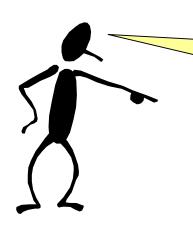
CHAPTER 6: EMPIRICAL MODEL IDENTIFICATION

When I complete this chapter, I want to be able to do the following.

- Design and implement a good experiment
- Perform the graphical calculations
- Perform the statistical calculations
- Combine fundamental and empirical modelling for chemical process systems

CHAPTER 6: EMPIRICAL MODEL IDENTIFICATION



Outline of the lesson.

- Experimental design for model building
- Process reaction curve (graphical)
- Statistical parameter estimation
- Workshop

CHAPTER 6: EMPIRICAL MODELLING

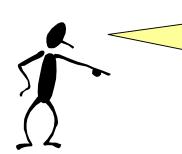


We have invested a lot of effort to learn fundamental modelling. Why are we now learning about an empirical approach?

TRUE/FALSE QUESTIONS

- We have all <u>data</u> needed to develop a fundamental model of a complex process
- We have the <u>time</u> to develop a fundamental model of a complex process
- Experiments are <u>easy</u> to perform in a chemical process
- We need <u>very</u> accurate models for control engineering

CHAPTER 6: EMPIRICAL MODELLING



We have invested a lot of effort to learn fundamental modelling. Why are we now learning about an empirical approach?

TRUE/FALSE QUESTIONS

false

We have all <u>data</u> needed to develop a fundamental model of a complex process

false

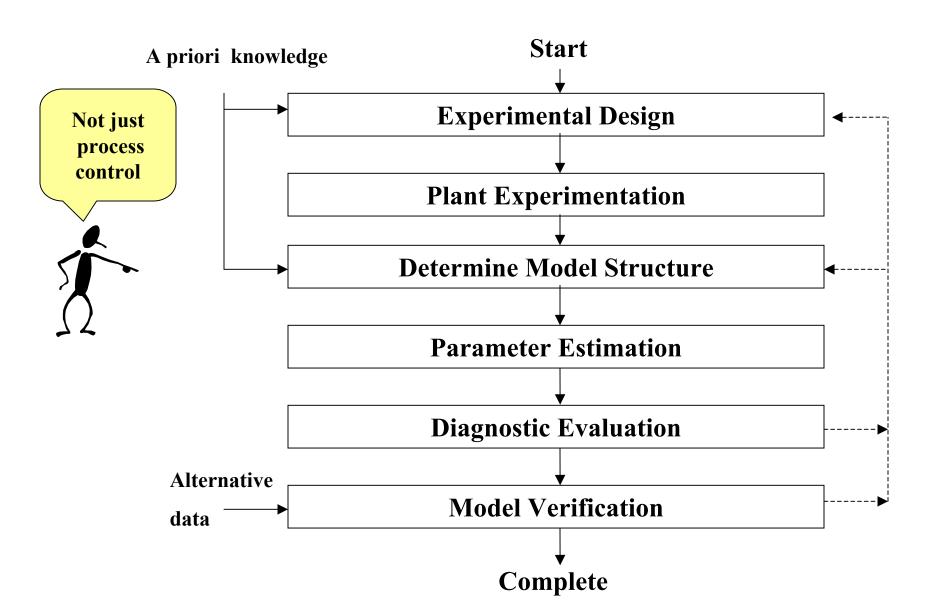
We have the <u>time</u> to develop a fundamental model of a complex process

false

Experiments are **easy** to perform in a chemical process

false

We need very accurate models for control engineering



Looks very general; it is!
However, we still need to understand the process!

Plant Experimentation

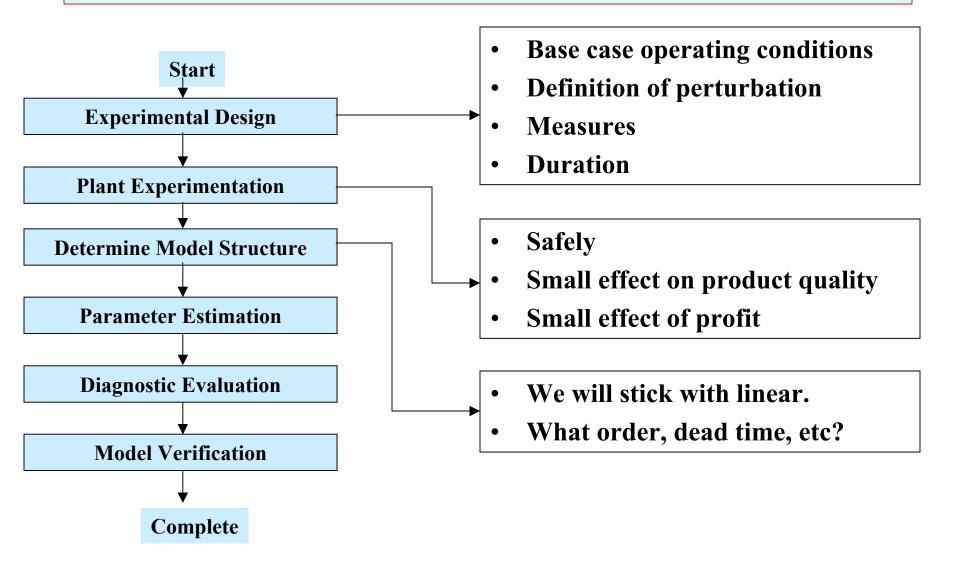
Parameter Estimation

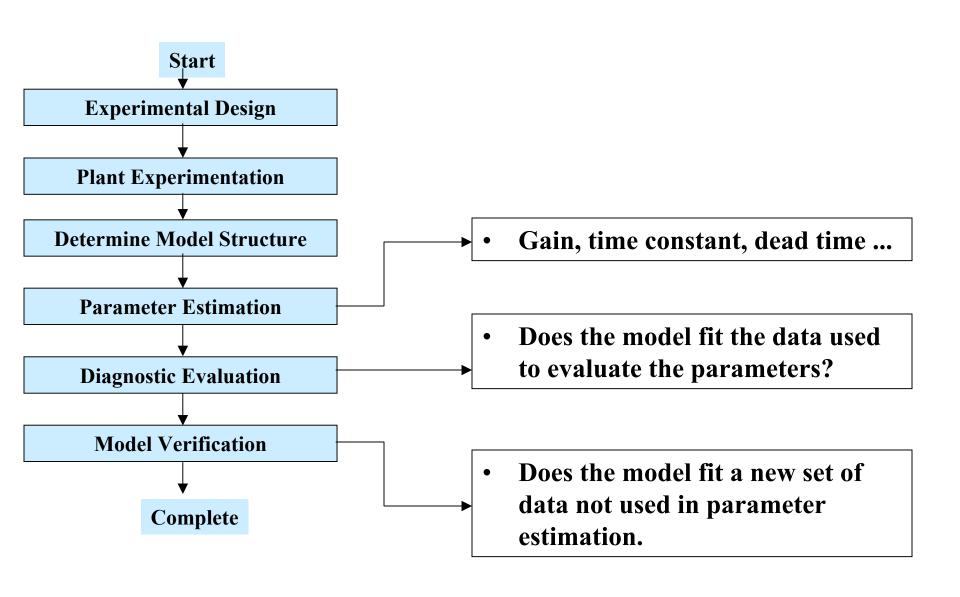
Diagnostic Evaluation

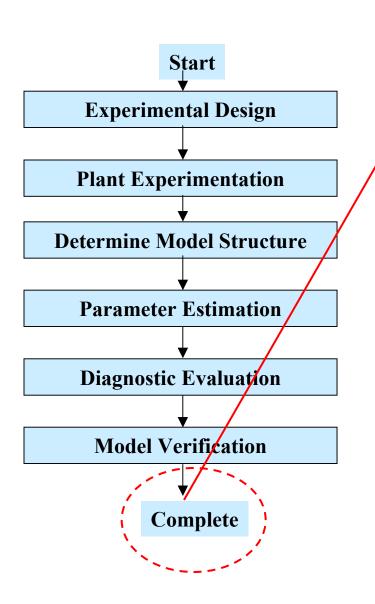
Model Verification

Complete

- Changing the temperature 10 K in a ethane pyrolysis reactor is allowed.
- Changing the temperature in a bio-reactor could kill micro-organisms







What is our goal?

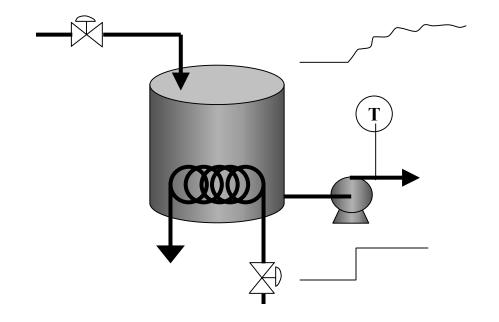
We seek models good enough for control design, controller tuning, and process design.

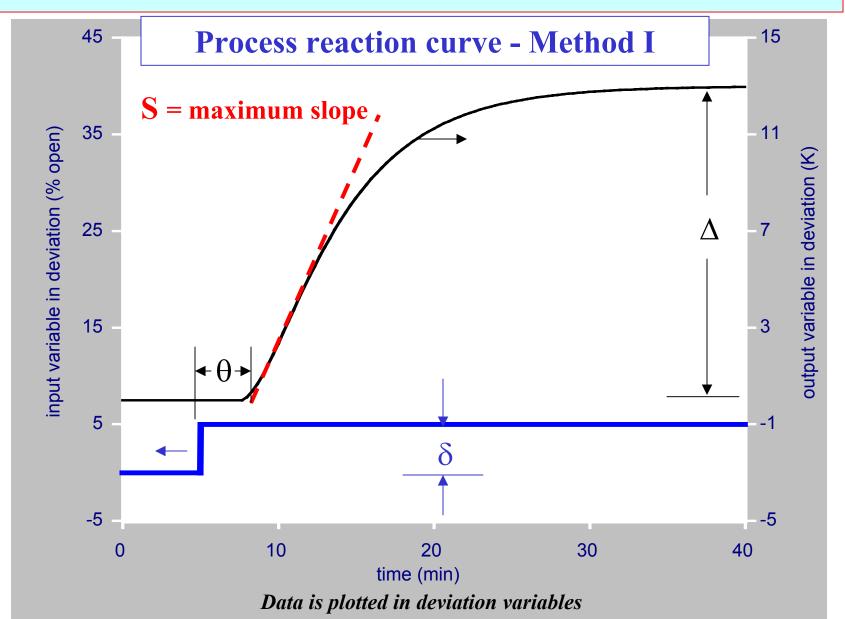
How do we know?

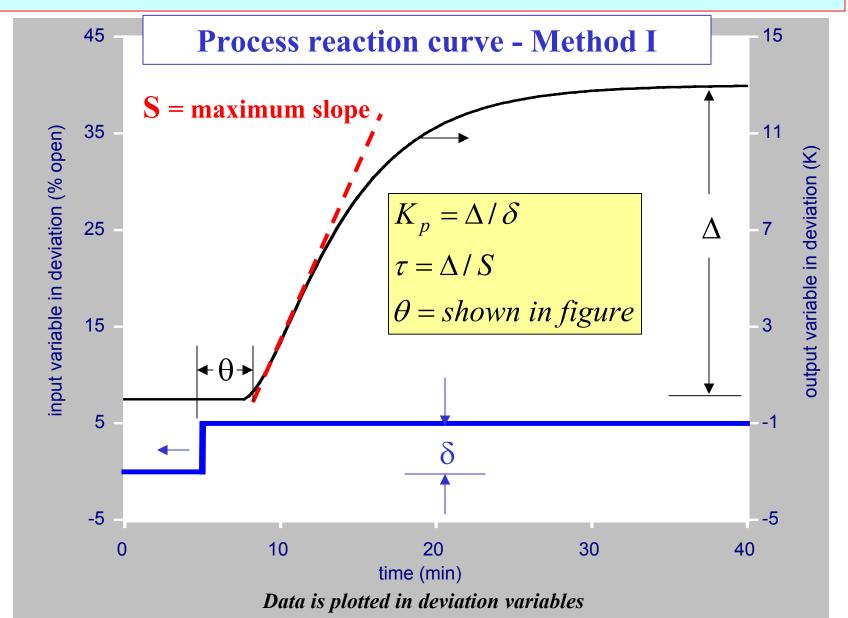
We'll have to trust the book and instructor for now. But, we will check often in the future!

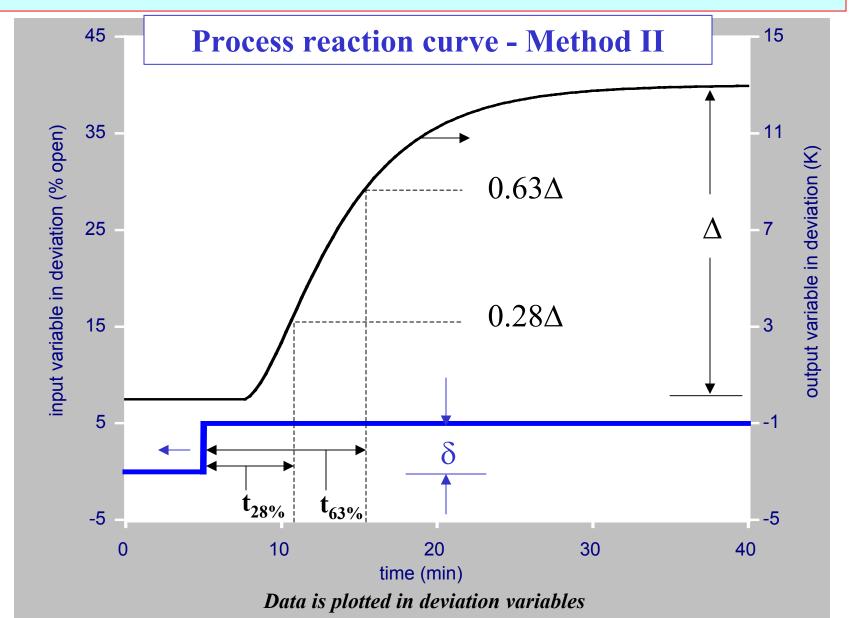
Process reaction curve - The simplest and most often used method. Gives nice visual interpretation as well.

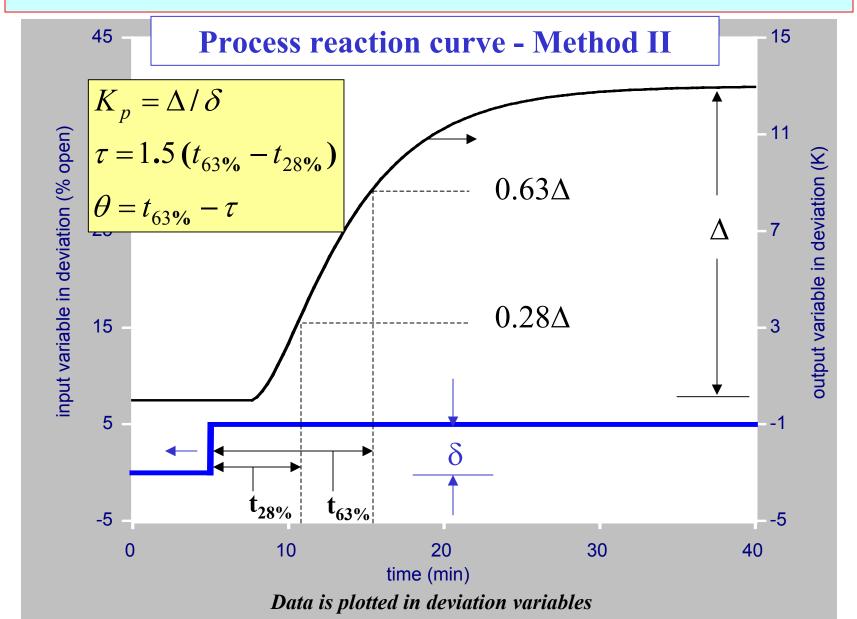
- 1. Start at steady state
- 2. Single step to input
- 3. Collect data until steady state
- 4. Perform calculations

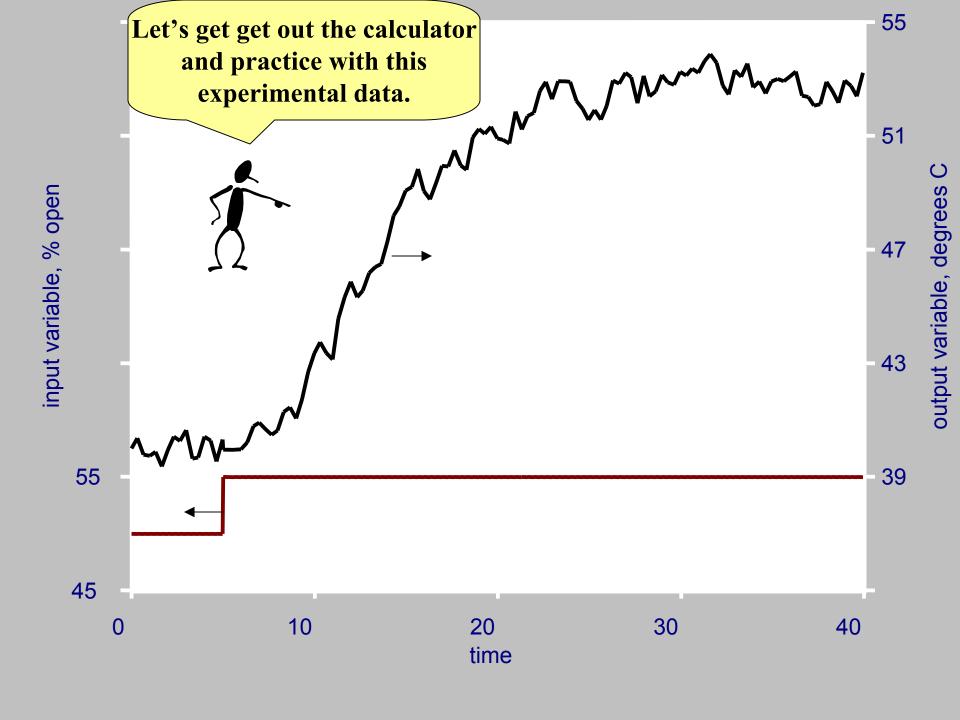












Process reaction curve - Methods I and II

The same experiment in either method!

Method I

- Developed first
- Prone to errors because of evaluation of maximum slope

Method II

- Developed in 1960's
- Simple calculations

Process reaction curve - Methods I and II

The same experiment in either method!

Method I

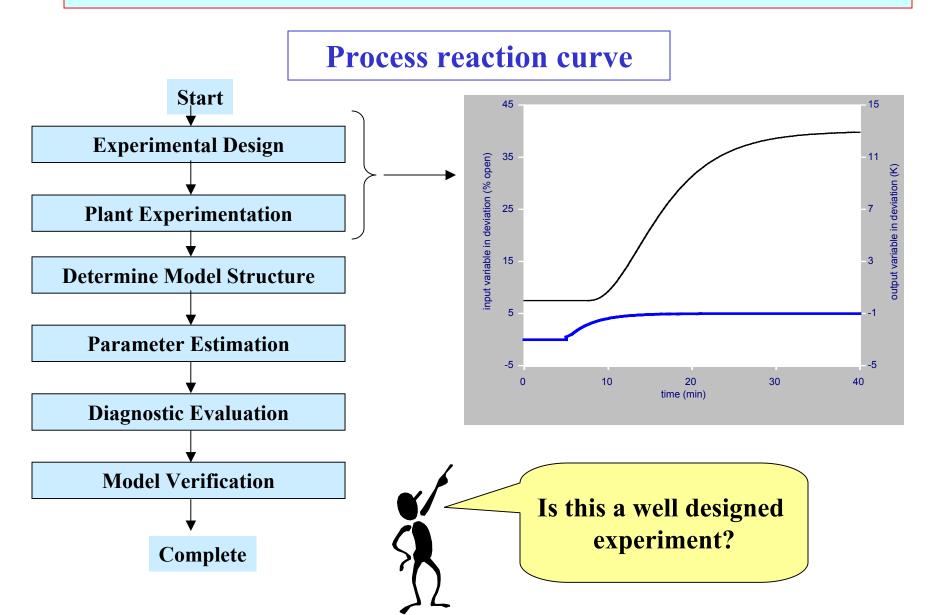
- Developed first
- Prone to errors because of evaluation of maximum slope

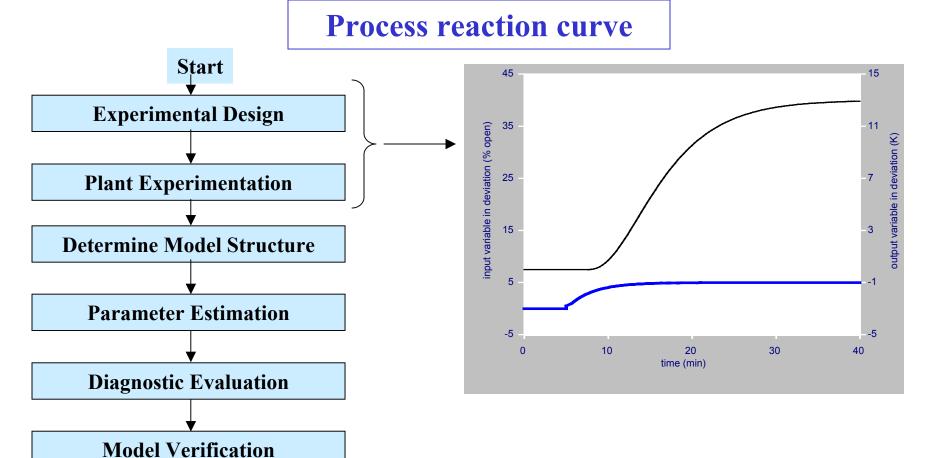
Method II

- Developed in 1960's
- Simple calculations

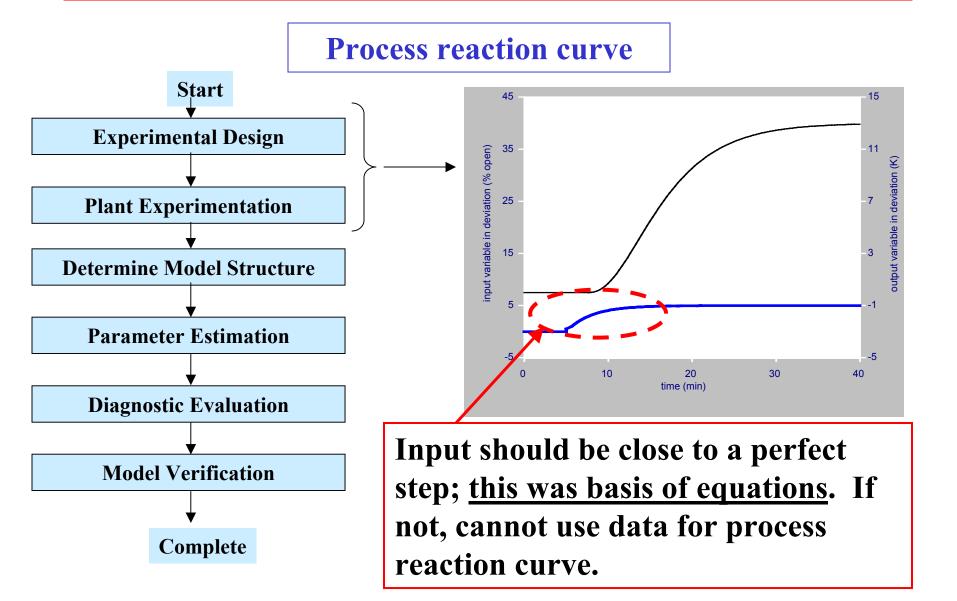


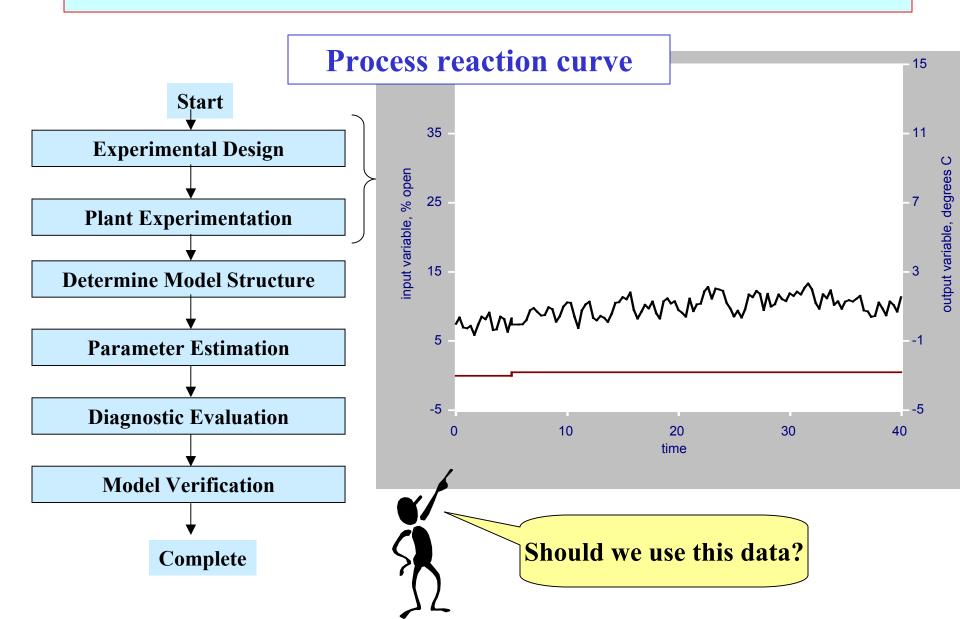
Recommended

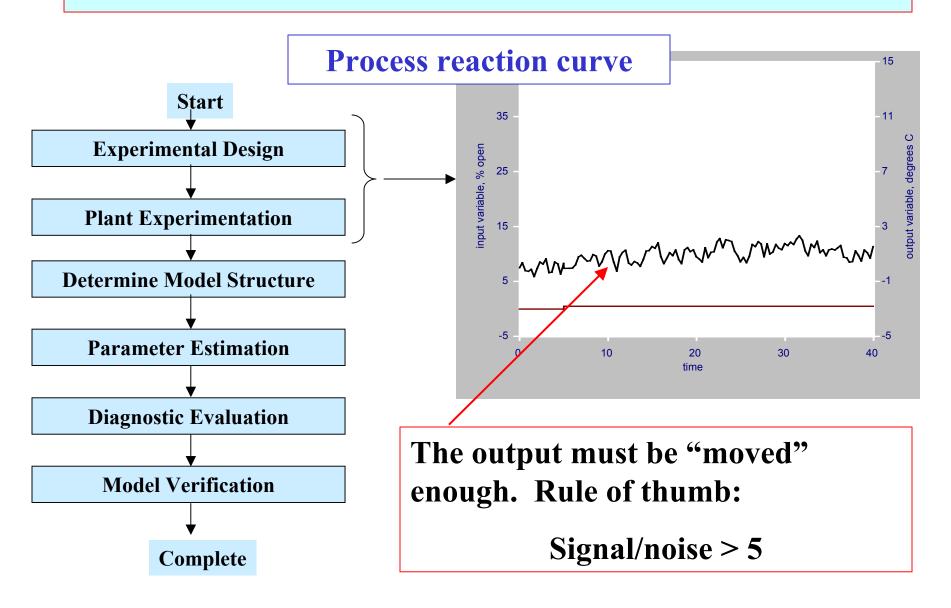




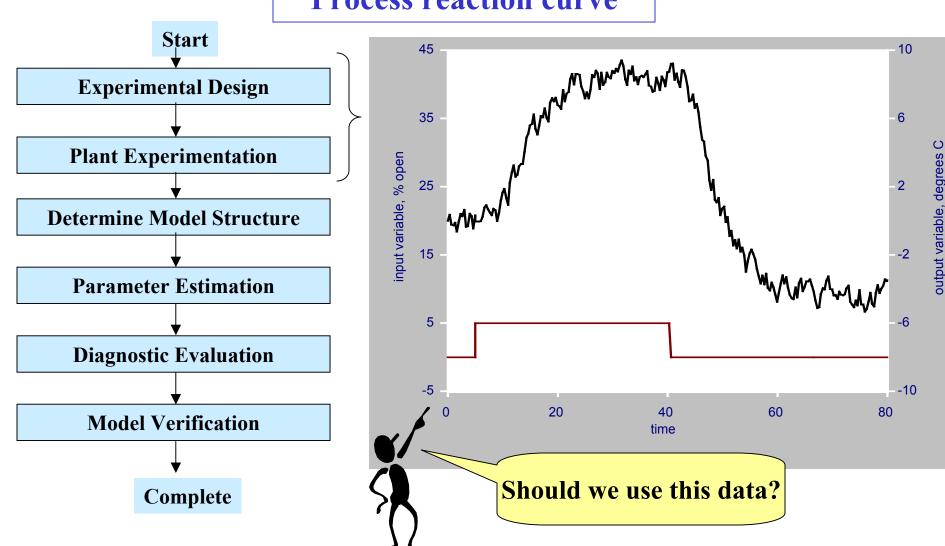
Complete

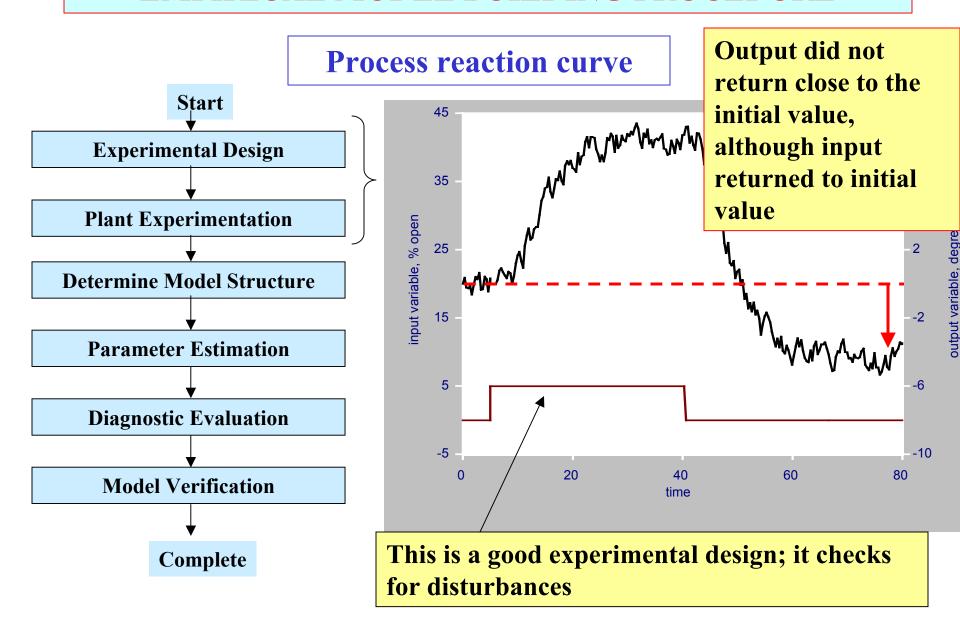




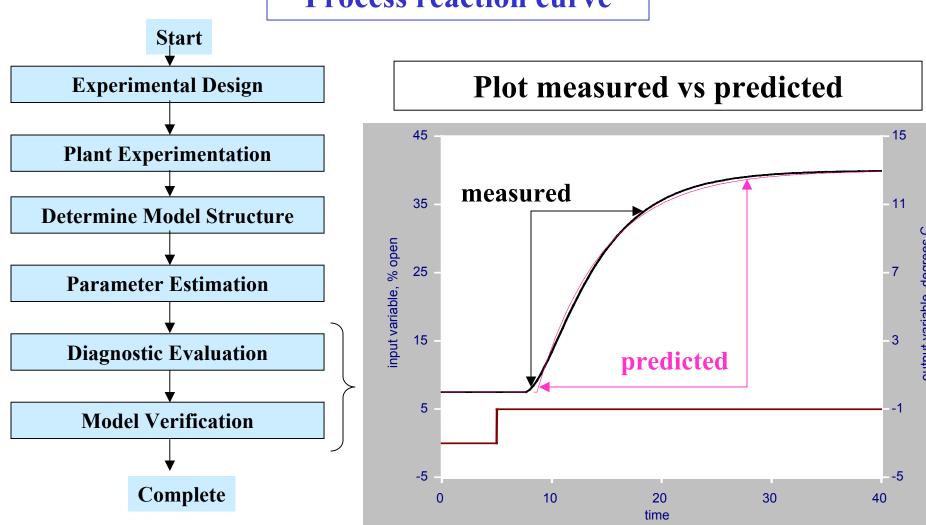








Process reaction curve



Statistical method

Provides much more general approach that is not restricted to

- step input
- first order with dead time model
- single experiment
- "large" perturbation
- attaining steady-state at end of experiment

Requires

more complex calculations

Statistical method

- The basic idea is to formulate the model so that regression can be used to evaluate the parameters.
- We will do this for a first order plus dead time model, although the method is much more general.
- How do we do this for the model below?

$$\tau \frac{dY(t)}{dt} + Y(t) = K_p X(t - \theta) \qquad \frac{Y(s)}{X(s)} = \frac{K_p e^{-\theta s}}{\tau s + 1}$$

Statistical method

We have discrete measurements, so let's express the model as a difference equation, with the next prediction based on current and past measurements.

$$(Y'_{i+1})_{predicted} = a(Y'_i)_{measured} + b(X'_{i-\Gamma})_{measured}$$

$$a = e^{-\Delta t/\tau}$$

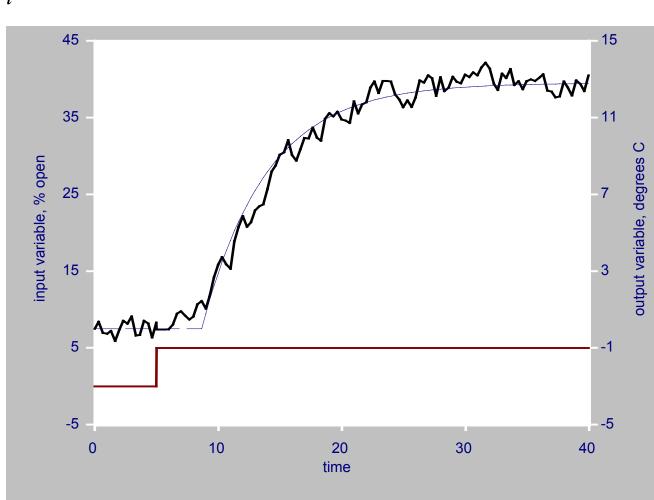
$$b = K_p (1 - e^{-\Delta t/\tau})$$

$$\Gamma = \theta / \Delta t$$

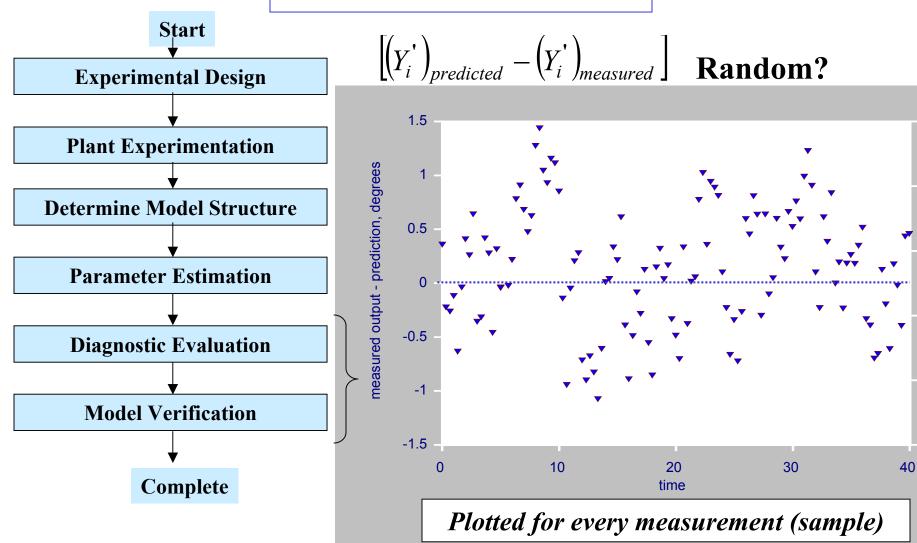
$$\mathbf{min} \quad \sum_{i} \quad \left[\left(Y_{i}' \right)_{predicted} - \left(Y_{i}' \right)_{measured} \right]^{2}$$

Now, we can solve a standard regression problem to minimize the sum of squares of deviation between prediction and measurements.

Details are in the book.







We performed a process reaction curve for the isothermal CSTR with first order reaction. The dynamic parameters are

$$K_p = \frac{\Delta C_A}{\Delta C_{A0}} = 0.50 \frac{kmol/m^3}{kmol/m^3}$$

$$\tau = 12.4 \text{ min}$$

Recently, we changed the feed flow rate by -40% and reached a new steady-state. What are the $C_{A0}\rightarrow C_A$ dynamics now?

F

C

C

V

A

B

$$-r_A = kC_A$$

$$\frac{dC'_A}{dt} = F(C'_{A0} - C'_A) - VkC'_A$$

$$\frac{dC'_A}{dt} + C'_A = KC'_{A0}$$

with $\tau = \frac{V}{F + kV}$ and $K = \frac{F}{F + kV}$



Match the method to the application.

Feature	Process reaction curve	Statistical method
Input magnitude	Signal/noise > 5	Can be much smaller
Experiment duration	Reach steady state	Steady state not required
Input change shape	Nearly perfect step	Arbitrary, sufficient "information"
		required
Model structure	First order with dead time	General linear dynamic model
Accuracy with	Poor with significant disturbance	Poor with significant disturbance
unmeasured		
disturbances		
Diagnostics	Plot prediction vs data	Plot residuals
Calculations	simple	Requires spreadsheet or other
		computer program

EMPIRICAL MODEL BUILDING

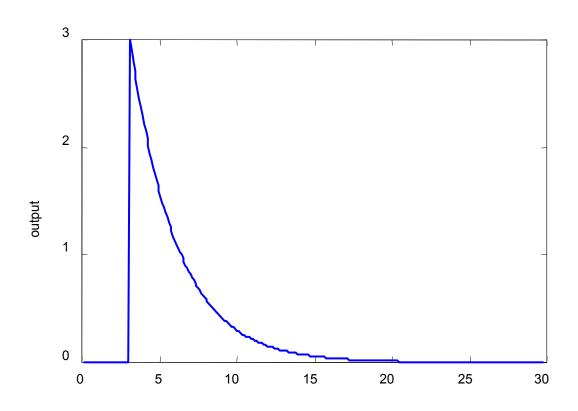
How accurate are empirical models?

- Linear approximations of non-linear processes
- Noise and unmeasured disturbances influence data
- Lack of consistency in graphical method
- lack of perfect implementation of valve change
- sensor errors



Let's say that each parameter has an error $\pm 20\%$. Is that good enough for future applications?

We introduced an impulse to the process at t=0. Develop and apply a graphical method to determine a dynamic model of the process.



State whether we can use a first order with dead time model for the following process. Explain your answer.

$$G_{valve}(s) = \frac{F_0(s)}{v(s)} = .10 \frac{m^3 s}{s_{0/0} open}$$

$$G_{tank1}(s) = \frac{T_1(s)}{F_0(s)} = \frac{-1.2 \ K/m^3 s}{250s + 1}$$

$$G_{sensor}(s) = \frac{T_{measured}(s)}{T_2(s)}$$

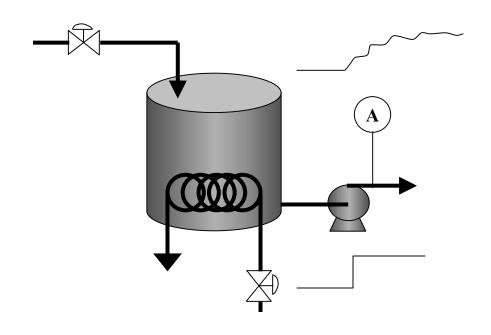
$$G_{tank2}(s) = \frac{T_2(s)}{T_1(s)} = \frac{1.0 \ K/K}{300s + 1}$$

$$G_{tank2}(s) = \frac{T_1(s)}{T_2(s)} = \frac{1.0 \ K/K}{10s + 1}$$

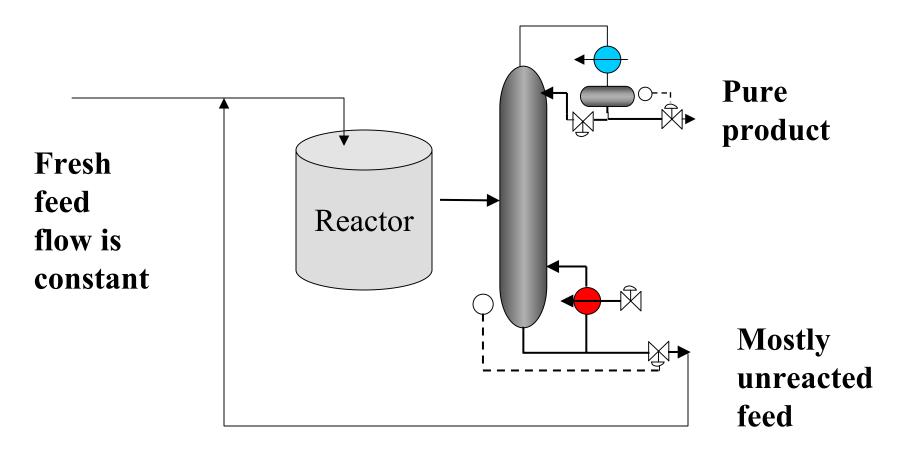
(Time in seconds)

We are familiar with analyzers from courses on analytical chemistry. In an industrial application, we can extract samples and transport them to a laboratory for measurement.

What equipment is required so that could we can achieve faster measurements for use in feedback control?



We are performing an experiment, changing the reflux flow and measuring the purity of the distillate. Discuss the processes that will affect the empirical dynamic model.



CHAPTER 6: EMPIRICAL MODEL IDENTIFICATION



When I complete this chapter, I want to be able to do the following.

- Design and implement a good experiment
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- Perform the statistical calculations
- Combine fundamental and empirical modelling for chemical process systems



Lot's of improvement, but we need some more study!

- Read the textbook
- Review the notes, especially learning goals and workshop
- Try out the self-study suggestions
- Naturally, we'll have an assignment!

CHAPTER 6: LEARNING RESOURCES

SITE PC-EDUCATION WEB

- Instrumentation Notes
- Interactive Learning Module (Chapter 6)
- Tutorials (Chapter 6)
- Software Laboratory
 - S_LOOP program to simulate experimental step data, with noise if desired
- Intermediate reference on statistical method
 - Brosilow, C. and B. Joseph, Techniques of Model-Based Control, Prentice-Hall, Upper Saddle River, 2002 (Chapters 15 & 16).

CHAPTER 6: SUGGESTIONS FOR SELF-STUDY

1. Find a process reaction curve plotted in Chapters 1-5 in the textbook. Fit using a graphical method.

Discuss how the parameters would change if the experiment were repeated at a flow 1/2 the original value.

- 2. Estimate the range of dynamics that we expect from
 - a. flow in a pipe
 - b. heat exchangers
 - c. levels in reflux drums
 - d. distillation composition
 - e. distillation pressure
- 3. Develop an Excel spreadsheet to estimate the parameters in a first order dynamic model.