

# Effect of equivalence ratio on flame temperature and exhaust composition of ethane-air & methane-air mixtures

Computational Methods in Combustion

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#### 1 Introduction

### 1.1 Description

The equivalence ratio is a dimensionless parameter used in combustion analysis to compare the actual fuel-air ratio to the stoichiometric fuel-air ratio and is defined as their quotient:

$$\phi = \frac{(F/A)_a}{(F/A)_s}$$

Let us note that:

- when  $\phi = 1$ , the mixture is stoichiometric, meaning there is exactly enough oxygen to completely combust the fuel;
- when  $\phi < 1$ , the mixture is lean, meaning there is excess air (or oxygen) relative to the amount of fuel;
- when  $\phi > 1$  the mixture is rich, meaning there is excess fuel relative to the amount of air (or oxygen).

This work aims to present the effect of the equivalence ratio on the adiabatic flame temperature and mass fractions of the main exhaust components of two combustible mixtures - ethane- and methane-air mixture.

## 1.2 Stoichiometric equations

Stoichiometric equation for methane-air combustion is given as follows:

$$CH_4 + 2(O_2 + 3.76N_2) \longrightarrow CO_2 + 2H_2O + 7.52N_2$$

Similarly, for ethane-air mixture:

$$C_2H_6 + \frac{7}{2}(O_2 + 3.76N_2) \longrightarrow 2CO_2 + 3H_2O + 13.16N_2$$

#### 1.3 Initial conditions

$$p = 101325 \ Pa$$

$$T = 298.15 \ K$$

# 2 Method description

The code simulates the combustion of ethane and methane, calculating the adiabatic flame temperature and equilibrium composition for different equivalence ratios  $(\phi)$ . It uses the Cantera library for combustion modeling and NumPy and Matplotlib for computations and plotting. It loads gas mixture data from the gri30.yaml file, sets gas compositions, and performs adiabatic equilibrium at constant pressure. The calculate\_adibatic\_flame\_temp function generates data on flame temperature and chemical composition. Then, the plot\_species\_mass\_fractions and plot\_adibatic\_flame\_temp functions create plots of mass fractions of selected chemical species and flame temperature as a function of phi. The final functions, make\_calc\_for\_ethane and make\_calc\_for\_methane, perform these calculations and create plots for ethane and methane, saving the results to graphic files and displaying them.

# 3 Results

# 3.1 Methane mixture

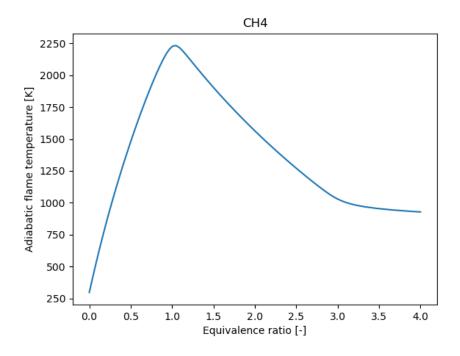


Figure 1: Methane flame temperature as a function of the equivalence ratio

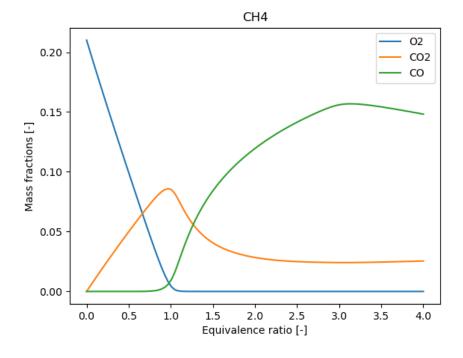


Figure 2: Methane exhaust components as a function of the equivalence ratio

## 3.2 Ethane mixture

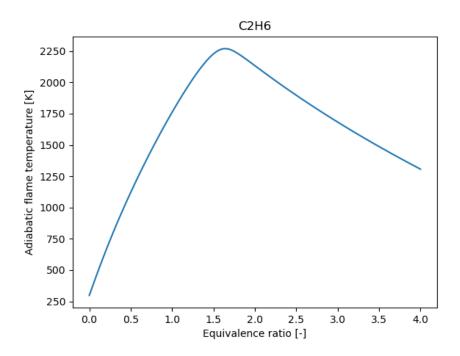


Figure 3: Ethane flame temperature as a function of the equivalence ratio

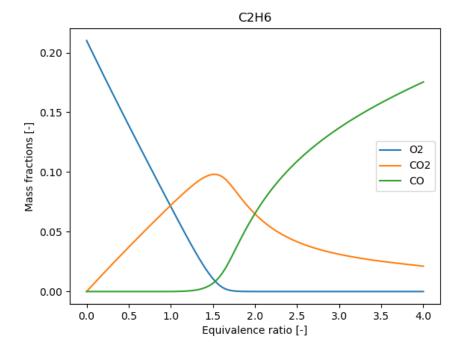


Figure 4: Ethane exhaust components as a function of the equivalence ratio

# 4 Conclusions

- When the equivalence ratio is small (<<1), the percentage of  $O_2$  in the exhaust components is very high, as not all of the fuel gets consumed in the combustion process.
- With  $\phi$  approaching 1, the amount of  $O_2$  drops significantly, quickly approaching 0 as  $\phi$  exceeds the value of 1.
- On the contrary, the percentage of CO is negligible when  $\phi < 1$  and rises drastically once the ratio reaches 1 for methane and approximately 1.5 for ethane. This happens because a lean mixture allows the fuel to be more completely combusted.
- The highest temperature is similar for both methane and ethane (around 2250K), however, for methane it is reached for a lower equivalence ratio about 1 for methane and 1.5 for ethane. The highest combustion temperature typically occurs when the mixture is stoichiometric because the fuel and oxygen are perfectly balanced for complete combustion.
- The  $CO_2$  concentration peaks at around the same equivalence ratio as the highest methane or ethane temperature respectively.
- At  $\phi$  < 1 the combustion temperatures are generally lower because the excess air absorbs heat, leading to cooler combustion products.
- When  $\phi > 1$ , combustion temperatures are also lower compared to the stoichiometric case because the excess fuel consumes heat to vaporize and partially oxidize

#### 5 References

- Plastics to Energy, Chapter 10 (Gasification of Plastic Solid Waste and Competitive Technologies) S.A. Salaudeen, Animesh Dutta
- Effect of Equivalence Ratio on Pollutant Formation in CH4O/H2/NH3 Blend Combustion Jingyun Sun, Qianqian Liu
- https://en.wikipedia.org/wiki/Methane
- https://en.wikipedia.org/wiki/Ethane
- https://github.com/Justyna349/mkws

## 6 Python code

```
import cantera as ct # Cantera library for combustion simulations
  import numpy as np # Numerical Python library for mathematical operations
  import matplotlib.pyplot as plt # Library for creating plots
  # Load the gas mixture from the gri30 database
  gas = ct.Solution("gri30.yaml")
  def calculate_adibatic_flame_temp(fuel_species, phi_min, phi_max, npoints, T, P):
      Calculate adiabatic flame temperature and equilibrium composition for a given fuel.
      fuel_species (str): The chemical formula of the fuel (e.g., 'C2H6' for ethane).
      phi_min (float): The minimum equivalence ratio.
      phi_max (float): The maximum equivalence ratio.
12
      npoints (int): The number of points to calculate between phi_min and phi_max.
14
      T (float): Initial temperature of the gas mixture.
      P (float): Initial pressure of the gas mixture.
16
      Returns:
17
      tuple: Arrays of equivalence ratios, adiabatic flame temperatures, and equilibrium compositions.
20
      # Indices for the fuel, oxygen, and nitrogen species
21
      ifuel = gas.species_index(fuel_species)
      io2 = gas.species_index("02")
22
      in2 = gas.species_index("N2")
23
24
      # Air composition: Nitrogen to Oxygen ratio
25
      air_N2_02_ratio = 3.76
26
27
      # Calculate stoichiometric oxygen needed for the fuel
28
      if fuel_species == 'C2H6':
29
          stoich_02 = 2 * gas.n_atoms(fuel_species, "C") + 0.25 * gas.n_atoms(fuel_species, "H")
30
      elif fuel_species == 'CH4':
31
          stoich_02 = gas.n_atoms(fuel_species, "C") + 0.25 * gas.n_atoms(fuel_species, "H")
35
33
      # Create arrays to store equivalence ratios, temperatures, and compositions
34
35
      phi_values = np.linspace(phi_min, phi_max, npoints)
      tad = np.zeros(npoints)
36
37
      xeq = np.zeros((gas.n_species, npoints))
38
39
      # Loop over each equivalence ratio
40
      for i, phi in enumerate(phi_values):
          # Set the composition of the gas mixture
41
          X = np.zeros(gas.n_species)
42
43
          X[ifuel] = phi # Fuel mole fraction
          X[io2] = stoich_02 # Oxygen mole fraction
44
          X[in2] = stoich_02 * air_N2_02_ratio # Nitrogen mole fraction
45
46
          # Set the gas state: temperature, pressure, and composition
47
          gas.TPX = T, P, X
48
          # Equilibrate the mixture adiabatically at constant pressure
49
50
          gas.equilibrate("HP")
51
          # Store the adiabatic flame temperature and equilibrium composition
          tad[i] = gas.T
          xeq[:, i] = gas.X
54
          print(f"At phi= {phi:.4f} Tad = {gas.T:.4f}")
56
57
      return phi_values, tad, xeq
  def plot_species_mass_fractions(fuel_species, phi_values, xeq, species_names):
60
      Plot the mass fractions of selected species against the equivalence ratio.
61
62
      Parameters:
      fuel_species (str): The chemical formula of the fuel.
63
      phi_values (array): Array of equivalence ratios.
64
      xeq (array): Array of equilibrium compositions.
65
      species_names (list): List of species names.
66
67
      # Select species to plot
68
      for species in ["02", "C02", "C0"]:
```

```
if species in species_names:
 71
                index = species_names.index(species)
                plt.plot(phi_values, xeq[index, :], label=species)
72
 73
       plt.xlabel("Equivalence ratio [-]")
 74
75
       plt.ylabel("Mass fractions [-]")
       plt.legend(loc="best")
 76
77
       plt.title(fuel_species)
 78
       plt.savefig(f'mass_fractions_{fuel_species}.png')
 79
       plt.show()
80
81
   def plot_adibatic_flame_temp(fuel_species, phi_values, tad):
82
       Plot the adiabatic flame temperature against the equivalence ratio.
83
84
       Parameters:
85
       fuel_species (str): The chemical formula of the fuel.
 86
       phi_values (array): Array of equivalence ratios.
       tad (array): Array of adiabatic flame temperatures.
87
       plt.plot(phi_values, tad)
89
90
       plt.xlabel("Equivalence ratio [-]")
       plt.ylabel("Adiabatic flame temperature [K]")
91
       plt.title(fuel_species)
92
       plt.savefig(f'flame_temp_{fuel_species}.png')
93
94
       plt.show()
95
   def make_calc_for_ethane():
96
97
98
       Perform calculations and plots for ethane ({\tt C2H6}).
90
       # Parameters for ethane
       fuel_species = "C2H6"
101
       phi_min = 0.3
       phi_max = 4
       npoints = 100
104
       T = 298.15 # Initial temperature in Kelvin
       P = 101325.0 # Initial pressure in Pascals
106
107
       # Calculate adiabatic flame temperature and equilibrium composition
108
       phi_values, tad, xeq = calculate_adibatic_flame_temp(fuel_species, phi_min, phi_max, npoints, T, P)
109
       # Plot results
       plot_species_mass_fractions(fuel_species, phi_values, xeq, gas.species_names)
       plot_adibatic_flame_temp(fuel_species, phi_values, tad)
112
   def make_calc_for_methane():
114
115
       Perform calculations and plots for methane (CH4).
116
117
       # Parameters for methane
119
       fuel_species = "CH4"
120
       phi_min = 0.3
       phi_max = 4
121
       npoints = 100
122
       T = 298.15 # Initial temperature in Kelvin
124
       P = 101325.0 # Initial pressure in Pascals
125
       # Calculate adiabatic flame temperature and equilibrium composition
126
127
       phi_values, tad, xeq = calculate_adibatic_flame_temp(fuel_species, phi_min, phi_max, npoints, T, P)
       # Plot results
       plot_species_mass_fractions(fuel_species, phi_values, xeq, gas.species_names)
129
130
       plot_adibatic_flame_temp(fuel_species, phi_values, tad)
131
   # Perform calculations and plots for ethane
   make_calc_for_ethane()
133
   # Perform calculations and plots for methane
135
make_calc_for_methane()
```