

ENERGY LOSSES IN FLOW

- Energy losses can occur through friction in pipes, bends and fittings, and in equipment
 - Friction in Pipes
 - Energy Losses in Bends and Fittings
 - Pressure Drop through Equipment
 - Calculation of Pressure Drops in Flow Systems

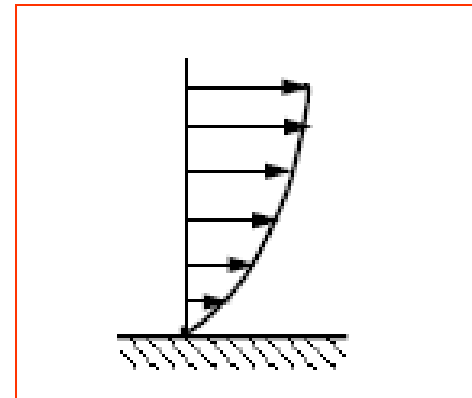
Friction losses in Pipes

Pressure loss due to friction in a pipeline

Because fluids are viscous, energy is lost by flowing fluids due to friction.

In a real flowing fluid shear stress slows the flow.

velocity profile:



Consider a cylindrical element of incompressible fluid flowing in the pipe,



The driving force due to pressure

driving force = Pressure force at 1 - pressure force at 2

$$\Delta p A = \Delta p \frac{\pi d^2}{4}$$

The retarding force is due to the shear stress

= shear stress \times area over which it acts

= $\tau_w \times$ area of pipe wall

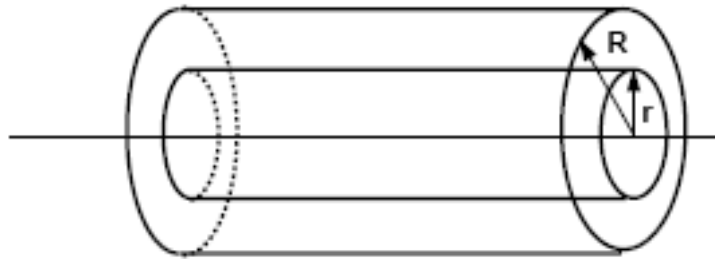
$$= \tau_w \pi d L$$

As the flow is in equilibrium,
driving force = retarding force

$$\Delta p \frac{\pi d^2}{4} = \tau_w \pi d L$$

$$\Delta p = \frac{\tau_w 4 L}{d}$$

What is the variation of shear stress in the flow?



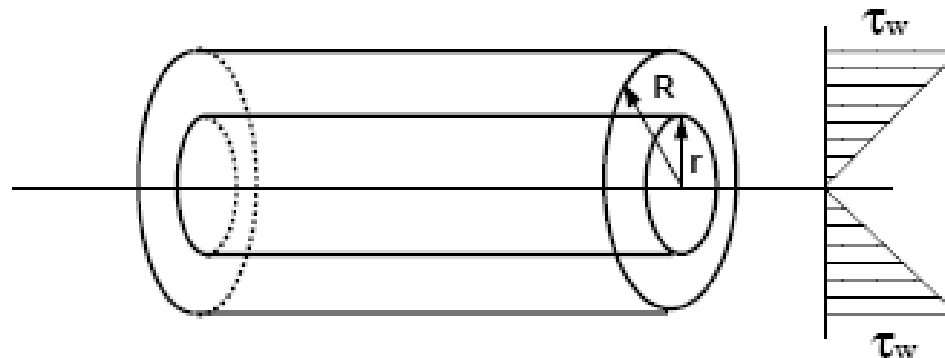
At the wall

$$\tau_w = \frac{R}{2} \frac{\Delta p}{L}$$

At a radius r

$$\tau = \frac{r}{2} \frac{\Delta p}{L}$$

$$\tau = \tau_w \frac{r}{R}$$



Pressure loss during laminar flow in a pipe

HAGEN-
POISEUILLE

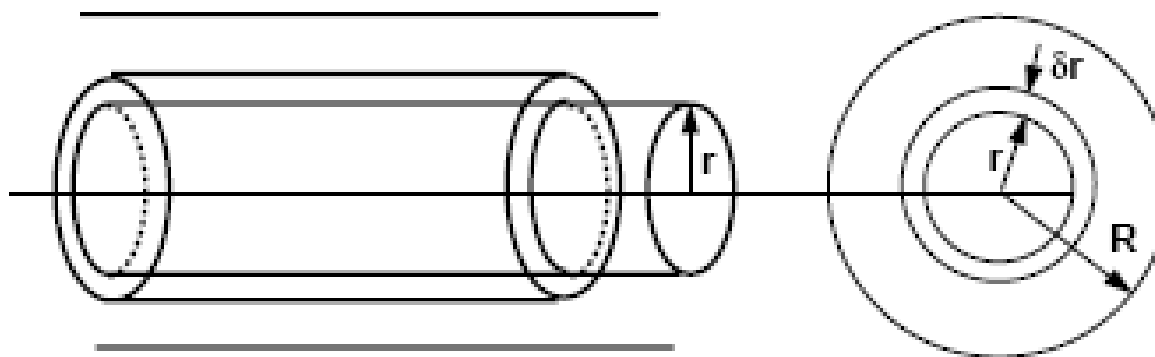
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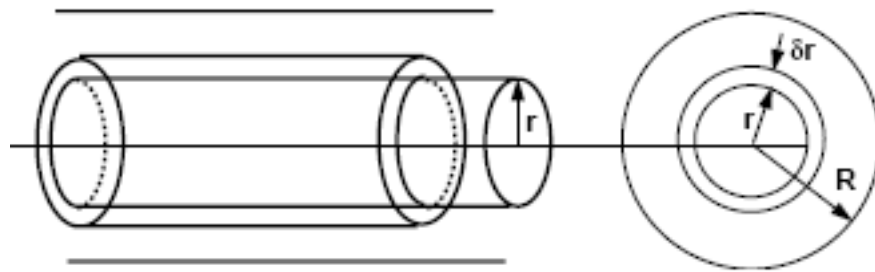
In laminar flow the paths of individual particles of fluid do not cross.

Flow is like a series of concentric cylinders sliding over each other.

And the stress on the fluid in laminar flow is entirely due to viscose forces.

As before, consider a cylinder of fluid, length L , radius r , flowing steadily in the centre of a pipe.





The fluid is in equilibrium,
shearing forces equal the pressure forces.

$$\tau 2\pi r L = \Delta p A = \Delta p \pi r^2$$

$$\tau = \frac{\Delta p}{L} \frac{r}{2}$$

Newtons law of viscosity says $\tau = \mu \frac{du}{dy}$,

We are measuring from the pipe centre, so

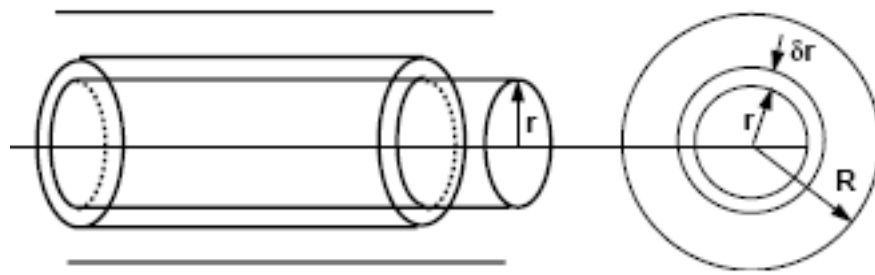
$$\tau = -\mu \frac{du}{dr}$$

$$\frac{\Delta p}{L} \frac{r}{2} = -\mu \frac{du}{dr}$$

$$\frac{du}{dr} = -\frac{\Delta p}{L} \frac{r}{2\mu}$$

In an integral form this gives an
expression for velocity,

$$u = -\frac{\Delta p}{L} \frac{1}{2\mu} \int r dr$$



The value of velocity at a point distance r from the centre

$$u_r = -\frac{\Delta p}{L} \frac{r^2}{4\mu} + C$$

At $r = R$ (the pipe wall) $u = 0$;

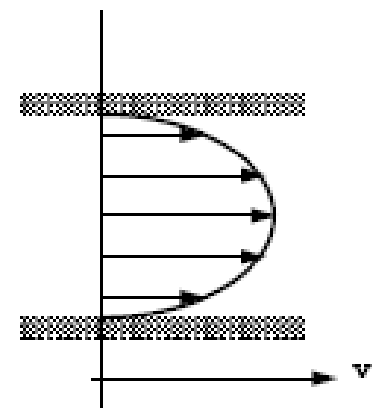
$$C = \frac{\Delta p}{L} \frac{R^2}{4\mu}$$

At a point r from the pipe centre when the flow is laminar:

$$u_r = \frac{\Delta p}{L} \frac{1}{4\mu} (R^2 - r^2)$$

This is a parabolic profile
(of the form $y = ax^2 + b$)

so the velocity profile in the pipe looks similar to



What is the discharge in the pipe?

The flow in an annulus of thickness δr

$$\delta Q = u_r A_{\text{annulus}}$$

$$A_{\text{annulus}} = \pi(r + \delta r)^2 - \pi r^2 \approx 2\pi r \delta r$$

$$\delta Q = \frac{\Delta p}{L} \frac{1}{4\mu} (R^2 - r^2) 2\pi r \delta r$$

$$Q = \frac{\Delta p}{L} \frac{\pi}{2\mu} \int_0^R (R^2 r - r^3) dr$$

$$= \frac{\Delta p}{L} \frac{\pi R^4}{8\mu} = \frac{\Delta p \pi d^4}{L 128\mu}$$

$$Q = \frac{\Delta p}{L} \frac{\pi d^4}{128\mu}$$

**This is the Hagen-Poiseuille Equation
for laminar flow in a pipe**

$$\text{Average velocity} = \bar{u} = \frac{Q}{A}$$

$$= \frac{Q}{\pi D^2 / 4}$$

$$\bar{u} = \frac{\Delta P D^2}{32 L \mu}$$

Another form of
HAGEN-
POISEUILLE
Eqn.

Maximum velocity.....

- We know, for laminar flow..... the average velocity is given by, Hagen-Poiseuille's eqn....

$$\bar{u} = \frac{\Delta P D^3}{32 L \mu}$$

- We know the velocity profile, $u_r = \frac{\Delta P}{L} \frac{1}{4\mu} (R^2 - r^2)$
- And @ $r = 0$ $u_r = u_{\max}$

$$\therefore u_{\max} = \frac{\Delta P R^2}{4 \mu L}$$

$$\therefore \frac{\bar{u}}{u_{\max}} = 0.5$$

Prob 1

- A small capillary with an ID of 2.22×10^{-3} m and a length 0.317m is being used to continuously measure the flow rate of a liquid having a density of 875 kg/m^3 and viscosity $1.3 \times 10^{-3} \text{ Pa-s}$. The pressure drop reading across the capillary during flow is 0.0655m of water (density 996 kg/m^3). What is the flow rate?
- $u = 0.275 \text{ m/s}$
- $Q = 1.066 \times 10^{-6} \text{ m}^3/\text{s}$
- $N_{\text{Re}} = 473$