

{Section 1}

{Given for Current System}

mdot_ref=62.99[g/s]
 P=2403[W] {Power at typical operating conditions}
 P_2=2420[kPa] {high-side operating temp}
 T_4=5[C] {Evaporator temperature}

{Assumptions}

x_1=1
 T_1=T_4
 s_2s=s_1
 P_3=P_2
 P_2s=P_2
 h_4=h_3
 x_3=0 {Subcooled not saturated}

{Design Variables}

electricityPrice=0.1072[\$/kWh]
 opperatingHours=240[hr]
 houseSize=830[ft^2]

{Solving}

h_1=enthalpy(R410A,T=T_1,x=x_1)
 P=mdot_ref*(h_2-h_1)
 s_1=entropy(R410A,T=T_1,x=x_1)
 h_2s=enthalpy(R410A,s=s_2s,P=P_2s)
 efficiency_isentropic=(h_2s-h_1)/(h_2-h_1)*100

h_3=enthalpy(R410A,P=P_3,x=x_3)
 COP=(h_1-h_4)/(h_2-h_1)

cost_hour=P*convert(W,kW)*electricityPrice
 cost_month=cost_hour*opperatingHours

capacity=mdot_ref*(h_1-h_4)*convert(kJ,J)/convert(kg,g)
 capacity_required=houseSize*25*convert(Btu/hr,W)

SOLUTION

Unit Settings: SI C kPa kJ mass deg

capacity = 9876 [W]
 COP = 4.11
 costmonth = 61.82 [\$/month]
 electricityPrice = 0.1072 [\$/kWh]
 h1 = 422.8 [kJ/kg]
 h2s = 448.5 [kJ/kg]
 h4 = 266 [kJ/kg]
 opperatingHours = 240 [hr]
 P2 = 2420 [kPa]
 P3 = 2420 [kPa]
 s2s = 1.801 [kJ/kg-K]
 T4 = 5 [C]
 x3 = 0

capacityrequired = 6081 [W]
 costhour = 0.2576 [\$/hr]
 efficiencyisentropic = 67.22 [%]
 houseSize = 830 [ft^2]
 h2 = 461 [kJ/kg]
 h3 = 266 [kJ/kg]
 mdotref = 62.99 [g/s]
 P = 2403 [W]
 P2s = 2420 [kPa]
 s1 = 1.801 [kJ/kg-K]
 T1 = 5 [C]
 x1 = 1

3 potential unit problems were detected.

KEY VARIABLES

capacity = 9876 [W]
 efficiencyisentropic = 67.22 [%]

COP = 4.11