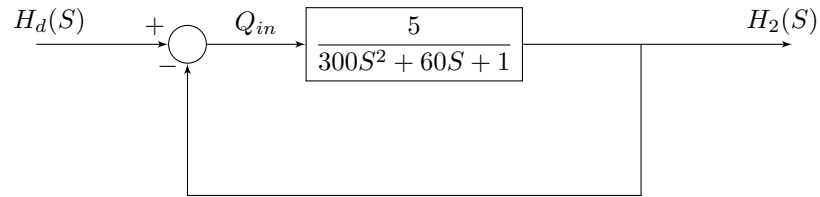


Figure 7: Block Diagram of the Feedback-Modified System

Simulating with $h_d = 5m$

After simulating we get the following results

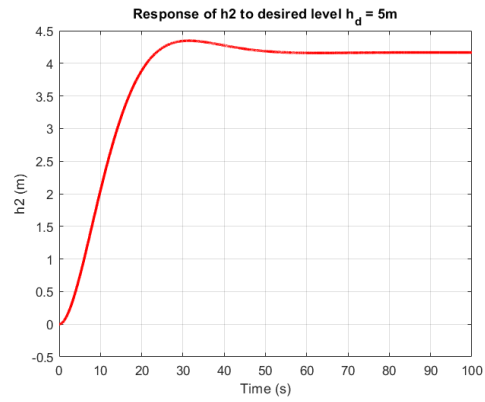


Figure 8: Steady-State Response for Feedback Stabilization

Theoretically

Natural frequency

$$\omega_n^2 = \frac{1}{50} \implies \omega_n = \frac{1}{5\sqrt{2}}$$

Damping ratio

$$2\zeta\omega_n = \frac{1}{5} \implies \zeta = \frac{1}{\sqrt{2}}$$

Phase angle

$$\zeta = \cos \psi = \frac{1}{\sqrt{2}} \implies \psi = \frac{\pi}{4}$$

Steady-state gain

$$M = \lim_{s \rightarrow 0} sH_2(s) = \frac{5}{6}h_d \approx 4.1667$$

Resonant frequency

$$\omega = \omega_n \sin \psi = \frac{1}{10}$$

Rise time

$$t_r = \frac{\pi - \psi}{\omega} = \frac{15}{2}\pi \approx 23.562 \text{ seconds}$$

Peak time

$$t_p = \frac{\pi}{\omega} = 10\pi \approx 31.416 \text{ seconds}$$

Peak overshoot

$$M_p = M \left(1 + e^{-\frac{\pi}{\tan \psi}} \right) = M (1 + e^{-\pi}) \approx 4.3467 \text{ meters}$$

Settling time

$$t_s = \frac{4}{\zeta\omega_n} = 40 \text{ seconds} \quad (2\% \text{ criterion})$$

Steady-state error

$$e_{ss} = 5 - 4.1667 = 0.8333 \text{ meters}$$

adding a proportional controller

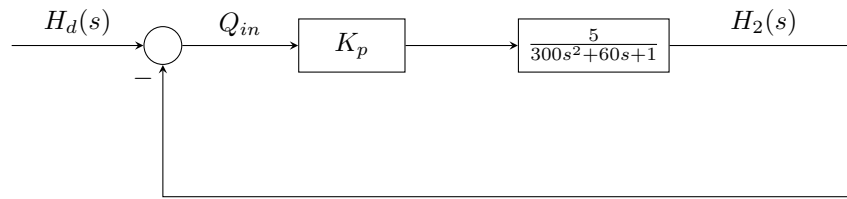
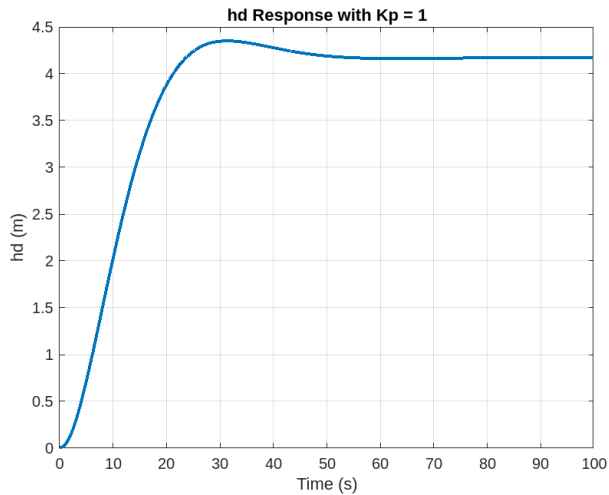


Figure 9: Block diagram of a unity feedback control system with a proportional controller K_p .

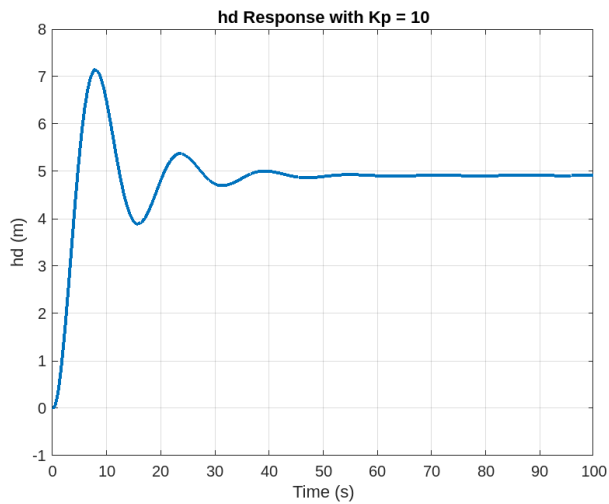


(a) Figure 9: proportional controller with $k_p = 1$

```

--- Kp = 1 ---
Rise Time: NaN s
Peak Time: 31.4131 s
Overshoot: 0.00 %
Settling Time: NaN s
Steady-State Error: 0.8331 m
    
```

(b) Figure 10: Transient Response Output with $k_p = 1$

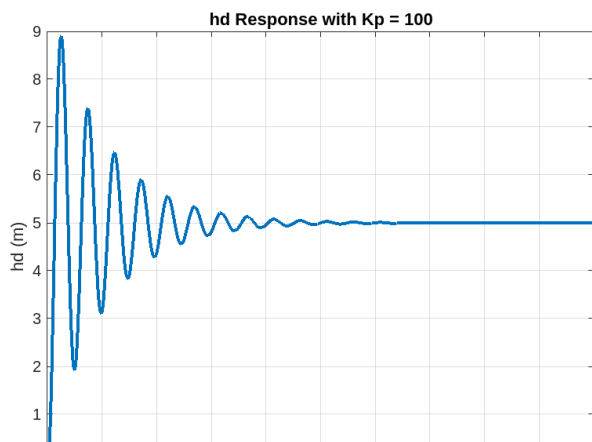


(c) Figure 11: proportional controller with $k_p = 10$

```

--- Kp = 10 ---
Rise Time: 3.0871 s
Peak Time: 7.8508 s
Overshoot: 42.74 %
Settling Time: 66.6018 s
Steady-State Error: 0.0979 m
    
```

(d) Figure 12: Transient Response Output with $k_p = 10$



```

--- Kp = 100 ---
Rise Time: 0.8400 s
Peak Time: 2.4402 s
Overshoot: 78.01 %
Settling Time: 20.3803 s
    
```

Comment on Previous Results

Increasing K_p decreases the steady-state error (ESS), but also reduces the system's stability and increases the transient response parameters.

Question 9: If the actual height of the second tank walls is 6 m, is it possible to obtain a steady-state error less than 0.01 using a proportional-only controller? Why?

Answer:

For a proportional controller, the steady-state error (ESS) is given by:

$$\text{ESS} = \frac{6}{1 + 5K_p}$$

To achieve a steady-state error less than 0.01, we set:

$$\frac{6}{1 + 5K_p} < 0.01$$

Solving for K_p :

$$\frac{6}{0.01} < 1 + 5K_p \Rightarrow 600 < 1 + 5K_p \Rightarrow 599 < 5K_p$$

$$K_p > \frac{599}{5} = 119.8$$

So, we need $K_p > 119.8$ to achieve ESS ≤ 0.01 .

Now, let's analyze the stability of the system. The closed-loop transfer function is:

$$\frac{5K_p}{300s^2 + 60s + (1 + 5K_p)}$$

From this, we can extract:

$$\omega_n^2 = \frac{1 + 5K_p}{300}$$

Let's use $K_p = 120$ as a practical value (just above 119.8). Then:

$$\omega_n^2 = \frac{1 + 5 \times 120}{300} = \frac{601}{300} \approx 2.003 \Rightarrow \omega_n \approx \sqrt{2.003} \approx 1.414$$

The damping ratio ζ is:

$$\zeta = \frac{60}{2 \cdot 300 \cdot \omega_n} = \frac{60}{600 \cdot 1.414} \approx \frac{60}{848.4} \approx 0.071$$

This shows that increasing K_p decreases ESS but also decreases ζ , meaning the system becomes less stable with more oscillatory transient response.

Conclusion:

Yes, it is theoretically possible to achieve ESS ≤ 0.01 using only a proportional controller by choosing $K_p > 119.8$, but this significantly reduces the damping ratio $\zeta \approx 0.071$, leading to a highly oscillatory and potentially unstable response.

Question 10: Suggest a suitable controller to eliminate the steady-state error. Then, simulate the system using your proposed controller.

Answer:

To eliminate the steady-state error, we propose using a Proportional-Integral (PI) controller:

$$C(s) = K_p \left(1 + \frac{1}{T_i s} \right)$$

This increases the system type and ensures zero steady-state error. However, we must also verify system stability.

The closed-loop transfer function becomes:

$$\frac{5K_p(s + \frac{1}{T_i})}{s(300s^2 + 60s + 1) + 5K_p(s + \frac{1}{T_i})}$$

Simplifying the denominator:

$$s(300s^2 + 60s + 1) + 5K_p \left(s + \frac{1}{T_i} \right) = 300s^3 + 60s^2 + s + 5K_p s + \frac{5K_p}{T_i}$$

So the closed-loop transfer function becomes:

$$\frac{5K_p(s + \frac{1}{T_i})}{300s^3 + 60s^2 + (1 + 5K_p)s + \frac{5K_p}{T_i}}$$

To ensure stability of this third-order system, the **Routh-Hurwitz** criteria must be satisfied. One important condition is:

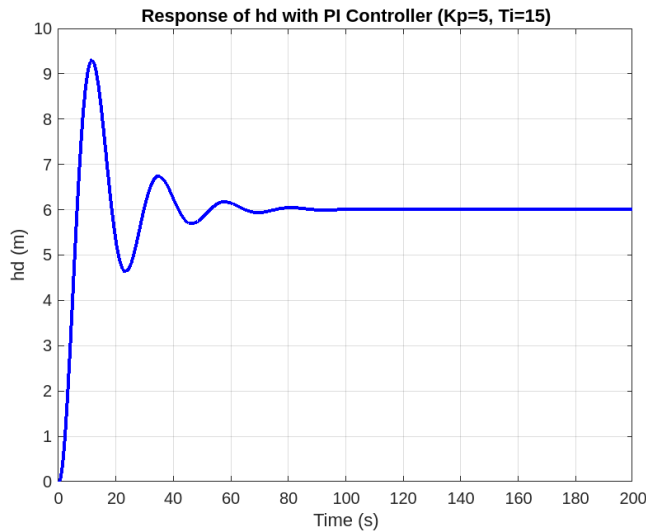
$$60(1 + 5K_p) > 300 \cdot \left(\frac{5K_p}{T_i} \right)$$

This ensures that the middle term product is greater than the product of the outer terms.

For the simulation, we choose:

$$K_p = 5, \quad T_i = 15$$

Simulation Results:



```

--- PI Controller Results (Kp = 5, Ti = 15) ---
Rise Time: 3.6638 s
Peak Time: 11.4611 s
Overshoot: 85.80 %
Settling Time: NaN s
Steady-State Error: 0.0000 m

```

Figure 16: ESS value and transient parameters values

Figure 15: System Output with PI Controller

Appendix A

Appendix

A.1 Code

```
1 A1 = 5; A2 = 4; R1 = 3; R2 = 5;
2 % State-space matrices
3
4 % Assume our state is [h1, h2] , input is Qin, outputs are Q2, Q1, H1, H2
5
6 % State Matrix
7 A = [-1/(A1*R1), 1/(A1*R1);           % dh1/dt equation
8       1/(A2*R1), -(1/(A2*R1) + 1/(A2*R2))]; % dh2/dt equation
9
10 % Input Matrix
11 B = [1/A1; 0];                       % Input only affects dh1/dt
12
13 % Output Matrix
14 C = [0, 1/R2;                         % q_out output
15       1/R1, -1/R1;                   % q1 output
16       1, 0;                          % h1 output
17       0, 1];                         % h2 output
18
19 % Direct Feedthrough Matrix
20 D = zeros(4,1);
21
22 sys = ss(A,B,C,D,'InputName','Qin','OutputName',{'Q2','Q1','H1','H2'});
23
24 transfer_functions = {
25     tf(sys(4)), % H2/Qin
26     tf(sys(3)), % H1/Qin
27     tf(sys(2)), % Q1/Qin
28     tf(sys(1)) % Q2/Qin
29 };
30
31 names = {'H2(S)/Qin(S)', 'H1(S)/Qin(S)', 'Q1(S)/Qin(S)', 'Q2(S)/Qin(S)'};
32
33 for k = 1:length(transfer_functions)
34     tf_current = transfer_functions{k};
35     [num, den] = tfdata(tf_current, 'v');
36
37     fprintf('\n\n\n%s = \n\n', names{k});
38
39     % Print numerator
40     for i = 1:length(num)
41         power = length(num)-i;
42         if num(i) == 0
43             continue;
44         end
45         if power > 0
46             if num(i) == 1
47                 fprintf('S^%d + ', power);
48             else
49                 fprintf('%.4gS^%d + ', num(i), power);
```

```

50         end
51     else
52         fprintf('%.4g', num(i));
53     end
54 end
55
56 % Print denominator
57 fprintf('\n-----\n');
58 for i = 1:length(den)
59     power = length(den)-i;
60     if den(i) == 0
61         continue;
62     end
63     if power > 0
64         if den(i) == 1
65             fprintf('S^%d + ', power);
66         else
67             fprintf('%.4gS^%d + ', den(i), power);
68         end
69     else
70         fprintf('%.4g', den(i));
71     end
72 end
73
74 end
75
76 % Stability analysis
77 P = pole(tf(sys(4)));
78 fprintf('\n\nPoles of H2/Qin: P0 = %.4f, P1 = %.4f\n', P(1), P(2));
79 is_stable = isstable(tf(sys(4)));
80 fprintf('Is stable: %d\n', is_stable);
81
82 figure;
83 pzmap(tf(sys(4)));
84 title('Pole-Zero Map of H2/Qin');
85 grid on;
86
87 % Simulate response to a step input (1 m^3/s)
88 t = linspace(0, 500, 10000); % 10,000 samples over 500 seconds
89 u = ones(size(t));          % Step input of 1 m^3/s
90
91 [y, t_out, x] = lsim(sys, u, t);
92
93 % Plot h1
94 figure;
95 plot(t_out, y(:,3), 'b', 'LineWidth', 1.5);
96 grid on;
97 title('h1 (m)');
98 xlabel('Time (s)');
99 ylabel('h1');
100
101 % Plot h2
102 figure;
103 plot(t_out, y(:,4), 'r', 'LineWidth', 1.5);
104 grid on;
105 title('h2 (m)');
106 xlabel('Time (s)');
107 ylabel('h2');
108
109 % Plot Q1
110 figure;
111 plot(t_out, y(:,2), 'g', 'LineWidth', 1.5);
112 grid on;
113 title('Q1 (m^3/s)');
114 xlabel('Time (s)');
115 ylabel('Q1');
116
117 % Plot Q2
118 figure;
119 plot(t_out, y(:,1), 'm', 'LineWidth', 1.5);
120 grid on;

```

```

121 title('Q2 (m^3/s)');
122 xlabel('Time (s)');
123 ylabel('Q2');
124
125 % Calculate steady-state values
126 steady_state_values = y(end, :);
127 fprintf('\nSteady-state values:\n');
128 fprintf('h1 = %.4f m\n', steady_state_values(3));
129 fprintf('h2 = %.4f m\n', steady_state_values(4));
130 fprintf('Q1 = %.4f m^3/s\n', steady_state_values(2));
131 fprintf('Q2 = %.4f m^3/s\n', steady_state_values(1));
132
133 % Modify the system to have a feedback with a reference signal h_d
134 sys_cl = feedback(sys(4,:),1);
135
136 % Simulate response to a step input (h_d = 5 meters)
137 t = linspace(0,100,10000); % 10,000 samples over 100 seconds
138
139 hd = 5 * ones(size(t));
140
141 [h2_response,t_out] = lsim(sys_cl,hd,t);
142
143 % Plot h2 response
144 figure;
145 plot(t_out, h2_response, 'r', 'LineWidth', 2);
146 grid on;
147 title('Response of h2 to desired level h_d = 5m');
148 xlabel('Time (s)');
149 ylabel('h2 (m)');
150
151 info = stepinfo(h2_response, t_out, 5); % 5 is the desired final value
152
153 fprintf('Rise time: %.4f seconds\n', info.RiseTime);
154 fprintf('Peak time: %.4f seconds\n', info.PeakTime);
155 fprintf('Maximum overshoot: %.2f%%\n', info.Overshoot);
156 fprintf('Settling time: %.4f seconds\n', info.SettlingTime);
157
158 % Steady-state error
159 ess = abs(5 - h2_response(end));
160 fprintf('Steady-state error (ess): %.4f meters\n', ess);
161
162 % adding the controller to the system
163
164 Kp_values = [1, 10, 100];
165 hd = 5 * ones(size(t)); % Desired height
166
167 for i = 1:length(Kp_values)
168     Kp = Kp_values(i);
169
170     % Closed-loop transfer function with proportional controller
171     sys_cl = feedback(Kp * tf(sys(4)), 1);
172
173     % Simulate response
174     [h2_response, t_out] = lsim(sys_cl, hd, t);
175
176     % Plot response
177     figure;
178     plot(t_out, h2_response, 'LineWidth', 2);
179     grid on;
180     title(sprintf('hd Response with Kp = %d', Kp));
181     xlabel('Time (s)');
182     ylabel('hd (m)');
183
184     % Step response characteristics
185     info = stepinfo(h2_response, t_out, 5); % Final value = 5
186     ess = abs(5 - h2_response(end)); % Steady-state error
187
188     fprintf('\n\n--- Kp = %d ---\n', Kp);
189     fprintf('Rise Time: %.4f s\n', info.RiseTime);
190     fprintf('Peak Time: %.4f s\n', info.PeakTime);
191     fprintf('Overshoot: %.2f %%\n', info.Overshoot);

```

```

192     fprintf('Settling Time: %.4f s\n', info.SettlingTime);
193     fprintf('Steady-State Error: %.4f m\n', ess);
194 end
195
196
197
198 % Define PI controller parameters
199 Kp = 5;
200 Ti = 15;
201
202 % Define PI controller transfer function:  $C(s) = K_p * (1 + 1/(T_i*s))$ 
203 s = tf('s');
204 C = Kp * (1 + 1/(Ti*s)); % Alternatively:  $C = (K_p*T_i*s + K_p)/(T_i*s)$ 
205
206 % Get plant  $G(s) = H_2(s)/Q_{in}(s)$ 
207 G = tf(sys(4)); % From  $Q_{in}$  to  $h_2$ 
208
209 % Closed-loop system: feedback of  $C(s)*G(s)$ 
210 sys_cl_PI = feedback(C * G, 1);
211
212 % Simulate step response to desired  $h_d = 5m$ 
213 t = linspace(0, 200, 10000);
214 hd = 6 * ones(size(t));
215
216 [h2_PI, t_out] = lsim(sys_cl_PI, hd, t);
217
218 % Plot response
219 figure;
220 plot(t_out, h2_PI, 'b', 'LineWidth', 2);
221 grid on;
222 title('Response of  $h_d$  with PI Controller ( $K_p=5$ ,  $T_i=15$ )');
223 xlabel('Time (s)');
224 ylabel('hd (m)');
225
226 % Analyze response characteristics
227 info = stepinfo(h2_PI, t_out, 5);
228 ess = abs(6 - h2_PI(end));
229
230 fprintf('\n--- PI Controller Results ( $K_p = 5$ ,  $T_i = 15$ ) ---\n');
231 fprintf('Rise Time: %.4f s\n', info.RiseTime);
232 fprintf('Peak Time: %.4f s\n', info.PeakTime);
233 fprintf('Overshoot: %.2f %%\n', info.Overshoot);
234 fprintf('Settling Time: %.4f s\n', info.SettlingTime);
235 fprintf('Steady-State Error: %.4f m\n', ess);

```

Listing A.1: project code