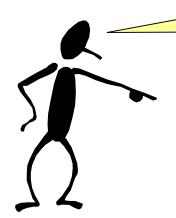


When I complete this chapter, I want to be able to do the following.

- Identify examples of analog and digital computation and signal transmission.
- Program a digital PID calculation
- Select a proper execution rate for a feedback controller.
- Tune a digital PID



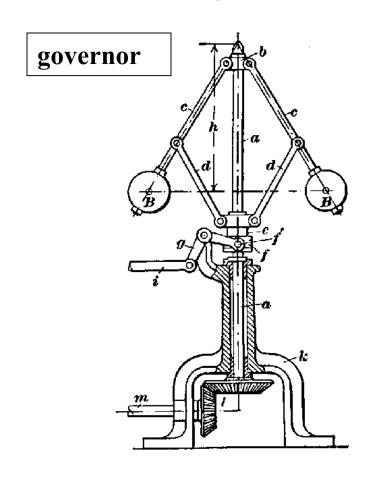
Outline of the lesson.

- Brief history of control equipment
- Sampling the measurement
- Digital PID calculation
- Effect of digital execution period on tuning and performance

A BRIEF HISTORY OF PROCESS CONTROL

- A little history helps us to understand the common approaches to process control. The realities of available equipment have shaped the theory and practice of process control.
- While digital technology has revolutionized what is possible today, equipment has a life of many decades. Therefore, we see older approaches in most plants, and will for a long time.
- Let's start from about the 19th century to today. What happened in the 19th century that "got things going"?

Making the steam engine work all the time



Inventors wanted to control the pressure of the boiler and the speed of the device driven by the steam (using a governor).

People experienced

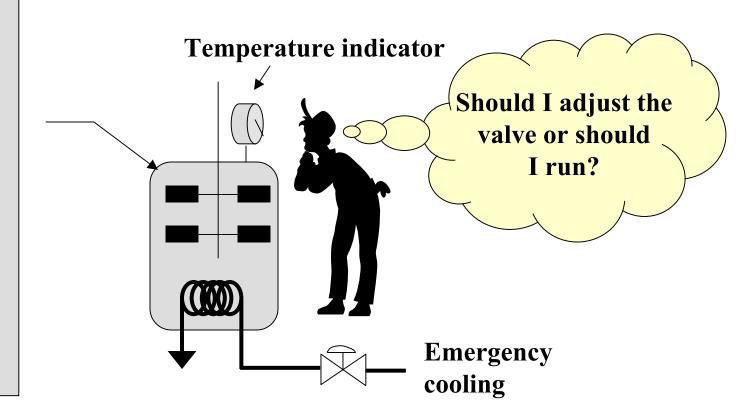
- Explosions!
- Unstable behavior

And control engineering was born!

- Manual _____operation
- Mechanical devices
- Pneumatic devices
- Electronic devices
- Digital calculations
- Digital calc. & communication

Manual Operation

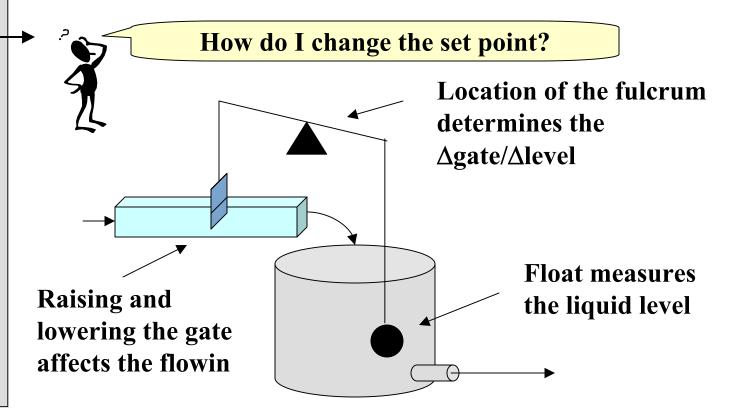
People know more than machines, so leave decisions to them.



- Manual operation
- Mechanical devices
- Pneumatic devices
- Electronic devices
- Digital calculations
- Digital calc. & communication

Mechanical Device

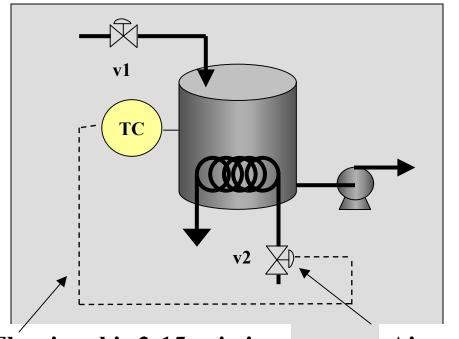
The value of the variable is represented by position of equipment.



- Manual operation
- Mechanical devices
- Pneumatic devices
- Electronic devices
- Digital calculations
- Digital calc. & communication

Pneumatic Device

The value of the variable is proportional to air pressure (50 - 150 C = 3 - 15 psi).



The signal is 3-15 psi air pressure in a pipe.

How do I perform the PID calculation?



Air pressure moves flexible diaphragm

- Manual operation
- Mechanical devices
- Pneumatic devices
- Electronic devices
- Digital calculations
- Digital calc. & communication

Pneumatic & Electronic Devices

Principle of analog computation!

$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' + T_d \frac{d E(t)}{dt} \right] + I$$

Build a physical system that (approximately) obeys the same model.

- Pneumatic force balance (Newton's laws)
- Electronic current balance (Kirkoff's laws)



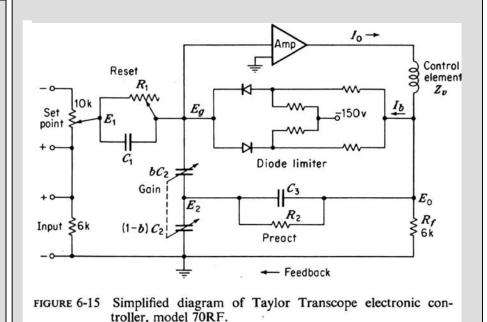
Analog computation!

$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' + T_d \frac{d E(t)}{dt} \right] + I$$

Pneumatic

Reset bellows Feedback bellows P₃ Reset valve Derivative bypass To valve FIGURE 6-9 Three-mode controller with parallel feedback.

Electronic

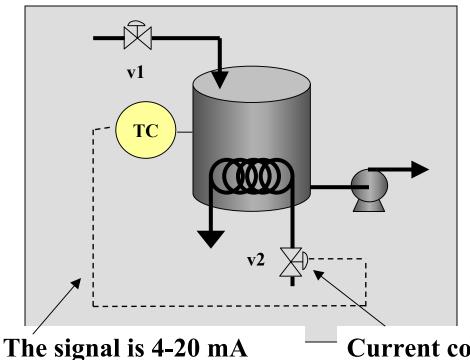


From Harriott, P., Process Control, McGraw-Hill, New York, 1964

- Manual operation
- Mechanical devices
- Pneumatic devices
- Electronic devices
- Digital calculations
- Digital calc. & communication

Electronic Device

The variable is proportional to current or voltage (50 - 150 C = 4 - 20 mA).



transmitted by wire.

Current converted to air pressure to affect valve

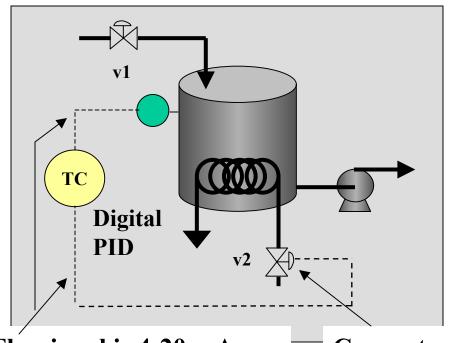
I'll use analog computation again.



- Manual operation
- Mechanical devices
- Pneumatic devices
- Electronic devices
- Digital –
 calculations
- Digital calc. & communication

Digital Calculation

Digital calculations with electronic transmission.



We'll soon see how to calculate PID digitally.

R

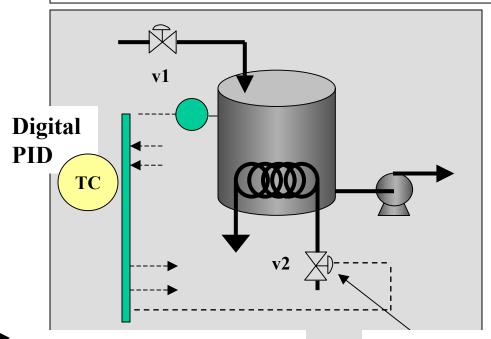
The signal is 4-20 mA transmitted by wire.

Current converted to air pressure to affect valve

- Manual operation
- Mechanical devices
- Pneumatic devices
- Electronic devices
- Digital calculations
- Digital calc. & communication

Digital Calculation & Communication

Digital calculations with transmission by local area network. Sensor and valve can have microprocessors too!



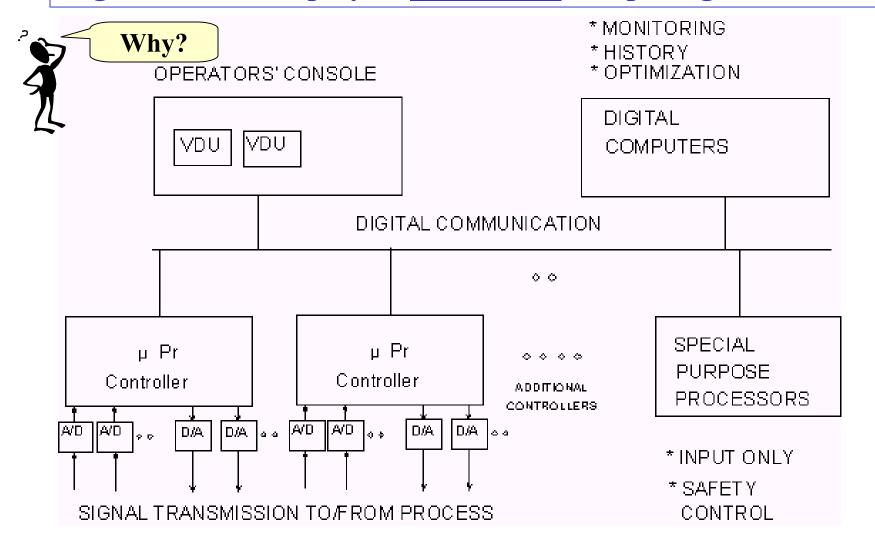
We soon see how to calculate PID digitally.



The signal transmitted digitally.

converted to air pressure to affect valve

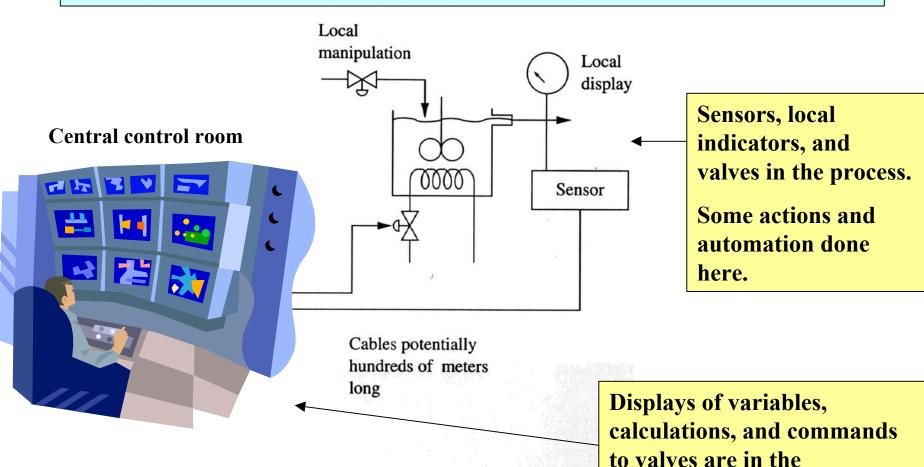
Digital control employs a <u>distributed</u> computing network



Digital control employs a <u>distributed</u> computing network

Feature	Effect on process control	
Calculations performed in parallel by numerous processors	Control calculations are performed faster than if by one processor	
Limited number of controller calculations performed by a single processor	Control system is more reliable since a processor failure affects only few control loops	
Control calculations and interfacing to process independent of other devices connected to the LAN	Control is more reliable since failure of other devices does not immediately affect a control processor	
Small amount of equipment required for the minimum system	Only the equipment required must be purchased, and the system is easily expanded at low cost	
Each type of processor can have different hardware and software	Hardware and software can be tailored to specific applications like control, monitoring, operator console, and general data processing	

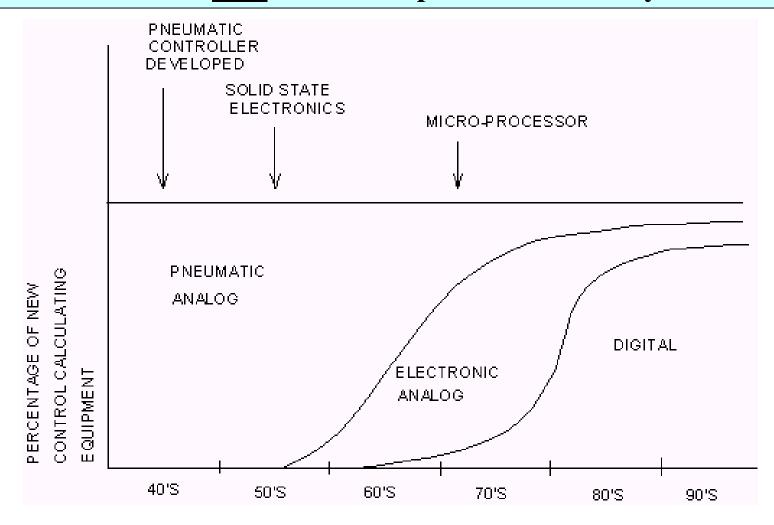
Let's remember that control is performed many places; locally and remotely by people and equipment.



centralized control center.

FIGURE 1.6

A rough indication of the use of various devices for control calculations for <u>new</u> industrial process control systems.

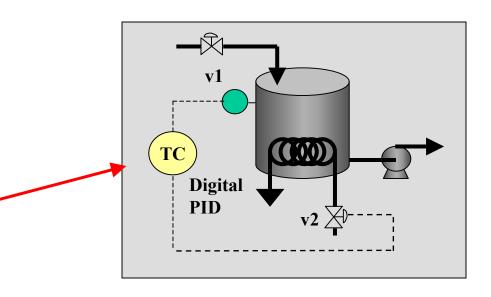


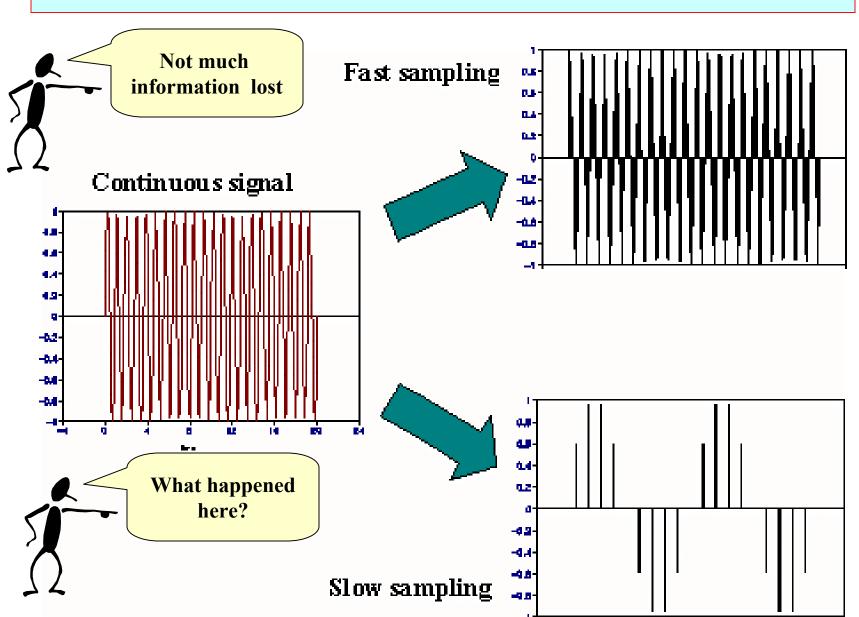
- Manual operation
- Mechanical devices
- Pneumatic devices
- Electronic devices
- Digital calculations
- Digital calc. & communication

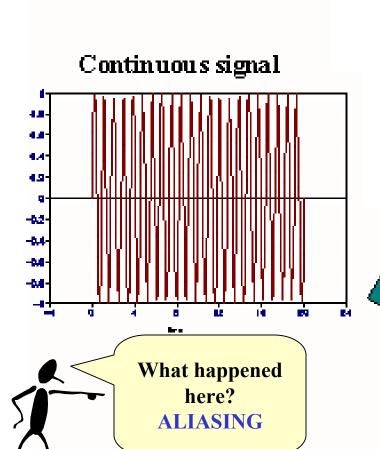
The techniques presented will be applicable for digital sampling and calculation.

Transmission can be electronic or digital.

Periodically, the measurement is sampled and a calculation is performed.

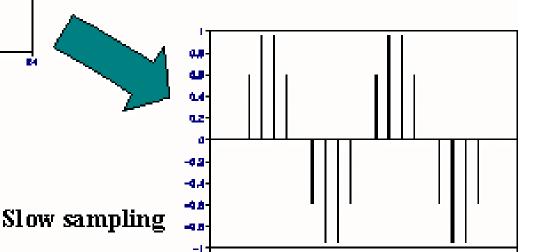




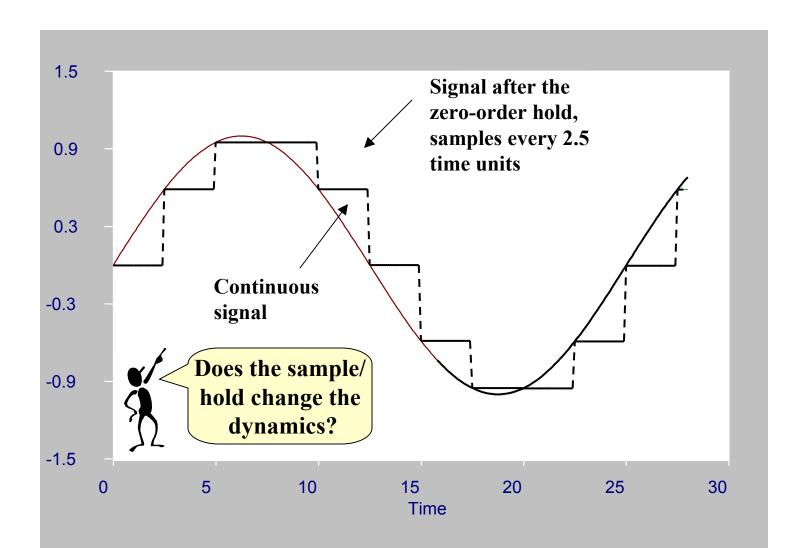


Aliasing: Sampling much slower than the measurement changes causes significant loss of information.

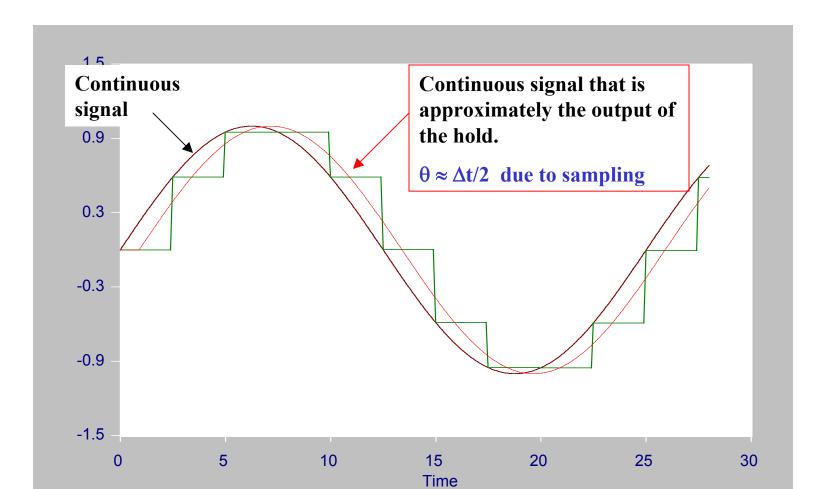
Engineer should design for sampling "fast enough".



We "hold" the last sampled value between control executions.



The red line is the continuous approximation of the signal after the sample & hold. This shows that the effect is to introduce a "dead time" of about $\Delta t/2$.



$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' - T_d \frac{dCV(t)}{dt} \right] + I$$

We have a sample of values; CV_1 , CV_2 ,, CV_N

Proportional:

Integral:



Hint: How would you estimate each mode using numerical methods?

$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' - T_d \frac{dCV(t)}{dt} \right] + I$$

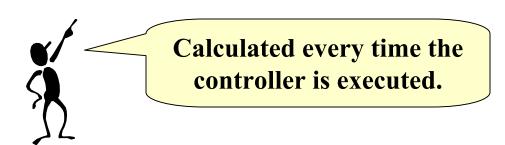
We have a sample of values; CV_1 , CV_2 ,, CV_N

Proportional:

$$E_N = SP_N - CV_N$$

 $(MV_N)_{proportional} = K_C E_N$

Integral:



$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' - T_d \frac{d CV(t)}{dt} \right] + I$$

We have a sample of values; CV_1 , CV_2 ,, CV_N

Proportional:

$$E_N = SP_N - CV_N$$

$$(MV_N)_{integral} = \frac{K_C(\Delta t)}{T_I} \sum_{i=1}^N E_i$$

Integral:



Calculated every time the controller is executed.

- $\Delta t = constant$
- How many elements in sum?

$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' - T_d \frac{dCV(t)}{dt} \right] + I$$

We have a sample of values; CV_1 , CV_2 ,, CV_N

Proportional:

$$E_{N} = SP_{N} - CV_{N}$$

$$SUM_{N} = SUM_{N-1} + E_{N}$$

Integral:

$$(MV_N)_{integral} = \frac{K_C(\Delta t)}{T_I} (SUM_N)$$



Efficient calculation in realtime!

$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' - T_d \frac{dCV(t)}{dt} \right] + I$$

We have a sample of values; CV_1 , CV_2 ,, CV_N

Proportional:

$$(MV_N)_{derivative} = -K_C T_d \frac{(CV_N - CV_{N-1})}{\Delta t}$$



Calculated every time the controller is executed.

$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' - T_d \frac{dCV(t)}{dt} \right] + I$$

We have a sample of values; CV_1 , CV_2 ,, CV_N

$$I = MV_1 - K_c \left[E_1 - T_d \frac{(CV_1 - CV_0)}{\Delta t} \right]$$

"I" is sometimes called the bias.



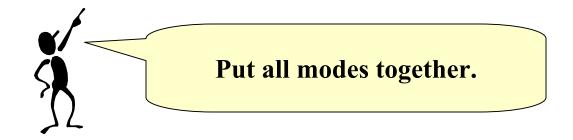
Calculated only when the controller is turned on, N=1.
Thereafter, I is constant

Bumpless transfer:No change to the MV when controller is first executed

$$MV(t) = K_c \left[E(t) + \frac{1}{T_I} \int_0^t E(t') dt' - T_d \frac{d CV(t)}{dt} \right] + I$$

Digital PID, positional form calculates the output to the final element

$$MV_N = K_c \left[E_N + \frac{\Delta t}{T_I} \sum_{i=1}^N E_i - \frac{T_d}{\Delta t} (CV_N - CV_{N-1}) \right] + I$$



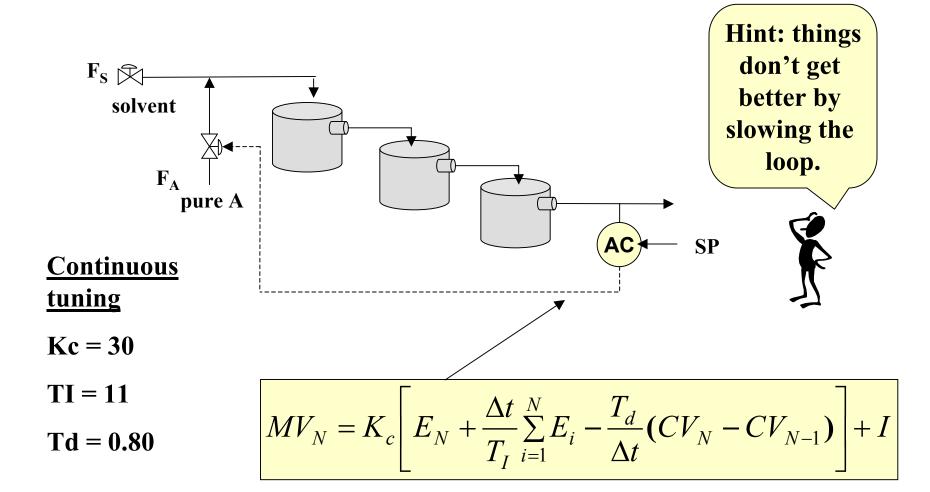
$$MV_N = K_c \left[E_N + \frac{\Delta t}{T_I} \sum_{i=1}^N E_i - \frac{T_d}{\Delta t} (CV_N - CV_{N-1}) \right] + I$$

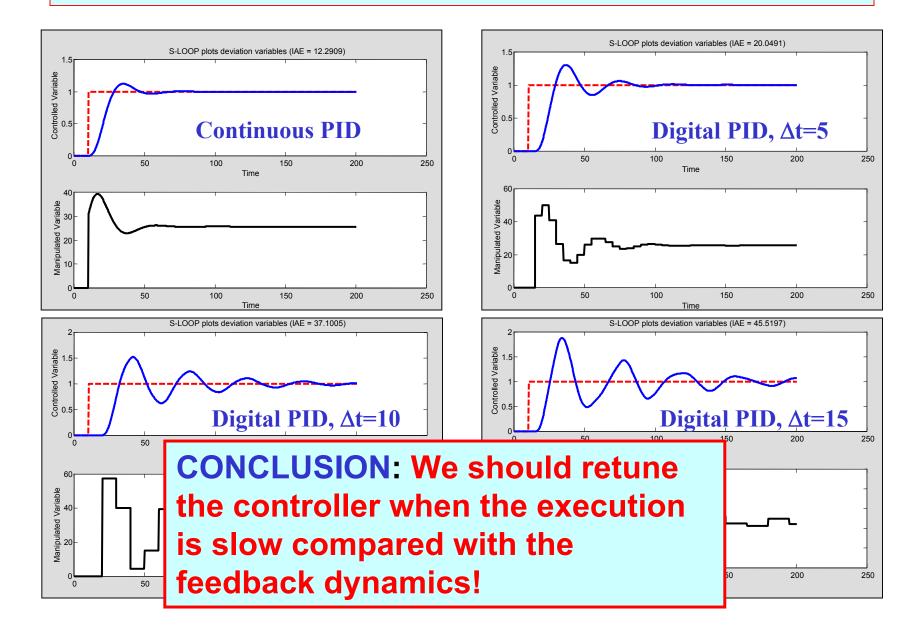
Digital PID, Velocity form - Alternatively, we can calculate the <u>change</u> in the signal at every execution.

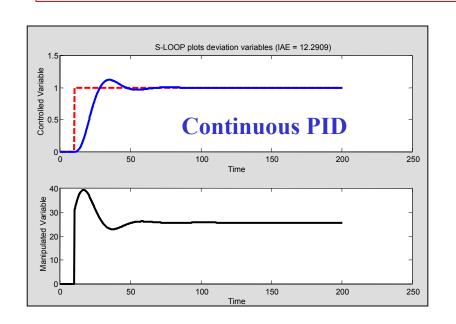
$$\Delta MV_N = K_c \left[E_N - E_{N-1} + \frac{(\Delta t)}{T_I} E_N - \frac{T_d}{\Delta t} (CV_N - 2CV_{N-1} + CV_{N-2}) \right]$$

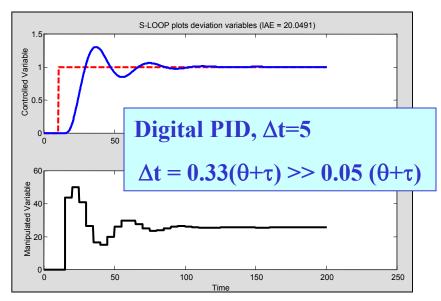
$$MV_N = MV_{N-1} + \Delta MV_N$$

What is the effect of digital execution of the PID controller on tuning and performance?









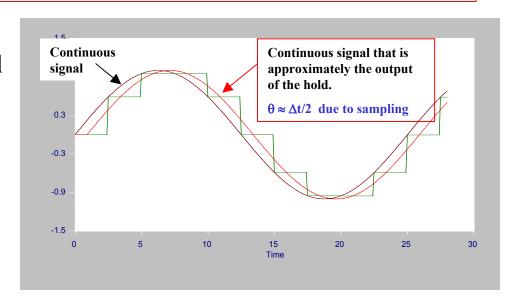
Guideline for selecting the execution time:

To prevent degradation of control loop performance, select a controller execution time of $\Delta t \leq 0.05(\theta+\tau)$.

Note: Typical sample period for chemical process control is 1/3-1/2 second. Much faster is possible, if needed.

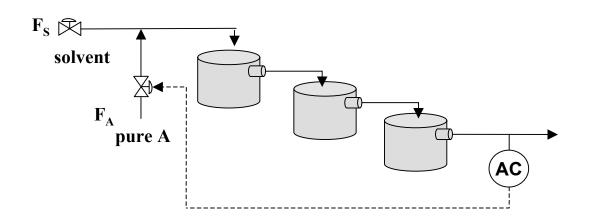
Modified PID tuning for digital controllers - this is a guideline that usually works adequately.

We learned that sampling introduces an additional dead time of about $\Delta t/2$.



- 1. Obtain model, usually using empirical method
- 2. Determine the sample period, $\Delta t \leq 0.05(\theta + \tau)$, if possible
- 3. Recalculate the dead time as $\theta' = \theta + \Delta t/2$
- 4. Calculate tuning using continuous method
- 5. Implement and fine tune as needed

Let's apply this guideline for the three-tank mixer with a long sample time = 15 minutes.



Process reaction curve

$$Kp = 0.039 \% A/\% open$$

$$\theta = 5.5 + ?? = ?? \min$$

$$\tau = 10.5 \text{ min}$$

Tuning from chart

$$Kc = ??$$

$$TI = ??$$

$$Td = ??$$

The performance is about as good as possible with this very long sampling time! Would you fine tune further?

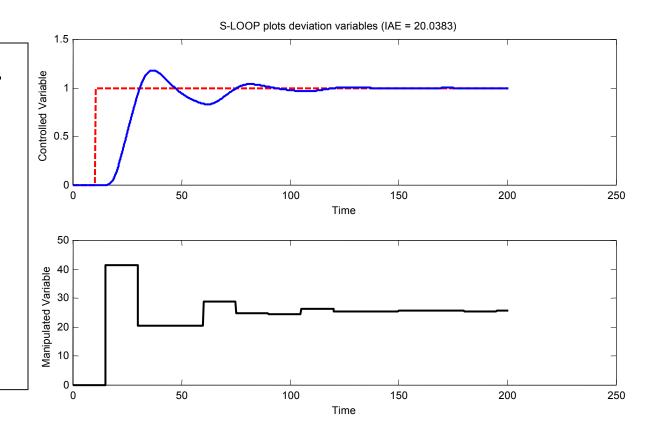
Tuning from chart

$$Kc = 20$$

$$TI = 14$$

$$Td = 2.35$$

IAE increased from 12.2 to 20+



If the PID is no better in digital form, why did we spend decades of engineering time and billions of dollars converting the world's control to digital?

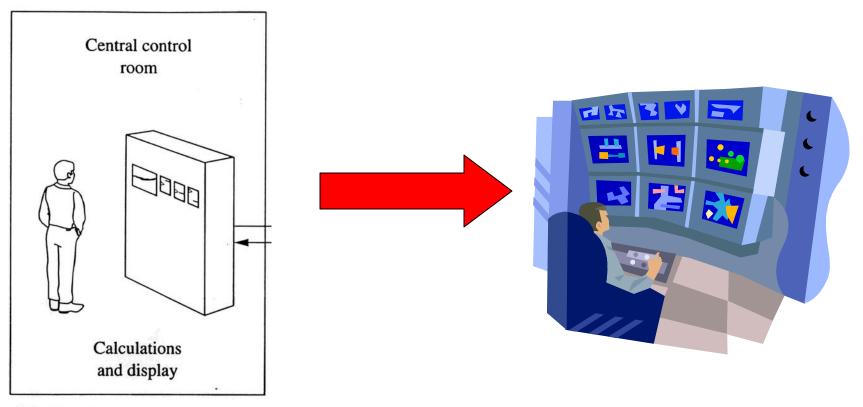
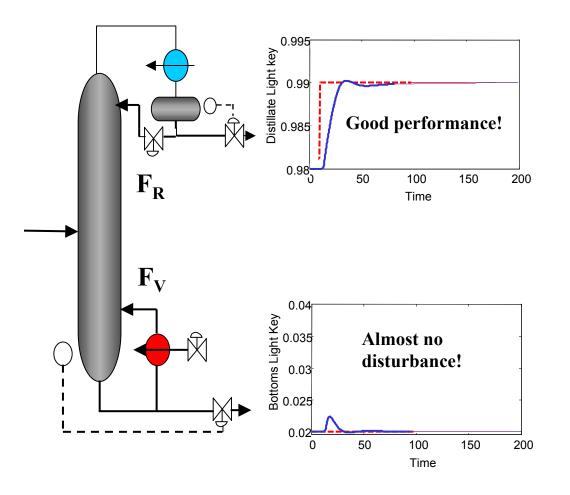


FIGURE 1.6

Why did we convert the world's control to digital - Complex controllers





Improved
performance can
be achieved with
algorithms that
optimize the path
to the set point,
every controller
execution!

(See Chapters 19 and 23)

Why did we convert the world's control to digital - Process monitoring

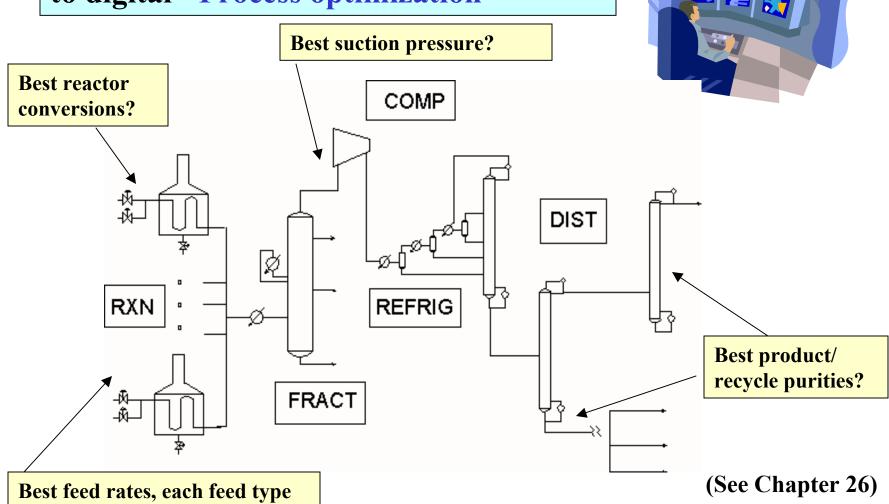


We have a digital history of measurements for

- Recall at any time for trouble shooting
- Calculation of process performance indicators, heat transfer coefficients, reactor yields, energy/kg of product, and so forth
- Excellent graphical displays with data in context of process schematic

(See Chapter 26)

Why did we convert the world's control to digital - Process optimization



Why did we convert the world's control to digital -Diagnostics



We have digital monitors at sensor, controller and valve!

- Compare signal to valve with actual valve position report significant errors
- Diagnose problems with sensor (voltage, etc.)
- Do not take feedback control action on questionable loop - alarm operator

And many other reasons that digital is a winner.



CHAPTER 11: DIGITAL CONTROL, WORKSHOP 1

- 1. Select all of the appropriate answers. Mechanical implementation of feedback control employs
 - a. Digital computation
 - b. Analog computation
 - c. Neither a nor b
 - d. Both a and b
- 2. A digital PID controller is operating "in automatic", i.e., it is calculating the signal to the final element. You are fine tuning the loop. You change the controller gain by -30% of its original value.

Describe what happens.

CHAPTER 11: DIGITAL CONTROL, WORKSHOP 2

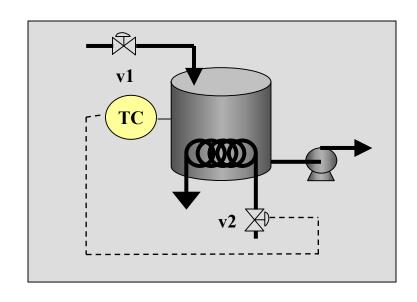
You are tuning the temperature controller shown in the figure. You have determined the dynamic model below.

Determine the PID tuning for this loop for execution periods below and simulate the results using S_LOOP.

$$\Delta t = 0.10$$

$$\Delta t = 1.0$$

$$\Delta t = 5.0$$



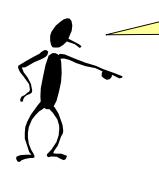
$$G_P(s) = \frac{T(s)}{v_2(s)} = \frac{-.53e^{-0.20 s}}{10 s + 1}$$

(All times are in minutes.)

CHAPTER 11: DIGITAL CONTROL, WORKSHOP 3

Develop a table with advantages and disadvantages for the six control equipment categories for many important issues.

	reliability	speed	Many more!!
Manual operation			
Mechanical devices			
Pneumatic devices			
Electronic devices			
Digital calculations			
Digital calcs. & communication			



When I complete this chapter, I want to be able to do the following.

- Identify examples of analog and digital computation and signal transmission.
- Program a digital PID calculation
- Select a proper execution rate for a feedback controller.
- Tune a digital PID



Lot's of improvement, but we need some more study!

- Read the textbook
- Review the notes, especially learning goals and workshop
- Try out the self-study suggestions
- Naturally, we'll have an assignment!

CHAPTER 11: LEARNING RESOURCES

SITE PC-EDUCATION WEB

- Instrumentation Notes
- Interactive Learning Module (Chapter 11)
- Tutorials (Chapter 11)
- Software Laboratory, S_LOOP
 - You can simulate a PID loop with continuous of digital control to determine the effect of execution period.

CHAPTER 11: SUGGESTIONS FOR SELF-STUDY

- 1. Find some process reaction curve plots in Chapters 3-5. Determine the maximum PID execution period. Then, for a controller execution period ten times the minimum, determine the tuning for PID and PI controllers using the tuning charts.
- 2. Using S_LOOP, simulate the system(s) in question 1.
- 3. Develop a flowchart for an excellent computer program to calculate the PID control. This should be a subroutine that can be called for every controller in the plant.

CHAPTER 11: SUGGESTIONS FOR SELF-STUDY

- 4. Take an inventory of your house and identify analog and digital control systems.
- 5. Develop a simulation that accepts a continuous signal and determines the output of a zero-order hold and first-order hold.