Phase Equilibria & Kirchhoff Equation

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Previously: Thermal & Electrochemical combustion-Enthalpy & Gibbs Free Energy Changes

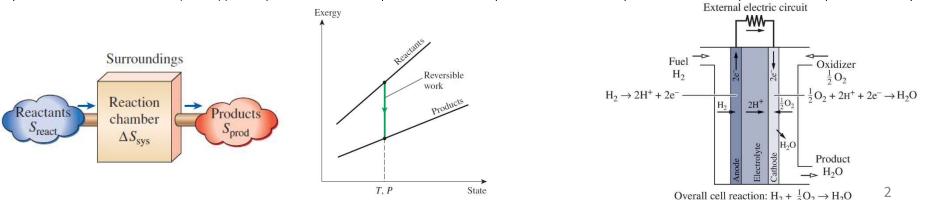
$$S_{\text{gen,adiabatic}} = S_{\text{prod}} - S_{\text{react}} \ge 0 \quad \overline{s}_{i}(T, P_{i}) = \overline{s}_{i}^{\circ}(T, P_{0}) - R_{u} \ln \frac{y_{i} P_{m}}{P_{0}}$$

$$X_{\text{destroyed}} = T_{0} S_{\text{gen}} \qquad (kJ) \qquad W^{\text{rev}} = \sum_{P} n_{i} \overline{g}_{i} - \sum_{P} n_{e} \overline{g}_{e} = -\Delta G$$

$$\Delta G = -nFE$$

Thermochemical Properties of Selected Substances at 298K and 1 atm

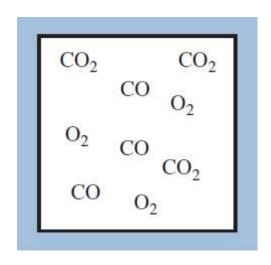
				011. 5 41		Heating Values	
Substance	Formula	Molar Mass, M (kg/ kmol)	Enthalpy of Formation, $\overline{h_f^o}$ (kJ/kmol)	Gibbs Function of Formation, \overline{g}_{f}^{o} (kJ kmol)	Absolute Entropy, \$° (kJ kmol·K)	Higher, HHV (kJ/kg)	Lower, LHV (kJ/kg)
Carbon	C(s)	12.01	0	0	5.74	32,770	32,770
Hydrogen	H ₂ (g)	2.016	0	0	130.57	141,780	119,950
Nitrogen	N ₂ (g)	28.01	0	0	191.50	_	_
Oxygen	O ₂ (g)	32.00	0	0	205.03	_	_
Carbon Monoxide	CO(g)	28.01	-110,530	-137,150	197.54	_	_
Carbon dioxide	CO ₂ (g)	44.01	-393,520	-394,380	213.69	_	_
Water	H₂O(g)	18.02	-241,820	-228,590	188.72	_	_
Water	H₂O(I)	18.02	-285,830	-237,180	69.95	_	_

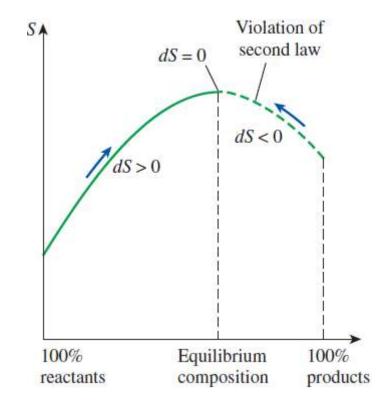


Figs: TD-Borgnakke & Sonntag; Moran, Shapiro, Boettner & Bailey; Cengel & Boles

From 2nd law to Chemical Equilibrium

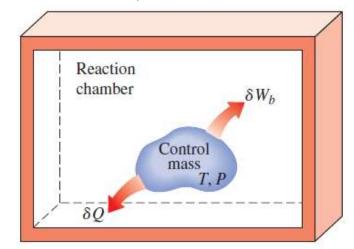
$$dS_{\rm sys} \ge \frac{\delta Q}{T}$$





Extremal condition for chemical equilibrium

$$\left. \begin{array}{l} \delta Q - P \, dV = dU \\ dS \geq \frac{\delta Q}{T} \end{array} \right\} \quad dU + P \, dV - T \, ds \leq 0$$

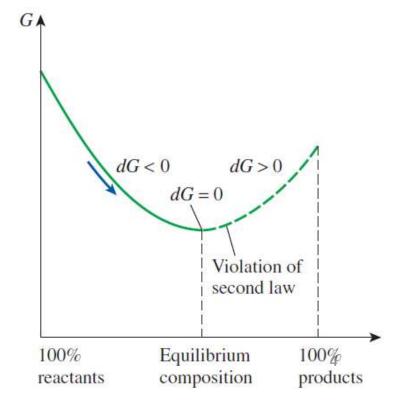


$$(dG)_{T,P} = dH - T dS - S dT$$

$$= (dU + P dV + V dP) - T dS - S dT$$

$$= dU + P dV - T dS$$

$$(dG)_{T,P} \le 0 \qquad (dG)_{T,P} = 0$$



Figs: TD-Cengel & Boles

Centrality of chemical potential/molar Gibbs function

Reaction
chamber
T, P
N_A moles of A
N_B moles of B
N_C moles of C
N_D moles of D
1999 1000 1990 1990 1990 1990 1990 1990
$dN_A A + dN_B B \to dN_C C + dN_D D$

$$\nu_A A + \nu_B B \Longrightarrow \nu_C C + \nu_D D$$

$$\nu_C \overline{g}_C + \nu_D \overline{g}_D - \nu_A \overline{g}_A - \nu_B \overline{g}_B = 0$$

Criterion for chemical equilibrium

$$(dG)_{T,P} = \sum (dG_i)_{T,P} = \sum (\overline{g}_i dN_i)_{T,P} = 0$$

$$\overline{g}_C dN_C + \overline{g}_D dN_D + \overline{g}_A dN_A + \overline{g}_B dN_B = 0$$

$$dN_A = -\varepsilon \nu_A \qquad dN_C = \varepsilon \nu_C$$

$$dN_B = -\varepsilon \nu_B \qquad dN_D = \varepsilon \nu_D$$

$H_2 \rightarrow 2H$
$0.1\text{H}_2 \rightarrow 0.2\text{H}$
$0.01\mathrm{H}_2\!\rightarrow 0.02\mathrm{H}$
$0.001\mathrm{H}_2 \rightarrow 0.002\mathrm{H}$
$v_{\rm H_2} = 1$
$v_{\rm H} = 2$

Chemical equilibrium of ideal-gas mixtures

$$u_C \overline{g}_C + \nu_D \overline{g}_D - \nu_A \overline{g}_A - \nu_B \overline{g}_B = 0$$
Criterion for chemical equilibrium

$$(\Delta \overline{g})_{T} = \Delta \overline{h}^{>0} T(\Delta \overline{s})_{T} = -T(\Delta \overline{s})_{T} = R_{u}T \ln \frac{P_{2}}{P_{1}}$$

$$v_{C}[\overline{g}_{C}^{*}(T) + R_{u}T \ln P_{C}] + v_{D}[\overline{g}_{D}^{*}(T) + R_{u}T \ln P_{D}]$$

$$-v_{A}[\overline{g}_{A}^{*}(T) + R_{u}T \ln P_{A}] - v_{B}[\overline{g}_{B}^{*}(T) + R_{u}T \ln P_{B}] = 0$$

$$\Delta G^{*}(T) = v_{C}\overline{g}_{C}^{*}(T) + v_{D}\overline{g}_{D}^{*}(T) - v_{A}\overline{g}_{A}^{*}(T) - v_{B}\overline{g}_{B}^{*}(T)$$

$$\Delta G^{*}(T) = -R_{u}T(v_{C}\ln P_{C} + v_{D}\ln P_{D} - v_{A}\ln P_{A} - v_{B}\ln P_{B}) = -R_{u}T \ln \frac{P_{c}^{v_{C}}P_{D}^{v_{D}}}{P_{A}^{v_{D}}P_{B}^{v_{B}}}$$

$$K_{P} = \frac{P_{C}^{v_{C}}P_{D}^{v_{D}}}{P_{A}^{v_{A}}P_{B}^{v_{B}}}$$

$$K_{P} = e^{-\Delta G^{*}(T)/R_{u}T}$$

$$P_{i} = y_{i}P = \frac{N_{i}}{N_{\text{total}}}P$$

$$K_{P} = \frac{N_{C}^{v_{C}}N_{D}^{v_{D}}}{N_{A}^{v_{A}}N_{B}^{v_{B}}} \left(\frac{P}{N_{\text{total}}}\right)^{\Delta v}$$

$$\Delta v = v_{C} + v_{D} - v_{A} - v_{B}$$

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$\mathcal{K}_p(T)$, Van't Hoff & Kirchhoff equation

$$\ln K_{P} = -\frac{\Delta G^{*}(T)}{R_{u}T} \qquad \qquad \frac{d(\ln K_{p})}{dT} = \frac{\Delta H^{*}(T)}{R_{u}T^{2}} - \frac{d[\Delta H^{*}(T)]}{R_{u}T dT} + \frac{d[\Delta S^{*}(T)]}{R_{u} dT}$$

$$T ds = dh - v dP$$

$$T d(\Delta S^*) = d(\Delta H^*)$$

$$\frac{d(\ln K_p)}{dT} = \frac{\Delta H^*(T)}{R_u T^2} = \frac{\overline{h}_R(T)}{R_u T^2}$$

$$\ln \frac{K_{P_2}}{K_{P_1}} \cong \frac{\overline{h}_R}{R_u} \left(\frac{1}{T_1} - \frac{1}{T_2} \right)$$

$$\left(\frac{\partial h_i}{\partial T}\right)_{\mathbf{p}} = c_{\mathbf{p_i}}$$

$$\frac{\mathrm{d}\Delta H}{\mathrm{d}T} \equiv \frac{\mathrm{d}}{\mathrm{d}T} (\Sigma \nu_i h_i)$$
$$= \Sigma \nu_i c_{p_i},$$

Fundamental equations of TD (Table TD)

Function	Extremum at Equilibrium	Fundamental Equation	Definition
$U(S, V, \mathbf{N})$	Minimum	$dU = T dS - p dV + \sum_{j} \mu_{j} dN_{j}$	
$S(U, V, \mathbf{N})$	Maximum	$dS = \left(\frac{1}{T}\right) dU + \left(\frac{p}{T}\right) dV - \sum_{j} \left(\frac{\mu_{j}}{T}\right) dN_{j}$	
$H(S, p, \mathbf{N})$	Minimum	$dH = T dS + V dp + \sum_{j} \mu_{j} dN_{j}$	H = U + pV
$F(T, V, \mathbf{N})$	Minimum	$dF = -S dT - p dV + \sum_{j} \mu_{j} dN_{j}$	F = U - TS
$G(T,p,{\sf N})$	Minimum	$dG = -S dT + V dp + \sum_{j} \mu_{j} dN_{j}$	G = H - TS = F + pV

The Limits on Constructing Thermodynamic Functions

What are the limits on constructing functions of T, S, p, V, N, U, F, H, and G? You can divide thermodynamic functions into four categories:

FUNDAMENTAL AND USEFUL. Table **TD** lists the main fundamental thermodynamic functions and their natural variables. The states of equilibrium are identified by extrema in these functions.

USEFUL BUT NOT FUNDAMENTAL. U(T,V,N), S(T,V,N), H(T,p,N), and S(T,p,N) are not functions of natural variables. These functions do not have corresponding extremum principles, but they are useful because they are components of F(T,V,N) and G(T,p,N).

COMPLETE BUT NOT USEFUL. Rearrangements of the dependent and independent variables from a fundamental thermodynamic function are possible, but not often useful. For example, T(F, V, N) is a rearrangement of the fundamental Helmholtz free energy function, F(T, V, N). This function is not very useful because you usually cannot constrain F at the system boundary.

INCOMPLETE. Additional functions could be constructed, such as U(p, V, N) or $S(U, \mu, N)$ but because these involve conjugate pairs p and V, or μ and N, and are missing other variables, they do not uniquely specify the state of a system. Such functions cannot be obtained by Legendre transforms of the fundamental equations.

What's next?

• Phase rule