Laminar and Turbulent flow

A laminar flow is one in which paths teken by the Individual particles do not cross one another and moves along well defined paths. It is also called streams line flow or viscous flow, eg Flow through capillary tube, flow of blood in Veins and arteries and ground water flow.

Turbulent flow is and in which flow in which fluid Particles move in a 3ig-zag way, ers high relocity flow in a Conduit of large size. Mearly all fluid flow problems encountered in engineering practice have a turbulent Characteristics.

Laminar and Turbulent flow are exerceterized on the basis of Reynolds number (Re)

For Reynolds Number (Re) < 2000 flow in pipes is laminer for Reynolds number (Re) 4000 Flow in pipe is turbulent For Reynolds Almber (Re) between 2000 and 4000 flow in the Pupe could be laminer or turbulent.

Types of flow lines

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Stream line: May be define as an imaginary line within the flow so that the tangent at any point on it melicates the relocity at that point.

Stream tube: 15 a fluid mass bounded by a group of
Streamlines. The contents of a stream
tube is known as "current filement"

streak line is a curve which gives an Instantaneous Preture of the location of the fluid particles, which have passed through a given point.

TYPES OF HEADS (OR ENERGIES) OF A LIQUIS

There are 3 types of heads (energies) of flowing liquid

1. Potential head or Potential energy is the potential energy

Per unit weight of fluid with respect to an arbitrary

datum of the fluid. It is denoted by Z is in The I/N or m

2. Pressure head. This is due to ressure of thowing liquid and is measure as P/Hy where P is ressure the flow and by is weight density of triguidity. It is the pressure enersy per unit weight of third. It represents the work done in prishing a body of third by fished pressure P=

3. Velocity head or Kinetic energy - This is due to the prossure relocity of flowing liquid and is measure is V2/29 where V = Velocity of flowing and 9 is acceleration the growthy to in J/N or m.

Total head or Total enersy - Total head of a liquid Particle in motion is the sum of its potential head, Kinetic head and Pressure head, Mathematically

Total head H = Z + \frac{12}{29} + \frac{1}{20} m of Irguid

Total energy = $2 + \frac{12}{29} + \frac{1}{29}$ Hm/kg of liquid

QUESTION - In a pipe of 90 mm diameter water is thowing with a mean velocity of 2mls and at a gauge pressure of 350 KN/m². Determine the total head, if the pipe is 8 metres above the datum line alegiecting frictim.

Solution

Diameter of Pipe = 90mm

Pressure, $P = 350 \text{ KN/m}^2$ Value of Water, V = 2m/sSchum head Z = 8mSpecific weight of water $W = 9.81 \text{ KN/m}^3$ Total head $H = 2 + \frac{\sqrt{2}}{2g} + \frac{P}{H}$ $A = 8 + \frac{2}{2x9.81} + \frac{350}{9.81}$

H = 43.88m

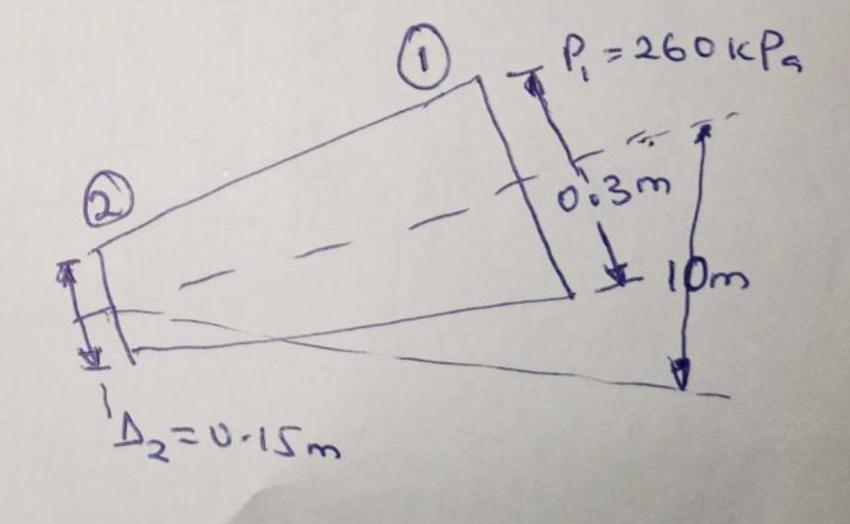
ANSINA QUESTION

Water flows in a circular pipe. At one section the chamber is 0.3 mg The stetic pressure is 260 kPagauge, the velocity is 3 mls and the elevation is 10 mm above ground level. The elevation at 10 a section clown stream is 0 m, and the pipe diameter is 0.15 m. Find the gauge pressure at the downstream section; bensity of water = 999 kg/m3

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$$D_1 = 0.30 \text{ m}$$
 $D_2 = 0.15 \text{ m}$
 $Z_4 = 0$
 $Z_2 = 10 \text{ m}$
 $Z_2 = 10 \text{ m}$
 $V_1 = 260 \text{ KPa}$
 $V_1 = 3 \text{ m/s}$

P = 999 Kg/m3



from continuity equietion,
$$A_1V_1 = A_2V_2$$

$$V_2 = \frac{A_1V_1}{A_2} = \frac{\left(\frac{\Delta}{4} \Delta_1^2\right)}{\left(\frac{\Delta}{4} \Delta_2^2\right)}V_1$$

$$= \left(\frac{\Delta_1}{\Delta_2}\right)^2 \times V_1 = \frac{\left(\frac{0.3}{4} \Delta_2^2\right)}{\left(\frac{0.15}{4} \Delta_2^2\right)} \times 3$$

$$= 12 \text{ m/s}$$

Weight density of water, $w = pg = 999 \times 9.81$.

= 9800.19 N/m³

From Bernolllis equation between 1 and 2 Section (neglecting friction effects as given) we have

$$\frac{P_1}{W} + \frac{\sqrt{2}}{29} + \frac{7}{2} + \frac{\sqrt{2}}{29} + \frac{7}{29}$$

$$=\frac{360 \times 1000}{9800 \cdot 19} + \frac{(3)^{2}}{9800 \cdot 19} + \frac{(3)^{2}}{2 \times 9.81} + 10 = \frac{P_{2}}{9800 \cdot 19} + \frac{(12)^{2}}{2 \times 9.81} + 0$$

$$26.53 + 0.439 + 10 = \frac{P_2}{9800.15} + 7.34$$

BERNOULLI'S EQUATION FOR REAR FLUID

The earlier equation was based on the assumption that fluid is non-viscous and therefore frictionless. Practically all fluids are real and not Ideal and hence are viscous and therefore there are always some losses in fluid flows. The losses hade to be taken into Consideration in the application of Bernsulli's equation

For real fluid

$$\frac{P_1}{N} + \frac{V_1^2}{29} + Z_1 = \frac{P_2}{N} + \frac{V_2^2}{25} + Z_2 + h_1$$

he 2 hoss of energy between Sechino 1 and 2

QUESTIONS

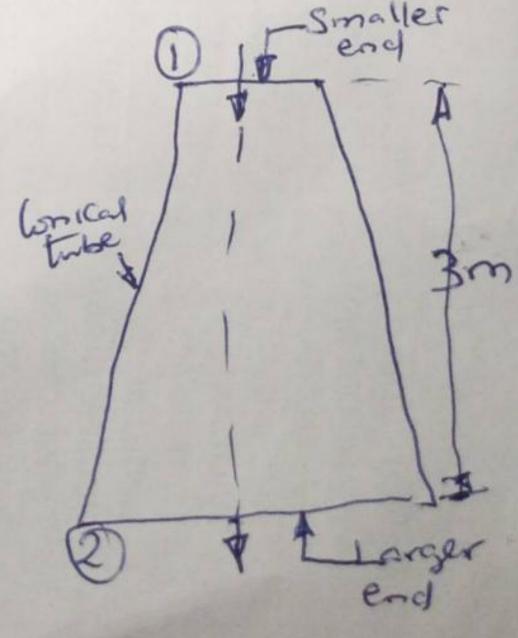
The follow data relates to a conical tube of length 3.0m fixed verticity with its smaller end upwards and corrying fluid in the downward clirection; The rewaity of flow at the small end is 10 mls while at large End is 4 mls

where V, and Va are relocation at the smaller and larger ends respectively. Pressure head at The smaller end w 4m of liquid. Determine the pressure head at The

larger end.

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Length of tube l = 3.0 mVelocity, $V_1 = 10 \text{ m/s}$ Pressure head, $\frac{p_1}{W} = 4 \text{ m of liquid}$ Velocity, $V_2 = 4 \text{ m/s}$ Loss of head $h_1 = \frac{0.4(v_1 - v_2)^2}{2 \times 9.81} = \frac{0.4(10 - 4)^2}{2 \times 9.81}$ $\frac{29}{29} = 0.73 \text{ m}$



pressure head at the larger end, B

Applying Bernoulli's equation at sections (1) and (2) $\frac{P_1}{N} + \frac{V_1^2}{29} + Z_1 = \frac{P_2}{N} + \frac{V_2^2}{29} + Z_2 + h_L$

Let the datum line Passes through Section 2

$$4 + \frac{10^2}{29} + 3 = \frac{p_2}{2} + \frac{4^2}{29} + 0 + 0.73$$

$$=4+5.09+3=\frac{P_2}{W}+0.815+0.73$$