

- a. Determine the optimal dilution rate maximizing the productivity of product formation (PD).
- b. Determine the optimal dilution rate maximizing the productivity of cell (biomass) formation (DS).

[Problem adapted from one suggested by L. Erickson.]

- 6.9. Ethanol is to be used as a substrate for single-cell protein production in a chemostat. The available equipment can achieve an oxygen transfer rate of 10 g O₂/l of liquid per hour. Assume the kinetics of cell growth on ethanol is of the Monod type, with $\mu_m = 0.5 \text{ h}^{-1}$, $K_s = 30 \text{ mg/l}$, $Y_{X/S} = 0.5 \text{ cells/g ethanol}$, and $Y_{O_2/S} = 2 \text{ g O}_2/\text{g EtOH}$. We wish to operate the chemostat with an ethanol concentration in the feed of 22 g/L. We also wish to maximize the biomass productivity and minimize the loss of unused ethanol in the effluent. Determine the required dilution rate and whether sufficient oxygen can be provided.
- 6.10. Plot the response of a culture to diauxic growth on glucose and lactose based on the following: $\mu_{\text{glucose}} = 1.0 \text{ h}^{-1}$; $\mu_{\text{lactose}} = 0.6 \text{ h}^{-1}$; $Y_{\text{glucose}} = Y_{\text{lactose}} = 0.5$; enzyme induction requires 30 min to complete. Plot cell mass, glucose, and lactose concentrations, assuming initial values of 2 g/l glucose, 3 g/l lactose, and 0.10 g/l cells.
- 6.11. The following data are obtained in oxidation of pesticides present in wastewater by a mixed culture of microorganisms in a continuously operating aeration tank.

| $D \text{ (h}^{-1}\text{)}$ | $S \text{ (Pesticides), mg/l}$ | $X \text{ (mg/l)}$ |
|-----------------------------|--------------------------------|--------------------|
| 0.05 | 15 | 162 |
| 0.11 | 25 | 210 |
| 0.24 | 50 | 250 |
| 0.39 | 100 | 235 |
| 0.52 | 140 | 220 |
| 0.7 | 180 | 205 |
| 0.82 | 240 | 170 |

Assuming the pesticide concentration in the feed wastewater stream as $S_0 = 500 \text{ mg/l}$, determine $Y_{X/S}^M$, k_d , μ_m , and K_s .

- 6.12. In a chemostat you know that if a culture obeys the Monod equation, the residual substrate is independent of the feed substrate concentration. You observe that in your chemostat an increase in S_0 causes an increase in the residual substrate concentration. Your friend suggests that you consider whether the Contois equation may describe the situation better. The Contois equation (eq. 6.36) is:

$$\mu = \frac{\mu_m S}{K_{sx} X + S}$$

- a. Derive an expression for S in terms of D , μ_m , K_{sx} , and X for a steady-state CFSTR (chemostat).
- b. Derive an equation for S as a function of S_0 , D , K_{sx} , $Y_{X/S}^M$, and μ_m .
- c. If S_0 increases twofold, by how much will S increase?
- 6.13. *Pseudomonas putida* with $\mu_m = 0.5 \text{ h}^{-1}$ is cultivated in a continuous culture under aerobic conditions where $D = 0.28 \text{ h}^{-1}$. The carbon and energy source in the feed is lactose with a