# **Experiment 7**

# Determination of overall volumetric oxygen mass transfer coefficient

### **Objective:**

To determine the overall volumetric mass transfer coefficient of oxygen  $(K_L a)$  from gas phase to liquid phase in cell free media using simple dynamic method

### **Introduction:**

Dissolved oxygen is an important substrate in aerobic fermentations. Since oxygen is sparingly soluble in water, it may be the growth-limiting substrate in these fermentations. For bacteria and yeast cultures, the *critical oxygen concentration* is about 10% to 50% of the saturated DO (dissolved oxygen concentration). Above this critical concentration, the oxygen concentration no longer limits growth. For optimum growth it is therefore important to maintain the DO above this critical level by *sparging* (bubbling gas through) the fermentor with air or pure oxygen. Of course, to be effective, the mass transfer rate from the gas bubbles to the liquid broth must equal or exceed the rate at which growing cells take up the oxygen.

Oxygen transfer is usually limited by the liquid film surrounding the gas bubbles. The rate of transport is given by:

Rate of oxygen transport, 
$$\frac{dC}{dt} = k_L a \left( C^* - C_t \right)$$
 (1)

where  $k_L$  is the oxygen transport coefficient (cm/h), a is the gas-liquid interfacial area (cm<sup>2</sup>/cm<sup>3</sup>),  $k_L a$  the volumetric oxygen transfer coefficient (h<sup>-1</sup>),  $C^*$  is saturated DO concentration,  $C_t$  is the actual DO concentration at time t.

In the model system used for the experiment to determine KLa in water i.e., in the case where no reaction is taking place (without microorganism), the following simplifications are valid:

- Oxygen uptake rate  $(OUR=q_{02}X) = 0$  because there is no O2 sink in the system
- Only data for oxygen transfer rate [OTR= $KLa(C^*-CL)$ ] will be considered in the following equation:

$$dCL/dt = OTR - OUR = K_{La}(C_{L} * - C_{L}) - q_{O2}X = K_{La}(C_{L} * - C_{L})$$
 (2)

Where,  $q_{02}$  is the specific oxygen uptake rate, X is biomass cocentration,  $C_L$  \* is the saturation dissolved oxygen concentration and  $C_L$  is the dissolved oxygen concentration at any time t. Solving the above differential equation with an initial concentation  $C_{L0}$  (at  $t_0$ ) results in equation:

$$\ln \left( C_L^* - C_{Lo} / C_L^* - C_L \right) = K_L a \left( t - t_0 \right)$$
 (3)

The concentration  $C_{Lo}$  can be achieved by flushing nitrogen in the system. At time  $t_0$  the degassing with nitrogen is stopped (Fig.1) and from time  $t_0$  there is constant aeration. To determine the  $K_La$  value by the dynamic method, short bursts of measurement with an electrode are necessary so that measurement time with the electrode has no influence on the value of  $K_La$ .

We will perform the "gassing-in" method to measure  $k_La$ . The fermenter should be filled with required amount of water/media. The dissolved oxygen would be first removed by sparging with nitrogen, and the air will be purged. The rate of gas transfer to the liquid is determined by using a DO probe that is mounted in the fermenter. This probe is connected to a DO meter, which in turn is connected to a data acquisition (DAQ) system on the PC. Copy the collected data and export it to MS Excel sheet to do the further analysis.

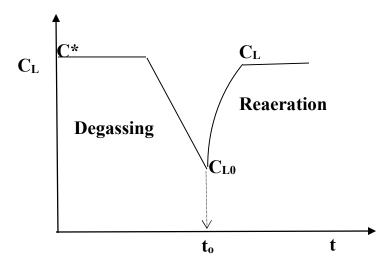


Fig.1 Schematic representation of Dynamic method

Here  $C^*$  = Saturation DO,  $C_{L0}$  = DO at time  $t_0$ ,  $C_L$  = steady state DO at time t

#### **Calculation:**

In a MS Excel sheet, prepare this table

Time (Sec)	C (DO)

**Plot C vs Time plot**. And identify the C\*.

To the existing table add new columns to create the following:

Time (Sec)	C (DO)	$\left(\frac{C^* - C_{L0}}{C^* - C_L}\right)$	$ \ln \left( \frac{C^* - C_{L0}}{C^* - C_L} \right) $
0		1	0

Plot 
$$\ln \left( \frac{C^* - C_{L0}}{C^* - C_L} \right)$$
 vs time plot. Use the data only from the linear region of the first plot

(C vs Time) to create this plot. Do linear regression to fit the data to a straight line (y=mx). Calculate  $k_La$  from this graph.

We will do the same experiment with different rate of stirring. For each case you have to calculate the  $k_L a$ , as we have mentioned above.

Prepare the following **table**:

Stirring speed (rpm)	k <sub>L</sub> a

Plot  $k_{L}a$  vs Stirring speed plot to show the effect of agitation on oxygen transfer. Usually, there exists a linear relation between these two. If possible, fit your data to a straight line.