

# Memo

# Volume shift for generic EOS

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## 1 Introduction

The volume shift was introduced by Péneloux et al. [7],

$$c = \frac{1}{n} \sum_{i} c_i n_i,\tag{1}$$

where  $c_i$  is a component constant representing the component volume shift.

Different properties change when working with volume translations, see Jaubert et al. [3] for details.

The volume-shift have found application in many cubic based equations of state (t-mPR[5], PSRK[2], VTPR[1], tc-PR/tc-RK[6], ...), and the component volume translations  $c_i$ , are often fixated to match the liquid density at  $T = 0.7T_{\text{Crit}}$ ,

# 2 Volume shifts for generic EOS

The residual reduced Helmholtz function of a generic EOS is found as follows,

$$F(T, V_{\text{eos}}, \boldsymbol{n}) = \frac{A^{\text{r}}(T, V_{\text{eos}}, \boldsymbol{n})}{RT} = \int_{V_{\text{eos}}}^{\infty} \left[ \frac{P(T, V'_{\text{eos}}, \boldsymbol{n})}{RT} - \frac{n}{V'_{\text{eos}}} \right] dV'_{\text{eos}}$$
(2)

Introducing the volume shift,

$$V = V_{\text{eos}} - \sum n_i c_i = V_{\text{eos}} - C, \tag{3}$$

The residual reduced helmholtz of the volume-shifted (vs) EOS can be found, using  $dV = dV_{eos}$  at constant n and T,

$$F^{\text{vs}}(T, V, \boldsymbol{n}) = \int_{V}^{\infty} \left[ \frac{P(T, V' + C, \boldsymbol{n})}{RT} - \frac{n}{V'} \right] dV'$$
(4)

$$= \int_{V}^{\infty} \left[ \frac{P(T, V' + C, \boldsymbol{n})}{RT} - \frac{\boldsymbol{n}}{V' + C} \right] dV' + n \int_{V}^{\infty} \left[ \frac{1}{V' + C} - \frac{1}{V'} \right] dV' \tag{5}$$

$$= \int_{V_{\text{eos}}}^{\infty} \left[ \frac{P(T, V_{\text{eos}}', \boldsymbol{n})}{RT} - \frac{n}{V_{\text{eos}}'} \right] dV_{\text{eos}}' + n \int_{V}^{\infty} \left[ \frac{1}{V' + C} - \frac{1}{V'} \right] dV'$$
 (6)

$$= F(T, V_{\text{eos}}, \boldsymbol{n}) + n \ln \left(\frac{V}{V_{\text{eos}}}\right) \tag{7}$$



Here we need to treat  $V_{\text{eos}} = V_{\text{eos}}(V, \boldsymbol{n})$  with the chain rule when differentiating  $F^{\text{vs}}$ .

If we introduce  $F^{C}$  as the corrected residual reduced Helmholtz energy, due to the difference in ideal volume,

$$F^{C}(V, \boldsymbol{n}) = n \ln \left(\frac{V}{V + C}\right), \tag{8}$$

the differentials can be derived in a organized manner.

$$F_V^C = n\left(\frac{1}{V} - \frac{1}{V+C}\right) = n\left(\frac{1}{V} - \frac{1}{V_{\text{eos}}}\right),\tag{9}$$

$$F_{VV}^{C} = n\left(-\frac{1}{V^{2}} + \frac{1}{(V+C)^{2}}\right) = n\left(-\frac{1}{V^{2}} + \frac{1}{V_{\text{eos}}^{2}}\right),\tag{10}$$

$$F_i^C = \ln\left(\frac{V}{V+C}\right) - \frac{nc_i}{V+C} = \ln\left(\frac{V}{V_{\text{eos}}}\right) - \frac{nc_i}{V_{\text{eos}}},\tag{11}$$

$$F_{ij}^{C} = -\frac{(c_j + c_i)}{V + C} + \frac{nc_i c_j}{(V + C)^2} = -\frac{(c_j + c_i)}{V_{\text{eos}}} + \frac{nc_i c_j}{V_{\text{eos}}^2},$$
(12)

$$F_{Vi}^{C} = \frac{1}{V} - \frac{1}{V+C} + \frac{nc_i}{(V+C)^2} = \frac{1}{V} - \frac{1}{V_{\text{eos}}} + \frac{nc_i}{V_{\text{eos}}^2}$$
(13)

In addition the compositional differentials change for since  $V_{\text{eos}} = V + C$ ,

$$F_i^{\text{eos}} = F_i^{\text{eos}} + F_{V_{\text{eos}}}^{\text{eos}} c_i, \tag{14}$$

$$F_{Ti}^{\text{eos}} = F_{Ti}^{\text{eos}} + F_{TV_{\text{cos}}}^{\text{eos}} c_i, \tag{15}$$

$$F_{Ti}^{\text{eos}} = F_{Ti}^{\text{eos}} + F_{TV_{\text{eos}}}^{\text{eos}} c_i,$$

$$F_{ij}^{\text{eos}} = F_{ij}^{\text{eos}} + F_{iV_{\text{eos}}}^{\text{eos}} c_j + F_{V_{\text{eos}}j}^{\text{eos}} c_i + F_{V_{\text{eos}}V_{\text{eos}}}^{\text{eos}} c_i c_j.$$

$$(15)$$

#### 2.1Test of the fugacity coefficient

Let us test this for the fugacity coefficient. It is defined as

$$\ln \hat{\varphi}_i^{\text{vs}} = \left(\frac{\partial F^{\text{vs}}}{\partial n_i}\right)_{T,V,n_i} - \ln(Z) = F_{n_i}^{\text{vs}} - \ln(Z)$$
(17)

Differentiating  $F^{vs}$ ,

$$F_{n_i}^{\text{vs}} = F_{n_i} + F_{V_{\text{eos}}} c_i + \ln\left(\frac{V}{V_{\text{eos}}}\right) - \frac{nc_i}{V_{\text{eos}}} = F_{n_i} + \ln\left(\frac{V}{V_{\text{eos}}}\right) - \frac{Pc_i}{RT}$$
(18)

Combining Equation 17 and 18, we get

$$\ln \hat{\varphi}_i^{\text{vs}} = F_{n_i} + \ln \left( \frac{V}{V_{\text{eos}}} \right) - \frac{Pc_i}{RT} - \ln \left( \frac{PV}{nRT} \right)$$
 (19)

$$= F_{n_i} - \ln\left(\frac{PV_{\text{eos}}}{nRT}\right) - \frac{Pc_i}{RT} \tag{20}$$

$$= \ln \hat{\varphi}_i - \frac{Pc_i}{RT} \tag{21}$$

which is the same result as reported by Péneloux et al.



# 3 Correlations used for $c_i$

The  $c_i$  for the SRK EOS is calculated from the following equation:

$$c_i = 0.40768 \frac{RT_{c_i}}{P_{c_i}} (0.29441 - Z_{RA})$$
(22)

 $Z_{\rm RA}$  are tabulated in TPlib. Reid et al. [8] also correlate  $Z_{\rm RA}$  as follows:

$$Z_{\rm RA} = 0.29056 - 0.08775\omega \tag{23}$$

Jhaveri and Youngren [4] have developed different paramaters for the PR EOS:

$$c_i^{\text{PR}} = 0.50033 \frac{RT_{c_i}}{P_{c_i}} (0.25969 - Z_{\text{RA}})$$
 (24)



### References

- [1] Eileen Collinet and Jürgen Gmehling. Prediction of phase equilibria with strong electrolytes with the help of the volume translated Peng-Robinson group contribution equation of state (VTPR). Fluid Phase Equilibria, 246(1-2):111 118, 2006.
- [2] K. Fischer and J. Gmehling. Further development, status and results of the PSRK method for the prediction of vapor-liquid equilibria and gas solubilities. *Fluid Phase Equilibria*, 121(1-2):185 206, 1996.
- [3] Jean-Noël Jaubert, Romain Privat, Yohann [Le Guennec], and Lucie Coniglio. Note on the properties altered by application of a péneloux-type volume translation to an equation of state. Fluid Phase Equilibria, 419:88 95, 2016.
- [4] B. S. Jhaveri and G. K. Youngren. Three-parameter modification of the peng-robinson equation of state to improve volumetric predictions. *SPE Reservoir Engineering*, 8:1033 1040, 1988.
- [5] Aris Kordas, Kostis Magoulas, Sofia Stamataki, and Dimitrios Tassios. Methane-hydrocarbon interaction parameters correlation for the Peng-Robinson and the t-mPR equation of state. Fluid Phase Equilibria, 112(1):33 44, 1995.
- [6] Yohann Le Guennec, Romain Privat, and Jean-Noël Jaubert. Development of the translated-consistent tc-PR and tc-RK cubic equations of state for a safe and accurate prediction of volumetric, energetic and saturation properties of pure compounds in the sub-and super-critical domains. Fluid Phase Equilibria, 429:301–312, 2016.
- [7] André Péneloux, Evelyne Rauzy, and Richard Fréze. A consistent correction for Redlich-Kwong-Soave volumes. Fluid Phase Equilibria, 8(1):7 23, 1982.
- [8] R. C. Reid, J. M. Prausnitz, and B. E. Poling. *The properties of gases & liquids*. McGraw-Hill, Inc., USA, 4 edition, 1987.