(1.1) yapyapyap

(2.1) The ordinary differential equation (ODE) governing the temperature T(t) is:

$$\frac{dT(t)}{dt} = \frac{Q_f(t) - UA(T(t) - T_a)}{\rho V c_p}$$

For this problem, the furnace is off, so $Q_f(t) = 0$. Substituting this into the equation:

$$\frac{dT(t)}{dt} = \frac{-UA(T(t) - T_a)}{\rho V c_p}$$

At steady state, the temperature T(t) no longer changes with time, so:

$$\frac{dT(t)}{dt} = 0$$

Substitute this condition into the ODE:

$$0 = \frac{-UA(T(t) - T_a)}{\rho V c_p}$$

Solve:

$$T(t) - T_a = 0$$

Thus:

$$T(t) = T_a$$

(2.2) Using the dervied equation for T(t), the behaviour of the furnace as defined below, and the given definition of one step of the univariate Euler's method, we can plot Figure 1.

$$Q_f(t) = \begin{cases} 0 & \text{When } T(t) > 23^{\circ}\text{C}, \\ 1.5 \times 10^6 & \text{When } T(t) < 17^{\circ}\text{C}, \\ \text{unchanged} & \text{For all } 17 \le T(t) \le 23^{\circ}\text{C}. \end{cases}$$

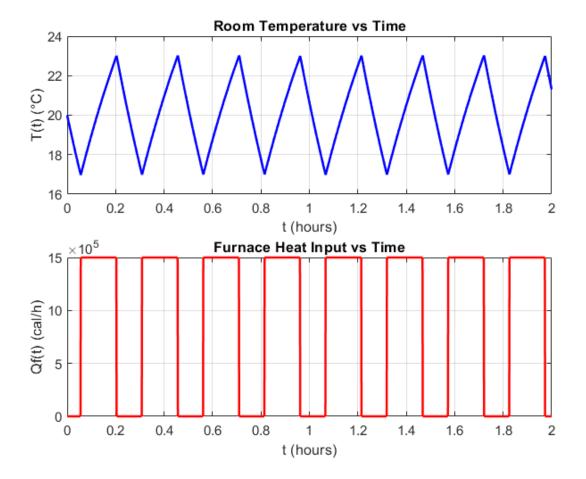


Figure 1: Temperature and Furnace Input Over Time

(2.3) To calculate the number of standard cubic meters of natural gas consumed, we follow the below equation:

Define $t_{on} \triangleq$ time the furnace was on in hours. The Matlab code says it was 1.182 hours

Define $Q_{f,on} \triangleq$ as the furnace heat input. Define $\rho_e \triangleq$ as the energy density. Define $e \triangleq$ as the efficiency.

Volume of gas consumed =
$$\frac{t_{on}Q_{f,\text{on}}}{\rho_e e} = \frac{(1.182)(1.5 \times 10^6)}{(9 \times 10^6)(0.9)} = 0.2188888$$

 $\approx 0.219 \text{ standard cubic meters}$

We also confirm with unit analysis that we get cubic meters.

Volume of gas consumed =
$$\frac{t_{\text{on}}Q_{f,\text{on}}}{\rho_e e} = \frac{\text{hour} \cdot \frac{\text{cal}}{\text{hour}}}{\frac{\text{cal}}{\text{m}^3}} = \text{m}^3$$

- (2.4) With a new oscillating defintion of Ta, we get Figure 2 below demonstrating the temperature and furnace input over time.
 - The simulation results align with the expected behavior of the system. The room temperature T(t) is maintained within the desired range of 17°C to 23°C as the furnace responds to changes in the ambient temperature $T_a(t)$. When $T_a(t)$ is lower, the furnace operates more frequently to offset increased heat loss, while at higher $T_a(t)$, the furnace operates less often due to reduced heat loss. This behavior reflects the thermal dynamics of the system and the influence of the bang-bang control logic.

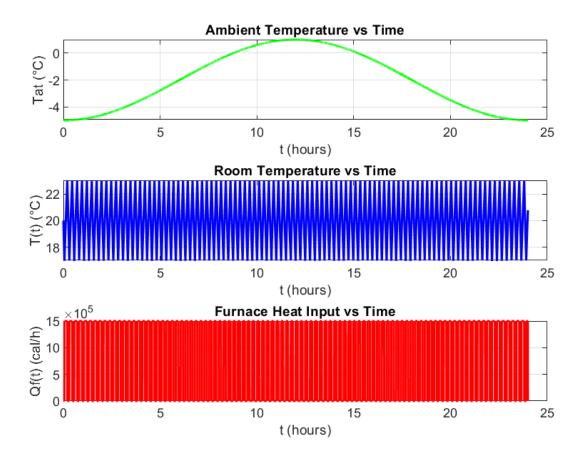


Figure 2: Temperature and Furnace Input Over Time

(3.1) We are given the following ODE describing the current going thorugh the system.

$$V_s(t) = Ri(t) + L\frac{di(t)}{dt}$$

During steady state, the current i(t) is constant, so the derivative of i(t) with respect to time is zero. Substituting this into the ODE:

$$V_s(t) = Ri(t) + L(0)$$

Rearranging, we get the following equation for i(t):

$$i(t) = \frac{V_s(t)}{R}$$

This is useful when designing a cirtcuit with a target current i(t) because you can control the voltage source to achieve the desired current while the resistance will always be a constant property of the circuit's hardware.

(3.2) Part B SOLUTION

- (4.1) Part A SOLUTION
- (4.2) Part B SOLUTION

- (5.1) Part A SOLUTION
- (5.2) Part B SOLUTION