

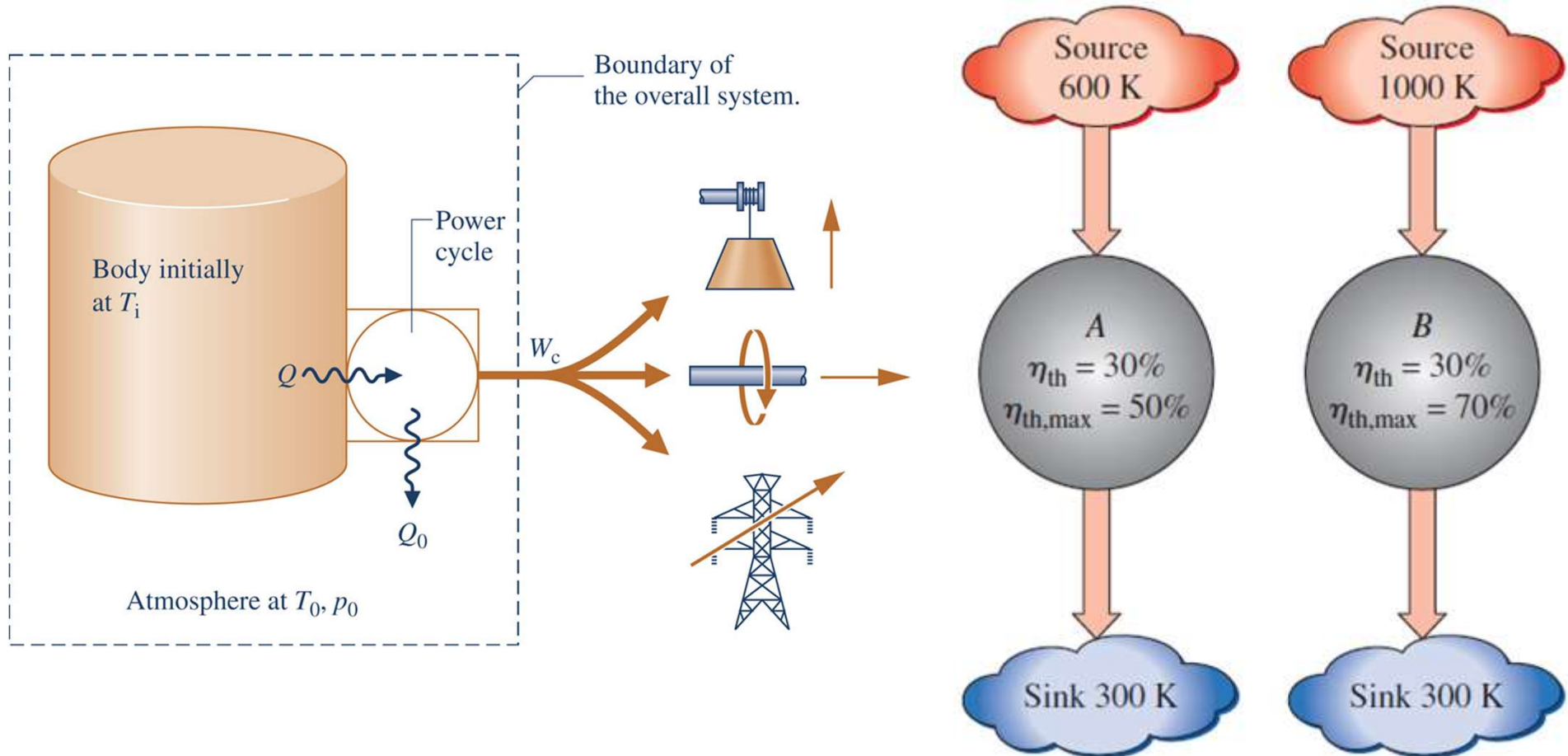
Quantifying Exergy Changes

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Previously: Best way to utilize energy resources?



$$\eta_{II} = \frac{\text{Exergy recovered}}{\text{Exergy expended}} = 1 - \frac{\text{Exergy destroyed}}{\text{Exergy expended}}$$

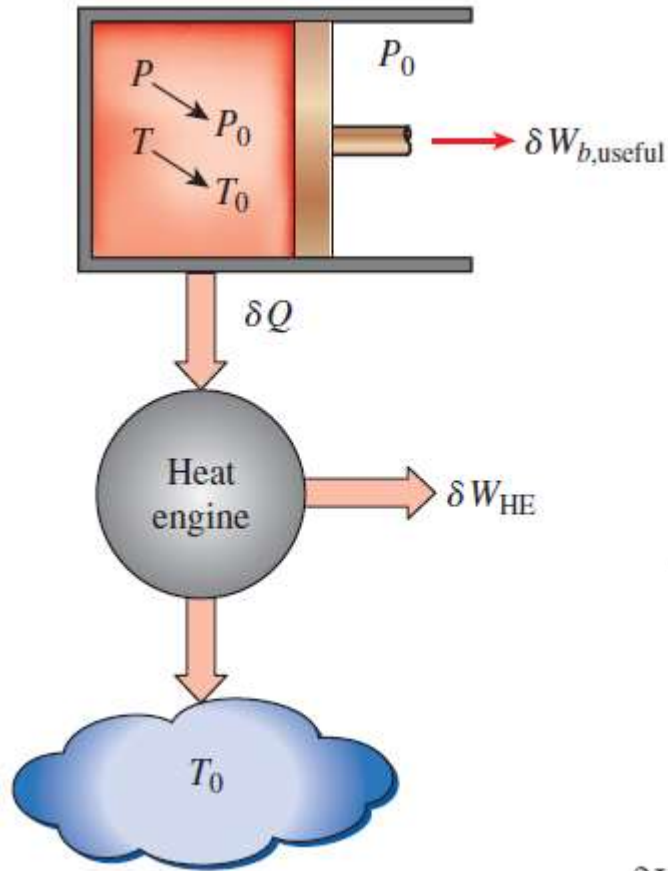
Some general features of exergy

- “Combination property”: Involves both system and surrounding
- Extensive **state** property that is **not conserved**

$$E = (U - U_0) + p_0(V - V_0) - T_0(S - S_0) + KE + PE$$

$$E_2 - E_1 = (U_2 - U_1) + p_0(V_2 - V_1) - T_0(S_2 - S_1) + (KE_2 - KE_1) + (PE_2 - PE_1)$$

Exergy of a fixed mass



$$\underbrace{\delta E_{in} - \delta E_{out}}_{\text{Net energy transfer by heat, work, and mass}} = \underbrace{dE_{system}}_{\text{Change in internal, kinetic, potential, etc., energies}}$$

$$-\delta Q - \delta W = dU$$

$$\delta W = P dV = (P - P_0) dV + P_0 dV = \delta W_{b,useful} + P_0 dV$$

$$\delta W_{HE} = \left(1 - \frac{T_0}{T}\right) \delta Q = \delta Q - \frac{T_0}{T} \delta Q = \delta Q - (-T_0 dS) \rightarrow$$

$$\delta Q = \delta W_{HE} - T_0 dS$$

$$\delta W_{\text{total useful}} = \delta W_{HE} + \delta W_{b,useful} = -dU - P_0 dV + T_0 dS$$

$$X = (U - U_0) + P_0(V - V_0) - T_0(S - S_0) + m \frac{V^2}{2} + mgz$$

Exergy changes in a closed system

$$\begin{aligned}\phi &= (u - u_0) + P_0(v - v_0) - T_0(s - s_0) + \frac{V^2}{2} + gz \\ &= (e - e_0) + P_0(v - v_0) - T_0(s - s_0)\end{aligned}$$

$$\begin{aligned}\Delta\phi &= \phi_2 - \phi_1 = (u_2 - u_1) + P_0(v_2 - v_1) - T_0(s_2 - s_1) + \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1) \\ &= (e_2 - e_1) + P_0(v_2 - v_1) - T_0(s_2 - s_1)\end{aligned}$$

$$\begin{aligned}\Delta X &= X_2 - X_1 = m(\phi_2 - \phi_1) = (E_2 - E_1) + P_0(V_2 - V_1) - T_0(S_2 - S_1) \\ &= (U_2 - U_1) + P_0(V_2 - V_1) - T_0(S_2 - S_1) + m\frac{V_2^2 - V_1^2}{2} + mg(z_2 - z_1)\end{aligned}$$

$$X_{\text{system}} = \int \phi \delta m = \int_V \phi \rho dV$$

Exergy can be zero but never negative

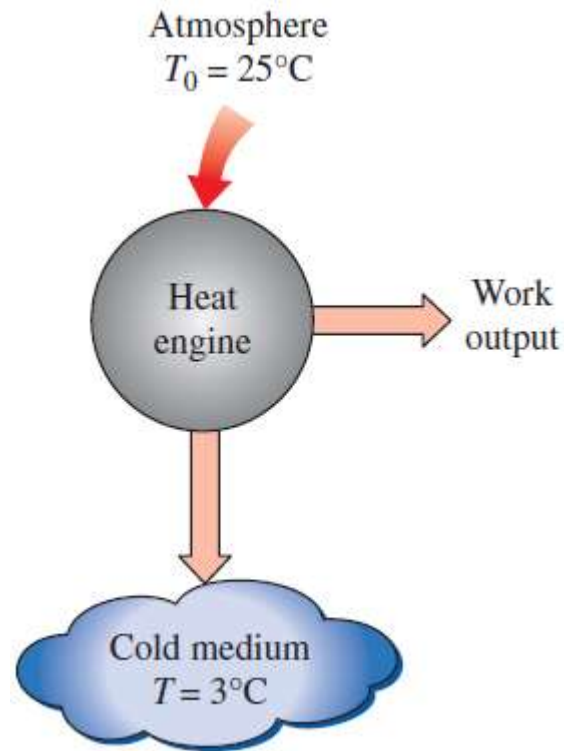
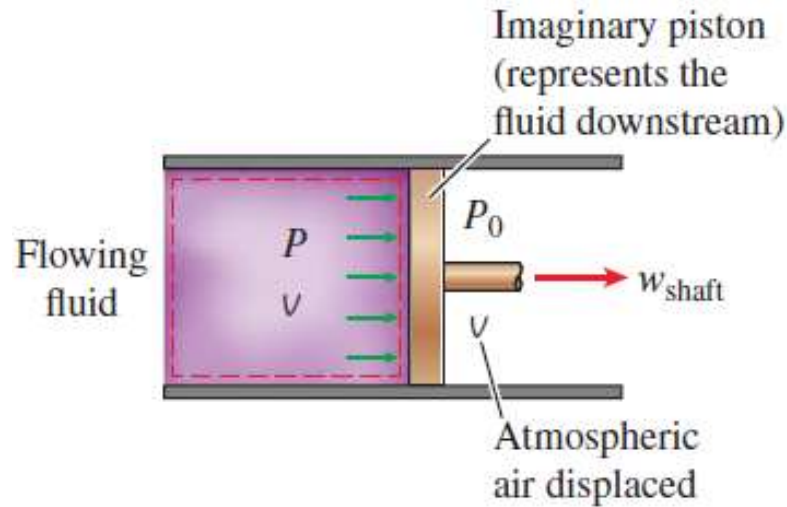


Fig-TD: Cengel & Boles

Exergy of flow system



$$x_{\text{flow}} = P\nu - P_0\nu = (P - P_0)\nu$$

$$P\nu = P_0\nu + w_{\text{shaft}}$$

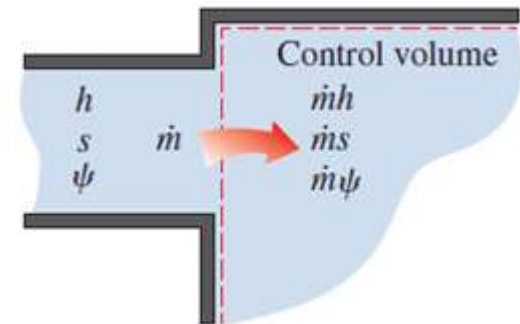
$$x_{\text{flowing fluid}} = x_{\text{nonflowing fluid}} + x_{\text{flow}}$$

$$= (u - u_0) + P_0(\nu - \nu_0) - T_0(s - s_0) + \frac{V^2}{2} + gz + (P - P_0)\nu$$

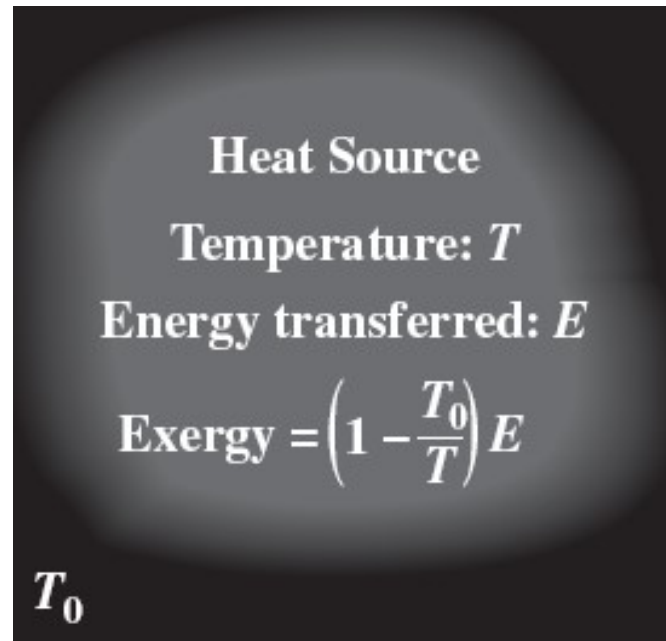
$$= (u + P\nu) - (u_0 + P_0\nu_0) - T_0(s - s_0) + \frac{V^2}{2} + gz$$

$$= (h - h_0) - T_0(s - s_0) + \frac{V^2}{2} + gz$$

$$\Delta\psi = \psi_2 - \psi_1 = (h_2 - h_1) + T_0(s_2 - s_1) + \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1)$$



Exergy of heat transfer



A dark rectangular box containing white text. The text lists the properties of a heat source and the formula for its exergy. At the bottom left of the box is the symbol T_0 .

Heat Source
Temperature: T
Energy transferred: E
Exergy = $\left(1 - \frac{T_0}{T}\right) E$
 T_0

$$X_{\text{heat}} = \int \left(1 - \frac{T_0}{T}\right) \delta Q$$

What's next?

- Exergy destruction, balance & 2nd law efficiency