

NATURALLY OCCURRING SUBSTANCE (*CALENDULA OFFICINALIS*- FLOWER) AS A CORROSION INHIBITOR OF MILD STEEL IN 1M HCl SOLUTION

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ABSTRACT

The influence of '*Calendula officinalis*' towards the corrosion of mild steel in 1M HCl has been evaluated by weight loss method and polarization technique. The results showed that *Calendula officinalis* is a very good inhibitor for mild steel in this medium. The inhibition efficiency of the compound was found to vary with the concentration of the inhibitor (0.001 to 0.5 % w/v), immersion time 1hr-24 hr) and temperature (40°C – 70°C). Good inhibition efficiency was found at 0.5% (w/v) concentration of the inhibitor for 2hours (94.67%). Thermodynamic parameters were calculated to investigate the mechanism of corrosion inhibition. The adsorption of the inhibitor on mild steel surface was found to obey Temkin and Langmuir adsorption model. Potentiodynamic polarization results revealed that the studied inhibitor behaves as a mixed type.

Key words: Inhibition efficiency, corrosion rate, adsorption isotherm, potentiodynamic polarization

INTRODUCTION

Acid pickling is the method used most frequently for the removal of mill scale and rust from iron and steel. Although the use of H₂SO₄ predominates, interest in the use of HCl is increasing due to shorter pickling time. In order to minimize the loss of metal, acid inhibitors are added to the pickling baths; the use of extracts of different plant materials as low cost, eco-friendly corrosion inhibitors is of special interest from the environmental point of view.(1 -2)

In this line, an effort is made in the present work to investigate the inhibitive effect of *calendula officinalis* (flower) extract on the corrosion of mild steel in 1M hydrochloric acid solution. The extract was obtained from *calendula officinalis* flower growing widely in the southern parts of India. The behaviour of this compound in 1M hydrochloric acid has been investigated and its protection efficiency has been determined by weight loss and polarization methods.

Experimental details

Extraction of the plant material

25gms of dried and powered flowers of *calendula officinalis* were refluxed with 500ml of 1M hydrochloric acid for 3hours. The extract was filtered and made up to 500ml. From this stock-solution; solutions of different concentrations of the inhibitor were prepared.

Weight - loss method

For the weight-loss measurements, mild steel rods of chemical composition, C-0.046%, Mn-0.248%, Si-0.029%, P-0.012%, S-0.019%, Cr-0.05% and the remainder iron and of size 1*5cm² were used. The samples were polished with different grade emery papers, cleaned with acetone, washed with double distilled water and finally dried and kept in desiccators. The cleaned samples were weighed before and after immersion in 1M hydrochloric acid for various immersion periods (1h, 2h, 5h, 7h and 24h) in the absence and presence of the various concentrations (0.001 to 0.5% w/v) of the inhibitor and in the temperature range 40°C to 70°C. The corrosion rate and inhibition efficiency were calculated from the loss in weight of the steel samples.

Polarization studies

For the electrochemical measurements, the cell used was a conventional three electrode system with platinum auxiliary electrode, saturated calomel as reference electrode and polished mild steel specimen as working electrode. The working electrode was lacquered so as to expose 1sq.cm area to contact with the solution. The potentiodynamic curves were recorded by changing the electrode potential automatically from ± 400 mv with scan rate of 2mv/sec. Anodic and cathodic branches of the polarization curves were recorded and joined by a computer into a Tafel diagram. The least square method was used to extrapolate Tafel straight lines and to determine electrochemical parameters.

RESULTS AND DISCUSSION

Weight loss method

Table -1 shows the values of inhibition efficiency obtained from weight loss measurement for different concentrations of the inhibitor in 1M hydrochloric acid at various times of immersion. From the calculated weight loss values the inhibitive efficiency (I.E %) for each concentration was calculated using the equation

$$\text{I.E\%} = W_0 - W / W_0 * 100 \text{ -----} > (1)$$

Where W_0 and W are weight losses in the absence and in the presence of inhibitor respectively.

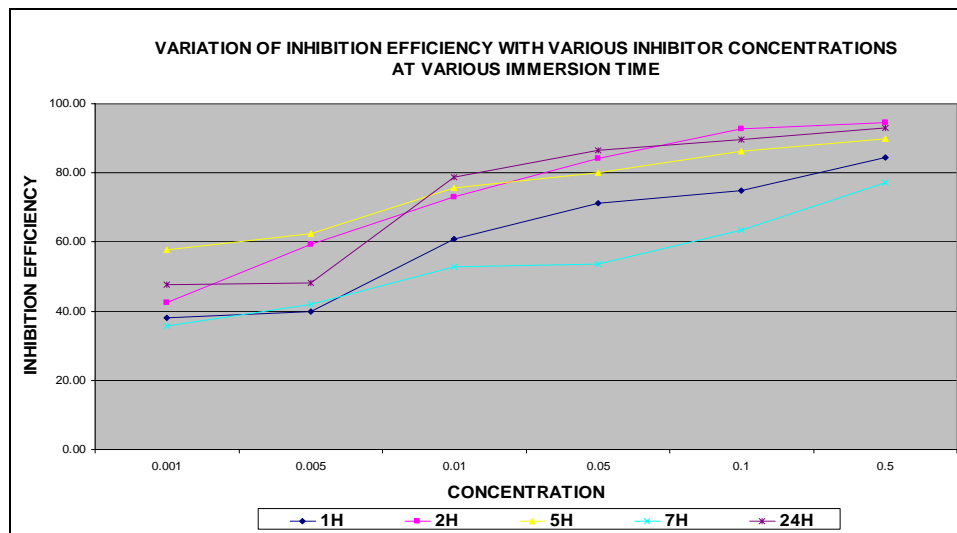
Table -1

Variation of I.E% with various inhibitor concentrations at various immersion times

Concentration of the inhibitor (w/v %)	Inhibition efficiency (%)				
	1h	2h	5h	7h	24h
0.001	38.00	42.59	57.67	35.66	47.61
0.005	40.00	59.23	62.47	42.09	48.24
0.01	61.00	73.01	75.72	52.96	78.77
0.05	71.33	84.21	80.02	53.61	86.45
0.1	75.00	92.87	86.17	63.57	89.54
0.5	84.33	94.67	89.88	77.18	92.89

The inhibition efficiency increases with increasing inhibitor concentration. This behavior may be attributed to the increase of the surface area covered by the adsorbed molecules of *calendula officinalis* with the increase in concentration of the inhibitor. Organic compounds present in *calendula officinalis* can easily be adsorbed on the corroding metal giving rise to such inhibition and the inhibition may be due to their synergistic action. The effect of immersion time on the I.E% is shown in fig (1). The maximum I.E (94.67%) of the inhibitor was achieved at 0.5(w/v %) of the concentration of inhibitor for 2hours of exposure in the corrosive medium.

Figure -1



Effect of temperature

It is clear from table (2) and figure (2) that in the temperature range examined the I.E (%) increases with the increase of inhibitor concentration. Nevertheless, and the combined effect of additive concentration and temperature seems to be more complex. In fact, there is no regular trend in I.E (%) with increase of temperature. (from 30° - 40°c, I.E (%) increases, but for 40° - 50°c, I.E (%) decreases).

Figure -2

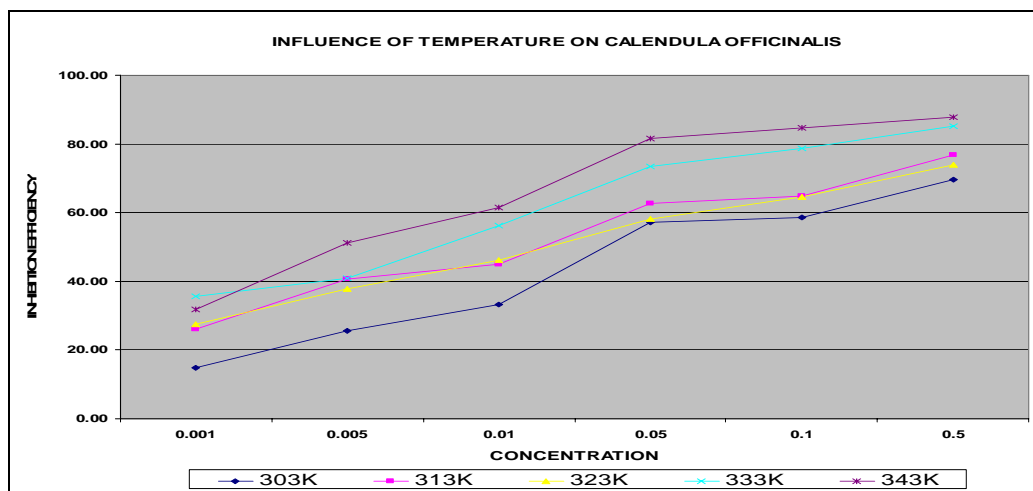


Table -2
Influence of temperature on *calendula officinalis*

Concentration of the inhibitor (w/v %)	Inhibition efficiency (%)				
	303k	313k	323k	333k	343k
0.001	14.76	26.15	27.50	35.58	31.93
0.005	25.71	40.68	37.72	40.95	51.58
0.01	33.33	45.04	46.14	56.16	61.59
0.05	57.14	62.71	58.18	73.50	81.48
0.1	58.57	64.89	64.55	78.59	84.64
0.5	69.52	76.76	73.86	85.20	87.85

Activation energy

The dependence of logarithm of the corrosion rate on the reciprocal values of the absolute temperature is presented in figure (3). Straight lines with correlation co-efficient (>0.9) were obtained. The values of the slopes of these straight lines permit the calculation of apparent activation energy E_a^0 , by the application of equation,

$$C.R = A \exp^{(-E_a/RT)} \text{ -----} > (2)$$

Where R is the universal gas constant. The values of the E_{act} , in the absence and presence of the inhibitor at different concentrations, thus obtained are reported in table3. The decrease in activation energy of corrosion (E_a) in the presence of the inhibitor when compared to that in its absence is attributed to its chemisorption.

Figure -3

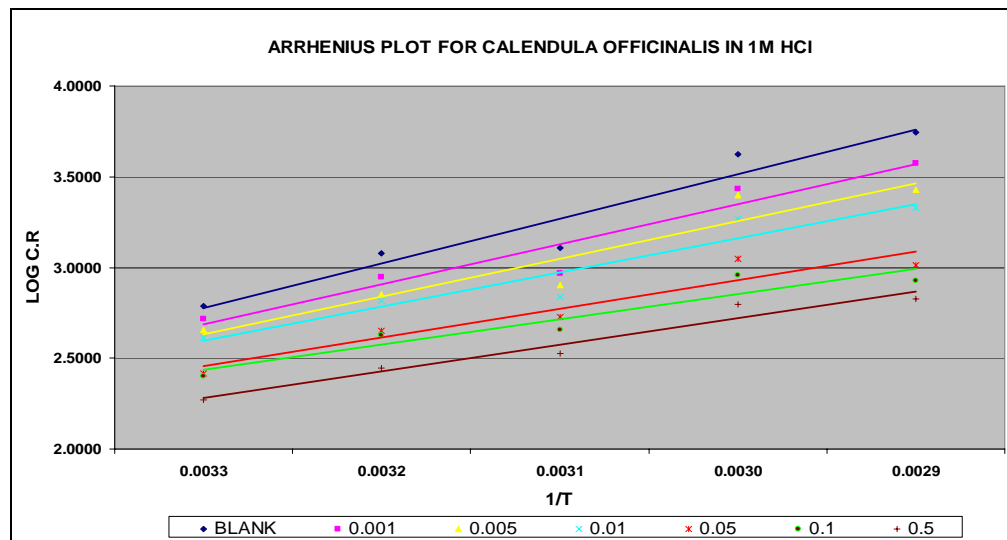


Table – 3

Apparent activation energies calculated from the Arrhenius plot of the corrosion rate

Conc. of the inhibitor%(w/v)	-E _a kJ/mol
Blank	48.82
0.001	43.68
0.005	41.50
0.01	37.36
0.05	31.65
0.1	27.64
0.5	29.19

Adsorption isotherm

The nature of inhibitor interaction on the corroding surface during corrosion inhibition of metals has been deduced in terms of adsorption characteristics of the inhibitor. The surface coverage data (θ) are very useful while discussing the adsorption characteristics. The surface coverage of the inhibitor at a given concentration is calculated by using the equation

$$\theta = (1-r/r_0) \text{ -----}>(3)$$

Where r and r_0 are the corrosion rates with and without inhibitor respectively. The adsorption process involves the displacement of water molecules from the metal surface. Langmuir isotherm was tested for its fit to the experimental data.

Langmuir isotherm

$$\text{Log} [\theta/1 - \theta] = \text{log K} + \text{log C} \text{ -----}> (4)$$

Though the plot (figure - 4) of $\text{log} [\theta/1 - \theta]$ versus log c was linear (correlation coefficient > 0.95). The deviation of the slopes from unity (table-4) (for ideal Langmuir isotherm) can be attributed to the molecular interaction among the adsorbed inhibitor species, a fact which was ignored during the derivation of the Langmuir equation.

Figure -4

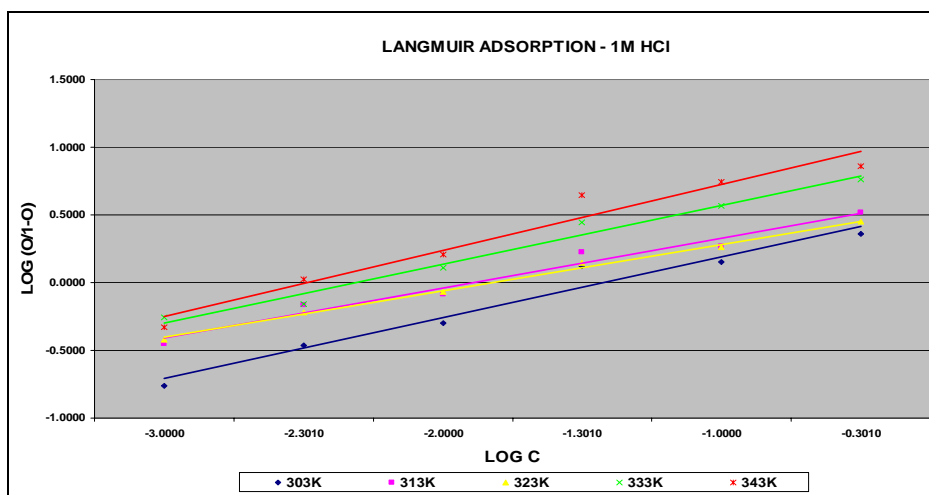


Table-4

Langmuir adsorption isotherm values

Slope	0.4347	0.3587	0.3299	0.4145	0.4699
Intercept	0.5691	0.6438	0.5693	0.9273	1.1326
Correlation coefficient	0.9874	0.9969	0.9979	0.9829	0.9804

Hence, the experimental data were fit into the El-awady's Kinetic thermodynamic model. The isotherm is written as

$$\text{Log } [\theta/1 - \theta] = \text{log } K' + Y \text{ log } C \text{ -----} \rightarrow (5)$$

In this model the number active sites Y is included. Values of 1/y less than one imply multilayer adsorption, while 1/y greater than one suggests that a given inhibitor molecule occupies more than one active site. Table -5 clearly shows that the data correspond well to the above said isotherm.

Table-5
El-awady adsorption isotherm values

1/y	2.3004	2.7875	3.3010	2.4125	2.1281
Intercept(logK')	1.3092	1.7946	1.7257	2.2371	2.4104
Correlation coefficient	0.9874	0.9969	0.9979	0.9829	0.9804

A plot of θ against logC (figure -5) was linear suggesting that the adsorption of the compound on to the mild steel surface follows the Temkin adsorption isotherm. The Temkin equation is

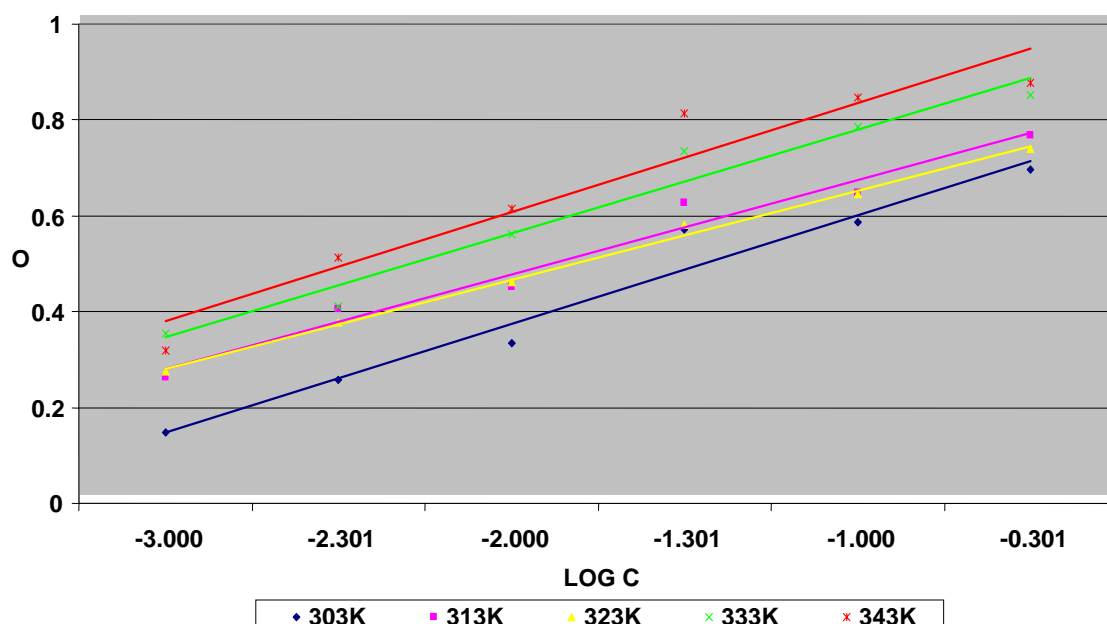
$$e^{a\theta} - KC \text{ -----} \rightarrow (6)$$

Where K is the equilibrium constant and a is the molecular interaction constant. For a > 0 attraction and for a < 0 => repulsion (4). In the present study, the value of the interaction parameter is high and positive (i.e., 10 to 13) leading to high surface coverage and hence better inhibitive efficiency of the inhibitor.

Table-6
Temkin adsorption isotherm values

Slope	0.2189	0.1906	0.1780	0.2060	0.2200
Intercept	0.7930	0.8417	0.8070	0.9567	1.0277
Correlation co-efficient	0.9854	0.9954	0.9965	0.9734	0.9649
a	10.5215	12.0810	12.9415	11.1784	10.4689
Log K	3.6229	4.4153	4.5347	4.6436	4.6717

Figure -5
TEMKIN ADSORPTION - 1M HCl



Polarization measurement

The electrochemical parameters used in this study were obtained from Potentiodynamic polarization curves and presented in table (7). The percentage inhibition efficiency was calculated from relationship,

$$I.E. (\%) = I_0 - I / I_0 * 100 \quad \text{-----> (7)}$$

Where I_0 and I are corrosion current densities in the absence and presence of inhibitor respectively and the polarization resistance R_p was calculated from Stern-Geary equation,

$$R_p = \beta_a \beta_c / 2.3 (\beta_a + \beta_c) I_{corr} \quad \text{-----> (8)}$$

β_a and β_c are the values of cathodic and anodic Tafel slopes and I_{corr} – the corrosion current density. The lower corrosion density (I_{corr}) values in the presence of the *calendula officinalis* extract without causing significant changes in the corrosion potential (E_{corr}) suggest that it is a mixed type inhibitor.

Table (7)

Electrochemical parameters for the corrosion of mild steel in 1M HCl

System	-E _{corr} mv	I _{corr} μAmp	β _a mv /dec	β _c mv /dec	R _p Ohm /cm ²	I.E (%)
Blank	523	1890	125.94	97.84	8.45	-
0.001	516	524	87.46	70.43	10.23	72.27
0.1	511	2673	84.67	67.78	18.94	85.85

Conclusions

- ✚ Acid extract of *calendula officinalis* flowers effectively inhibits the corrosion of mild steel in 1M HCl acid medium.
- ✚ Inhibition efficiency increased with increase in concentration of the extract. The maximum efficiency (94.67%) was found for 0.5% at 2hours of an immersion time.
- ✚ The extract was found to be efficient at higher temperatures. The optimum temperature being 323k in 1M HCl.
- ✚ The adsorption of *calendula officinalis* flower extract on mild steel in HCl medium obeys El-Awady and Temkin adsorption isotherm models.
- ✚ The polarization studies reveal that the extract under the study behaved as a mixed type of inhibitor.

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