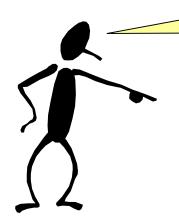


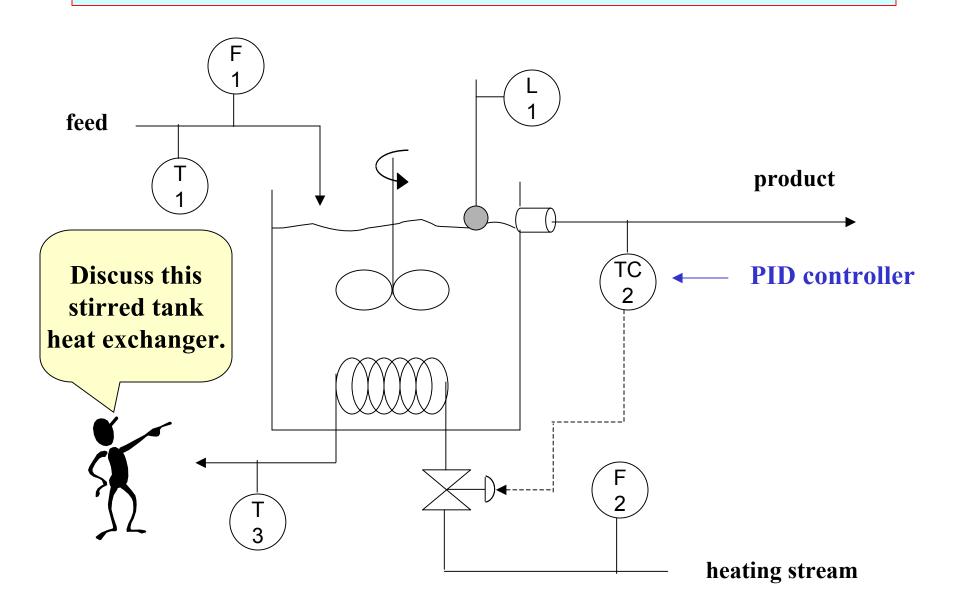
When I complete this chapter, I want to be able to do the following.

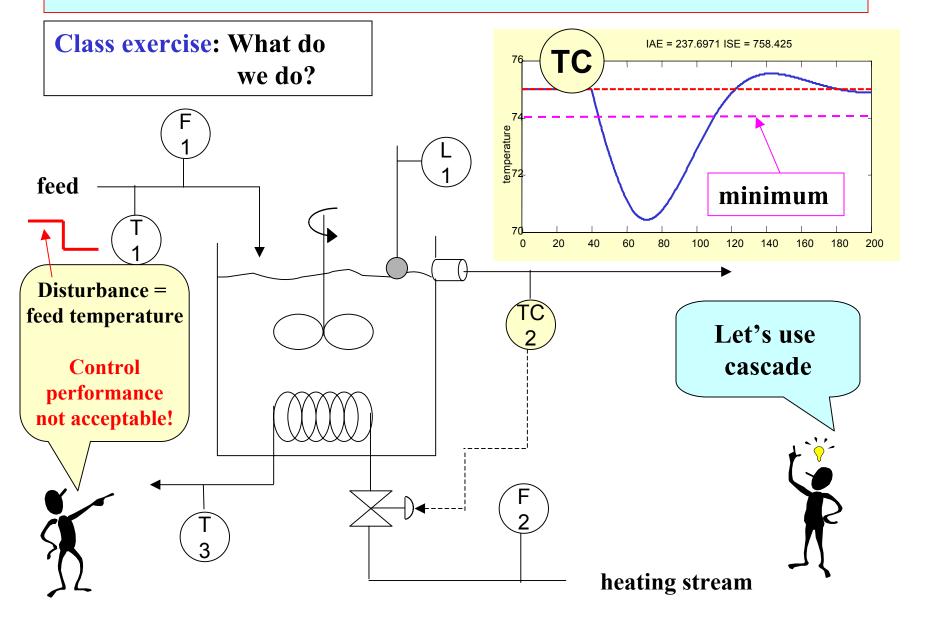
- Identify situations for which feedforward is a good control enhancement
- Design feedforward control using the five design rules
- Apply the feedforward principle to other challenges in life



Outline of the lesson.

- A process challenge improve performance
- Feedforward design rules
- Good features and application guidelines
- Several process examples
- Analogy to management principle





CASCADE DESIGN CRITERIA FOR T1

Cascade is desired when

- 1. Single-loop performance unacceptable
- 2. A measured variable is available

- 3. Indicate the occurrence of an important disturbance
- 4. Have a causal relationship from valve to secondary
- 5. Have a faster response than the primary

CASCADE DESIGN CRITERIA FOR T1

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OK

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CASCADE DESIGN CRITERIA FOR T1

Cascade is desired when

OK

NO!

- 1. Single-loop performance unacceptable
- 2. A measured variable is available

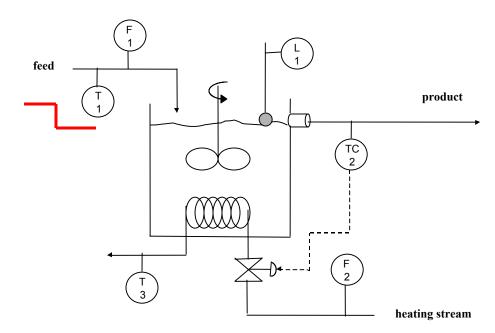
A secondary variable must

- 3. Indicate the occurrence of an important disturbance
- 4. Have a causal relationship from valve to secondary
- 5. Have a faster response than the primary

Cascade not possible. We need another enhancement!

Let's think about the process behavior.

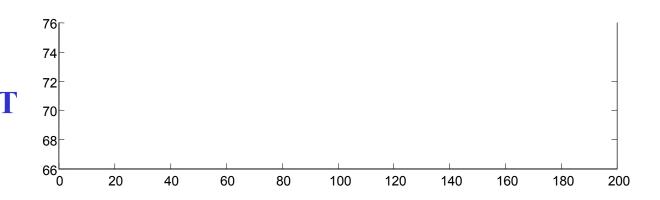
- Causal relationship from T₁ disturbance to T₂ (without control)
- How can we manipulate valve to compensate?



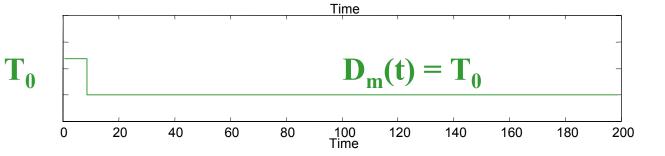
$$v \text{ (valve)} \rightarrow Q \rightarrow TC$$

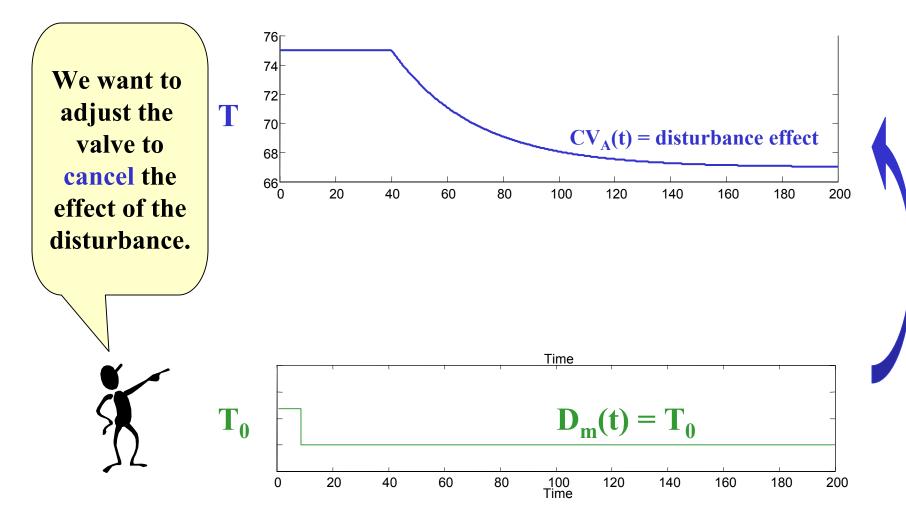
$$T_0$$
(Feed temperature)

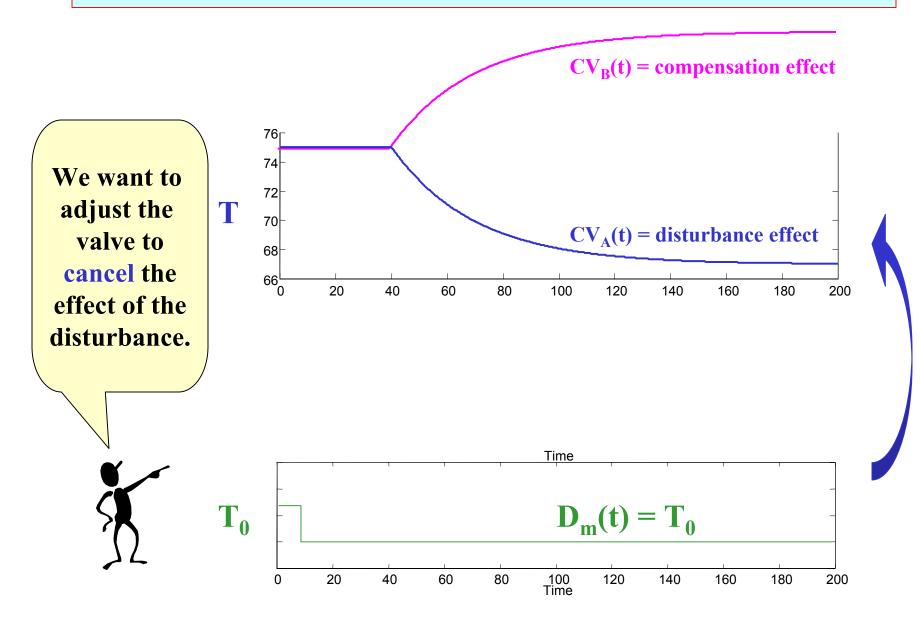
We want to adjust the valve to cancel the effect of the disturbance.

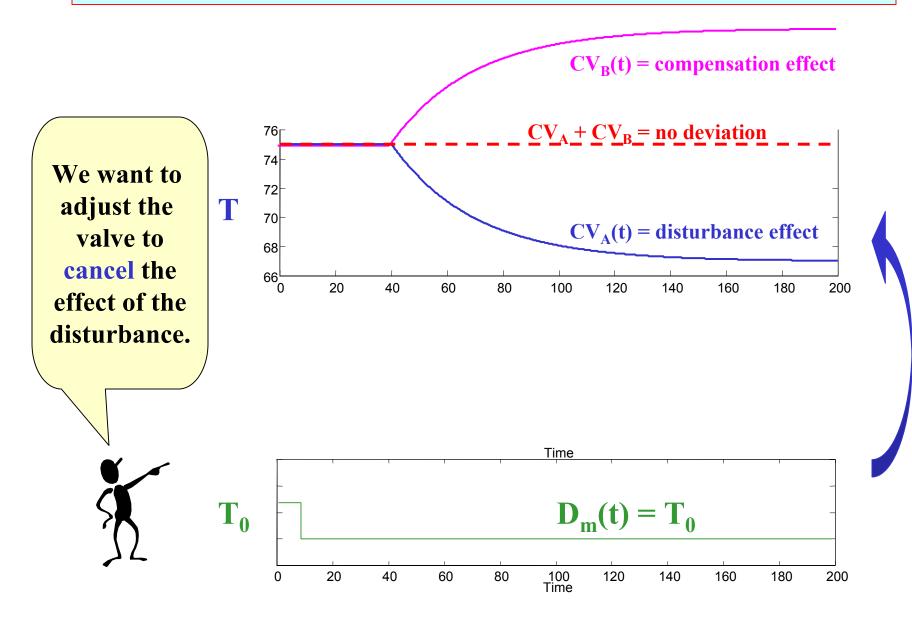


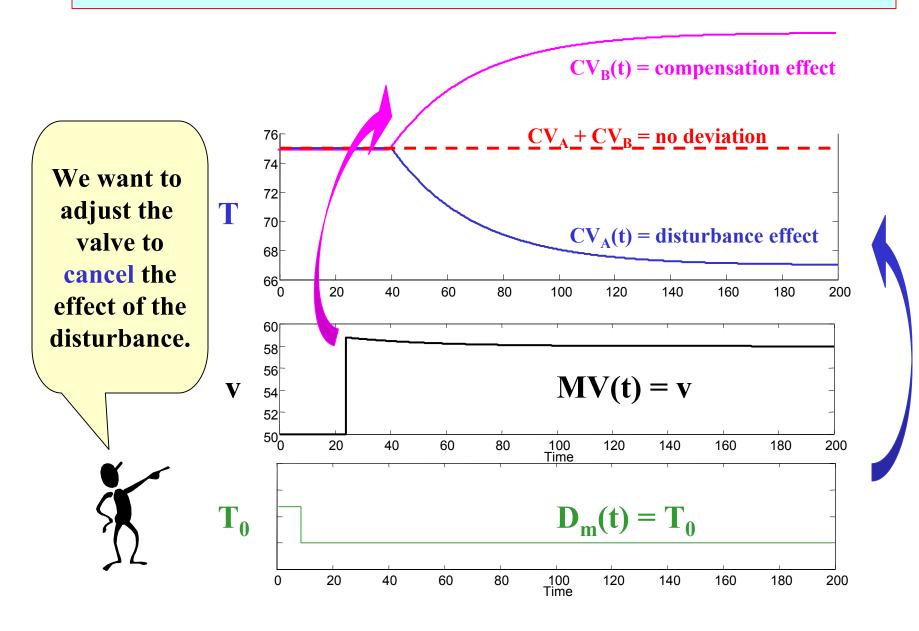




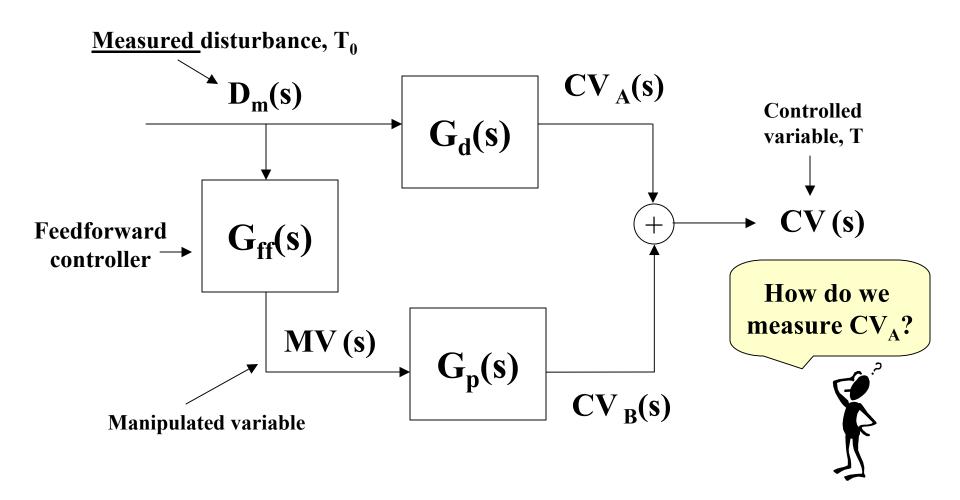








We use block diagram algebra to determine the form of the calculation $[G_{ff}(s)]$ to achieve the desired performance.



$$CV(s) = CV_A(s) + CV_B(s) = 0$$
??
$$= \left[G_d(s) + G_{ff}(s)G_p(s)\right]D_m(s) = 0$$

Not a PID algorithm! Why?



$$G_{ff}(s) = \frac{MV(s)}{D_m(s)} = -\frac{G_d(s)}{G_p(s)}$$

This is general!



$$G_{ff}(s) = \frac{MV(s)}{D_m(s)} = -\frac{G_d(s)}{G_p(s)}$$

Special case of $G_p(s)$ and G_d(s) being first order with dead time

Please verify.

$$G_{ff}(s) = \frac{MV(s)}{D_m(s)} = K_{ff} \frac{T_{ld}s + 1}{T_{lg}s + 1} e^{-\theta_{ff}s}$$

$$Gain \qquad Lead-lag \qquad Dead time$$

Gain

$$G_{ff}(s) = K_{ff} \frac{T_{ld}s + 1}{T_{lg}s + 1} e^{-\theta_{ff}s}$$

Lead-lag

 $= (T_{ld}s+1)/T_{lg}s+1)$

FF controller gain

 $= K_{ff} = - K_d/K_p$

controller dead time

 $=\theta_{\rm ff}=\theta_{\rm d}$ - $\theta_{\rm p}$ ≥ 0

Lead time

 $=T_{ld}=\tau_{p}$

Lag time

 $=T_{lg}= au_d$



How do we get values for these parameters?

$$G_{ff}(s) = K_{ff} \frac{T_{ld}s + 1}{T_{lg}s + 1} e^{-\theta_{ff}s}$$

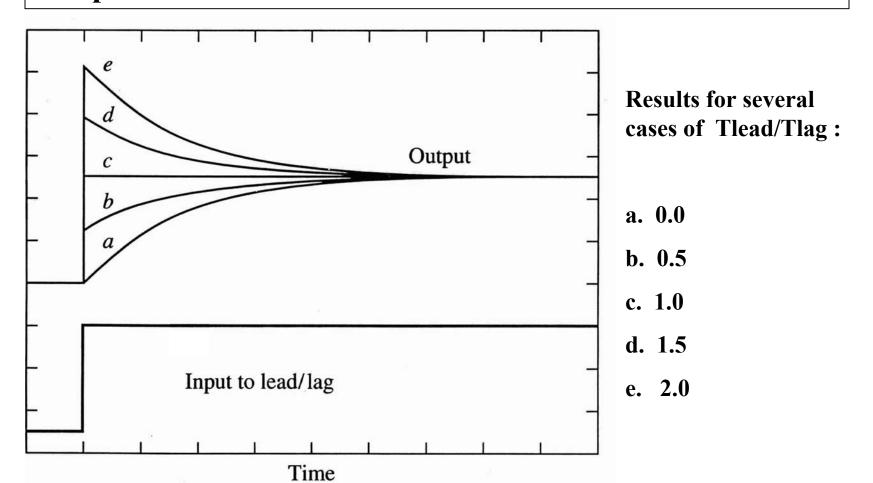
$$(MV_{ff})_{N} = \frac{T_{lg} / \Delta t}{T_{lg} / \Delta t + 1} (MV_{ff})_{N-1} + K_{ff} \left(\frac{T_{ld} / \Delta t + 1}{T_{lg} / \Delta t + 1}\right) (D_{m})_{N-\Gamma}$$
$$-K_{ff} \left(\frac{T_{ld} / \Delta t}{T_{lg} / \Delta t + 1}\right) (D_{m})_{N-\Gamma-1}$$

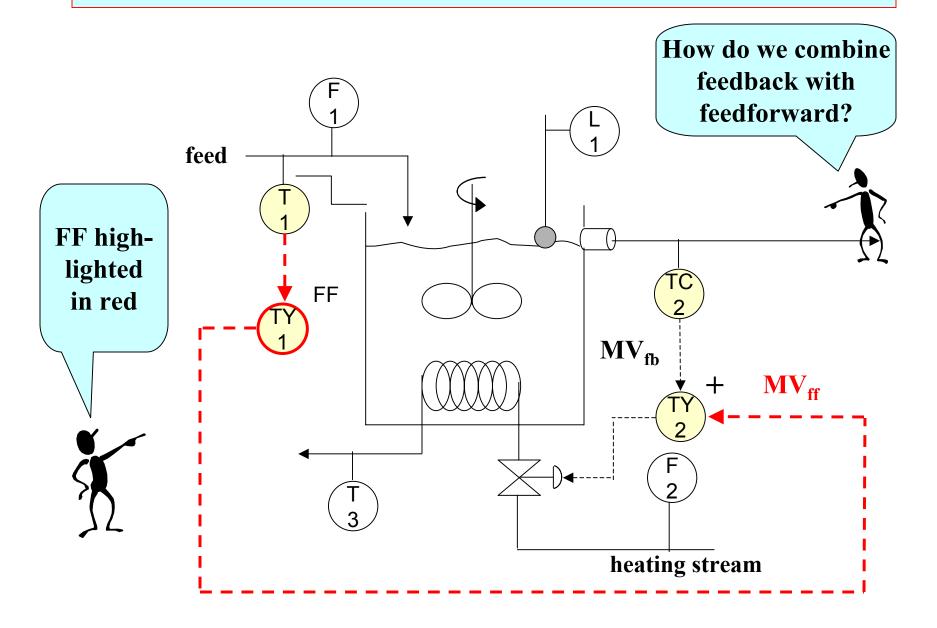
$$(MV_{ff})_N = a(MV_{ff})_{N-1} + b(D_m)_{N-\Gamma} + c(D_m)_{N-\Gamma-1}$$



Digital implementation is straightforward. Its derived in textbook.

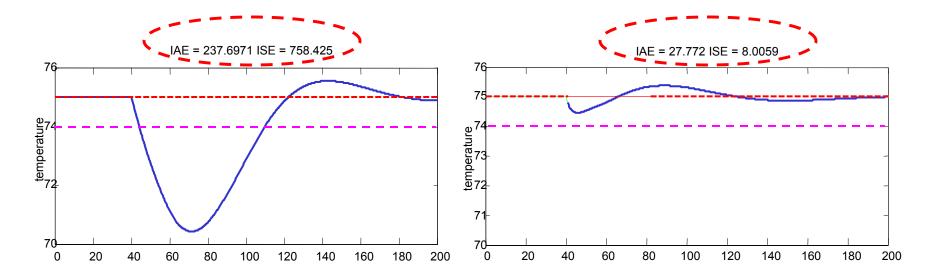
Typical dynamic responses from the lead-lag element in the feedforward controller. It synchronizes the compensation and disturbance effects.



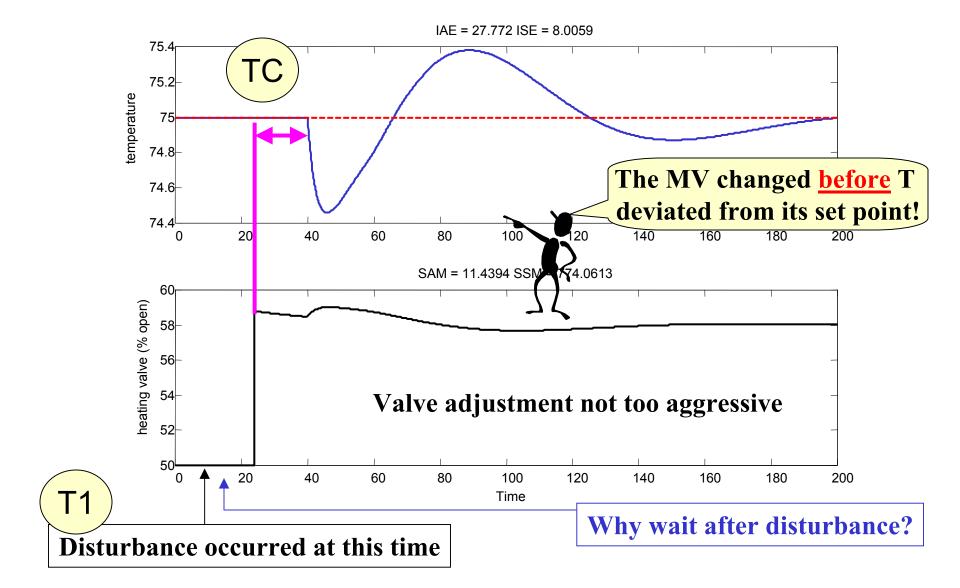


Control Performance Comparison for CST Heater

Single-Loop Feedforward with feedback

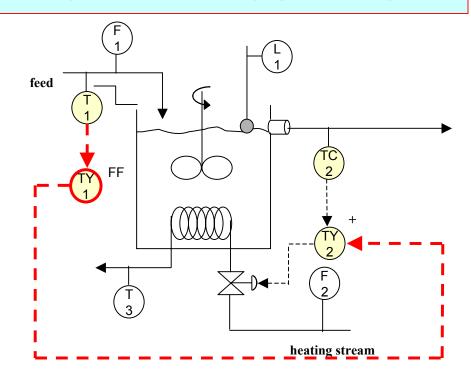


Much better performance! WHY?



What have we gained and lost using feedforward and feedback?

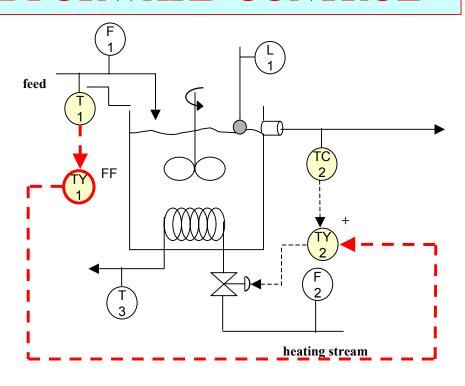
For each case, is FF with FB better, same, worse than single-loop feedback (TC2 \rightarrow v)??



- A disturbance in feed inlet temperature
- A disturbance in heating medium inlet pressure
- A disturbance in feed flow rate
- A change to the TC set point

What have we gained and lost using feedforward and feedback?

For each case, is FF and FB better, same, worse than single-loop feedback (TC2 \rightarrow v)??



• A disturbance in feed inlet temperature

FF/FB better

A disturbance in heating medium inlet pressure

Both the same

A disturbance in feed flow rate

Both the same

A change to the TC set point

Both the same

FEEDFORWARD DESIGN CRITERIA

Feedforward is desired when

- 1. Single-loop performance unacceptable
- 2. A measured variable is available

A measured disturbance variable must

- 3. Indicate the occurrence of an important disturbance
- 4. **NOT** have a causal relationship from valve to measured disturbance sensor
- 5. Not have a much faster affect on the CV than the MV (when combined with feedback)

Feedforward and Feedback are complementary

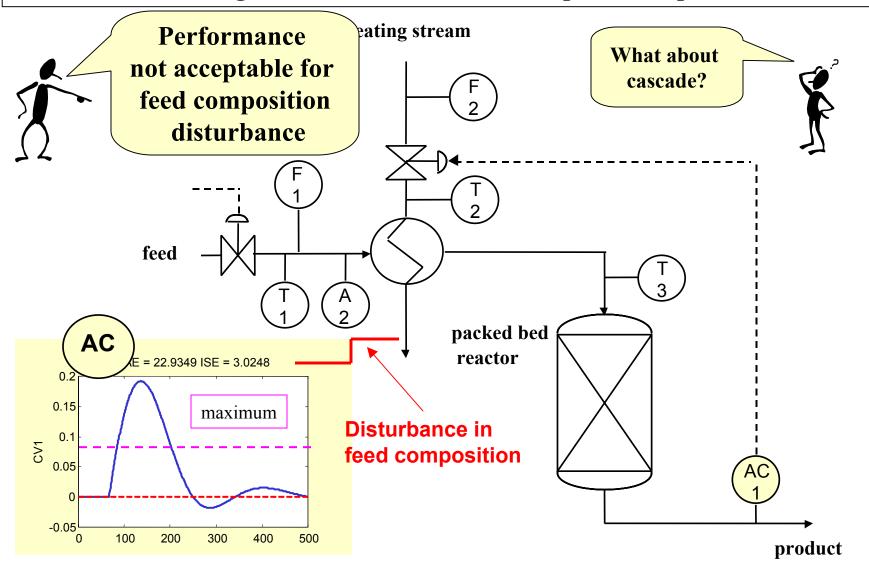
	Feedforward	Feedback
Advantages	 Compensates for disturbance before CV is affected Does not affect the stability of the control sysytem (if G_{ff}(s) stable) 	 Provides zero steady- state offset Effective for all disturbances
Disadvantages	 Cannot eliminate steady- state offset Requires a sensor and model for each disturbance 	 Does not take control action until the CV deviates from its set point Affects the stability of the control system

CLASS EXERCISE: SOME QUESTIONS ABOUT FEEDFORWARD CONTROL

- Why do we retain the feedback controller?
- When would feedforward give zero steady-state offset?
- Why does the feedforward controller sometimes delay its compensation? Don't we always want fast control?
- What is the additional cost for feedforward control?
- How can we design a strategy that has two controllers both adjusting the same valve?
- What procedure is used for tuning feedforward control?

heating stream Discuss this packed bed reactor. packed bed reactor Notes: 1. Al measures reactant concentration 2. "Circle" is shell & tube heat exchanger 3. Feed valve is adjusted by upstream process product 4. Increasing temperature increases reaction rate

Class exercise: Design feedforward control to improve the performance.



Class exercise: Design feedforward control to improve the performance.

Feedforward design criteria	A2	F 1	F2	T1	T2	T3
1. Single-loop not acceptable						
2. Disturbance variable is						
measured						
3. Indicates a key disturbance						
4. No Causal relationship, valve \rightarrow						
$\overline{\mathbf{D}_{\mathbf{m}}}$						
5. Disturbance dynamics <u>not</u>						
much faster than compensation						

Let's use the feedforward design rules!

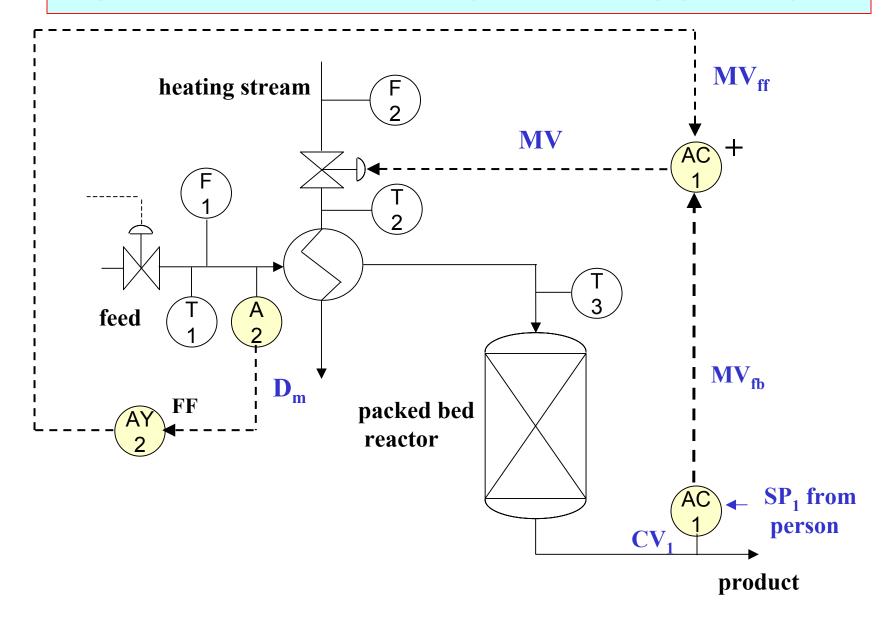


Remember: The disturbance is the feed composition.

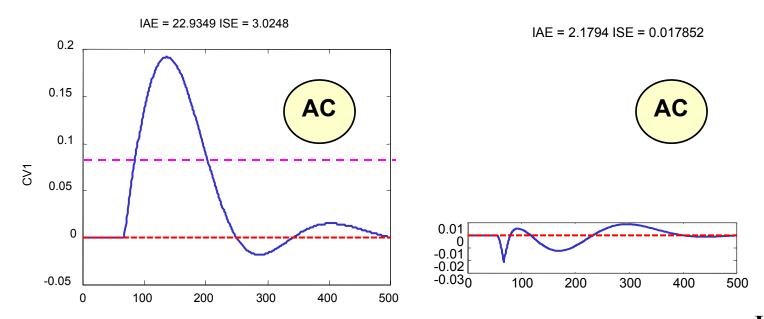
Class exercise: Design feedforward control to improve the performance.

		•				
Feedforward design criteria		F 1	F2	T1	T2	T3
1. Single-loop not acceptable		Y	Y	Y	Y	Y
2. Disturbance variable is measured		Y	Y	Y	Y	Y
3. Indicates a key disturbance		N	N	N	N	N
4. No Causal relationship, valve \rightarrow D _m		Y	N	Y	Y	N
5. Disturbance dynamics <u>not</u>	Y	N/A	N/A	N/A	N/A	N/A
much faster than compensation						

A2 satisfies all of the rules and can be used as a feedforward variable.



Control Performance Comparison for Packed Bed Reactor Single-Loop Feedforward and feedback



Much better performance! WHY?



Little model error, most experimental feedforward not this good!

What have we gained and lost using feedforward and feedback?

How does the system respond to the following?

A disturbance in T2

 MV_{ff} heating stream MV MV_{fb} packed bed reactor SP₁ from Both the same product

• A disturbance in heating medium inlet pressure

Both the same

A disturbance inT1

Both the same

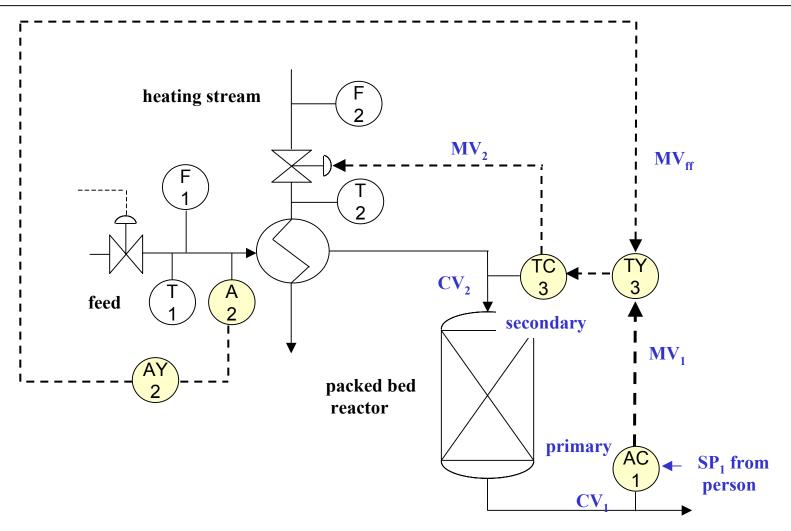
A disturbance to feed composition, A2

FF/FB better

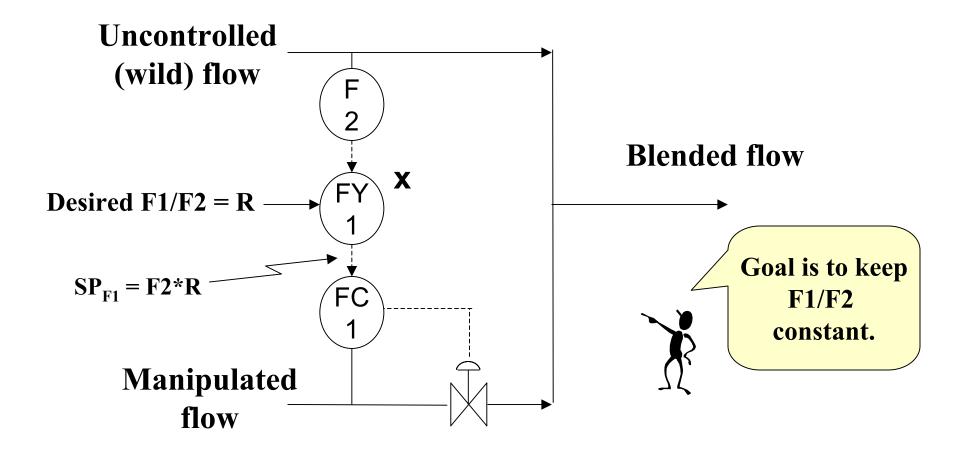
A change to the AC-1 set point

Both the same

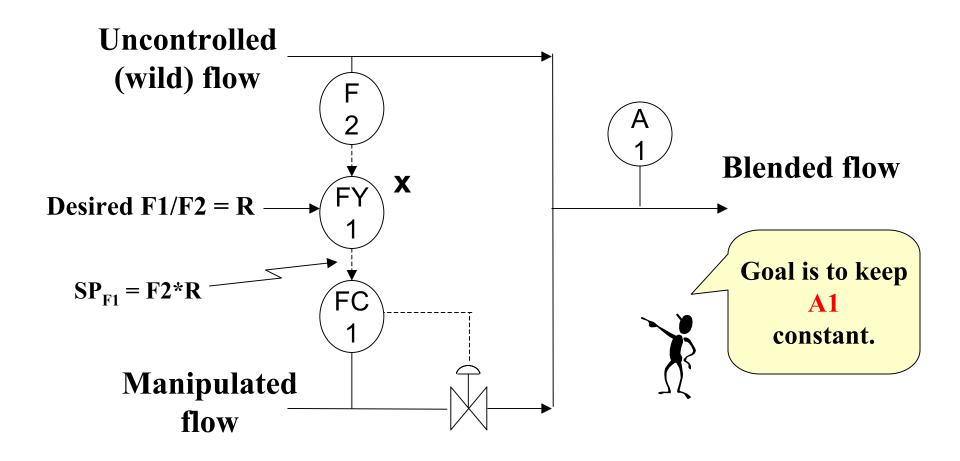
We can combine cascade and feedforward to gain the advantages of both.



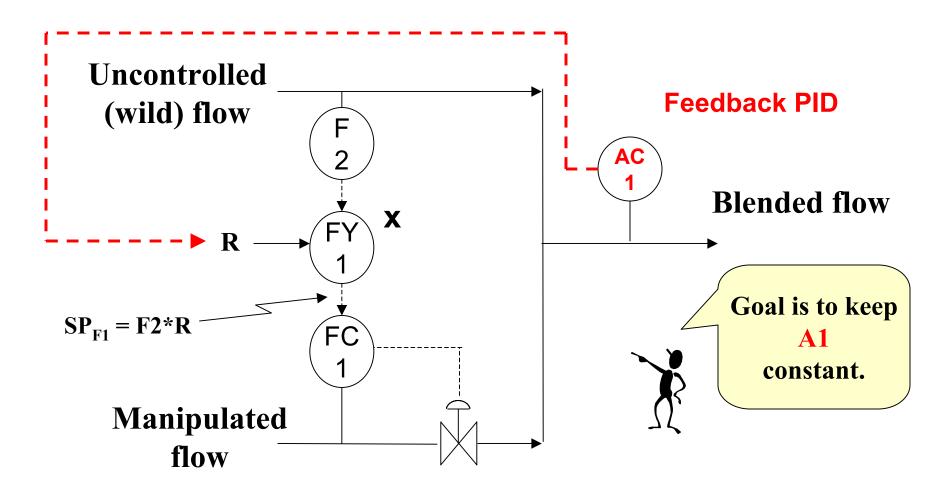
Ratio control is a simple and frequently used feedforward application. In ratio control, the dynamics are negligible.



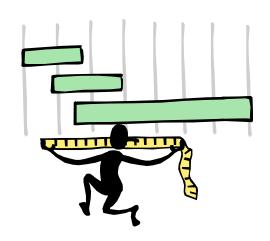
CLASS EXERCISE: Use analyzer in automatic control while retaining the good aspects of ratio control.



CLASS EXERCISE: Use analyzer in automatic control while retaining the good aspects of ratio control.



In many organizations, we take actions on inputs to prevent large disturbances to outputs. Sometimes, these are called "pre-actions".



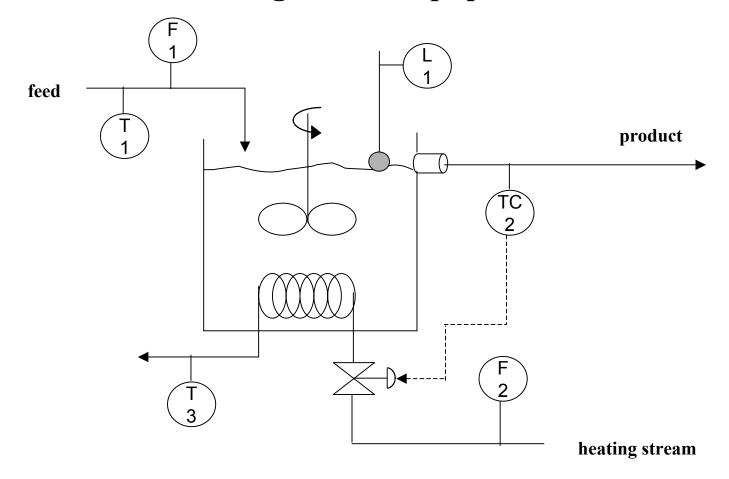
After you have measured the change, you have some time to react before it hits you

What would you do if?

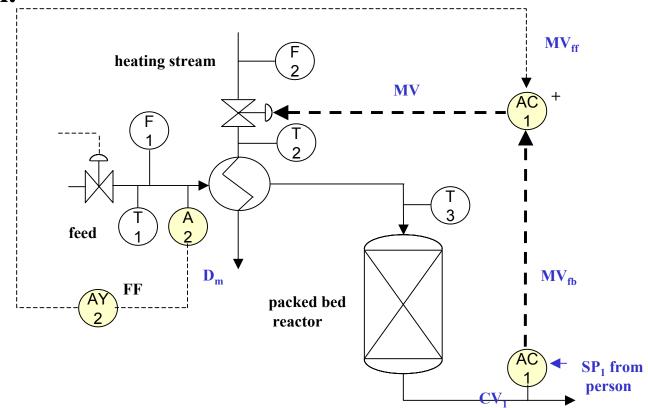
- Number of births per year increases by 10% in your country
- A drought occurs in in the most fertile area of your country
- New legislation will impose stricter emissions regulations in three years

Do we need feedback? What is your algorithm? What would you do if the measurement were noisy?

Evaluate feedforward control for a disturbance in the heating medium inlet temperature. You may add a sensor but make no other changes to the equipment.



Prepare a flowchart for the calculations performed by the packed bed feedforward controller. Show every calculation and use process variable symbols (e.g., A1), not generic symbols (CV_1). Report the equations for digital control.



Answer each of the following questions true or false

- 1. The feedback controller tuning does not change when combined with feedforward compensation.
- 2. The feedforward controller has no tuning parameter.
- 3. The feedforward controller should react immediately when the measured disturbance is measured.
- 4. Feedforward could be applied for a set point change.

Identify a process that would benefit from ratio control. You may select from examples in your summer/co-op jobs, engineering laboratories, and course projects.

Draw a sketch of the process with ratio control. Explain the advantages and any disadvantages of the design.

CHAPTER 15: FEEDFORWARD



When I complete this chapter, I want to be able to do the following.

- Identify situations for which feedforward is a good control enhancement
- Design feedforward control using the five design rules
- Apply the feedforward principle to other challenges in life



Lot's of improvement, but we need some more study!

- Read the textbook
- Review the notes, especially learning goals and workshop
- Try out the self-study suggestions
- Naturally, we'll have an assignment!

CHAPTER 15: LEARNING RESOURCES

- SITE PC-EDUCATION WEB
 - Instrumentation Notes
 - Interactive Learning Module (Chapter 15)
 - Tutorials (Chapter 15)
- The Textbook, naturally, for many more examples

CHAPTER 15: SUGGESTIONS FOR SELF-STUDY

- 1. Suggest some methods for fine-tuning a feedforward controller.
- 2. Program a feedforward controller for one of the processes modelled in Chapters 3-5.
- 3. Explain why the feedforward compensation should not be much slower than the disturbance. Why doesn't this guideline apply when no feedback is implemented?
- 4. Discuss whether you would recommend more than one feedforward controller on the same process.
- 5. Write a memorandum explaining feedforward compensation for a company with non-technical employees

CHAPTER 15: SUGGESTIONS FOR SELF-STUDY

- 6. A friend asks whether the general sketch for feedback, textbook Figure 1.4, applies to feedforward. Answer completely, including any changes to the sketch.
- 7. Discuss why the feedforward controller dead time must be positive.