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# Memo

# Wong-Sandler equation of state

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#### 1 Introduction

Derivation of the Wong-Sandler first and second differentials needed for thermopack implementation[5]. The appendix of the Wong-Sandler paper contain parameter definitions and first order differentials with respect to mole numbers for the Peng-Robinson equation of state.



### 2 Infinite pressure limit of the equations of state

To determine the *C* parameter of equation A3 and A4, the pressure limit of the equation of state must be found.

Table 1: Different equations of state

Year:	Name:	Functional form:
1873	Van der Waals	$P = \frac{RT}{v - b} - \frac{a}{v^2}$
1949	Redlich Kwong	$P = \frac{RT}{\nu - b} - \frac{a/T^{0.5}}{\nu(\nu + b)}$
1972	Soave Redlich Kwong	$P = \frac{RT}{v - b} - \frac{\alpha(T)a}{v(v + b)}$
1976	Peng Robinson	$P = \frac{RT}{\nu - b} - \frac{\alpha(T)a}{\nu(\nu + b) + b(\nu - b)}$
1980	Schmidt-Wensel	$P = \frac{RT}{v - b} - \frac{\alpha(T)a}{v^2 + (1 + 3c)bv - 3cb^2}$
1982	Patel Teja	$P = \frac{RT}{v-b} - \frac{\alpha(T)a}{v(v+b)+c(v-b)}$
1987	Yu-Lu	$P = \frac{RT}{v-b} - \frac{\alpha(T)a}{v(v+b) + b(3v+c)}$
1987	Trebble-Bishnoi	$P = \frac{RT}{\nu - b} - \frac{\alpha(T)a}{\nu^2 + (b(T) + c)\nu - b(T)c - d^2}$

$$P = \frac{nRT}{V - B} - \frac{A}{(V - B(T)m_1)(V - B(T)m_2)}$$
(1)

Table 2: Equation of state parameters

Name:	$m_1$	$m_2$
Van der Waals:	0	0
Redlich Kwong:	0	-1
Soave Redlich Kwong:	0	-1
Peng Robinson:	$-1+\sqrt{2}$	$-1-\sqrt{2}$
Schmidt-Wensel	$\frac{-1 - 3w + \sqrt{1 + 18w + 9w^2}}{2}$	$\frac{-1 - 3w - \sqrt{1 + 18w + 9w^2}}{2}$
Patel Teja:	$\frac{-b-c+\sqrt{b^2+2bc+c^2+4bc}}{2b}$	$\frac{-b-c-\sqrt{b^2+2bc+c^2+4bc}}{2b}$
Yu-Lu	$\frac{-c-3b+\sqrt{c^2+2bc+9b^2}}{2b}$	$\frac{-c-3b-\sqrt{c^2+2bc+9b^2}}{2b}$
Trebble-Bishnoi	$\frac{-b(T)-c+\sqrt{b(T)^2+6b(T)c+c^2+4d}}{2b(T)}$	$\frac{-b(T) - c - \sqrt{b(T)^2 + 6b(T)c + c^2 + 4d}}{2b(T)}$

The residual Helmholtz function, F, becomes

$$F(T, V, \mathbf{n}) = n \left[ \ln \left( \frac{V}{V - B} \right) - \frac{A}{(m_1 - m_2) BRT} \ln \left( \frac{V - m_2 B}{V - m_1 B} \right) \right]. \tag{2}$$

In order to find the pressure limit, we use that,

$$F(T, P, \mathbf{n}) = F(T, V, \mathbf{n}) - \ln(Z), \tag{3}$$

where Z = PV/(nRT). We then get,

$$F(T, P, \mathbf{n}) = n \left[ -\ln \left( \frac{P(V - B)}{nRT} \right) - \frac{A}{(m_1 - m_2)BRT} \ln \left( \frac{V - m_2 B}{V - m_1 B} \right) \right]. \tag{4}$$

From 1 we see

$$\lim_{P \to \infty} \frac{P(V - B)}{nRT} = 1 \tag{5}$$



We therefore get

$$\lim_{P \to \infty} F(T, P, \mathbf{n}) = \frac{nA}{BRT} \frac{1}{(m_1 - m_2)} \ln \left( \frac{B - m_1 B}{B - m_2 B} \right) = \frac{nAC}{BRT},\tag{6}$$

where *C* is given as follows,

$$C = \frac{1}{(m_1 - m_2)} \ln \left( \frac{1 - m_1}{1 - m_2} \right). \tag{7}$$

Table 3: Equation of state *C*-parameter

EOS	С
Van der Waals	-1
Redlich Kwong	-ln 2
Soave Redlich Kwong	-ln 2
Peng Robinson	$\frac{1}{\sqrt{2}}\ln\left(\sqrt{2}-1\right)$
Otherwise	Úse Eq. 7

### 3 The Wong-Sandler mixing rule

The Wong-Sandler mixing rule give a relation between the *B* and *A* parameter of the equation of state. In effect the *B* parameter become temperature dependent.

$$B = \frac{Q}{n - D} \tag{8}$$

$$B(n-D) = Q (9)$$

$$\frac{A}{RT} = BD \tag{10}$$

$$A = BDRT \tag{11}$$

Q is defined as follows,

$$Q = \sum_{i} \sum_{j} n_{i} n_{j} \left( b - \frac{a}{RT} \right)_{ij}, \tag{12}$$

where

$$\left(b - \frac{a}{RT}\right)_{i,i} = \frac{\left(b_i - \frac{a_i(T)}{RT}\right) + \left(b_j - \frac{a_j(T)}{RT}\right)}{2} \left(1 - k_{ij}(T)\right), \tag{13}$$

and

$$a_i(T) = \tilde{a}_i \alpha(T), \tag{14}$$



To simplify the differentials, we introduce  $r_i$ ,

$$r_i = \left(b_i - \frac{a_i(T)}{RT}\right),\tag{15}$$

$$r_{i,T} = -\frac{a_{i,T}}{RT} + \frac{a_i}{RT^2},\tag{16}$$

$$r_{i,TT} = -\frac{a_{i,TT}}{RT} + \frac{2a_{i,T}}{RT^2} - \frac{2a_i}{RT^3}.$$
 (17)

(18)

D is defined as,

$$D = \sum_{i} n_i \frac{a_i}{b_i RT} + \frac{A_{\infty}^{E}}{CRT}$$
 (19)

#### 4 Partial differentials

### 4.1 Temperature differentials

Differentiating 9 with respect to *T* gives:

$$B_T(n-D) - BD_T = Q_T \tag{20}$$

$$B_T = \frac{Q_T + BD_T}{n - D} \tag{21}$$

Further differentiating 20 with respect to *T* gives:

$$B_{TT}(n-D) - 2B_TD_T - BD_{TT} = Q_{TT}$$

$$\Leftrightarrow \qquad (22)$$

$$B_{TT} = \frac{Q_{TT} + 2B_T D_T + BD_{TT}}{n - D} \tag{23}$$

Differentiating 11 with respect to *T* gives:

$$A_T = B_T DRT + BD_T RT + BDR (24)$$

(25)

Further differentiating 24 with respect to *T* gives:

$$A_{TT} = B_{TT}DRT + 2B_TD_TRT + 2B_TDR + 2BD_TR + BD_{TT}RT$$
 (26)

Differentiating 12, gives,

$$Q_T = \sum_{i} \sum_{j} n_i n_j \left( \frac{\left(r_{i,T} + r_{j,T}\right) \left(1 - k_{ij}\right)}{2} - \frac{r_i + r_j}{2} k_{ij,T} \right), \tag{27}$$

$$Q_{TT} = \sum_{i} \sum_{j} n_{i} n_{j} \left( \frac{\left(r_{i,TT} + r_{j,TT}\right) \left(1 - k_{ij}\right)}{2} - \left(r_{i,T} + r_{j,T}\right) k_{ij,T} \right)$$
(28)

$$-\frac{r_i+r_j}{2}k_{ij,TT}\Big),\tag{29}$$



Differentiating 19, gives,

$$D_T R T + D R = \sum_i n_i \frac{a_{i,T}}{b_i} + \frac{A_{\infty,T}^{\mathcal{E}}}{C}, \tag{30}$$

$$D_{T} = \frac{\sum_{i} n_{i} \frac{a_{i,T}}{b_{i}} + \frac{A_{\infty,T}^{E}}{C} - DR}{RT}.$$
(31)

Differentiating 30 further gives,

$$D_{TT}RT + 2D_{T}R = \sum_{i} n_{i} \frac{a_{i,TT}}{b_{i}} + \frac{A_{\infty,TT}^{E}}{C},$$

$$(32)$$

$$D_{TT} = \frac{\sum_{i} n_{i} \frac{a_{i,TT}}{b_{i}} + \frac{A_{\infty,TT}^{E}}{C} - 2D_{T}R}{RT}.$$
(33)

#### 4.2 Mole number differentials

Differentiating 9 with respect to  $n_i$  gives:

$$B_i(n-D) + B(1-D_i) = Q_i$$

$$\Leftrightarrow (34)$$

$$B_i = \frac{Q_i + B(D_i - 1)}{n - D} \tag{35}$$

Further differentiating 34 with respect to  $n_i$  gives:

$$B_{ij}(n-D) + B_i(1-D_j) + B_j(1-D_i) - BD_{ij} = Q_{ij}$$

$$\Leftrightarrow$$
(36)

$$\frac{Q_{ij} + B_i(D_j - 1) + B_j(D_i - 1) + BD_{ij}}{n - D} = B_{ij}$$
(37)

Differentiating 11 with respect to  $n_i$  gives:

$$A_i = RT \left( B_i D + B D_i \right) \tag{38}$$

(39)

Further differentiating 38 with respect to  $n_j$  gives:

$$A_{ij} = RT \left( B_{ij}D + B_iD_j + B_jD_i + BD_{ij} \right) \tag{40}$$

Differentiating 12, with respect to  $n_i$  and thereafter  $n_j$  gives,

$$Q_i = 2\sum_j n_j \left(b - \frac{a}{RT}\right)_{ij},\tag{41}$$

$$Q_{ij} = 2\left(b - \frac{a}{RT}\right)_{ij}. (42)$$



Differentiating Equation 19 with respect to  $n_i$  gives,

$$D_i RT = \frac{a_i}{b_i} + \frac{A_{\infty,i}^{\rm E}}{C}.$$
 (43)

Differentiating 43 further with respect to  $n_j$  gives,

$$D_{ij}RT = \frac{A_{\infty,ij}^{E}}{C}. (44)$$

#### 4.3 Cross differentials

Differentiating 34 with respect to *T* gives:

$$B_{iT}(n-D) - B_i D_T + B_T (1-D_i) - B D_{iT} = Q_{iT}$$
(45)

$$\frac{Q_{iT} + B_i D_T + B_T (D_i - 1) + B D_{iT}}{n - D} = B_{iT}$$
 (46)

Differentiating 38 with respect to *T* gives:

$$A_{iT} = R (B_{iT}DT + B_{i}D_{T}T + B_{i}D + B_{T}D_{i}T + BD_{i}T + BD_{i})$$
(47)
(48)

Differentiating 41, with respect to T gives,

$$Q_{iT} = 2\sum_{j} n_{j} \left( \frac{\left( r_{i,T} + r_{j,T} \right) \left( 1 - k_{ij} \right)}{2} - \frac{r_{i} + r_{j}}{2} k_{ij,T} \right). \tag{49}$$

(50)

Differentiating Equation 43 with respect to T gives,

$$D_{iT}RT + D_{i}R = \frac{a_{i,T}}{b_{i}} + \frac{A_{\infty,iT}^{E}}{C}.$$
(51)

$$D_{iT} = \frac{\frac{a_{i,T}}{b_i} + \frac{A_{\infty,iT}^{E}}{C} - D_i R}{RT}.$$
 (52)

## 5 The NRTL infinite free energy model

The NRTL model [2]:

$$\frac{A_{\infty}^{\rm E}}{RT} = \sum_{i} n_{i} \left( \frac{\sum_{j} n_{j} \tau_{ji} g_{ji}}{\sum_{k} n_{k} g_{ki}} \right), \tag{53}$$

where

$$g_{ij}(T) = \exp\left(-\alpha_{ij}\tau_{ij}(T)\right). \tag{54}$$



Looking at the NRTL model it is very similar to the Huron-Vidal model (HV) [1],

$$\frac{G_{\infty}^{E}}{RT} = \sum_{i} n_{i} \left( \frac{\sum_{j} n_{j} b_{j} \tau_{ji} g_{ji}}{\sum_{k} n_{k} b_{k} g_{ki}} \right). \tag{55}$$

Comparing equation 55 and equation 53, the substitution  $b_j g_{ji}^{HV} = g_{ji}^{NRTL}$  can be made, that lets us reuse the existing HV implementation. For the combination of NRTL for some binaries and simple van der Waals mixing for other binaries, the following can be done,

$$g_{ji} = b_j, (56)$$

$$\beta_{ii} = \frac{a_i}{b_i}C, \tag{57}$$

$$\beta_{ii} = \frac{a_i}{b_i}C, \qquad (57)$$

$$\beta_{ji} = -\frac{\sqrt{b_i b_j}}{b_{ij}} \sqrt{\beta_{ii}\beta_{jj}} (1 - k_{ij}), \qquad (58)$$

$$\tau_{ji} = \frac{\beta_{ji} - \beta_{ii}}{RT}. (59)$$

This follows from the relations for HV described in [4]. Alternatively the relations developed by [3], can be used.

#### 5.1 **Differentials**

Follows the approach above, the differentials are already available from [4].



#### References

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