

- 16.5.** For the activated-sludge unit shown in Fig. 16.7, the specific growth rate of cells is given by

$$\mu_{\text{net}} = \frac{\mu_m S}{K_s + S} - k_d$$

The following parameter values are known:  $F = 500 \text{ l/h}$ ,  $\alpha = 0.4$ ,  $\gamma = 0.1$ ,  $X_e = 0$ ,  $V = 1500 \text{ l}$ ,  $K_s = 10 \text{ mg/l}$ ,  $\mu_m = 1 \text{ h}^{-1}$ ,  $k_d = 0.05 \text{ h}^{-1}$ ,  $S_0 = 1000 \text{ mg/l}$ ,  $Y_{X/S}^M = 0.5 \text{ g dw/g substrate}$ .

- a. Calculate the substrate concentration ( $S$ ) in the reactor at steady state.
  - b. Calculate the cell concentration(s) in the reactor.
  - c. Calculate  $X_r$  and  $S_r$  in the recycle stream.
- 16.6.** In a trickling biological filter, the BOD value of the feed stream is  $S_{0i} = 500 \text{ mg/l}$  with a feed flow of  $F = 10^3 \text{ l/h}$ . The effluent BOD value is desired to be  $S_0 = 10 \text{ mg/l}$ . The following kinetic parameters for the biocatalysts are known:  $r_m = 20 \text{ mg/S/l} \cdot \text{h}$  and  $K_s = 200 \text{ mg S/l}$ . The biofilm thickness is  $L = 0.1 \text{ mm}$ . The cross-sectional area of the filter is  $A = 2 \text{ m}^2$ , and the biofilm surface area per unit volume of the bed is  $a = 500 \text{ cm}^2/\text{cm}^3$ . Assume that dissolved oxygen is the rate-limiting substrate and the diffusion coefficient of oxygen is  $D_{O_2} = 2 \times 10^{-5} \text{ cm}^2/\text{s}$ . Determine the required height of the bed. You can assume first-order bioreaction kinetics.
- 16.7.** An activated-sludge waste treatment system is required to reduce the amount of  $BOD_5$  from  $1000 \text{ mg/l}$  to  $20 \text{ mg/l}$  at the exit. The sedimentation unit concentrates biomass by a factor of 3. Kinetic parameters are  $\mu_m = 0.2 \text{ h}^{-1}$ ,  $K_s = 80 \text{ mg/l}$ ,  $k_d = 0.01 \text{ h}^{-1}$ , and  $Y_{X/S}^M = 0.5 \text{ g MLVSS/g BOD}_5$ . The flow of waste water is  $10000 \text{ l/h}$  and the size of the treatment basin is  $50,000 \text{ l}$ .
- a. What is the value of the solids residence time (i.e.,  $\theta_s$ )?
  - b. What value of the recycle ratio must be used?
- 16.8.** Consider a well-mixed waste treatment system for a small-scale system. The system is operated with a reactor of  $1000 \text{ l}$  and flow rate of  $100 \text{ l/h}$ . The separator concentrates biomass by a factor of 2. The recycle ratio is 0.7. The kinetic parameters are  $\mu_m = 0.5 \text{ h}^{-1}$ ,  $K_s = 0.2 \text{ g/l}$ ,  $Y_{X/S}^M = 0.5 \text{ g/g}$ , and  $k_d = 0.05 \text{ h}^{-1}$ . What is the exit substrate concentration?
- 16.9.** Redo Example 16.4 if the Contois equation for growth applies. In this case

$$\mu_{\text{net}} = \frac{\mu_m S}{K_{sx} X + S} - k_d$$

The values of  $\mu_m$  and  $k_d$  are the same as for Example 16.4, but  $K_s$  no longer applies. Assume  $K_{sx} = 0.02 \text{ g BOD}_5/\text{g MLVSS}$ .