

Introduction to Turbulence Modeling

or Why Turbulence Modeling is Black Magic

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Reynolds Averaged Navier Stokes

Let $\phi = \bar{\phi} + \phi'$, where

$$\bar{\phi} = \lim_{T \rightarrow \infty} \int_{t_0}^{t_0+T} \phi(t) dt$$

Interested in solving for \bar{u}_i . Nondimensionalizing such that $\rho = 1$,

Continuity Equation

$$\frac{\partial u_i}{\partial x_i} = 0$$

\Downarrow

$$\frac{\partial \bar{u}_i}{\partial x_i} = 0$$

Momentum Equation

$$\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{1}{Re} \frac{\partial^2 u_i}{\partial x_j \partial x_j}$$

\Downarrow

$$\frac{\partial \bar{u}}{\partial t} + \bar{u}_j \frac{\partial \bar{u}_i}{\partial x_j} = -\frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} \left[-\overline{u'_i u'_j} + \frac{1}{Re} \frac{\partial \bar{u}_i}{\partial x_j} \right]$$

But the Reynolds stress, $\overline{u'_i u'_j}$ is an unclosed quantity.

Modeling the Reynolds Stress

$$\frac{\partial \bar{u}}{\partial t} + \bar{u}_j \frac{\partial \bar{u}_i}{\partial x_j} = -\frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_j} \left[-\overline{u'_i u'_j} + \frac{1}{Re} \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \right]$$

Eddy Viscosity Hypothesis

$$\overline{u'_i u'_j} = -\nu_T \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) + \frac{2k}{3} \delta_{ij}$$

where $k = \frac{1}{2} \overline{u'_i u'_i}$.

This assumption is fundamentally flawed, but useful.

We still need a model for ν_T and k .

Spalart-Allmaras Model

- Model the eddy viscosity
- Assume k is negligible
- Surprisingly decent for the types of flows it was designed for
 - ▶ External aerodynamics with minimal flow separation
- Highly nonlinear equation

$$\frac{\partial \tilde{\nu}}{\partial t} + \bar{u}_j \frac{\partial \tilde{\nu}}{\partial x_j} = C_{b1} [1 - f_{t2}] \tilde{S} \tilde{\nu} + \frac{1}{\sigma} \left\{ \nabla \cdot [(\nu + \tilde{\nu}) \nabla \tilde{\nu}] + C_{b2} |\nabla \tilde{\nu}|^2 \right\} \\ - \left[C_{w1} f_w - \frac{C_{b1}}{\kappa^2} f_{t2} \right] \left(\frac{\tilde{\nu}}{d} \right)^2 + f_{t1} \Delta U^2$$

$$\nu_T = \tilde{\nu} f_{v1}, \quad f_{v1} = \frac{\chi^3}{\chi^3 + \nu_{v1}^3}, \quad \chi = \frac{\tilde{\nu}}{\nu} \quad \dots$$

$k - \epsilon$ Exact Equations

Turbulence Kinetic Energy Equation

$$\frac{\partial k}{\partial t} + \bar{u}_i \frac{\partial k}{\partial x_i} = -\overline{u'_i u'_j} \frac{\partial \bar{u}_i}{\partial x_j} - \frac{\partial}{\partial x_i} \left(\frac{1}{2} \overline{u'_j u'_j u'_i} + \overline{p' u'_i} \right) + \nu \frac{\partial^2 k}{\partial x_i \partial x_i} - \epsilon$$

Dissipation Equation

$$\frac{\partial \epsilon}{\partial t} + \bar{u}_i \frac{\partial \epsilon}{\partial x_i} = \nu \frac{\partial^2 \epsilon}{\partial x_i \partial x_i} + P_\epsilon + D_\epsilon - \Phi_\epsilon$$

$$P_\epsilon = -2\nu \left[\overline{\frac{\partial u'_i}{\partial x_j} \frac{\partial u'_k}{\partial x_j} \frac{\partial \bar{u}_i}{\partial x_k}} + \overline{\frac{\partial u'_j}{\partial x_i} \frac{\partial u'_j}{\partial x_k} \frac{\partial \bar{u}_i}{\partial x_k}} + \overline{u'_k \frac{\partial u'_i}{\partial x_j} \frac{\partial^2 \bar{u}_i}{\partial x_k \partial x_j}} + \overline{\frac{\partial u'_i}{\partial x_k} \frac{\partial u'_i}{\partial x_m} \frac{\partial u'_k}{\partial x_m}} \right]$$

$$D_\epsilon = -\frac{\partial}{\partial x_k} \left(\overline{u'_k \epsilon'} + 2\nu \overline{\frac{\partial p'}{\partial x_m} \frac{\partial u'_k}{\partial x_m}} \right)$$

$$\Phi_\epsilon = 2\nu^2 \overline{\frac{\partial^2 u'_i}{\partial x_k \partial x_m} \frac{\partial^2 u'_i}{\partial x_k \partial x_m}}$$

$k - \epsilon$ Approximations

Turbulence Kinetic Energy Equation

$$\frac{1}{2} \overline{u'_j u'_j u'_i} + \overline{p' u'_i} \approx - \frac{\nu_T}{\sigma_k} \frac{\partial k}{\partial x_i}$$

Dissipation Equation

From dimensional analysis

$$\nu_T \approx C_\mu \frac{k^2}{\epsilon}$$

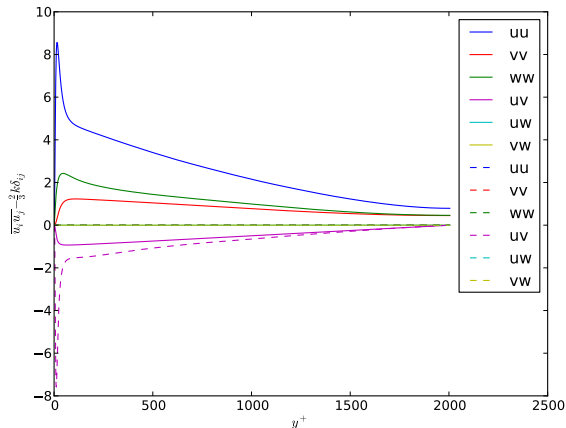
$$P_\epsilon \approx -C_{\epsilon 1} \frac{\epsilon}{k} \overline{u'_i u'_j} \frac{\partial \bar{u}_i}{\partial x_j}$$

$$\Phi_\epsilon \approx C_{\epsilon 2} \frac{\epsilon^2}{k}$$

From gradient transport model

$$D_\epsilon \approx \frac{\partial}{\partial x_i} \left(\frac{\nu_T}{\sigma_\epsilon} \frac{\partial \epsilon}{\partial x_i} \right)$$

Channel Flow Predictions

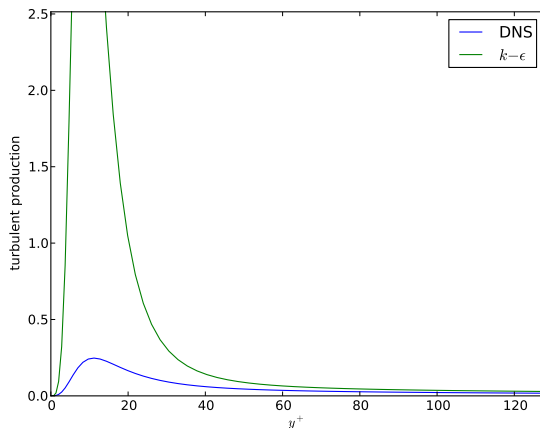


$$\overline{u'_i u'_j} - \frac{2}{3} k \delta_{ij}$$

$$\approx -\nu_T \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right)$$

Figure: Reynolds Stress Components

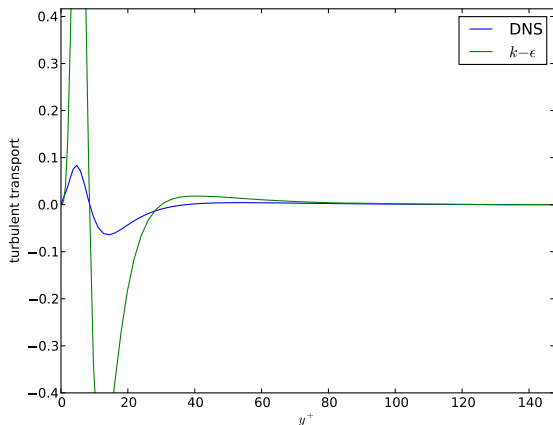
Channel Flow Predictions



$$\overline{u'_i u'_j} \frac{\partial \bar{u}_i}{\partial x_j} \approx C_\mu \frac{k^2}{\epsilon} \left(\frac{\partial \bar{u}_i}{\partial x_j} + \frac{\partial \bar{u}_j}{\partial x_i} \right) \frac{\partial \bar{u}_i}{\partial x_j}$$

Figure: Production of Turbulent Kinetic Energy

Channel Flow Predictions



$$\frac{\partial}{\partial x_i} \left(\frac{1}{2} \overline{u'_k u'_k u'_i} + \overline{p' u'_i} \right) \approx - \frac{\partial}{\partial x_i} \left(\frac{\nu_T}{\sigma_k} \frac{\partial k}{\partial x_i} \right)$$

Figure: Transport of Turbulent Kinetic Energy

Channel Flow Predictions

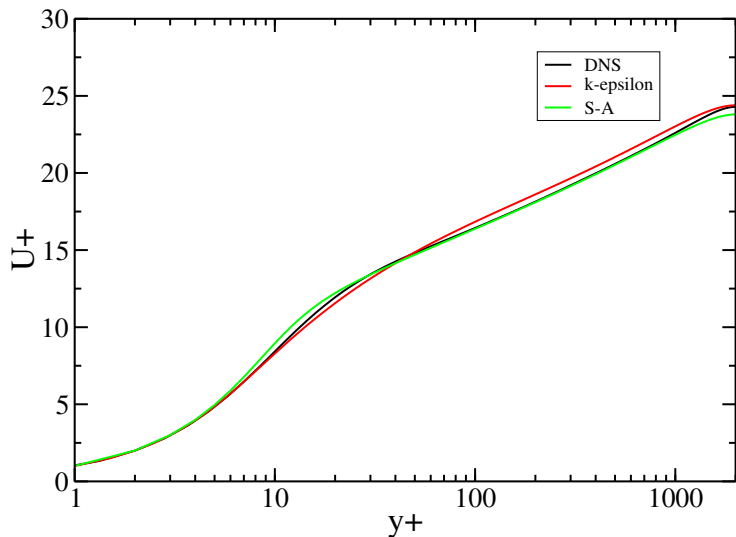


Figure: Time averaged velocity profile $Re = 2000$

Channel Flow Predictions

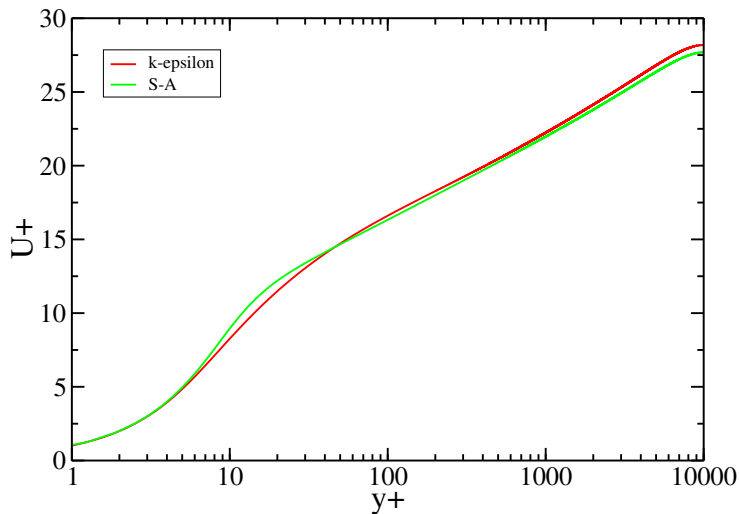


Figure: Time averaged velocity profile $Re = 10000$

Channel Flow Predictions

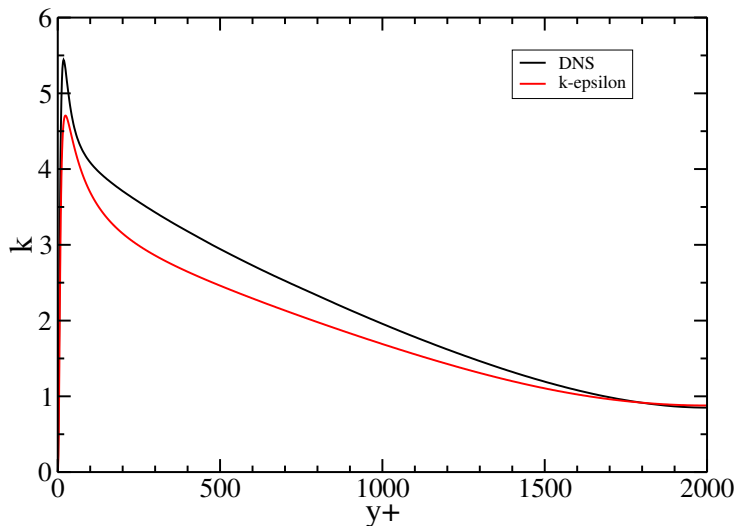


Figure: Turbulence kinetic energy profile $Re = 2000$

Channel Flow Predictions

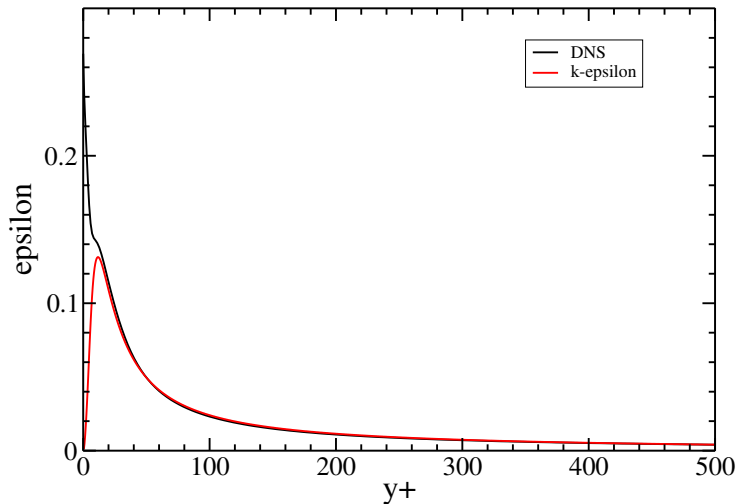


Figure: Dissipation profile $Re = 2000$

Notes on $k - \epsilon$

Fixes near the wall

- Wall functions
- Two-layer models
- SST $k - \omega$
- $\overline{v^2} - f$ four equation model (f is an elliptic relaxation function)

Boundary conditions

- BC on ϵ is not obvious
- Enforce both $k = 0$ and $\frac{\partial k}{\partial n} = 0$ at walls.

Popularity

- One of the earliest models
- Physically motivated derivation
- Insensitive to freestream conditions on k and ϵ

Typical Solution Procedure

From a presentation by a Fluent engineer

- Start calculations by performing 100 iterations or so with standard $k - \epsilon$ model and first order upwind differencing. For very simple flows (no swirl or separation) converge with second order upwind and $k - \epsilon$ model.
- If the flow involves jets, separation, or moderate swirl, converge solution with the realizable $k - \epsilon$ model and second order differencing.
- If the flow is dominated by swirl converge solution deeply using RSM and a second order differencing scheme. If the solution will not converge, use first order differencing instead.

Wilcox (1993) $k - \omega$ Model

Turbulence Kinetic Energy Equation

$$\frac{\partial k}{\partial t} + \bar{u}_j \frac{\partial k}{\partial x_j} = 2\nu_T |S|^2 - C_\mu k\omega + \frac{\partial}{\partial x_j} \left(\left(\nu + \frac{\nu_T}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \right)$$

Specific Dissipation Equation

$$\frac{\partial \omega}{\partial t} + \bar{u}_j \frac{\partial \omega}{\partial x_j} = 2C_{\omega 1} |S|^2 - C_{\omega 2} \omega^2 + \frac{\partial}{\partial x_j} \left(\left(\nu + \frac{\nu_T}{\sigma_\omega} \right) \frac{\partial \omega}{\partial x_j} \right)$$

$$\omega \equiv \frac{\epsilon}{C_\mu k}$$

$$\nu_T = \frac{k}{\omega}$$

Notes on $k - \omega$

Wall Treatment

- Formally, ω is singular at a perfectly smooth wall
- Numerically, this is fixed by assuming a finite roughness
 - ▶ $\omega_{wall} = \frac{40000\nu_{wall}}{k_s^2}$, need $\frac{u_\tau k_s}{\nu} < 5$
- Produces decent results at the wall
- Can perform the same trick with two BCs on k

Other Notes

- Early models were very sensitive to freestream conditions on ω
- Menter proposed SST model to overcome this shortcoming
- Possible to write a $k - \epsilon$ model with $k - \omega$ “physics”

Other Ideas – Unsteady RANS

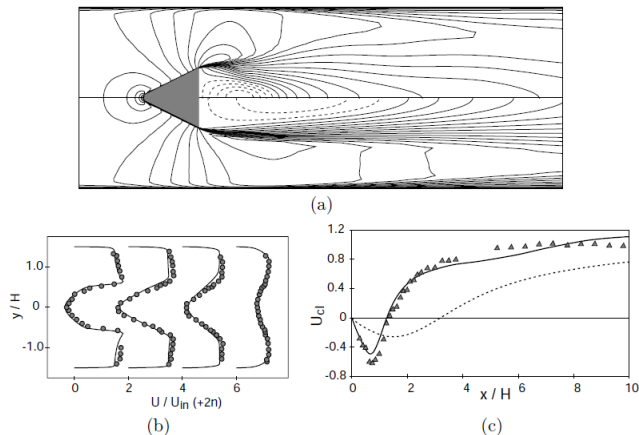
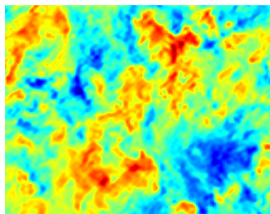


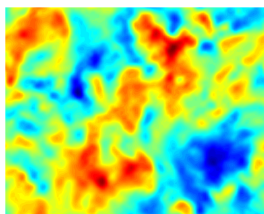
Figure 7.72 Vortex shedding from a triangular cylinder. (a) composite showing time-average contours of U in the upper half, versus a steady solution in the lower half. The dashed lines indicate negative velocity. (b) time-averaged velocity profiles in the wake. (c) velocity along centerline: time-average, ———; steady computation, - - - - (Durbin, 1995).

Other Ideas

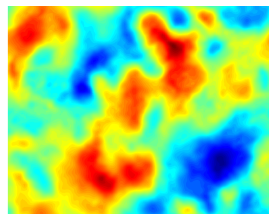
- Large Eddy Simulation
- Reynolds Stress Models
 - ▶ Elliptic relaxation model solves 18 coupled, highly nonlinear PDEs
- Variational Multiscale
- Direct Numerical Simulation



DNS Velocity Field



Filtered Velocity Field
 $\Delta = L/32$



Filtered Velocity Field
 $\Delta = L/16$