

Chemical Kinetics →



★ 1st Order Reaction → Vimp (Que)

Topics to be Covered →

- ① Rate of Reaction
- ② Factors affecting rate of reaction
- ③ Reaction mechanism by which, Reaction proceeds.

Types of Reaction →

Very fast Rx. ⁿ	Moderate rx. ⁿ / slow rx. ⁿ	Very slow Rx. ⁿ
10 ⁻¹⁴ - 10 ⁻¹⁶ sec for completion	sec, min, hours for completion	days, months, Years for completion
Ionic Rx. ⁿ Acid-Base Rx. ⁿ Neutralisation Rx. ⁿ	N ₂ + 3H ₂ ⇌ 3NH ₃ H ₂ O ₂ ⇌ H ₂ O	Rusting of iron
HCl + NaOH → NaCl + H ₂ O		

Types of ROR →

avg. rate of rx.ⁿ
interval of time

$$\text{Rate} = \frac{\Delta C}{\Delta t}$$

instantaneous rate
of rx.ⁿ
particular instant of time.

$$\text{Rate} = \frac{dC}{dt} \quad \text{slope of graph}$$

Average Rate

	(R) → (P)	
t ₁	A ₁ B ₁	A ₁ > A ₂ B ₂ > B ₁ t ₂ > t ₁
t ₂	A ₂ B ₂	

$$\text{avg rate} = \frac{\Delta C}{\Delta t} = \frac{A_2 - A_1}{t_2 - t_1} \quad (-ve)$$

avg speed with reactant, already ek (-ve) sign lena hai
So that, product + hojaye

$$R = - \left(\frac{A_2 - A_1}{t_2 - t_1} \right)$$

avg rate with respect to product →

$$R = + \left(\frac{B_2 - B_1}{t_2 - t_1} \right)$$

Rate / Speed / Velocity of a Reaction



t=0	a	0	$\left. \begin{array}{l} \\ x \\ a \end{array} \right\} \begin{array}{l} \text{Rate} = \frac{a-x-a}{t_1-0} = -\frac{x}{t_1} \\ \\ \text{Rate} = \frac{0-a-x}{t_2-t_1} = -\frac{a-x}{t_2-t_1} \end{array}$
t=t ₁	a-x	x	
t=t ₂	0	a	

Rate of Rx.ⁿ = $\frac{\text{Change in Conc. of Reactant / product}}{\text{Change in time}}$

Reactant → (-ve), product → (+ve)

$$R = \frac{\Delta C}{\Delta t}$$

$$\Delta C = C_f - C_i$$

$$\Delta t = t_f - t_i$$

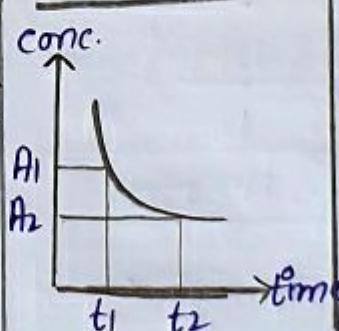
Unit of Rate →

$$R = \frac{\Delta C}{\Delta t} \sim \frac{\text{mol}}{\text{lit} \cdot \text{sec}}$$

$$\text{mol lit}^{-1} \text{sec}^{-1}$$

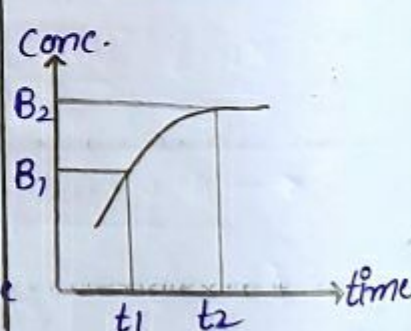
Graphs →

Reactant



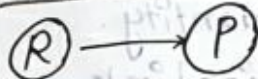
$$\text{avg rate} = - \left(\frac{A_2 - A_1}{t_2 - t_1} \right)$$

Product



$$\text{avg rate} = + \left(\frac{B_2 - B_1}{t_2 - t_1} \right)$$

Instantaneous Rate \rightarrow



$$\text{Rate} = -\frac{dR}{dt}$$

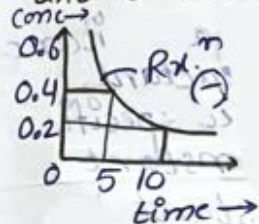
$$\text{Rate} = +\frac{dP}{dt}$$

graph \rightarrow



$$\text{slope} = \tan \theta = \frac{dC}{dt}$$

Que) Calculate avg rate b/w 0 to 5 sec. and 5-10 sec.



$$\text{avg rate} = \frac{\Delta C}{\Delta t}$$

$$R = -\left(\frac{0.4 - 0.6}{5 - 0}\right)$$

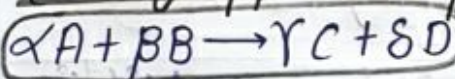
$$= \frac{0.2}{5} = \frac{1}{25} \quad (1)$$

$$(2) \rightarrow R = -\left(\frac{0.4 - 0.2}{10 - 5}\right)$$

$$= \frac{0.2}{5} = \frac{1}{25} \quad (2)$$

$$\text{mol L}^{-1} \text{s}^{-1}$$

Rate of appearance / disappearance



Stoichiometry not needed.

$$\text{Rate of disappearance} = -\frac{\Delta C}{\Delta t} \quad (\text{Reactant})$$

$$(ROD)_A = -\frac{\Delta A}{\Delta t} = -\frac{dA}{dt}$$

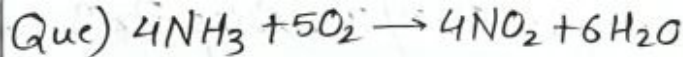
$$(ROD)_B = -\frac{\Delta B}{\Delta t} = -\frac{dB}{dt}$$

Coeff. se
Koi matlab
nahi

$$\text{Rate of appearance (products)} = +\frac{\Delta C}{\Delta t}$$

$$(ROA)_C = \frac{\Delta C}{\Delta t} = \frac{dC}{dt}$$

$$(ROA)_D = \frac{\Delta D}{\Delta t} = \frac{dD}{dt}$$



R.O.A. of NO?

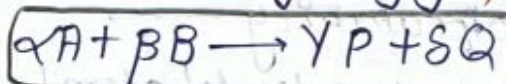
$$\text{Sol.} \rightarrow \text{ROA} = \frac{\Delta C}{\Delta t} = +\frac{\Delta [\text{NO}]}{\Delta t}$$

ROD of NH_3 ?

$$\text{ROD} = -\frac{\Delta [\text{NH}_3]}{\Delta t} \text{ or } -\frac{d[\text{NH}_3]}{dt}$$

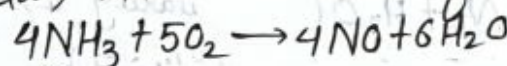
Rate of Reaction
Stoichiometry aayega.

Rx.ⁿ must be balance



$$\text{ROR} = -\frac{1}{\alpha} \frac{\Delta A}{\Delta t} = -\frac{1}{\beta} \frac{\Delta B}{\Delta t} = +\frac{1}{\gamma} \frac{\Delta P}{\Delta t} = +\frac{1}{\delta} \frac{\Delta Q}{\Delta t}$$

Que) Write the Rate of Rx.ⁿ



$$\text{Sol.} \rightarrow \text{ROR} = \frac{1}{4} \frac{\Delta \text{NH}_3}{\Delta t} = -\frac{1}{5} \frac{\Delta \text{O}_2}{\Delta t} = \frac{1}{4} \frac{\Delta \text{NO}}{\Delta t} = \frac{1}{6} \frac{\Delta \text{H}_2\text{O}}{\Delta t}$$

Que) If rx.ⁿ $2\text{NO}_2 \rightarrow 2\text{NO} + \text{O}_2$, rate of formation of NO is 6m/s. Calculate rate of disappearance of NO_2 .

$$\text{Sol.} \rightarrow \frac{d[\text{NO}]}{dt} = 6\text{m/s}$$

$$\text{ROR} = -\frac{1}{2} \frac{d[\text{NO}_2]}{dt} = \frac{1}{2} \frac{d[\text{NO}]}{dt} = \frac{d[\text{O}_2]}{dt}$$

$$= -\frac{d[\text{NO}_2]}{dt} = \frac{d[\text{NO}]}{dt}$$

$$\text{ROD} = 6\text{m/s}$$

Types of Reaction (Mechanism)

① Elementary Reaction / Simple Rx.ⁿ
Single step Rx.ⁿ \rightarrow

Completes in single step.

Don't need mechanism

Exponents in rate law = stoichiometric coeff. of Rx.ⁿ

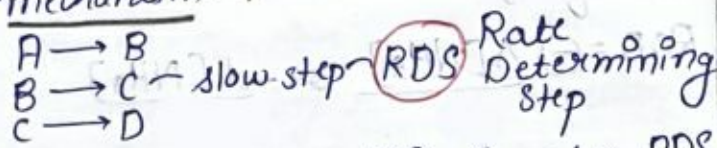


$$R = k[A]^a[B]^b \quad \text{Order} = n = a + b$$

$a + b \rightarrow$ can't be negative, zero, fraction

② Complex Rxⁿ / Multistep Rxⁿ →

Rxⁿ completes in multisteps.
Mechanism is must.
main Rxⁿ $A \rightarrow D$
mechanism →



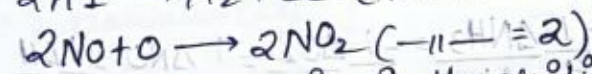
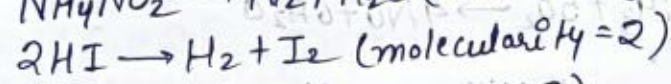
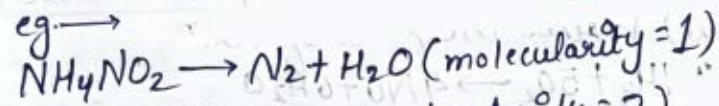
Rate of complex rxⁿ is given by RDS

$$\text{Rate} = k[B]^1$$

Molecularity →

Total number of molecule/atom/ion participating in an elementary rxⁿ is called **molecularity**.

eg →



→ molecularity is theoretical concept

→ only integer, can't be 0, -ve, fraction.

Elementary Rxⁿ

Molecularity = stoichiometry = Order.

Complex Rxⁿ

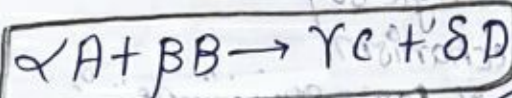
molecularity is seen for each step.

Rxⁿ todo, mechanism me aur hai step ka likho.

Complex Rxⁿ → Overall molecularity is meaningless.

Max. value of molecularity is (3).

← Rate Law →



$$\text{Rate} \propto [A]^x [B]^y$$

x = Order wrt A

y = Order wrt B

$\begin{matrix} x = \alpha & \text{or} & x \neq \alpha \\ y = \beta & & y \neq \beta \end{matrix}$
elementary rxⁿ

$$x + y = n \text{ — overall order of Rxⁿ —}$$

Order →

→ experimental quantity

→ Zero / -ve / fraction / integer

Elementary Rxⁿ

→ Order = Stoichiometric Coeff

Rate Constant (K) →

proportionality constant / rate const. / Velocity cons. / Specific rate const.

$$R \propto [A]^x [B]^y$$

$$R = k[A]^x [B]^y$$

If, $[A] = [B] = 1$ → ROR at unit conc. of reactant.
Then, $\text{Rate} = k$ is called specific Rate constant.

Unit of Rate Constant K

$$R \propto [A]^x [B]^y \quad x + y = n \text{ — order —}$$

$$R = k[A]^x [B]^y$$

$$k = \frac{\text{Rate}}{[A]^x [B]^y} = \frac{\text{Rate}}{\text{conc}} = \frac{(\text{mol/litre}) \text{ time}^{-1}}{(\text{mol/litre})^n}$$

$$k = (\text{mol/litre})^{1-n} \text{ time}^{-1}$$

Unit for Zero Order → $\text{mol lit}^{-1} \text{ time}^{-1}$

$$k = (\text{mol/litre})^1 \text{ time}^{-1}$$

Unit for 1st order →

$$k = (\text{time}^{-1})$$

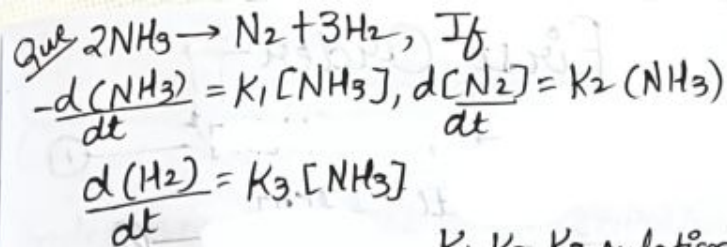
Unit for 2nd Order →

$$k = (\text{mol/litre})^{-1} \text{ time}^{-1} \text{ or } \text{mol}^{-1} \text{ litre time}^{-1}$$

Factors affecting K →

K → Temp (dependent)

Independent of Conc.



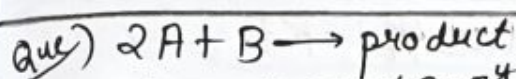
K_1, K_2, K_3 relation?

Solⁿ ROR = $-\frac{1}{2} \frac{d[\text{NH}_3]}{dt} = +\frac{d[\text{N}_2]}{dt} = \frac{1}{3} \frac{d[\text{H}_2]}{dt}$

$\frac{K_1[\text{NH}_3]}{2} = K_2[\text{NH}_3] = \frac{1}{3} K_3[\text{NH}_3]$

$\frac{K_1}{2} = K_2 = \frac{K_3}{3}$

$3K_1 = 0.6K_2 = 2K_3$ (X by 6)



Rate law = $K[\text{A}]^x[\text{B}]^y$

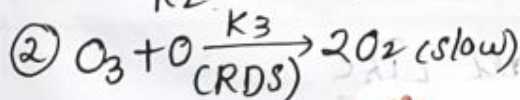
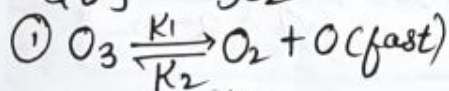
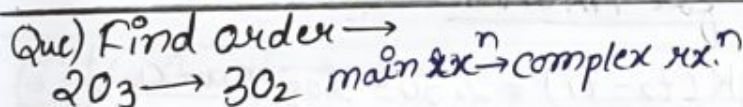
→ if conc. of A is doubled, ROR becomes double, cal. X.

→ $R \propto [\text{A}]^x$ $x=1$
 $2 \propto 2^x$

→ Conc of B → double, then ROR becomes half, Calculate Y.

Solⁿ $R \propto [\text{B}]^y$

$\frac{1}{2} \propto [2]^y$ $y=-1$
 $2^{-1} \propto 2^y$



Rate = $K_3[\text{O}_3][\text{O}]$

$K_{eq} = \frac{[\text{O}_2][\text{O}]}{[\text{O}_3]}$

$[\text{O}] = \frac{[\text{O}_3] K_{eq}}{[\text{O}_2]}$

(O intermediate)

Rate = $(K_3)[\text{O}_3] \frac{K_{eq}[\text{O}_3]}{[\text{O}_2]}$

$= K' \frac{[\text{O}_3]^2}{[\text{O}_2]} \rightarrow K' [\text{O}_3]^2 [\text{O}_2]^{-1}$

Order = $2-1=1$

Zero Order Reaction



Rate = $K[\text{A}]^0$ — (2)

Differential rate eq.ⁿ →

Rate = $-\frac{d[\text{A}]}{dt}$ — (1)

① = ②

$-\frac{d[\text{A}]}{dt} = K[\text{A}]^0$

$-d[\text{A}] = K dt$

$d[\text{A}] = -K dt$

Integral Rate Law → ① = ②

$-\frac{d[\text{A}]}{dt} = K[\text{A}]^0$

$-\frac{d[\text{A}]}{[\text{A}]^0} = K dt$

$\int_{A_0}^{A_t} d[\text{A}] = \int_0^t K dt$

$A_0 - A_t = Kt$

Half life

$t_{50\%} / t_{1/2} / t_{50\% \text{ remaining}} / t_{\text{half}}$

$[\text{A}_t] = \frac{A_0}{2}$ when $t = \frac{t_1}{2}$

$A_0 - A_t = Kt \rightarrow 0 \text{ order}$

$A_0 - \frac{A_0}{2} = K t_{1/2}$

$\frac{A_0}{2} = K t_{1/2}$

$t_{1/2} = \frac{A_0}{2K}$

$t_{1/2} \propto A_0$ initial concentration

Time for Completion →

when $t = t_{100}$, $A_t = 0$

$$A_0 - A_t = Kt \quad \text{Zero order}$$

$$A_0 - 0 = K t_{100} \quad \boxed{2 \times t_{50\%} = t_{100\%}}$$

$$\boxed{t_{100} = \frac{A_0}{K}}$$

$$\boxed{2 \times t_{\text{half}} = t_{\text{complete}}}$$

Zero Order Rxⁿ completes in two half life

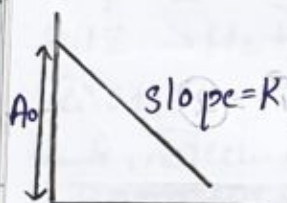
Graph → Zero Order

① A_t v/s t →

$$A_0 - A_t = Kt$$

$$A_t = A_0 - Kt$$

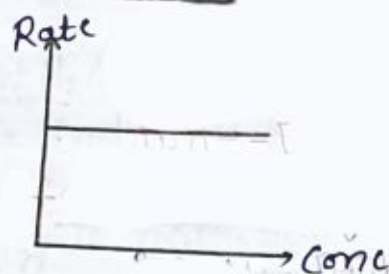
$$\boxed{y = c - mx}$$



② Rate v/s Conc →

$$\text{Rate} = K[A]^0$$

$$\boxed{\text{Rate} = K}$$

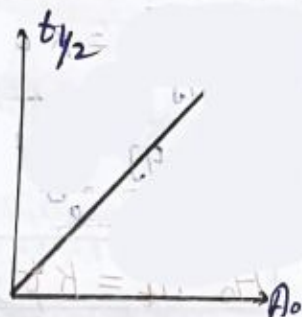


③ $t_{1/2}$ v/s A_0 →

$$t_{1/2} = \frac{A_0}{2K}$$

$$\boxed{m = \frac{1}{2K}}$$

$$y = mx$$



Zero Order

t_{fraction}

$$\boxed{t_{\text{frac}} = \text{frac} \times \frac{A_0}{K}}$$

$$\frac{50}{100} = t_{1/2} = \frac{1}{2} \times \frac{A_0}{K}$$

$$\frac{100}{100} = t_1 = \frac{A_0}{K}$$

$$\frac{75}{100} = t_{3/4} = \frac{3}{4} \times \frac{A_0}{K}$$

$$\frac{20}{100} = t_{1/5} = \frac{1}{5} \times \frac{A_0}{K}$$

$$\frac{25}{100} = t_{4/5} = \frac{1}{4} \times \frac{A_0}{K}$$

**NEET
SLAYER**

First Order →

$$\text{Rate law} \rightarrow \text{Rate} = K[A]^1 \quad \text{--- ①}$$

$$\text{Rate} = -\frac{d[A]}{dt} \quad \text{--- ②}$$

$$\text{①} = \text{②}$$

$$K[A] = -\frac{d[A]}{dt}$$

$$\boxed{-\frac{d[A]}{A} = K dt}$$

Integral rate eqⁿ →

$$\boxed{\ln[A_0] - \ln[A_t] = Kt}$$

$$\boxed{\ln \frac{A_0}{A_t} = Kt}$$

$$\frac{A_0}{A_t} = e^{Kt}$$

$$\boxed{A_t = A_0 e^{-Kt}}$$

$$Kt = 2.303 \log \frac{A_0}{A_t}$$

$$\boxed{Kt = 2.303 \log \left(\frac{a}{a-x} \right)}$$

for interval →

$$\boxed{K(t_2 - t_1) = 2.303 \log \left(\frac{a-x_1}{a-x_2} \right)}$$

Half Life

$$A_t = \frac{A_0}{2} \quad \text{when } t = t_{1/2}$$

$$\boxed{\ln \frac{A_0}{A_t} = Kt} \quad \text{--- 1st order}$$

$$\ln \frac{A_0}{A_0/2} = K t_{1/2}$$

$$\ln 2 = K \times t_{1/2}$$

$$t_{1/2} = \frac{\ln 2}{K} = \frac{0.693}{K}$$

$t_{1/2}$ of first order reaction is independent of initial concentration

Time for Completion $\rightarrow t_{100\%}$

When $t = t_{100\%}$, $A_t = 0$

$$Kt = \ln \frac{A_0}{A_t} \rightarrow t_{100\%} = \infty$$

1st order reaction never completes.

Short trick \rightarrow

$$t_{3/4} = 2 t_{1/2} \quad t_{75\%} = 2 t_{50\%}$$

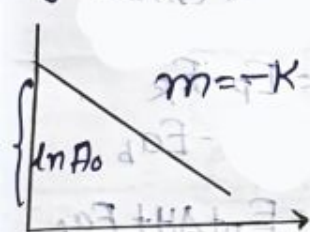
Que) \leftarrow Graph \rightarrow

① $\ln A_t$ v/s $t \rightarrow$ ② A_t v/s $t \rightarrow$

$$\ln A_0 - \ln A_t = Kt$$

$$\ln A_t = \ln A_0 - Kt$$

$$y = c - mx$$



$$A_t = A_0 e^{-Kt}$$

$$y = C e^{-x}$$



③ $\log A_t$ v/s $t \rightarrow$

$$Kt = 2.303 \log \frac{A_0}{A_t}$$

$$Kt = 2.303 (\log A_0 - \log A_t)$$

$$\log A_t = \frac{-Kt}{2.303} + \log A_0$$

$$y = -mx + c$$

Degree of Dissociation (α) \rightarrow

$$\alpha = \frac{\text{moles dissociated}}{\text{initial moles}}$$

$$\alpha = \frac{x}{a}$$

$$A_t = A_0 e^{-Kt} \text{ 1st Order}$$

$$a - x = a e^{-Kt}$$

$$x = a(1 - e^{-Kt})$$

$$\frac{x}{a} = 1 - e^{-Kt}$$

$$\alpha = 1 - e^{-Kt}$$

Que) $t_{1/2}$ of 1st Order reaction, 0.3 min, then ROR when conc. of reactant is 0.5 M.

$$\text{Soln} \rightarrow \text{Rate} = K[A]^1$$

$$t_{1/2} = \frac{0.693}{K}$$

$$0.3 = \frac{0.693}{K}$$

$$K = 2.31 \text{ min}^{-1}$$

$$\text{Rate} = 2.31 \times 0.5 = 1.155 \text{ M min}^{-1}$$

n^{th} Order \rightarrow

$$Kt = \frac{1}{n-1} \left[\frac{1}{[A_t]^{n-1}} - \frac{1}{[A_0]^{n-1}} \right] \quad n \neq 1$$

$t_{1/2}$ of n^{th} Order \rightarrow

$$t_{1/2} \propto \frac{1}{[A_0]^{n-1}}$$

$$t_{1/2} \propto \frac{1}{a^{n-1}}$$

Zero Order \rightarrow

$$t_{1/2} \propto A_0$$

First Order \rightarrow

$$t_{1/2} \propto 1$$

Second Order \rightarrow

$$n = 2$$

$$Kt = \left[\frac{1}{[A_t]} - \frac{1}{[A_0]} \right]$$

$$t_{1/2} \rightarrow$$

$$t_{1/2} \propto \frac{1}{[A_0]}$$

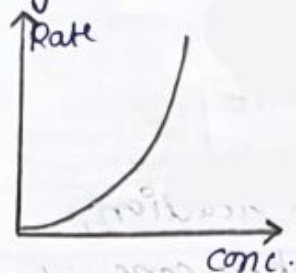
$$t_{1/2} = \frac{1}{K[A_0]}$$

Graph

① Rate v/s Conc.

$$\text{Rate} = K(\text{conc})^2$$

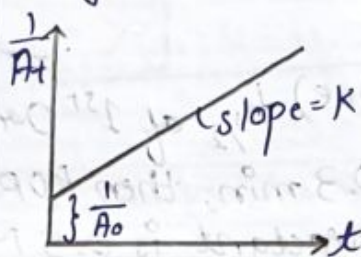
$$y = Kx^2$$



② $\frac{1}{A_t}$ v/s t

$$Kt = \frac{1}{A_t} - \frac{1}{A_0}$$

$$y = mx + c$$

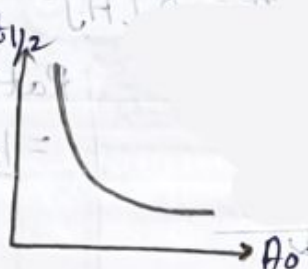


③ $t_{1/2}$ v/s $A_0 \rightarrow$

$$t_{1/2} = \frac{1}{K A_0}$$

$$y = \frac{1}{Kx}$$

$$xy = K$$

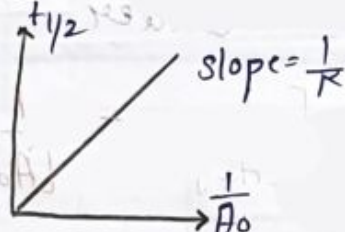


④ $t_{1/2}$ v/s $\frac{1}{[A_0]}$

$$t_{1/2} = \frac{1}{K A_0}$$

$$y = \frac{1}{K} \cdot \frac{1}{A_0}$$

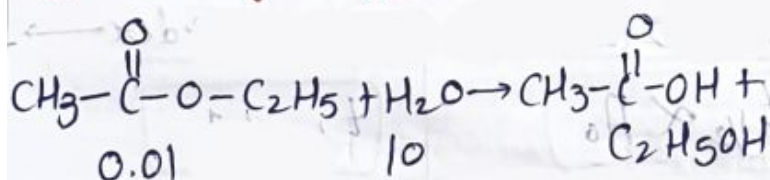
$$y = mx$$



Pseudo 1st Order Rx.ⁿ

$Rx.^n \rightarrow \text{Order} = 1$ but molecularity = 2

eg - Hydrolysis of ester



$$R = K [\text{CH}_3 - \overset{\text{O}}{\parallel} \text{C} - \text{OC}_2\text{H}_5] [\text{H}_2\text{O}]$$

const

$$R = K' [\text{CH}_3 - \overset{\text{O}}{\parallel} \text{C} - \text{O} - (\text{C}_2\text{H}_5)]$$

Order = 1
molecularity = 2

One reactant be in excess.

Collision Theory \rightarrow

activation energy -

minimum energy required by reactant for converting into product

Threshold Energy -

min. energy possessed by reacting molecule for chemical rx.ⁿ to occur

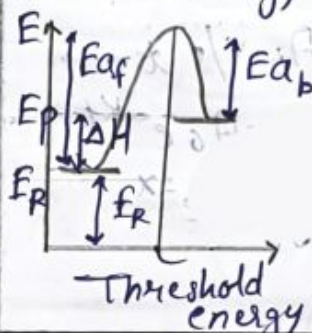
Energy diagram

Endothermic

$$H_p - H_R > 0$$

$$\Delta H > 0$$

$R + \text{Heat} \rightarrow P$
Stable \rightarrow less energy



$$\Delta H = E_P - E_R = E_{a_f} - E_{a_b}$$

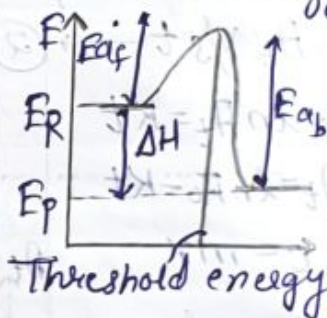
$$\begin{aligned} TE &= E_R + E_{a_f} \\ &= E_R + \Delta H + E_{a_b} \\ &= E_P + E_{a_b} \end{aligned}$$

Exothermic

$$H_p - H_R < 0$$

$$\Delta H < 0$$

$R \rightarrow P + \text{heat}$
Stable
less energy

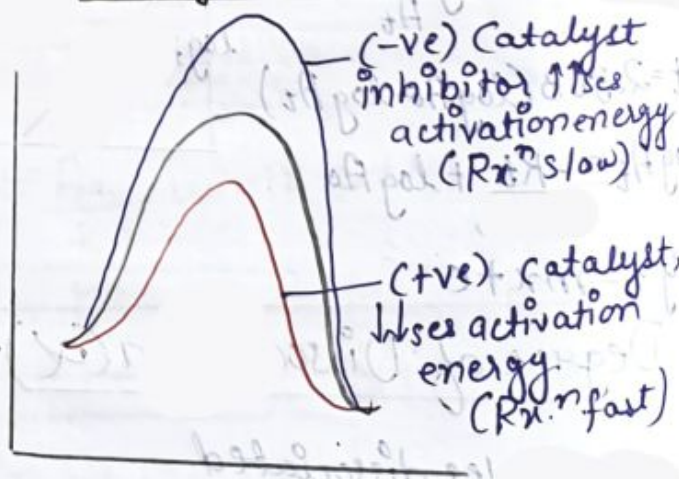


$$\Delta H = E_P - E_R$$

$$= E_{a_f} - E_{a_b}$$

$$\begin{aligned} TE &= E_P + \Delta H + E_{a_f} \\ &= E_P + E_{a_b} \end{aligned}$$

Catalyst and TE \rightarrow



Arrhenius Eqⁿ

$$K = A e^{\frac{-E_a}{RT}}$$

Rate constant Arrhenius Const. Activation energy Temp (K) gas const

$$\ln K = \ln A - \frac{E_a}{RT}$$

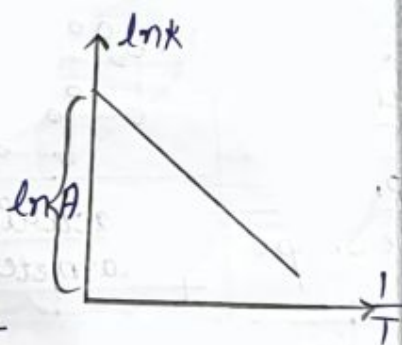
Graph →

$\ln K$ v/s $\frac{1}{T}$ →

$$\ln K = \ln A - \frac{E_a}{RT}$$

$$y = c - mx$$

$$m = \tan \theta = -\frac{E_a}{R}$$



Relation b/w K_1 and K_2 in Arrhenius

$$K_1 = A e^{\frac{-E_a}{RT_1}} \quad \text{--- (1)}$$

$$K_2 = A e^{\frac{-E_a}{RT_2}} \quad \text{--- (2)}$$

$$\left(\frac{2}{1}\right) \rightarrow$$

$$\frac{K_2}{K_1} = \frac{e^{-E_a/RT_2}}{e^{-E_a/RT_1}}$$

$$\ln \frac{K_2}{K_1} = \frac{E_a}{R} \left[\frac{1}{T_1} - \frac{1}{T_2} \right]$$

$$\log \frac{K_2}{K_1} = \frac{E_a}{2.303R} \left[\frac{1}{T_1} - \frac{1}{T_2} \right]$$

Que) Cal value of pre-exponential factor and activation energy, (Kcal) — $\log K = 6 - \frac{200}{T}$

Solⁿ → $\log K = \log A - \frac{E_a}{2.303RT}$

$$\log A = 6 \rightarrow A = 10^6$$

$$\frac{E_a}{2.303RT} = \frac{200}{T} = E_a = 9.2 \text{ Kcal}$$

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