

WPI

Lecture 13

Cont. Linear Control of Manipulators
and PID Controller and Tuning

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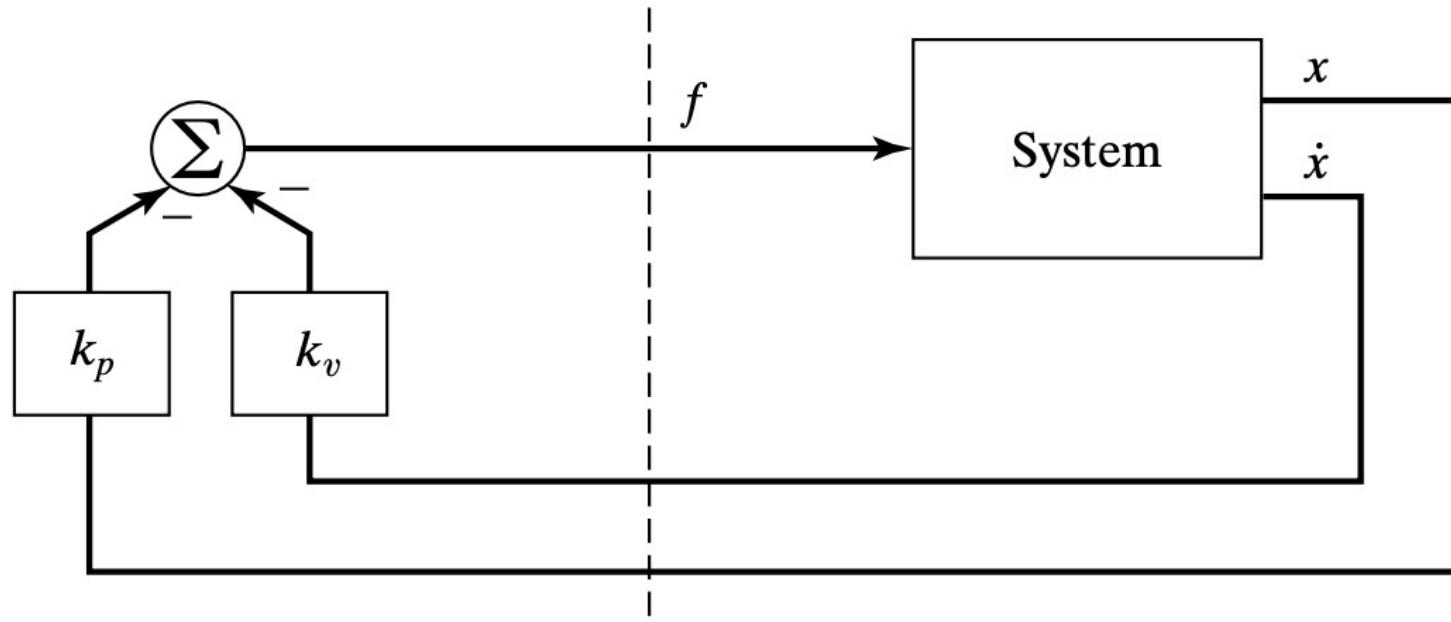
Control of Second-Order Systems

- **Position-regulation system:** It simply attempts to maintain the position of the block in one fixed place regardless of disturbance forces applied in the block.

$$m\ddot{x} + b'\dot{x} + k'x = 0,$$

$$b' = b + k_v$$

$$k' = k + k_p.$$

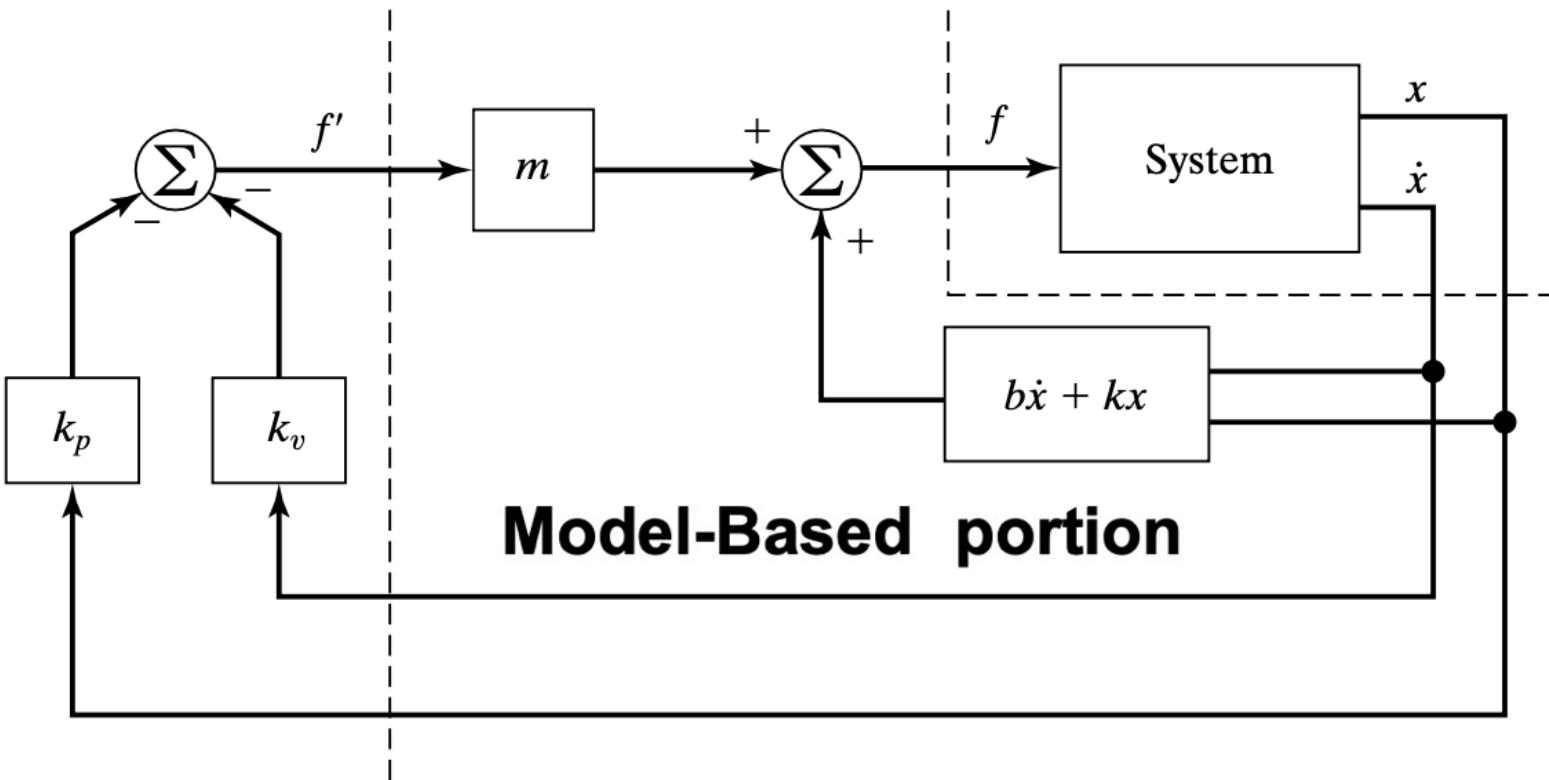
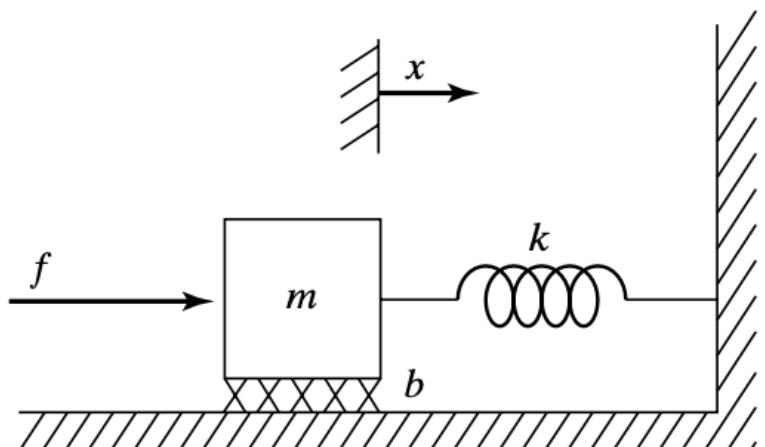


Control-Law Partitioning

- **Model-Based portion:** $f = \alpha f' + \beta$, where α, β are functions or constants and are chosen so that, if f' is taken as a new input, the system appears as a single unit mass.

$$\begin{aligned}\alpha &= m, \\ \beta &= b\dot{x} + kx.\end{aligned}$$

- $m\ddot{x} + b\dot{x} + kx = \alpha f' + \beta.$



Model-Based portion

Control-Law Partitioning

$$\begin{aligned}\ddot{x} &= f'. \\ f' &= -k_v \dot{x} - k_p x.\end{aligned}$$

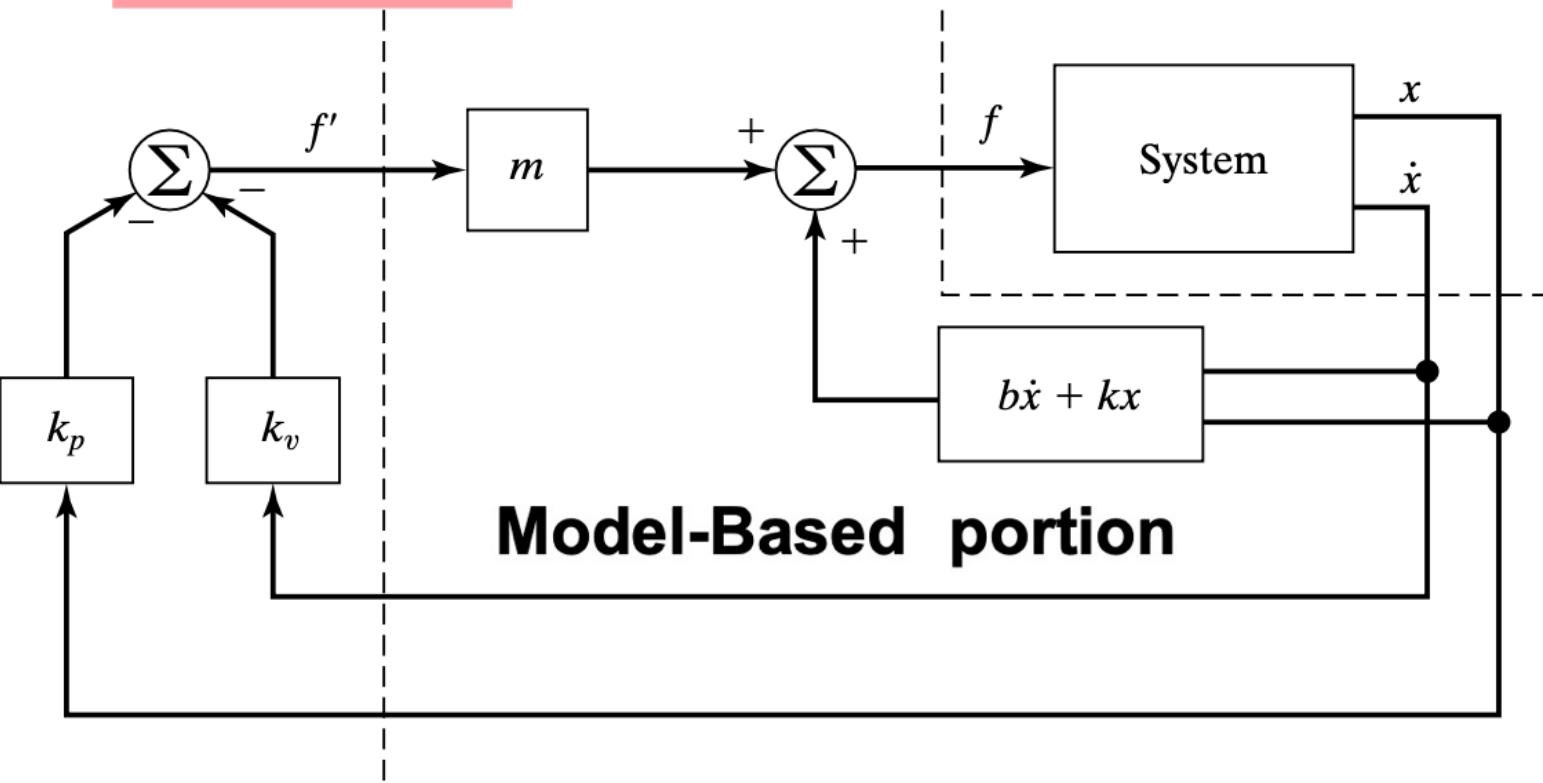
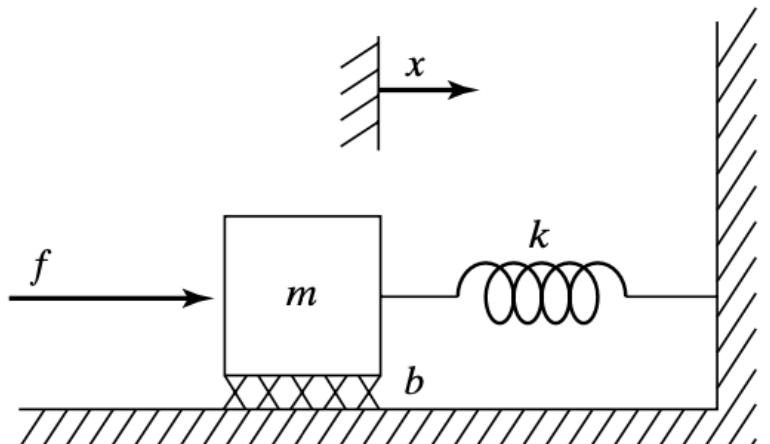
}

$$\ddot{x} + k_v \dot{x} + k_p x = 0.$$

$$k_v = 2\sqrt{k_p}$$

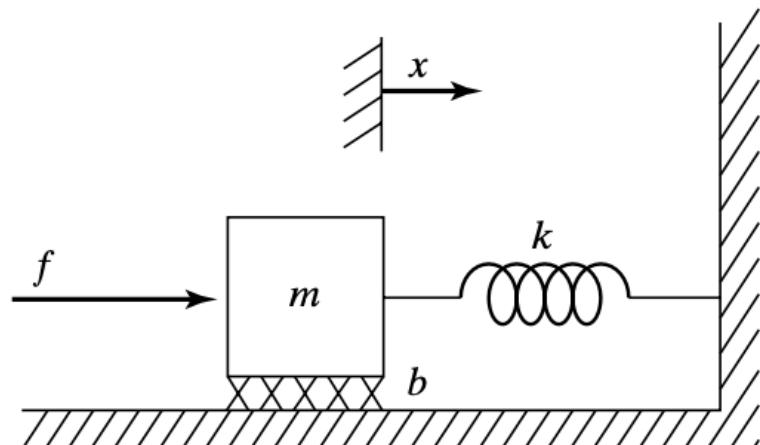
$$\begin{aligned}\alpha &= m, \\ \beta &= b\dot{x} + kx.\end{aligned}$$

$$m\ddot{x} + b\dot{x} + kx = \alpha f' + \beta.$$



Control-Law Partitioning - Example

If the parameters of the system in Figure are $m = 1$, $b = 1$, and $k = 1$, find α , β , and the gains k_p and k_v for a position-regulation control law that results in the system's being critically damped with a closed-loop stiffness of 16.0.



Control-Law Partitioning - Example - Solution

If the parameters of the system in Figure are $m = 1$, $b = 1$, and $k = 1$, find α , β , and the gains k_p and k_v for a position-regulation control law that results in the system's being critically damped with a closed-loop stiffness of 16.0.

We choose

$$\alpha = 1,$$

$$\beta = \dot{x} + x,$$

so that the system appears as a unit mass from the fictitious f' input. We then set gain k_p to the desired closed-loop stiffness and set $k_v = 2\sqrt{k_p}$ for critical damping.

This gives

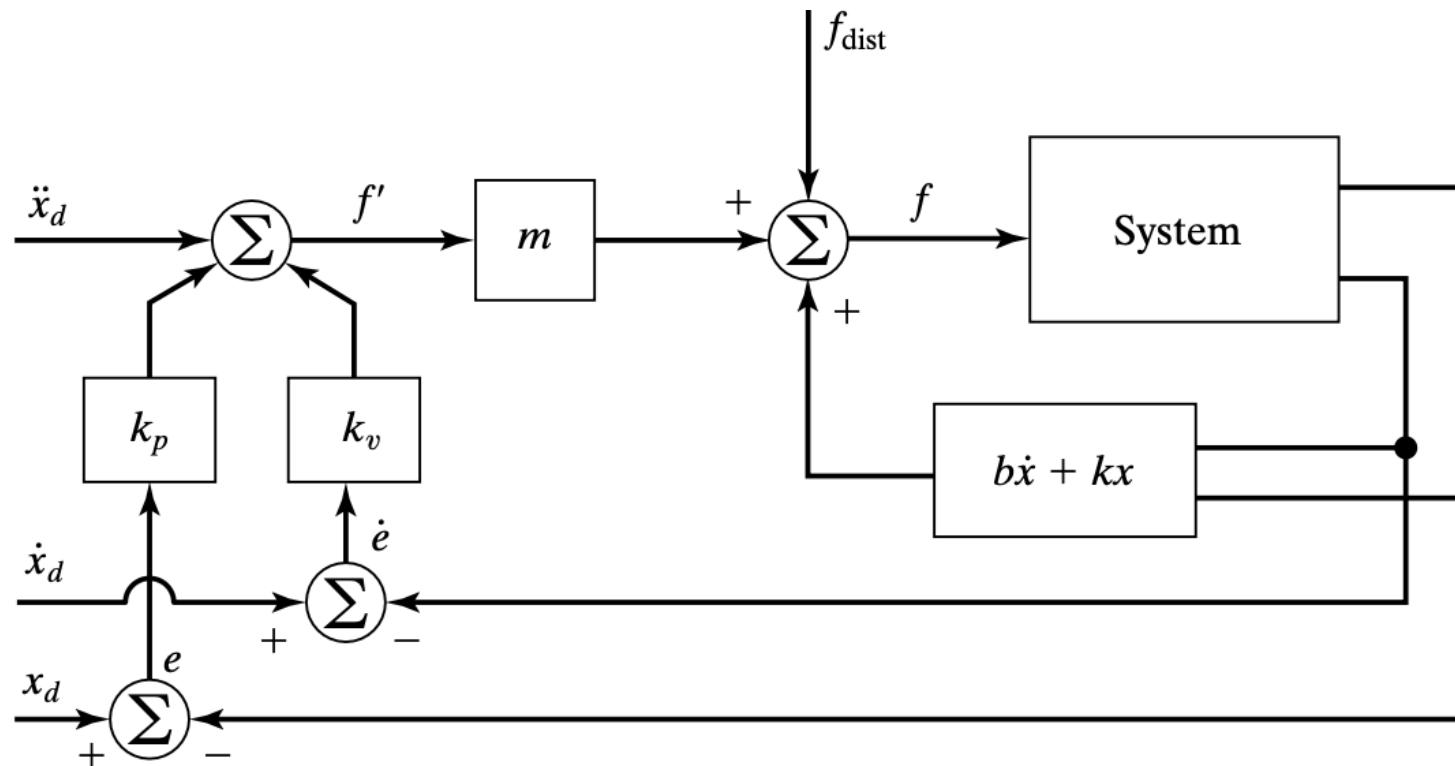
$$k_p = 16.0,$$

$$k_v = 8.0.$$

Disturbance Rejection

- $\ddot{e} + k_v \dot{e} + k_p e = f_{\text{dist}}$
- f_{dist} : bounded \Rightarrow the solution of $e(t)$ is also bounded
- Bounded input, bounded output (BIBO) stability

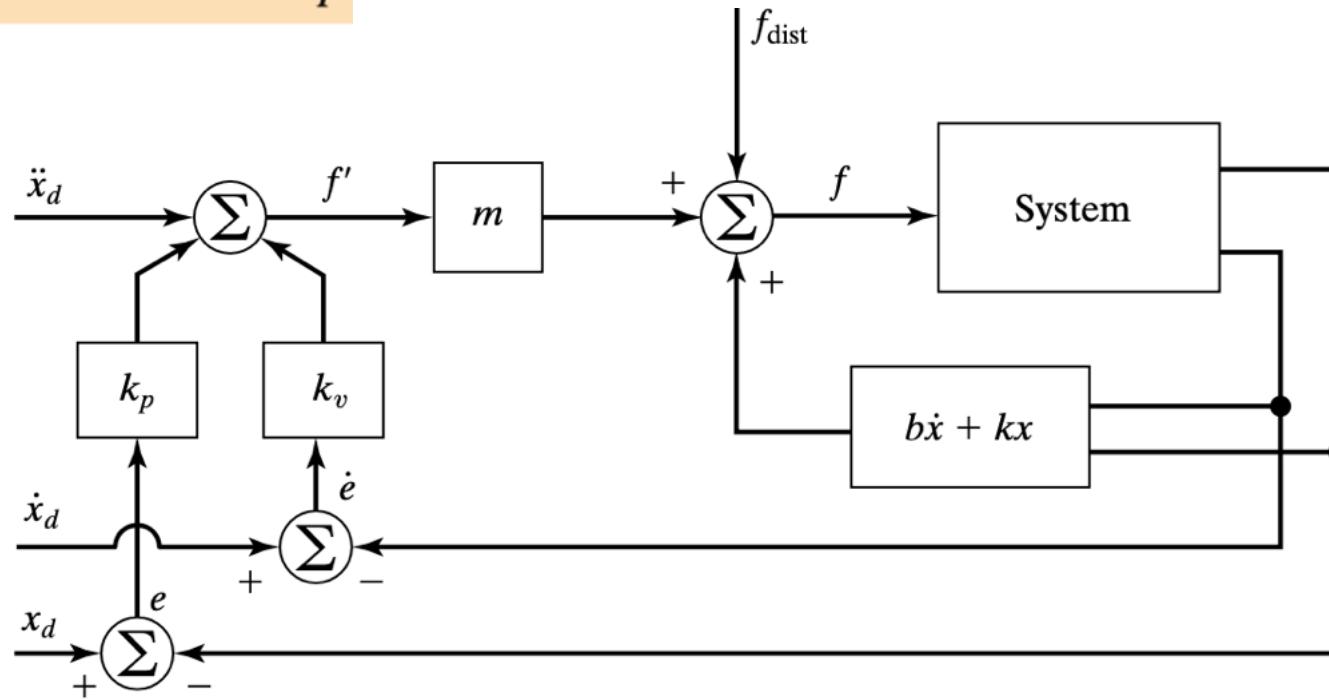
$$\max_t f_{\text{dist}}(t) < a,$$



Steady-state Error

- f_{dist} : constant
- **Steady-state analysis:** analyzing the system at rest (i.e. the derivatives of all system variables are zero)
- $e = f_{\text{dist}}/k_p$: steady-state error

$$\ddot{e} + k_v \dot{e} + k_p e = f_{\text{dist}}$$



Addition of an Integral term

- Addition of an integral term to eliminate steady-state error

- Modified control law:

$$f' = \ddot{x}_d + k_v \ddot{e} + k_p e + k_i \int e dt$$

- Error equation:

$$\ddot{e} + k_v \dot{e} + k_p e + k_i \int e dt = f_{\text{dist}}$$

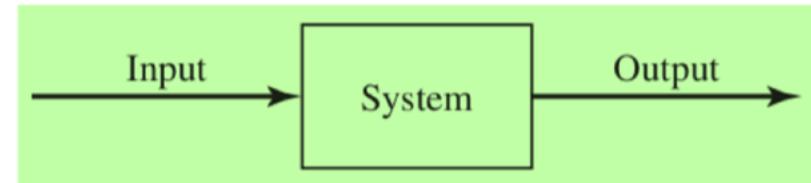
- If $e(t)=0$ for $t<0$, for $t>0$ we have: $\ddot{e} + k_v \ddot{e} + k_p \dot{e} + k_i e = \dot{f}_{\text{dist}},$

$k_i e = 0 \Rightarrow e = 0$: **steady-state error**

PID Control law (Proportional, Integral, Derivative)

Steps for controlling a given system

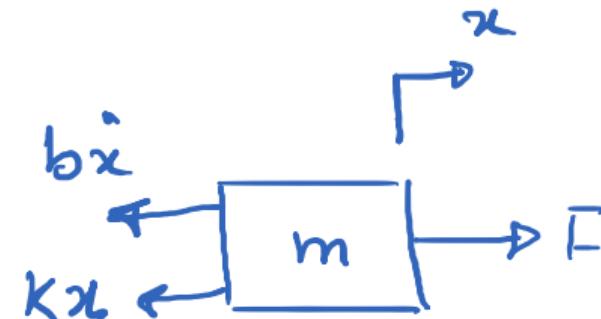
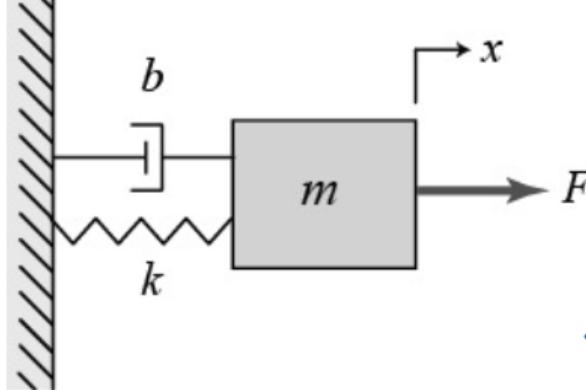
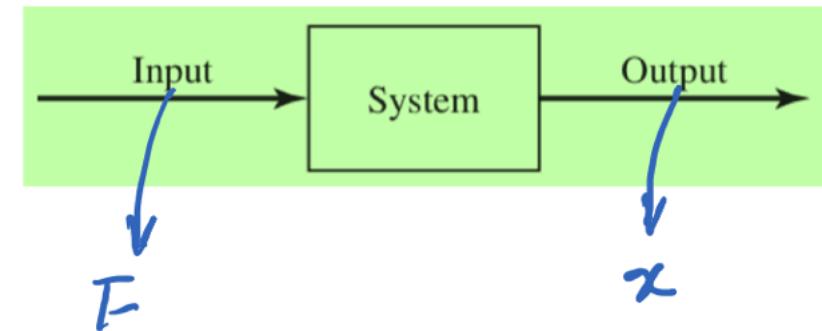
1. Dynamic model
2. Transfer Function
3. Evaluation / Analysis
4. Add Controller (P, PD, PI, PID) and close the loop



1. Dynamic Model

- We have a physical system with a specific behavior.
 - If you apply an input to the system, you will get an output
- We need Mathematical Equations describing the behavior of the system
 - What is the output given the input?
- These equations are called “Dynamic Model” of the system.
- Dynamic Model is in the form of “Differential Equations” and is in the “time” domain.

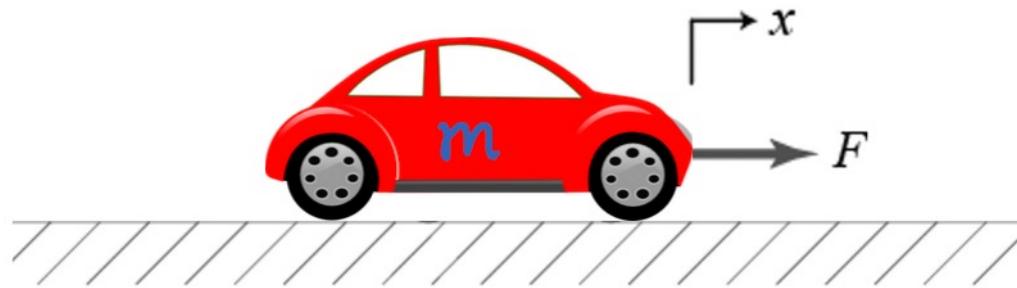
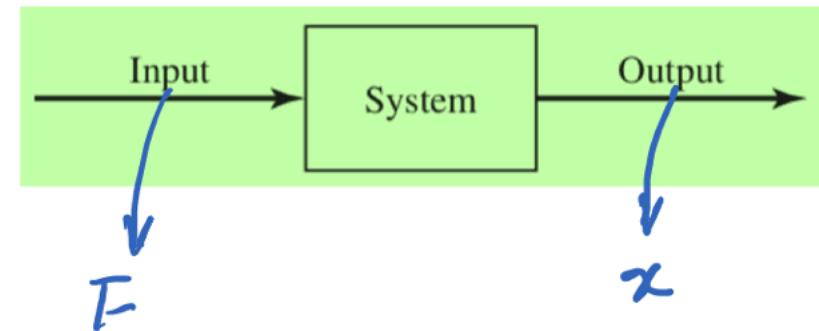
1. Dynamic Model - Example 1



$$\sum F = ma \Rightarrow F - bx - kx = m\ddot{x}$$

$$\Rightarrow \boxed{m\ddot{x} + bx + kx = F}$$

1. Dynamic Model - Example 2



$$\begin{aligned}\sum F &= ma \\ \Rightarrow F &= m\ddot{x}\end{aligned}$$

2. Transfer Function (TF)

- From the dynamic model, there is a relation between output and input, and we need to know that.
- It is not straight-forward to derive this relation in the "time domain"
 - because of the derivative terms
- We need "Frequency Domain" because in the frequency domain, there is no derivatives.
- Laplace Transformation is used to represent the dynamical model in the "Frequency Domain".
- Derive the output/input relation (ratio of output/input) → This ratio is called "**Transfer Function**".

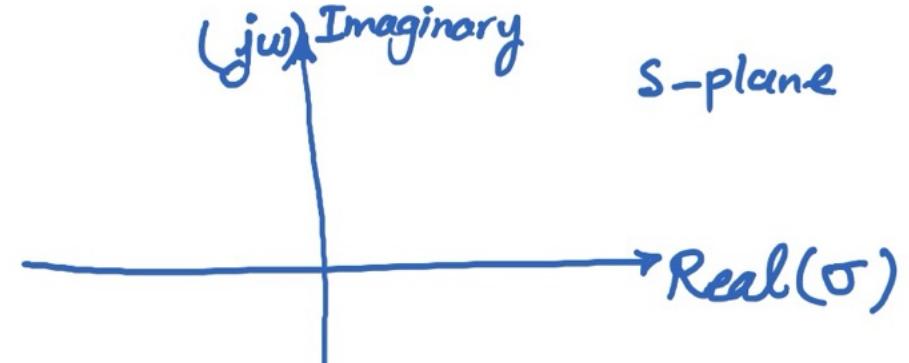
Time domain vs. Complex Frequency domain (s-domain)

- System models are usually in the form of differential equations.
- Differential equations are in the “time domain” and include time derivatives. They are difficult to solve ☹
- Differential equations are composed of multiple terms/functions in time domain.
- For each function $f(t)$ in time domain, there is a corresponding function in the complex frequency domain ($F(s)$)
- $f(t)$ and $F(s)$ are transformable and they both represent the same think but in different domains.
- s is a complex number located in the s-plane and depends on the system’s frequency and damping.

$$F(s) = \int_0^{\infty} f(t) e^{-st} dt$$

$$i = j = \sqrt{-1}$$

$$s = \sigma + i\omega$$



Laplace Transformations

Table of Laplace Transforms

$f(t) = \mathcal{L}^{-1}\{F(s)\}$	$F(s) = \mathcal{L}\{f(t)\}$	$f(t) = \mathcal{L}^{-1}\{F(s)\}$	$F(s) = \mathcal{L}\{f(t)\}$
1. 1	$\frac{1}{s}$	2. e^{at}	$\frac{1}{s-a}$
3. $t^n, n=1,2,3,\dots$	$\frac{n!}{s^{n+1}}$	4. $t^p, p > -1$	$\frac{\Gamma(p+1)}{s^{p+1}}$
5. \sqrt{t}	$\frac{\sqrt{\pi}}{2s^{\frac{3}{2}}}$	6. $t^{n-\frac{1}{2}}, n=1,2,3,\dots$	$\frac{1 \cdot 3 \cdot 5 \cdots (2n-1)\sqrt{\pi}}{2^n s^{n+\frac{1}{2}}}$
7. $\sin(at)$	$\frac{a}{s^2 + a^2}$	8. $\cos(at)$	$\frac{s}{s^2 + a^2}$
9. $t \sin(at)$	$\frac{2as}{(s^2 + a^2)^2}$	10. $t \cos(at)$	$\frac{s^2 - a^2}{(s^2 + a^2)^2}$
11. $\sin(at) - at \cos(at)$	$\frac{2a^3}{(s^2 + a^2)^2}$	12. $\sin(at) + at \cos(at)$	$\frac{2as^2}{(s^2 + a^2)^2}$
13. $\cos(at) - at \sin(at)$	$\frac{s(s^2 - a^2)}{(s^2 + a^2)^2}$	14. $\cos(at) + at \sin(at)$	$\frac{s(s^2 + 3a^2)}{(s^2 + a^2)^2}$
15. $\sin(at+b)$	$\frac{s \sin(b) + a \cos(b)}{s^2 + a^2}$	16. $\cos(at+b)$	$\frac{s \cos(b) - a \sin(b)}{s^2 + a^2}$
17. $\sinh(at)$	$\frac{a}{s^2 - a^2}$	18. $\cosh(at)$	$\frac{s}{s^2 - a^2}$

Laplace Transformations

Table of Laplace Transforms

$f(t) = \mathcal{L}^{-1}\{F(s)\}$	$F(s) = \mathcal{L}\{f(t)\}$	$f(t) = \mathcal{L}^{-1}\{F(s)\}$	$F(s) = \mathcal{L}\{f(t)\}$
19. $e^{at} \sin(bt)$	$\frac{b}{(s-a)^2 + b^2}$	20. $e^{at} \cos(bt)$	$\frac{s-a}{(s-a)^2 + b^2}$
21. $e^{at} \sinh(bt)$	$\frac{b}{(s-a)^2 - b^2}$	22. $e^{at} \cosh(bt)$	$\frac{s-a}{(s-a)^2 - b^2}$
23. $t^n e^{at}, \quad n=1, 2, 3, \dots$	$\frac{n!}{(s-a)^{n+1}}$	24. $f(ct)$	$\frac{1}{c} F\left(\frac{s}{c}\right)$
25. $u_c(t) = u(t-c)$ <u>Heaviside Function</u>	$\frac{e^{-cs}}{s}$	26. $\delta(t-c)$ <u>Dirac Delta Function</u>	e^{-cs}
27. $u_c(t)f(t-c)$	$e^{-cs}F(s)$	28. $u_c(t)g(t)$	$e^{-cs}\mathcal{L}\{g(t+c)\}$
29. $e^{at}f(t)$	$F(s-c)$	30. $t^n f(t), \quad n=1, 2, 3, \dots$	$(-1)^n F^{(n)}(s)$
31. $\frac{1}{t}f(t)$	$\int_s^\infty F(u)du$	32. $\int_0^t f(v)dv$	$\frac{F(s)}{s}$
33. $\int_0^t f(t-\tau)g(\tau)d\tau$	$F(s)G(s)$	34. $f(t+T) = f(t)$	$\frac{\int_0^T e^{-st}f(t)dt}{1-e^{-sT}}$
35. $f'(t)$	$sF(s) - f(0)$	36. $f''(t)$	$s^2F(s) - sf(0) - f'(0)$
37. $f^{(n)}(t)$	$s^n F(s) - s^{n-1}f(0) - s^{n-2}f'(0) - \dots - sf^{(n-2)}(0) - f^{(n-1)}(0)$		

Laplace Transformations - Properties

$f(t) = L^{-1}\{F(s)\}$	$F(s) = L\{f(t)\}$
$e^{at} f(t)$	$F(s-a)$
$\int_0^t f(\tau) d\tau$	$\frac{F(s)}{s}$
$f'(t) = \dot{f}(t)$	$sF(s) - f(0)$
$f''(t) = \ddot{f}(t)$	$s^2 F(s) - sf(0) - f'(0)$
$f'''(t)$	$s^3 F(s) - s^2 f(0) - sf'(0) - f''(0)$

Initial Conditions :
 $f(0) = 0, \dot{f}(0) = 0$
 $\ddot{f}(t) = x(t)$

2. Transfer Function - Example 1

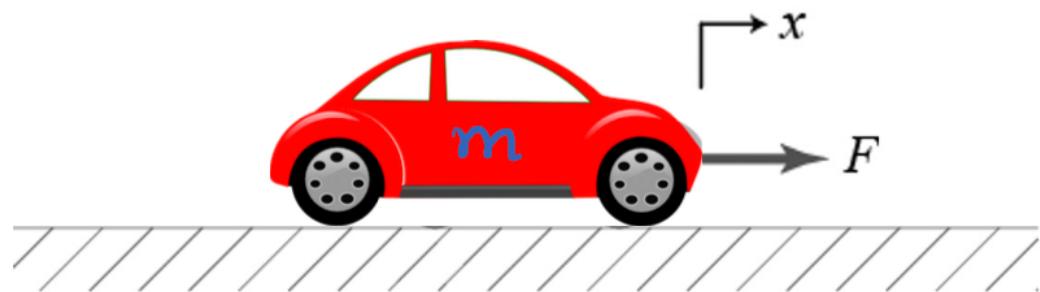


$$\begin{aligned} & \text{Free Body Diagram: } m\ddot{x} + b\dot{x} + kx = F(t) \\ & \text{Laplace Transform: } ms^2X(s) + bsX(s) + kX(s) = F(s) \\ & \Rightarrow X(s)[ms^2 + bs + k] = F(s) \\ & \Rightarrow \boxed{\boxed{TF = \frac{X(s)}{F(s)} = \frac{1}{ms^2 + bs + k}}} \end{aligned}$$

$$\begin{array}{l} \text{output} \rightarrow X \\ \text{input} \rightarrow F \end{array} \Rightarrow TF = \frac{X(s)}{F(s)}$$

$$\begin{array}{l} \dot{x}(t) \xrightarrow{\mathcal{L}} sX(s) \\ \ddot{x}(t) \xrightarrow{\mathcal{L}} s^2X(s) \end{array}$$

2. Transfer Function - Example 2



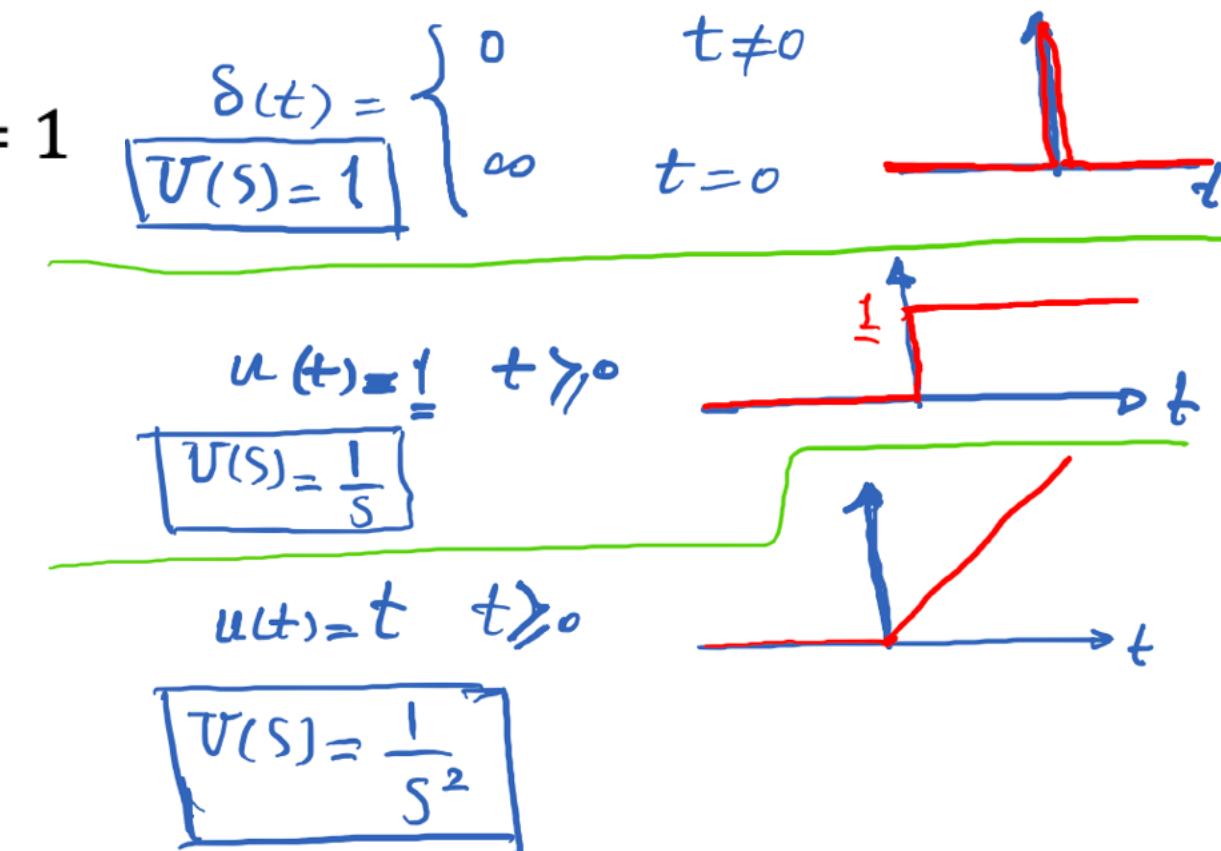
$$\begin{aligned} m\ddot{x} &= F \\ \mathcal{L} \Rightarrow m s^2 X(s) &= F(s) \\ \Rightarrow \boxed{TF = \frac{X(s)}{F(s)} = \frac{1}{ms^2}} \end{aligned}$$

3. Evaluation/Analysis

- Having the Transform Function (TF), we can conclude about the **performance** (transient and steady-state response) and ability of the system.
- To evaluate the performance, we use tests inputs (input signals) to see how the system reacts to tests inputs.
- The response of the system to the test inputs replicates the response of the system to real world inputs.
- There are multiple tests inputs. Here are three of them:
 - Unit Impulse: $u(t) = \delta(t) \rightarrow U(s) = 1$
 - Unit Step: $u(t) = 1 \rightarrow U(s) = \frac{1}{s}$
 - Unit Ramp: $u(t) = t \rightarrow U(s) = \frac{1}{s^2}$

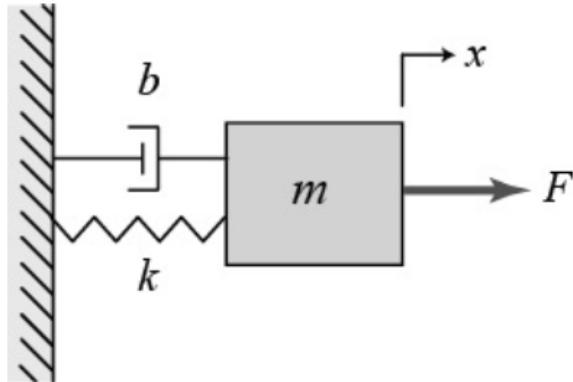
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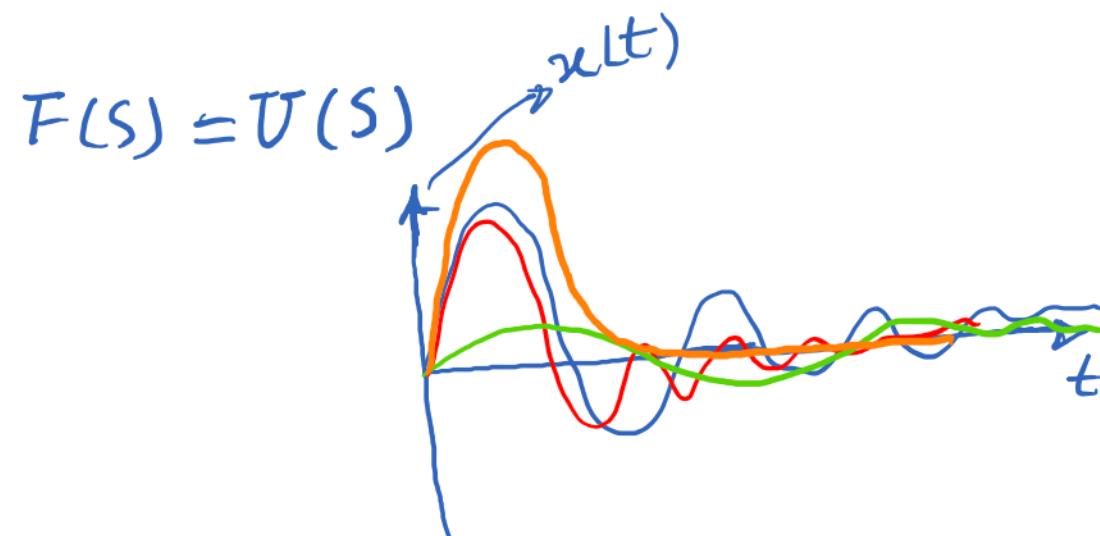


3. Evaluation/Analysis - Example 1

- Unit Impulse: $u(t) = \delta(t) \rightarrow U(s) = 1$



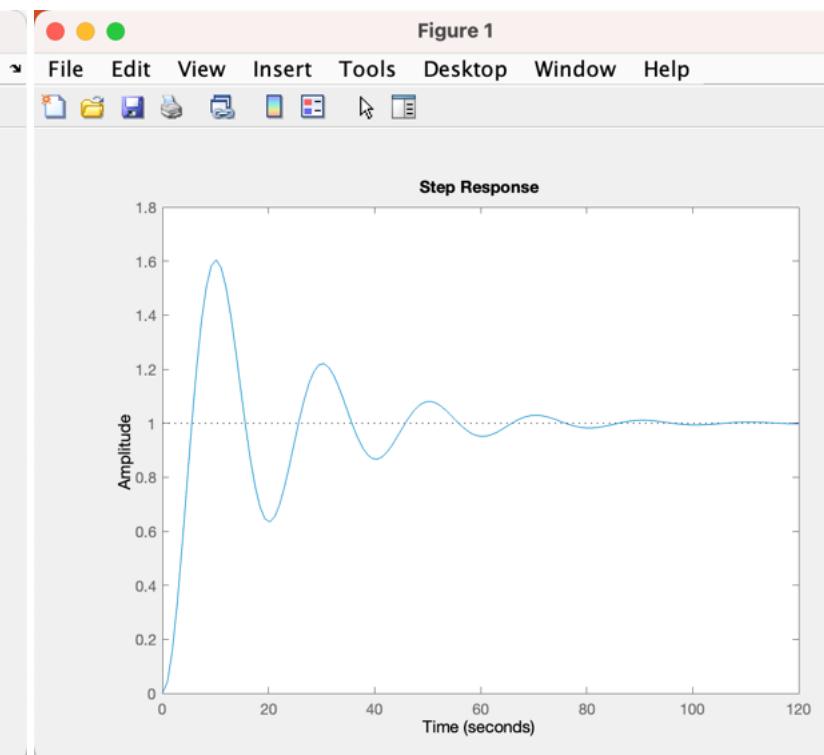
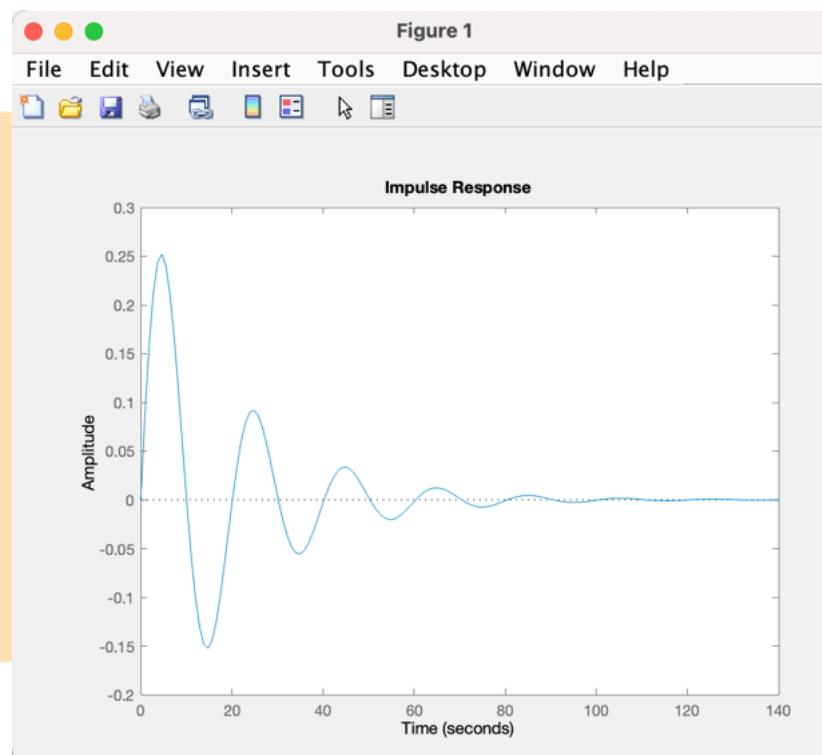
$$\frac{x(s)}{U(s)} = \frac{1}{ms^2 + bs + k}$$
$$U(s) = 1$$



3. Evaluation/Analysis - Example 1 - in MATLAB

- Unit Impulse: $u(t) = \delta(t) \rightarrow U(s) = 1$

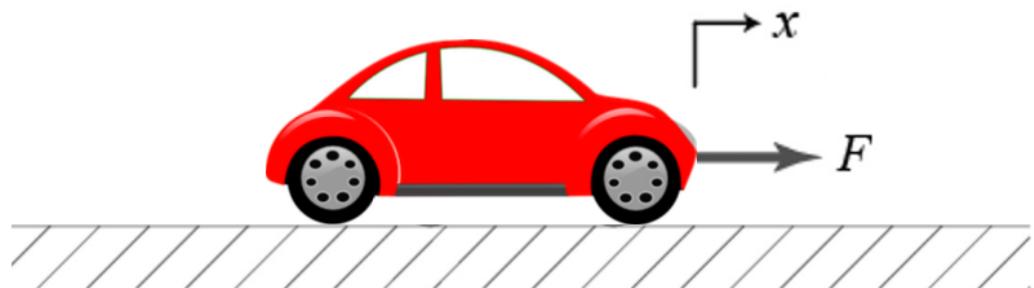
```
>> sys = tf([1],[10 1 1])  
  
sys =  
  
    1  
-----  
 10 s^2 + s + 1  
  
Continuous-time transfer function.  
  
>> impulse(sys)  
>> step(sys)
```



- Unit Step: $u(t) = 1 \rightarrow U(s) = \frac{1}{s}$

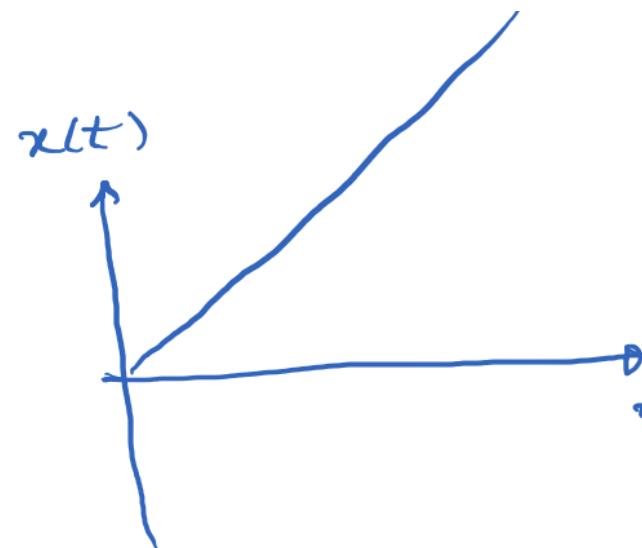
3. Evaluation/Analysis - Example 2

- Unit Impulse: $u(t) = \delta(t) \rightarrow U(s) = 1$



$$TF = \frac{x(s)}{U(s)} = \frac{1}{ms^2}$$

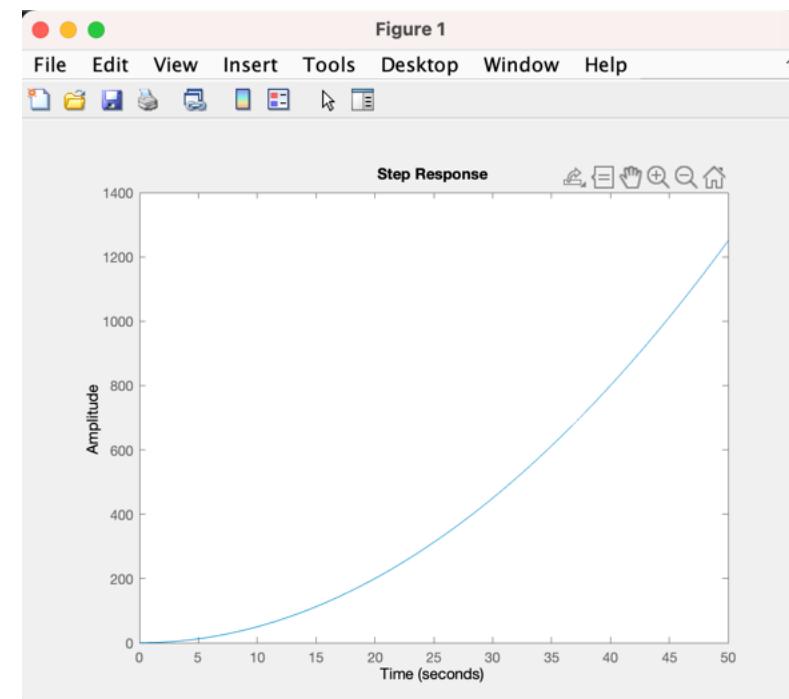
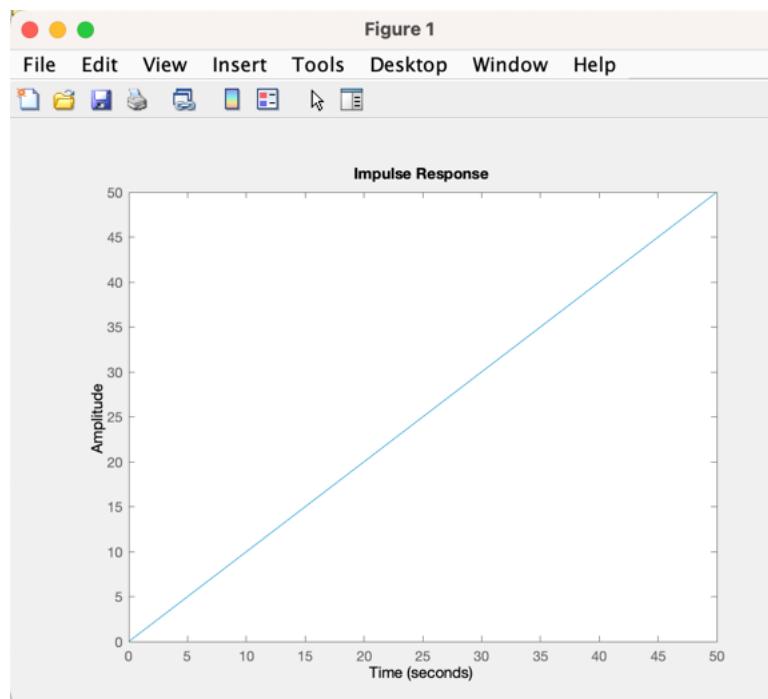
$$\underline{U(s) = 1}$$



3. Evaluation/Analysis - Example 2 - in MATLAB

- Unit Impulse: $u(t) = \delta(t) \rightarrow U(s) = 1$

```
>> sys = tf([1], [1 0 0])  
  
sys =  
  
    1  
    ---  
    s^2  
  
Continuous-time transfer function.  
  
>> impulse(sys)  
>> step(sys)
```



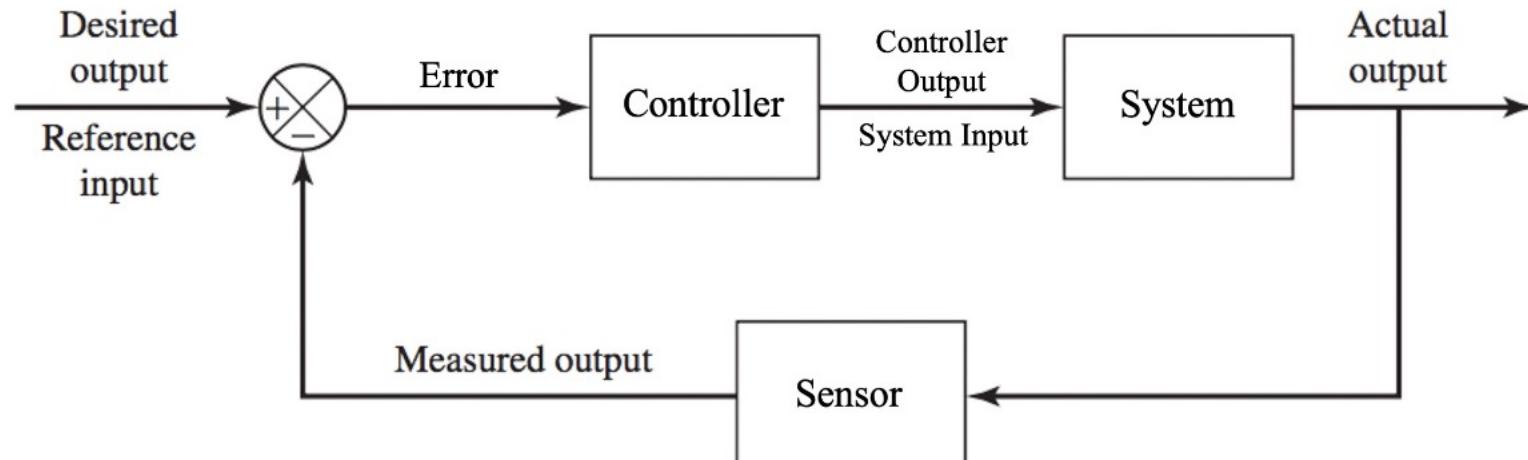
- Unit Step: $u(t) = 1 \rightarrow U(s) = \frac{1}{s}$

Classical Control - NOT satisfactory 😞

- **Almost always, the performance of the system is NOT satisfactory and that is why we add a controller to the system.**

4. Add Controller (P, PD, PI, PID) and close the loop

- Depending on the control goal, add a controller and find the Closed-Loop Transfer Function (CLTF) of the system.
- By adding a controller, the output/response/behavior of the system will change (why?)
- Repeat Step 3 (Evaluate/Analysis) and Step 4 (Add a controller) until a satisfactory performance is achieved.



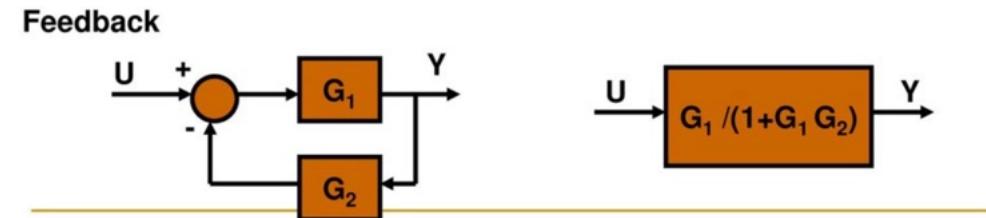
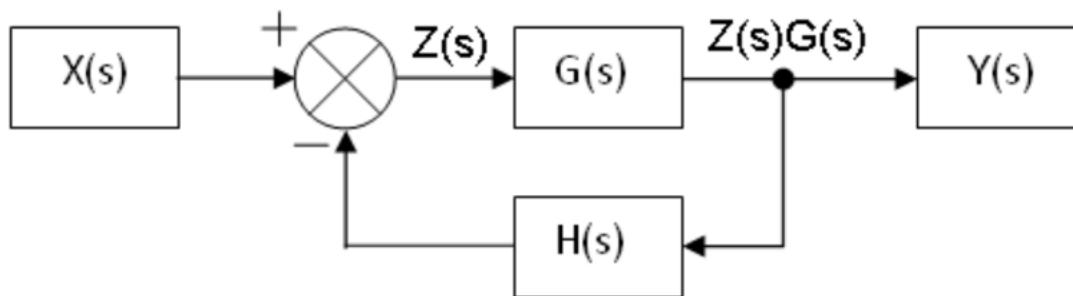
Closed-Loop Transfer Function (CLTF)

In control theory, a **closed-loop transfer function** is a mathematical function describing the net result of the effects of a **feedback control loop** on the input signal to the **plant** under control.

Overview [edit]

The closed-loop **transfer function** is measured at the output. The output signal can be calculated from the closed-loop transfer function and the input signal. Signals may be **waveforms**, **images**, or other types of **data streams**.

An example of a closed-loop transfer function is shown below:



The summing node and the $G(s)$ and $H(s)$ blocks can all be combined into one block, which would have the following transfer function:

$$\frac{Y(s)}{X(s)} = \frac{G(s)}{1 + G(s)H(s)}$$

$G(s)$ is called **feedforward** transfer function, $H(s)$ is called **feedback** transfer function, and their product $G(s)H(s)$ is called the **open-loop transfer function**.

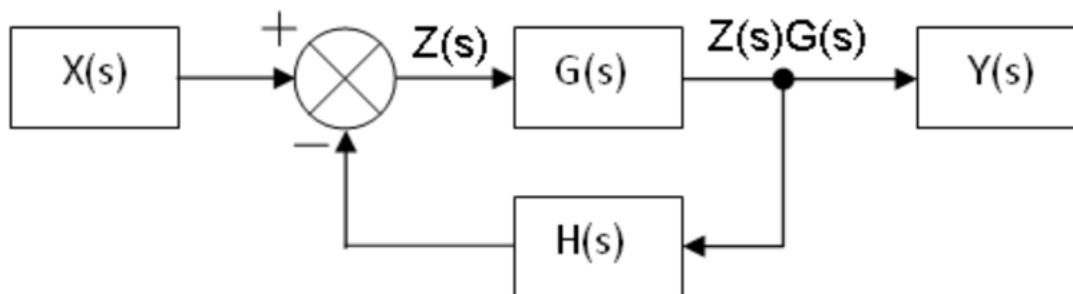
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Signals may be **waveforms**, **images**, or other types of **data streams**.

An example of a closed-loop transfer function is shown below:



The summing node and the $G(s)$ and $H(s)$ blocks can all be combined into one block.

$$\frac{Y(s)}{X(s)} = \frac{G(s)}{1 + G(s)H(s)}$$

Derivation [edit]

We define an intermediate signal Z (also known as error signal) shown as follows:

Using this figure we write:

$$Y(s) = G(s)Z(s)$$

$$Z(s) = X(s) - H(s)Y(s)$$

Now, plug the second equation into the first to eliminate $Z(s)$:

$$Y(s) = G(s)[X(s) - H(s)Y(s)]$$

Move all the terms with $Y(s)$ to the left hand side, and keep the term with $X(s)$ on the right hand side:

$$Y(s) + G(s)H(s)Y(s) = G(s)X(s)$$

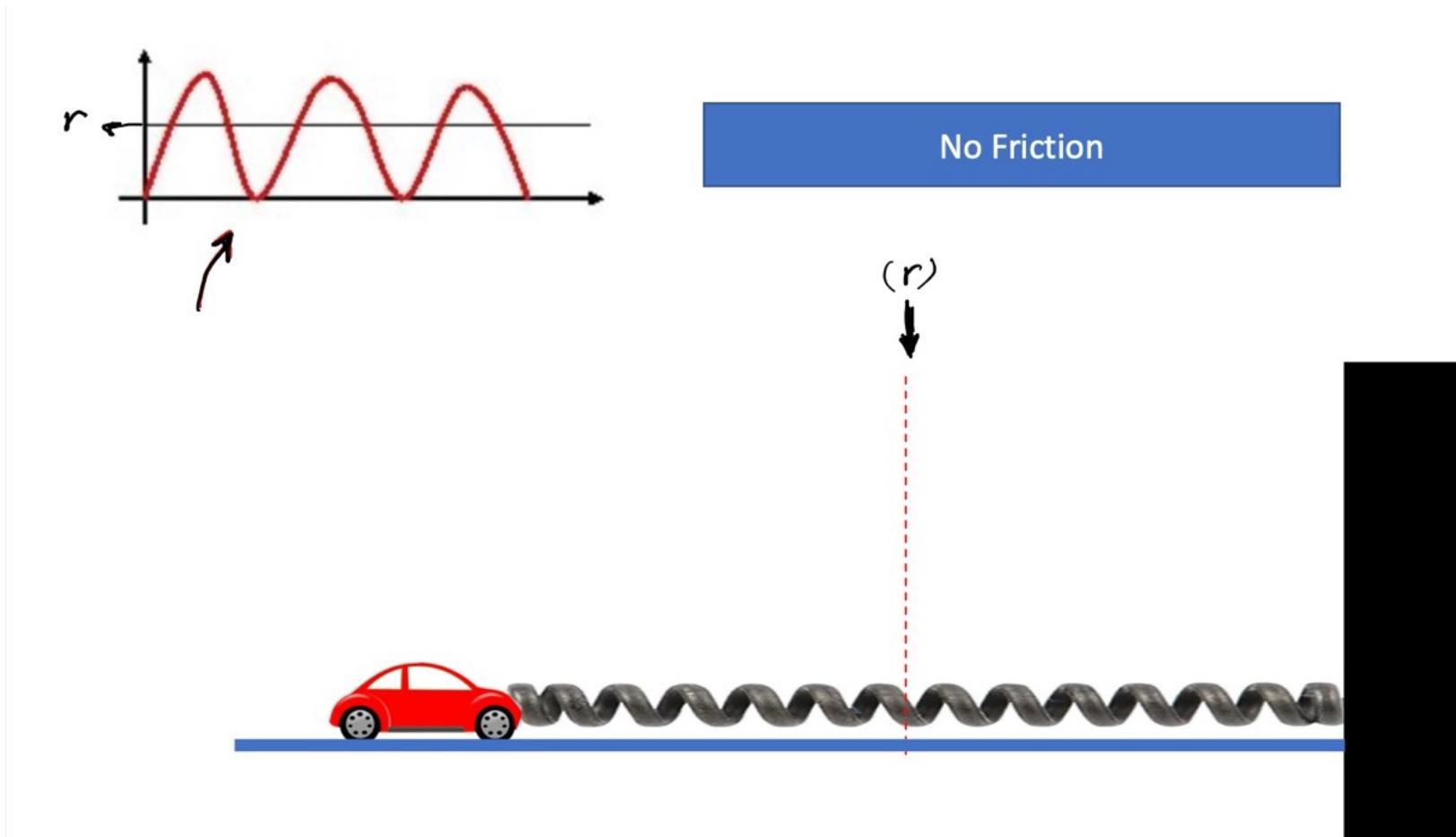
Therefore,

$$Y(s)(1 + G(s)H(s)) = G(s)X(s)$$

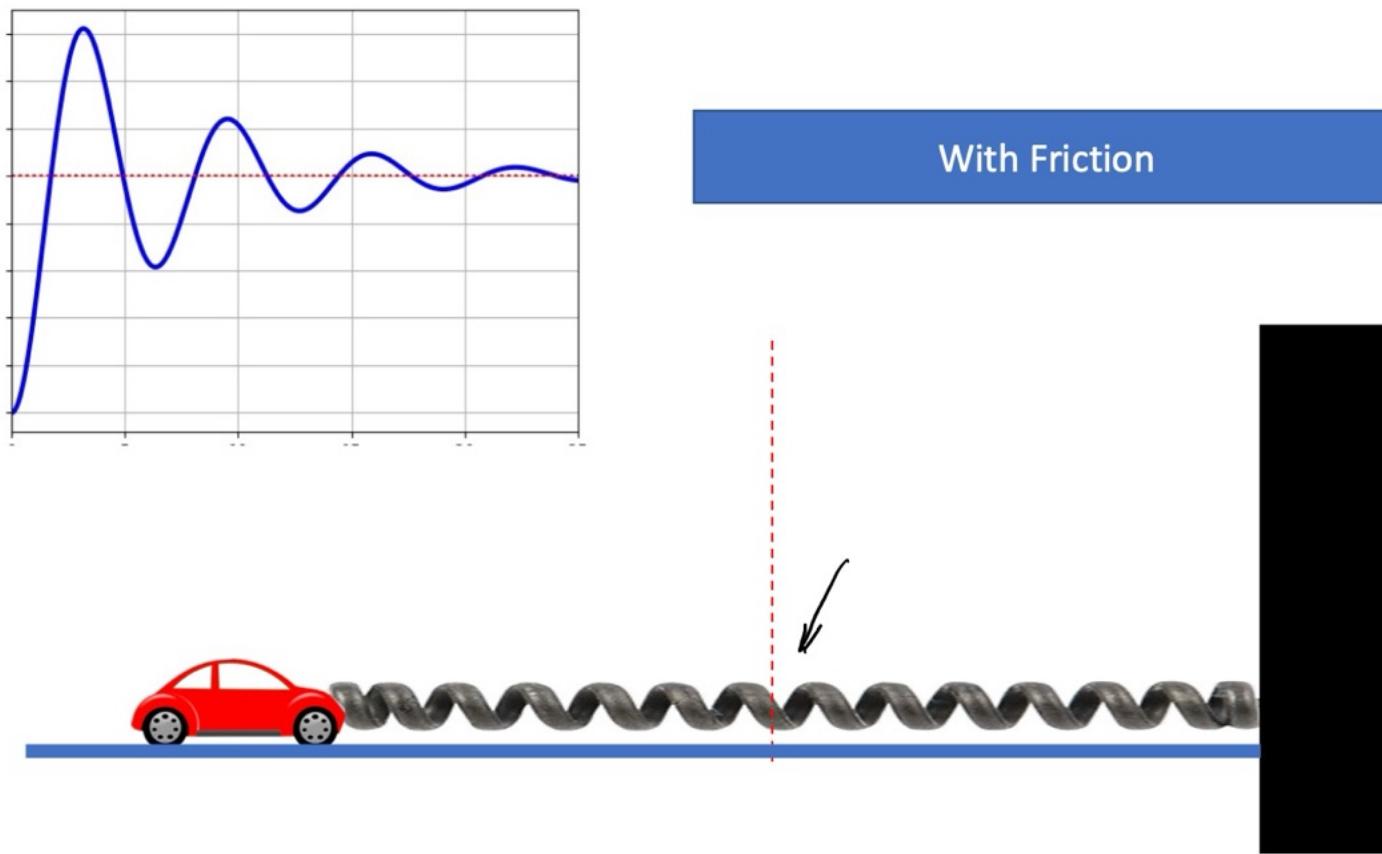
$$\Rightarrow \frac{Y(s)}{X(s)} = \frac{G(s)}{1 + G(s)H(s)}$$

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Proportional Controller



Proportional Controller



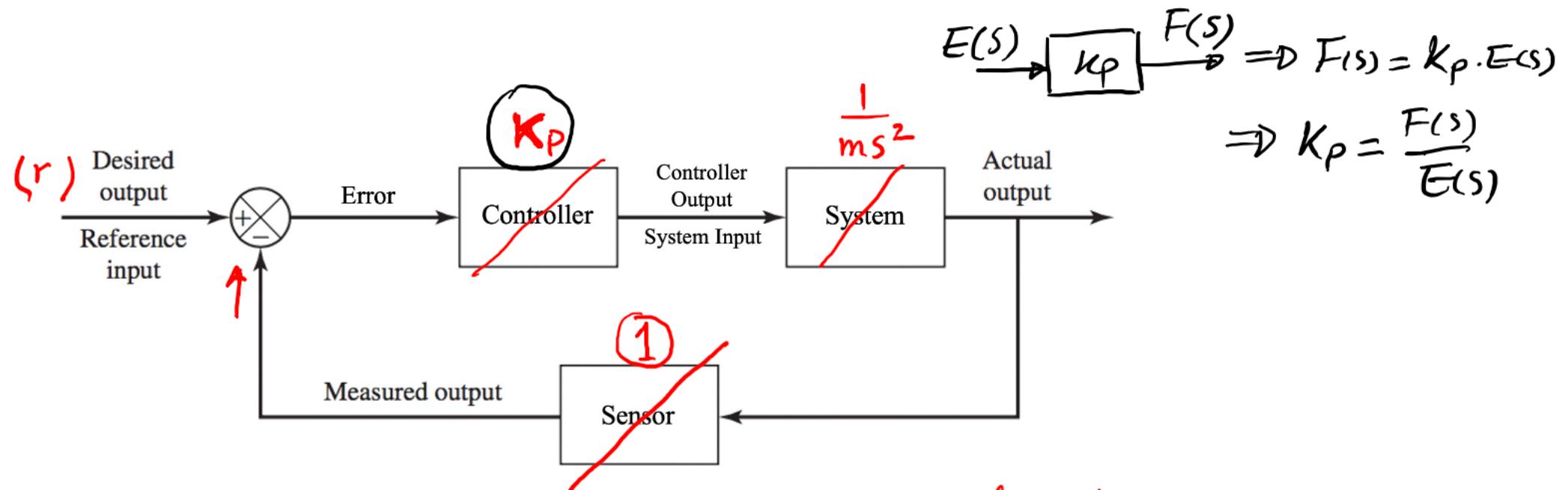
Proportional Controller

- Adding a Proportional Controller (K_p) is equivalent to adding a Spring!

Proportional Controller

proportional controller: K_p

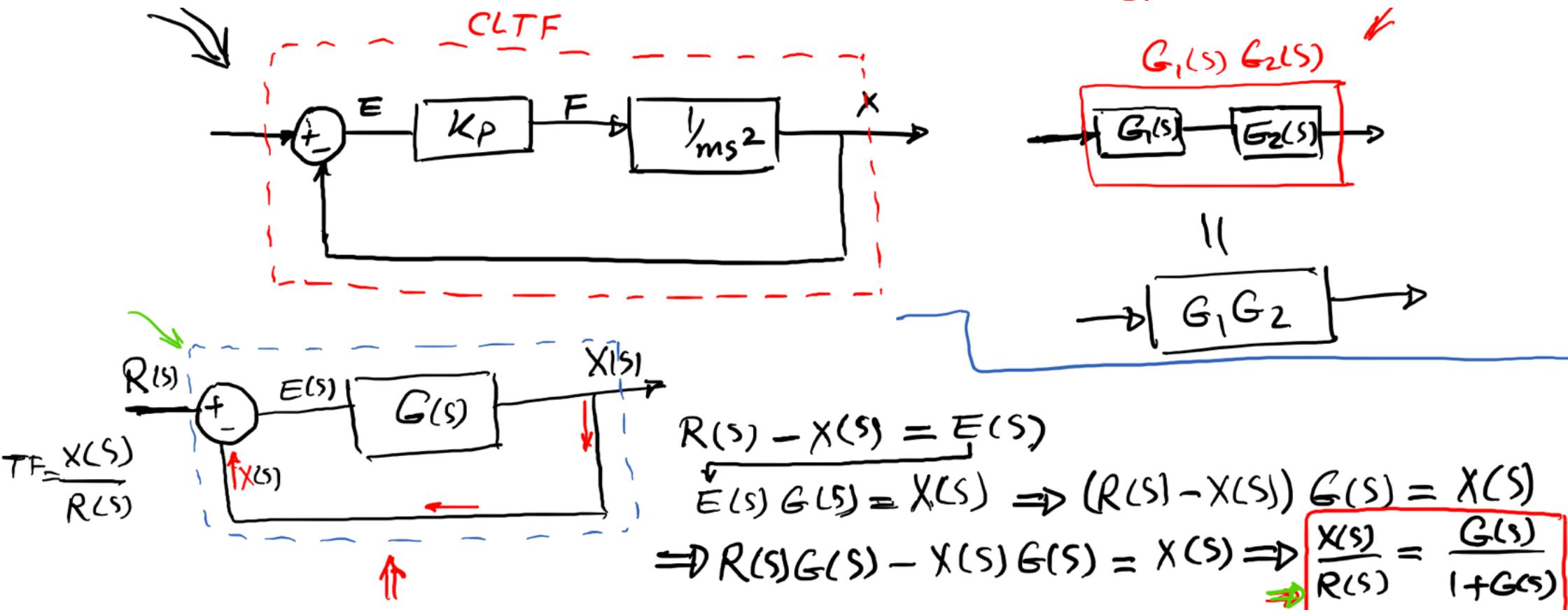
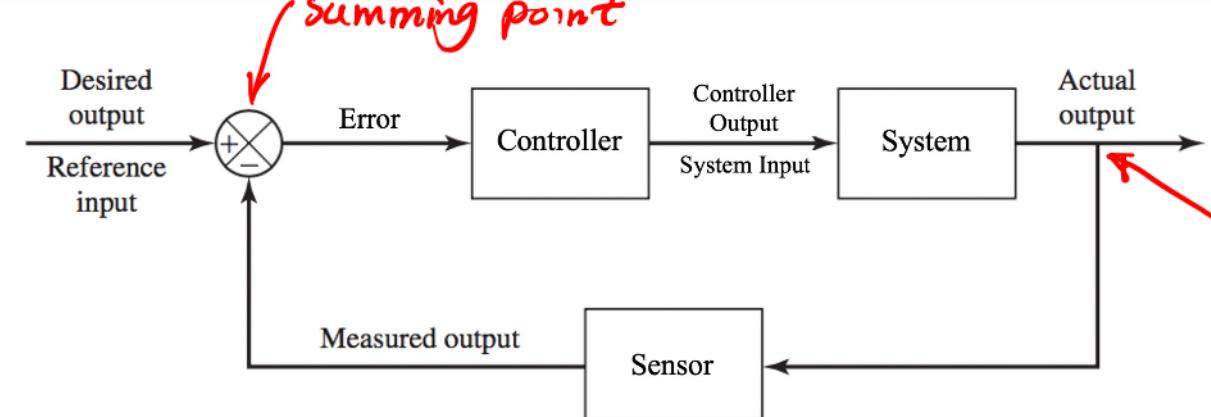
$$\rightarrow e \rightarrow [K_p] \rightarrow F \Rightarrow F = K_p e$$



$$E(s) \xrightarrow{K_p} F(s) \Rightarrow F(s) = K_p \cdot E(s)$$
$$\Rightarrow K_p = \frac{F(s)}{E(s)}$$

unity-feedback control systems

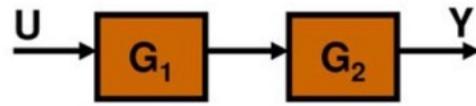
Proportional Controller



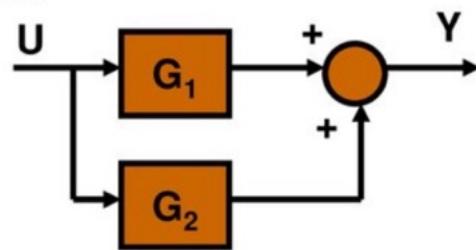
Proportional Controller

Block diagram reduction rules

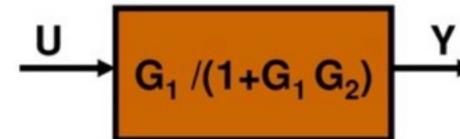
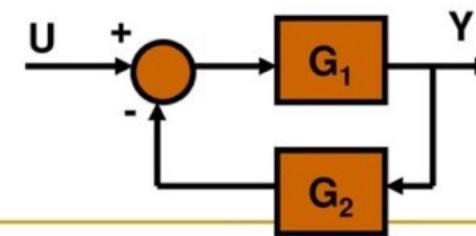
Series



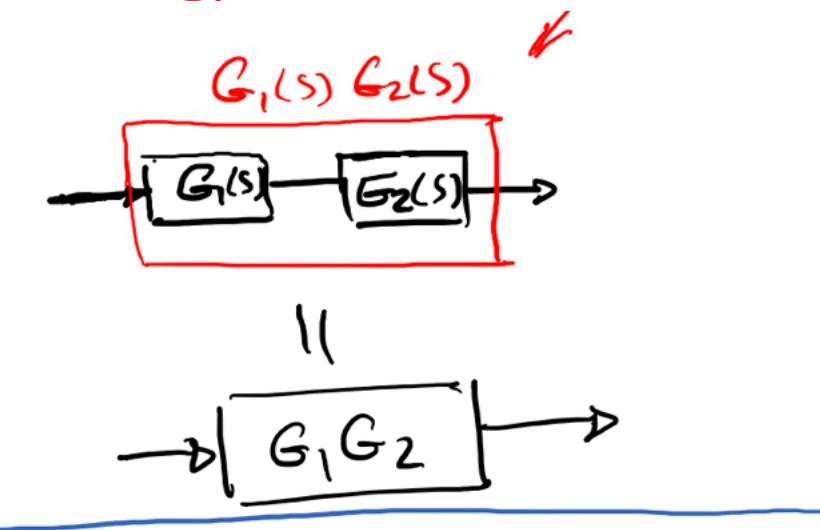
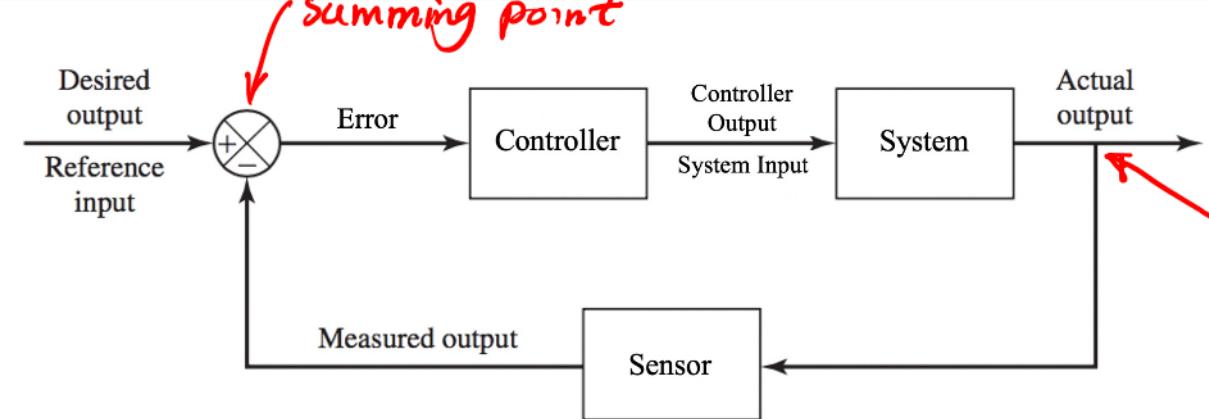
Parallel



Feedback

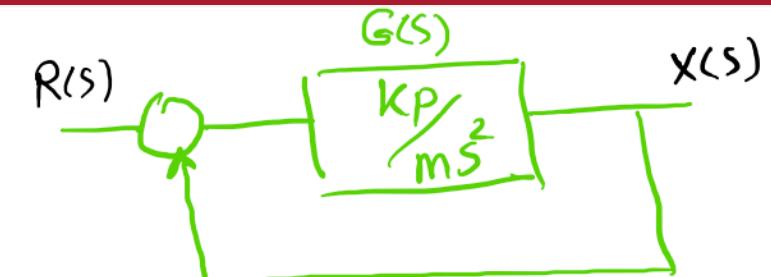
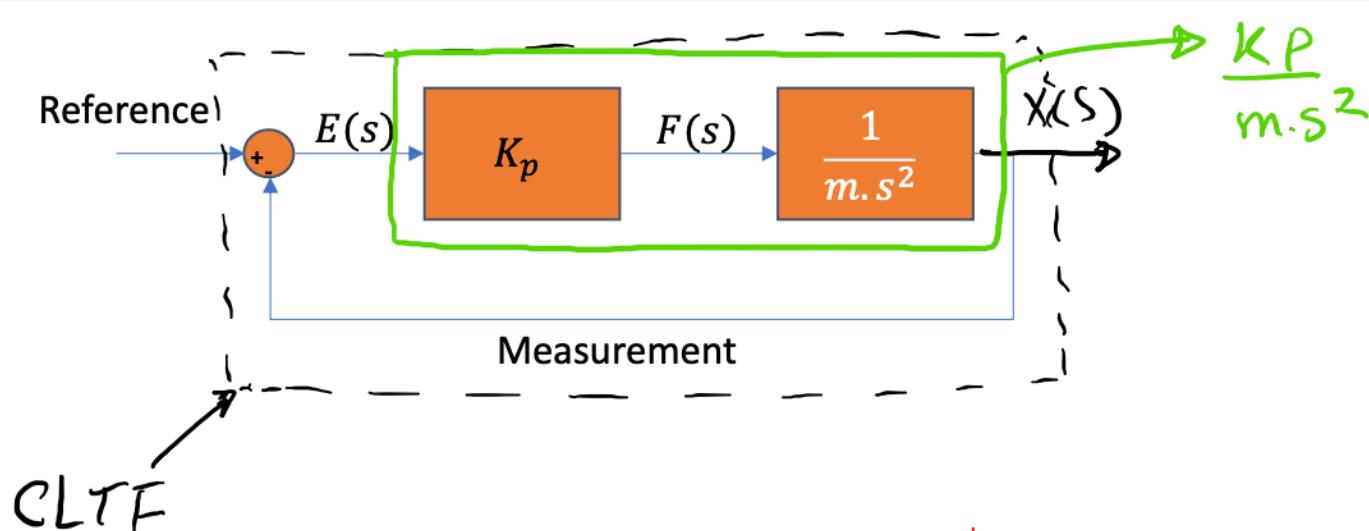


5. Transfer functions



$$\begin{aligned}
 & E(s) \\
 & \Rightarrow (R(s) - X(s)) G(s) = X(s) \\
 & (s) G(s) = X(s) \Rightarrow \frac{X(s)}{R(s)} = \frac{G(s)}{1 + G(s)}
 \end{aligned}$$

Proportional Controller



$$\frac{X(s)}{R(s)} = \frac{K_p/m s^2}{1 + K_p/m s^2}$$

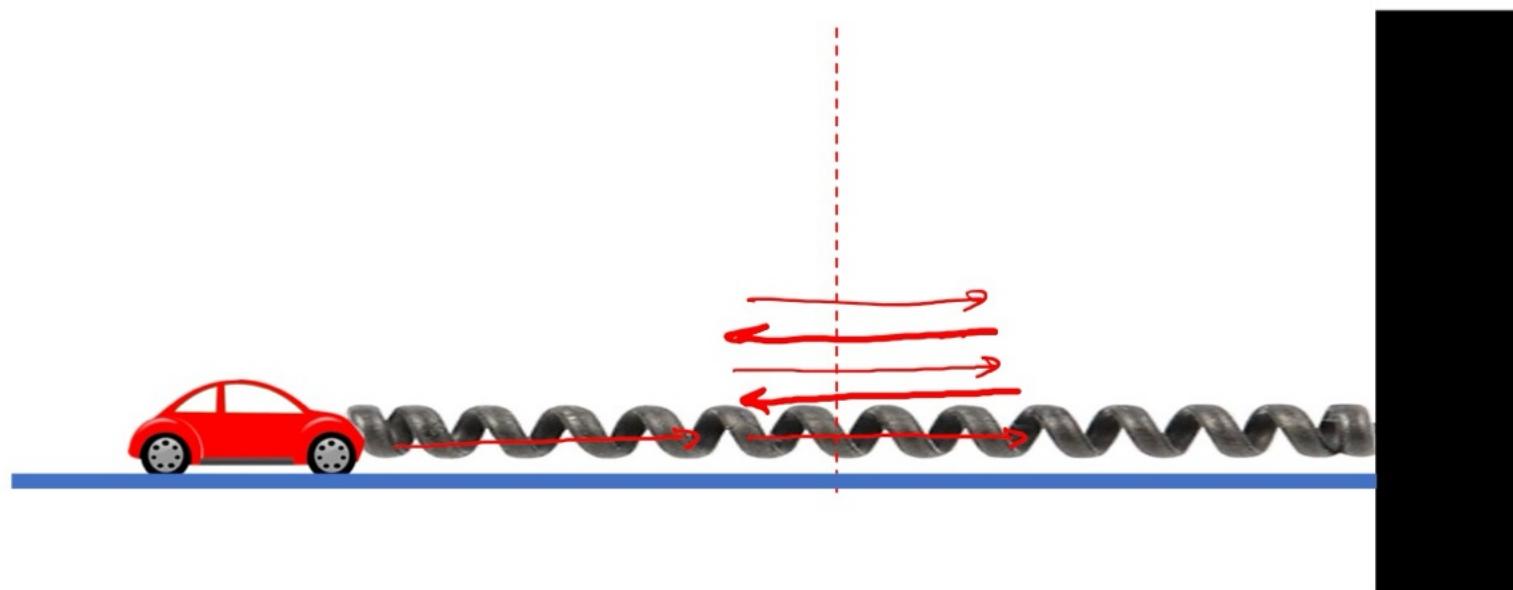
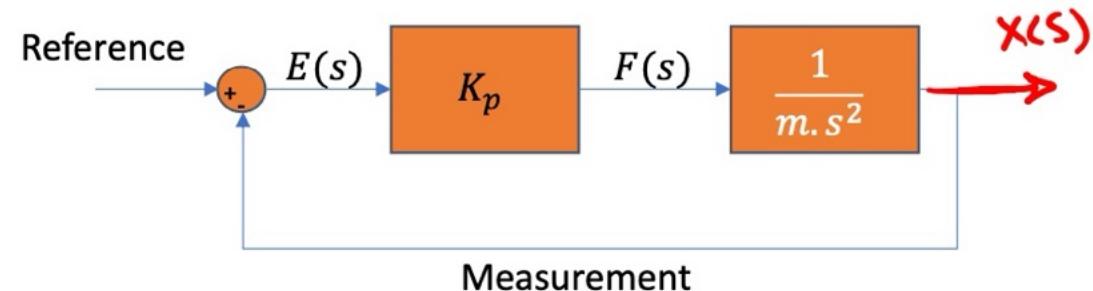
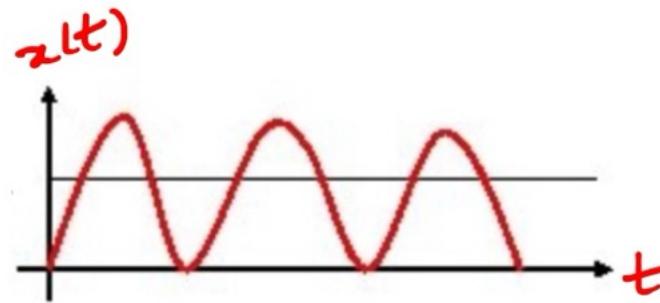
$$\Rightarrow \frac{X(s)}{R(s)} = CLTF = \frac{K_p}{m s^2 + K_p}$$



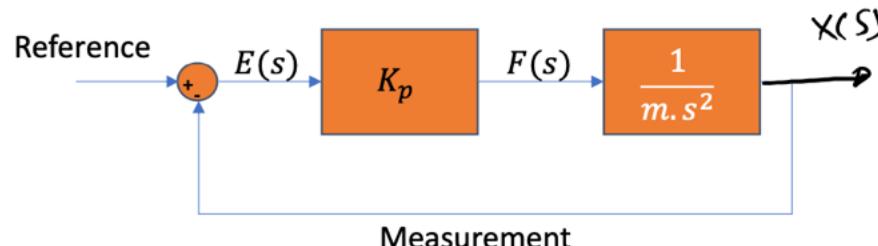
$$m = 500$$

$$K_p > 0$$

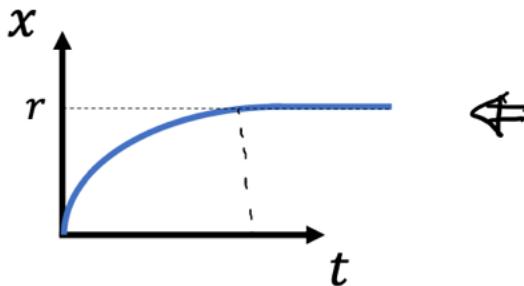
Proportional Controller



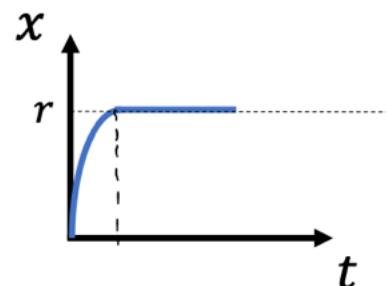
Derivative Controller



- By trying different values of K_p , we might get:

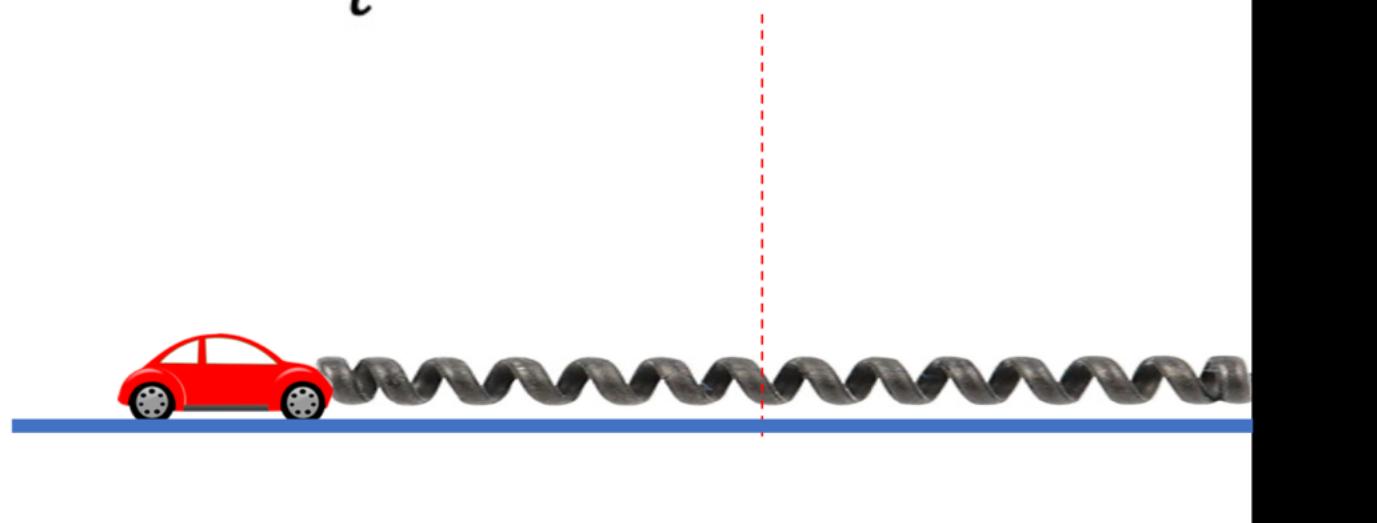
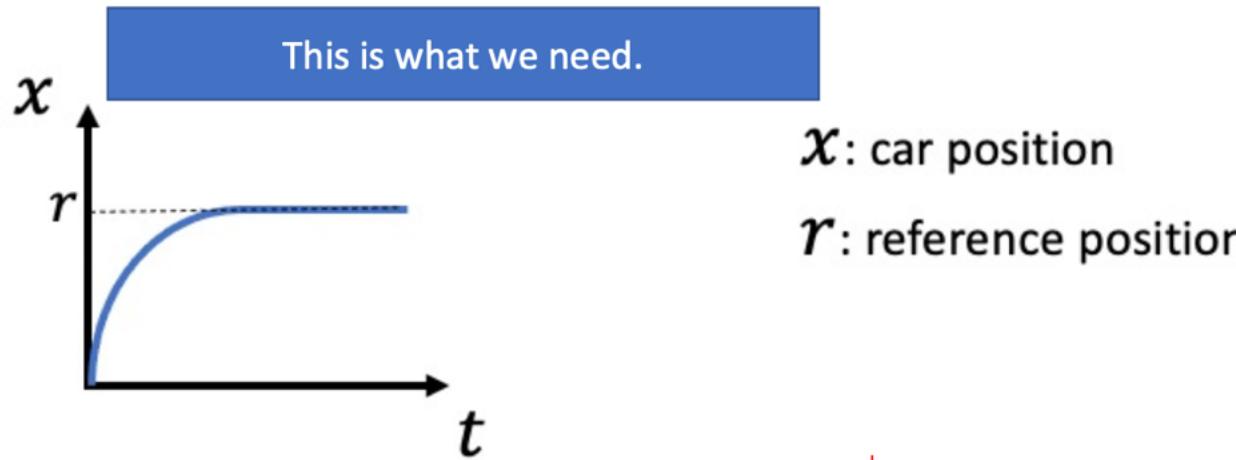


- But what if we want:

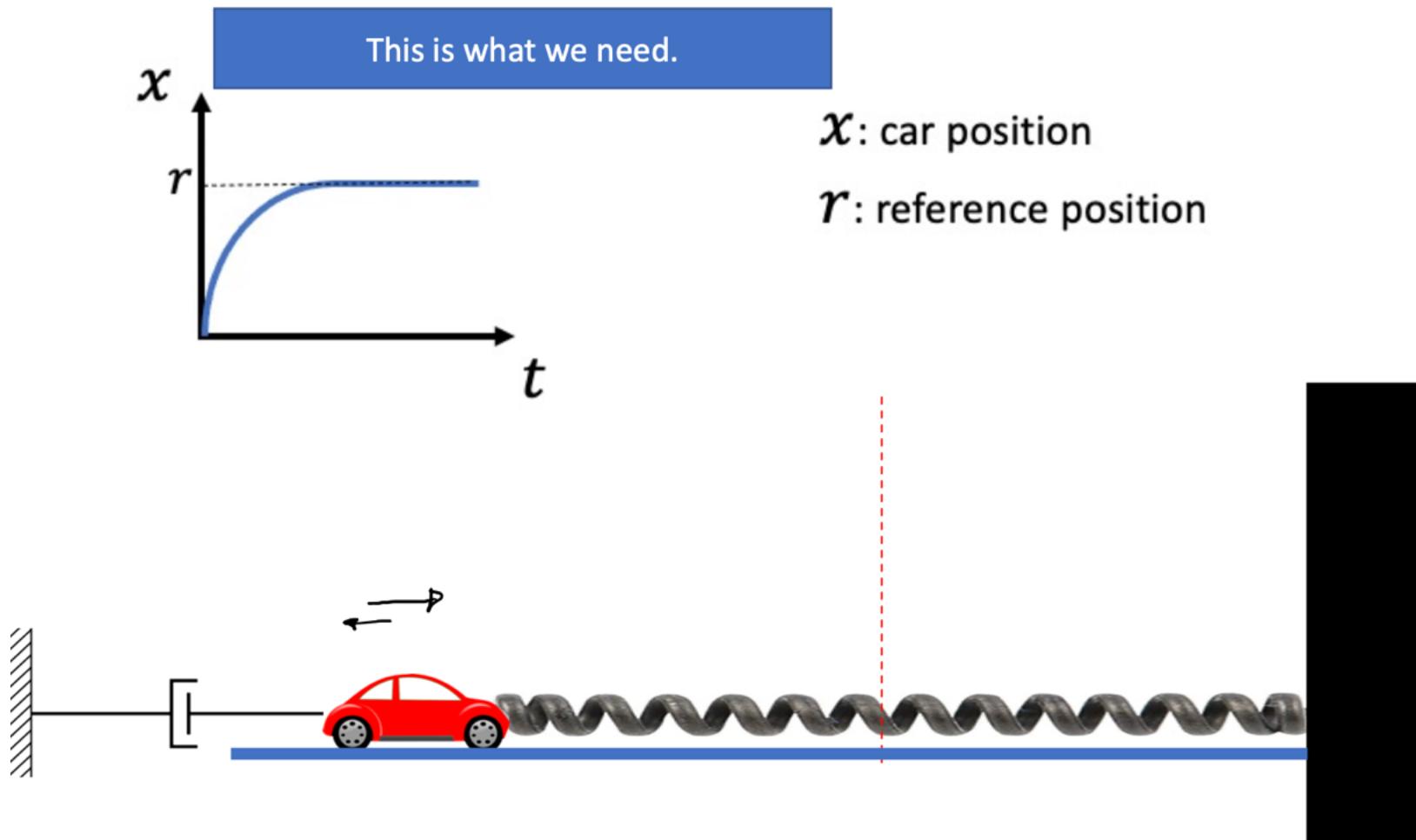


We need different strategies

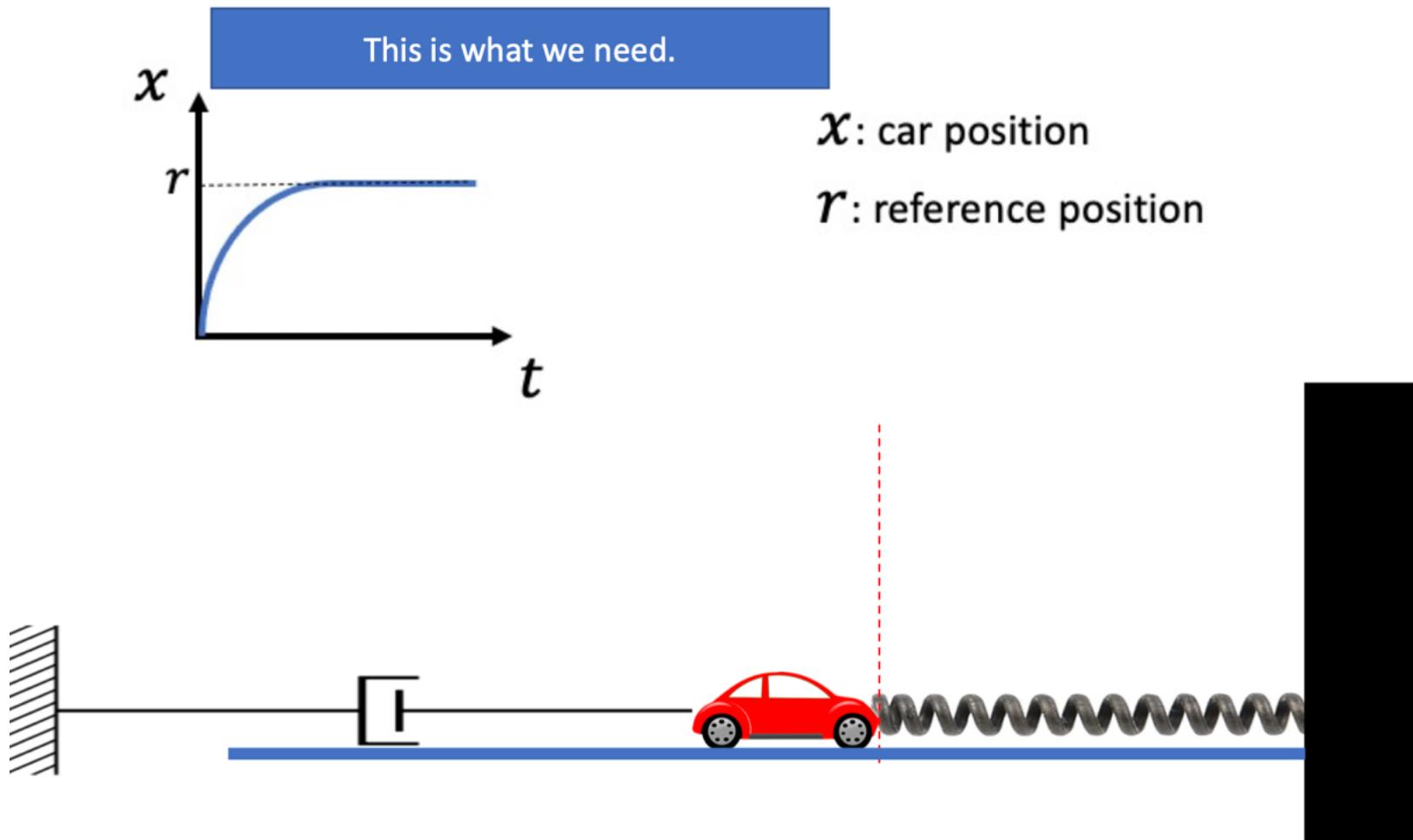
Derivative Controller



Derivative Controller



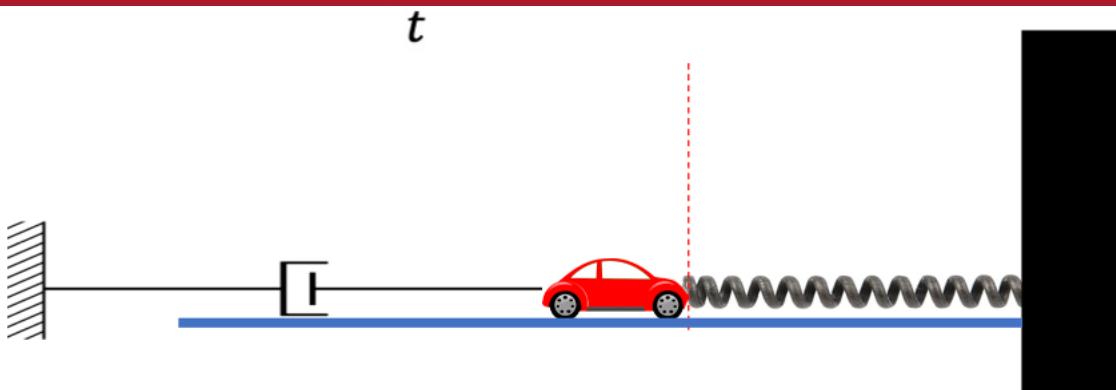
Derivative Controller



Derivative Controller

- **Adding a Derivative Controller ($K_d \cdot s$) is equivalent to adding a Damper!**

Derivative Controller

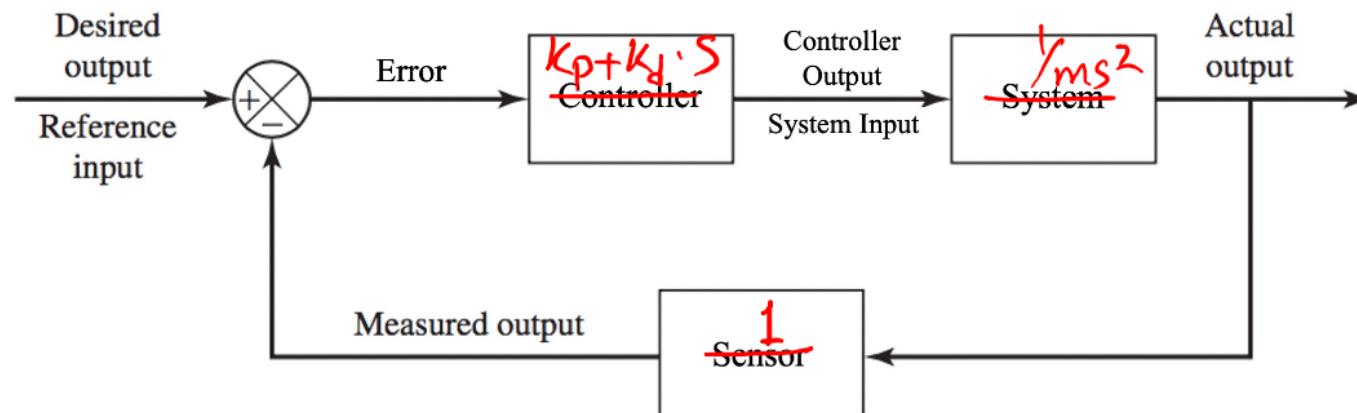


$$F(s) = K_p \cdot E(s) + K_d \cdot \dot{E}(s)$$

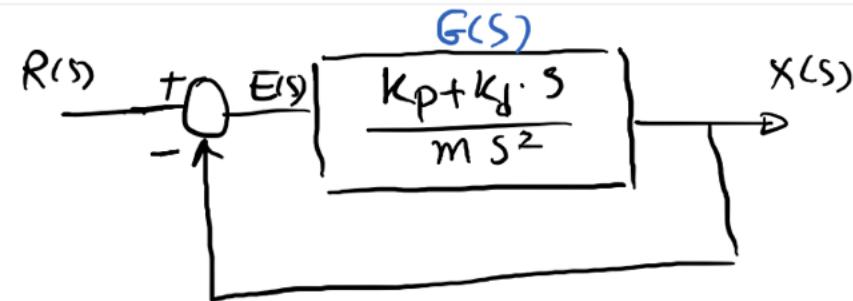
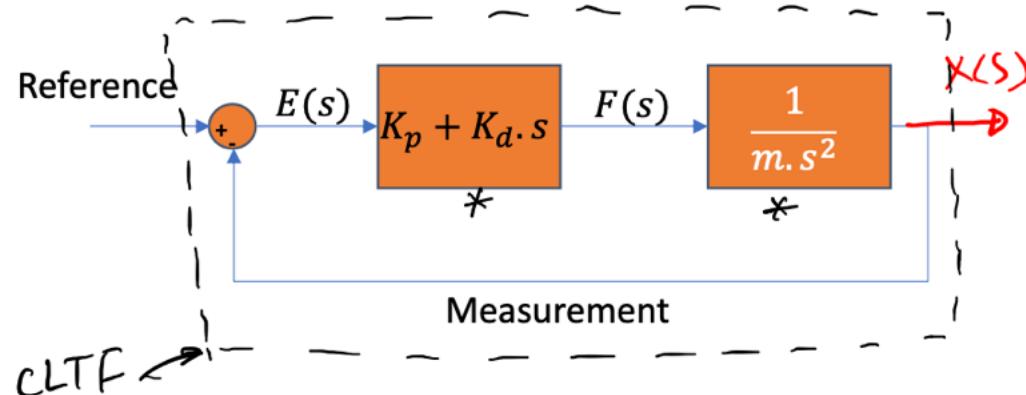
\Rightarrow time domain: $F = K_p e + K_d \dot{e}$

\Rightarrow S-domain: $\frac{F(s)}{E(s)} = C(s) = K_p + K_d \cdot s$

$$E(s) \xrightarrow{K_p + K_d \cdot s} F(s)$$



Derivative Controller



$$\Rightarrow CLTF = \frac{G(s)}{1 + G(s)}$$

$$CLTF = \frac{k_d \cdot s + k_p}{m s^2 + k_d \cdot s + k_p}$$

$R(s)$

$X(s)$

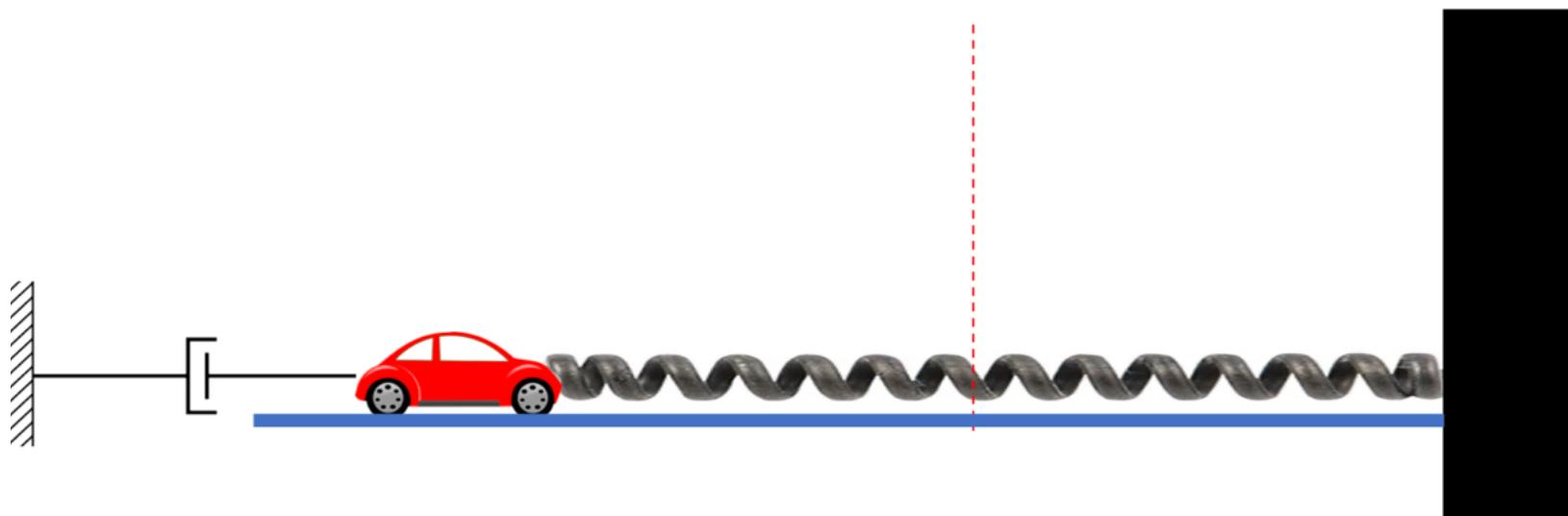
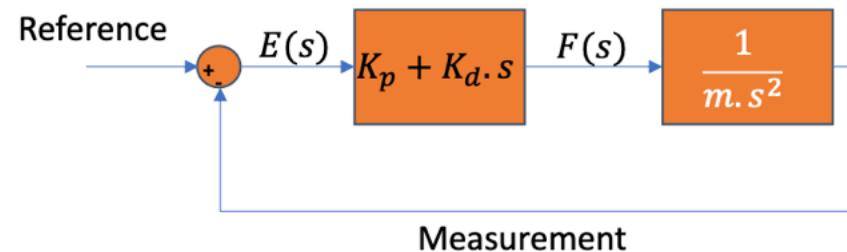
$$m = 500$$

$$k_p > 0$$

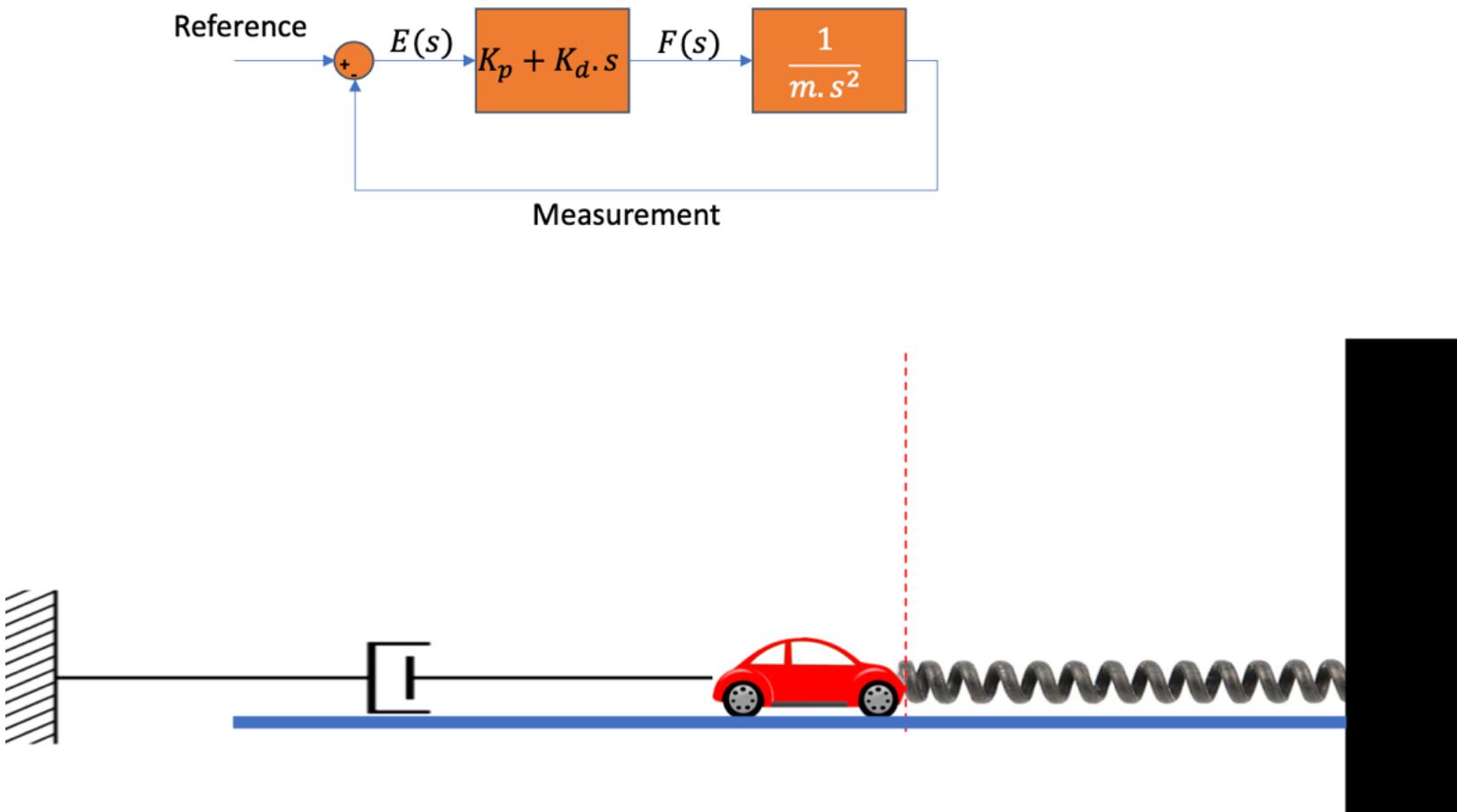
$$k_d > 0$$



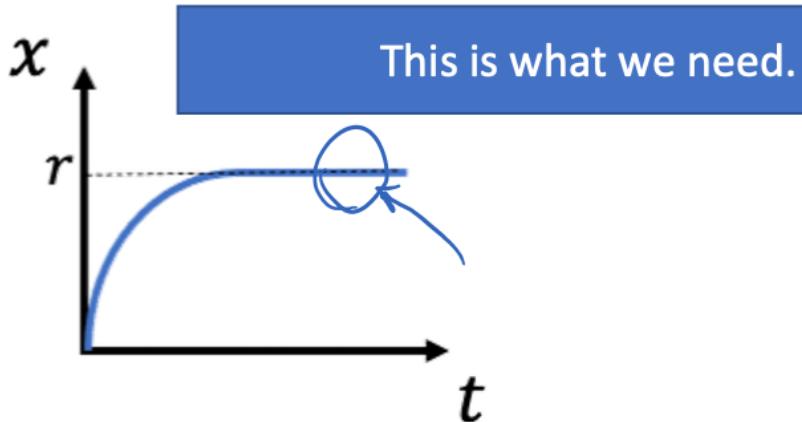
Derivative Controller



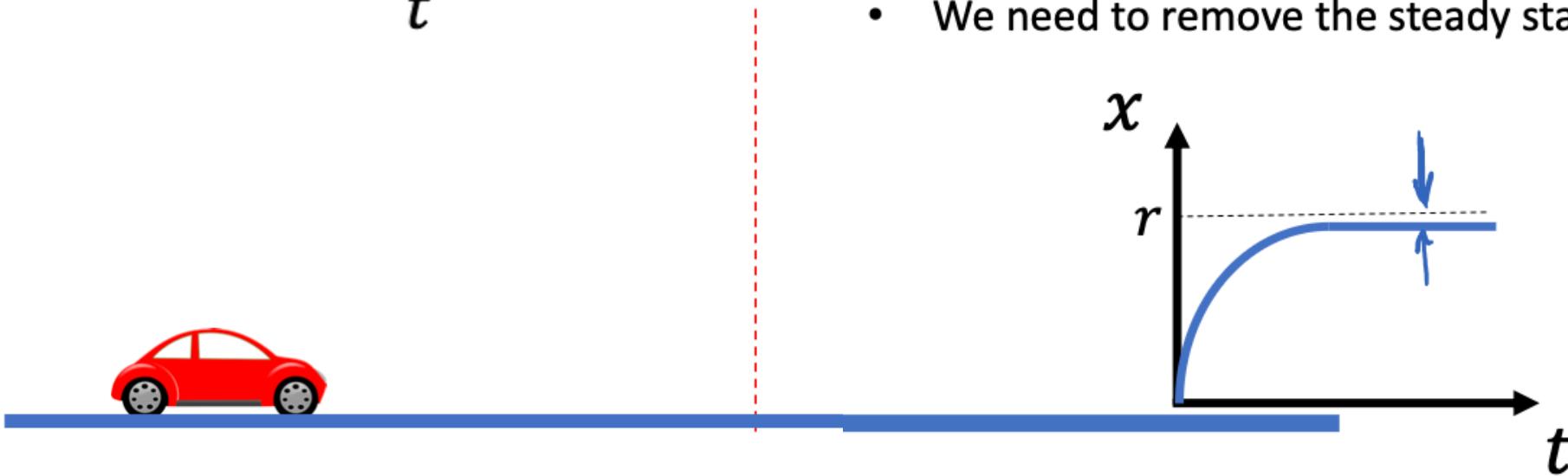
Derivative Controller



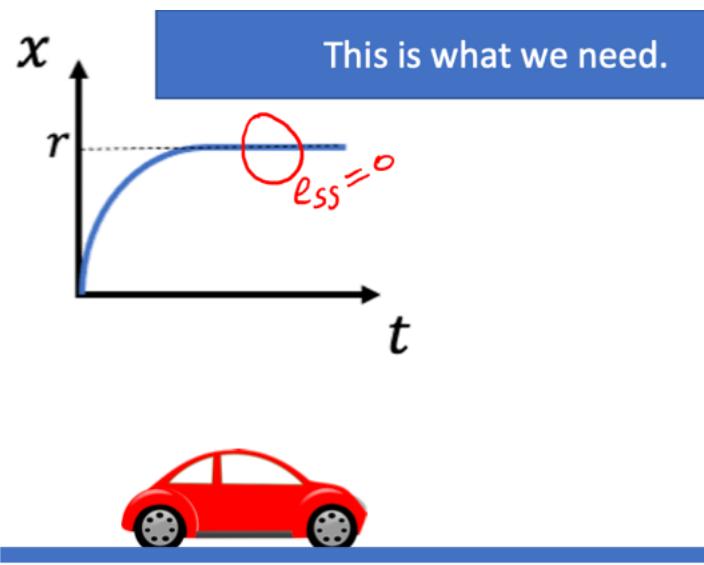
Remove the Steady-state Error



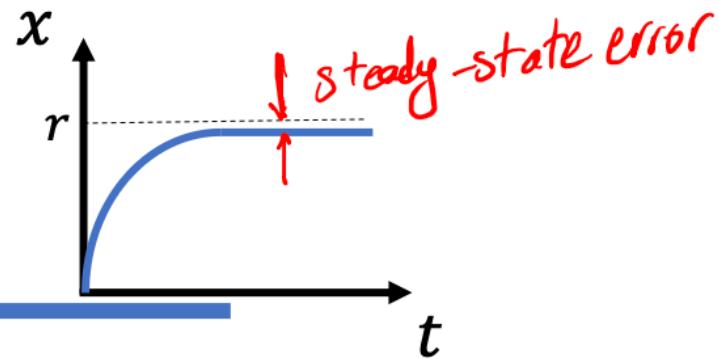
- Good, but it is not enough.
- We need to remove the steady state error.



Integral Controller



- Good, but it is not enough.
- We need to remove the steady state error.



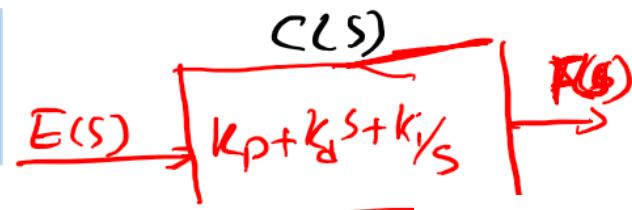
PID in time domain : $F = K_p + K_d \dot{e} + K_i \int e dt$

- For that we will add a term to the controller with the integral of the error

in S-domain :

$$\int F(s) = K_p + K_d s E(s) + \frac{K_i E(s)}{s} \Rightarrow \frac{F(s)}{E(s)}$$

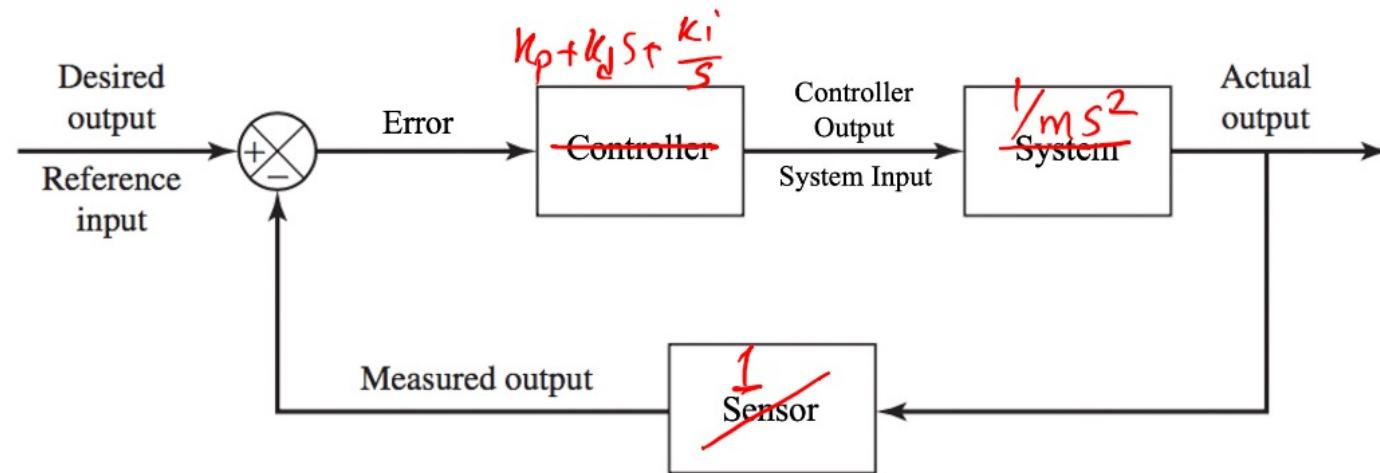
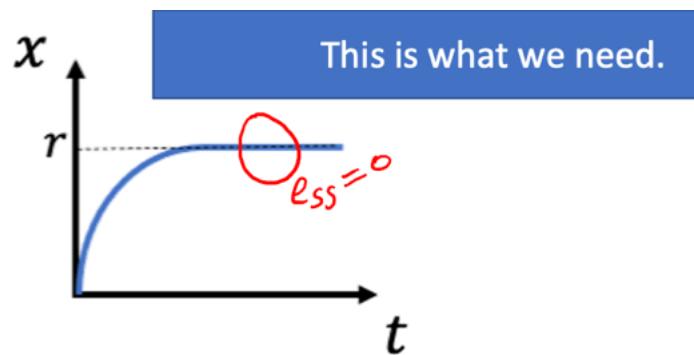
$$C(s) = K_p + K_d \cdot s + \frac{K_i}{s}$$

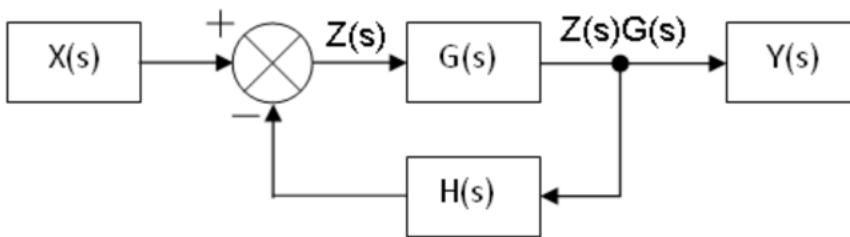


Integral Controller

- Adding an Integral Controller (K_i/s) will help removing the Steady-state Error!

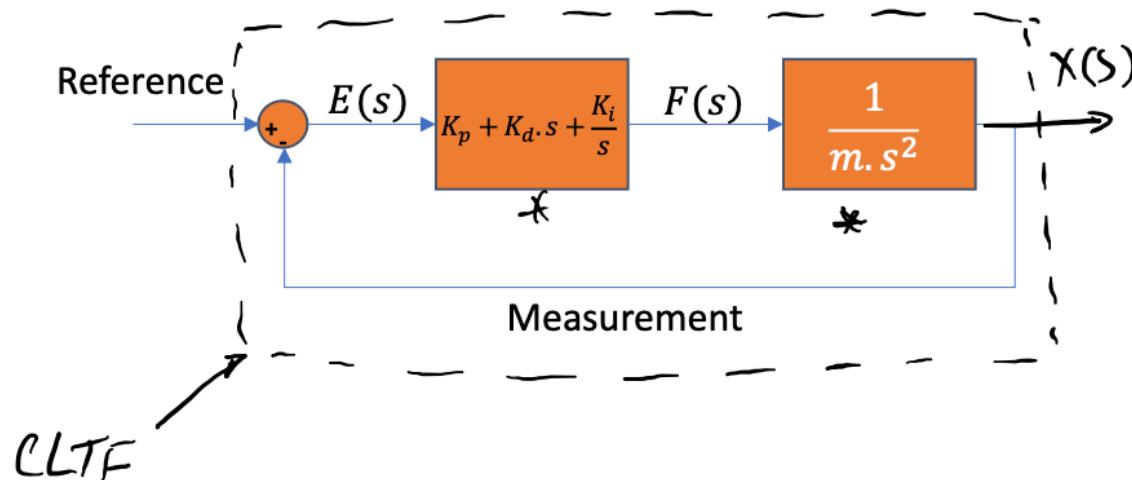
Integral Controller



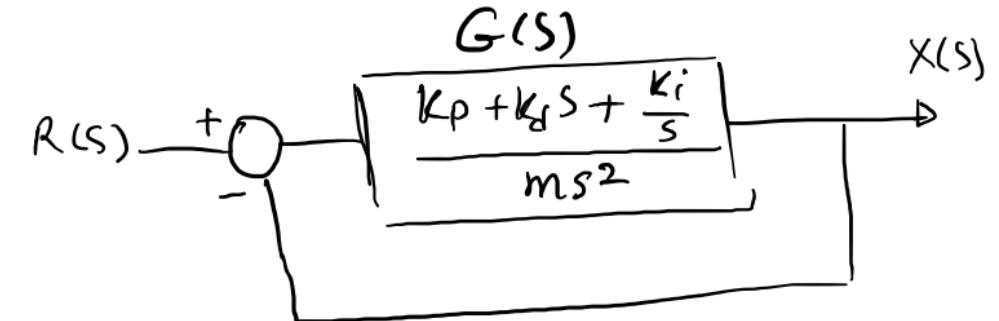


$$\frac{Y(s)}{X(s)} = \frac{G(s)}{1 + G(s)H(s)}$$

Integral Controller



CLTF



$$\frac{X(s)}{R(s)} = \frac{G(s)}{1 + G(s)}$$

$$\frac{X(s)}{R(s)} = CLTF = \frac{k_d s^2 + k_p s + k_i}{m s^3 + k_d s^2 + k_p s + k_i}$$

$$m = 500$$

$$k_p, k_d, k_i > 0$$



PID Controller - Gains

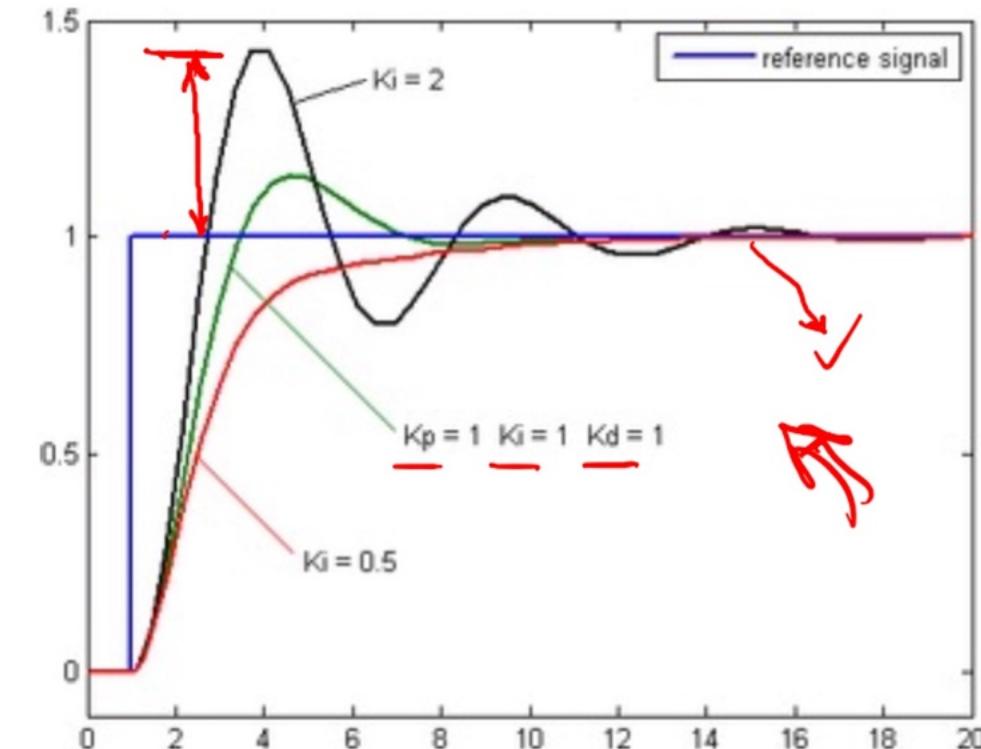
- This is PID controller in time domain (proportional, integral, derivative)

$$F = K_p e + K_d \dot{e} + K_i \int e$$

- This is PID controller in s-domain (complex frequency domain)

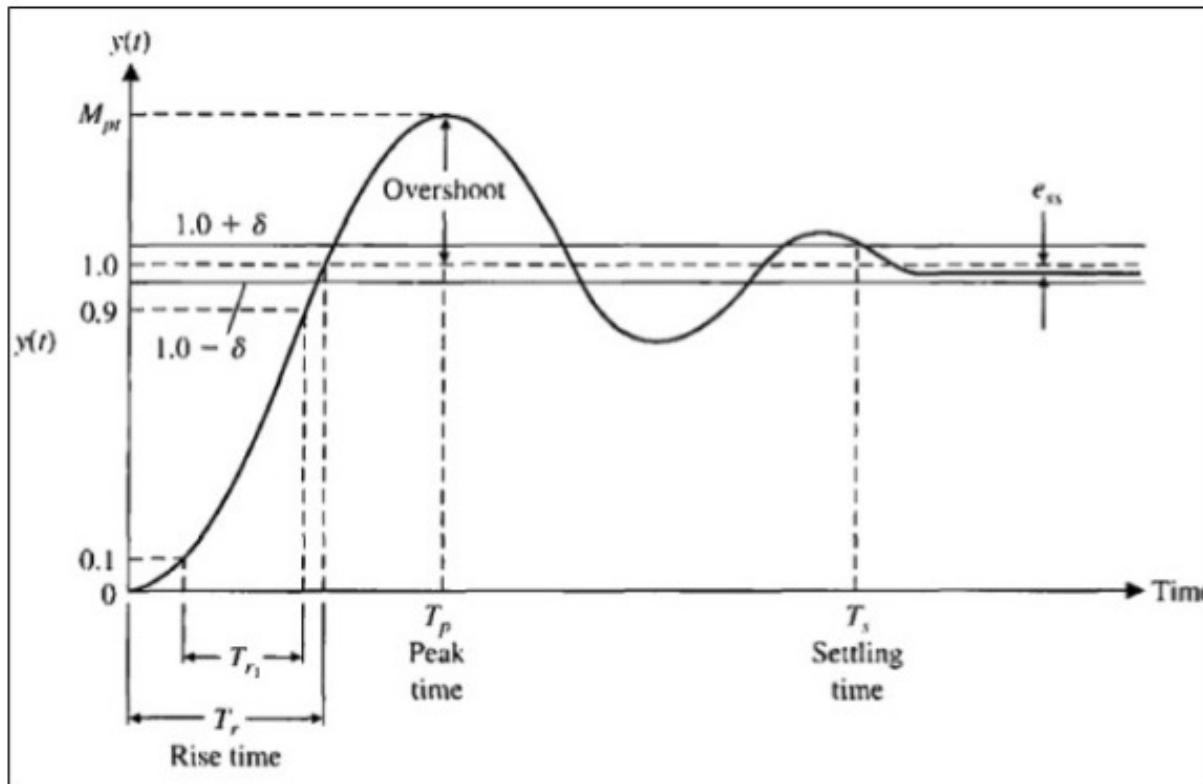
$$\frac{F(s)}{E(s)} = C(s) = K_p + K_d \cdot s + \frac{K_i}{s}$$

- The K_p , K_i and K_d are the **gains** of the controller
 - They are oftentimes tuned:
 - Trial error
 - There are also systematic procedures for tuning them

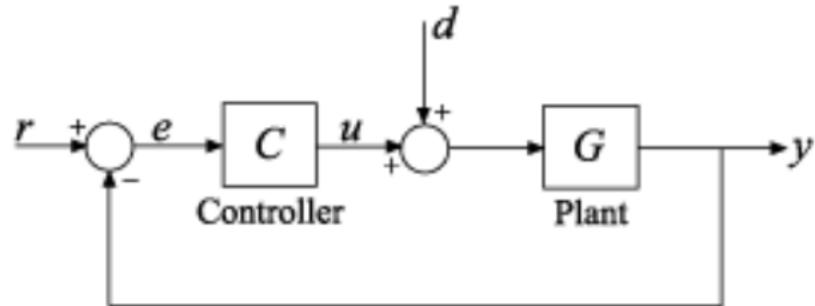


PID Controller - Gains effects

Parameter	Rise time	Overshoot	Settling time	Steady-state error	Stability
K_p	Decrease	Increase	Small change	Decrease	Degrade
K_i	Decrease	Increase	Increase	Eliminate	Degrade
K_d	Minor change	Decrease	Decrease	No effect in theory	Improve if K_d small



Tune PID Controller to Favor Reference Tracking or Disturbance Rejection (PID Tuner) - in MATLAB



$$Plant = \frac{0.3}{s^2 + 0.1s}.$$

Design Initial PI Controller

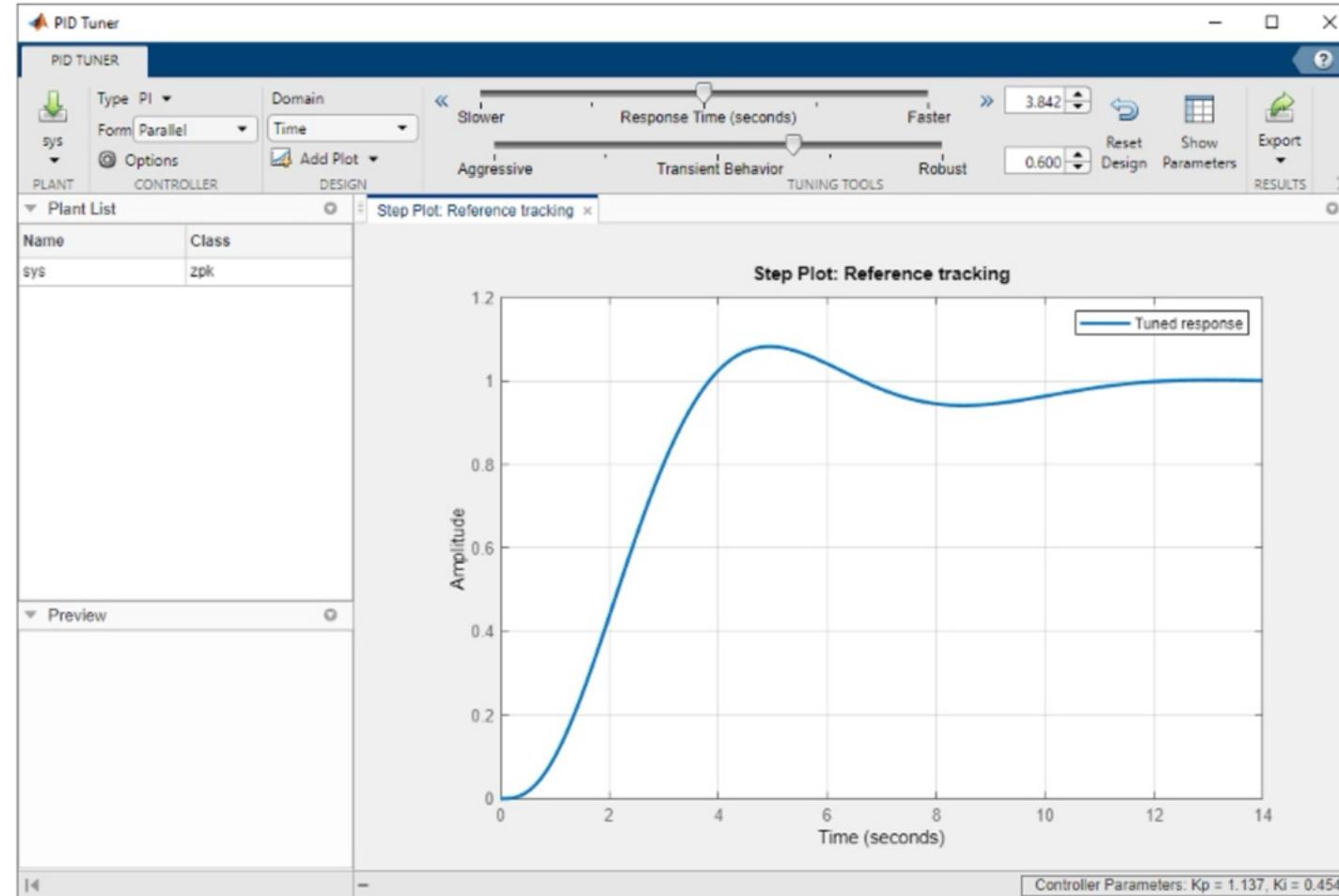
Having an initial controller design provides a baseline against which you can compare results as you tune a PI controller. Create an initial PI controller design for the plant using PID tuning command `pidtune`.

```
G = tf(0.3,[1,0.1,0]); % plant model  
C = pidtune(G,'PI');
```

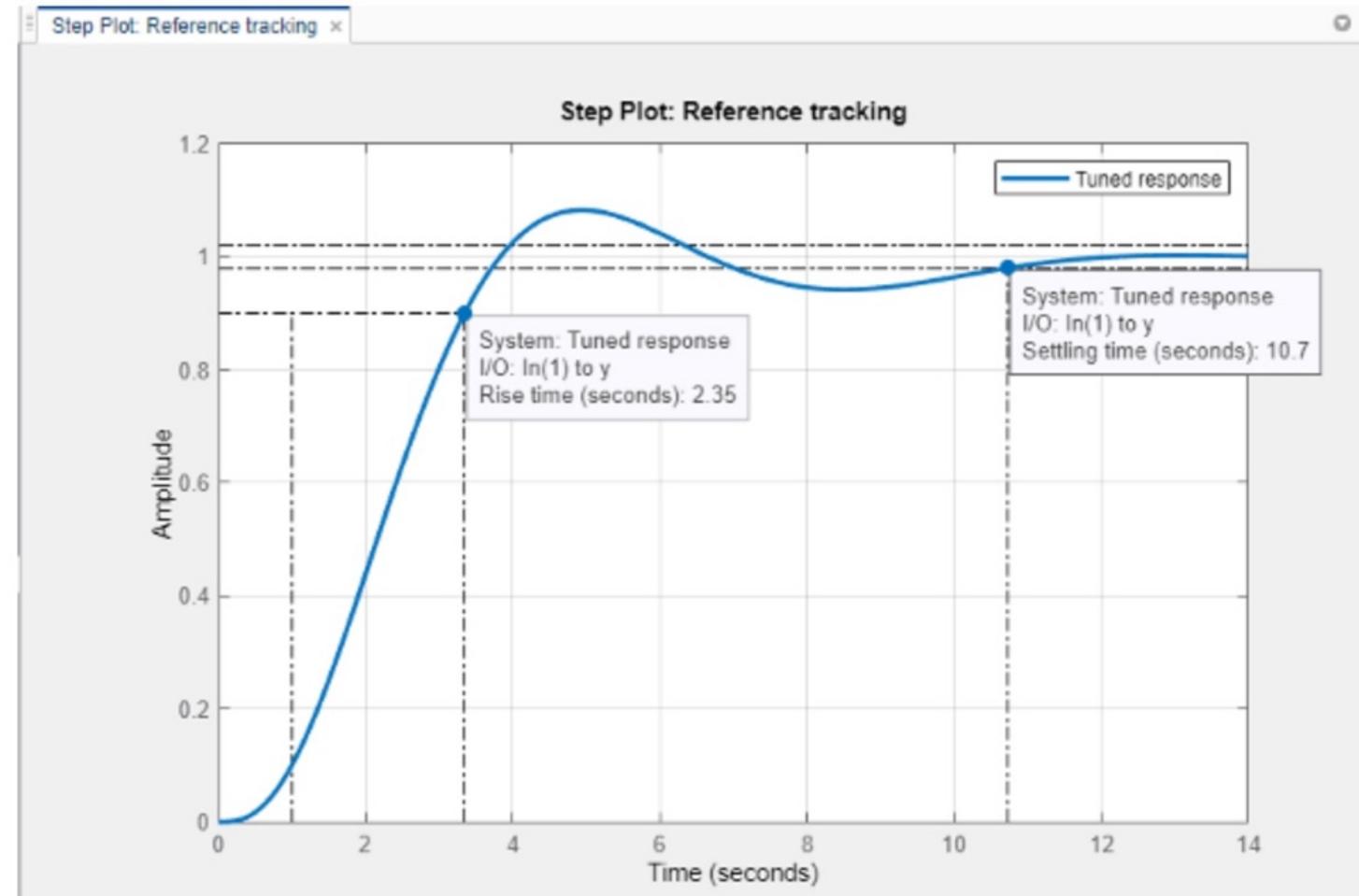
Use the initial controller design to open **PID Tuner**.

```
pidTuner(G,C)
```

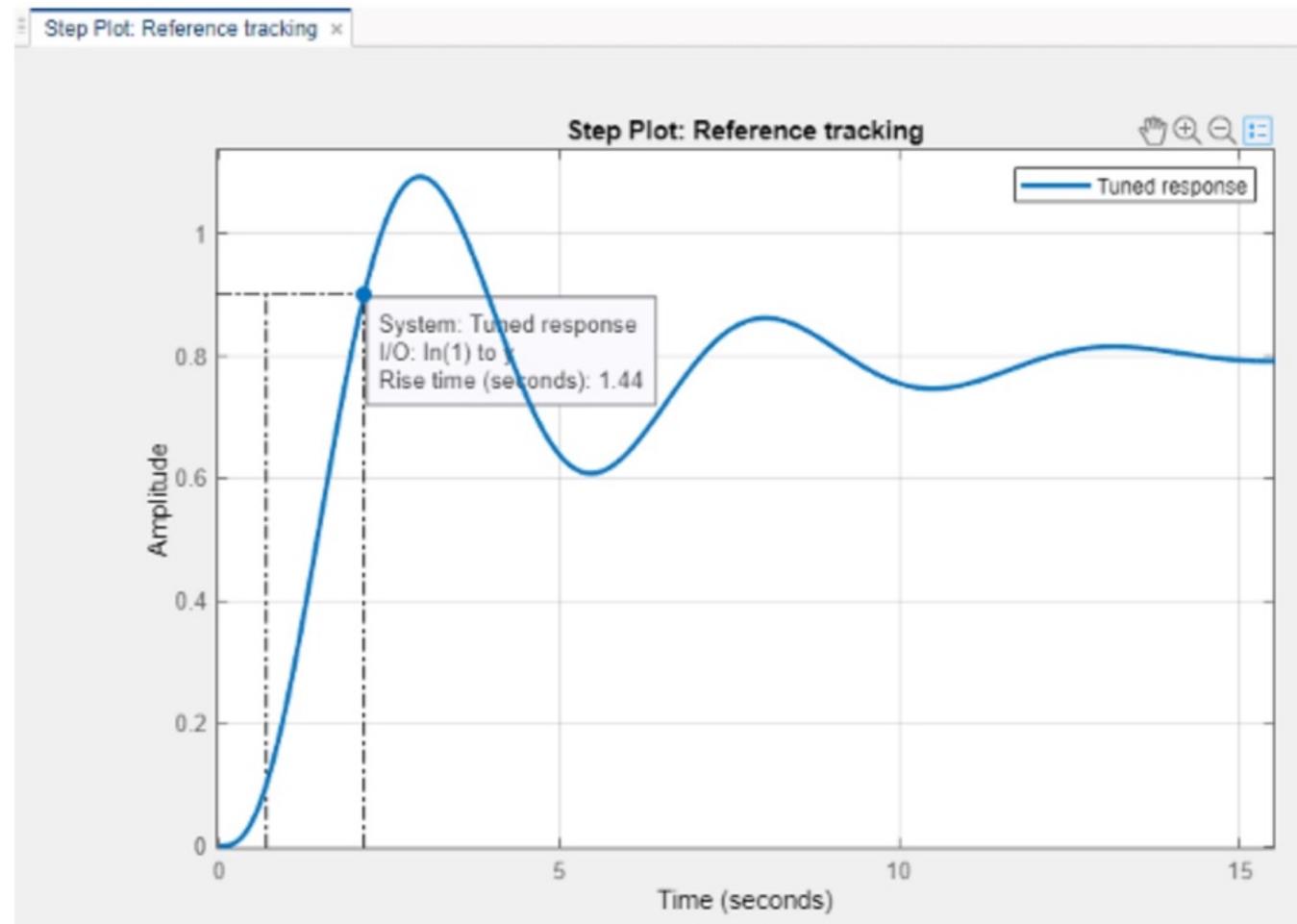
Tune PID Controller to Favor Reference Tracking or Disturbance Rejection (PID Tuner) - in MATLAB



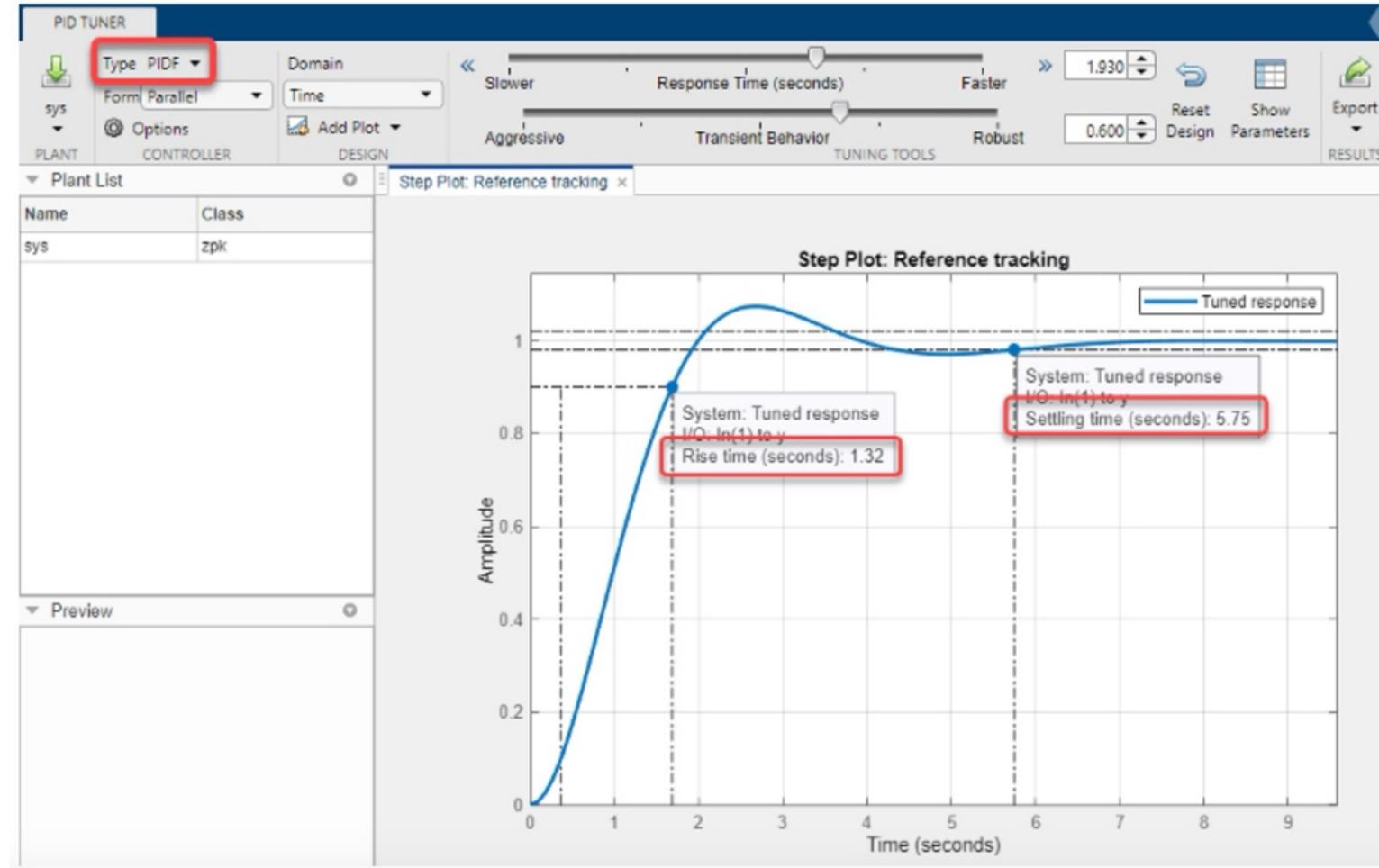
Tune PID Controller to Favor Reference Tracking or Disturbance Rejection (PID Tuner) - in MATLAB



Tune PID Controller to Favor Reference Tracking or Disturbance Rejection (PID Tuner) - in MATLAB



Tune PID Controller to Favor Reference Tracking or Disturbance Rejection (PID Tuner) - in MATLAB



PID Tuner - Example

- Consider a system described by the equation of motion:

$$4\ddot{x} + 20\dot{x} + 25x = f$$

- Design a PD controller using the **pidTuner** function of **MATLAB**.

PID Tuner - Example - in MATLAB

```
>> sys = tf([1],[4,20,25])
```

```
sys =
```

```
1
```

```
-----  
4 s^2 + 20 s + 25
```

Continuous-time transfer function.

```
>> pd = pidtune(sys, 'pd')
```

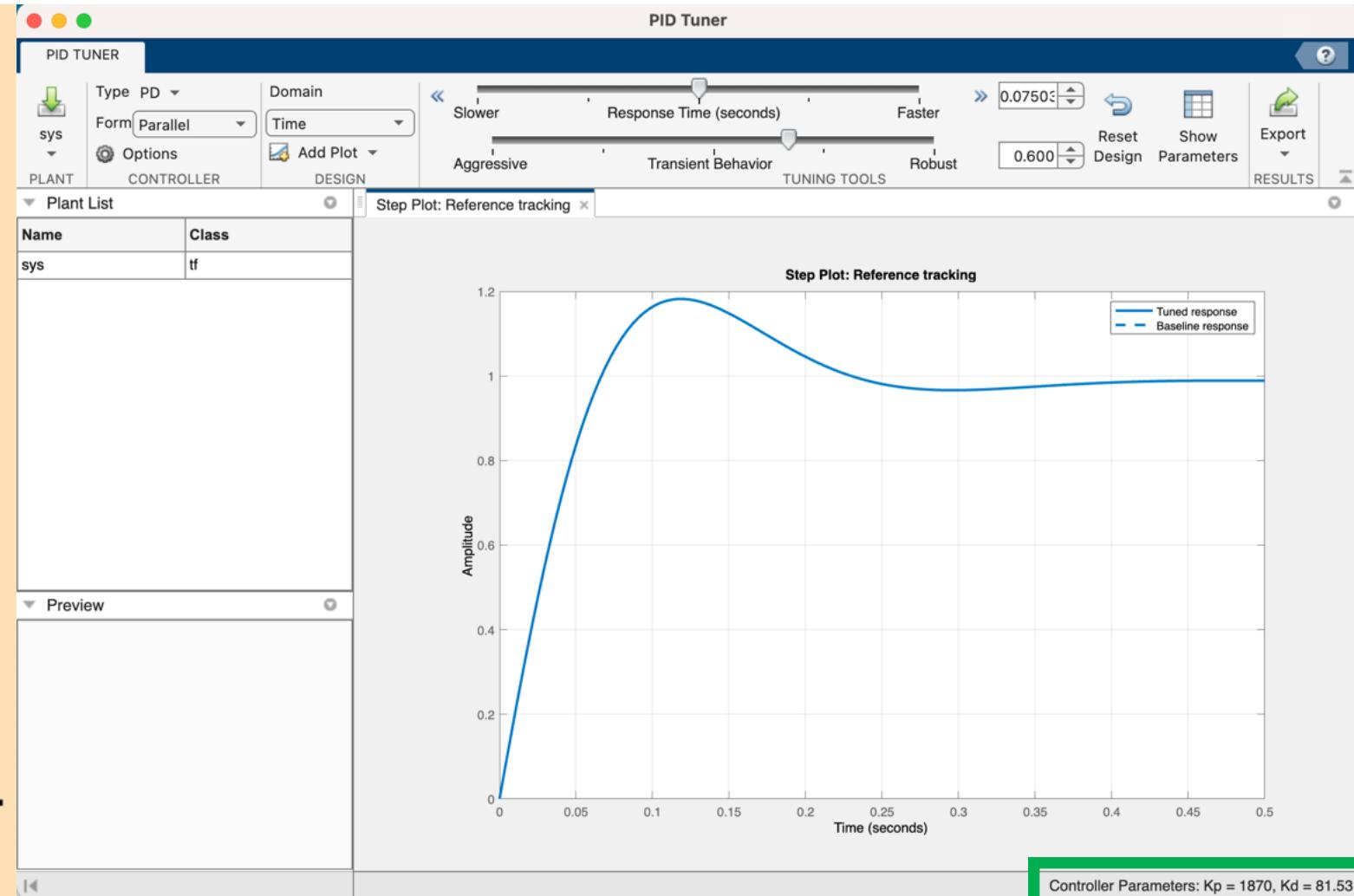
```
pd =
```

```
Kp + Kd * s
```

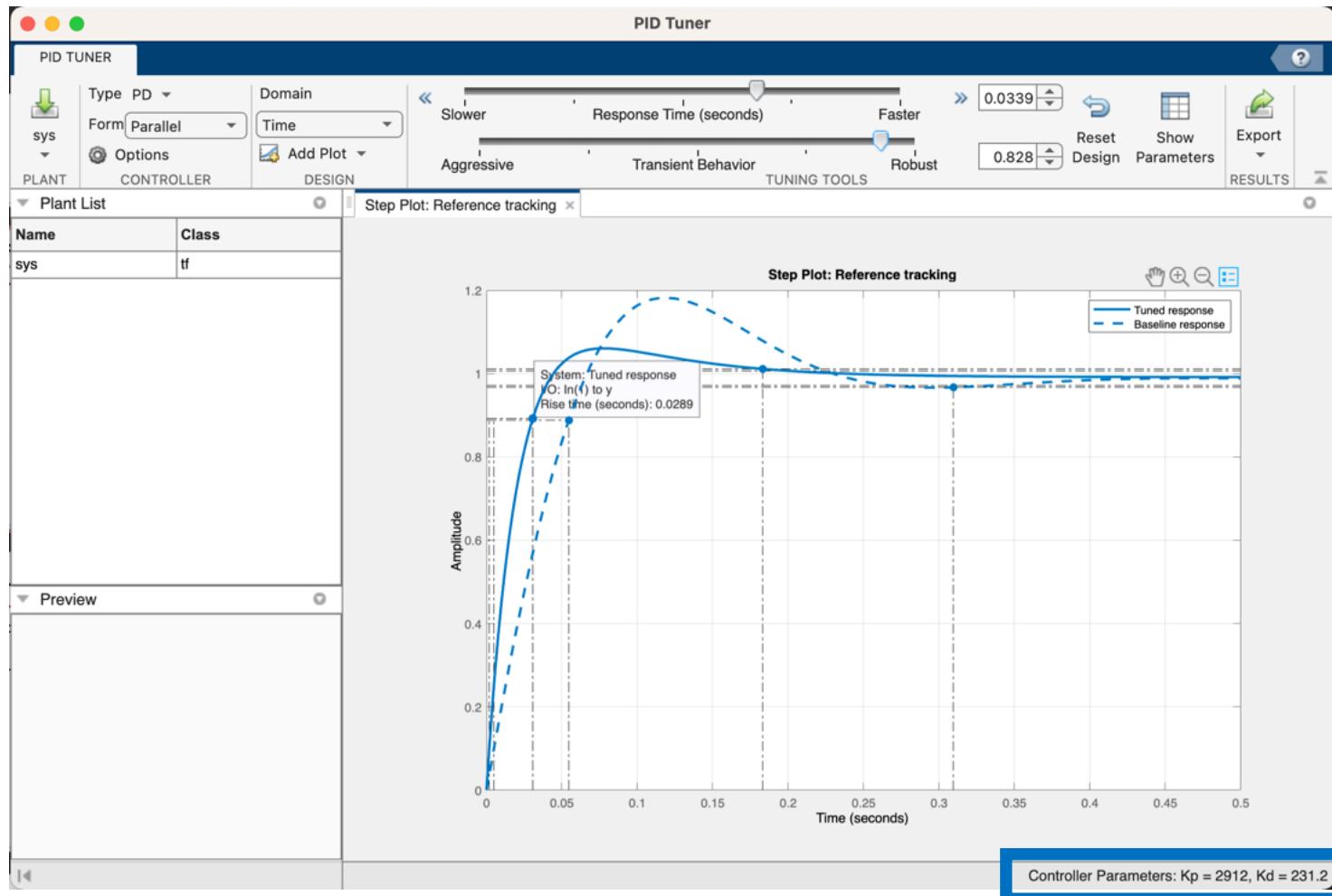
with $K_p = 1.87e+03$, $K_d = 81.5$

Continuous-time PD controller in parallel form.

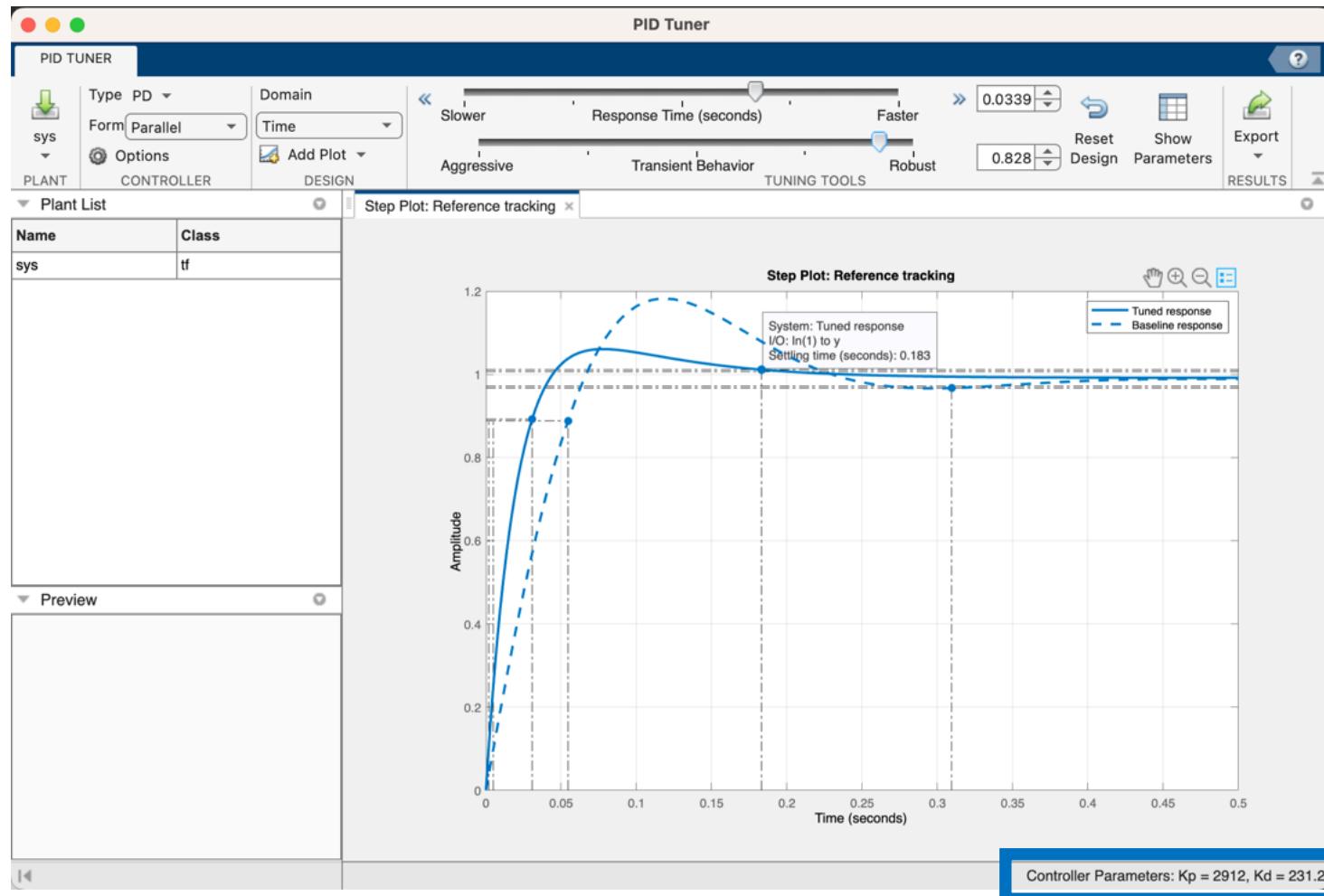
```
>> pidTuner(sys,pd)
```



PID Tuner - Example - in MATLAB (Rise Time)



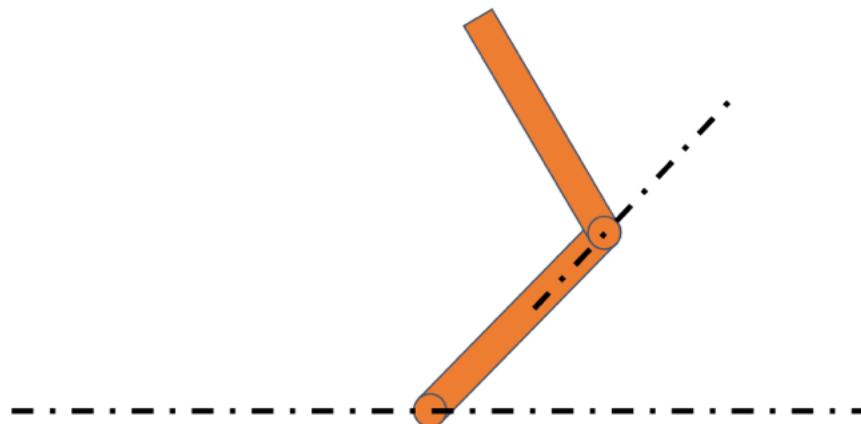
PID Tuner - Example - in MATLAB (Settling Time)



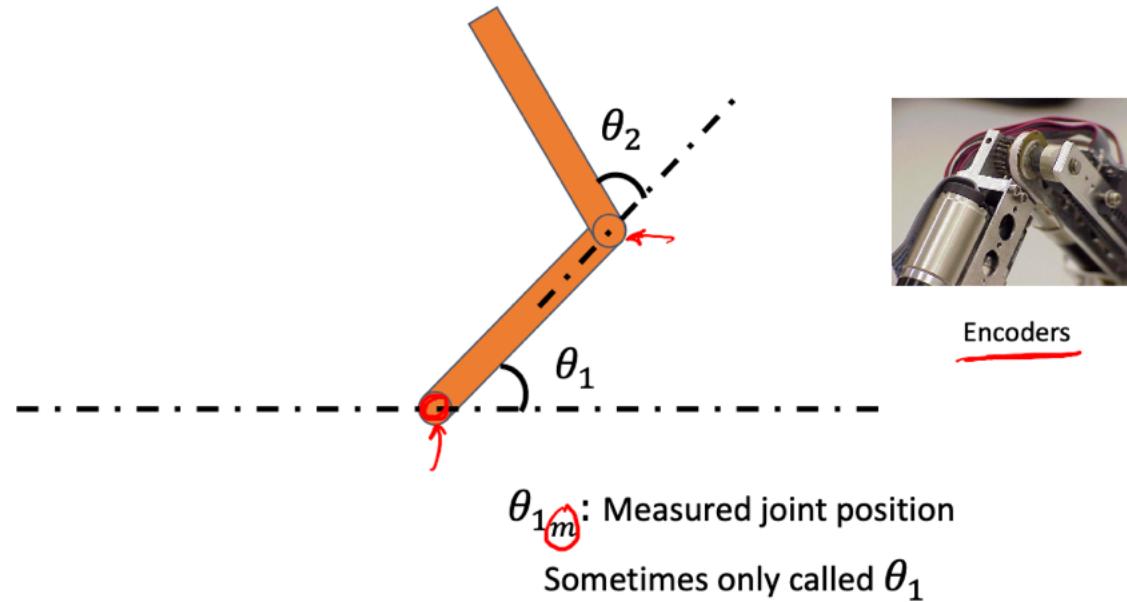
Two-link robotic manipulator



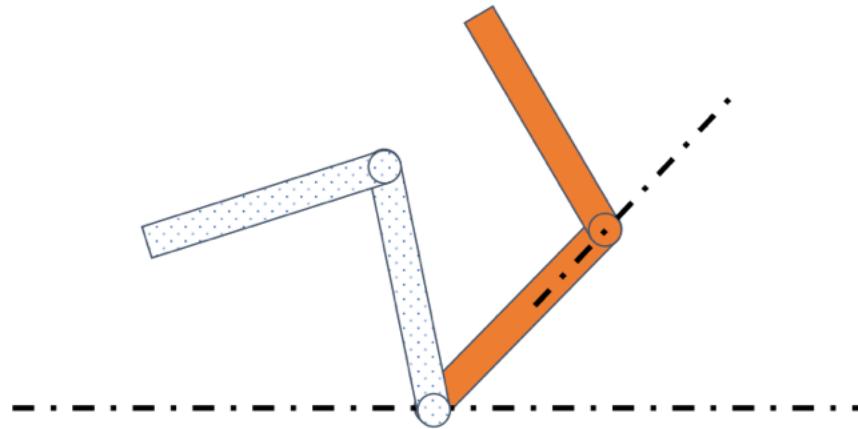
Two-link robotic manipulator



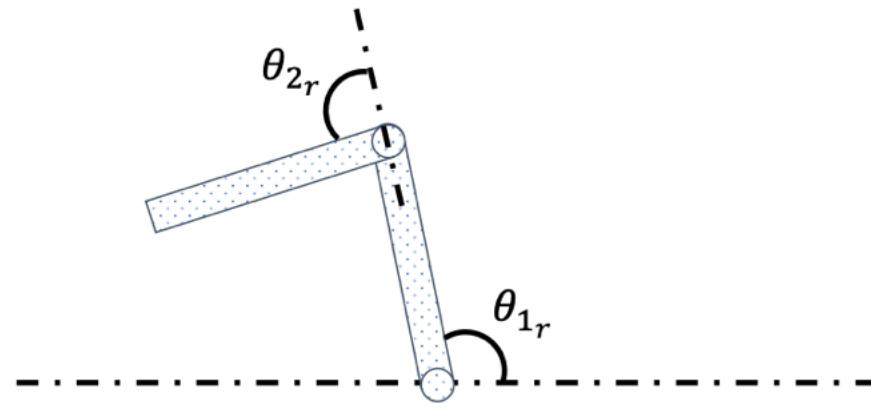
Two-link robotic manipulator - Joint positions



Two-link robotic manipulator - Desired position

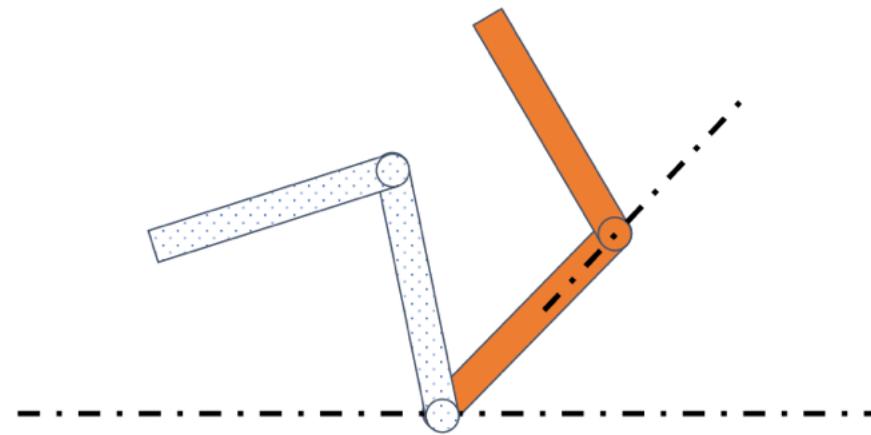


Two-link robotic manipulator - Joint Reference



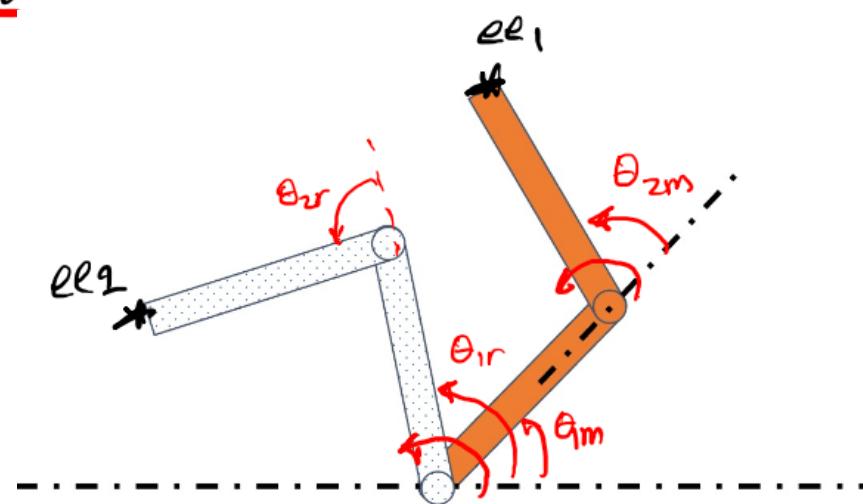
θ_{1r} : Joint reference value

Position Control Problem



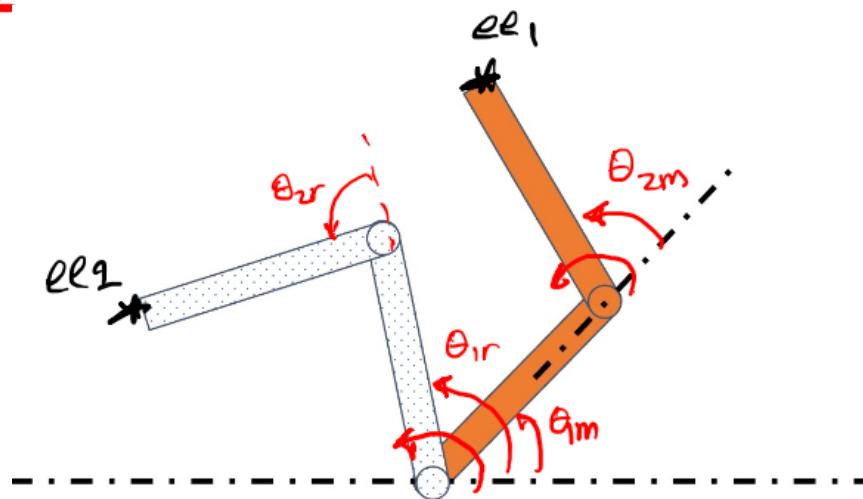
Position Control Problem

- We have a reference position value for the robot: $\underline{\theta_r}$
- We measure the current position of the robot: $\underline{\theta_m}$
- We can supply force: $\underline{\tau}$ or \underline{u}



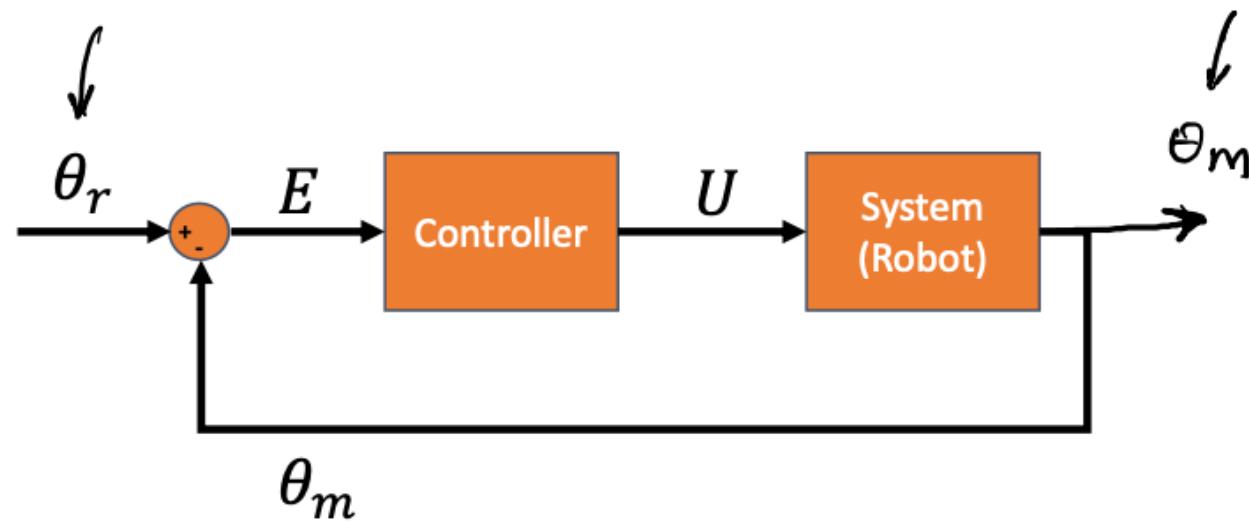
Position Control Problem

- We have a reference position value for the robot: $\underline{\theta_r}$
- We measure the current position of the robot: $\underline{\theta_m}$
- We can supply force: $\underline{\tau}$ or \underline{u}



How should I design u so that θ_m converges to θ_r ?

Position Control Problem



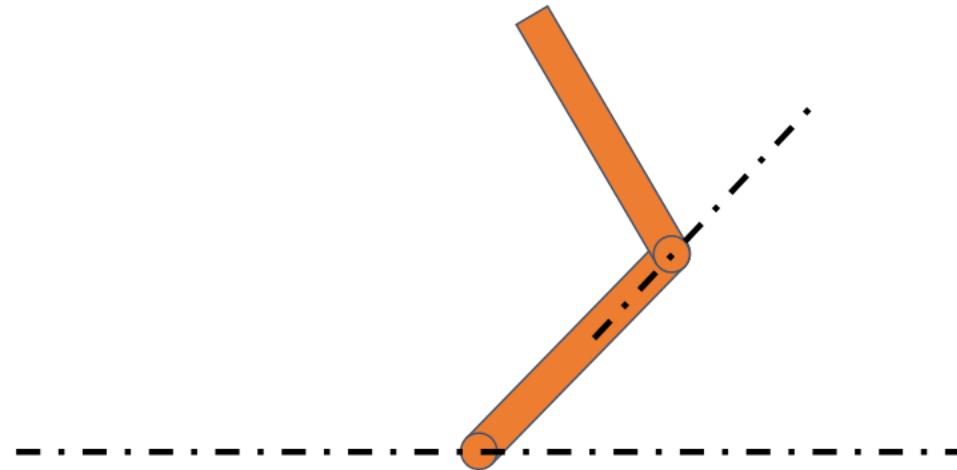
Position Control Problem

- What we have just mentioned is **joint space position control!**
- The end-effector position is given in **task space**.
- What do we do?



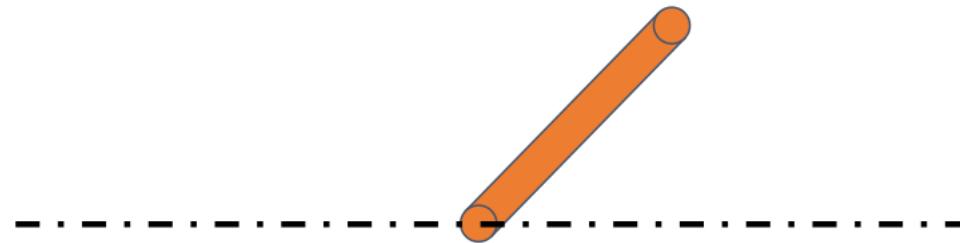
Position Control Problem

- Single input, single output (SISO) systems
 - Joints will be handled one by one



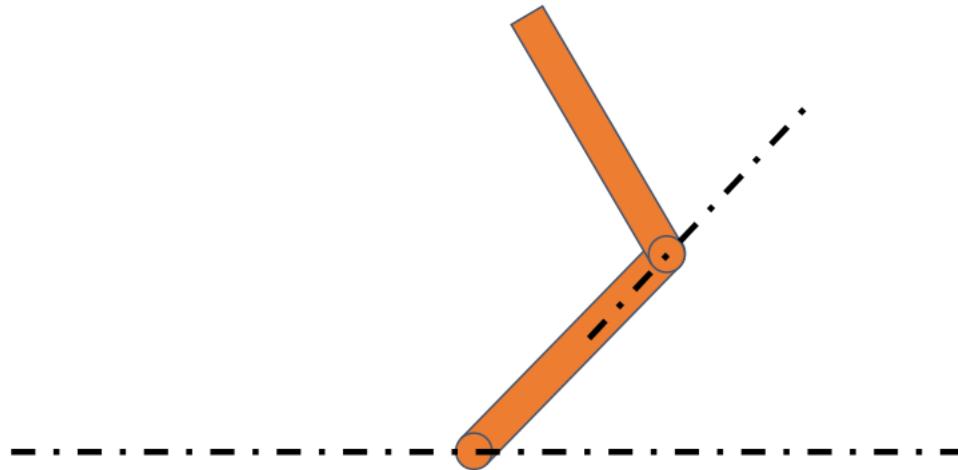
Position Control Problem

- Control the first link



Position Control Problem

- Control the second link



Position Control Problem

- So, we will learn about 1-link arm robot,
and it can be repeated for other links as well !!!

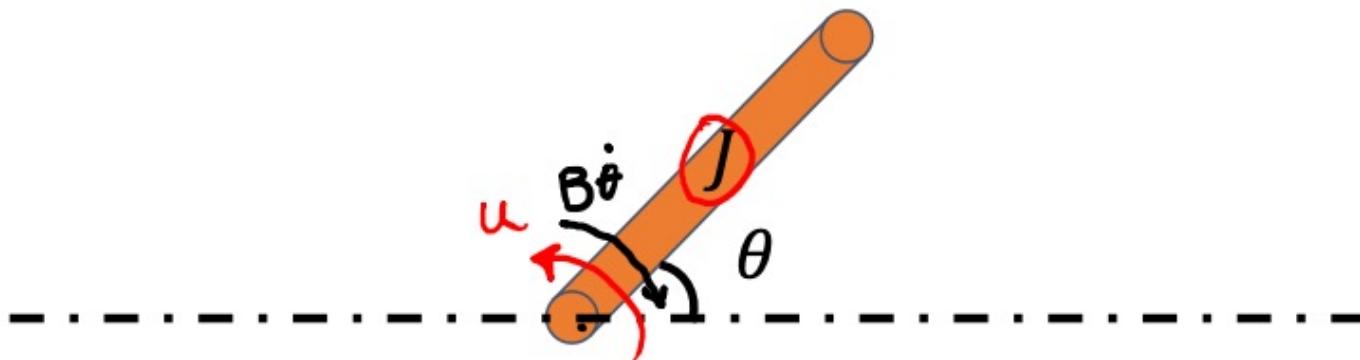
Steps for controlling a given system

1. Dynamic model
2. Transfer Function
3. Evaluation / Analysis
4. Add Controller (P, PD, PI, PID) and close the loop

1. Dynamic model

$$\tau_{\text{net}} = J \ddot{\theta}$$

torque inertia angular acceleration



$$u = J \ddot{\theta} + B \dot{\theta}$$

2. Transfer Function

$$\mathcal{L} \rightarrow \boxed{U = Js^2\theta + Bs\theta}$$
$$u = J\ddot{\theta} + B\dot{\theta}$$

$$U = Js^2\theta + Bs\theta$$

$$U = (Js^2 + Bs)\theta$$

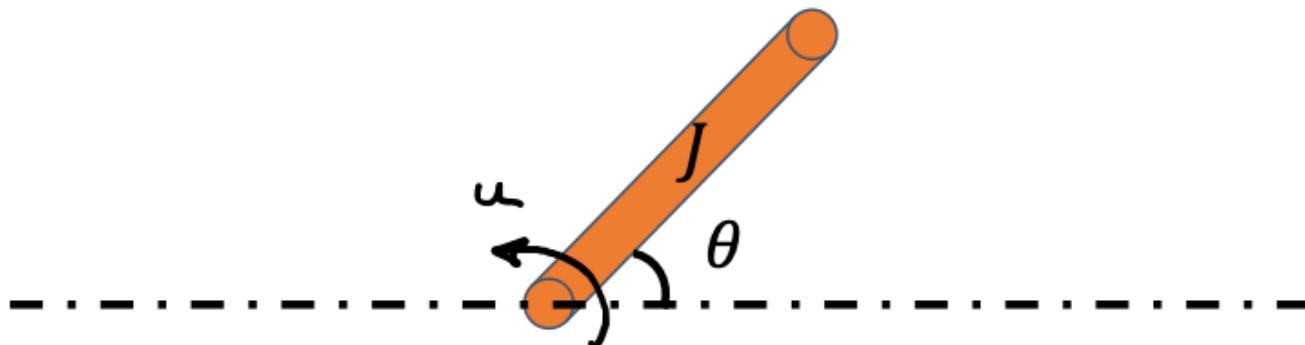
Output Signal

Input Signal

$$\frac{1}{U} = \frac{1}{(Js^2 + Bs)}$$

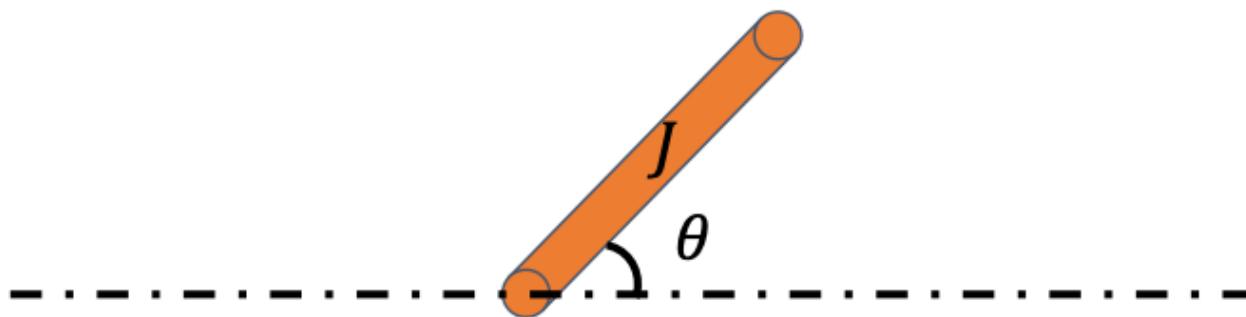
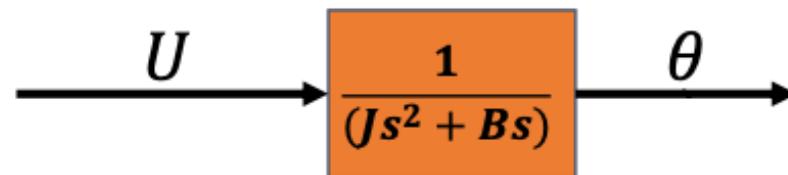
Transfer function
of our system

→ A transfer function transforms one signal to the other



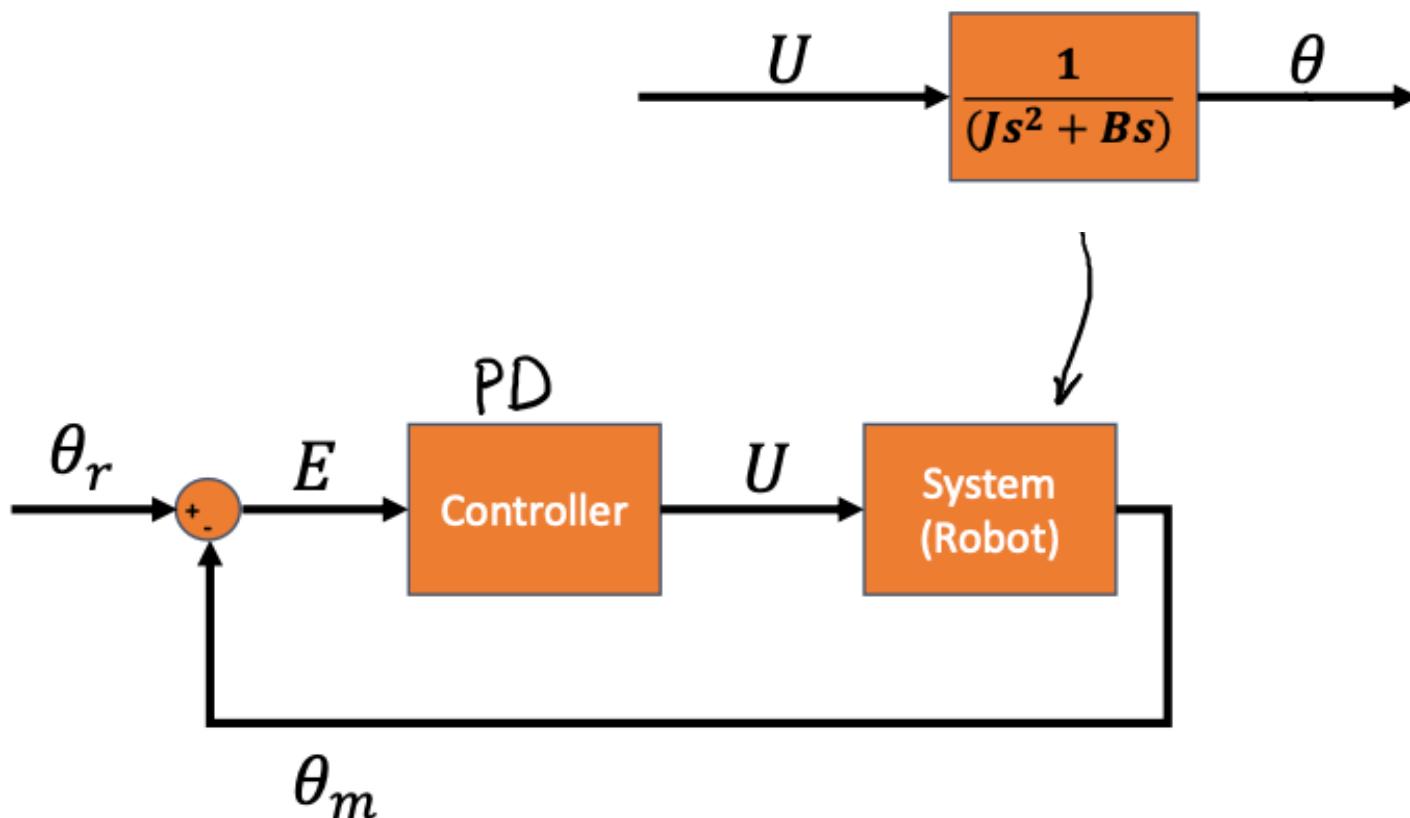
3. Evaluation / Analysis

$$\frac{\theta}{U} = \frac{1}{(Js^2 + Bs)}$$

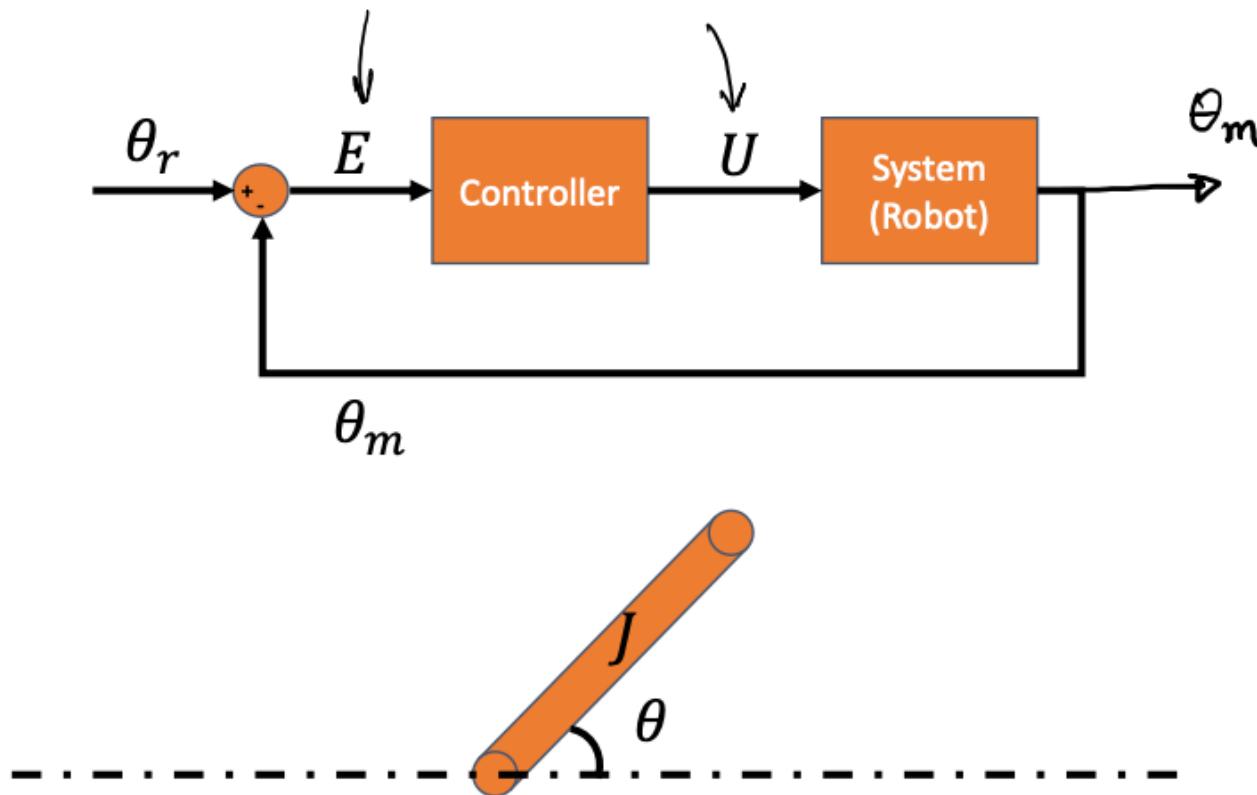


In Block Diagram

$$\frac{\theta}{U} = \frac{1}{(Js^2 + Bs)}$$



4. Add PD Controller and close the loop



PD Controller

- PD controller is

$$u(t) = K_p e(t) + K_d \dot{e}(t)$$

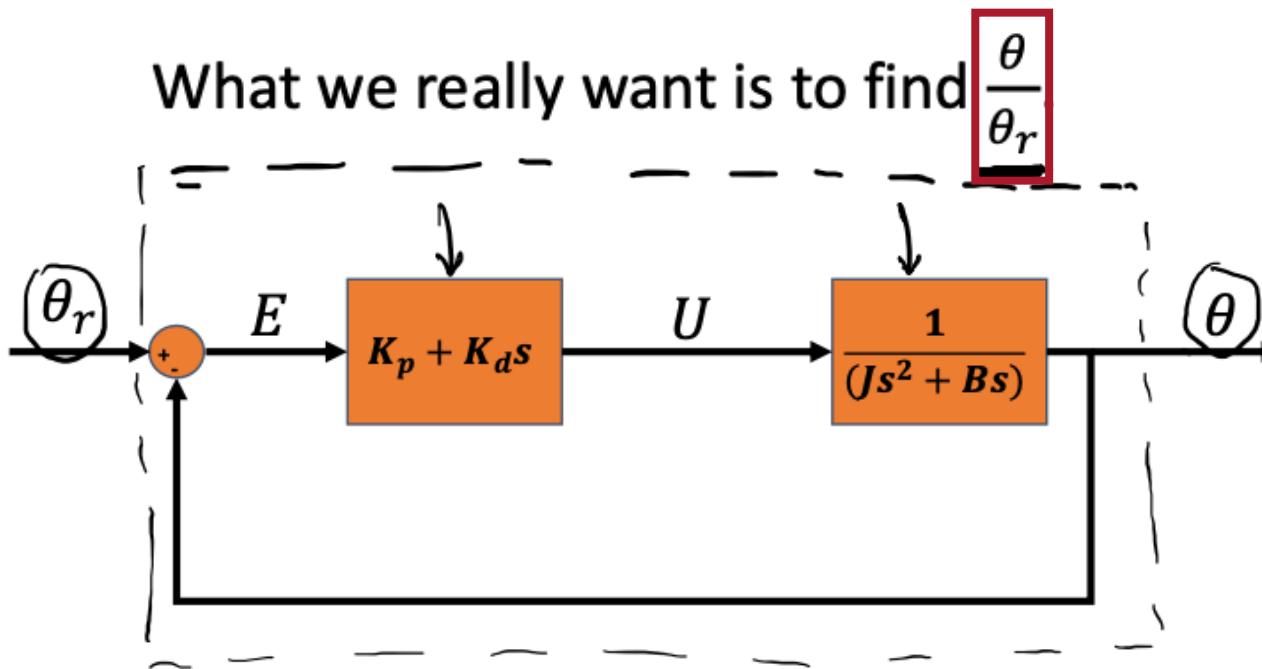
- In frequency domain

$$U(s) = K_p E(s) + K_d s E(s)$$

- Transfer function of our controller is

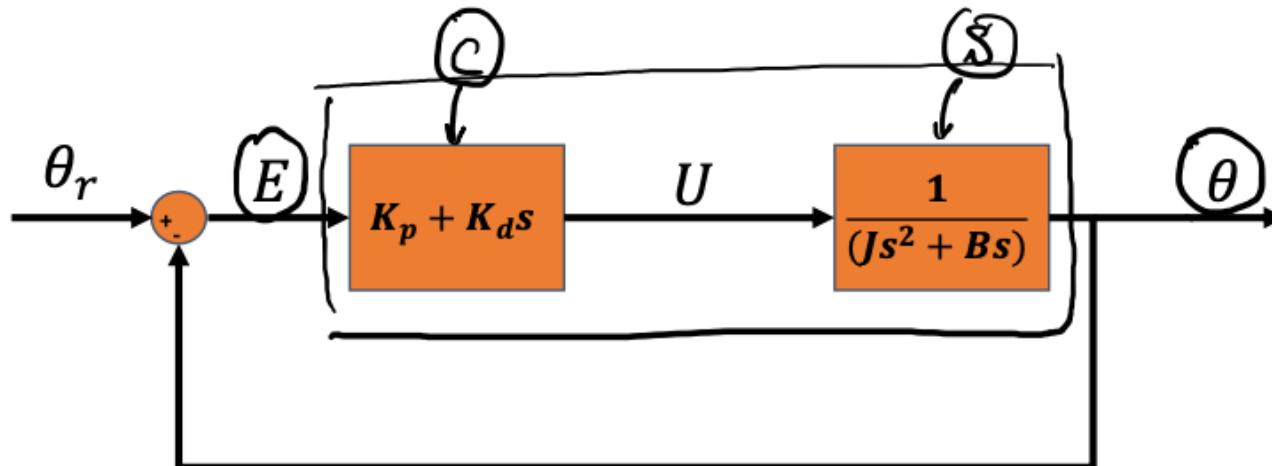
$$\frac{U(s)}{E(s)} = K_p + K_d s$$

Closed-Loop Transfer Function



Closed-Loop Transfer Function

Remember: Serial transforms get multiplied in frequency domain



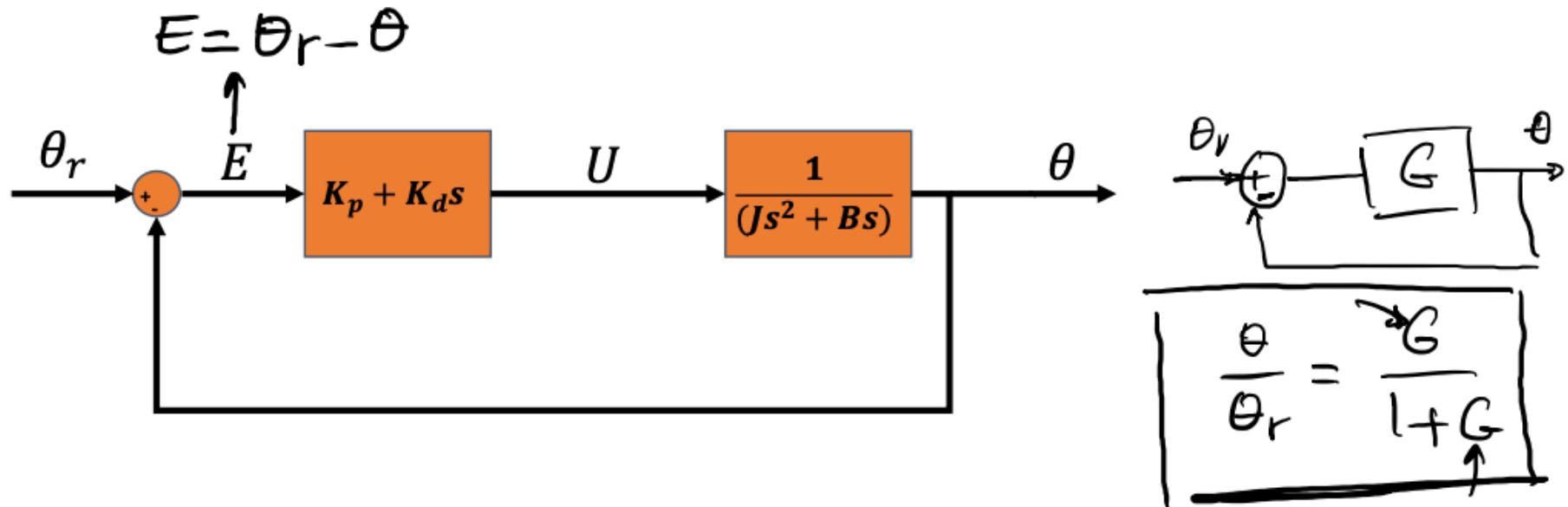
$$E \xrightarrow{C} U ; \frac{U}{E} = C \Rightarrow U = \underline{E} C$$

$$U \xrightarrow{S} \theta \Rightarrow \frac{\theta}{U} = S \Rightarrow \theta = U S \Rightarrow \theta = E C S \Rightarrow \frac{\theta}{E} = C S$$

$$E \xrightarrow{CS} \theta$$

Closed-Loop Transfer Function

Remember: Serial transforms get multiplied in frequency domain



$$E(s) \frac{(K_p + K_d s)}{Js^2 + Bs} = \theta$$

$$\Rightarrow G = \frac{\theta}{E} = \frac{K_p + K_d \cdot s}{Js^2 + Bs} = G$$

Closed-Loop Transfer Function

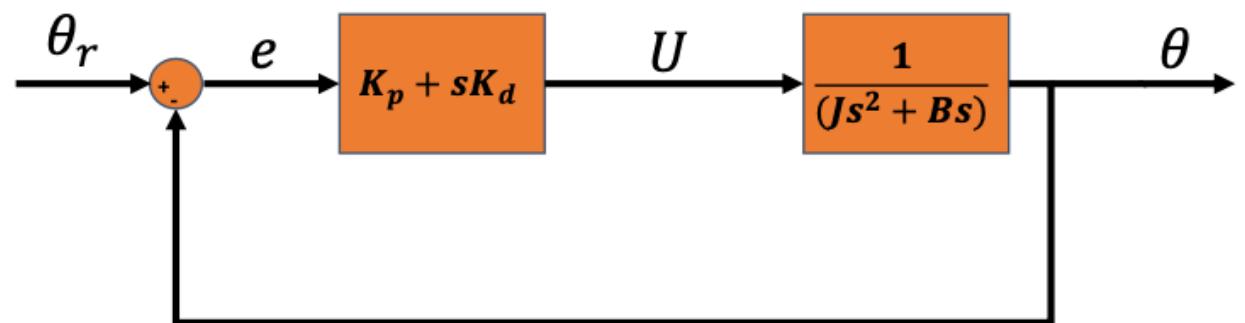
$$E(s) \frac{(K_p + K_d s)}{J s^2 + B s} = \theta(s)$$

$$E(s) = \theta_r - \theta$$

$$\theta_r - \theta = \frac{J s^2 + B s}{(K_p + K_d s)} \theta$$

$$\theta_r = \left(1 + \frac{J s^2 + B s}{(K_p + K_d s)} \right) \theta$$

$$\boxed{\frac{\theta}{\theta_r} = \left(\frac{(K_p + K_d s)}{J s^2 + (B + K_d)s + K_p} \right)}$$



... end of Lecture 13

