

TWO HOURS

Department of Mechanical, Aerospace & Civil Engineering

UNIVERSITY OF MANCHESTER

ENGINEERING THERMODYNAMICS

xxxxxx 2021

09:00 - 11:00

Special Instruction(s):

- ANSWER ALL QUESTIONS
- A FORMULA SHEET IS PROVIDED AT THE END OF THE PAEPR.
- MAKE USE OF THE 'PROPERTY TABLES AND CHARTS (SI UNITS)', GIVEN AS APPENDIX OF 'THERMODYNAMICS-AN ENGINEERING APPROACH (SI VERSION) (9TH ED.) (MCGRAW HILL) CENGEL, BOLES AND KANOGLU.

- Q1. A hot reservoir provides heat to a Carnot heat engine at 900°C at a rate of 0.8 MJ/min and the waste heat is rejected to the ambient air at 27°C. The total work from the heat engine is used to power a refrigerator operating between a refrigerated space kept at -5°C and the same ambient air at 27°C. You may assume that the heat engine and the refrigerator operate steadily.
 - (a) Sketch the heat engine/refrigerator in the question using a simple diagram and highlight all the main components. [5 marks]
 - (b) Calculate the thermal efficiency of the Carnot heat engine and its maximum power output. [6 marks]
 - (c) Calculate the Coefficient of Performance (COP) of the Carnot refrigerator and the maximum rate of heat removal in kJ/min from the refrigerated space.
 [6 marks]
 - (d) Calculate the total rate of heat rejection to the ambient air in kJ/min from both the heat engine and refrigerator.[8 marks]

Q2. A gas-turbine power plant shown in **Figure Q2**, which is based on a Brayton cycle, consists of a compressor, a combustion chamber and a turbine. Air enters the compressor at 0°C and 1 bar with a pressure ratio of 7. The compressor has an isentropic efficiency of 80%. The turbine has an isentropic efficiency of 90%. The temperature at the outlet of the combustion chamber is 1500 K. The net power output is 150 MW.

Assume steady operating conditions and constant properties for air at 300 K with $c_V = 0.718$ kJ/kgK, $c_P = 1.005$ kJ/kgK, R = 0.287 kJ/kgK, $\gamma = 1.4$. You may ignore any kinetic and potential energy changes and assume air as an ideal gas.

- (a) Sketch the *T-s* diagram for the cycle. [4 marks]
- (b) Calculate the exit temperature of the compressor. [4 marks]
- (c) Calculate the exit temperature of the turbine. [4 marks]
- (d) Calculate the mass flow rate through the power plant in kg/s and the volumetric flow rate of the air into the compressor in m³/s. [8 marks]
- (e) Assuming all parameters of the problem remain the same, explain the impact of raising the compressor inlet temperature on the inlet mass flow rate and net power output (for a fixed compressor inlet velocity and flow area).
 [5 marks]

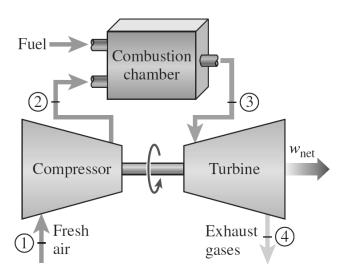


Figure Q2. A gas-turbine power plant

- Q3. The mass-based composition of a hydrocarbon-based gas mixture is: 15% butane, 25% propane and 60% methane. By a reversible, isothermal, steady-flow compressor, the mixture, initially at 20°C, is compressed from 1 bar to 8 bar. Ignoring any kinetic and potential energy changes and assuming air as an ideal gas, calculate:
 - (a) the mole numbers of the component within the mixture. [10 marks]
 - (b) the gas constant of the mixture. [5 marks]
 - (c) the work input and heat transfer for this compression per unit mass of the mixture. [10 marks]
- Q4. In a simple air-cooling unit depicted in **Figure Q4**, air enters at atmospheric pressure and temperature of 32°C with a relative humidity of 70% at the velocity of 120 m/min. The diameter of the cooling unit is 400 mm. The air is cooled by passing through a cold water cooling coil. The temperature of the water increases by 6°C as it cools the air. The air at the outlet of the cooling section is saturated at 20°C. Assuming a steady-flow process (i.e. constant mass flow rate for air), taking dry air and water vapour as ideal gases and ignoring the kinetic and potential energy changes, determine:

(a) the mass flow rate of air through the unit. [7 marks]
(b) the rate of heat transfer. [6 marks]
(c) the mass flow rate of the water. [6 marks]
(d) the exit velocity of the airstream. [6 marks]

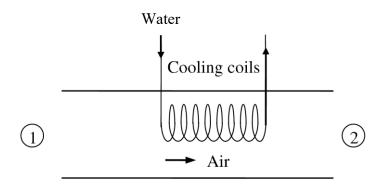


Figure Q4. Air cooling arrangement

END OF THE EXAMINATION PAPER

DATA SHEETS

- 1 Work
 - **positive work:** is done by a system on the surroundings (a system does positive work if it can raise a weight)
 - **negative work:** is done by the surroundings on a system.

Incremental piston, or displacement work , is $\delta W = p dV$, and for a process in which the pressure varies with volume the work is $W = \int p dV$

Constant pressure (isobaric) process: $pV^0 = c$

$$W_{12} = \int_{1}^{2} p dV = p(V_{2} - V_{1})$$

Constant volume (isochoric) process: $pV^{\infty}=c$

$$W_{13} = \int_{1}^{3} p dV = 0$$
, because $dV = 0$

Process defined by pV = c

$$W_{14} = p_1 V_1 \ln \frac{V_4}{V_1} = p_1 V_1 \ln \frac{p_1}{p_4} = etc$$

Process defined by $pV^n = c$

$$W_{15} = \frac{p_1 V_1 - p_5 V_5}{n - 1} = \frac{p_5 V_5 - p_1 V_1}{1 - n}$$

2 First Law of Thermodynamics - closed systems

$$Q - W_s = m \left(u_2 + \frac{V_2^2}{2} + gz_2 \right) - m \left(u_1 + \frac{V_1^2}{2} + gz_1 \right)$$

First Law for a closed system in the absence of kinetic and potential energy

$$\delta Q = dU + \delta W$$

Specific heat at constant volume

$$c_{v} = \left(\frac{\partial u}{\partial T}\right)_{v} = \left(\frac{\partial u}{\partial t}\right)_{v} = \left(\frac{\partial Q}{\partial T}\right)_{v}$$

Enthalpy, H

$$H = U + pV$$

Specific enthalpy, h

$$h = \frac{H}{m} = \frac{U + pV}{m} = \frac{U}{m} + \frac{pV}{m} = u + pv$$

Specific heat at constant pressure

$$c_p = \left(\frac{\partial h}{\partial T}\right)_p = \left(\frac{\partial h}{\partial t}\right)_p = \left(\frac{\partial q}{\partial T}\right)_p$$

3 Steady flow energy equation

$$\dot{Q} - \dot{W} = \dot{m} \left(h_e - h_i + \frac{V_e^2 - V_i^2}{2} + g(z_e - z_i) \right)$$

Stagnation enthalpy

$$h_0 = h + \frac{V^2}{2}$$

Velocity at exit to a nozzle

$$V_2 = \sqrt{2\left\{ \left(h_1 - h_2\right) + \frac{V_1^2}{2} \right\}}$$

Work from an adiabatic machine

$$-\dot{W}_{s} = \dot{m}(h_{e} - h_{i}) = \dot{m}(h_{2} - h_{1}).$$

4 Second Law of Thermodynamics

Efficiency

Thermal efficiency,
$$\eta_{th} = \frac{\text{Useful work output}}{\text{Thermal energy input}},$$
for a heat engine operating in a cycle .

Thermal efficiency of heat engine

Thermal efficiency ,
$$\eta_{th} = \frac{\text{Net work}}{\text{Heat supplied}}$$

$$\eta_{th} = \frac{W_s}{Q_1} = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1}$$

Coefficient of performance of refrigerator

Coefficient of performance,
$$\beta = \frac{\text{Heat transferred from cold reservoir}}{\text{Work done}}, = \frac{Q_2}{W_s} = \frac{Q_2}{Q_1 - Q_2}.$$

Coefficient of performance of heat pump

Coefficient of performance,
$$\beta = \frac{\text{Heat transferred to hot reservoir}}{\text{Work done}}, = \frac{Q_1}{W_s} = \frac{Q_1}{Q_1 - Q_2}$$
.

Relationship between coefficients of performance

$$\beta = 1 + \frac{Q_2}{W_s} = 1 + \beta$$

Entropy

Entropy is denoted by the symbol-S; specific entropy is denoted by -s.

The change of entropy between states 1 and 2 is
$$S_2 - S_1 = \int_1^2 \frac{\delta Q_R}{T}$$

Central Equation of Thermodynamics

$$Tds = du + pdv = dh - vdp$$

Steady flow entropy equation for an adiabatic machine

$$\dot{S}_i = \dot{m}(s_e - s_i) \ge 0$$

5 Properties of pure substances

Dryness fraction, or quality

Dryness fraction,
$$x = \frac{\text{Mass of dry vapour}}{\text{Total mass of liquid}} + \text{vapour}$$

$$v = xv_g + (1-x)v_f = v_f + xv_{fg}$$

$$u = xu_g + (1-x)u_f = u_f + xu_{fg}$$

$$h = xh_g + (1-x)h_f = h_f + xh_{fg}$$

$$s = xs_g + (1-x)s_f = s_f + xs_{fg}$$

6 Perfect gases, and mixtures of perfect gases

Ideal gas

$$\frac{pv}{T} = const, R$$

Universal Gas Constant $\Re = MR$

S.I. units Imperial

 \Re = 8.3145 kJ/kmol K

 \Re = 1545 ft.lbf/lb mol °R

= 1.986 Btu/lb mol °R

Molar Masses for Common Gases/Elements

Gas/Element	M (kg/kmol)
H ₂	2
O ₂	32
N_2	28
CO	28
CO ₂	44
H ₂ O	18
С	12

Internal energy

$$u = \int_{T_o}^{T} c_v dT + u_o$$
, where u_0 is the value of u at temperature T_0

Enthalpy

$$h = u + pv = u + RT$$

 $h = \int_{T_0}^{T} c_p dT + h_0$, where h_0 is the enthalpy at temperature T_0 .

Relationship between c_p and c_v

$$c_p = c_v + R$$

$$\gamma = c_p/c_v$$

Entropy change

$$ds = \frac{c_{v}dT + pdv}{T} = c_{v}\frac{dT}{T} + \frac{p}{T}dv$$

$$s_{2} - s_{1} = \int_{T_{1}}^{T_{2}} \frac{c_{v}}{T}dT + R\ell n \frac{v_{2}}{v_{1}}$$

$$s_{2} - s_{1} = \int_{T_{1}}^{T_{2}} \frac{c_{p}}{T}dT - R\ell n \frac{p_{2}}{p_{1}}$$

7 Isentropic or process efficiencies

For compressors:
$$\eta_c = \frac{h_{2i} - h_1}{h_2 - h_1}$$

For turbines:
$$\eta_t = \frac{h_1 - h_2}{h_1 - h_{2i}}$$

where the process is from state 1 to state 2 and subscript *i* denotes ideal (isentropic) values

8 Ideal cycle efficiencies

Otto cycle:
$$\eta = 1 - r_v^{-(\gamma - 1)}$$

Diesel cycle:
$$\eta = 1 - r_v^{-(\gamma - 1)} \frac{(r_c^{\gamma} - 1)}{\gamma(r_c - 1)}$$

Dual cycle:
$$\eta = 1 - r_v^{-(\gamma - 1)} \frac{(r_p r_c^{\gamma} - 1)}{(r_p - 1) + \gamma r_p (r_c - 1)}$$

where
$$r_{v}$$
 is the volumetric compression ratio

$$r_p$$
 is the constant-volume heat input pressure ratio

9 Mean effective pressures of reciprocating engine cycles

The indicated mean effective pressure (imep)

$$p_m = \frac{W_{net}}{V_{s}}$$

where W_{net} is the net cycle work, V_s is the swept volume

The brake mean effective pressure (bmep)

$$p_b = \frac{W_{net} - W_f}{V}$$

where W_f is the work lost to friction.

The friction mean effective pressure (fmep)

$$p_f = p_m - p_b$$