

Under diffusion limitations, the rate per unit volume is usually expressed in terms of the effectiveness factor as follows:

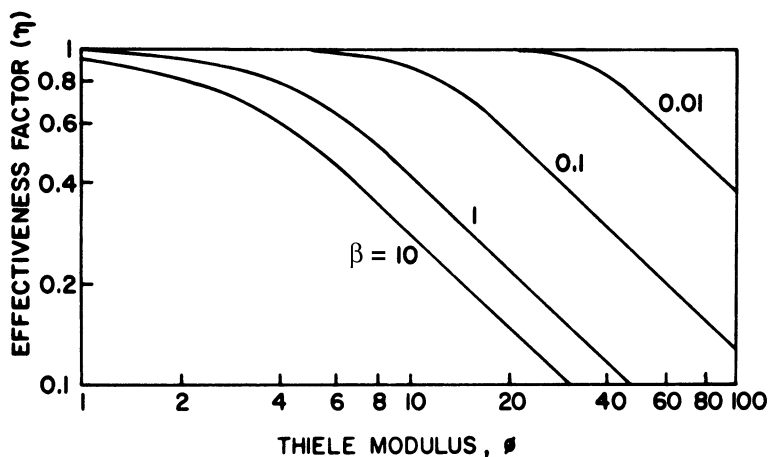
$$r_s = \eta \frac{V_m'' [S_s]}{K_m + [S_s]} \quad (3.59)$$

The *effectiveness factor* is defined as the ratio of the reaction rate with diffusion limitation (or diffusion rate) to the reaction rate with no diffusion limitation. The value of the effectiveness factor is a measure of the extent of diffusion limitation. For  $\eta < 1$ , the conversion is diffusion limited, whereas for  $\eta \approx 1$  values, conversion is limited by the reaction rate and diffusion limitations are negligible. The factor is a function of  $\phi$  and  $\beta$  as depicted in Figure 3.20.

For a zero-order reaction rate ( $\beta \rightarrow 0$ ),  $\eta \approx 1$  for a large range of Thiele modulus values such as  $1 < \phi < 100$ . For a first-order reaction rate ( $\beta \rightarrow \infty$ ),  $\eta = (\phi, \beta)$  and  $\eta$  is approximated to the following equation for high values of  $\phi$ .

$$\eta = \frac{3}{\phi} \left[ \frac{1}{\tanh \phi} - \frac{1}{\phi} \right] \quad (3.60)$$

When internal diffusion limits the enzymatic reaction rate, the rate-constant  $V_{m,app}$  and  $K_{m,app}$  values are not true intrinsic rate constants, but apparent values. To obtain true intrinsic rate constants in immobilized enzymes, diffusion resistances should be eliminated by using small particle sizes, a high degree of turbulence around the particles, and high substrate concentrations.



**Figure 3.20.** Theoretical relationship between the effectiveness factor  $\eta$  and first-order Thiele modulus,  $\phi$ , for a spherical porous immobilized particle for various values of  $\beta$ , where  $\beta$  is the dimensionless Michaelis constant. (With permission, from D. I. C. Wang et al., *Fermentation and Enzyme Technology*, John Wiley & Sons, Inc., New York, 1979, p. 329.)