



A numerical study of bend-induced particle deposition in and behind duct bends

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ARTICLE INFO

Article history:

Received 24 October 2011

Received in revised form

14 December 2011

Accepted 15 December 2011

Keywords:

Particle

Bend

Deposition ratio

Deposition velocity

Enhancement factor

New decay equation

ABSTRACT

This paper investigated the microparticle deposition and distribution due to the presence of duct bends by employing the Eulerian approach with Reynolds stress turbulent model and a Lagrangian trajectory method. The air velocity, particle velocity and particle deposition velocity were validated with available experimental data. Several particle deposition ratios were proposed to describe the particle accumulation due to bends. Particle deposition velocities in and behind bends were analyzed numerically. It is found that bend walls with surfaces of higher capture velocity tend to accumulate more contaminant particles as seen with an increased factor of 1.2 times on particle deposition velocity. Particle deposition reaches a maximum value near bend outlet, e.g. 15.2 times deposition ratio for particles of $d_p = 23 \mu\text{m}$, and decay exponentially to a status of fully developed deposition in approximately $10D$ length. Compared to traditional consideration of sole deposition in bends, a new general concept of total deposition including that in bends and behind bends is proposed to better describe the particle deposition induced by bends since the enhancement deposition ratios behind bends compose 42–99% in the total ratios for particles of $d_p = 3\text{--}23 \mu\text{m}$. Furthermore, models of fast power and exponential decay trend are demonstrated to uncover the relationship among enhancement factor of deposition velocity behind bend, dimensionless distance behind bends and particle Stokes number. The present study can contribute to the understanding and controlling of contaminant aerosol flow behavior in ducts, e.g. particle sampling, removal and associated epidemiologic study between particle and human health.

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1. Introduction

Contaminant particles suspending in a room may cause health problems to the occupants [1–5], for example, robust associations between ambient PM concentrations and human morbidity and mortality [6] and the transmission of severe acute respiratory syndrome (SARS) [7]. Nowadays, to provide a comfortable built environment, central ventilation systems are commonly installed in modern commercial, institutional and public buildings, and therefore the ventilation ducts become one main way to transport particle-laden airflow [8]. In real ventilation ducts, one of the main parts is the bend for flow direction adjustment and pollutant aerosol deposition [9]. Additionally, there are other practical applications of particle flowing through bends, including the removal of particulates from industrial duct bends [10] and extractive sampling of pollutants in gas flow [11,12].

To construct the ventilation ducts, many kinds of materials can be adopted [13,14]. Several kinds of steel and aluminum with

different coatings are used widely, and materials with special usage such as plastic, glass and masonry could also be found. Construction materials of ducts play significant roles in ventilation systems [13,15]. In previous research, however, only Sippola and Nazaroff [16] investigated the deposition in 90° ventilation bends related to typical commercial or public mechanical ventilation systems. Peters and Leith [10] studied industrial pipe bends with grease coating which was assumed to capture all particles approaching it. In the reported studies of McFarland et al. [11] and Pui et al. [12], the deposition surface materials were not considered. Few research was conducted to investigate the particle distribution and deposition in 90° bends regarding different wall materials.

In view of the experimental approach, particle distribution and deposition are affected by many factors [17–19], hence the experimental analysis of the particle behavior throughout duct bends becomes quite challenging. The other method, computational fluid dynamics (CFD), has become an efficient and robust tool to investigate the airflow and particle behavior in ventilation ducts according to previous studies [20–23]. However, little research adopted the CFD method including a discrete trajectory approach to study particle deposition and distribution throughout bends. In our previous studies [24,25], the CFD approach together with an

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improved particle–wall impact model was successfully applied to predict the particle distribution and deposition in 90° bends.

Furthermore, experimental studies of the enhanced particle deposition behind bends have been reported recently [16,26]. Miguel et al. [26] conducted the study of aerosol deposition and distribution in bifurcating duct system which corresponded to human respiratory system. It was found that particles accumulated mainly around the bend segment. Sippola and Nazaroff [16] investigated the mechanical ventilation system with bends and reported sharp increase of deposition velocity behind a bend about one to two order of magnitude. However, related research about the sole bend effect on the succeeding long straight duct was seldom found.

Therefore, this work aims to further study the particle deposition and distribution caused by bends by initiating the concept of deposition ratio and enhancement factor. The airflow phase and particle phase are solved by the Eulerian method with Reynolds Stress turbulent model and a Lagrangian discrete tracking approach with a particle–wall collision model, respectively. The improved CFD approach is then used to analyze the particle deposition ratio, deposition velocity and associated distributions inside and behind bends. In these perspectives, four demonstrating decaying equations are proposed to describe the enhanced deposition behind bends.

2. Research methods

2.1. Air phase model

The air phase which was governed by Eulerian conservation equations was predicted by employing the generic CFD approach, FLUENT [27]. The Reynolds stress model (RSM) was adopted to solve the airflow turbulence along with two-layer enhanced-wall model. This is attributed to the reason that this RSM model performs reasonably well for two-dimensional flows [28] because it accounts for the effects of curvature, swirl and rotation and can resolve the near-wall flow features. The ability of this model together with two-layer model has been verified clearly to prediction particle deposition in straight ducts accurately [29].

The flow boundary conditions were given as follows. At the flow outlet, Neumann boundary condition was adopted, i.e. mass conservation conditions for velocities and zero gradient boundary conditions for other variables. The duct walls were assumed to be smooth. In order to impose fully developed turbulence profile, the velocity profiles at flow inlet of y direction were defined according to the following 1/7th power law equations,

$$U = U_{\infty} \left(\frac{x_D}{D/2} \right)^{1/7} \quad (1)$$

$$U_{\infty} = \frac{8}{7} U_{ave} \quad (2)$$

Where U_{ave} is the averaged velocity in the straight duct before bend, D is the cross dimension accordingly and x_D is nearest distance from one of the two inlet duct walls. The turbulent kinetic energy k was given as,

$$k = \frac{\tau_w}{\rho_a \sqrt{C_0}} + \frac{x_D}{D/2} \left(0.002 U_{\infty}^2 - \frac{\tau_w}{\rho_a \sqrt{C_0}} \right) \quad (3)$$

$$\tau_w = \frac{\rho_a U_{\infty}^2}{2} \cdot f \quad (4)$$

Where ρ_a is the air density, the constant C_0 equals 0.09 and f is the fanning friction factor. This inlet condition was integrated into the CFD code by programming a user-defined function (UDF).

With regard to numerical scheme, the finite volume method (FVM) together with SIMPLE algorithm [30] was adopted within the CFD code. The RSM model employed the second-order upwind scheme for all the variables except pressure. The discretization of pressure was based on a staggered PRESTO! scheme [27]. Scaled convergent residuals were less than 10^{-5} for velocity components, turbulent quantities and Reynolds stress variables.

2.2. Particle phase model

The solid and spherical particle flow was assumed to be diluted enough to ignore the interaction of particle to particle and particle to air. Therefore, all the computational results were obtained by utilizing one-way coupling method. Depending on these assumptions [9], the Lagrangian formulations of particle motion were formed as follows,

$$\frac{du_{pi}}{dt} = F_D(u_i - u_{pi}) + g_i \left(1 - \frac{\rho_a}{\rho_p} \right) + F_{ai} \quad (5)$$

Where u_{pi} stands for particle velocity in the i th direction (m/s) and u_i is the air velocity. The first term on the right is the drag forces exerted on the particle (per unit particle mass) in the i th direction (m/s^2), and the second one is the gravitational force per unit particle mass. The third term means other potential forces. These forces were studied by Zhao et al. [22], and Saffman force was suggested to be important for large particles. Therefore, only this lift force was added into the third term of Eq. (5). Since the particle motion trajectory can be influenced by the instantaneous fluctuating airflow velocity, 'Eddy lifetime' model was utilized [31].

2.3. Particle–wall impact model

This particle–wall impact model initiated by Brach and Dunn [15] accounts for the particle–wall interaction including material dissipation, friction and adhesion in a convenient algebraic formula. The coefficient of restitution, e , can be written as follows,

$$e = \frac{v_{2,n}^p}{v_{1,n}^p} = R_{pw} (1 - \rho_{pw}) \quad (6)$$

Where, $v_{1,n}^p$ and $v_{2,n}^p$ are particle normal incident and reflected velocities, respectively, R_{pw} for the coefficient of restitution without adhesion, ρ_{pw} as the coefficient of adhesion. If this coefficient satisfies the relation $\rho_{pw} = 1$, particles will be all trapped on a surface; if R_{pw} equals 0, it means there is no adhesion effect. These two coefficients can be expressed as,

$$R_{pw} = \frac{\kappa^a}{\kappa^a + |v_{1,n}^p|^a} \quad (7)$$

$$\rho_{pw} = \frac{l^b}{l^b + |v_{1,n}^p - v_c|^b} \quad (8)$$

where, the parameters κ , l , a , b , and v_c (capture/critical velocity) are determined by experimental method [15].

Due to the limited numbers of experimental surfaces, only three types of experimental surfaces were selected to analyze the material effect on particle deposition and distribution near the wall surfaces. These surface parameters are listed in Table 1. The capture velocities for the three pairs of copper, mica and molybdenum surfaces are 0.29, 1.10 and 1.47 m/s respectively. It means that the particle motion near copper surface possesses the lowest capture

Table 1
Condition and information for example particle impacts [15].

Particle diameter (μm)	Particle material	Surface material	k	l	a	b	v_c (m/s)
8.6 [1–30]	Ag-coated glass	Copper	38.7	1.61	1.0	1.0	0.29
3–7	Ammonium fluorescein	Mica	72.5	1.333	1.0	1.0	1.10
	Ammonium fluorescein	Molybdenum	55.7	0.586	1.0	1.0	1.47

velocity and that near molybdenum hold the highest. The particles are assumed to be captured on a surface if the incident normal velocity falls below the capture velocity. To incorporate the particle–wall impact model into the CFD code, a UDF program in bends was developed.

Three particle size groups (3, 5 and 7 μm) were studied with three different surface materials to conduct material comparisons considering the available narrow range (3–7 μm) of particle diameter provided by existing experimental data [15]. For copper surface, another four particle sizes (10, 16, 20 and 23 μm) were also investigated to estimate the particle deposition velocity, and to compare the prediction result with available experimental data.

2.4. Particle deposition analysis in bends

This study presented the following two methods for the investigation of the particle deposition results in bends:

- 1) By demonstrating the particle deposition amount at different reflection angle from $\theta = 0^\circ$ to 90° . The deposited particle number $N_{d\theta}$ from the bend entrance to a specific angle θ was expressed as,

$$N_{d\theta} = N_0 - N_\theta \quad (9)$$

Where N_0 and N_θ are the particle number traveling through bend entrance and reflection angle θ , respectively.

In order to interpret the deposition amount increase caused by bend, a concept of “bend-induced deposition ratio throughout a bend” (R_{db}) was proposed as follows,

$$R_{db} = \frac{N_d/(\alpha R_b)}{N_f/D} \quad (10)$$

Where N_d and N_f are the particle number deposited in a bend and those in the straight duct of fully developed flow section with a length D , respectively. In this article, N_f is selected as the average deposited particles between the reference sections of $3D-2D$ and $2D-1D$ before bend inlet. R_b and D are bend radius and the cross dimension of the straight duct before bend, respectively. The symbol α stands for the total reflection angle of the bend, and in this paper it is $\pi/2$. In this formula, the deposition in the bend is treated as “equivalent length of straight duct” with fully developed flow. This deposition ratio can show the average deposition amount enhancement due to bend-induced flow turbulence and direction change.

- 1) By employing the correlation between dimensionless particle deposition velocity V_d^+ and particle relaxation time τ_p^+ , which are determined by the following equations,

$$V_d^+ = \frac{V_d}{u_w} \quad (11)$$

$$\tau_p^+ = \frac{C_c \rho_p d_p^2 u_w^2}{18 \mu \nu} \quad (12)$$

where, V_d means the deposition velocity, u_w is the friction velocity, C_c is the Cunningham slip correction factor, ρ_p stands for the particle density, d_p is the particle diameter, μ and ν are dynamic and kinematic viscosity respectively of air. In this proposed Lagrangian tracking approach, the particle deposition velocity onto a bend surface can be generally estimated by calculating the number of deposited trajectories in a time period as below,

$$V_d = \frac{N_d/A/t_b}{N_0/V} \quad (13)$$

where, t_b is the flying time scale for particles through a bend; N_0 and N_d are the numbers respectively of the particles that enter the entrance of the bend and those deposited within the bend; and, A and V are the area and volume of deposition bend respectively. Similar method to Eq. (13) has been successfully employed before by previous researchers [18,32] to predict particle deposition in straight duct flow.

2.5. Particle deposition analysis behind bends

To investigate bend-induced particle deposition behind bends, this paper gives two methods as follows:

- 1) By adopting the relationship between dimensionless particle deposition velocity V_d^+ and dimensionless particle relaxation time τ_p^+ , which has been expressed in Eqs. (11) and (12). The particle deposition velocity V_{da} behind bends was estimated by the following equation,

$$V_{da} = -\frac{Du_b \ln(N_{out}/N_{in})}{L} \quad (14)$$

Where u_b stands for the bulk flow velocity at the domain inlet, N_{in} is the particle number entered into a specific straight duct section, N_{out} is the particle number escaped from the straight duct section, D is the duct cross dimension, L is the length of the straight duct. This approach has been proved before in sole straight duct particle deposition [9], and it is applied here to study the deposition behind bends with developing turbulence [16]. The enhancement factor of deposition velocity behind bends (e_{da}) can be calculated by,

$$e_{da} = \frac{V_{da}}{V_{df}} \quad (15)$$

Where V_{df} is the deposition velocity in straight duct between the reference sections of $3D-2D$ and $2D-1D$ before bend inlet, where the flow is assumed to be fully developed. This deposition velocity is also estimated by Eq. (14).

- 2) By introducing a concept of “bend-induced deposition ratio behind a bend” (R_{da}) as follows,

$$R_{da} = \frac{N_{da}}{N_f} \quad (16)$$

Where N_{da} is the deposited particle number behind a bend at a specific straight duct section. Following this expression, the increased degree and trend of particle deposition can be clearly seen due to the bend-induced turbulence behind the bend.

Combining Eq. (10) and Eq. (16), “total bend-induced deposition ratio per cross dimension D ” (R_{dt}) can be expressed as,

$$R_{dt} = \frac{\alpha R_b}{D} \cdot R_{db} + \sum_{s=D}^{\infty} R_{da} = \frac{N_d}{N_f} + \sum_{s=D}^{\infty} \frac{N_{da}}{N_f} \quad (17)$$

Where s is the distance away from bend outlet. This equation reflects the total particle deposition amount increase due to bend.

Furthermore, relatively to the deposition in fully developed flow section, “total bend-induced enhancement deposition ratio per

cross dimension D ” (R_{dte}) can be determined by subtracting the deposition of fully developed section in the equation above,

$$R_{dte} = \frac{\alpha R_b}{D} \cdot (R_{db} - 1) + \sum_{s=D}^{\infty} (R_{da} - 1) = \left(\frac{N_d}{N_f} - \frac{\alpha R_b}{D} \right) + \sum_{s=D}^{\infty} \left(\frac{N_{da}}{N_f} - 1 \right) \quad (18)$$

This definition shows the total ratio of the additional deposition increase attributed to the existence of bend.

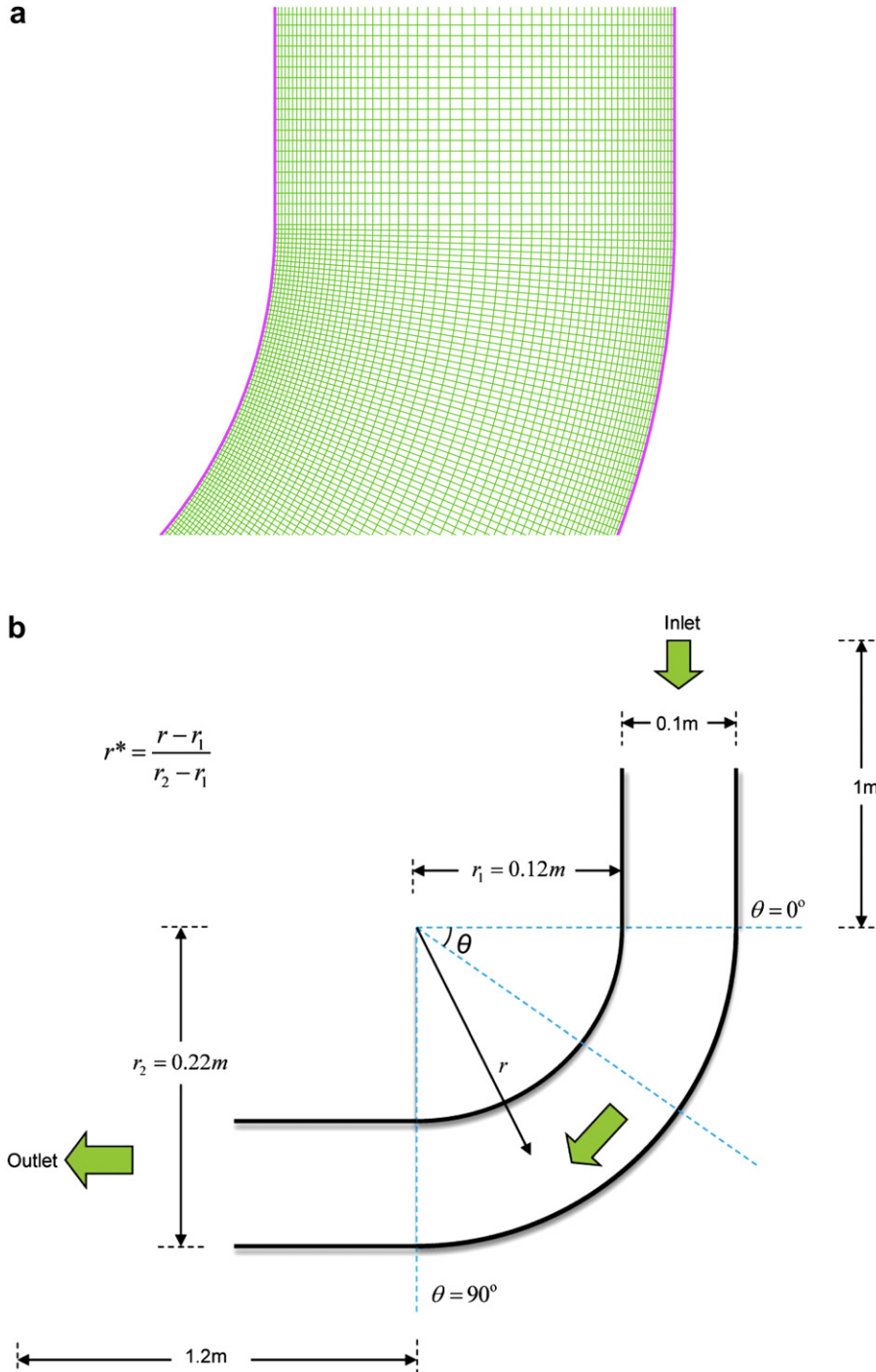


Fig. 1. Two-dimensional 90° bends geometry and mesh.

Table 2

Characteristics of the four grid systems for mesh independence test.

Grid system	Total mesh no.	Mesh no. before bend	Mesh no. in bend	Mesh no. behind bend
System 1	240 000	120 × 750	120 × 350	120 × 900
System 2	85 400	70 × 460	70 × 220	70 × 540
System 3	57 884	58 × 380	58 × 168	58 × 450
System 4	31 500	45 × 270	45 × 130	45 × 300

3. Results and discussion

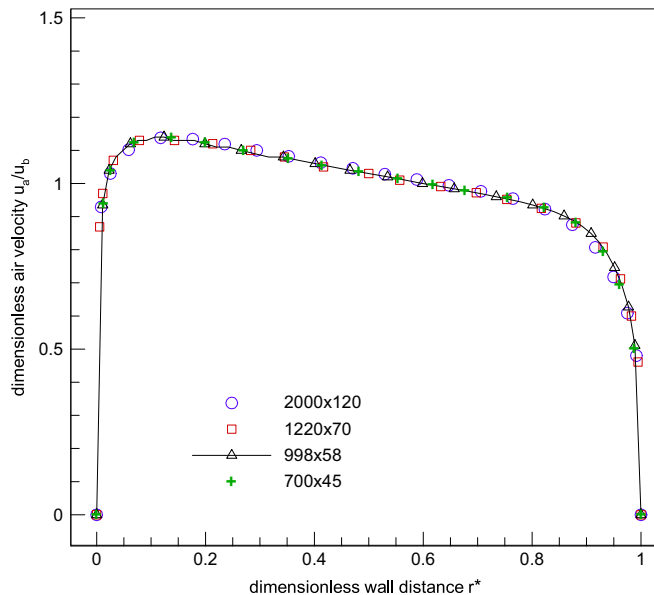
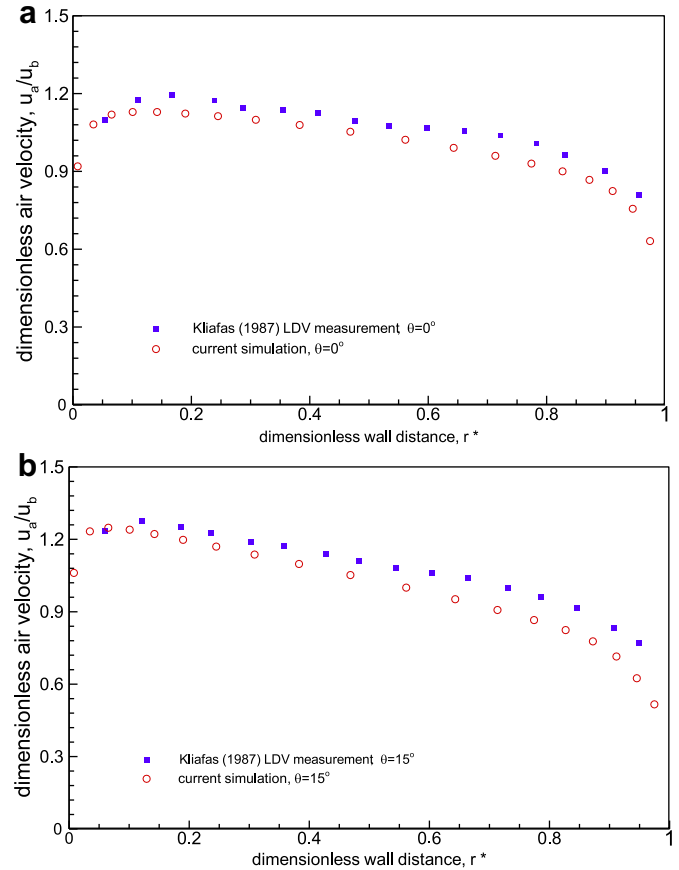
3.1. Numerical domain and mesh

The geometry and mesh of a two-dimensional 90° bend are shown in Fig. 1. With regard to this bend, the width D , radius R_b and curvature ratio R_o are 0.1 m, 0.17 m and 3.4, respectively. Four grid systems were tested to check the mesh independence as shown in Table 2. All the grids were denser near the wall areas to solve boundary flows with the first near-wall grid from 0.0044 to 4.2 for the four grid systems. The mesh numbers in bends were respectively 42 000, 15 400, 9744 and 5850 from grid system 1 to 4 as stated in Table 2. The results in Fig. 2 show similar results are obtained from the different grid systems with 97% agreement. Therefore, a relatively coarser grid system, i.e. system 3, was chosen to benefit the computational efficiency.

3.2. Numerical validation

Sixty thousand monodisperse spherical particles uniformly distributed at the entrance of the computational domain were released as Lagrangian discrete tracking approach was employed to solve the particle motion equation. The influence of this particle number on particle motion was checked with two hundred thousand particles, and subtle difference was found. In addition, the densities of the particles and the air are 2990 kg/m³ and 1.225 kg/m³, respectively. The air viscosity is 1.7894×10^{-5} kg/m/s.

Present simulation results are shown together with previous results of laser Doppler velocimetry (LDV) experiment [33] in Figs. 3 and 4. The air and particle velocities were normalized by the bulk air velocity u_b , and these dimensionless velocities were plotted against

**Fig. 2.** Comparison of air velocity profile at bend inlet at four grid systems.**Fig. 3.** Comparison of air velocity profile with experimental data in the bend at $\theta = 0^\circ$ and 15° .

dimensionless wall distance r^* for comparison as shown in Fig. 1. The comparisons indicate that the present model achieve more than 95% consistency with experimental data. This result shows that two-dimensional flow is accurate enough and relatively efficient. Since current numerical study focuses on introducing and studying the concept of bend-induced deposition in and behind bends, therefore, the simplified two-dimensional bend is utilized in this article.

3.3. Particle deposition distribution with three surface materials in bends

Fig. 5 demonstrates the detailed particle numbers deposited from bend inlet to locations at the four deflection section $\theta = 0^\circ$ – 90° with three surfaces for $d_p = 3$ – $7 \mu\text{m}$ particles. The deposited particles are calculated by Eq. (9). The deposition particle number increases slowly from $\theta = 0^\circ$ to 60° and obviously from $\theta = 60^\circ$ – 90° . When particle diameter d_p increase from $3 \mu\text{m}$ to $7 \mu\text{m}$, the particle number at the bend entrance decreases considerably, especially for molybdenum surfaces. With much larger particles in the experimental parameters, this decreased degree would be much higher, especially for large capture velocity surfaces. Take $d_p = 7 \mu\text{m}$ for example, the deposited particles in bends are 1.7 times on molybdenum surfaces to those on copper surfaces.

3.4. Particle deposition velocity with three surface materials in bends

Fig. 6 summarizes previous experimental data and predicted particle deposition velocities against particle relaxation time in 90°

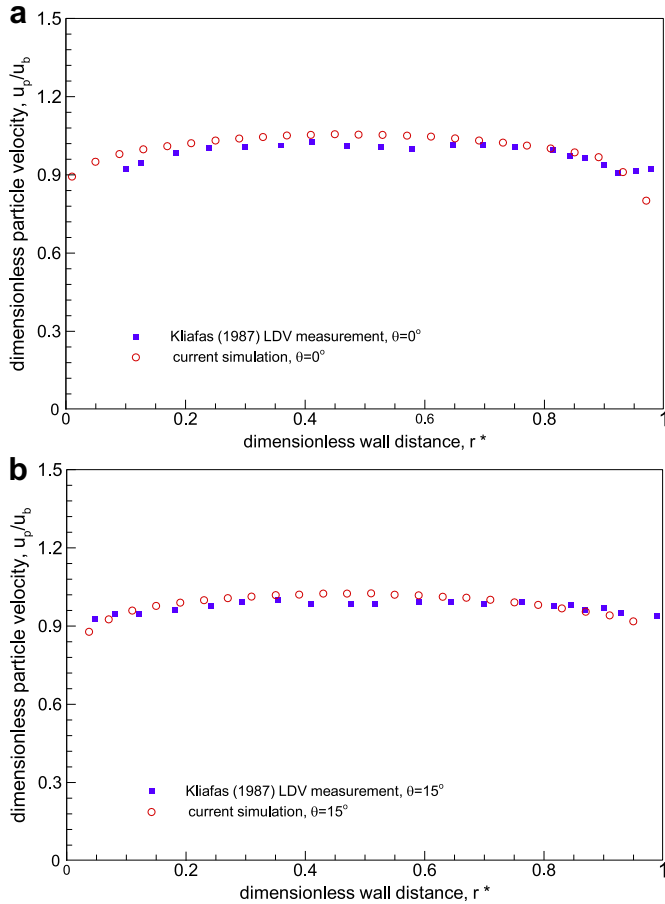


Fig. 4. Comparison of particle velocity profile with experimental data in the bend at $\theta = 0^\circ$ and 15° .

bends. The average particle deposition velocities were calculated through control volume method by Eqs. (11)–(13) for $d_p = 3\text{--}16\text{ }\mu\text{m}$ particles. To validate and compare the simulated results, three typical experiments [11,12,16] in 90° bends were collected in the figure. The experimental data from Liu & Agarwal [34] was also presented to compare the deposition velocities in bends with those in straight ducts.

It can be seen that predicted deposition velocities in bends are much larger than those in straight ducts by one or two orders of magnitude. Sippola and Nazaroff [16] also drew a similar conclusion when comparing their experimental data in bends with those in their straight ducts. Among the three experiments in bends, result data also change by about one order of magnitude due to different experimental conditions. Simulated particle deposition velocities from $\tau_p^+ = 1.2$ to 32.9 fall within the experimental data [11,12,16].

The surface effect on particle deposition velocity can be clearly seen from Fig. 7. The deposition velocity with copper surface is the lowest. This observation can also be seen in Fig. 5 where deposited particle numbers with different surfaces are presented. The reason of a low deposition velocity with copper surface could be due to the low capture velocity near such surface. Between particle relaxation time $\tau_p^+ = 1.2$ and 6.4, the particle deposition velocity with molybdenum surface is 0.7–1.2 times larger than that of a copper surface. Given more experimental data about particle collision behavior onto different surfaces with a wide particle diameter range, more deposition velocities could be predicted following the proposed method in this work.

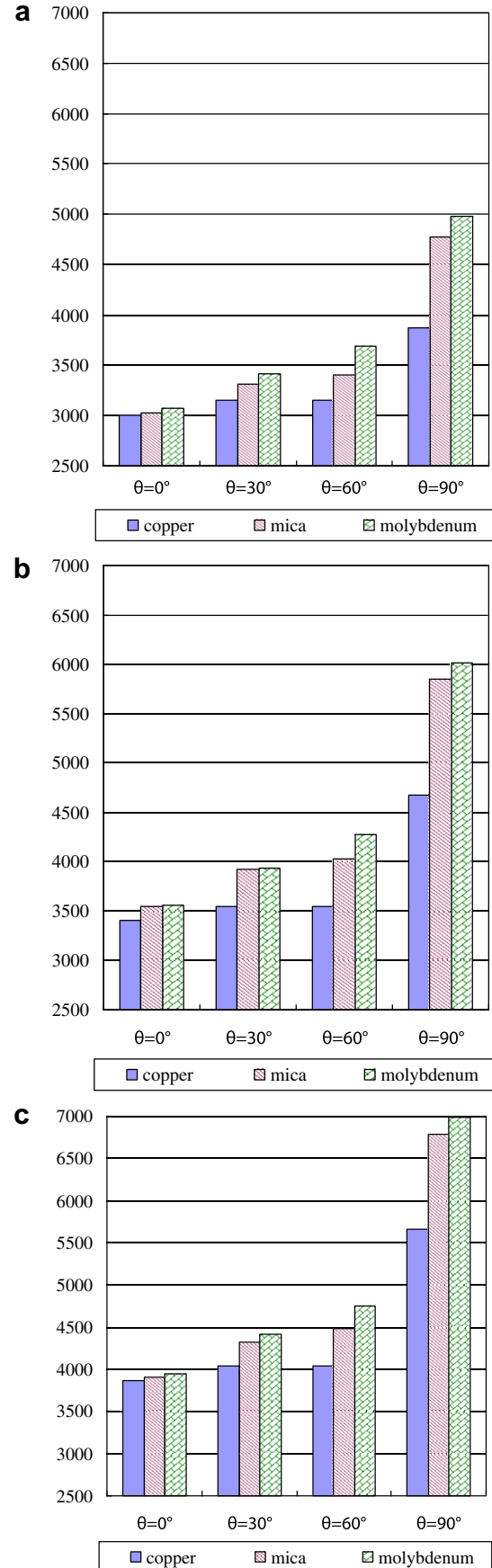


Fig. 5. Comparison of deposited particle number before locations of $\theta = 0^\circ\text{--}90^\circ$ with three surfaces: (a) $d_p = 3\text{ }\mu\text{m}$; (b) $d_p = 5\text{ }\mu\text{m}$; (c) $d_p = 7\text{ }\mu\text{m}$.

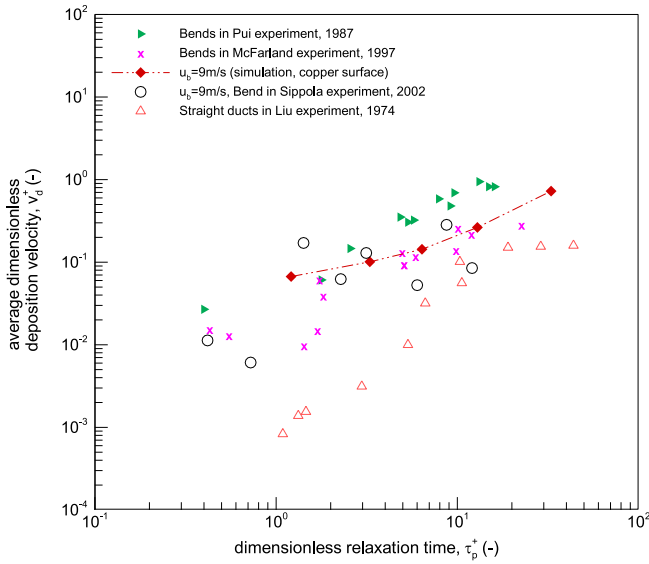


Fig. 6. Comparison of average particle deposition velocity with experimental data in 90° bends with copper surface for $d_p = 3\text{--}16\ \mu\text{m}$ particles.

3.5. Particle deposition velocity behind bends

Since a bend in the flow stream can cause the change of flow pattern and lead to flow turbulence behind bends, the particle deposition behind bends would be enhanced due to the bend. To describe the deposition change along the straight duct behind a bend, dimensionless distance (s^*) is expressed as $s^* = (L_a - x)/D$, which is shown in Fig. 8. In the present work, the dimensionless distance is an integer number. In the equation, L_a is the total straight duct length behind bends, which equals 1.2 m in this paper, and x is the horizontal coordinate. In addition, the predicted results in the following discussion were simulated based on the wall surfaces of the lowest capture velocity.

Fig. 9 shows the comparison of average particle deposition velocity behind 90° bends for $d_p = 3\text{--}23\ \mu\text{m}$ particles from $s^* = 1$ to 12. Correspondingly, the Stokes numbers of these particles are from

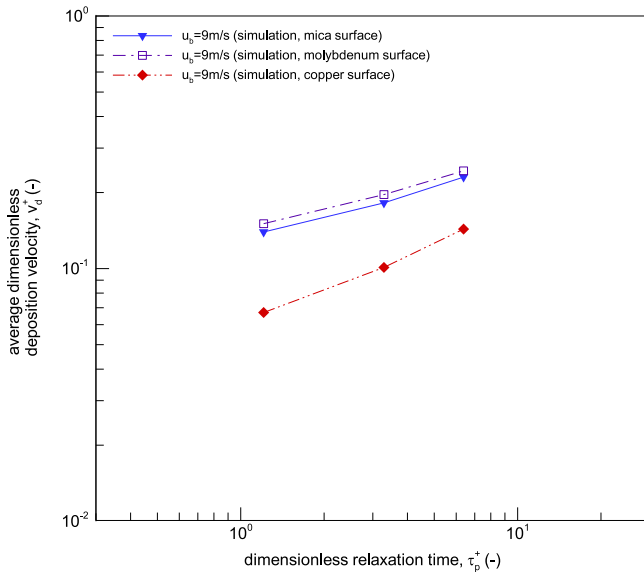


Fig. 7. Comparison of average particle deposition velocity in 90° bends with three surfaces for $d_p = 3\text{--}7\ \mu\text{m}$ particles.

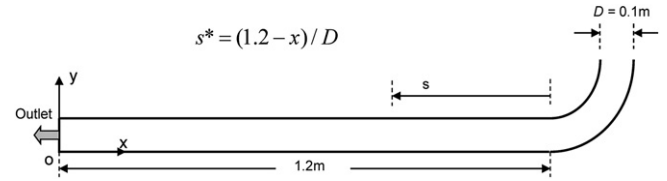


Fig. 8. Dimensionless distance behind bend, s^* .

0.016 to 0.89. Each particle deposition velocity at an s^* value is the average deposition velocity based on the deposition particle numbers from $s^* - 1$ to s^* . The calculation method can be found in Eq. (14). As shown in the figure, the magnitude of the dimensionless particle deposition velocity changes from 0.0317 to 1.332, which is much higher than those illustrated in Figs. 6 and 7. This behavior provides quantitative evidence through simulation that the deposition behind the bend is enhanced due to bend-induced

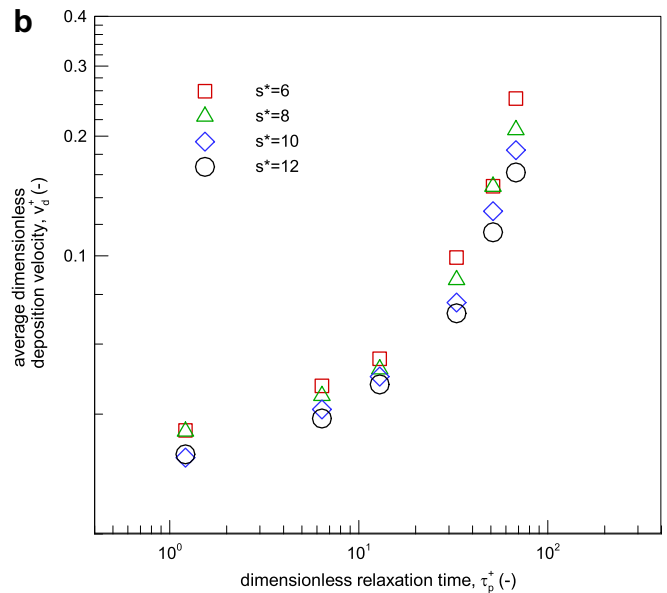
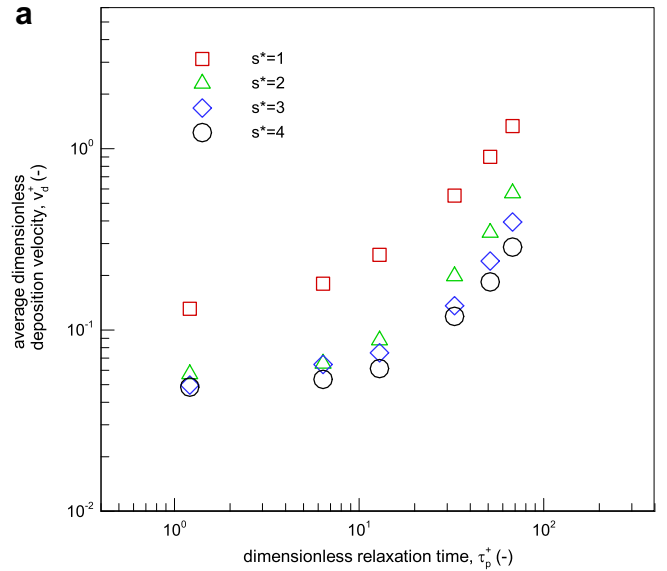


Fig. 9. Comparison of average particle deposition velocity behind bends for $d_p = 3\text{--}23\ \mu\text{m}$ particles from $s^* = 1$ to 12.

turbulence. Along with the increasing of dimensionless particle relaxation time from $\tau_p^+ = 1.21$ to 67.8, the deposition velocity increases sharply by 4.8–10 times. Current results of the enhanced particle deposition behind bends and the changing trend could explain and support previous experimental visualized observations and reports behind bends qualitatively [16,26].

However, when the distance increases away from the bend outlet, i.e. from $s^* = 1$ to 12, the particle deposition velocity decrease. The maximum deposition velocity is located at $s^* = 1$, which means the areas between bend outlet and one cross dimension distance for particles of specific Stokes number. From $s^* = 1$ to 2, the particle deposition velocity reduces tremendously, which reflects the rapidly decreasing influence of bend-induced vortices. The reduction degree from $s^* = 2$ to 5 is moderate and from $s^* = 6$ to 12 is minor. The decreasing deposition could be probably attributed to the turbulent level reduction when the distance increase behind bends as shown in Fig. 10. From $s^* = 1$ to 5, it can be seen in the figure that large vortices are produced behind the bend, while from $s^* = 6$ to 12, turbulent levels are rather low.

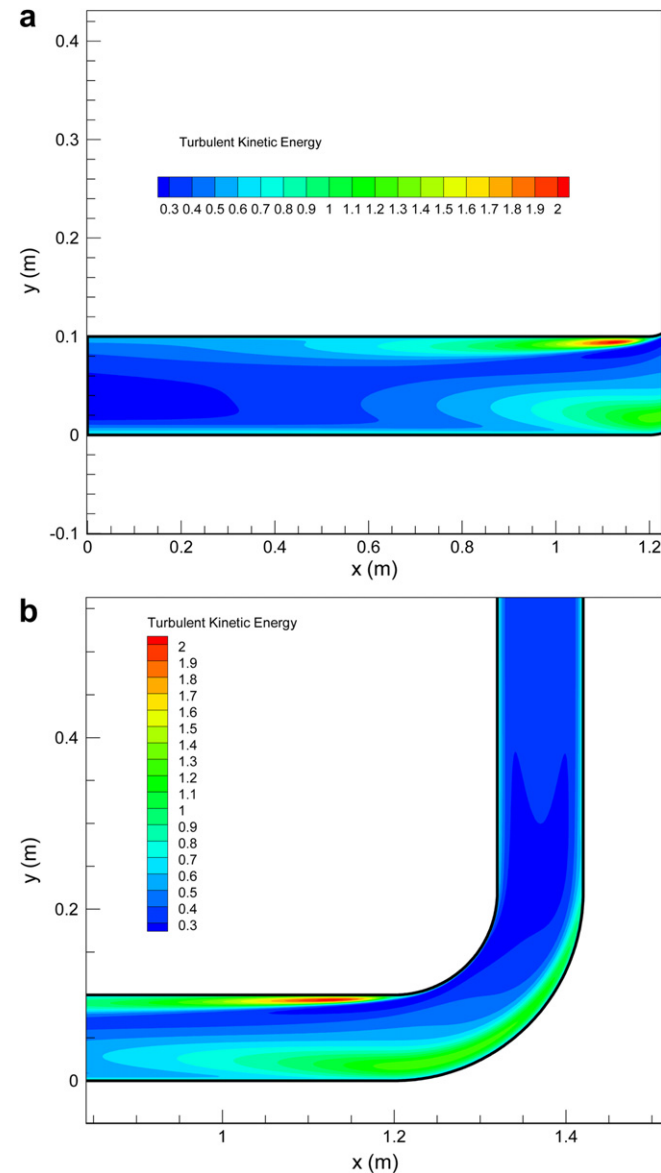


Fig. 10. Turbulent kinetic energy of the airflow in and behind bends.

3.6. Bend-induced deposition ratio

To describe the quantity of particle deposition along the straight duct behind bends, the bend-induced deposition parameter R_{da} is demonstrated in Fig. 11. In the presentations of the deposition ratio and the following enhancement factor, Eqs. (1–4) were adopted at the domain inlet to guarantee the airflow was fully developed in straight duct ahead of bends. The results range from $R_{da} = 0.91$ to 15.2, which indicate the quantitative increase of particle deposition caused by bend. Particle accumulation is very high near the bend outlet. Deposition ratios increase from 4.61 to 15.2 times for particle diameters increasing from $d_p = 3$ – $23 \mu\text{m}$. The deposition is reduced sharply from areas near the bend outlet to those further away from it. From $s^* = 10$ to 12, the deposition ratios are close to unity 1. This phenomena means that the flow disturbance due to bend is weakened to a marginal level at these areas, and the length of increased deposition due to the presence of the bend is

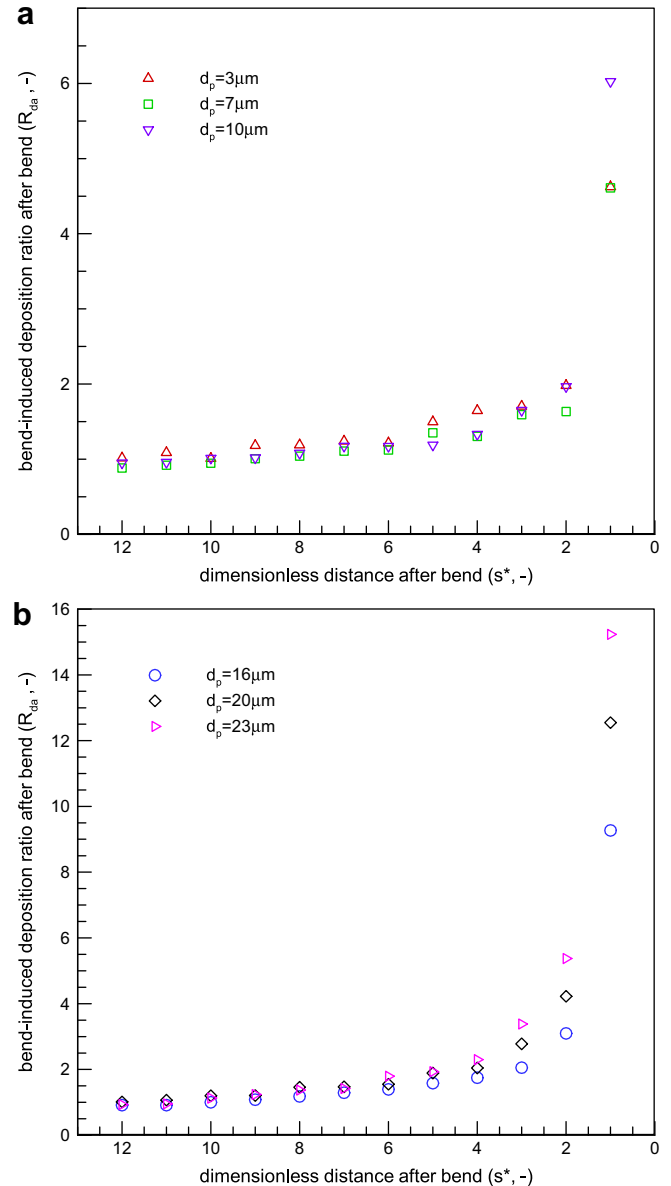


Fig. 11. Bend-induced deposition ratio distribution along the distance behind bend for different particle diameter.

10 times as long as the cross dimension (D) of straight duct. This interpretation is partially supported by the experimental measurements of particle deposition in developing turbulent flow in the studies of Sippola and Nazaroff [16].

Fig. 12 illustrates the bend-induced enhancement deposition ratio in and behind bends for present simulation domain. The enhancement deposition ratios in bends and behind bends correspond to the first and second term in Eq. (18), respectively. These ratios are calculated based on Eqs. (16)–(18). They can be also called as additional deposition caused by bend. For small particles, for example, $d_p = 3 \mu\text{m}$, the enhancement deposition ratio is rather low because the ratio considers the bend as equivalent straight duct and the Stokes number indicates that small particles are easy to follow fluid flow. In other words, smaller particles are hardly to impact onto bend walls. However, the flow pattern change by bends also leads to deposition enhancement behind bends, and the total ratio is mainly composed of the enhancement deposition behind bends, approximately 99% for particles of $d_p = 3 \mu\text{m}$. This behavior is probably due to that eddies behind bends are adaptable to catch smaller particles onto wall surfaces as demonstrated in Fig. 12. For larger particles, the major composition of the total ratio is still of a great portion, approximately 42% for particles of $d_p = 23 \mu\text{m}$. Therefore, when describing the particle deposition induced by bends, the general concept of total deposition including that in bends and behind bends is much better than sole particle accumulation in bends.

3.7. Changing trend of bend-induced deposition ratio

It is interesting to find that the decay trend of particle deposition ratio behind bend in Fig. 11. This decay trend satisfies two conditions: (1) it peaks at $s^* = 1$; (2) when $s^* \geq \infty$, the deposition ratio asymptotically approaches unity 1. The second condition means the particle deposition is in a fully developed flow. Therefore, subtracting the deposition in a fully developed flow, the “enhancement deposition ratio behind a bend” (R_{dae}) would be infinitely small at $s^* \geq \infty$. Take the particles of $d_p = 20 \mu\text{m}$ for example, as shown in Fig. 13, the relationship between the enhancement deposition ratio (R_{dae}) and dimensionless distance (s^*) can be built as follows,

$$R_{\text{dae}} = 11.5(s^*)^{-1.67}, \text{ at } St = 0.674 \quad (19)$$

The R^2 value is as high as 0.982, which shows a well-fitting between the simulation data and the proposed equation. In

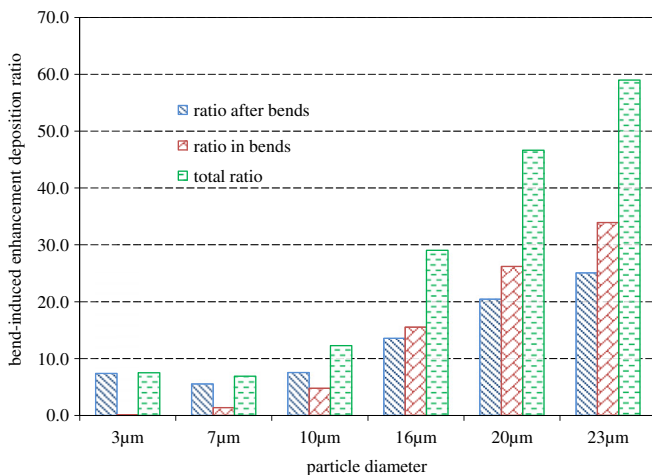


Fig. 12. Bend-induced enhancement deposition ratio for six particle diameters.

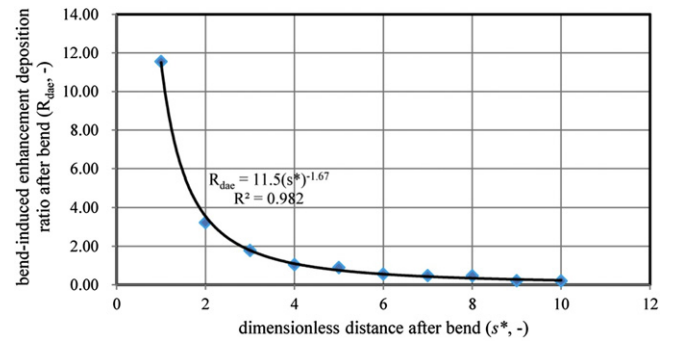


Fig. 13. Bend-induced enhancement deposition ratio behind bend for $d_p = 20 \mu\text{m}$ particles.

addition, this fitting can also transformed as exponential correlation between the two variables. For other particle diameters, similar fittings can be obtained through this method.

3.8. Changing trend of enhancement deposition ratio

Enhancement factor of deposition velocity behind a bend (e_{da}) varies with dimensionless distance (s^*) and particle diameter or Stokes number (St), as shown in Fig. 11. A three-dimensional surface fitting code (TableCurve 3D, Jandel Scientific, San Rafael, CA) was adopted to develop least square fits of the current simulation data [11]. Therefore, a non-linear fitting of $R^2 = 0.994$ could be expressed as follows,

$$e_{\text{da}} = 0.8697 + 7.522 \cdot x_{s^*} + 4.662 \cdot y_{St} + 111.7 \cdot x_{s^*} \cdot y_{St} \quad (20)$$

$$x_{s^*} = \exp \left\{ -\frac{1}{2} \left[\frac{1}{1.157} \ln \left(\frac{s^*}{0.1703} \right) \right]^2 \right\}$$

$$y_{St} = \exp \left[-\frac{1}{2} \left(\frac{St - 1.410}{0.5476} \right)^2 \right]$$

Where x_{s^*} is the lognormal distribution function with s^* and y_{St} stands for the Gaussian distribution function with St , as shown in Fig. 14. The enhancement deposition ratio has exponential

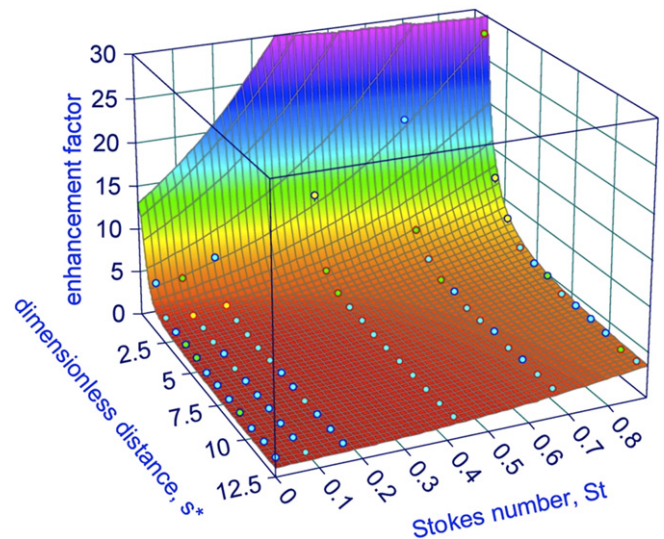


Fig. 14. Enhancement factor of particle deposition velocity behind bend for $d_p = 3\text{--}23 \mu\text{m}$ particles.

decreasing relationship only with dimensionless distance and particle Stokes number. This relationship is valid for $s^* = 1\text{--}12$ and $St = 0.016\text{--}0.89$.

3.9. Changing trend of dimensionless deposition velocity behind bend

Combining Eq. (15) and Eq. (20), the dimensionless deposition velocity behind bend (V_{da}^+) is deducted as,

$$V_{da}^+ = \frac{V_{da}}{u_w} = e_{da} V_{df}^+ \quad (21)$$

$$V_{da}^+ = (0.8697 + 7.522 \cdot x_{s^*} + 4.662 \cdot y_{St} + 111.7 \cdot x_{s^*} \cdot y_{St}) \cdot V_{df}^+$$

Which means the dimensionless deposition velocity in the developing turbulent flow behind bend can be associated with the reference dimensionless deposition velocity V_{df}^+ by the enhancement factor. Substituting the dimensionless parameter St with τ_p^+ , the function y_{St} becomes,

$$y_{St} = \exp \left[-\frac{1}{2} \left(\frac{2\nu U \tau_p^+ - 1.410 u_w^2 D_h}{0.5476 u_w^2 D_h} \right)^2 \right] \quad (22)$$

This equation reveals that the dimensionless deposition velocity behind bend (V_{da}^+) is related to dimensionless particle relaxation time as shown in Fig. 9.

Furthermore, the curves of $s^* = 6\text{--}12$ shown in Fig. 9 exhibit similarity to develop a more universal relationship than that in Eq. (21). By averaging seven dimensionless deposition velocities at each dimensionless relaxation time, Fig. 15 is obtained together with the standard deviation of the averaged values. Using a polynomial fitting of $R^2 = 0.999$, the relationship is expressed as,

$$V_{da}^+ = 0.03248 + 0.00193 \cdot \tau_p^+ - 5.761 \cdot 10^{-5} \cdot (\tau_p^+)^2 + 1.736 \cdot 10^{-6} \cdot (\tau_p^+)^3 - 1.162 \cdot 10^{-8} \cdot (\tau_p^+)^4 \quad (23)$$

Under current simulation conditions, this relationship reveals that dimensionless deposition velocity depends only on dimensionless relaxation time for $s^* = 6\text{--}12$ as demonstrated in Fig. 15. Therefore, Eq. (23) is easy to use in the applications.

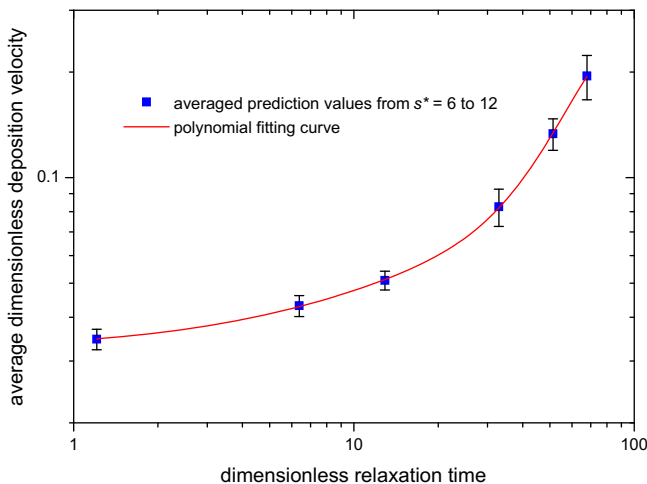


Fig. 15. Fitting curve of dimensionless deposition velocity averaged from $s^* = 6$ to 12 behind bends for $d_p = 3\text{--}23 \mu\text{m}$ particles.

4. Conclusions

This paper investigated the microparticle deposition in and behind 90° bends. Particle deposition distribution and deposition velocity in 90° ventilation bends with different surface materials were analyzed numerically, and the simulation results were also validated with experimental data. Bend-induced deposition ratio and deposition velocity were also discussed and fitted quantitatively. To summarize, the following conclusions can be drawn:

- Predicted particle deposition velocities in bends are much higher than those in straight ducts by one to two orders of magnitude. Between the predicted particle relaxation time 1.2 and 6.4, the particle deposition velocities with surfaces of highest capture velocity can be 1.2 times larger than those of lowest capture velocity. This behavior indicates that the duct bend wall with surfaces of high capture velocity is easy to accumulate contaminant particles.
- Current simulation provided quantitative evidence that the deposition behind a bend is sharply enhanced due to bend-induced turbulence. Particle deposition had a peak value near bend outlet. Along the straight duct behind bends, the depositions decreased exponentially toward a deposition pattern of fully developed turbulent flow since the bend-induced eddies are weakened.
- It is much better to adopt the general concept of total deposition including that in bends and behind bends to describe the particle deposition induced by bends. Deposition behind bends forms a large portion of the total bend-induced deposition, especially for smaller particles.
- Power decay trend was obtained between the enhancement deposition ratio (R_{dae}) and dimensionless distance (s^*). Non-linear exponential decay trend was also given among enhancement factor of deposition velocity behind a bend (e_{da}), dimensionless distance (s^*) and particle Stokes number (St). These fitting equations are valid according to the current simulation condition for the ranges of $s^* = 1\text{--}12$ and $St = 0.016\text{--}0.89$. Finally, two fitting equations of dimensionless deposition velocity behind bend were developed to model the deposition trend easily and universally.

This work proposed new concepts of bend-induced deposition which includes the deposition both in bends and behind bends. Quantitative discussion was given to evaluate the two location depositions. The decaying correlations were proposed based on current results. This paper contributes to the understanding of pollutant particle deposition and distribution in and behind ventilation duct bends, which can be applied on contaminant particle sampling, removal and associated epidemiologic study between particle and human health through ventilation system.

Acknowledgment

This work was financially supported by the Hong Kong Polytechnic University through research grants A-PJ61 and A-PJ12.

Nomenclature

A	area of deposition, m^2
C_0	constant in Eq. (3)
C_c	Cunningham slip correction factor
d_p	particle diameter, m
D	bend width or cross dimension of straight duct, m
e	kinematic restitution coefficient
e_{da}	enhancement factor of deposition velocity behind a bend

f	fanning factor
g_i	gravity acceleration, ms^{-2}
$l_{a,b}$	empirical constants in Eqs. (7 and 8)
L	length of the straight duct behind a bend, m
La	total length of the straight duct behind a bend, m
k	turbulent kinetic energy, kg ms^{-1}
N_0	number of particles flow across bend entrance
N_d	number of particles deposited on bend wall surface
N_{da}	number of particles deposited behind a bend at a specific straight duct section
N_f	number of particles deposited on straight duct of fully developed flow section ahead of a bend
N_{in}	number of particles entered into a specific straight duct section behind a bend
N_{out}	number of particles escaped from a specific straight duct section behind a bend
N_θ	number of particles flow across bend reflection angle θ
r_1, r_2	radius of the inner and outer wall of the bend, respectively, m
r^*	dimensionless wall distance
R_o	bend curvature ratio
R_b	bend radius, m
R_{da}	bend-induced deposition ratio behind a bend
R_{dae}	bend-induced enhancement deposition ratio behind a bend
R_{db}	bend-induced deposition ratio throughout a bend
R_{dt}	total bend-induced deposition ratio per cross dimension D
R_{dte}	total bend-induced enhancement deposition ratio per cross dimension D
R_{pw}	coefficient of restitution in the absence of adhesion
t	time, s
s	distance behind bend outlet, m
s^*	dimensionless distance behind bend outlet, integer in this paper
St	Stokes number
t_b	flying time scale for particles through a bend, s
u_b	air bulk velocity, ms^{-1}
u_a, U	air velocity, ms^{-1}
u_p, u_{pi}	particle velocity, ms^{-1}
u_w	friction velocity, ms^{-1}
v_c	capture velocity, ms^{-1}
$v_{1,n}^p, v_{2,n}^p$	particle normal incident and reflected velocity, respectively, ms^{-1}
V	volume of the domain, m^3
V_d	deposition velocity, ms^{-1}
V_{da}	deposition velocity in straight duct behind a bend, ms^{-1}
V_{df}	deposition velocity in straight duct of fully developed flow section ahead of a bend, ms^{-1}
V_d^+	dimensionless deposition velocity
x_D	horizontal coordinate, m
x_{s^*}	lognormal distribution function with s^*
y	vertical coordinate, m
y_{St}	Gaussian distribution function with St
Greek symbols	
α	total reflection angle of the bend, i.e. here $\pi/2$
k	empirical constant in Eq. (7)
μ	dynamic viscosity of air, Pa s
ν	kinematic viscosity of air, $\text{m}^2 \text{s}^{-1}$
ρ_a	air density, kg m^{-3}
ρ_p	particle density, kg m^{-3}
ρ_{pw}	adhesion coefficient
θ	deflection angle
τ_p^+	dimensionless particle relaxation time

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