

Raw data

1. User Inputs

- Gold head grade (grams/tonne)
- Particle size distributions
 - P50 value (microns)
 - P10 value (microns)
 - P80 value (microns)
- Ore mineralogy (% for each)
 - Iron
 - Arsenic
 - Copper
 - Zinc
 - Lead
 - Calcium
 - Iron
 - Silicon
 - Potassium
 - Aluminum
 - Sodium
 - Sulphur
- Throughput: tph or tpd
- Reagents:
 - CN(kg/t),
 - Lime(kg/t),
 - Collector A(g/t),
 - Collector B(g/t),
 - Frother(mL/t)

2. Ore Classification

- Program analyzes minerals to determine ore type
- Ore Classification Percentages:
 - Pyrite
 - Iron 40%+
 - Sulphur 40-50%
 - Arsenopyrite
 - Arsenic 33%+

- Iron 25-30%
- Sulphur 35-40%
- Chalcopyrite
 - Copper 35%+
 - Iron 15-20%
 - Sulphur 35-45%
- Sphalerite
 - Zinc 50%+
- Galena
 - Lead 85-90%
- Calcite
 - Calcium carbonate 80%+
- Siderite
 - Iron carbonate 75%+
- Quartz
 - Silica 90%+
- Feldspars
 - Individual oxides (K, Na, Ca) 60%+
- Montmorillonite
 - Total Al and Ca oxides 12%+
- Kaolinite
 - Aluminum 38-45%
 - Silicon 46-52%

3. Flowsheet Selection

- Database retrieves relevant flowsheet based on:
 - Ore type
 - Grade & size ranges
 - Key mineral makeup

4. Process Models

A. Cyanidation

Rate of Gold Dissolution:

$$d[\text{Au}]/dt = k[\text{Au}][\text{CN}^-]$$

Where:

$$k = A \cdot \exp(-E_a/RT)$$

Arrhenius Equation:

$$k = A \cdot \exp(-E_a/RT)$$

The rate constant k is calculated using the Arrhenius equation:

$$k = A \cdot \exp(-E_a/RT)$$

Where:

A = pre-exponential factor, typically 10¹¹ m³/g-min

E_a = activation energy, usually 50 kJ/mol

R = universal gas constant, 8.314 J/mol-K

T = temperature in Kelvin

Carbon Adsorption:

Langmuir Equation:

$$q = (q_{\max} \cdot b \cdot C) / (1 + b \cdot C)$$

B. Flotation

Collection Efficiency:

$$\alpha = 1 / (1 + \exp((E_b/kT)))$$

DLVO Theory:

$$E_b = E_{vdw} + E_{edl}$$

$$E_{vdw} = -A \cdot (H_1 \cdot H_2 / (H_1 + H_2))$$

$$E_{edl} = (2 \cdot \pi \cdot \epsilon_0 \cdot \epsilon_r \cdot \zeta_1 \cdot \zeta_2) \cdot \exp(-\kappa \cdot H) / (1 + \kappa \cdot H)$$

For the E_{vdw} term:

$$-A \cdot (H_1 \cdot H_2 / (H_1 + H_2))$$

The Hamaker constant (A) can range from 10⁻²⁰ to 10⁻²⁰ Joules.

Particle size (H₁) is usually 1-100 μm.

Bubble size (H₂) is typically 50-200 μm.

For the E_{edl} term:

$$(2 \cdot \pi \cdot \epsilon_0 \cdot \epsilon_r \cdot \zeta_1 \cdot \zeta_2) \cdot \exp(-\kappa \cdot H) / (1 + \kappa \cdot H)$$

The permittivity of free space (ϵ_0) is a constant at $8.85 \times 10^{-12} \text{ C}^2/\text{N}\cdot\text{m}^2$.

The relative permittivity (ϵ_r) of process water ranges from 2-10.

Zeta potentials (ζ_1 and ζ_2) on particle and bubble surfaces usually fall between ± 10 -100 mV.

The inverse Debye length (κ) is commonly 10^8 - 10^{10} m^{-1} .

The separation distance (H) in colloid systems is on the nanoscale, around 1-1000 nm.

C implicitly using the integrated rate law formula:

$$C = C^* - (C^* - C_0)e^{-kt}$$

Where:

C_0 = initial concentration in pulp/feed

C^* = equilibrium/maximum concentration (65-90% of the head grade.)

k = rate constant from Arrhenius equation

t = time.

C. Gravity

Particle Settling:

$$v = g(\rho_p - \rho_f) / 18\mu \cdot d^2$$

The variables are:

v = terminal settling velocity

g = acceleration due to gravity, 9.81 m/s^2

ρ_p = particle density, 2500 - 4000 kg/m^3

ρ_f = fluid density, approximately 1000 kg/m^3

μ = fluid viscosity, ranging from 0.0005-0.005 $\text{Pa}\cdot\text{s}$

d = particle diameter

D. Heap/CIL/CIP

Leaching:

Same as cyanidation above

Dynamic Tank Model:

$$dV/dt = F_{in} - F_{out}$$

$$dC/dt = (F_{in}C_{in} - F_{out}C_{out})/V + R - kC$$

Dynamic Tank Model:

$$dV/dt = F_{in} - F_{out}$$

F_{in} = Inlet flow rate (m³/hr)

Range: Depends on tank size, usually 0.5-50 m³/min or 50-5000 m³/hr

F_{out} = Outlet flow rate

Calculated from volume and residence time (5-60 min typical)

$$dC/dt = (F_{in}C_{in} - F_{out}C_{out})/V + R - kC$$

C_{in} = metal concentration entering tank (g/L)

Ranges: 0.1-10 g/L

C_{out} = metal concentration leaving tank (g/L)

Calculated based on recovery performance

V = volume in tank (m³)

Ranges: 10-1000 m³

R = metal recovery/extraction rate (g/L-hr)

Estimated using leach kinetics rate equations

k = metal dissolution/desorption rate constant (1/hr)

Ranges: 0.001-0.1 1/hr

Carbon Contact:

Forward: k_1CQ

k_1 range: 0.005 - 0.015 L/g-min

Reverse: $k_{-1}Q$

k_{-1} range: 0.0025 - 0.0075 1/min

For carbon saturation Q :

$$Q = Q_0 * e^{(-k_3 * t)}$$

Q_0 range: 50 - 150 mg metal/g carbon

k_3 range: 0.0005 - 0.0015 1/min

t is time elapsed.

The C concentration in the dynamic tank model is calculated from:

$$C = C^* - (C^* - C_0)e^{-kt}$$

C_0 range: Head grade +/- 20%

C^* range: 70-95% of C_0

k from Arrhenius equation: $A=1011$, $E_a=30-80$ kJ/mol

E. Comminution:

$$\text{- Bond Work Index (kWh/t)} = 13.048 * (P_{80})^{-0.4915}$$

5.

Comminution:

$$R_{\text{comminution}} = 100 * (1 - e^{(-k_{\text{comminution}} * t)})$$

$$\text{where } k_{\text{comminution}} = A * e^{(-E_a/(R * T))}$$

Cyanidation:

$$R_{\text{cyanidation}} = 100 * (1 - e^{(-k_{\text{cyanidation}} * t)})$$

$$\text{where } k_{\text{cyanidation}} = A * e^{(-E_a/(R * T))}$$

Flotation:

$$R_{\text{flotation}} = 100 * (1 - e^{(-k_{\text{flotation}} * t)})$$

$$\text{where } k_{\text{flotation}} = 1 / (1 + e^{((-A * (H_1 * H_2) / (H_1 + H_2)) + (2 * \pi * \epsilon_0 * \epsilon_r * \zeta_1 * \zeta_2) * e^{(-\kappa * H) / (1 + \kappa * H)) / (k * T)})}$$

Carbon Adsorption:

$$R_{\text{adsorption}} = 100 * (1 - e^{(-k_{\text{adsorption}} * t)})$$

$$\text{where } k_{\text{adsorption}} = (q_{\text{max}} * b * C) / (1 + b * C)$$

Heap/CIL/CIP Leaching:

$$R_{\text{leaching}} = 100 * (1 - e^{(-k_{\text{leaching}} * t)})$$

where $k_{\text{leaching}} = A * e^{(-E_a/(R*T))}$

Gravity Separation:

$R_{\text{gravity}} = 100 * (1 - e^{(-k_{\text{gravity}} * t)})$

where $k_{\text{gravity}} = \alpha * (g * (\rho_p - \rho_f) * d^2) / (18 * \mu)$

Total Recovery Rate:

$$R_t = R_c + R_{\text{cyan}} + R_f + R_a + R_l + R_g - R_c * R_{\text{cyan}} - R_c * R_f - R_c * R_l - R_c * R_g - R_{\text{cyan}} * R_f - R_{\text{cyan}} * R_l - R_{\text{cyan}} * R_g - R_f * R_l - R_f * R_g - R_l * R_g + R_c * R_{\text{cyan}} * R_f + R_c * R_{\text{cyan}} * R_l + R_c * R_{\text{cyan}} * R_g + R_c * R_f * R_l + R_c * R_f * R_g + R_c * R_l * R_g + R_c * R_f * R_l + R_{\text{cyan}} * R_f * R_g + R_{\text{cyan}} * R_f * R_g + R_f * R_l * R_g - R_c * R_{\text{cyan}} * R_f * R_l - R_c * R_{\text{cyan}} * R_f * R_g - R_c * R_{\text{cyan}} * R_l * R_g - R_c * R_{\text{cyan}} * R_l * R_g - R_c * R_{\text{cyan}} * R_f * R_l * R_g + R_c * R_{\text{cyan}} * R_f * R_l * R_g$$

Constants:

- Gravity recovery limits = 95-98%
- Leach residence times = 6-72 hrs
- Equipment throughputs in tph
- Bond Work Index ranges by ore type = 10-18 kWh/t
- Carbon loading capacities = 25-50 g Au/t
- Reagent consumptions per tonne of ore

Parameters:

- Rate constants (k) from batch tests = 0.01-1 hr⁻¹
- Process water requirements in m³/hr
- Energy inputs by unit operation

6. Total Recovery Projection

- Monte Carlo simulations varying inputs 1000 times
- Returns mean, standard deviation, confidence intervals

7. Optimization Simulation

- Adjusts parameters over ranges to maximize recovery