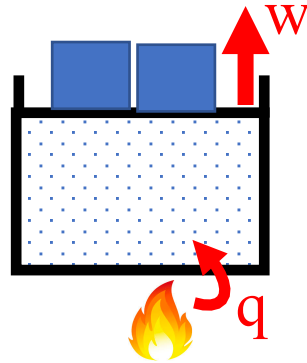


1st law for open system

CLOSED SYSTEM:



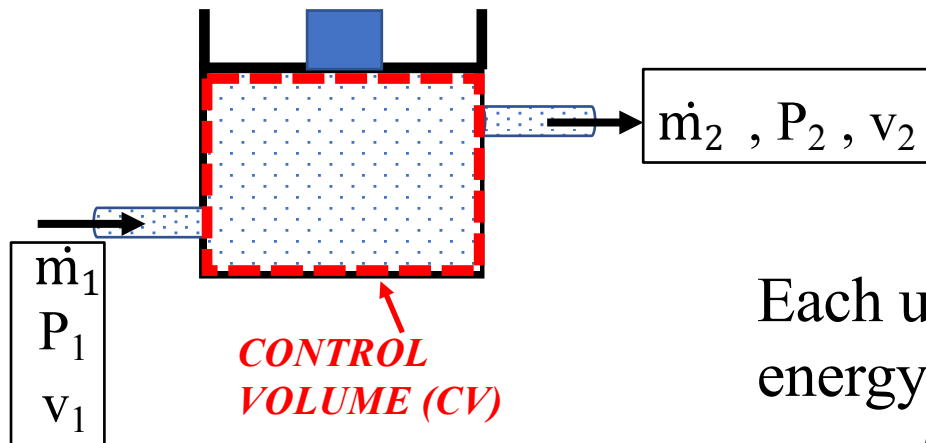
$$\Delta U = q + w \quad (\text{First law})$$

Change with respect to time

$$\frac{\Delta U}{t} = \frac{q}{t} + \frac{w}{t} \quad (t = \text{time})$$

$$\Rightarrow \Delta \dot{U} = \dot{q} + \dot{w}$$

OPEN SYSTEM:



1st Law open system

$$\Rightarrow \Delta \dot{U} = \dot{q} + \dot{w} + \frac{d}{dt} [\text{Stream flow energy}]$$

Each unit of stream carries with a total energy = $u + \frac{1}{2} v^2 + z g$

*Internal
energy*

*Kinetic
energy*

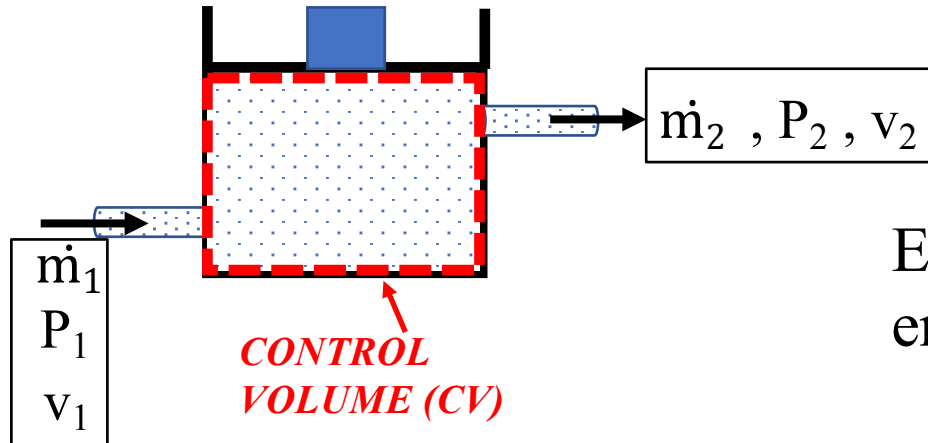
*Potential
energy*

v = velocity

z = elevation from the ground

g = gravitational acceleration

OPEN SYSTEM:



1st Law open system

$$\Rightarrow \Delta \dot{U}_{CV} = \dot{q} + \dot{w} + \frac{d}{dt} [\text{Stream flow energy}]$$

Each unit of stream carries with a total

$$\text{energy} = \underbrace{u}_{\text{Internal energy}} + \underbrace{\frac{1}{2} v^2}_{\text{Kinetic energy}} + \underbrace{z g}_{\text{Potential energy}}$$

v = velocity

z = elevation from the ground

g = gravitational acceleration

Thus, stream of mass “ m ” transport energy as the rate = $\dot{m} (u + \frac{1}{2} v^2 + z g)$

$$\Rightarrow \Delta \dot{U}_{CV} = \dot{q} + \dot{w} + [\dot{m}_1 (u_1 + \frac{1}{2} v_1^2 + z_1 g) - \dot{m}_2 (u_2 + \frac{1}{2} v_2^2 + z_2 g)]$$

Work rate (\dot{w})

$$\dot{w} = \dot{w}_{CV} + \dot{Flow\ work}$$

$$\begin{aligned}
 \text{Flow work} &= \frac{d}{dt} [\text{Force} \times \text{distance}] \\
 &= \frac{d}{dt} [(\text{Force} / \text{Area}) \times (\text{Area} \times \text{distance})] \\
 &= \frac{d}{dt} [\text{Pressure} \times \text{Area} \times \text{distance}] \\
 &= \text{Pressure} \times \text{Area} \times \frac{d}{dt} [\text{distance}] \\
 &= \text{Pressure} \times \text{Area} \times \text{velocity} \\
 &= P A v
 \end{aligned}$$

Pressure = P Area = A $\frac{d}{dt} [\text{distance}] = \text{velocity} = v$
--

Now, rate of change of mass (m):

$$\dot{m} = \frac{dm}{dt} = \frac{d(\text{density} \times \text{volume})}{dt} = \frac{d(\text{density} \times \text{Area} \times \text{distance})}{dt} = \boldsymbol{\rho} A v$$

density = $\boldsymbol{\rho}$

$$\dot{m} = \rho A v$$

$$\Rightarrow \frac{\dot{m}}{\rho} = A v$$

$$\Rightarrow \dot{m} \bar{V} = A v$$

\bar{V} = Specific volume

$$\text{Flow work} = P \boxed{A v} = P \boxed{\dot{m} \bar{V}}$$

1st law open system

$$\begin{aligned}
 \Delta \dot{U}_{cv} &= \dot{q} + \dot{w} + [\dot{m}_1(u_1 + \frac{1}{2} v_1^2 + z_1 g) - \dot{m}_2(u_2 + \frac{1}{2} v_2^2 + z_2 g)] \\
 &= \dot{q} + \dot{w}_{cv} + \text{Flow work} + [\dot{m}_1(u_1 + \frac{1}{2} v_1^2 + z_1 g) - \dot{m}_2(u_2 + \frac{1}{2} v_2^2 + z_2 g)] \\
 &= \dot{q} + \dot{w}_{cv} + (P_1 \dot{m}_1 \bar{V}_1 - P_2 \dot{m}_2 \bar{V}_2) + [\dot{m}_1(u_1 + \frac{1}{2} v_1^2 + z_1 g) - \dot{m}_2(u_2 + \frac{1}{2} v_2^2 + z_2 g)] \\
 &= \dot{q} + \dot{w}_{cv} + \dot{m}_1(\underbrace{u_1 + P_1 \bar{V}_1}_{\text{Enthalpy}} + \frac{1}{2} v_1^2 + z_1 g) - \dot{m}_2(\underbrace{u_2 + P_2 \bar{V}_2}_{\text{Enthalpy}} + \frac{1}{2} v_2^2 + z_2 g) \\
 &= \dot{q} + \dot{w}_{cv} + \dot{m}_1(\bar{H}_1 + \frac{1}{2} v_1^2 + z_1 g) - \dot{m}_2(\bar{H}_2 + \frac{1}{2} v_2^2 + z_2 g)
 \end{aligned}$$

Mass Balance

Mass of the system within the control volume is constant

$$\dot{m}_1 = \dot{m}_2 = \dot{m}$$

$$\Delta \dot{U}_{CV} = \dot{q} + \dot{w}_{cv} + \dot{m}_1 (\overline{H}_1 + \frac{1}{2} v_1^2 + z_1 g) - \dot{m}_2 (\overline{H}_2 + \frac{1}{2} v_2^2 + z_2 g)$$

$$\Delta \dot{U}_{CV} = \dot{q} + \dot{w}_{cv} + \dot{m}_1 [(\overline{H}_1 + \frac{1}{2} v_1^2 + z_1 g) - (\overline{H}_2 + \frac{1}{2} v_2^2 + z_2 g)]$$

$$\Delta \dot{U}_{CV} = \dot{q} + \dot{w}_{cv} + \dot{m} (\overline{H}_1 - \overline{H}_2) + \frac{1}{2} \dot{m} (v_1^2 - v_2^2) + \dot{m} (z_1 g - z_2 g)$$

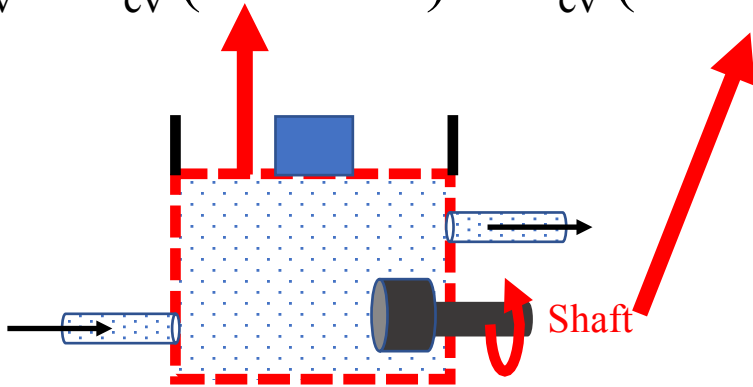
$$\Delta \dot{U}_{CV} = \dot{q} + \dot{w}_{cv} + \dot{m} \Delta (\overline{H} + \frac{1}{2} v^2 + zg)$$

Steady Flow $\Delta \dot{U}_{CV} = 0$

$$\dot{q} + \dot{w}_{cv} + \dot{m} \Delta (\overline{H} + \frac{1}{2} v^2 + zg) = 0$$

Work (\dot{w}_{cv})

$$\dot{w}_{cv} = \dot{w}_{cv} \text{ (PV work)} + \dot{w}_{cv} \text{ (Shaft work)}$$



$$\dot{w}_{cv} \text{ (Shaft work)} = 2\pi T \dot{n}$$

T = Torque

n = number of times it rotate/revolutions

Lecture 5

Mechanical Forms of Work

Shaft Work

- A force F acting through a moment arm r generates a torque T of:

$$T = F \times r \quad \rightarrow \quad F = \frac{T}{r}$$

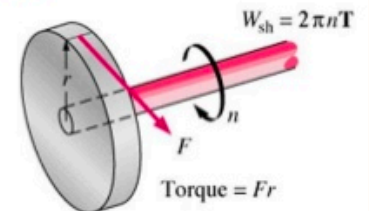
- This force acts through a distance s, which is related to the radius r by:

$$s = (2\pi r)n$$

where n is the number of revolutions

- The shaft work will be:

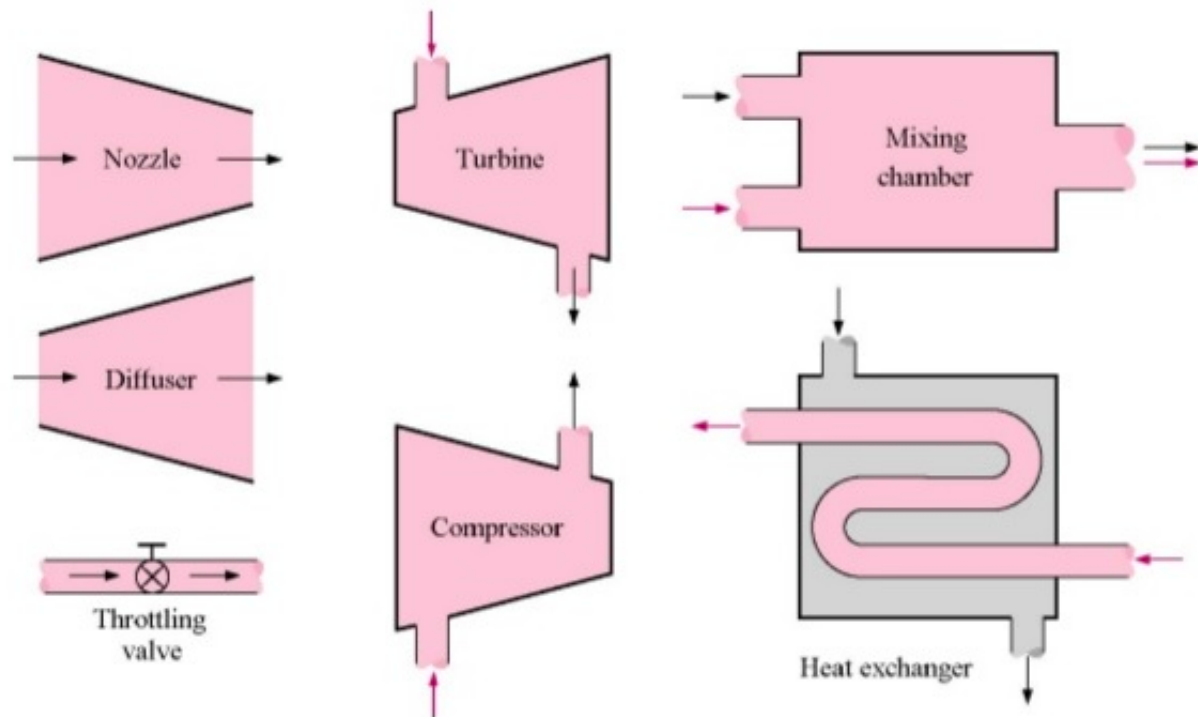
$$W_{sh} = Fs = \left(\frac{T}{r}\right)(2\pi rn) = 2\pi nT$$



- The power transmitted through the shaft is the shaft work done per unit time:

$$\dot{W}_{sh} = 2\pi \dot{n} T$$

Steady Flow Devices



APPLYING SFEE in STEADY-FLOW SYSTEMS

Nozzles and Diffusers

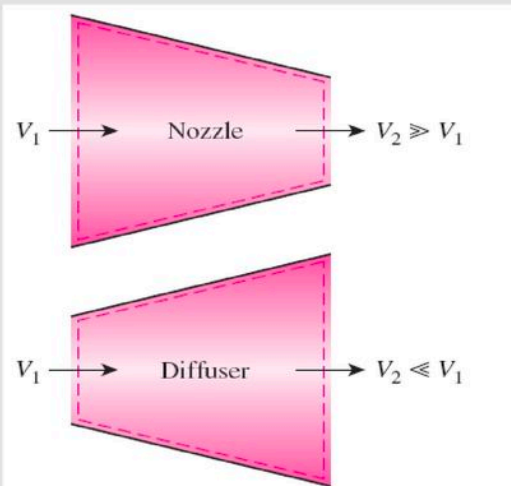


FIGURE 5-25

Nozzles and diffusers are shaped so that they cause large changes in fluid velocities and thus kinetic energies.

Mass balance for a nozzle or diffuser:

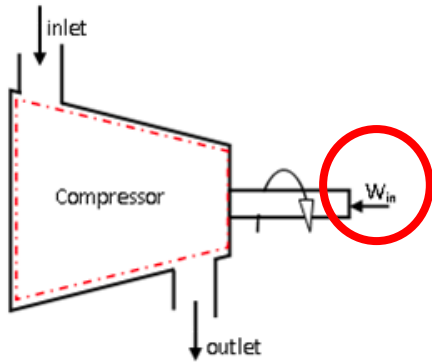
$$\dot{m}_i = \dot{m}_e = \dot{m}$$

$$\rho_i A_i V_i = \rho_e A_e V_e$$

Energy balance for a nozzle or diffuser:

$$\dot{E}_{\text{in}} = \dot{E}_{\text{out}}$$
$$\dot{m} \left(h_1 + \frac{V_1^2}{2} \right) = \dot{m} \left(h_2 + \frac{V_2^2}{2} \right)$$

(since $\dot{Q} \cong 0$, $\dot{W} = 0$, and $\Delta p_e \cong 0$)



➤ Compressor/ Turbines are Steady Flow Devices: $\Delta U_{cv} = 0$

➤ Furthermore, $m_{out}=m_{in}$ because of conservation of mass.

$$\dot{q} + \dot{w}_{cv} + \dot{m} \Delta \left(\bar{H} + \frac{1}{2} v^2 + zg \right) = 0$$

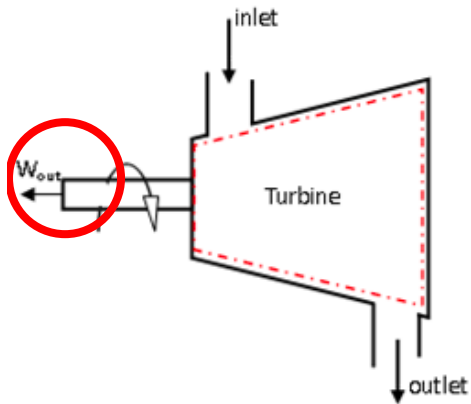
➤ The change of kinetic energy and potential energy of fluid flowing into and out of turbines and compressors are very small that can usually be neglected.

➤ Well insulated device, $q = 0$

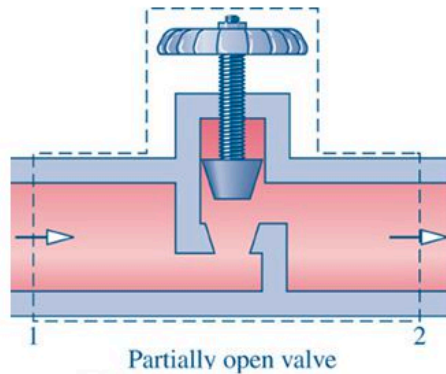
$$\dot{w}_{cv} + \dot{m} \Delta \bar{H} = 0$$

$$W_{cv} = m \left(\bar{H}_{out} - \bar{H}_{in} \right)$$

$W_{cv} > 0 \rightarrow \text{compressor}$
 $W_{cv} < 0 \rightarrow \text{turbine}$

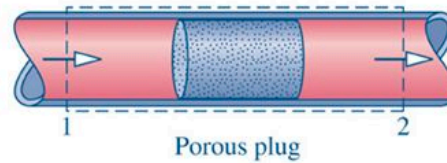


Throttling devices

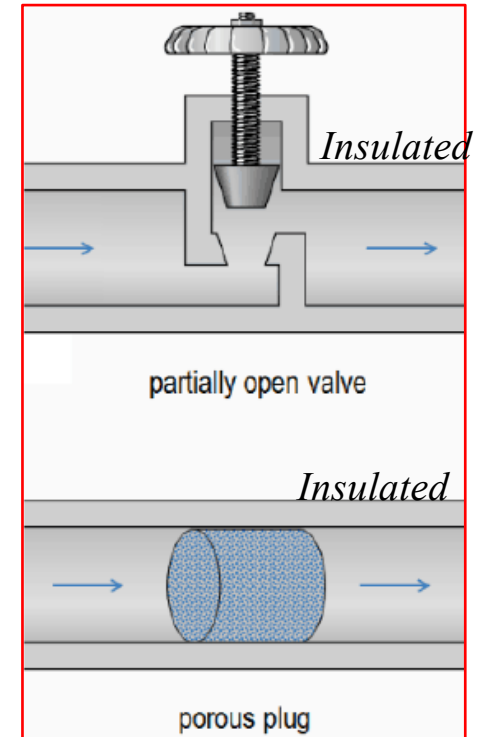


A device that causes a drop in pressure by restricting the flow passage can be termed a throttling device.

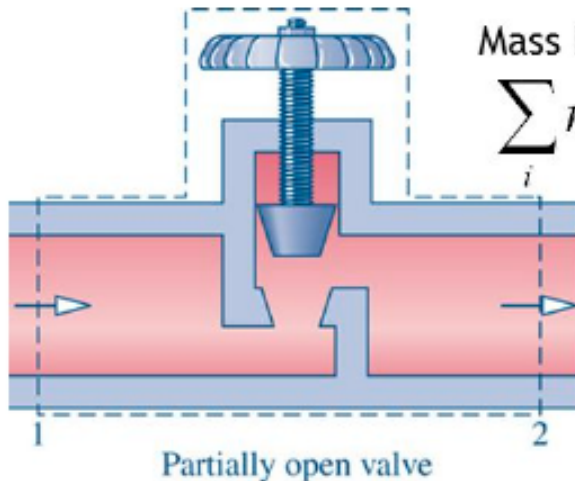
Flow restriction



Lecture 0

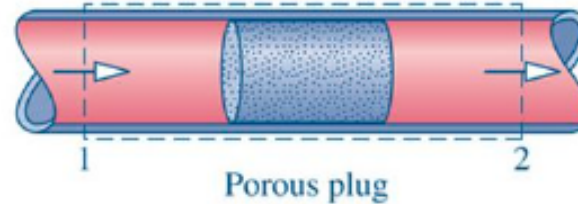


Throttling Device: Reduces Pressure



Mass Balance:

$$\sum_i \dot{m}_{in} = \sum_i \dot{m}_{exit} \rightarrow \dot{m}_{in} = \dot{m}_{exit} = \dot{m}$$



Typical Energy Balance simplifications,

$$\frac{dU_{cv}}{dt} = \dot{Q}_{cv} + \dot{W}_{cv} + \dot{m}_i \left(h_i + \frac{v_i^2}{2} + gz_i \right) - \dot{m}_e \left(h_e + \frac{v_e^2}{2} + gz_e \right)$$

$\frac{dU_{cv}}{dt}$ → Steady State
 \dot{Q}_{cv} → No heat transfer
 \dot{W}_{cv} → No work
 $\frac{v_i^2}{2}$ → $\Delta v \approx 0$
 gz_i → Horizontal Section (or very short vertical)
 $h_i = h_e$

Throttling devices

$H_1 = H_2$ (isoenthalpic)

