

BT209

Bioreaction Engineering

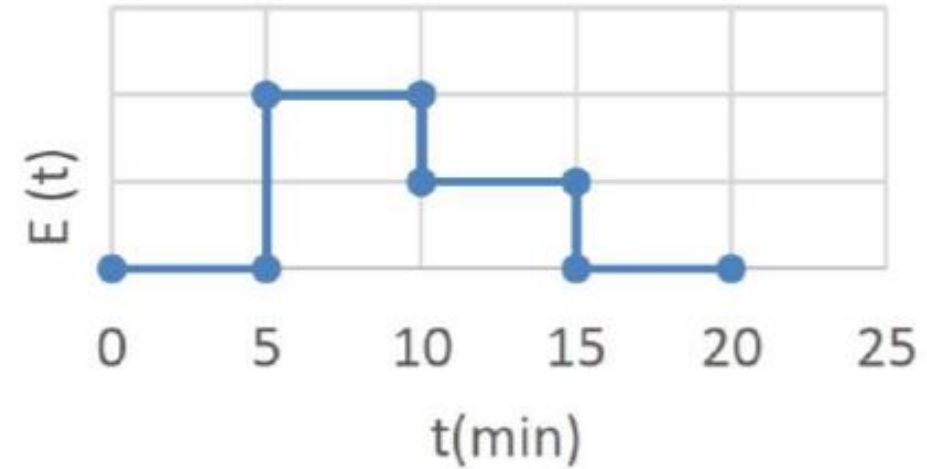
28/04/2023 (Extra class)

Tutorial: (RTD and non ideal reactor)

Problem 1

Segregation model

1) A reactor has a residence time distribution showing in the Fig. A second order reaction ($A \rightarrow P$) is carried out in this reactor. The feed concentration of A is 1.5 mol/L. The rate constant of the reaction is 0.2 L/(mol.min). What would be the conversion of A in this reactor considering the segregated flow model?



Solution

Diagram 11.0.1

Segregated model: $\bar{Y} = \int_0^{\infty} \underset{\text{value}}{X(t)} E(t) dt$

for 2nd order rxn:

$$\frac{dC_A}{dt} = -kC_A^2 \Rightarrow X = \frac{C_{A0}kt}{1 + C_{A0}kt}$$

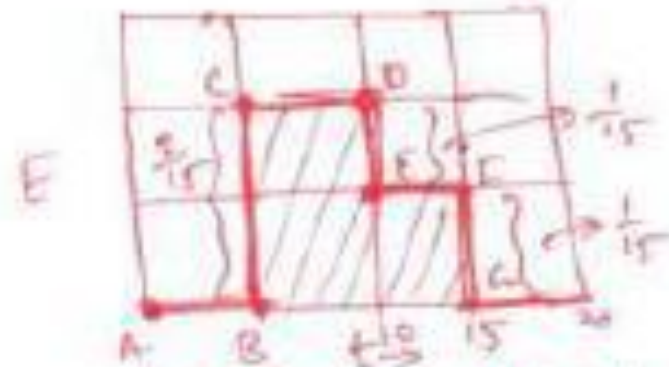
$$= \frac{0.3t}{1 + 0.3t}$$

$$\bar{Y} = \int_0^{\infty} \frac{0.3t}{1 + 0.3t} E(t) dt$$

$$= \int_0^5 \frac{0.3t}{1 + 0.3t} \times 0 + \int_5^{10} \frac{0.3t}{1 + 0.3t} \times \frac{2}{15}$$

$$+ \int_{10}^{15} \frac{0.3t}{1 + 0.3t} \times \frac{1}{15} + \int_{15}^{\infty} \frac{0.3t}{1 + 0.3t} \times 0$$

$$= 0.72$$



$\int_0^{\infty} E(t) dt = 1 \therefore \text{Area } B C D E F = 1$

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$$BC \times (10 - 5) + \frac{1}{2} BC \times (15 - 10) = 1$$

$$\left. \begin{aligned} BC &= \frac{2}{15} \\ FH &= \frac{1}{15} \end{aligned} \right\}$$

Problem 2

Tank in series (TIS) model

2) A sample of the tracer was injected as a pulse to a tubular reactor and the effluent concentration measured as a function of time, resulting in the following data:

t(min)	0	1	2	3	4	5	6	7	8	9	10	12	14
C(g/m ³)	0	1	5	8	10	8	6	4	3	2.2	1.5	0.6	0

A first order reaction ($A \rightarrow P$) is carried out in this tubular reactor (diameter=10 cm and length=6.36 m). The feed concentration of A is 10 mol/L. The rate constant of the reaction is 0.25 min^{-1} . What would be the conversion of A in this reactor considering the TIS model?

Solution

t	0	1	2	3	4	5	6	7	8	9	10	12	14
C	0	1	5	8	10	8	6	4	3	2.2	1.5	0.6	0
E	0	0.02	0.1	0.16	0.2	0.16	0.12	0.08	0.06	0.044	0.03	0.012	0
tE	0	0.02	0.2	0.48	0.8	0.8	0.72	0.56	0.48	0.4	0.3	0.14	0
t ² E	0	0.02	0.4	1.44	3.2	4	4.32	3.92	3.84	3.60	3.0	1.68	0

$$\therefore \int_0^{\infty} C(t) dt = 50 \text{ g. min}, \quad \bar{t} = \int_0^{\infty} tE dt = 5.15 \text{ min}$$

$$\begin{aligned} \int_0^{\infty} t^2 E dt &= \frac{1}{3} [1(0) + 4(0.02) + 2(0.4) + 4(1.44) + 2(2.2) + 4(4.0) \\ &\quad + 2(4.32) + 4(3.92) + 2(3.84) + 4(3.6) + 1(3.0)] \\ &\quad + \frac{2}{3} [3.0 + 4(1.68) + 0] \\ &= 32.63 \text{ min}^2 \end{aligned}$$

$$\begin{aligned} \therefore \sigma^2 &= \int_0^{\infty} (t - \bar{t})^2 E dt = \int_0^{\infty} t^2 E dt - \bar{t}^2 \\ &= 32.63 - (5.15)^2 = 6.10 \text{ min}^2 \end{aligned}$$

$$n = 5.15 \times 5.15 / (6.10) = 4.34 \approx 5$$

$$T_i = T / 4.34 = 5.15 / 4.34 = 1.187$$

$$\text{For first order reaction, } x = 1 - 1 / (1 + k T_i)^n = 1 - 1 / (1 + 0.25 \times 1.187)^{4.34} = 1 - 1 / 3.089 = 1 - 0.3237 = 0.686$$