

# Experimental Investigation of laminar length for Impinging Jet

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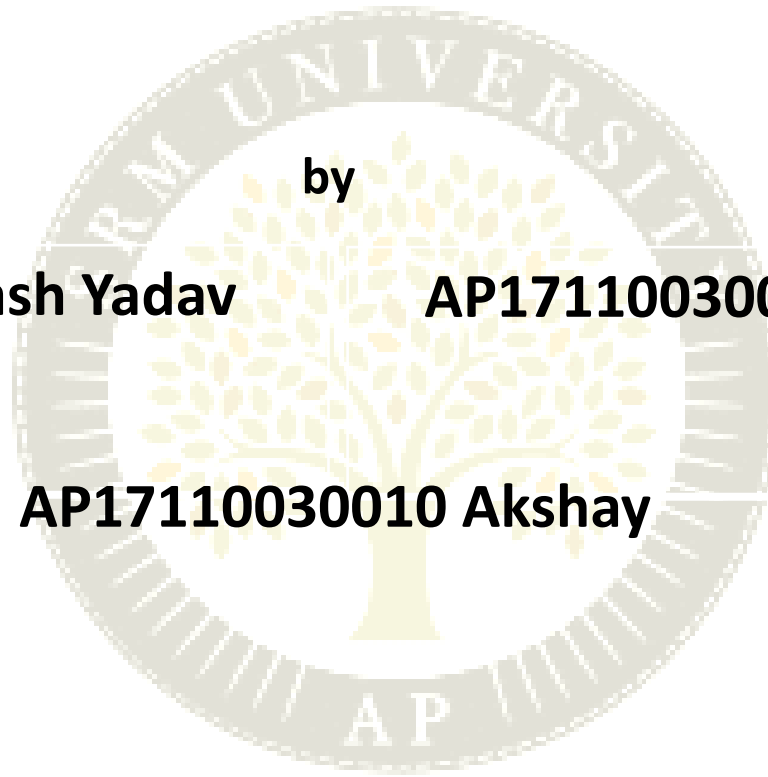
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# Overview

- **Background**
- **Literature review**
- **Experimental setup and procedure**
- **Result Comparison**
- **Result**
- **Conclusion**
- **Uncertainty**
- **Applications**



# Background

**Jet:** A jet is a stream of fluid that is projected into a surrounding medium, usually from some kind of a nozzle, aperture or orifice.

**Impinging Jet:** The impinging jet is defined as a high-velocity jet of cooling fluid forced through a hole or slot which impinges on the surface to be cooled, which results in high heat transfer rate between the wall and the fluid.

**Laminar flow:** At low velocities, the fluid appeared to move in layer or lamina, and hence the nature of this flow is termed laminar flow or stream line.

**Transition zone :** The region of flow bounded by the lower and upper critical velocities is termed as the transition zone.

**Turbulent:** Further increase in velocity of flow the streamline remains in a diffused state and the nature of this type of flow is termed turbulent.

# Literature Review

Table 1: Brief overview of Literature on submerged jets

Author	Experimental method	Dimensions of test tank	Jet dimension	Fluid used in jet	Range of Reynolds number	Remarks
			$D_j$ (mm)		$Re = \frac{\rho U D_j}{\mu}$	
Reynolds A. J (1962)	Observations of Liquid into Liquid jets.	Cylindrical tank (glass) $L = 1200$ mm $D = 300$ mm	$0.32$ mm $\pm 0.05$ mm	Water and Dyed water (Eosine dye)	$10 < Re < 300$ $Re > 300$	Long steady jet at relatively low $Re$ i.e. ( $10 < Re < 30$ ).  For $150 < Re < 300$ , Longer jet with complex breakdown.  For $Re > 300$ , jet become disordered near nozzle.
K.J Mc Naughton and C.G Sinclair (1965)	Submerged jets in short cylindrical flow vessels.	Cylindrical vessel (discharging)  $D = 30$ mm $L = 1200$ mm	Circular jet diameter = $0.32$ mm	Water and Dyed water	$Re < 300$ , $300 < Re < 1000$ , $1000 < Re < 3000$ , $Re > 3000$	Dissipated Laminar Jet, Fully laminar jet, Semi turbulent Jet and Fully turbulent jets are observed. Furthermore, Equation correlated with laminar length 'a': $a/d = 9.97 \times 10^{-7} Re^{-2.46} \times (D/d)^{-0.48} \times (L/d)^{0.74}$

# Literature Review

T. Chafekar, Nishant Nayan, Ranjit Kumar, V. Katti and S.V.Prabhu. (2008)	Flow visualization studies on submerged free and impinging jets.	Cubical vessel of 500*500*500 mm <sup>3</sup> . Impinging plate 300 mm * 300 mm.	Circular jet of Diameter = 7.3 mm.	Water and Dyed water	$1000 < Re < 3500$	<p>Flow visualization on submerged free jet (free and free orifice jet) and impinging jet.</p> <p>For <math>Re &lt; 2000</math>, the flow is observed to be laminar for free and impinging jets.</p> <p>At <math>Re = 2200</math> and <math>Re = 2500</math>, transition zone for free jet and impinging jet.</p> <p><math>Re &gt; 2700</math>, turbulent zone started for all jets.</p>
Vadiraj Katti, S.V. Prabhu (2008)	Experimental study and theoretical analysis of local heat transfer between smooth flat surface and impinging air jet from a circular straight pipe nozzle.	Stainless steel target plate of 80 mm * 160 mm having 0.06 mm thickness.	Impinging circular jet on flat plate with length to diameter ratio = 83 and diameter = 7.35 mm	High Pressure Air at 4 bar	$12000 < Re < 28000$	<p>Local heat transfer characteristics are estimated and heat transfer at stagnation point and transition region obtained from laminar boundary. Increase in <math>Re</math>, increases the heat transfer.</p>

# Experimental set-up and Procedure

1. Dyed tank.
2. U-tube manometer with scale.
3. Table stand
4. Flow Pipe
5. Visualization tank
6. Festo Needle valve ( 0.5 in.)
7. High Shutter speed Camera
8. Tripod stand
9. Drain Valve.

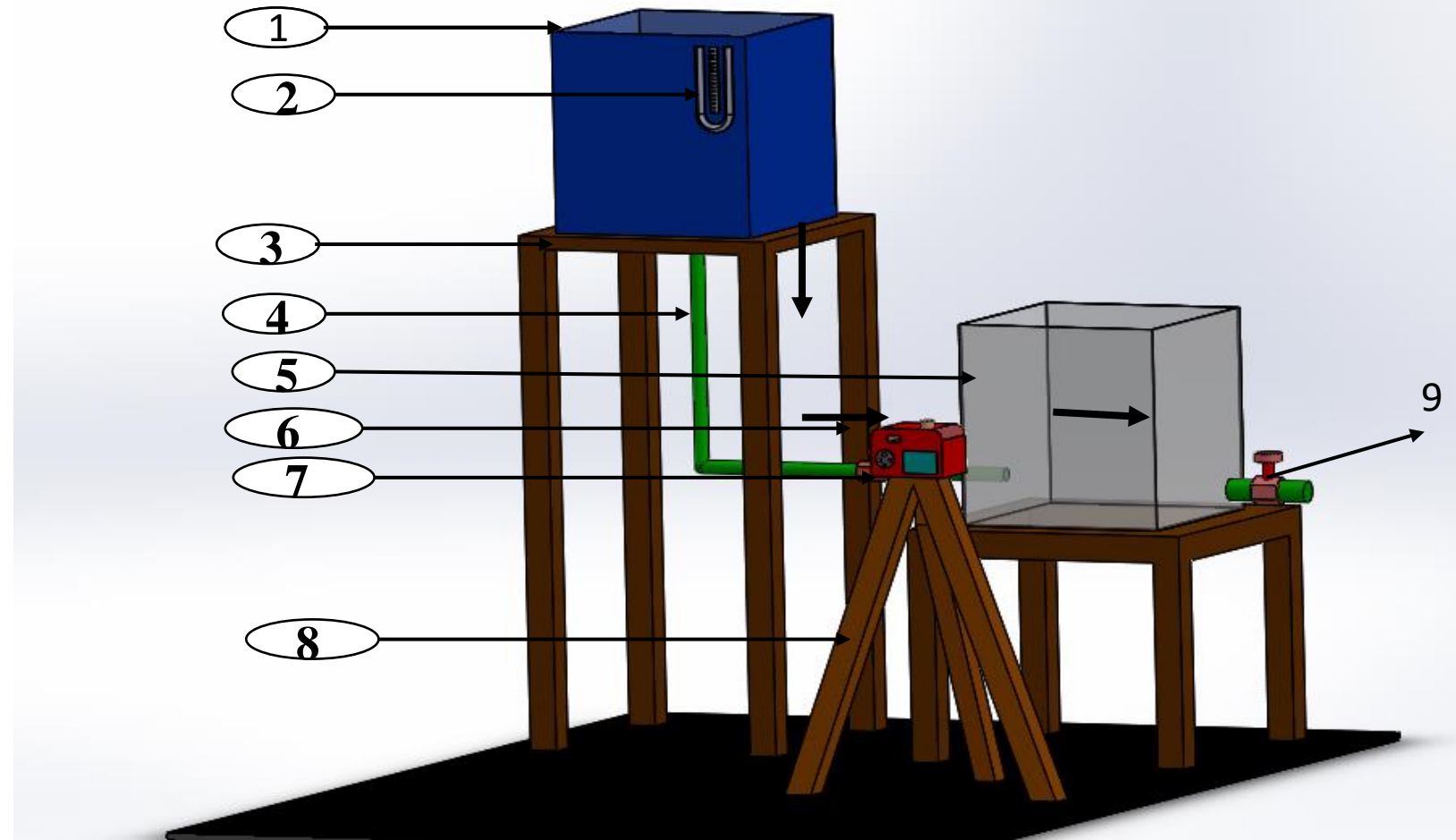


Figure 1: Schematic of experimental set up

# Formulae

- Flow rate (Q) = Area x Velocity ; where Area =  $\frac{\pi D^2}{4} m^2$  and Velocity =  $\frac{(initial - final)reading\ of\ peizometer}{total\ time\ taken} \frac{m}{s}$
- Velocity of Jet ( $V_{jet}$ ) =  $\left[ \left( \frac{D^2}{d^2} \right) \times \left( \frac{(initial - final)reading\ of\ peizometer}{total\ time\ taken} \right) \right] \frac{m}{s}$   
where D = Diameter of Dye Tank ,  
d = Diameter of Jet
- Reynold's Number (Re) =  $\frac{\rho v d}{\mu}$  ; where  $\rho$  = density of dye ink = 997 kg/m<sup>3</sup> at 25 °C  
v = velocity of jet (m/s)  
d = diameter of jet (m)  
 $\mu$  = Dynamic Viscosity of Dye ink (Pa.s)

# Result Comparison

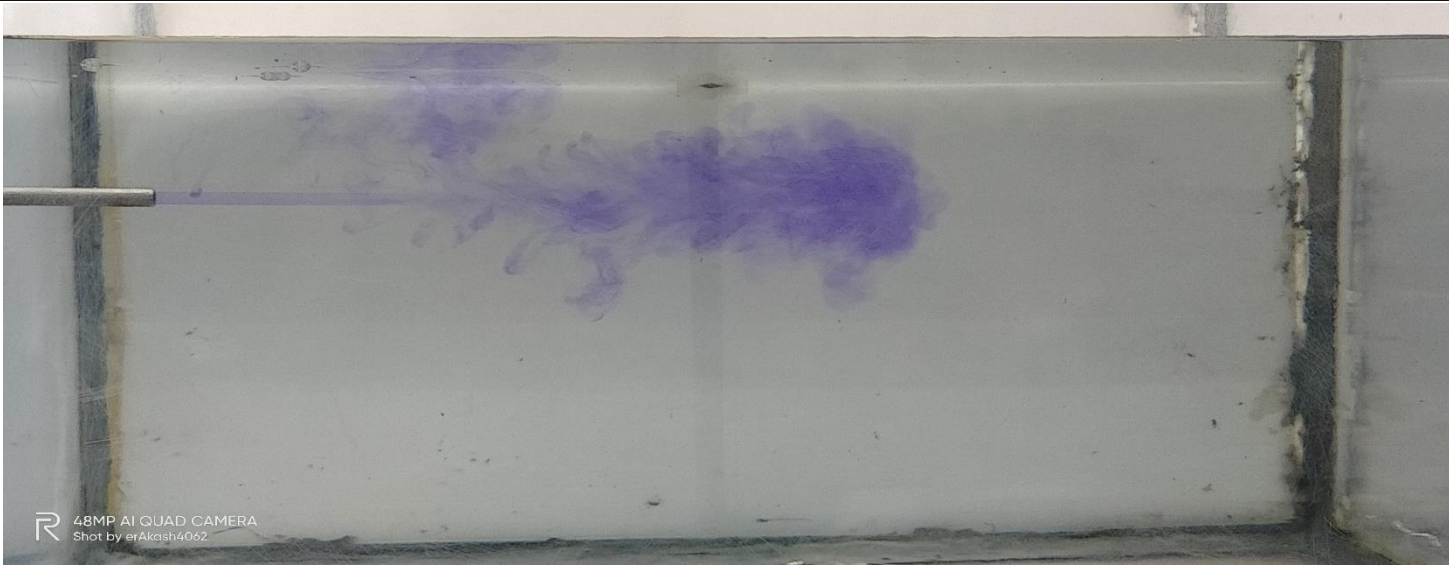


Fig.2. Submerged Free Jet

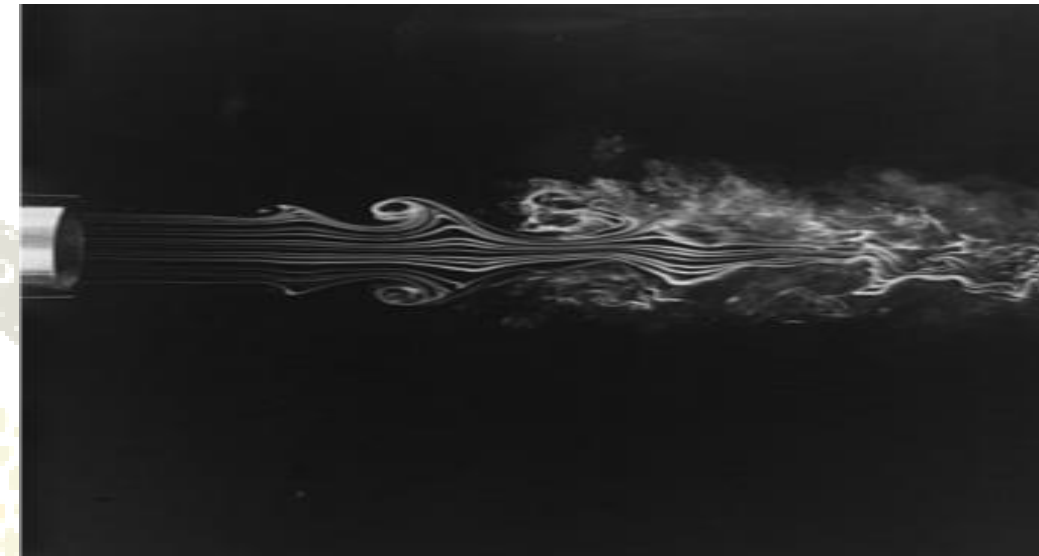


Fig.2. Free Jet

Image Source: C. Cornaro et al. / Experimental Thermal and Fluid Science 20 (1999)

- Non Eddying Jet rose into a vessel up to certain length and then it mushroomed or pedal breakdown takes place.
- Indication of higher Reynolds Number than 240.
- Dissipated Laminar Jet.



# Results

- Diameter of Jet = 8mm
- Viscosity =  $8.6840 \times 10^{-4} \text{ Pa}\cdot\text{s}$
- Density of Water =  $997 \text{ kg/m}^3$
- Flow Rate =  $5.3162 \mu\text{m}^3/\text{s}$
- Velocity =  $0.1058 \text{ m/s}$
- Reynolds Number = 1010.3
- Laminar Length = 9.59 cm

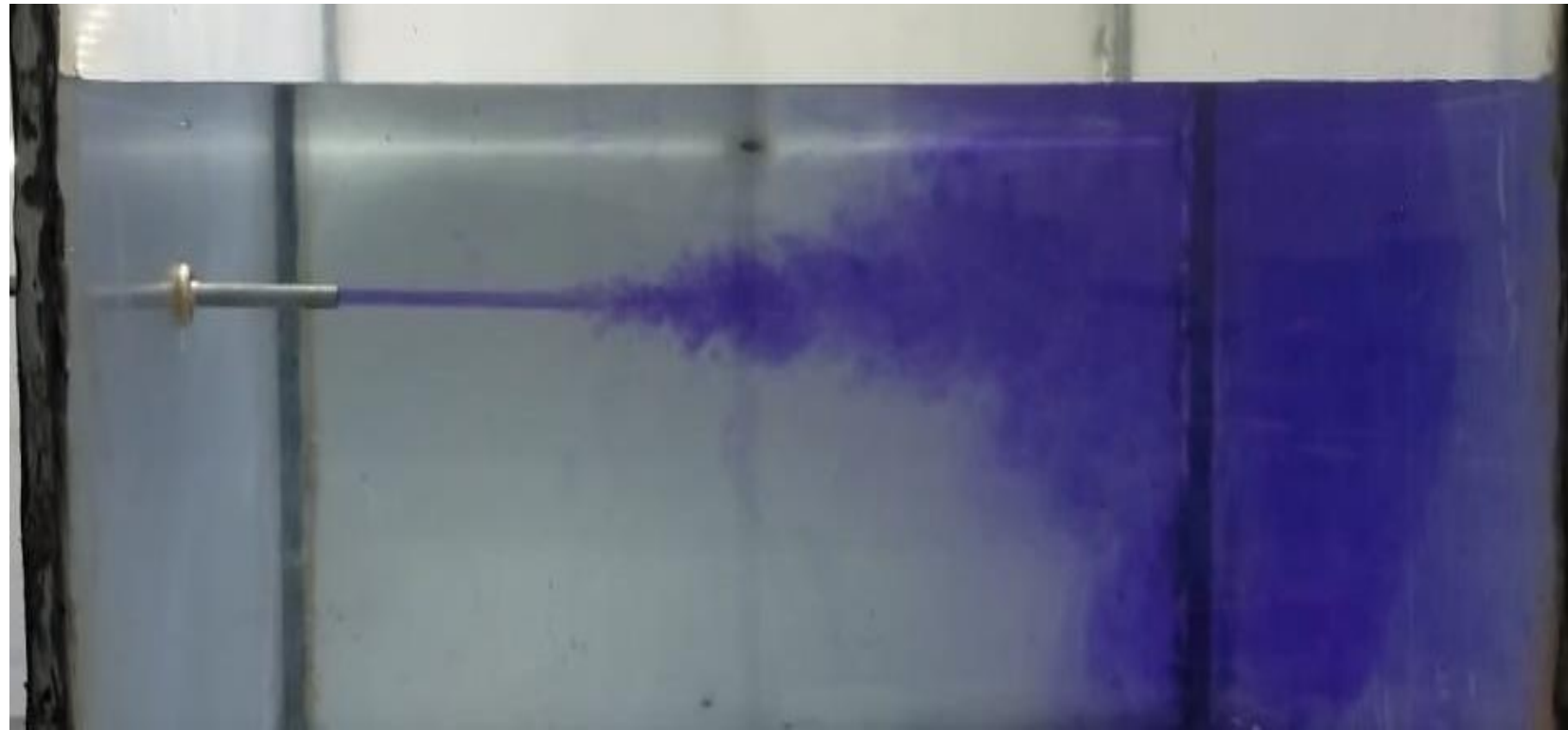


Fig.4. Laminar Jet at  $Re = 1010.3$

# Results

- Diameter of Jet = 8mm
- Viscosity =  $8.6840 \times 10^{-4} \text{ Pa}\cdot\text{s}$
- Density of Water =  $997 \text{ kg/m}^3$
- Flow Rate =  $2.8213 \mu\text{m}^3/\text{s}$
- Velocity =  $0.0563 \text{ m/s}$
- Reynolds Number = 514.3
- Laminar Length = 11.15 cm

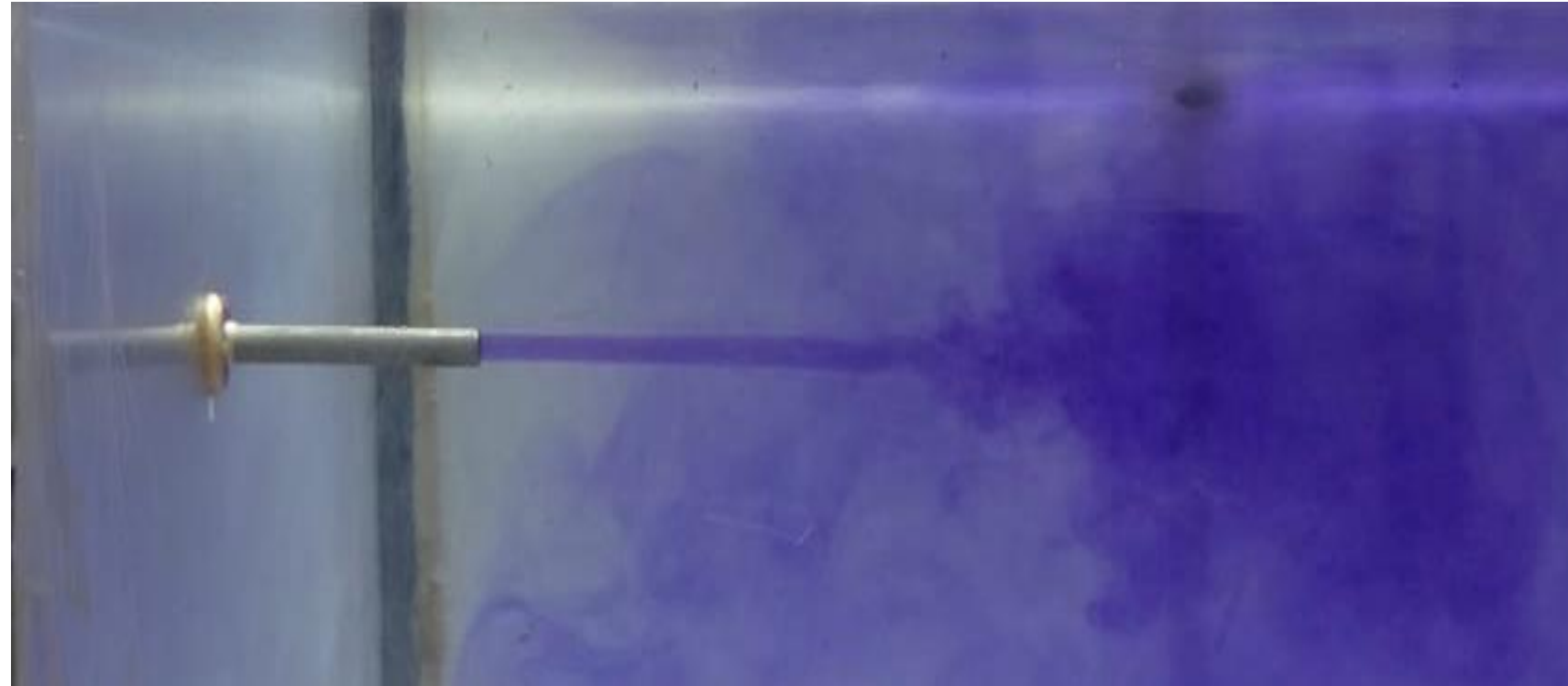


Fig.5. Laminar Jet at  $Re = 514.3$

# Results

- Diameter of Jet = 8mm
- Viscosity =  $8.6840 \times 10^{-4} \text{ Pa}\cdot\text{s}$
- Density of Water =  $997 \text{ kg/m}^3$
- Flow Rate =  $2.1551 \mu\text{m}^3/\text{s}$
- Velocity =  $0.0429 \text{ m/s}$
- Reynolds Number = 395
- Laminar Length = 18 cm

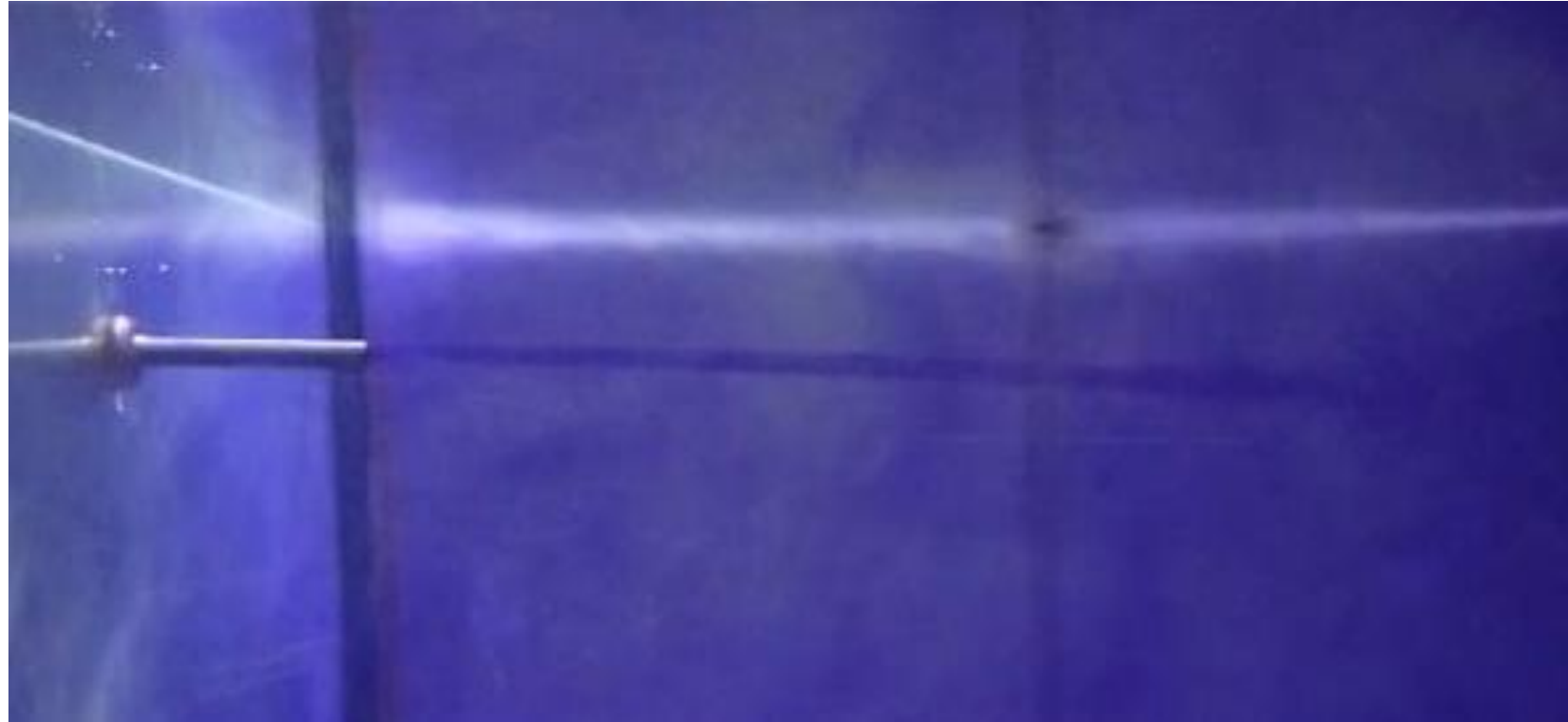


Fig.4. Laminar Jet at  $Re = 395$

# Uncertainty

- Uncertainty in Velocity( $\omega_v$ ):

$$\omega_v = \sqrt{\left(\frac{2D\Delta l}{d^2 t} \omega_D\right)^2 + \left(\frac{-2D^2\Delta l \omega_d}{d^3 t}\right)^2 + \left(\frac{D^2 \omega_L}{d^2 t}\right)^2 + \left(\frac{-D^2\Delta l \omega_t}{d^2 t^2}\right)^2} = \pm (2.6 \% - 8.3 \%)$$

where D = Diameter of Dye Tank (m),

d = Diameter of Jet (m) ,

$\Delta l$  = (*initial – final*)reading of peizometer (m)

t = total time taken (sec)

Here ,  $\omega_D = 1$  mm,  $\omega_L = 1$  mm,  $\omega_d = 1$  mm,  $\omega_t = 0.1$  sec.

- Uncertainty in Reynolds Number( $\omega_{Re}$ ) =  $\sqrt{\left(\frac{\rho d}{\mu} \omega_v\right)^2 + \left(\frac{\rho v}{\mu} \omega_d\right)^2} = \pm (10.3 \% - 14.5 \%)$ ,

where  $\rho$  = density of dye ink = 997 kg/m<sup>3</sup> ,  $v$  = velocity of jet (m/s)

d = diameter of jet (m) and

$\mu$  = Dynamic Viscosity of Dye ink (Pa.s)

# Conclusion

**For Low Jet Exit Velocity**



**Reynolds Number is Low, which indicate Laminar Region**

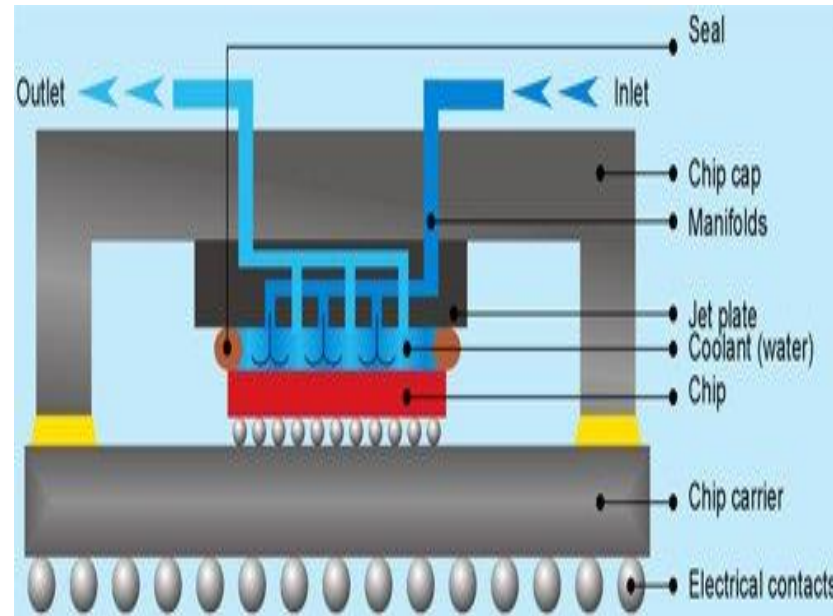


**As the Reynolds Number decreases, the Laminar Length Increases respectively**

# Applications



**Fig.1: Jet Blast Deflector**  
Image Courtesy: F-35C



**Fig.2: Cooling of Processors and IGBTs**  
Image Courtesy: Google



**Fig.3: Water Jet Cutting**  
Image Courtesy: Aqua technology



# Acknowledgement

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# Any Queries ???



Image Courtesy: FSSAI

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# Thank you



Image Courtesy: Julie Blais Comeau

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