

# Manual For Darcy Impes Leaching

## Before using the mobile immobile model and leaching chemical model

- please **TURN ON** the porosity on the pressure mesh (`/material_phase::Phase2/scalar_field::Porosity_pmesh`) and liquid viscosity on the pressure mesh (`/material_phase::Phase2/scalar_field::Viscosity_pmesh`)
- please **TURN ON** the field for average ore diameter (`/porous_media/scalar_field::Rock_diameter`)

### ❖ Mobile-Immobile model:

(1). **TURN ON**: `</material_phase::Phase2/MobileImmobileModel>`

(a). The immobile saturation and mass transfer coefficient between mobile and immobile phase could either be a prescribed field or calculated by an internal algorithm proposed by Lima (2006)[1].

(b). `tensor_field(Dispersivity_MIM)`:

- To include the dynamic dispersivity according to the dynamic liquid velocity, turn on this field and turn off the dispersivity of all of the scalar fields under this phase, the dispersivity is assumed to be same for all the scalar fields.
- Otherwise, turn off 'Dispersivity\_MIM' and include the dispersivity individually under each scalar field.
- There are two internal algorithms for the dynamic dispersivity, one is proposed by Lima (2006)[1]. Another one is fitted by the curve presented by Ilankoon (2012)[2]

(2). **Under EACH prognostic scalar field** of liquid phase,

(a). **TURN ON** the mass of this field in the stagnant region:

`</material_phase::Phase2/scalar_field/prognostic/scalar_field::Immobile>`

- `scalar_field(Average_mass)`: the average bulk concentration of this field
- `scalar_field(Mobile_ratio)` and `scalar_field(Immobile_ratio)`: is the weighting ratio of the mobile and immobile mass to the total mass

(b). IF there is the leaching chemical source term of this field, also **TURN ON**:

`<`

`/material_phase::Phase2/scalar_field/prognostic/LeachingChemicalSourceTerm/Mobile_Immobile_Model >` for chemical species OR `<`

`/material_phase::Phase2/scalar_field::Temperature/prognostic/leaching_temperature_source/Mobile_Immobile_Model >` for liquid temperature

- `scalar_field(Mobile_chemical_src)`: the chemical source term for mobile field (mass/m<sup>3</sup> mobile Liquid/s)
- `scalar_field(immobile_chemical_src)`: the chemical source term for immobile field (mass/m<sup>3</sup> immobile Liquid /s)

### ❖ Leaching chemical model:

#### (1). Mineral dissolution

(For chalcopurite and pyrite dissolution, two internal algorithms are available, Semi-empirical model and Shrinking core model)

(a).1. Semi-empirical model for chalcopyrite and pyrite Dissolution:

`reaction(CuFeS2_oxidation_aqueous_ferric_sulfate)` and

`reaction(FeS2_oxidation_aqueous_ferric_sulfate)`

- `scalar_field(dCuFeS2_dt)` and `scalar_field(dFeS2_dt)` is the mass conversion rate with the unite of (mol/m<sup>3</sup> heap/s)

- `scalar_field(extraction_rate)` is the conversion rate of the mineral with the unit ( $s^{-1}$ )
- `scalar_field(current_extraction)` is the current conversion of the mineral (-)
- `scalar_field(molar_concentration)` is the total molar mass of the mineral per volume of heap ( $\text{mol}/\text{m}^3$  heap), this is the initial mass available inside the heap before leaching.
- **experiment data:** the data from the semi-empirical lookup curve,  $\frac{d\varepsilon}{dt} \frac{1}{\eta_t \kappa} = f(\varepsilon)$ 
  - `number_of_data_points`: the total number of the point to interpolate the semi-empirical curve
  - `extraction`: the x axis of the semi-empirical curve,  $\varepsilon$ . Write down the corresponding value of each the data point
  - `empirical_extraction_rate_over_k`: the y axis of the semi-empirical curve,  $\frac{d\varepsilon}{dt} \frac{1}{\eta_t \kappa}$ . Write down the corresponding values of the each data point.
- **rate\_constant\_Arrhenius:** it is the reaction rate constant calculated by the Arrhenius equation. In semi-empirical model, it is the  $\kappa$  in the equation, which is from literature.
  - `scalar_field(prefactor)`: it is the prefactor  $k$  inside the Arrhenius equation, in semi-empirical model it is neglected (set as 1.0) since the pre-factor is neglected when calibrating the semi-empirical curve, the error of from the pre-factor can be cancelled as long as the same value of the pre-factor is used in the simulation with the one used in the calibration.
  - `activation_energy`: it is the activation energy of the corresponding reactions in the Arrhenius equation.
  - `gas_constant`:  $8.314 \text{ J}/(\text{K mol})$
- **bulk\_fluid\_conditions:** the dependence of the bulk concentrations in the Arrhenius equation, write down
  - `phase`: the material phase of that field (i.e. if it is in the liquid phase then write 2)
  - `order`: the order of the reaction in that field according to the Arrhenius equation (for example, the reaction rate of chalcopyrite dissolution is  $\kappa_{\text{CuFeS}_2} = 4\pi r^2 k e^{-E_a/RT} [\text{H}^+]^{0.8} [\text{Fe}^{3+}]^{0.42}$ , write down 0.42 for the order of bulk\_concentration(Fe3) and 0.8 for the bulk\_concentration(H))

(a).2. Shrinking core model for chalcopyrite and pyrite dissolution:

`reaction(CuFeS2_oxidation_aqueous_ferric_sulfate_SCM)` and  
`reaction(FeS2_oxidation_aqueous_ferric_sulfate_SCM)`:

This SCM model is based on the mathematical formulation proposed by Leahy et al.(2005)[3]. The value  $\tau_c$  and  $\tau_d$  in this model is calibrated by column experiment and directly written in the code. It requires to change the code if different values for  $\tau$  is to be used (for example different ore and leaching temperature).

(b). `reaction(S0_dissolution)`: elemental sulphur dissolution,  $\kappa_{\text{gangue}} = v_{\text{gangue}} C_{\text{H}^+}$

- `scalar(S0)`: the molar concentration of S0, ( $\text{mole}/\text{m}^3$  heap)
- `scalar_field(dS0_dt)`: change rate of the S0 concentration, ( $\text{mole}/\text{m}^3$  heap/s)
- `Dissolution_Algorithm(Non-bio_leaching)`: only the non-bioleaching algorithm is available, which linearly depends on the S0 formation from chalcopyrite dissolution,
  - `percentage_of_dissolve`: which indicate the percentage of the S0 formed from chalcopyrite dissolution are dissolved,  $v_{\text{gangue}}$ .
- `o2_name`: which is the scalar field name of the liquid oxygen in liquid phase.

- **H\_name**: which is the scalar field name of  $H^+$  in liquid phase.
- (c). **reaction(Gangue\_mineral\_acid\_dissolution)**:  $\kappa_{S_0} = 2v_{S_0}\kappa_{CuFeS_2}$  for  $v_{S_0} \in [0, 1]$
- **scalar\_field(dG\_dt)**: change rate of the gangue mineral concentration, (mole/m<sup>3</sup> heap/s)
  - **rate\_constant**: the gangue mineral dissolution is assumed to be under linear rate, please specify the rate constant of dissolution,  $v_{S_0}$ , (s<sup>-1</sup>)
  - **H\_name**: which is the scalar field name of  $H^+$  in liquid phase.

## **(2). Solution phase reactions**

- (a). **reaction(Ferrous\_Oxidation)**
- **scalar\_field(dFe2\_dt)**: the oxidation rate of Fe2, (mole/m<sup>3</sup> heap/s)
  - **Dissolution\_Algorithm(Non-bio\_leaching)**: the reaction rate is calculated by empirical Arrhenius equation
    - rate\_constant\_Arrhenius**: it is the reaction rate constant calculated by the Arrhenius equation
    - scalar\_field(prefactor)**: it is the prefactor  $k$  inside the Arrhenius equation
    - activation\_energy**: it is the activation energy of the corresponding reactions in the Arrhenius equation.
    - gas\_constant**: 8.314 J/(K mol)
  - **bulk\_fluid\_conditions**: the dependence of the bulk concentrations in the Arrhenius equation, write down
    - name**: the corresponding scalar field name of the reactant that is in the Arrhenius equation (could be a name that is different from the name in the Arrhenius equation but it should be the same name given to the prognostic scalar field. )
    - phase**: the material phase of that field (i.e. if it is in the liquid phase then write 2)
    - order**: the reaction order of that reactant.
- ✓ **Dissolution\_Algorithm(bio\_leaching)**: this is the bio-leaching algorithm for ferrous oxidation and it will be explained in a separate part below.
- (b). **reaction(Jarosite\_Precipitation)**: the algorithm is based on Leahy and Schwarz (2009)[4],  
 $\kappa_{jarosite} = v_{jarosite} [Fe^{3+}]$   
 if  $\log_{10}(0.056[Fe^{3+}]) > -1.43pH + 0.87$
- **scalar\_field(dM\_dt)**: precipitation rate of Fe3+ by jarosite (mole/ m<sup>3</sup> heap/s)
  - **scalar\_field(molar\_concentration)**: the current molar concentration of jarosite, (mol/ m<sup>3</sup> liquid solution)
  - **H\_name**: The scalar filed name for  $H^+$  in Phase 2 used to calculate pH
  - **Fe3\_name**: The scalar filed name for Fe3 in Phase 2 used to calculate jarosite precipitation
  - **rate\_constant**: The jarosite precipitation rate constant, which is a linear constant ,  $v_{jarosite}$
- (c). **reaction(Oxygen\_dissolution)**: the equilibrium algorithm based on Tromans (1998)[5]
- **scalar\_field(dOg\_dt)**: the change rate of gas oxygen (mole/ m<sup>3</sup> of heap/s)
  - **scalar\_field(molar\_concentration)**: the current molar concentration of jarosite (mol/ m<sup>3</sup> liquid solution)
  - **og\_name**: The scalar filed name for gas phase oxygen in Phase 1
  - **o2\_name**: The scalar filed name for liquid phase oxygen in Phase 2

### (3) heat transfer model

- (a). [single\\_phases\\_heat\\_transfer](#): only calculate the heat change of the liquid phase
- (b). [two\\_phases\\_heat\\_transfer](#): the heat generations by solution phase reactions are added to liquid phase temperature, while the heat generations by mineral dissolutions are added to rock temperature.

- [scalar\\_field\(Rock\\_Temperature\)](#): the rock temperature which is calculated by a conduction equation with the source terms from dissolution reactions and liquid-solid heat transfers. (unite: k)
- [scalar\\_field\(Rock\\_density\)](#): in  $\text{kg/m}^3$
- [scalar\\_field\(Rock\\_Cp\)](#): heat capacity of the rock,  $\text{kJ/kg/k}$
- [heat transfer sources](#): the source terms of the rock temperature
  - i. [scalar\\_field\(solid\\_liquid\\_heat\\_transfer\\_rock\\_phase\)](#), it is the heat transfer from the rock to liquid.  $[-\Delta H = h_t a_t (T_r - T_l)]$ , unite: (k/s)
    - [scalar\\_field\(K\\_eff\\_sl\)](#): effective heat transfer coefficient between solid and liquid, ( $\text{kw/k/m}^3$ ),  $h_t a_t$ . Either using a [prescribed](#) value OR [diagnostic](#) field by using an internal algorithm.
  - ii. [scalar\\_field\(mineral\\_dissolution\\_heat\\_sources\)](#): unite is  $(\text{k/s}) * (\text{m}^3_{\text{rock}} / \text{m}^3_{\text{heap}})$ 
    - please **SELECT** the mineral dissolutions which can generate heat to the rock, and specify the [enthalpy](#) (KJ/mol) of each reaction

✓ If using the **heat transfer model**, please TURN ON the liquid temperature under phase 2, `</material_phase::Phase2/scalar_field::Temperature>`  
AND  
TURN ON  
`</material_phase::Phase2/scalar_field::Temperature/prognostic/leaching_temperature_sources>`

- [scalar\\_field\(Liquid\\_Cp\)](#): liquid heat capacity,  $\text{kJ/Kg/K}$
- [heat transfer sources](#):
  - i. [scalar\\_field\(solid\\_liquid\\_heat\\_transfer\\_rock\\_phase\)](#), it is the heat transfer from the rock to liquid. k/s
  - ii. [scalar\\_field\(solution\\_phase\\_heat\\_sources\)](#): unite is  $(\text{k/s}) * (\text{m}^3_{\text{liquid}} / \text{m}^3_{\text{heap}})$ 
    - please **SELECT** the solution phase reactions which can generate heat to the rock, and specify the [enthalpy](#) (KJ/mol) of each reaction

- (4). **Liquid solid wetting efficiency**: please TURN ON it IF using heat transfer model and semi-empirical model.

- [scalar\\_field\(Wetting\\_efficiency\)](#): it is the non-dimentional parameter. It is calculated by the algorithm from Al-Dahhan and Dudukovic (1995)[6].

### When using leaching chemical model, under EACH prognostic field of the solutes (including Og in phase 1):

- (1). TURN ON <

`/material_phase::Phase2/scalar_field/prognostic/LeachingChemicalSourceTerm >`

- According to the equations of chemical reactions, **SELECT** the corresponding solution phase or/and mineral dissolution reactions which can change the value of this scalar field. Write down the [stoichiometric factor](#) of this field in the reaction equation (positive if on the left hand side, negative if on the right hand side).

❖ **Bioleaching model for ferrous oxidation:**

The bioleaching model is based on the model proposed by Leahy et al.(2005)[3]

(1). Under Phase 2, **TURN ON** the fields **phi\_1** (now it supports 3 different phi\_1, it could be extended to include more phi, and it is not necessary to turn on all of the phi), phi\_1 is  $\varphi_i$  in the bioleaching model.

(2). **TURN ON** <

/Leaching\_chemical\_model/SolutionPhaseReactions/reaction::Ferrous\_Oxidation/Dissolution\_Algorithm::bio\_leaching >

(a). **TURN ON** the corresponding **scalar\_field(phi\_1)** under the bio\_leaching algorithm, (e.g, phi\_12 under the phase 2, then turn on phi\_12 under the bio\_leaching model)

(b). **TURN ON** the corresponding **scalar\_field(miu)** under the bio\_leaching algorithm, (e.g, phi\_12 under the phase 2, then turn on miu2 under the bio\_leaching model) , miu is  $\mu$  in the model.

i. **k1**: rate constant of attachment

ii. **k2**: rate constant of detachment

iii. **k\_death**: death rate constant

iv. **phi\_max**:  $\Psi_{\max}$

v. **miu\_max**:  $\mu_{\max}$

vi. **T\_shift**:  $T_{\text{shift},i} = T_{\text{optimal},i} - T_{\text{optimal},1}$

(c). **Y**: yield coefficient

(d). **kmo**: Monod parameter for oxygen

(e). **kmfe2**: Monod parameter for ferrous ions

(f). **ferrous\_name**: the name of the scalar field of Fe2 in liquid phase

(g). **oxygen\_name**: the name of the scalar field liquid phase oxygen

- [1] L. R. P. de Andrade Lima, "Liquid axial dispersion and holdup in column leaching," *Miner. Eng.*, vol. 19, no. 1, pp. 37–47, Jan. 2006.
- [2] I. Ilankoon, "Hydrodynamics of unsaturated particle beds pertaining to heap leaching," 2012.
- [3] M. J. Leahy, M. R. Davidson, and M. P. Schwarz, "A model for heap bioleaching of chalcocite with heat balance: Bacterial temperature dependence," 2005.
- [4] M. Leahy and M. Schwarz, "Modelling jarosite precipitation in isothermal chalcopyrite bioleaching columns," *Hydrometallurgy*, 2009.
- [5] D. Tromans, "Oxygen solubility modeling in inorganic solutions: concentration, temperature and pressure effects," *Hydrometallurgy*, 1998.
- [6] M. Al-Dahhan and M. Duduković, "Catalyst wetting efficiency in trickle-bed reactors at high pressure," *Chem. Eng. Sci.*, 1995.