

- a) Estimate the overall heat transfer coefficient  $u_i$  at the section where the water is at  $40^\circ\text{C}$ . Assume fully developed conditions.
- b) Determine the length of the tube required to condense  $0.05 \text{ kg/s}$  of steam, assuming that the overall heat transfer coefficient determined in part (a) is uniform.

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**ME - 605****B.E. VI Semester**

Examination, June 2013

**Heat and Mass Transfer****Time : Three Hours****Maximum Marks : 70/100**

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**Note:** Solve all the questions, internal choice is given with all the questions, missing data is to be assumed suitably.

1. Saturated steam at  $200^\circ\text{C}$  flows inside a  $5\text{cm}$  O.D. Carbon steel tube with a wall thickness of  $3\text{mm}$ . The tube surface is insulated with  $5\text{cm}$  thick fiberglass. The surface heat transfer coefficient on the steam and air sides are  $8000 \text{ W/m}^2\text{ }^\circ\text{C}$  and  $10 \text{ W/m}^2\text{ }^\circ\text{C}$  respectively. If the temperature of the outside air is  $25^\circ\text{C}$ .

Determine :

- a) Heat transfer rate per meter length of the tube
- b) The temperature of the outer surface of the insulation.
- c) The rate of condensation of steam per meter length of the tube.

OR

Consider two long, hollow cylinders of an insulating material of the same axial length. Cylinder 1 has an ID of  $25\text{mm}$  and OD of  $50\text{mm}$ . Cylinder 2 has an ID of  $100\text{mm}$  and an OD of  $175\text{mm}$ . For the same inner and outer surface temperatures in both cases, find the ratio of heat transfer rates  $q_1/q_2$ .

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OR

Write short notes on following :

- a) Regimes of Pool Boiling
- b) Film wise and drop wise condensation.

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[2]

2. Coffee, initially at  $80^{\circ}\text{C}$ , is served in a silver cup which is modeled as a 6cm diameter, 5cm high cylinder. Assuming that the properties of the coffee are the same as those of water and the heat capacity of the cup (the product of the mass of the cup and its specific heat) is negligible compared with the heat capacity of the coffee. Estimate the temperature of the coffee 10 minutes later if the surface heat transfer coefficient (on all surface including the top) is  $6 \text{ W/m}^2 \text{ }^{\circ}\text{C}$ . Air at  $20^{\circ}\text{C}$ . Surrounds the entire cup and that the effect of evaporation from the top surface is 0 accounted for in the value of the surface heat transfer coefficient.

OR

Stainless steel balls of 4mm diameter, initially at  $30^{\circ}\text{C}$ , are heated for 1min with air at  $95^{\circ}\text{C}$  with a surface heat transfer coefficient of  $40 \text{ W/m}^2 \text{ }^{\circ}\text{C}$  and then cooled in  $20^{\circ}\text{C}$  with a surface heat transfer coefficient of  $20 \text{ W/m}^2 \text{ }^{\circ}\text{C}$  for 1 min. What is the temperature of the balls when they are removed from the cool air.

3. An experimental apparatus consists of a flat plate, 1m long in the diversion of flow 0.6m wide, and 4mm thick maintained at  $40^{\circ}\text{C}$ . The water at  $20^{\circ}\text{C}$  flows parallel to the plate with a free stream velocity of 3m/s. Estimate the heat fluxes at a distance of 1cm and 50 cm from the leading edge and the total Heat transfer rate from one surface. Take the properties of water at mean film temperature of  $30^{\circ}\text{C}$  as below:-

$$\begin{aligned}\rho &= 995.6 \text{ kg/m}^3 \\ C_p &= 4183 \text{ J/kg }^{\circ}\text{C} \\ K &= 0.6154 \text{ W/m }^{\circ}\text{C} \\ \mu &= 797.7 \times 10^{-6} \text{ N-s/m}^2 \\ Pr &= 5.422\end{aligned}$$

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[3]

OR

A room heater is modeled as a series of 40 vertical plates, each 400mm high, 150mm wide and 15mm thick. If the temperature of the surface of the plates and air are  $60^{\circ}\text{C}$  and  $10^{\circ}\text{C}$  respectively, estimate the heat transfer rate to the air by natural convection from the vertical surfaces. The properties of air at mean film temperature of  $35^{\circ}\text{C}$  are as below :

$$\begin{aligned}\rho &= 1.146 \text{ kg/m}^3 \\ C_p &= 1007 \text{ J/kg }^{\circ}\text{K} \\ K &= 0.02625 \text{ W/m }^{\circ}\text{K} \\ \mu &= 1.895 \times 10^{-5} \text{ N-s/m}^2 \\ Pr &= 0.7268 \text{ and} \\ \beta &= 3.532 \times 10^{-3} / ^{\circ}\text{K}\end{aligned}$$

4. In an oil cooler for a diesel engine 0.1kg/s of oil (specific heat =  $2131 \text{ J/kg }^{\circ}\text{C}$ ) is to be cooled from  $120^{\circ}\text{C}$  to  $60^{\circ}\text{C}$  in a double pipe heat exchanger with 0.1 kg/s of water available at  $10^{\circ}\text{C}$ . The over all heat transfer coefficient is  $400 \text{ W/m}^2 \text{ }^{\circ}\text{C}$ . Determine the heat transfer surface area if the flow is
- Parallel
  - Counter flow

OR

Dry saturated steam at  $100^{\circ}\text{C}$  enters the annulus of a double pipe, horizontal heat exchanger with negligible velocity. It is condensed on the outer surface of the 3mm thick, 25mm outside diameter type 316 stainless steel tube. Water at  $30^{\circ}\text{C}$  enters the tube with a mass flow rate of 0.6 kg/s.

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