# ESD - Assignment 1 - Alt658

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### 1 Energy Systems Design - Assignment 1

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```
[435]: import numpy as np
import matplotlib.pyplot as plt
import sympy as sp
from IPython.display import Image
```

# 2 Question (1)

Using the Moody diagram to determine the following properties:

(a) For a segment of a pipe, =0.06 mm, D = 5 cm, V = 4 m/s, and = $6 \times 10$  m<sup>2</sup>/s. Find the fiction factor f and the fully rough friction factor f\_T

```
[436]: D = 5/100
V = 4
vis = 6e-6
ep = 0.06/1000

Re = D*V/vis
print("Re ", Re)

roughness = ep/D
print("roughness", roughness)
print("The fully rough friction factor is 0.025")
print("The calculated friction factor is approx. 0.035")
```

```
Re 33333.3333333333336
roughness 0.0012
The fully rough friction factor is 0.025
The calculated friction factor is approx. 0.035
```

## 3 Question (2)

[]:

# 4 Question (3)

## 5 Question (4)

A 14-inch (nominal) schedule 40 cast-iron pipe is used to convey 12 million gallons per day of benzene. The pipeline is 3 miles long, the pump motor is 39% efficient, and electricity costs 7.5 cents per kWh. An arrangement with a 12-inch and a 16-inch line in parallel with the existing 14-inch line is to be investigated. (a) What is the yearly pumping cost for the single pipe?

```
[]:
[437]: Di = 13.124/12 #ft
       rho = 55.5/32.2 \#lbm/ft^3
       u = 4.60e-4/32.2 \# lbm/ft/s
       ep = 0.00015
       g = 32.2
       Q_T = (12e6*0.134)/(24*3600) # ft^3/s
       1 = 3*5280 \# ft
       n = 0.39
       print("Q", Q)
       V = Q/(0.25*sp.pi*(Di**2))
       print("V [m/s] = ", float(V))
       print("Di", Di)
      Q 18.61111111111111
      V [m/s] = 19.811276951504023
      Di 1.09366666666668
[438]: Rey = V*Di*rho/u
       print("Rey ", float(Rey))
       # based off moody diagram, Re = 2.6e6
       rough = ep/Di
       print("The relative roughness is ", rough)
       print("Based on the moody diagram, relative roughness, reynolds number, the
        ⇔friction factor f is approx. 0.013")
       f = 0.013
```

Rey 2614162.5957410154
The relative roughness is 0.00013715330691862235

Based on the moody diagram, relative roughness, reynolds number, the friction factor f is approx. 0.013

```
[439]: Ws = (V**2)*(f*1)/(2*g*Di)
print("Ws ", float(Ws))
```

Ws 1147.4998171428113

```
[440]: power_to_fluid = rho*Ws*Q
print("Power to fluid [lbf-ft/sec] =", float(power_to_fluid))

power_required = power_to_fluid/n
print("Power required to fluid [hp] =", float(power_required))
```

Power to fluid [lbf-ft/sec] = 36809.67969328453 Power required to fluid [hp] = 94383.79408534494

#### 5.0.1 Scratch Work showing conversion of cost rate:

```
[441]: # 1kw = 1.34102 hp
# 1kw = 737.56 lb-ft/s

costrate = 0.89077 #unit conversion gave $0.89352/ftlb/s - year

yearly_cost_single = power_required*costrate
print("Annual cost for the single pipe [$] ", float(yearly_cost_single))
```

Annual cost for the single pipe [\$] 84074.25225740271

#### 5.0.2 Part B

Since the system is parallel, the pressure drop must be the same across the nodes, therefore, Ws must be the same.

```
[442]: print(float(Ws))
# This is head of 14" pipe
```

1147.4998171428113

```
[443]: # Head for the 12" pipe
Di_2 = 11.938/12 #ft
V_2 = Q/(0.25*sp.pi*(Di_2**2))
Rey_2 = V_2*Di_2*rho/u
print("Rey ", float(Rey_2))
rough_2 = ep/Di_2
print("The relative roughness for 12in is ", rough_2)
print("Based on Moody, the friction factor is approx. 0.014")
f_2 = 0.014
```

```
Rev 2873870.8248035745
      The relative roughness for 12in is 0.00015077902496230523
      Based on Moody, the friction factor is approx. 0.014
[444]: Ws_2 = V_2*(f_2*1)/(2*g*Di_2)
      print("Ws for 12in pipe ", float(Ws_2))
      power_to_fluid_2 = rho*Ws_2*Q
      print("Power to fluid [ft-lbf/s] =", float(power_to_fluid_2))
      Ws for 12in pipe 82.87599978593235
      Power to fluid [ft-lbf/s] = 2658.5093616631248
[445]: # Head for the 16" pipe
      Di_3 = 15 / 12 \# ft
      V_3 = Q / (0.25 * sp.pi * (Di_3 ** 2))
      Rey_3 = V_3 * Di_3 * rho / u
      print("Rey ", float(Rey_3))
      rough_3 = ep / Di_3
      print("The relative roughness for 16in is ", rough_3)
      print("Based on Moody, the friction factor is approx. 0.013")
      f_3 = 0.013
      Rey 2287217.993767006
      Based on Moody, the friction factor is approx. 0.013
[446]: Ws_3 = V_3*(f_3*1)/(2*g*Di_3)
      print("Ws for 12in pipe ", float(Ws_3))
      power_to_fluid_3 = rho*Ws_3*Q
      print("Power to fluid [ft-lbf/s] =", float(power_to_fluid_3))
      Ws for 12in pipe 38.79404308068998
      Power to fluid [ft-lbf/s] = 1244.441418181036
[447]: import numpy as np
      from scipy.optimize import fsolve
      # Define the missing functions
      def Ws_2(Ws, Q):
          # Define this function based on your system's equations
          return Ws - 0.5 * Q**2 # Example equation, replace with your actual
       \rightarrowequation
      def Ws_func(Ws, Q):
          # Define this function based on your system's equations
```

return Ws - 0.7 \* Q\*\*2 # Example equation, replace with your actual

 $\hookrightarrow$  equation

```
def Ws_3(Ws, Q):
           # Define this function based on your system's equations
           return Ws - 0.9 * Q**2 # Example equation, replace with your actual_
        \rightarrowequation
       # Define Q_T (total flow rate)
       Q_T = 10  # This is an example value, replace with your actual value
       def system(x):
           Ws, Q1, Q2, Q3 = x
           return [
               Ws_2(Ws, Q1),
               Ws_func(Ws, Q2),
               Ws_3(Ws, Q3),
               Q_T - Q1 - Q2 - Q3
           1
       # Initial quess
       initial_guess = np.array([100, Q_T/3, Q_T/3, Q_T/3])
       # Solve the system
       Ws, Q_1, Q_2, Q_3 = fsolve(system, initial_guess)
       print(f'The head required to push the fluid is {Ws:.2f} feet squared per second ∪
        ⇔squared.')
       print(f'12" pipe flow rate is {Q 1:.2f} cfs.')
       print(f'14" pipe flow rate is {Q_2:.2f} cfs.')
       print(f'16" pipe flow rate is {Q_3:.2f} cfs.')
      print(Ws)
      The head required to push the fluid is 7.45 feet squared per second squared.
      12" pipe flow rate is 3.86 cfs.
      14" pipe flow rate is 3.26 cfs.
      16" pipe flow rate is 2.88 cfs.
      7.450739428319538
[448]: # This number seems realy low, not sure where the error is in my code
       power_B = rho*Q_T*Ws/0.39
       annual_cost_par = power_B*costrate
       print(f'The cost per year for the parallel arrangement is {annual_cost_par} ⊔
        ⇔dollars per year.')
```

The cost per year for the parallel arrangement is 293.31715353664015 dollars per year.

#### 5.1 Problem 5

```
[449]: # easier to read these as sympy symbols
       gamma = sp.symbols(r'\gamma')
       Ws = sp.symbols('W_s')
       hf = sp.symbols('h_f')
       g = sp.symbols('g')
       P_in = sp.symbols('P_{in}')
       P_out = sp.symbols('P_{out}')
       V_in = sp.symbols('V_{in}')
       V_out = sp.symbols('V_{out}')
       z_in = sp.symbols('z_{in}')
       z_out = sp.symbols('z_{out}')
       # defining my values
       L_num = 7000
       D_num = 60
       ep_num = 0.01
       h = 1250
       rho_num = 1.934 #converted to slug/ft^3
       mu_num = 2.043e-5 #also divided by 32.2 for conversion
       n_{turbine} = 0.92
       n_pump = 0.82
       z_{in} = h
```

Since the pressures are at atmospheric conditions,  $P_i$ ,  $P_j$  out = 0 The resevoirs are big, so we can say the velocity Vin, Vout = 0 Zout = datum = 0

```
[450]: headeq_1 = sp.Eq(Ws, g*z_in - hf) headeq_1 

[450]: W_s = 1250g - h_f Now, hf = (K_major + K_ minor)*(V^2/2) 

[451]: f_laminar_sym = sp.symbols('f_{laminar}') 

K_minor = sp.symbols('K_{minor}') 

Q_sym = sp.symbols('Q_{sym}')
```

```
# I calculated ft on my calculator using epsilon = 0.01 and D = 60, it is_

space faster just to input into python manually

Ft = 0.013259

K_minor_1 = 1.5 + 498*Ft

headeq_2 = headeq_1.subs(hf, 8*(Q_sym**2)*(f_laminar_sym*(L_num/D_num) +_

space for the symmetry of the
```

[451] :  $W_s = -\frac{Q_{sym}^2 \left(116.66666666667 f_{laminar} + 8.102982\right)}{1620000\pi^2} + 1250g$ 

Equation looks strange, but it should be Ws = .... K\_minor = 0.5 + 1 + 6(8)Ft + 14(30)Ft + 10(3)Ft

and Ft is now known, so we know K minor simplifies to:

```
[453]: headeq_3 = headeq_2.subs(f_laminar_sym, f_laminar_eq)

# headeq_4 = headeq_2.subs(K_minor, K_minor_1)

# headeq_4

#

# headeq_5 = headeq_4.subs(K_major, K_major_1)

# headeq_5
```

```
[454]: from sympy import solve
       head_4 = headeq_3.subs(Q_sym, 50000)
       head_4
       solution = solve(head_4)
       print(solution)
       [{W_s: 1250.0*g - 1509.0448389156}]
[455]: head 4 = headeg 3.subs(Q sym, 150000)
       head 4
       solution = solve(head_4)
       print(solution)
       [{W_s: 1250.0*g - 13580.208169733}]
[456]: head_4 = headeq_3.subs(Q_sym, 175000)
       head_4
       solution = solve(head_4)
       print(solution)
       [{W_s: 1250.0*g - 18484.0558748449}]
[457]: head_4 = headeq_3.subs(Q_sym, 250000)
       head 4
       solution = solve(head_4)
       print(solution)
       [{W_s: 1250.0*g - 37722.1354837542}]
      Couldn't figure out how to get it to plot, so I did a few values manually:
      1- 50,000 cfs 2- 150,000 cfs 3- 175,000 cfs 4- 250,000 cfs
      at 150,000 cfs, I finished the rest of the calculations by hand to find the power of the fluid then
      multiplied that by the turbine efficiency ws(150,000) is Ws as a function of 150,000
      Ws(150,000) rho150,000 / 550 = 14067212
      then 14067212*0.89 = my maximum power
      MAX Power in [hp] = 12,941,835
      5.2 Part B
```

The max power occurs at approximately 150,000 cfs

```
[458]: \# Ws_= sp.lambdify(Q_sym, headeq_3.rhs, modules='numpy')
```

```
[459]: # vol_flow_rates = np.linspace(50000, 250000, 100000)
# power_of_fluid = rho*Ws_(vol_flow_rates)*vol_flow_rates/550
# power_shaft = n_turbine*power_of_fluid

# fig, ax = plt.subplots()
# ax.plot(vol_flow_rates, power_of_fluid, label='Fluid Power', ls='--')
# ax.plot(vol_flow_rates, power_shaft, label='Shaft Power')
# ax.set_xlabel(r'Flow Rate, $Q$ ($\frac{ft^3}{s}\})')
# ax.set_ylabel(r'Power ($hp$)')
# ax.set_title('Turbine')
# ax.legend()
# plt.show()

[460]: # max_power_gen = np.max(power_of_fluid)
# print(f'The maximum power is {max_power_gen} horse power.')

[461]: # jupyter nbconvert --to pdf my_notebook.ipynb
# jupyter nbconvert --to pdf '.\ESD - Assignment 1 - Alt658.ipynb'
```