



Liquid Lithium solid impurities cyclone separator  
First Light Fusion  
01/2024

Chemical assessment of particulate impurities  
S022641 / SIM0001 v.0

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First Light Fusion  
Liquid Lithium solid impurities cyclone separator

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## MEASUREMENT SYSTEM IDENTIFICATION

International System of Units (see ref. [1]).

## GLOSSARY OF TERMS

Term	Term definition
<b>Fusion</b>	Nuclear reaction that results in the union of two or more nuclei resulting in an excess of energy
<b>RTPR</b>	Reference Theta-Pinch Reactor tor2
$v$	Velocity [m/s]
$Q/VFR$	Volumetric flow rate [ $m^3/s$ ]
$\dot{m}/MFR$	Mass flow rate [kg/s]
$v_{.,f}$	Fluid velocity [m/s]
$v_{.,p}$	Particle velocity [m/s]
$v_{r,.}$	Radial velocity [m/s]
$v_{\theta,.}$	Tangential velocity [m/s]
$V$	Volume [ $m^3$ ]
$V_{cs}$	Cyclone effective volume [ $m^3$ ]
$c$	Specific concentration [ $mol/m^3$ ]
$d_p$	Particle diameter [m]
$t_{res}$	Residence time [s]
$\eta$	Separation efficiency
$d_{p,c}$	Cut particle diameter [m], diameter for which there is 50% separation

## **1 EXECUTIVE SUMMARY**

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## 2 INTRODUCTION AND BACKGROUND

First Light Fusion (FLF) inertial confinement fusion device is based on the nuclear reaction induced by the impact of a high-speed projectile onto a target mainly made of the fusion fuel (D-T). The use of Liquid Lithium (LL) in form of jet array in the Reactor Chamber (RC) plays a key role as tritium breeder, primary carrier of energy throughout the system, heat and nuclear shielding.

Taking into account that the primary carrier of energy is the LL, its circulation through the system is key to achieve the desired power cycle. This involves ensuring optimal circulation within the primary loop to maximize desired outcomes, such as purification of liquid metal from impurities introduced during operation and efficient management of tritium generated by neutron interactions for overall fuel cycle efficiency.

Considering the requirement to achieve an impurities control in the LL loop of the RC system, the current project studies the feasibility to separate the solid impurities from the liquid metal by means of centrifugal technologies. The first deliverable ref. [2] explored the different technologies that potentially could address the LL loop purification.

The objective of the present document is to study from chemical point of view the feasibility of separate the solids impurities from the liquid media (LL), by means of Classical Nucleation Theory (CNT) where fundamental parameters such as critical radius, and its evolution by means of nucleation in the media.

### 3 SCOPE

The present document is part of three deliverables: the first deliverable ref. [2] addressed the SoA of centrifugal technologies. The second deliverable (which is the current document) is focused in the chemical analysis of the impurities and the technology selection for the centrifuge device, being more specific:

- **Impurity and Corrosion Analysis:**

- Impurities matrix, given different source.
- Corrosion products identification.
- Maroni's process analysis.

- **Chemical analysis:**

- Particle Size Distribution (PSD) by means of CNT, for the given FLF impurities:
  - \* Fe
  - \* Cr
  - \* AlN
  - \* Li<sub>2</sub>O
  - \* LiQ
  - \* Li<sub>2</sub>C<sub>2</sub>
- Impurity critical radius time-evolution: Nucleation analysis.
- Homogeneous precipitation: advective-reacting diffusion equation.

- **Centrifugal technology selection:**

- Single step separation stage approach.
- Multi-step separation stage approach.
- Conceptual design approach.
- Thermo-hydraulic analytical model.

#### 3.1 Exceptions

N/A

#### 3.2 Exclusions

N/A

## 4 STRUCTURE OF THE DOCUMENT

The present document it is divided in three main blocks, as per the scope section 3 list. The blocks are divided by disciplines: impurities analysis SoA, chemical assessment, and engineering assessment including the thermo-hydraulic solid separator mathematical model.

Section 7 reviews the impurities and corrosion products in the FLF primary loop. The source of impurities are analyzed from chemical perspective in order to establish a baseline for future analysis. At the same time, a subsection is dedicated to review in the literature the corrosion products from the interaction of liquid lithium with the pipelines made SS316-Ti. The last subsection discusses the Maroni method for tritium extraction and addresses its advantages/disadvantages.

Section 8 is deeply dedicated to the chemical analysis of the impurities, specially focused on six impurities (established by FLF: Fe, Cr, AlN, Li<sub>2</sub>O, LiQ, Li<sub>2</sub>C<sub>2</sub>) studying the Particle Size Distribution and its temporal evolution to establish the critical radius of the impurities. A specific analysis has been carried to explain the solvers and convergence benchmarks for the Ordinary Differential Equations (ODE's) system develop to understand the different phenomena. Finally, for the non-metallic impurities, a dedicated analysis is the precipitation of those impurities by means of advective-reacting diffusion equation model.

Section 9 studies the single and multi-step solid separators with the aim to select the most appropriate centrifugal system for the FLF purification process for the primary loop. Mathematical model has been developed of a solid separator to study different parameter in order to set the possible efficiencies of the device per particle size. Finally, the section describes which device should be studied in the next stage of the current project, from a design and CFD point of view.

## 5 METHODOLOGY

The development of the present document follows a methodology (figure 5-1) based on three lines of work by discipline (SoA, Chemistry, ) that run by batches (presented in box form and sub-tasks). Besides the tasks runs in parallel, they are transversal to all disciplines in terms of technical results, as per the interaction of the outputs and intermediate results.

The figure 5-1 presents the diagram of the methodology and the expected outputs per batch & disciplines.

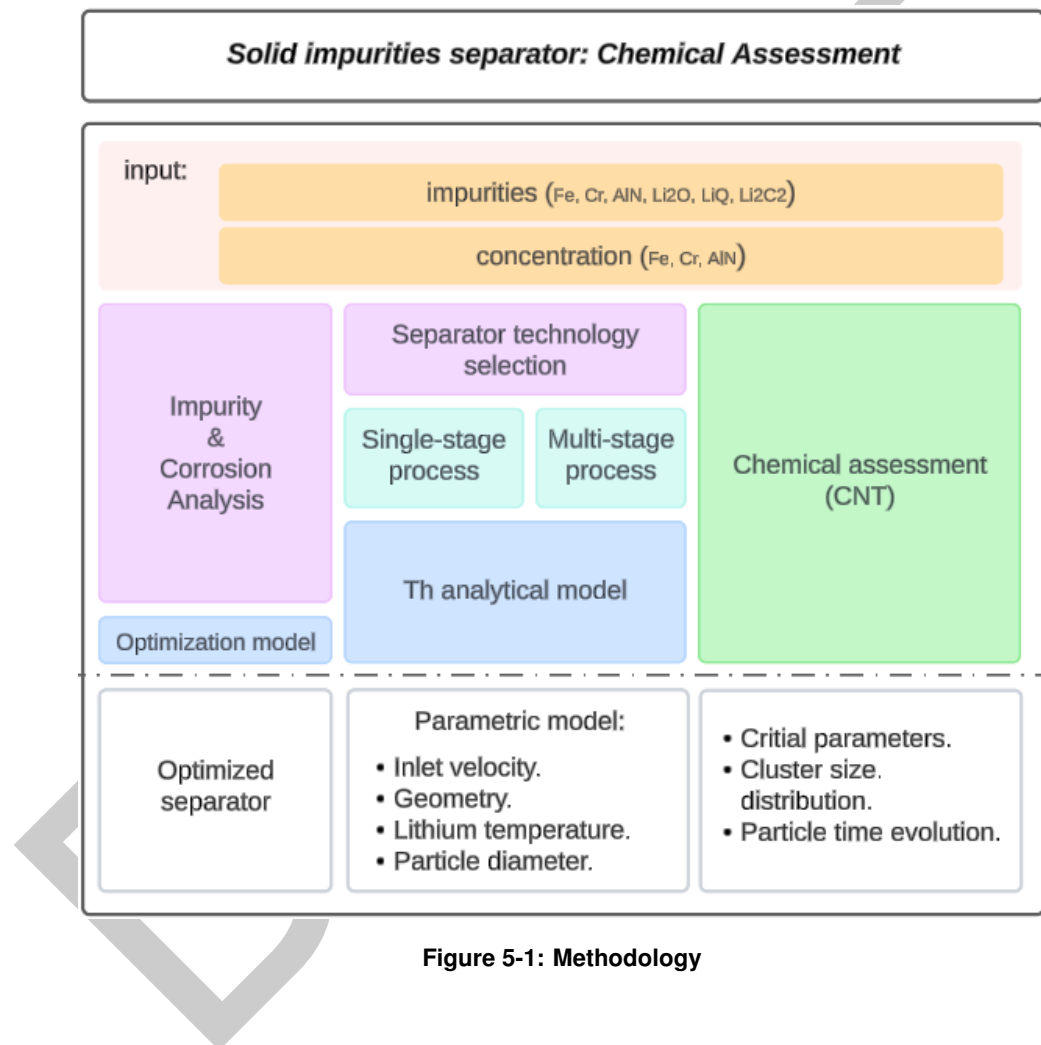


Figure 5-1: Methodology



## 6 INPUTS

To accurately analyze the impact of the impurities from chemical point of view, the following assumptions based on FLF inputs has been considered to target the impurities concentration, as follows:

### Inputs & Assumptions

The metallic impurities are calculated in the following manner:

- **135.000 kg/yr** of insoluble metal per year are generated as impurity.
- **8000 hr/yr** of Reactor Chamber (RC) operation.
- Assumed concentration:
  - 80% Fe
  - 10% Cr
  - 10% AlN
- **1/10 Hz** of Pulsed operation.
- **439.38 Tn** of LL in the loop.

Impurities mass produced in 1 pulse in the entire LL loop: **0.421 Kg**

Where the concentrations are:

- Fe = 0.00839 mol/ $m^3$
- Cr = 0.00112 mol/ $m^3$
- AlN = 0.00142 mol/ $m^3$

With an impurities ratio:

- Li = 0.999 e-00
- Fe = 1.201 e-07
- Cr = 1.613 e-08
- AlN = 2.046 e-08

## 7 IMPURITY AND CORROSION ANALYSIS

### 7.1 Impurities Matrix

Within the scope of the current document, the identification of the impurities source and its main properties is key to provide the necessary context for the coming sections. Given the FLF machines and components, such as: machine gun (upper launcher), Reactor Chamber (RC), and the liquid lithium primary loop, the identified impurity sources are:

- **Lithium initial impurities.**
- **Corrosion:** mainly given by the primary loop (piping and components) made of SS316-Ti, it is assumed at some point the RC vessel made of P91 will be a secondary source of corrosion impurities. The section 7.2 is dedicated to identify the corrosion products, mechanisms, and its source.
- **Pulsed shot (projectile + target):** considering the input metallic impurities given by FLF (Fe, Cr, AlN), it is assumed in the current document that part of these impurities will be generated at the pulsed operation due to the projectile impact with the target, example of this is the presence of Cr. Future studies will be necessary to identify and classify the impurities result of the pulsed operation.

#### 7.1.1 Lithium initial impurities

The initial lithium impurities is a key source in terms of traceability, even more considering that these impurities can mutate within the system under neutronic irradiation. The Figure 7-1 shows the list of impurities, ranked in the horizontal axis by concentration and vertically the density of element.

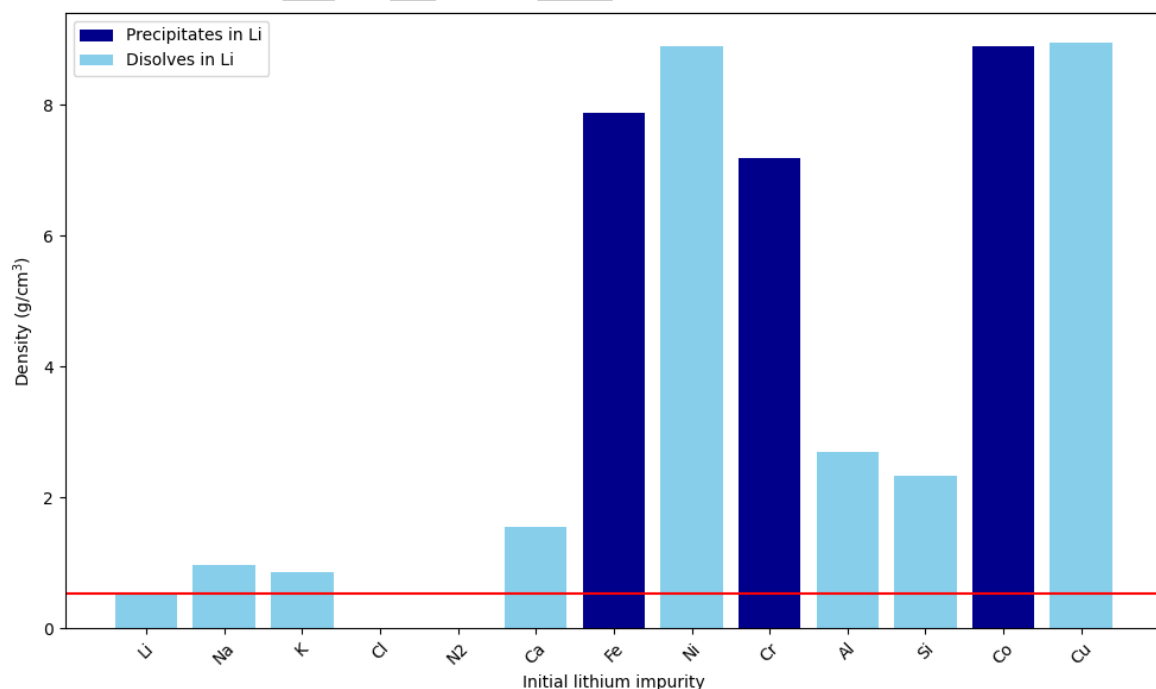


Figure 7-1: Initial lithium impurities.

xxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxxx explanation here about the results in the graph,

Element	Content	Density
Li	99.98 %	0.534 g/cm <sup>3</sup>
Na	0.0034 %	0.971 g/cm <sup>3</sup>
K	0.0032 %	0.862 g/cm <sup>3</sup>
Cl	0.0031 %	0.003214 g/cm <sup>3</sup>
N <sub>2</sub>	0.0020 %	0.001250 g/cm <sup>3</sup>
Ca	< 0.001 %	1.550 g/cm <sup>3</sup>
Fe	< 0.001 %	7.874 g/cm <sup>3</sup>
Ni	< 0.001 %	8.900 g/cm <sup>3</sup>
Cr	< 0.001 %	7.190 g/cm <sup>3</sup>
Al	< 0.001 %	2.702 g/cm <sup>3</sup>
Si	< 0.001 %	2.330 g/cm <sup>3</sup>
Co	< 0.001 %	8.900 g/cm <sup>3</sup>
Cu	< 0.001 %	8.960 g/cm <sup>3</sup>

**Table 7-1: Lithium initial impurities concentration ref. [3].**

## 7.2 Corrosion Products

The deliverable [2], listed the lithium impurities and how they are related with the corrosion products together with the effects in steel pipework (SS316). The current section, aims to provide more information gathered from the literature, producing the following table:

Li impurities	Effect on Materials	Corrosion Product	Conditions/Notes	References
Nitrogen	General dissolution and intergranular penetration in stainless steel.	Primary attack via chromium forming $\text{Li}_9\text{CrN}_5$ and iron forming $\text{Li}_3\text{FeN}_2$ .	High nitrogen levels lead to corrosion at temperatures between 400-600 °C.	[4], [5], [6], [7]
Oxygen	Formation and dissolution of unstable ternary oxides.	$\text{Li}_5\text{FeO}_4$ , $\text{LiCrO}_2$ , $\text{Li}_2\text{Ni}_8\text{O}_{17}$ formed between $\text{Li}_2\text{O}$ and steels.	Limited information, reactions involve $\text{Li}_2\text{O}$ interacting with Fe, Cr	[8], [9], [10]
Carbon	Formation of $\text{Cr}_{23}\text{C}_6$ precipitates on stainless steel surfaces.	$\text{Cr}_{23}\text{C}_6$ precipitates enhance chromium concentration at the surface.	Higher weight loss in type 316 stainless steel compared to 9Cr1Mo ferritic steel.	[11]
Hydrogen	Significant decarburisation of stainless steel. Formation of new phase $\text{Fe}_{50}\text{Cr}_{43}\text{Mo}_3\text{Ni}_4$ on steel surface exposed at 700 °C showing intergranular corrosion.	Decrease in carbon content more pronounced in austenitic steel.	Affects both austenitic and ferritic/martensitic steels.	[11] [12]
Aluminium	Not known to cause corrosion in stainless steel directly.	Addition of Al reduces weight loss in stainless steel; may form $\text{AlN}$ in presence of dissolved nitrogen.	Adding 5wt% Al to lithium reduced weight loss of type 316 stainless steel.	[13], [4]
No impurities added.	The austenitic area in the welded joint showed morphological changes induced by the dissolution of Ni in Li. The ferritic parts exhibit a fine-grained surface structure.	$\text{M}_{23}\text{C}_6$ and $\text{NiC}_x$ particles in sizes of 1-2 $\mu\text{m}$ .	Study of welded joints (SS316 and SS410) in liquid lithium.	[12], [14]

**Table 7-2: Corrosion Effects of Impurities in Liquid Lithium on Materials.**

### 7.3 Maroni's Process

The Maroni process has been studied in the SoA deliverable ref. [2], where the process diagram Figure 7-2 of a molten-salt extraction and its stages were analyzed. Nevertheless, the current section is focused in study the advantages/disadvantages of Maroni process, presented in Table 7-3.

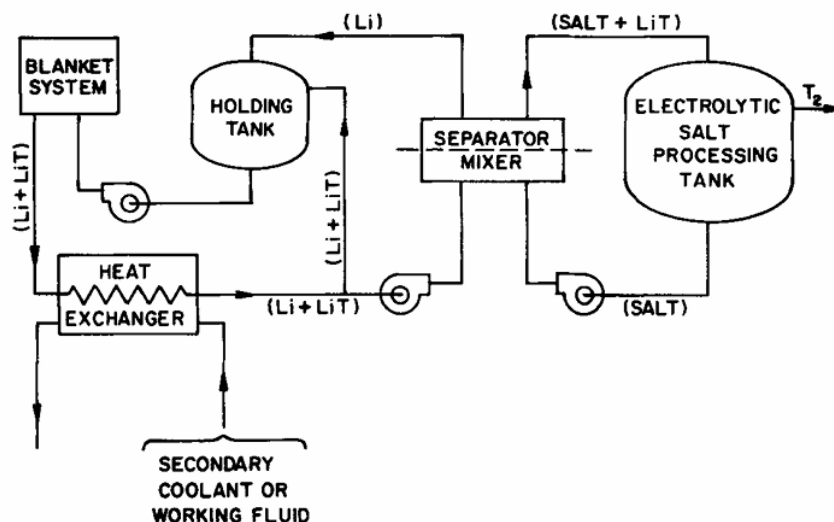


Figure 7-2: Schematic diagram of a molten-salt extraction diagram [15].

Before jumping in the Table 7-3, it is important to remind the Maroni process: based on high temperature molten mixed alkali-metals halide salts (LiCl-KCl at 530 °C) as an extraction solvent for the Li + LiT.

Advantages	Disadvantages
<p><b>Continuous tritium extraction:</b> The capability to maintain a steady-state tritium inventory within the lithium loop has been incorporated as a critical consideration in the design of the RTPR. This aspect of the design underscores the importance of ensuring a consistent tritium flow and concentration within the system, which is fundamental to the reactor's operational efficiency and safety.</p>	<p><b>Solubility:</b> At the operational temperatures of mixing/separating the lithium and salts, the saturation solubility will be reached in the other. The main concern is the presence of salt dissolved in lithium, being significant in terms of corrosion and the products formed under neutronic irradiation (with regard of long-lived radioactive-isotope from the presence of KCl in the lithium jets).</p>

Advantages	Disadvantages
<p><b>Tritium-salts affinity:</b> The distribution coefficients for 500-600 °C are 2.6 for volumetric distribution and 5.8 for molar distribution, being the ratio of tritium content in the salt (<math>T_{salt}</math>) to tritium content in lithium (<math>T_{Li}</math>) demonstrating that distributions of LiT between the salt and metal phases can be achieved. This advantage of tritium-salts affinity, might allow tritium recovery in the HEX system.</p>	<p><b>Required potential (V):</b> The extraction of tritium from the salt medium is proposed to be conducted via electrolysis at a potential of 1.5V. However, this process is constrained by the limitation that salt decomposition occurs at potentials exceeding 2.0V. Consequently, to maintain the integrity of the salt medium while ensuring a steady-state tritium inventory, the efficiency of the tritium recovery process must be optimized for operation at the designated 1.5V potential.</p>
<p><b>Density:</b> Lithium density is less dense than the molten salt by a factor of 3, thus leading to exploit separation system from gravitational settling to centrifugal action. The later separation system could be exploited with hydrocyclones due to its efficiency and low energy cost.</p>	<p><b>Corrosion:</b> The interaction of materials with lithium, particularly in contexts requiring controlled corrosion rates, remains a significant area of ongoing research. This challenge is further intense in scenarios involving lithium-salt mixtures within mixing/separator devices. To mitigate these issues, the employment of specialized alloys, such as Niobium, was studied in the literature. However, the selection of appropriate materials for lithium loops presents complex considerations, notably due to the specific corrosion behaviors and operational temperature demands associated with fusion nuclear environments.</p>
	<p><b>Volatile elements:</b> The use of electrolytic process to extract the tritium from salts could involve potential volatile elements such as hydrogen chloride, hydrogen fluoride, hydrogen bromide or its tritium analogs have a direct impact in the feasibility of the tritium extraction in form of gas. Recent studies mitigate the volatile using benign lithium hydroxide (LiOH) or lithium carbonate (<math>Li_2CO_3</math>).</p>

**Table 7-3: Maroni process: advantages/disadvantages [15], [16].**

## 8 CHEMICAL ANALYSIS

This section investigates the nucleation of impurities within liquid lithium, which serves as a breeder and shielding material in the reaction chamber. The nucleation of impurities within liquid lithium poses a complex challenge, impacting not only the material's thermal and physical properties but also the safety and longevity of the fusion reactors. Despite its significance, the study of impurity nucleation in liquid lithium remains underexplored, with limited literature providing a comprehensive understanding of these mechanisms.

Due to the objective of using purification processes based on centrifugation phenomena, the limiting factor of these impurities will be their densities, the quantities in which they are present and above all the particle size of these impurities. Therefore, as a starting point for the characterisation of these impurities from a thermodynamic and kinetic point of view, classical nucleation theory (CNT) and kinetic theory have been used to study the evolution and speed of this phenomenon.

The primary issue with this model stems from its oversimplifications, which will be detailed in subsequent sections. A significant limitation is that these models originate from statistical mechanics, constraining them to a limited number of particles. Specifically, when examining clusters of macroscopic particles on the scale of micrometers, employing statistical mechanics or molecular dynamics models proves impractical. Consequently, for such scales, the application of continuous models becomes more appropriate, examples of which include phase field models [17, 18], computational fluid dynamics or precipitation dynamics [19].

Furthermore, this research can serve as a foundational basis for applying continuous models more effectively. For instance, one could enhance these models by incorporating the distributions of nanometric particles within the system as input parameters.

This section is structured for clarity and comprehension, starting with an explanation of classical nucleation theory and the thermodynamics of the nucleation process. This is followed by an analysis of the kinetic treatment of the process. The section concludes with the characterization of each impurity.

### 8.1 Nucleation Theory

First-order phase transitions, such as the condensation of vapor, boiling of a liquid, and crystallization of a melt, are critical phenomena in materials science and thermodynamics. The decay of metastable states, such as the solidification of a supercooled liquid, takes place through the nucleation and growth of some small-sized clusters within the system [20]. The initial stage of the phase transformation is usually described within the time-honored CNT [21, 22], where the droplet is described as a sphere of, say, bulk solid, separated from the liquid by a sharp interface, giving rise to a free-energy penalty proportional to the interface area and a total Gibbs-free-energy activation barrier.

$$\Delta G(i) = -|\Delta\mu|i + A\gamma_{\infty}i^{2/3}, \quad (1)$$

where  $i$  is the number of particles in the cluster,  $\Delta\mu < 0$  is the chemical potential difference between

the two phases,  $A = (36\pi\nu^2)^{1/3}$  being  $\nu$  the molecular volume and  $\gamma_\infty$  the specific surface energy (surface tension) of the planar interface, all anisotropies being neglected at this stage. The droplet grows if it exceeds a critical size  $i^*$  corresponding to the maximum  $\Delta G(i) (\equiv \Delta G^*)$ . The CNT relies on the liquid droplet model, which assumes that tiny droplets possess the same characteristics as the bulk condensed phases and have surface energies identical to those of an infinite flat surface. Nonetheless, there is an ongoing debate about the applicability of macroscopic thermodynamic principles to describe liquid drops when dealing with small clusters composed of merely a few dozen molecules [23]. The inadequacy of the droplet model for small particles is highlighted by the fact that the energy required to form monomers is not zero [24]. This indicates that the attributes of small clusters cannot be simply categorized into bulk and surface properties, rendering the notion of surface tension somewhat misleading when applied to these clusters [25]. For instance, the 'monomers' of the new phase are indistinguishable from the molecules of the parent phase, leading to the conclusion that the free energy of monomers should logically be zero ( $\Delta G(1) = 0$ ) [26].

However, in the conceptual state of this work, this simple model is useful to provide quantitatively and qualitatively the critical size of these nuclei.

CNT also is able to estimate the nucleation rate

$$I = I_0 e^{-\beta \Delta G^*}, \quad (2)$$

where  $\beta = 1/(k_B T)$  is the inverse temperature and  $I_0$  a kinetic prefactor that varies slowly with  $T$ . Clearly, this connection between  $I$  and  $\gamma_\infty$  relies on several severe approximations. Moreover,  $I_0$  is notoriously influenced by genuinely non-equilibrium effects and various expressions resulting from a more detailed consideration of the nucleation kinetics are known since a long time [22].

In the nucleation regime, the evolution of the system is significantly marked by the formation of clusters that represent a new equilibrium phase. The dynamics of this process are intricately governed by the balance between volume and surface contributions, as encapsulated by the capillary approximation. The volume contribution, acting as the driving force behind nucleation, lowers the system's free energy and is directly proportional to the cluster's volume, thereby favoring the formation and growth of these clusters. Conversely, the surface contribution introduces an energetic cost, scaling with the cluster's surface area. This cost is associated with creating an interface between the original phase and the new cluster, serving as a barrier that inherently inhibits the growth of the cluster [27].

The critical size of the nucleus and the nucleation barrier are determined by setting the derivative of  $\Delta G$  with respect to the size,  $i$ , equal to zero:

$$R^* = -2\gamma_\infty(\Delta\mu/\nu)^{-1}, \quad (3)$$

and

$$\Delta G^* = \frac{16\pi}{3}\gamma_\infty^3(\Delta\mu/\nu)^{-2}. \quad (4)$$



Analyzing the critical parameters obtained from the CNT, is it evident that the key variables of the model are the nucleation driving force and the surface energy. In the following sections, some formalisms for the driving force will be presented and discussed, as well as for the surface energy.

### 8.1.1 Driving force

The nucleation driving force is obtained by considering the difference in chemical potentials between the parent and the equilibrium phases for all atoms composing the cluster:

$$\Delta\mu = \sum_i y_i^e (\mu_i^e - \mu_i^0), \quad (5)$$

where  $y_i^e$  is the atomic fraction of type  $i$  atoms in the nucleating equilibrium phase, and  $\mu_i^e$  and  $\mu_i^0$  are the corresponding chemical potentials in the nucleating equilibrium phase and in the parent phase, respectively. In a metastable parent phase, chemical potentials are higher than those at equilibrium. The critical factors for applying CNT are the driving force,  $\Delta\mu$ , and the surface energy,  $\gamma_\infty$ , of the solid particle. The driving force depends on the nucleation pathway, such as the saturation-based formalism commonly used in the context of vapor to liquid or crystal transitions [28, 29, 30]:

$$\Delta\mu = \mu - \mu_{\text{coex}} = kT \ln \left( \frac{n_1}{n_1^{\text{sat}}} \right), \quad (6)$$

where the chemical potential is represented using the ideal gas expression, introducing a monomer density  $n_1^{\text{sat}}(T)$  appropriate to a saturated vapor, i.e., a gas phase in coexistence with the condensed phase at the environmental temperature. The ratio of the monomer density in a metastable vapor to its value in a saturated vapor defines the supersaturation,  $S$ :

$$\Delta\mu = kT \ln S. \quad (7)$$

This driving force dictates the nucleation process, which is governed by temperature, the degree of supersaturation, and the interfacial energy. The nucleation rate increases with the degree of supersaturation and temperature and decreases with the interfacial energy. This behavior is illustrated in Figure 8-1, which shows the energy barrier that must be overcome to form a new phase for various degrees of supersaturation.

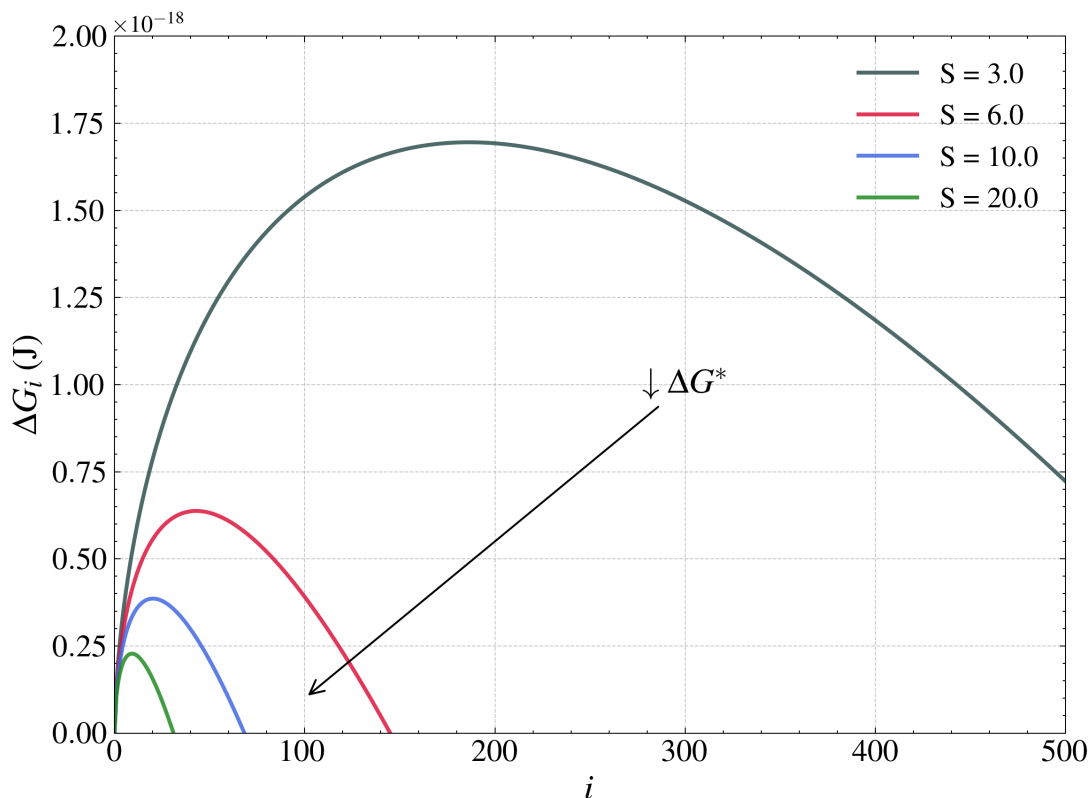


Figure 8-1: Required free energy, as per classical nucleation theory, for the formation of a cluster of size  $i$ . Curves represent different constant values of supersaturation and temperature, illustrating the free energy barrier associated with the critical size.

This formalism is pertinent for analyzing solutes dissolved in liquids that nucleate in either liquid or crystalline states. However, CNT is not always successful, primarily because the capillarity approximation, upon which it is based, is a very primitive characterization of small molecular clusters. Nevertheless, the expressions derived provide intuitive value, suggesting that increasing the vapor supersaturation,  $S$ , accelerates the nucleation of droplets, all other parameters being constant. Additionally, the nucleation rate is influenced by the surface tension of the condensed phase: higher surface tension,  $\gamma_\infty$ , results in a slower rate. The rate is also quite sensitive to supersaturation, surface tension, and temperature, as these quantities appear inside an exponential function [31].

To surpass the predictive capability of classical theory, it is necessary to compute the partition functions of clusters of various sizes and develop a more realistic model of the excess free energy; however, this is beyond the scope of this work.

Another formalism that may be useful for this study involves the definition of the driving force commonly used in the phase transition between melts and crystalline phases. Consider a single-component liquid initially at equilibrium, quenched to a temperature  $T$ , below its melting temperature  $T_m$ . Since the liquid and solid phases have the same composition, the nucleation free energy corresponds to the free energy difference between the liquid and solid states at temperature  $T$ , in other words, the driving force is a function that depends on the undercooling rate [27, 32]:

$$\Delta\mu = \frac{\Delta H_m}{T_m}(T_m - T) + \int_T^{T_m} \Delta C_p dT' - T \int_T^{T_m} \frac{\Delta C_p}{T'} dT', \quad (8)$$

where  $\Delta H_m$  and  $T_m$  are the molar heat of melting and the melting temperature of the crystal, respectively, and  $\Delta C_p = C_p^l - C_p^c$  is the difference between the molar heat capacities of liquid and crystal at constant pressure. The experimental values of  $\Delta G_V$  are normally bounded by the approximations usually assigned to Turnbull and Hoffman that assume  $\Delta C_p = 0$  and  $\Delta C_p = \text{constant}$ , respectively:

$$\Delta\mu(T) = \frac{\Delta H_m}{N_A} \left(1 - \frac{T}{T_m}\right), \quad (9)$$

$$\Delta\mu(T) = \frac{\Delta H_m}{N_A} \left(1 - \frac{T}{T_m}\right) \frac{T}{T_m}, \quad (10)$$

Here,  $\Delta H_m$  is the melting enthalpy per mole of the crystal and  $N_A$  is Avogadro's number. When the undercooling is large, the expression may not be precise enough. One can then consider the next term in the Taylor expansion leading to the Turnbull and Hoffman equations respectively [27]:

$$\Delta\mu(T) = \frac{\Delta H_m}{N_A} \left(1 - \frac{T}{T_m}\right) - \Delta C_p \left(\frac{(T - T_m)^2}{2T_m}\right), \quad (11)$$

$$\Delta\mu(T) = \frac{\Delta H_m}{N_A} \left(1 - \frac{T}{T_m}\right) \frac{T}{T_m} - \Delta C_p \left(\frac{(T - T_m)^2}{2T_m}\right). \quad (12)$$

This formalism is widely used in the study of the nucleation of impurities in metallic melts, with a wide range of materials, such as metallic glasses like  $\text{Li}_2\text{O}_2\text{SiO}_2$  and  $\text{LS}_2$ , or other metallic alloys like  $\text{Ge}_2\text{Sb}_2\text{Te}_5$  and (Ag,In)-doped  $\text{Sb}_2\text{Te}$  (AIST) [26, 33, 34, 35, 36, 30].

Using these models to describe the driving force, they exhibit certain limitations. Firstly, within the formalism derived from the degree of saturation, an ideal mixture is assumed. This is evident since concentrations or mole fractions are used to determine the degree of supersaturation rather than activities. To rigorously work through activities, the driving force can be determined if the interaction parameters between the components of the solution are known [37], or determine the mixing parameters starting from the partition function derived from the grand canonical potential, employing the **quasi-chemical approximation** formulation [38] or exponential models [39].

In the second formulation, which utilizes the undercooling rate to determine the driving force, the approach is widely recognized and accepted. However, this formula encounters limitations when applied to mixtures exhibiting degrees of immiscibility. Specifically, the challenge arises in scenarios where two phases coexist, such as in solid-liquid equilibrium. In these instances, given a particular composition for which a certain temperature allows both phases to be in equilibrium; this temperature is referred to as the liquidus temperature  $T_l$ .

The standard application of this formulation presents issues as it traditionally employs the absolute melting point to determine the driving force, neglecting the presence of different phases that may manifest within the system.

A potential rectification for this oversight involves the utilization of the  $T_l$  instead of  $T_m$ . However, this correction is not without its challenges. Specifically, when the fraction of one of the phases is exceedingly low, accurately determining the liquidus temperature within the phase diagram becomes problematic. This difficulty is compounded by the typical unavailability of high-resolution phase diagrams.

Ideally, the driving force in phase transition studies is determined by a comprehensive thermodynamic model that includes information about the elements present in the system, as demonstrated in previous works [40, 41]. However, due to the limitations previously stated, an alternative formulation for the driving force has been developed to provide a more accurate description of the volumetric free energy. This method involves calculating the Gibbs free energy change,  $\Delta G$ , defined by the free energy expressions for the liquid ( $l$ ) and solid ( $s$ ) phases.

The chemical potential for component A in the liquid phase,  $\mu_A^l$ , is determined by constructing a tangent to the liquid free energy curve at the composition  $x_l$ . The point where this tangent line intersects the  $x_A = 1$  axis defines  $\mu_A^l$ . Similarly, the chemical potential for component A in the solid phase,  $\mu_A^s$ , is identified at the intersection of the tangent line with the  $x_A = 0$  axis.

At the liquidus temperature  $T_l$ , the free energy curves for both the liquid and solid phases are tangent to the line constructed from the previous step. The solid composition that is in equilibrium with the liquid composition  $x_l$  at  $T_l$  is given by the tangent point on the Gibbs free energy curve. This equilibrium composition is denoted as  $x_{s,eq}$  and can be identified on the equilibrium phase diagram.

At a temperature  $T$ , arbitrarily lower than  $T_l$ , the chemical potentials in the solid,  $\mu_A^s$  and  $\mu_B^s$ , and for the liquid,  $\mu_A^l$  and  $\mu_B^l$ , are determined as before for the liquid phase. The differences in chemical potential, which drive the phase transition, are defined as follows:

$$\Delta\mu_A = \mu_A^l - \mu_A^s \quad (13)$$

$$\Delta\mu_B = \mu_B^l - \mu_B^s. \quad (14)$$

The free energy change, per unit volume, associated with forming a small amount of solid of composition  $x_s^*$  out of the liquid is given by

$$\Delta G_v = [x_s^* \Delta\mu_A + (1 - x_s^*) \Delta\mu_B] / V \quad (15)$$

where  $V$  is the average molar volume of the solid, assumed here to vary linearly between the molar volumes  $V^A$  and  $V^B$  of the pure solid systems:

$$V = x_s^A V^A + (1 - x_s^A) V^B. \quad (16)$$

The solid composition that is most likely to nucleate,  $x_n$ , is assumed to be the one with the largest difference in free energy,  $\Delta G_v$ , between the liquid and solid state. This intuitively obvious assumption is used because of its simplicity. Further justification based on a more rigorous calculation is given in Appendix I. It can be seen from that  $\Delta G_n$  is maximized if  $\Delta\mu^A = \Delta\mu^B$ , so that the composition  $x_n$

corresponds to the point of tangency on the solid curve of a line parallel to the tangent to the liquid curve at  $x_l$ , so that

$$\Delta \bar{G}_v \approx \Delta \mu^A \approx \Delta \mu^B. \quad (17)$$

Therefore, given the composition dependence of the liquid and solid free energies, one can calculate the solid nucleus composition and the free energy of formation for the nucleus as a function of initial liquid composition,  $x_l$ , and undercooling  $\Delta T = T_l - T$ .

For an actual calculation of  $\Delta G_p$ , it is necessary to use solution models. Therefore, regular solution behavior is assumed for the liquid phase so that

$$\mu_l^A = \mu_l^{A,0} + RT \ln(x_l^A) + \alpha_l(x_l^A), \quad (18)$$

$$\mu_l^B = \mu_l^{B,0} + RT \ln(x_l^B) + \alpha_l(x_l^B). \quad (19)$$

The solid phase is assumed to be a dilute or ideal solution so that  $\alpha_s^A$  and  $\alpha_s^B$  are independent of composition:

$$\mu_s^A = \mu_s^{A,0} + RT \ln(x_s^A) + \alpha_s^A, \quad (20)$$

$$\mu_s^B = \mu_s^{B,0} + RT \ln(x_s^B) + \alpha_s^B. \quad (21)$$

Combining equations (18) and (20) gives

$$\Delta \mu^A = (\mu_l^A - \mu_s^A) + RT \ln \left( \frac{x_l^A}{x_s^A} \right) + \alpha_l(x_l^A) - \alpha_s^A. \quad (22)$$

For pure metals, it can be assumed that the difference between the heat capacities of the solid and liquid,  $\Delta C_p$ , is small, so that

$$\mu_l^{A,0} - \mu_s^{A,0} \approx \Delta S_f(T_m^A - T), \quad (23)$$

where  $\Delta S_f$  and  $T_m^A$  are, respectively, the entropy of fusion and the melting temperature of pure A. Therefore, combining equations (22) and (23) gives

$$\Delta \mu^A = T \left[ R \ln \left( \frac{x_l^A}{x_s^A} \right) - \Delta S_f \right] + \alpha'_l(x_l^A), \quad (24)$$

where

$$\alpha'_l(x_l^A) = \alpha_l(x_l^A) - \alpha_s^A + \Delta H_f. \quad (25)$$

Similarly, for component B

$$\Delta \mu^B = T \left[ R \ln \left( \frac{x_l^B}{x_s^B} \right) - \Delta S_f \right] + \alpha'_l(x_l^B). \quad (26)$$

Now recall that at  $T = T_l$ ,  $\Delta\mu^A = 0$  so that

$$\alpha'(x_l^A) = -T_l \left[ R \ln \left( \frac{x_l^A}{x_{s,eq}^A} \right) - \Delta S_f^A \right]. \quad (27)$$

For a given  $x_l^A$ ,  $T_l$ , and  $x_{s,eq}^A$  can be found from the equilibrium phase diagram. Combining equations (24) and (27) and rearranging terms gives

$$\Delta\mu^A = (T_l - T)\Delta S_f^A + RT \ln \left( \frac{x_l^A}{x_s^A} \right) - RT_l \ln \left( \frac{x_l^A}{x_{s,eq}^A} \right). \quad (28)$$

Similarly, for component B

$$\Delta\mu^B = (T_l - T)\Delta S_f^B + RT \ln \left( \frac{x_l^B}{x_s^B} \right) - RT_l \ln \left( \frac{x_l^B}{x_{s,eq}^B} \right). \quad (29)$$

Finally, as discussed previously, at  $T < T_l$ , the free energy change on nucleation is

$$V\Delta G_v = \Delta\mu^A = \Delta\mu^B. \quad (30)$$

Also, since  $\Delta\mu^A = \Delta\mu^B$ , from equations (28) and (29)

$$(T_l - T)(\Delta S_f^A - \Delta S_f^B) + RT \ln \left( \frac{x_l^A(1 - x_s^A)}{x_{s,eq}^A(1 - x_l^A)} \right) = RT \ln \left( \frac{x_l^A(1 - x_{s,eq}^A)}{x_{s,eq}^A(1 - x_l^A)} \right). \quad (31)$$

Therefore, given  $x_l$ ,  $\Delta S_f^A$ ,  $\Delta S_f^B$ , and the equilibrium phase diagram, one can find  $\Delta G$ , and  $x_n$  at an arbitrary temperature  $T$  from equations (28)–(31). In the limiting case that the solubility of B in crystalline A is zero, the derivation simplifies considerably. Equation (18) still holds but equation (20) becomes  $\mu_s^A = \mu_{s,0}^A$ . Therefore, as before

$$\Delta\mu^A = T(R \ln x_l^A - \Delta S_f^A) + \alpha'(x_l^A) \quad (32)$$

and since  $\Delta\mu^A = 0$ , at  $T_l$ ,

$$\alpha'(x_l^A) = -T_l(R \ln x_l^A - \Delta S_f^A) \quad (33)$$

so that

$$V\Delta G_v = \Delta\mu^A = (T_l - T)(\Delta S_f^A - R \ln x_l^A). \quad (34)$$

An analogous equation holds for crystallization of pure B. This simplified result is particularly useful for metal-metalloid glass forming alloys such as Au–Si where the equilibrium solid solubility of the metalloid in the crystalline metal is very low.

### 8.1.2 Surface energy

As discussed in the previous section, surface energy is one of the critical parameters in CNT. Firstly, because this theory fails to predict the behaviour of small clusters and at the same time assumes a surface

energy value for a flat surface. In addition, the dependence of the surface energy on the nucleation rate is probably the most important part of this formalism.

Because this parameter is an exponential in the calculation of the nucleation rate, it depends very strongly on the value of the surface tension. For example, a change in  $\gamma_\infty$  of only one order of magnitude leads to a change in the nucleation rate of about eight orders of magnitude [42].

Nonetheless, a dependable method for measuring surface tension is absent, with the exception of aligning experimental nucleation rate data with theoretical models [43]. Furthermore, a critical hypothesis of the CNT, referred to as the capillarity approximation, overlooks the influence of curvature and size on surface tension [44]. Therefore, ideally it has to be obtained from experiments or from ab-initio calculations [45, 46, 47, 48, 49]. Another well-accepted methodology is from the complete thermodynamic model of the mixture, using Buttler's formulation [50, 51, 52], the problem with this methodology arises in having all the information and having a detailed phase diagram.

Given the difficulties noted above in measuring or simulating the surface free energy of the liquid-solid interface, the natural question is whether theoretical methods can predict its magnitude and the physical processes that affect it. theoretical methods can predict its magnitude and the physical processes that affect it.

In order to determine *gamma*, it is useful to discuss the energetic and entropic components that make it up, since, as we shall see, the different models that have been developed differ markedly in the relative contributions they attribute to these two components. The surface Gibbs free energy can be written as

$$\gamma = E^{(s)} - TS^{(s)} + PV^{(s)} \quad (35)$$

In this context,  $E^{(s)}$  represents the energy excess at the surface,  $S^{(s)}$  denotes the entropy at the surface, and  $V^{(s)}$  is the additional volume. The latter term remains negligible unless under conditions of high pressure, and can be completely negated by appropriately selecting the Gibbs dividing surface such that  $V^{(s)}$  becomes zero. This results in only energetic and entropic elements contributing to  $\gamma$ .

An early and widely adopted model for assessing the free energy at the liquid-solid interface was introduced by [53]. This model presupposes complete wetting of the crystal by the liquid, leading to a contact angle  $\theta$  of zero in the equilibrium involving three phases: crystal, liquid, and vapor. Following from Eq. 35, with  $\theta$  set to zero and consequently  $\cos \theta$  equal to one, the derived expression is

$$\gamma_{sl} = \gamma_{sv} - \gamma_{lv} \quad (36)$$

Assuming the general case holds, the analysis simplifies to evaluating  $\gamma_{sv}$  and  $\gamma_{lv}$  independently. This method involves deducing the energy difference due to bond disruption between the solid-vapor and liquid-vapor phases, incorporating the solid's fusion enthalpy and melting-induced volume change, alongside a modest entropic variation from the external layers of both phases. Consequently, the derived formula is

$$\gamma_{sl} = \frac{\Delta H}{4fN_A v^{2/3}} + \frac{2\Delta V}{3V_s} \gamma_{lv} + \frac{T_m(\Delta S_l - \Delta S_s)}{fN_A v^{2/3}} \quad (37)$$

where  $f$  is a factor that relates the area  $A$  of a mole of surface atoms to the volume of a mole of atoms in the bulk solid through

$$A = fN_A v^{2/3} \quad (38)$$

Numerically, the factor stands at 1.12 for the bcc (110) surface and 1.09 for the fcc (111) surface. Given the minimal entropic contribution in Eq. 36, this framework primarily emphasizes energy aspects. Predominantly, the initial term, hinting at a direct relationship between  $\gamma_{sl}$  and  $\Delta H/v^{2/3}$ , aligns with empirical findings from initial nucleation studies, underpinning classical homogeneous nucleation theory.

In [54] introduced an energy-centric model for surface free energy, emphasizing electron-ion interactions and significant volume changes upon melting. Conversely, Turnbull proposed an entropy-focused model, envisioning the solid as a plane intersecting the liquid, effectively halving the surface density compared to the bulk liquid. This model assumes negligible energy alteration when replacing absent atoms, albeit with reduced configurational entropy due to their fixed positions, tying this adjustment directly to the fusion entropy.

$$\gamma_{sl} = \frac{T_m \Delta S}{2fN_A v^{2/3}} - \frac{\Delta H}{2fN_A v^{2/3}} \quad (39)$$

Recent approaches have applied physical or computational simulations, notably using hard sphere packings, to gauge surface free energy, as detailed by [55]. In these models, spheres form a densely packed crystalline structure, excluding octahedral voids to mirror the dense liquid's random packing. Preference is given to tetrahedral gaps, aiming to enhance interfacial layer density. After assessing the configurational entropy across different surface arrangements, findings indicated no significant density reduction at the interface compared to the dense, random liquid structure. This suggests a minimal energetic impact if hard spheres mimic atoms with attractive forces, thus classifying the model as predominantly entropic and forecasting minor energy contributions to  $\gamma_{sl}$ .

$$\gamma = \frac{\alpha_m \Delta S}{N_A v^{2/3}} T \quad (40)$$

where  $\alpha_m$  is 0.86 for the fcc (111) or hcp (0001) surfaces, and 0.71 for the bcc (110) surface. At  $T = T_m$ , this has the same form as the empirical equation with  $\gamma$  proportional to  $\Delta H/v^{2/3}$ .

Up to now we discussed almost exclusively the case of one-component substances. There is considerable interest, especially for metallurgical applications, in the nucleation of binary mixtures or alloys. Calculations in this case require a knowledge not only of the bulk thermodynamics of the mixtures (both liquid and solid), but also information about the liquid–solid surface free energy.

In [56] extended the theory of [55] to binary alloys. They use Eq. 40

$$\gamma = \frac{\alpha_m \Delta S}{N_A v^{2/3}} T \quad (41)$$

and take  $v$  to change linearly with mole fraction between its values for the two pure components. In the same way they take

$$\Delta S = x_A \Delta S_A + (1 - x_A) \Delta S_B \quad (42)$$



where  $x_A$  is the mole fraction of A in the solid and  $\Delta S_A$  and  $\Delta S_B$  are the entropies of fusion of the two separate components.

## 8.2 Temporal Dynamics of Particles Formation

XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX

XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX

## 8.3 Homogeneous Precipitation

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XXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX

## 9 CENTRIFUGAL TECHNOLOGY SELECTION

With the aim to review the available commercial centrifuges, the current section analyses its application for the purification loop of the RC.

The baseline for the given technologies in sections 9.1 and 9.2 is taken from the SoA report [2], where centrifuge devices for liquid-liquid and liquid-solid separators has been analyzed.

### 9.1 Single Step Separation Approach

The aim of this study is to provide the centrifuge technology/ies for FLF primary loop with the purpose to extract the solid impurities in the system. The captured requirements for the impurity loop of FLF has been identified as follows:

- Continuous solid impurity extraction.
- Material compatibility.
- Energy efficiency.
- Efficiency for given particle size.
- Operating temperature.
- Maintenance and cleaning.
- Scalability: maximum flow rate.
- Scalability: pressure drop.
- Concentration of impurities.
- Residence time.

#### Disclaimer

The requirements outlined herein pertain specifically to centrifuge technologies and serve as the foundational basis for the current project. Please note that these requirements are not exhaustive and may be subject to expansion or modification as the project progresses through subsequent stages.

The technologies can be compared based in the criteria given by the requirements, in order to capture which device or set of devices meet successfully the limited framework. Figure 9-1 shows a radar chart with the aim to provide a benchmark based on 8 criteria aligned with the solid separator baseline.

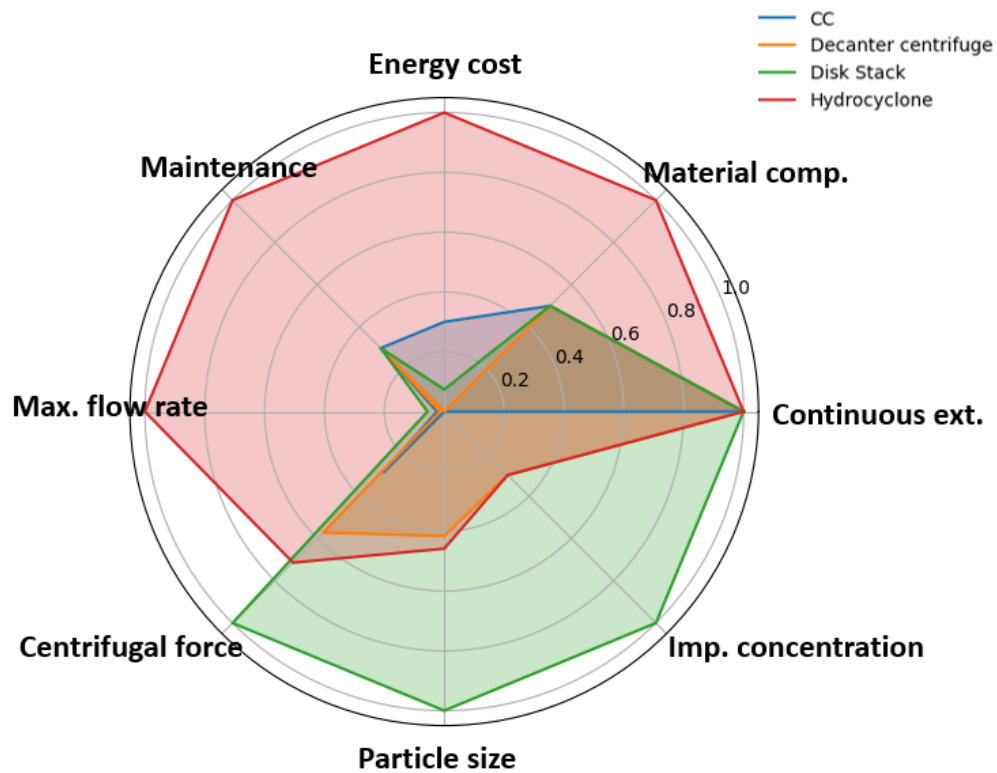


Figure 9-1: Centrifugal technologies comparison chart

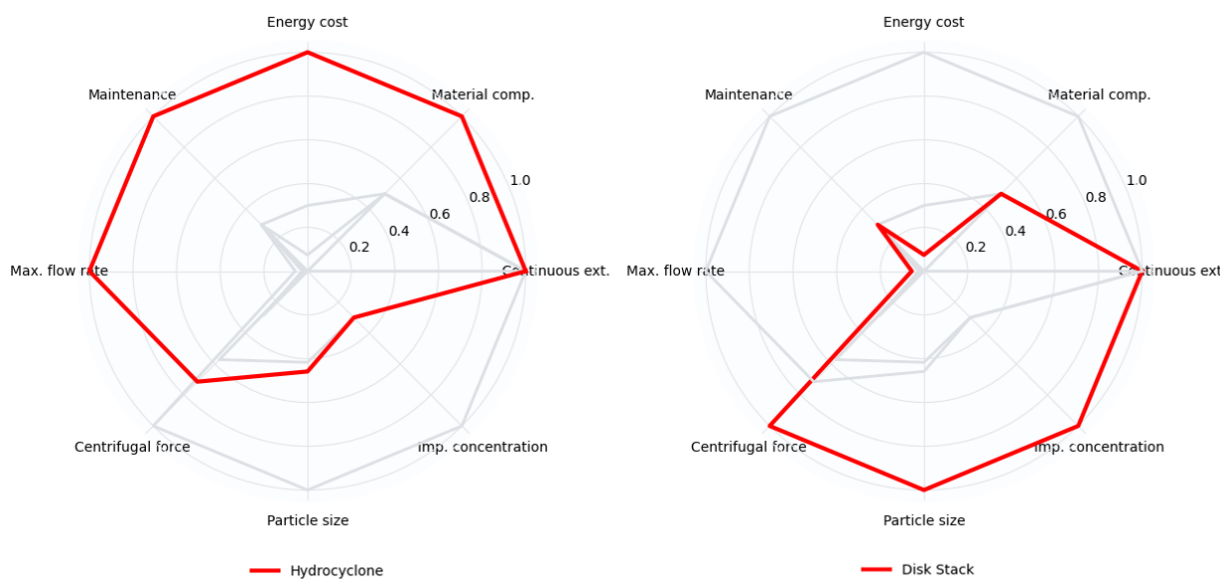


Figure 9-2: Hydrocyclone vs Disk Stack separator: radar plot results

Figure 9-1 shows the performance of 4 centrifugal technologies, with a direct comparison for 8 scores (table 11-1 has the values used for the comparison, that has been normalized, and inverted for Energy Cost, Particle Size, Imp. Concentration). Hydrocyclone and Disk Stack Separator are the technologies with better performance in the evaluated fields, better single definition can be found in figure 9-2, where:

## Hydrocyclone

### **Advantages:**

- **Material compatibility:** The hydrocyclone can be constructed using stainless steel, with SS16 being a commercially available option. Additionally, it can be fabricated from Fiber Reinforced Polymers (FRP), offering notable advantages in aggressive environments such as those found in chemical and nuclear applications with activating products. This versatility in material selection ensures adaptability to varying operational requirements and environmental conditions, enhancing the hydrocyclone's reliability and longevity in demanding settings.
- **Maintenance:** Characterized by its absence of rotatory components, comprising four conical segments interconnected via flange bolted connections. This design feature ensures facilitated access to the internal cavity, enabling procedures for cleaning, replacement, or repair purposes.
- **Energy cost:** The inherent design features, including a tangent inlet inducing a vortex through the cone, eliminates the necessity for moving parts, thus precluding the need for an engine. This architectural advantage translates into significant energy savings, as the hydrocyclone operates without any associated energy costs. Moreover, rigorous examination of inlet velocity's impact underscores the meticulous engineering approach applied to optimize performance.
- **Flow rate:** It demonstrates superior flow rate management in comparison to the other three analyzed technologies. Moreover, it is commercially available to operate within a manifold architecture, allowing for efficient handling of large volumes. Consequently, it emerges as a prime candidate for processing the primary loop lithium in a single operation.

### **Disadvantages:**

- **Particle size:** Commercially available up to a particle size of 12  $\mu m$ , with an impressive efficiency rate of 98%, while maintaining scalability with a compromise on pressure drop (10-200 KPa). This equilibrium represents the optimal trade-off. Consequently, particles below 12  $\mu m$  can be captured by the hydrocyclone; however, ensuring consistent efficiency for particles of this size is not assured. Therefore, additional stages specifically designed for particles of this size range must be incorporated into the purification system to ensure thorough filtration and purification.
- **Impurity concentration:** The technology's optimal operational range encompasses concentrations of impurities in the medium exceeding 10%. Therefore, it is recommended to position this technology as the initial stage within the purification system. This strategic

placement ensures efficient removal of contaminants at higher concentrations, thereby enhancing the overall effectiveness of the purification process. Future stages may address more accurate the impurity concentration in the system.

**Assessment:** The hydrocyclone offers exceptional material compatibility, maintenance-friendly design (without of rotatory components), with negligible energy costs and superior flow rate management, based on manifold architectures: the hydrocyclone emerges as an ideal candidate for processing the primary loop fluid. Despite limitations in capturing particles below 12  $\mu m$  and optimal operation at impurity concentrations exceeding 10%, strategic integration within purification systems enhances overall effectiveness.

### Disk Stack Separator

#### **Advantages:**

- **Particle size:** One of the most notable strengths of this technology lies in its ability to effectively capture particles as small as 1  $\mu m$ , facilitated by its high centrifugal force and innovative ribs cavity design, which accelerates solid precipitation. Particularly advantageous in scenarios where prior classification or clearance of larger particle sizes has been performed, allowing for optimal exploitation of its particle-capturing capabilities.
- **Impurity concentration:** The operational range for these devices remains optimal when impurity concentrations are below 10%, presenting an advantageous characteristic when integrated into multi-stage system operations.
- **Centrifugal force:** As a high-speed separator capable of achieving up to 14,000 G, the disk stack separator offers a distinct advantage due to its efficient operation at relatively low energy costs, contrasting with decanter centrifuges. While centrifuge contractor may require similar energy inputs, they do not attain comparable levels of centrifugal force, highlighting the disk stack separator's pivotal role in separation processes based on its design principles.

#### **Disadvantages:**

- **Energy cost:** Exhibits relatively higher energy consumption compared to alternative solutions. This aspect should be considered in the evaluation of operational costs and efficiency metrics within the full-scale context.
- **Maintenance:** The trade-off associated with attaining high-speed rotation velocities may influence the maintenance of components, wherein direct access to elements is not a direct action, requiring mechanical assembly-disassembly processes that are less straightforward compared to hydrocyclones.

- **Flow rate:** The limited maximum flow rate capacity of such devices makes them unsuitable for fully processing all the lithium within the primary loop. Furthermore, the absence of commercially available manifolds presents a challenge. Therefore, a rigorous study could be needed to strategically place these devices within the system, coupled with the feasibility assessment for developing a manifold configuration to optimize operational efficiency.

**Assessment:** The Disk Stack Separator offers good particle capture capabilities, particularly for particles as small as  $1\ \mu m$ , making it ideal for scenarios requiring precise filtration after prior particle classification. However, its higher energy consumption and maintenance complexities warrant careful consideration. When compared with hydrocyclones, which excel in energy efficiency and maintenance simplicity, they form complementary components in a comprehensive purification system, each tailored to specific operational requirements and constraints. Integrating both technologies strategically within a multi-stage system can optimize overall efficiency and performance, complementing their disadvantages.

#### Decanter Centrifuge

Decanter centrifuges demonstrate comparable performance to hydrocyclones in particle size handling, centrifugal force generation, and impurity concentration control. However, hydrocyclones offer superior energy efficiency, enhanced material compatibility, and lower maintenance requirements, presenting clear advantages. Notably, hydrocyclones excel in maximizing the maximum flow rate, making them a preferred choice in scenarios prioritizing throughput efficiency and operational cost-effectiveness.

#### Centrifuge Contactor

While centrifuge contactors offer the advantage of producing four-phase liquid separation, they do not present a significant advantage in the fields compared to hydrocyclones. The technology lacks suitability in efficiently handling impurities at required flow rates with the precision demonstrated by alternative technologies, diminishing its practical utility in for the primary loop.

## 9.2 Multi-Step Separation Approach

In the context of a multi-stage separation process, the integration of hydrocyclones and Disk Stack Separators offers a comprehensive solution for fluid purification. The hydrocyclone, as particle cut-off controlled by operation parameters, is particularly adept at classifying and separating coarser particles ( $> 12 \mu m$ ), thereby facilitating the initial removal of larger impurities. Its attributes, including superior material compatibility and a maintenance-friendly design, make it a suitable choice for efficiently processing substantial fluid volumes, thanks to its ability to handle high flow rates and adapt to various manifold configurations.

However, the hydrocyclone's inherent limitations, such as its inability to capture particles below  $12 \mu m$  and its optimal operation in scenarios with impurity concentrations above 10%, necessitate additional stages for thorough purification. This is where the Disk Stack Separator comes into play, especially in scenarios where specific targets, such as low impurities or activated products separated by density differences like Li-H, need to be addressed. Renowned for its exceptional particle capture efficacy, particularly for particles as small as  $1 \mu m$ , the Disk Stack Separator strategically placed downstream of the hydrocyclone enhances the purification process by effectively removing finer particles and residual impurities at low concentrations (up to 0.05%), thereby ensuring the level of lithium purity.

Despite its advantages, the Disk Stack Separator incurs relatively higher energy consumption and maintenance complexities compared to the hydrocyclone. Therefore, meticulous attention is needed in optimizing the integration of these technologies to ensure overall efficiency. For example, incorporating the Disk Stack Separator as a secondary stage in the purification process allows for precise filtration after larger particles have been removed by the hydrocyclone, as shown in Figure 9-3. At the same time, it raises the requirement to project a future device that captures the high efficiency for small particles at the energy cost and lithium volumes of the hydrocyclone.

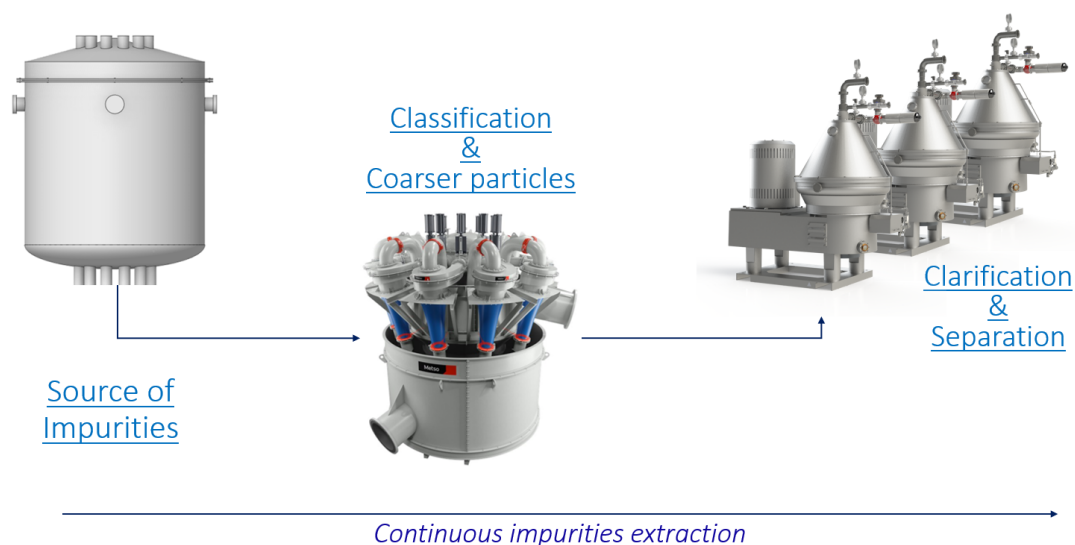


Figure 9-3: Multi stage configuration

In this multi-stage paradigm, the symbiotic relationship between the hydrocyclone and Disk Stack Separator maximizes each technology's strengths while mitigating respective weaknesses.

The relevant technical specifications for both technologies are delineated in Figure 9-4. This technical data serves as the foundational benchmark for subsequent stages of the project, guiding the development of solutions aligned with the current multi-stage framework. The analysis of this data informs decisions regarding the integration of technologies, aiming to optimize the process schema and ultimately enhance overall efficiency and effectiveness.

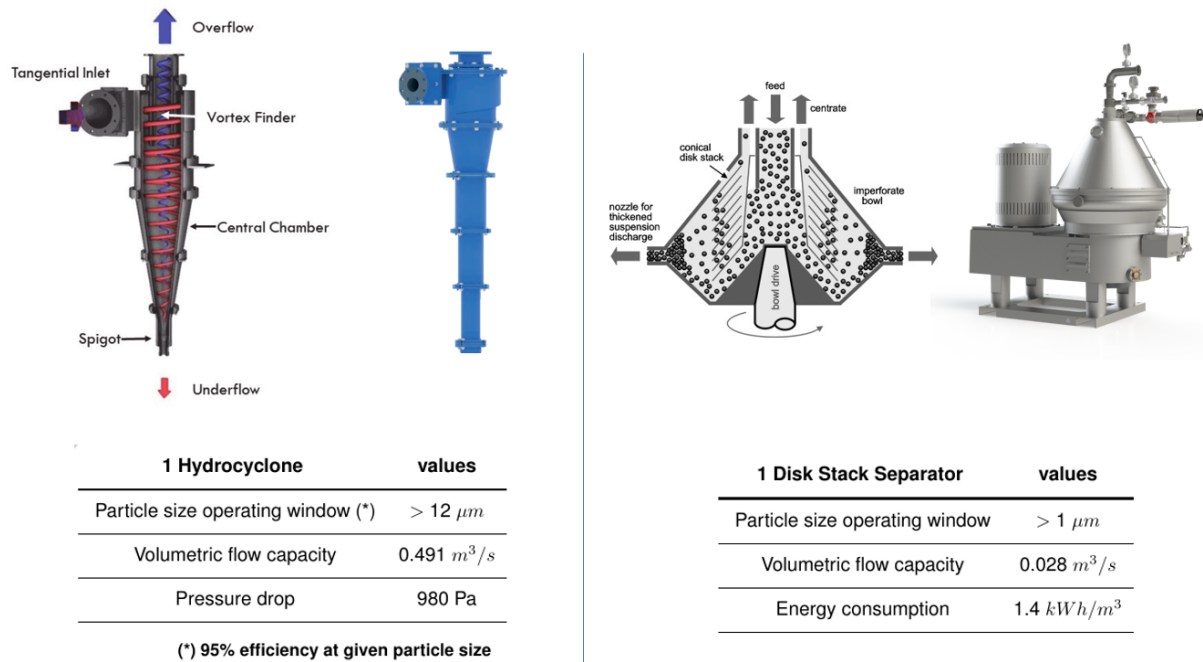


Figure 9-4: Multi stage device data-sheet



### 9.3 Hydrocyclone: Mathematical modelling

Cyclone separators are widely used in the field of chemical, mine and petroleum industries. ref.[57] With the advantages of relative simplicity to fabricate, low cost to operate and good adaptability to extremely harsh conditions, cyclone separators have become one of the most important particle removal devices which are preferably utilized in both environmental and chemical engineering. In order to describe the performance of cyclone separators, many (gas or liquid)-particle separation theories were developed using different methods with different simplifications and assumptions. All these can be roughly divided into the pure theory, the semi-empirical theory and the numerical simulation. The former two include the equilibrium-orbit model, time-of-flight model and hybrid model, etc., the later mainly refers to the computation fluid dynamics (CFD) approach ref.[58].

In detail, the equilibrium-orbit model, as an early methodology of particle separation, determines the particle size for which centrifugal force is exactly balanced by the drag force. Correspondingly, the collection efficiency for the critically sized particle is often assumed to be 50% efficiency called cut particle diameter  $d_{c,p}$  ref.[59].

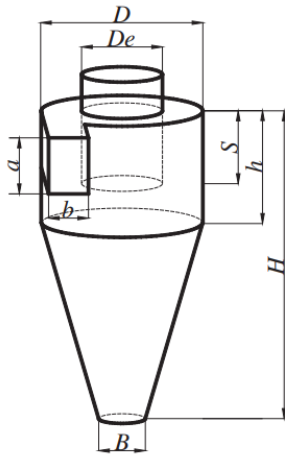
In this section, the necessary parameters and assumptions are defined to correctly define the equilibrium orbit model and obtain an expression for the cyclone separation efficiency.

#### Assumptions

The following assumption have been made in order to develop the equilibrium-orbit model ref. [60]:

- The particle is spherical in shape, the motion of the single particle is not influenced by the presence of neigh-boring particle.
- The tangential velocity of the particle is same as the disperse phase stream; and with the particle is the right dispersed phase, the radial velocity direction fo the particle always point to inner vortex.
- The particle move into the inner vortex is the only way to be separated.

Figure (9-5) show a generic scheme of the cyclone and the description of the different variables is presented in table (9-1).



**Figure 9-5: Schematic diagram of typical cyclone dimensions.**

variable	description
$a$	Cyclone inlet height (m)
$b$	Cyclone inlet width (m)
$B$	Particle outlet diameter (m)
$D$	Cyclone body diameter (m)
$D_e$	Liquid outlet diameter (vortex finder diameter) (m)
$h$	Cyclone cylinder height (m)
$H$	Cyclone height (m)
$S$	Liquid outlet duct length (m)

**Table 9-1: Description of the geometrical variables of one cyclone.**

## 9.4 Fluid model

Swirling flow, or vortex flow, occurs in different types of equipment, such as cyclones, hydrocyclones, spray dryers and vortex burners. Two types of ideal swirling flows are ref.[61]:

- Forced vortex flow: swirling flow with the same tangential velocity distribution as a rotating solid body.

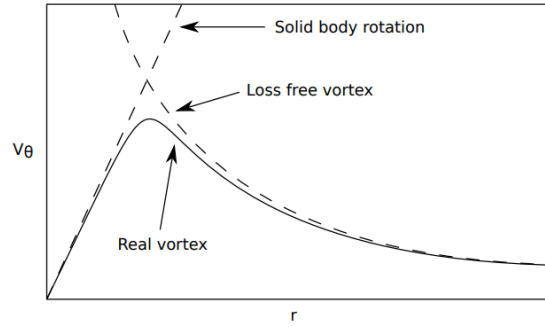
$$v_{\theta,f} = \omega r \quad (43)$$

- Free vortex flow: the way a frictionless fluid would swirl. The tangential velocity in such a swirl is such that the moment-of-momentum of fluid elements is the same at all radius.

$$v_{\theta,f}(r) = \frac{\kappa}{r^n} \text{ where } 0.4 < n < 0.9 \quad (44)$$

where  $\kappa$  is a geometrical parameter and  $n$  is a experimental value taken 0.88 as in ref.[62]

Figure (9-6) show the schema of the real tangential velocity distribution and the comparison with the forced and free vortex flow.



**Figure 9-6: Scheme of the 2 ideal vortex model and the tangential velocity distribution in a real vortex. ref.[61]**

## 9.5 Motion of suspended particles

In a hydrocyclone, the particles of interest are almost always moving relative to the liquid at their terminal velocity, and the terminal velocity of a given particle determines whether the particle will be captured or lost.

Applying Newton's law to a particle moving in a fluid, equating its mass times acceleration to the sum of the forces acting on it, gives :

$$m \frac{dv}{dt} = F_{body} + F_{drag} + F_{unsteady} \quad (45)$$

where the body force is normally due to a centrifugal force and the fluid drag represents the drag acting on a particle that moves with a steady velocity relative to the fluid ref.[62] . According to several authors ref.[57, 61], it turns out that these unsteady terms can be ignored both for the case of a gas cyclone and a hydrocyclone, as practical plant experience with their design and operation indicates that it is not necessary to include either of the terms.

The centrifugal force (first term on the right part ) can be expressed as :

$$F_{body} = F_{centrifugal} = V_p (\rho_p - \rho_f) \mathbf{a} \quad (46)$$

where  $V_p$  is the particle volume,  $\rho_p$  is the particle density,  $\rho_f$  is the fluid density and  $\mathbf{a}$  is the global effect of the radial and angular particle acceleration.

In cylindrical coordinate, omitting the axial contribution,

- $a_r = \frac{dv_{r,p}}{dt} = \frac{d^2 r}{dt^2}$  particle radial acceleration
- $a_c = r \left( \frac{d\theta}{dt} \right)^2 = r \left( \frac{v_{\theta,f}(r)}{r} \right)^2$  particle angular acceleration

assuming that the radial particle acceleration in the steady state is negligible, the centrifugal force is equal to:

$$F_{centrifugal} = \frac{1}{6} \pi d_p^3 \cdot (\rho_p - \rho_f) \cdot \frac{v_{\theta,f}^2(r)}{r} \quad (47)$$

on the other hand, when the particle Reynolds number is low ( $Re_p = \frac{d_p v_{r,p}}{\nu} \ll 1$ ), the equations of

motion for the fluid moving around the particle can be solved, and the drag force calculated. If there is no slip between fluid and particle surface, the particle velocity is equal to the velocity of the fluid at the surface, the result is Stokes drag law:

$$F_{drag} = 3\pi\mu d_p v_{r,p}(r) \quad (48)$$

Therefore, in the steady state, the drag force have to be equal that the centrifugal force:

$$\sum F_p = 0 \Rightarrow F_{centrifugal} = F_{drag} \quad (49)$$

and the radial velocity of the particle can be expressed as a function of the angular velocity of the fluid given by the vortex flow model as

$$v_{r,p}(r) = \frac{\Delta\rho d_p^2}{18\mu} \cdot \frac{v_{\theta,f}^2(r)}{r} \quad (50)$$

The following subsections define different parameters necessary to calculate the cyclone separation efficiency.

## 9.6 Cyclone effective volume

To avoid the non-uniform effect on particle collection distance caused by difference between cylindrical and conical shape, the cylinder-conical geometry is equivalently modified as a right cylinder cyclone according to the principle of conservation of effective volume. The equivalent cyclone volume ( $V_{cs}$ ) and radius ( $R$ ) can be calculated by: ref.[59]

$$V_{cs} = \begin{cases} \frac{\pi D^2 h}{4} + \frac{\pi D^2}{4} \cdot \frac{S+l-h}{3} \cdot \left[1 + \frac{D_c}{D} + \left(\frac{D_c}{D}\right)^2\right], & \text{if } l \leq (H-S) \\ \frac{\pi D^2 h}{4} + \frac{\pi D^2}{4} \cdot \frac{H-h}{3} \cdot \left[1 + \frac{B}{D} + \left(\frac{B}{D}\right)^2\right], & \text{if } l > (H-S) \end{cases} \quad (51)$$

$$R_w^* = \begin{cases} \left[\frac{V_{cs}}{\pi(S+l)}\right]^{1/2}, & \text{if } l \leq (H-S) \\ \left[\frac{V_{cs}}{\pi H}\right]^{1/2}, & \text{if } l > (H-S) \end{cases} \quad (52)$$

where  $D_c = D - \frac{(D-B)(S+l-h)}{H-h}$  and  $l$  is called as the natural vortex length of cyclone separator. It is defined as the vertical distance from the bottom of the vortex finder to the end of the vortex at which the outer vortex is reversed or turned into the inner vortex.  $l$  is actually the effective vortex length in cyclone separator if it is less than the dimension  $H-S$ . Otherwise,  $H-S$  should be the effective vortex length because it depends on the geometrical dimensions of cyclone. The most famous and widely used relation for estimating the natural vortex length is the Alexander' formula ref.[59]:

$$l = 2.3 \left(\frac{D^2}{ab}\right)^{1/3} \quad (53)$$

## 9.7 Residence time model

The residence time  $t_{res}$  is the average time that a particle is inside the cyclone. The expression to calculate  $t_{res}$  depend of the geometry of the cyclone and the inlet volumetric flow rate, so according to the geometry selected (Figure 9-5) the residence time can be calculates as ref.[59]:

$$t_{res} = \begin{cases} \frac{\pi(R^2 - R_e^2)}{Q/2} \cdot l, & \text{if } l \leq (H - S) \\ \frac{\pi(R^2 - R_e^2)}{Q/2} \cdot (H - S), & \text{if } l > (H - S) \end{cases} \quad (54)$$

## 9.8 Separation efficiency model

In order to calculate the separation efficiency of the cyclone, a balance of mass was made in the volume of control presented in the Figure (9-7) ref.[59, 60].

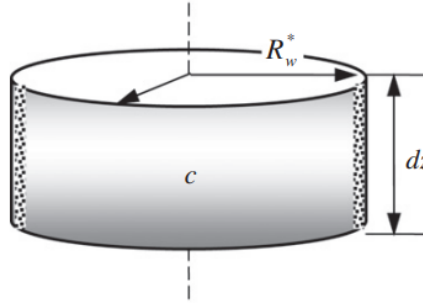


Figure 9-7: volume of control used in the separation efficiency model. ref.[59]

In this control volume, it is assumed that uncollected particles in any plane perpendicular to the cyclone axis presents a status of complete radial back-mixing, the boundary layer near the equivalent wall is neglected and particles which move to the equivalent wall will be trapped. If the particle concentration in the control volume is  $c$ , then the particle flux toward the equivalent wall is  $cv_{r,p}(R_w^*)$ . Therefore, over a height  $dz$  the sedimentation rate of particles at the equivalent wall is  $2\pi R_w^* cv_{r,p}(R_w^*) dz$ . Correspondingly, the rate of particles separated from the control volume is  $c\pi R_w^{*2} dz$ . According to particle mass balance, we have:

$$\frac{dM}{dt} = \sum M_{in} - \sum M_{out} \quad (55)$$

$$\frac{d(c\pi R_w^{*2} dz)}{dt} = - \sum M_{out} = -cv_{r,p}(R_w^*) 2\pi R_w^* dz \quad (56)$$

$$\frac{dc}{dt} = - \frac{2v_{r,p}(R_w^*)}{R_w^*} \cdot c \quad (57)$$

$$\frac{c(t)}{c_0} = \exp\left(-\frac{2v_{r,p}(R_w^*)t}{R_w^*}\right) \quad (58)$$

Integrating, with  $c(t=0) = c_0$  and  $c_{final} = c(t_{res})$  where  $t_{res}$  is the particle residence time:

$$\frac{c_{final}}{c_0} = \exp\left(-\frac{2v_{r,p}(R_w^*)t_{res}}{R_w^*}\right) \quad (59)$$

therefore, the separation efficiency is defined as

$$\eta = 1 - \frac{c_{final}}{c_0} \quad (60)$$

$$\eta = 1 - \exp\left(-\frac{2v_{r,p}(R_w^*)t_{res}}{R_w^*}\right) \quad (61)$$

where  $v_{r,p}(R_w^*)$  is the particle settling velocity at the equivalent wall and is calculated according to Eq. (50)

## 10 Results: Parametric analysis

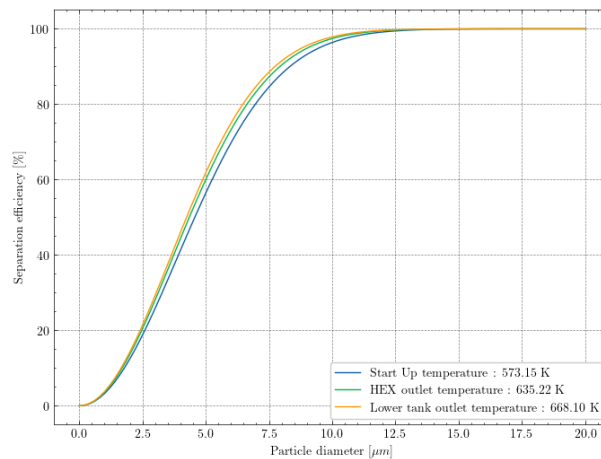
For the following analysis, the geometric dimensions present in the table 10-1 have been used as a basis. This information was used to see how the separation efficiency of the cyclone varies when the Lithium temperature, the diameter of the cyclone and the inlet flow change.

variable	value
$D$	0.5 m
$\frac{D_e}{D}$	0.5
$\frac{a}{D}$	0.5
$\frac{b}{D}$	0.2
$\frac{S}{D}$	0.5
$\frac{H}{D}$	4
$\frac{h}{D}$	1.5
$\frac{B}{D}$	0.375
<b>Fluid material</b>	Lithium
<b>Fluid Temperature</b>	688 K
<b>Particle material</b>	Fe

Table 10-1: Input information used for the parametric analysis section

### 10.1 Parametric analysis: Temperature

Figure (10-1) shows the efficiency as a function of the particle diameter of Fe for the temperature of the Start-Up, HEX outlet and lower tank calculated in ref. [63].

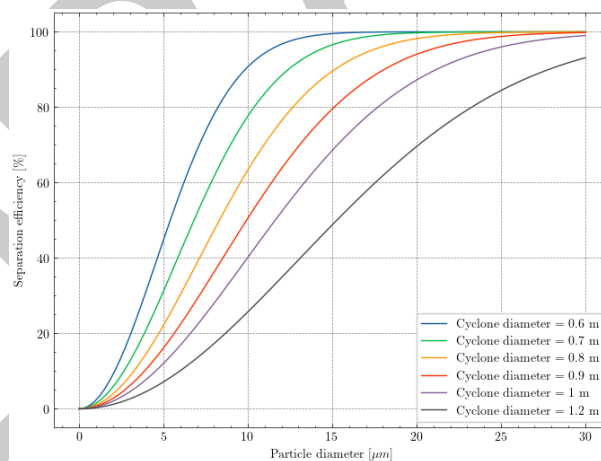


**Figure 10-1: Separation efficiency as a function of the particle diameter of Fe for different temperatures.**

As the temperature increases, the fluid viscosity decreases, so the drag force decreases and the particle velocity increases. Also, the difference in density fluid-particle also increases (since the density of lithium decreases with temperature) so that the centrifugal force grows. Those effects allow efficiency to increase with temperature.

## 10.2 Parametric analysis: Cyclone diameter

Figure (10-2) shows the separation efficiency as a function of the particle diameter of Fe for different cyclone diameters.



**Figure 10-2**

By increasing the diameter and keeping the scaling and flow variables constant, the velocity in the inlet decreases. This decrease causes that the velocity of the particles to drop and the efficiency to drop. On the other hand, as the diameter increases, the residence time increases given by the equation (54) and this effect tends to increase efficiency, however, it is not as important as the other effect mentioned before.

Thus, there is a trade-off in deciding the optimal cyclone diameter, and it will also depend on the minimum particle diameter of the impurities which need to be eliminated.

### 10.3 Parametric analysis: volumetric inlet flow rate

Given one of the limitations of cyclones is the possibility of scaling efficiency to industrial-type flows, in the chemical or mine industry it is very common to use more than 1 cyclone in parallel ref. [57]. For this reason it is of interest to know how the efficiency changes as we increase the volumetric inlet flow rate of the cyclone.

Figure (10-3a) show the separation efficiency as a function of the particle diameter for different volumetric inlet flow rate form from 0.5 to 3.5  $m^3/s$  (similar to pilot plant).

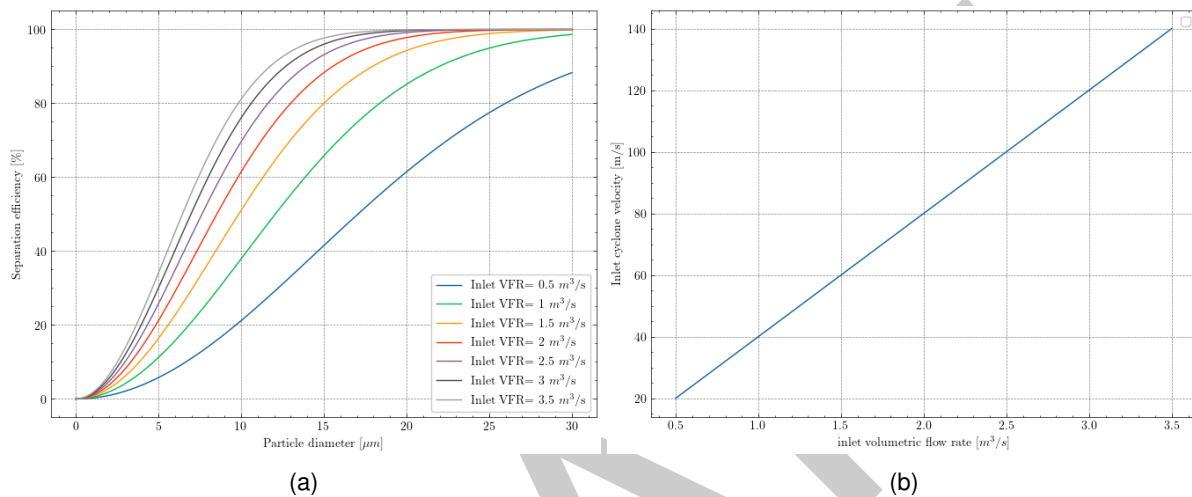


Figure 10-3

It can be seen that as volumetric flow rate decrease, the separation efficiency decreases. This is because as the flow rate at the inlet of the cyclone decreases, the velocity in the inlet drop (Figure 10-3b) and consequently the velocity with which the particle heads towards the walls of the cyclone. It is important to note that industrial-scale cyclones usually operate with an inlet speed between 20-30 m/s, so this limitation should be added in the following sections to have a realist results.

Figure (10-4a) show the separation efficiency as a function of the particle diameter when VFR change +/- 20 % using 3  $m^3/s$  as a  $VFR_{base}$ . Figure (10-4) display the relative separation efficiency  $\left( \frac{\eta(VFR) - \eta(VFR_{base})}{\eta(VFR_{base})} \right)$  as a function of the particle diameter.



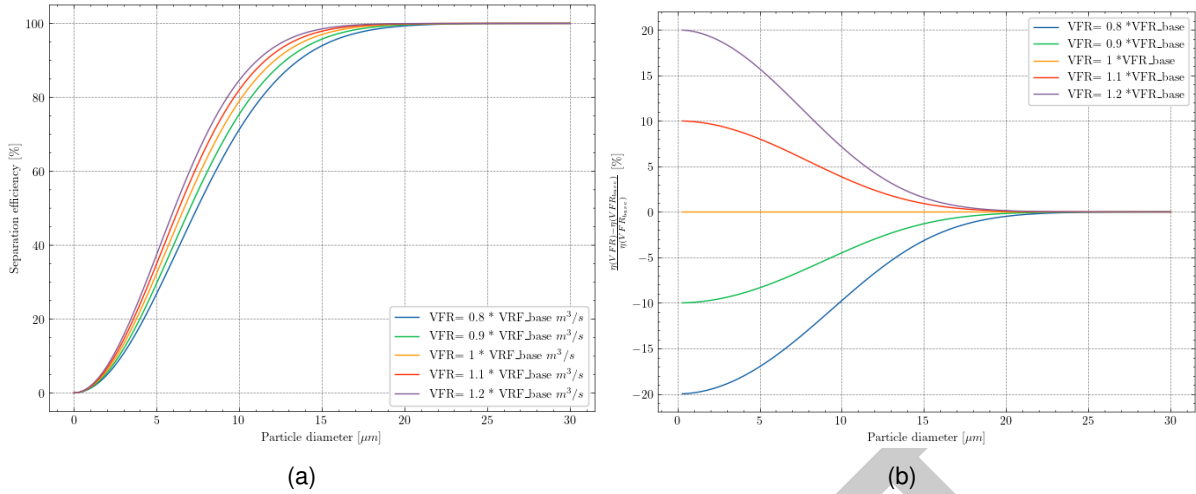


Figure 10-4

Figure (10-4) shows that the efficiency increases proportionally to the increase in VFR when the particle diameter is low. As the diameter of the particle increases, the effect of increasing VFR begins to decrease. However, it must be taken into account that the pressure loss varies with the square of the velocity in the inlet ( $\Delta p \propto v_{inlet}^2$ ), so if the flow rate changes 10% the pressure loss would increase by approximately 21%.

## 10.4 Optimization methodology

In the previous section, the dimensions of a cyclone present in ref.[59] were used. That cyclone was used as a reference to see how the efficiency change for some parameters of interest such as temperature or flow rate, but said geometry was not optimal for the problem to be solved. For this reason, in this section the optimization process of the cyclone geometry is presented to maximize the separation efficiency, using both the fluid and the particle materials of interest for the problem.

### 10.4.1 Geometrical optimization

The next section presents how the optimization process was developed. For this, the Python library Optimize is used and SLSQP (Sequential Least Squares Programming) is used as the optimization method. In order to use this method, it is necessary to define the function to be minimized, the variables and both geometric and performance limitations.

In order to define the function, if a target efficiency  $\eta_{target}$  is defined, according to equation (61) the radial velocity of the particle is

$$v_{r,p} = -\frac{\ln(1 - \eta_{target})}{2t_{res}} \cdot R_w^* \quad (62)$$

On the other hand, using the equation (44), (52) and (54) the diameter of the particle can be expressed

as:

$$d_p^2 = \frac{18\mu v_{r,p}(R_w^*)R_w^*}{\Delta\rho v_{\theta,f}^2(R_w^*)} \quad (63)$$

$$d_p^2 = -\frac{\ln(1 - \eta_{target})}{2t_{res}} \cdot \frac{18\mu R_w^{*2}}{\Delta\rho v_{\theta,f}^2(R_w^*)} \quad (64)$$

$$d_p^2 = -\frac{\ln(1 - \eta_{target})}{2t_{res}} \cdot \frac{18\mu R_w^{*(2+2n)}}{\kappa^2} \quad (65)$$

where the diameter of the particle is defined as a function of the target efficiency, inlet velocity (present in the parameter  $\kappa$ ) and geometry (present in  $t_{res}$ ,  $R_w^*$  and  $\kappa$ ). With this information, was used as a function to minimize, the cut diameter defined as the particle diameter for which the capture efficiency is equal to 50 %  $d_{p,c} = d_p(\eta = 50\%)$ :

$$d_{p,c}(\vec{x}) = \left( -\frac{\ln(0.5)}{2t_{res}} \cdot \frac{18\mu R_w^{*(2+2n)}}{\kappa^2} \right)^{1/2} \quad (66)$$

where  $\vec{x} = (D, D_e, H, B, h, S, a, b)$  is the vector with all of geometrical variables of the cyclone.

In order to close the problem, the constrains used were:

1.  $h > S$
2.  $h > a$
3.  $D > D_e + b$
4.  $D_e > b$
5.  $H > S$
6.  $H > h$
7.  $D_e > B$
8.  $10^\circ < \alpha < 20^\circ$ , where  $\alpha = \arctan\left(\frac{D-B}{2(H-h)}\right)$
9.  $v_{inlet} < v_{max}$

Given that the problem has 8 variables there are only inequalities as a constrains, more than one local minimum may exist within the domain. For this reason, the optimizer was initialized with different seeds in order to obtain the different local minima present in the domain. Then, a family of cyclones was obtained that meet the conditions within the domain, where the cutting diameter varies by less than 10% and the geometric dimensions change.

#### 10.4.2 Optimization: Results

Table (10-2) show the total volumetric mass flow rate for the commercial and pilot plant calculated in ref. [63].

Parameter	Pilot plant	Commercial plant
VFR per loop [m3/s]	3.27	4.9
VFR total [m3/s]	3.27	29.4

Table 10-2: Volumetric flow rate for the pilot and commercial plant calculated in ref. [63]

For the optimization process, a parametric analysis was carried out where the VFR was varied in the inlet of the cyclone in order to have the same operating conditions in the cyclone for both the commercial and pilot plants and, consequently, the highest separation efficiency with the minimum loss of energy. The ratio between the VFR of the commercial plant and the pilot plant is approximately 9 ( $\frac{(VFR_{total})_{commercial}}{(VFR_{total})_{pilot}} \approx 9$ ) so if you want to have the same efficiency for both plants, it is necessary to increase the number of cyclones 9 times when scaling the plant from the pilot to the commercial one.

Figure (10-5a), (10-5b) and (10-5c) shows the cut off diameter ( $\eta = 50\%$ ) for the Fe, Cr and AlN, respectively. For this analysis, it has been used that the maximum velocity in the inlet has to be less than 25 m/s.

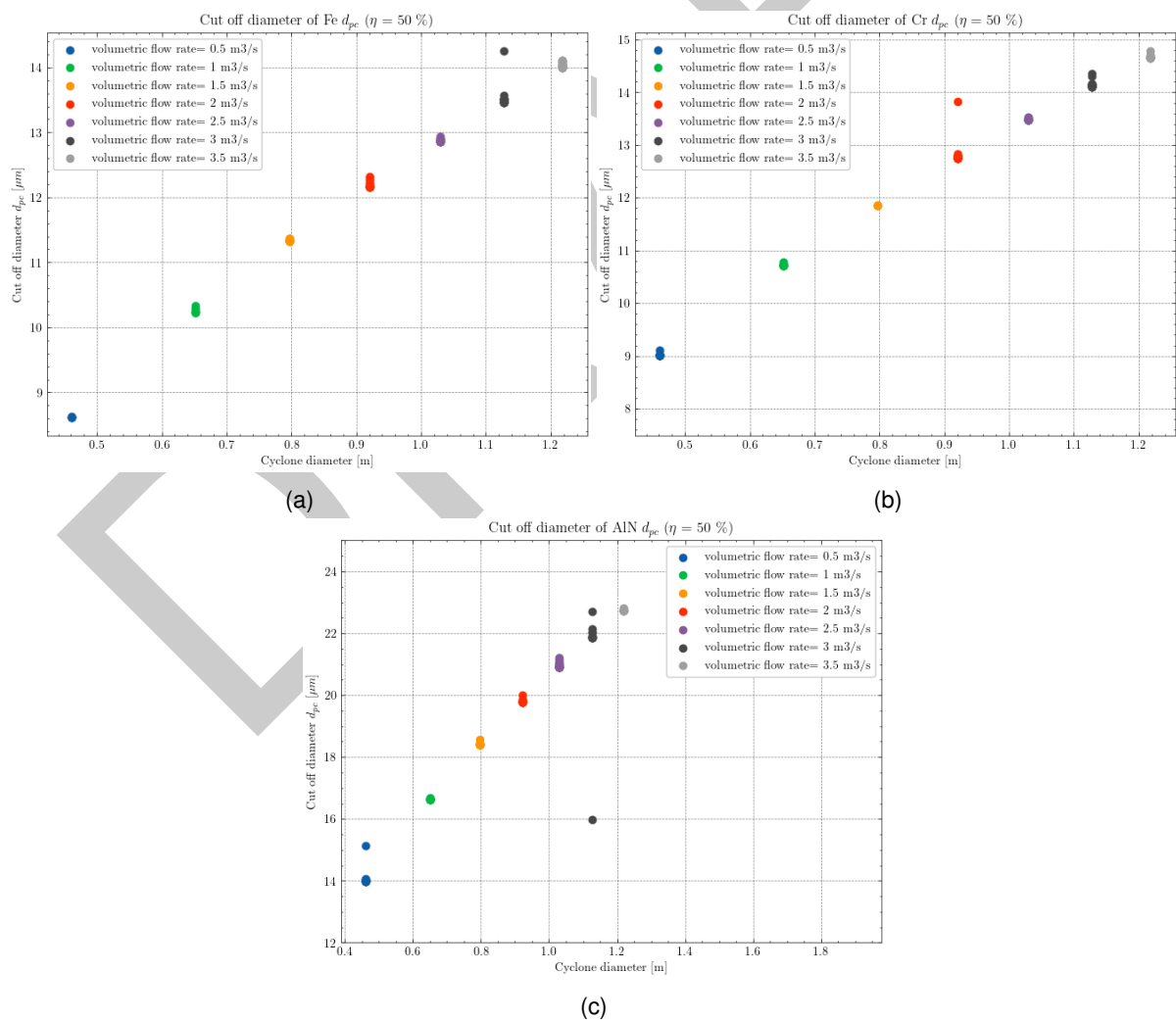


Figure 10-5

It can be seen that the cutting diameter of both Fe and Cr are quite similar and smaller than that of AlN. This is because the density of Fe is similar to that of Cr, while the density of AlN is much lower. This causes the radial velocity of the particle towards the walls to be lower and the efficiency tends to decrease, so the diameter of the particle must be larger to be captured.

Since the inlet maximum velocity was limited in the optimization process, when the volumetric flow rate increase the cyclone diameter and the inlet dimensions have to grow to have enough space to allocate the inlet and reduce the velocity.

Table (10-3) presents the dimensions of 5 cyclones that can operate at different VFRs. In addition, the cutting diameter for Fe, Cr and AlN is presented and an estimate of the number of cyclones that could be used either in the commercial plant or in the pilot plant.

<b>Cyclone case</b>	<b>I</b>	<b>II</b>	<b>III</b>	<b>IV</b>	<b>V</b>
<b>Cyclone body diameter (m)</b>	0.460	0.651	0.797	0.921	1.030
<b>Liquid outlet diameter (vortex finder diameter) (m)</b>	0.211	0.291	0.357	0.412	0.461
<b>Cyclone inlet height (m)</b>	0.230	0.326	0.399	0.460	0.515
<b>Cyclone inlet width (m)</b>	0.092	0.130	0.159	0.184	0.206
<b>Liquid outlet duct length (m)</b>	0.436	0.620	0.760	0.877	0.981
<b>Cyclone cylinder height (m)</b>	1.483	2.063	2.526	2.917	3.261
<b>Cyclone height (m)</b>	0.460	0.651	0.797	0.921	1.030
<b>Particle outlet diameter (m)</b>	0.046	0.065	0.080	0.092	0.103
<b>Angle (°)</b>	11.453	11.723	11.732	11.731	11.731
<b>Inlet VFR (m<sup>3</sup>/s)</b>	0.5	1.0	1.5	2.0	2.5
<b>Inlet Velocity (m/s)</b>	23.585	23.585	23.585	23.585	23.585
<b>Cut off diameter Fe (microns)</b>	8.610	10.230	11.322	12.053	12.864
<b>Cut off diameter Cr (microns)</b>	9.013	10.468	11.861	12.746	13.477
<b>Cut off diameter AlN (microns)</b>	10.207	16.620	18.393	19.765	21.215
<b>Number of cyclone pilot plant</b>	6	3	2		
<b>Number of cyclone commercial plant</b>	54	27	18		

Table 10-3: Cyclone optimization results

It can be seen that as the volumetric flow rate at the inlet increases, the cut off diameter decrease for all the particles analyzed, causing the lose of separation efficiency. On the other hand, in order to choose the correct cyclone, the total pressure loss of the system have to be considered. In the literature there are a large number of correlations to calculate pressure loss [57, 58], however these are developed mainly for gas-solid cyclones and not for liquid-solid as in this case. For this reason, in the CFD section,

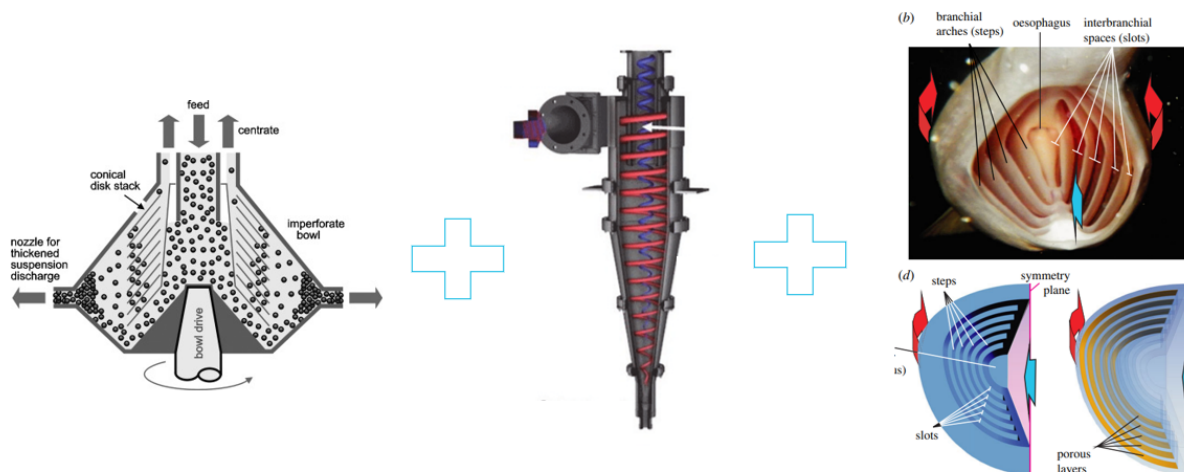
importance will be given to the calculation of said parameter.

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## 10.5 Conceptual Design Approach

In the forthcoming project phases, the conceptual design will navigate the design space between the hydrocyclone and Disk Stack Separator, aiming to optimize the multi-stage purification process. With the requirements outlined in Section 9.1 and the technical specifications detailed in Figure 9-4 serving as foundational guidelines, the design endeavor will seek to exploit the current capabilities of the multi-stage purification system. Drawing inspiration from external sources, such as referenced paper ref. [64], the conceptual design will explore innovative approaches (Figure 10-6) to enhance particle capture efficiency, impurity removal, and overall system performance.

Integration of advanced materials, novel geometries, and optimized operational parameters will be central to the conceptual design exploration. By leveraging insights from existing research and technological advancements, the conceptual design aims to push the boundaries of purification efficiency, ultimately culminating in the development of a device that maximizes the potential of the multi-stage purification process.



**Figure 10-6: Conceptual design approach: possible lines of work**

## 11 CONCLUSIONS

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**ANNEX 1**

<b>Evaluation</b>	<b>units</b>	<b>CC</b>	<b>Decanter centrifuge</b>	<b>Disk Stack</b>	<b>Hydrocyclone</b>
Continuous extraction	yes/not	yes	yes	yes	yes
Material compatibility	-	SS	SS	SS	SS/Polymers
Energy cost <sup>1</sup>	<i>kW</i>	18.5	250	75	0
Particle size	$\mu m$	NRAI <sup>2</sup>	>10	>1	>12
Maintenance & cleaning	-	moving parts	moving parts	moving parts	excellent
Max. flow rate	$m^3/s$	0.012	0.007	0.028	0.5
Impurities concentration	%	NRAI <sup>2</sup>	>10%	>0.02%	>10%
Centrifugal force	G	2000	4000	14000	5000

**Table 11-1: Centrifugal separator comparison data-sheet**<sup>1</sup>Based on required engine power to achieve the operation centrifugal force, for comparative reasons.<sup>2</sup>Not Reasonable Available Information.