Software Information

- Please check, whether your inputs, the equations applied and the charactersitics are displayed correctly.
- You are welcome to send your feedback via https://github.com/oemof/tespy/issues.
- \bullet LATEX packages required are:
 - graphicx
 - float
 - hyperref
 - booktabs
 - amsmath
 - units
 - cleveref
- To supress these messages, call the model documentation with the keyword draft=False.

TESPy Version: 0.4.0 - dev

Commit: d918f10d@feature/self_documenting_models

CoolProp version: 6.4.0

Python version: 3.8.0 (default, Oct 28 2019, 16:14:01) [GCC 8.3.0]

1 Connections in design mode

1.1 Specified connection parameters

label	p in bar (1)	T in °C (2)
cycle closer:out1_turbine inlet valve:in1	110.000	550.000
turbine inlet valve:out1_high pressure turbine:in1	100.000	-
high pressure turbine:out1_extraction splitter:in1	10.000	-
$source_cw:out1_condenser:in2$	10.000	60.000
$condenser: out 2_sink_cw: in 1$	-	110.000

Table 1: Specified connection parameters

1.2 Equations applied

$$0 = p - p_{\text{spec}} \tag{1}$$

$$0 = T(p,h) - T_{\text{spec}} \tag{2}$$

1.3 Specified fluids

label	water (3)
cycle closer:out1_turbine inlet valve:in1	1.000
$source_cw:out1_condenser:in2$	1.000

Table 2: Specified fluids

1.4 Equations applied

$$0 = x_{\text{water}} - x_{\text{water,spec}} \tag{3}$$

2 Components in design mode

2.1 Components of type CycleCloser

2.1.1 Mandatory constraints

$$0 = p_{\text{in},i} - p_{\text{out},i} \ \forall i \in [1]$$

$$0 = h_{\text{in},i} - h_{\text{out},i} \ \forall i \in [1]$$

$$\tag{5}$$

2.2 Components of type Valve

2.2.1 Mandatory constraints

$$0 = \dot{m}_{\text{in},i} - \dot{m}_{\text{out},i} \ \forall i \in [1]$$

$$0 = x_{fl,\text{in},i} - x_{fl,\text{out},i} \ \forall fl \in \text{network fluids}, \ \forall i \in [1]$$
 (7)

$$0 = h_{\text{in},i} - h_{\text{out},i} \,\forall i \in [1]$$

$$\tag{8}$$

2.3 Components of type Turbine

2.3.1 Mandatory constraints

$$0 = \dot{m}_{\text{in},i} - \dot{m}_{\text{out},i} \ \forall i \in [1] \tag{9}$$

$$0 = x_{fl,\text{in},i} - x_{fl,\text{out},i} \ \forall fl \in \text{network fluids}, \ \forall i \in [1]$$
(10)

2.3.2 Inputs specified

label	eta_s (11)
high pressure turbine low pressure turbine	0.900 0.900

Table 3: Parameters of components of type Turbine

2.3.3 Equations applied

$$0 = -(h_{\text{out}} - h_{\text{in}}) + (h_{\text{out,s}} - h_{\text{in}}) \cdot \eta_{\text{s}}$$
(11)

2.4 Components of type Splitter

2.4.1 Mandatory constraints

$$0 = \sum \dot{m}_{\text{in},i} - \sum \dot{m}_{\text{out},j} \ \forall i \in \text{inlets}, \forall j \in \text{outlets}$$
 (12)

$$0 = x_{fl,\text{in}} - x_{fl,\text{out},j} \ \forall fl \in \text{network fluids}, \ \forall j \in \text{outlets}$$
 (13)

$$0 = h_{in} - h_{\text{out}, j} \,\forall j \in \text{outlets} \tag{14}$$

$$0 = p_{\text{in},1} - p_{\text{in},i} \ \forall i \in \text{inlets} \setminus \{1\}$$

$$0 = p_{\text{in},1} - p_{\text{out},j} \ \forall j \in \text{outlets}$$
(15)

2.5 Components of type Condenser

2.5.1 Mandatory constraints

$$0 = \dot{m}_{\text{in},i} - \dot{m}_{\text{out},i} \ \forall i \in [1,2]$$

$$\tag{16}$$

$$0 = x_{fl,\text{in},i} - x_{fl,\text{out},i} \,\forall fl \in \text{network fluids}, \,\forall i \in [1,2]$$

$$\tag{17}$$

$$0 = \dot{m}_{\text{in},1} \cdot (h_{\text{out},1} - h_{\text{in},1}) + \dot{m}_{\text{in},2} \cdot (h_{\text{out},2} - h_{\text{in},2})$$
(18)

2.5.2 Inputs specified

label	ttd_u (19)	pr1 (20)	pr2 (21)	subcooling (22)
preheater condenser	5.000 12.000	1.000 1.000	$0.990 \\ 0.990$	True True

Table 4: Parameters of components of type Condenser

2.5.3 Equations applied

$$0 = ttd_{u} - T_{sat}(p_{in,1}) + T_{out,2}$$
(19)

$$0 = p_{\text{in},1} \cdot pr1 - p_{\text{out},1} \tag{20}$$

$$0 = p_{\text{in},2} \cdot pr2 - p_{\text{out},2} \tag{21}$$

$$0 = h_{\text{out},1} - h\left(p_{\text{out},1}, x = 0\right) \tag{22}$$

2.6 Components of type Merge

2.6.1 Mandatory constraints

$$0 = \sum \dot{m}_{\text{in},i} - \sum \dot{m}_{\text{out},j} \ \forall i \in \text{inlets}, \forall j \in \text{outlets}$$
 (23)

$$0 = \sum_{i} \dot{m}_{\text{in},i} \cdot x_{fl,\text{in},i} - \dot{m}_{\text{out}} \cdot x_{fl,\text{out}} \,\forall fl \in \text{network fluids}, \,\forall i \in \text{inlets}$$
 (24)

$$0 = \sum_{i} (\dot{m}_{\text{in},i} \cdot h_{\text{in},i}) - \dot{m}_{\text{out}} \cdot h_{\text{out}} \ \forall i \in \text{inlets}$$
 (25)

$$0 = p_{\text{in},1} - p_{\text{in},i} \ \forall i \in \text{inlets} \setminus \{1\}$$

$$0 = p_{\text{in},1} - p_{\text{out},j} \ \forall j \in \text{outlets}$$
(26)

2.7 Components of type Pump

2.7.1 Mandatory constraints

$$0 = \dot{m}_{\text{in},i} - \dot{m}_{\text{out},i} \ \forall i \in [1]$$

$$0 = x_{fl,\text{in},i} - x_{fl,\text{out},i} \ \forall fl \in \text{network fluids}, \ \forall i \in [1]$$
 (28)

2.7.2 Inputs specified

Table 5: Parameters of components of type Pump

2.7.3 Equations applied

$$0 = -(h_{\text{out}} - h_{\text{in}}) \cdot \eta_{\text{s}} + (h_{\text{out,s}} - h_{\text{in}})$$
(29)

2.8 Components of type HeatExchangerSimple

2.8.1 Mandatory constraints

$$0 = \dot{m}_{\text{in},i} - \dot{m}_{\text{out},i} \,\forall i \in [1]$$

$$(30)$$

$$0 = x_{fl,\text{in},i} - x_{fl,\text{out},i} \ \forall fl \in \text{network fluids}, \ \forall i \in [1]$$
 (31)

2.8.2 Inputs specified

label	pr (32)
steam generator	0.950

Table 6: Parameters of components of type HeatExchangerSimple

2.8.3 Equations applied

$$0 = p_{\text{in},1} \cdot pr - p_{\text{out},1} \tag{32}$$

3 Busses in design mode

3.1 Bus "power"

Specified total value of energy flow: $\dot{E}_{\rm bus} = -5000000.000\,{\rm W}$

$$0 = \dot{E}_{\text{bus}} - \sum_{i} \dot{E}_{\text{bus},i} \tag{33}$$

label	$\dot{E}_{ m comp}$	$\dot{E}_{ m bus}$	η
high pressure turbine			
low pressure turbine	$\dot{m}_{ m in} \cdot (h_{ m out} - h_{ m in})$		f(X)(1)
pump	$\dot{m}_{\rm in} \cdot (h_{\rm out} - h_{\rm in})$	$rac{\dot{E}_{ m comp}}{\eta}$	f(X)(2)

Table 7: power

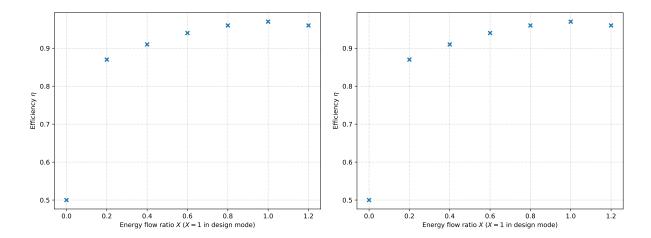


Figure 1: Bus efficiency characteristic

Figure 2: Bus efficiency characteristic

3.2 Bus "heat"

This bus is used for postprocessing only.

label	$\dot{E}_{ m comp}$	$\dot{E}_{ m bus}$	η
condenser	$\dot{m}_{\mathrm{in},1} \cdot (h_{\mathrm{out},1} - h_{\mathrm{in},1})$	$\dot{E}_{\mathrm{comp}} \cdot \eta$	-1.000

Table 8: heat