## **CENG 102 Project Submission Sheet**

## Plant for Hydrodealkylation of Toluene to Benzene

| Team Name: |  |
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|            |  |

| Student ID # | <b>Project Contribution</b> |
|--------------|-----------------------------|
|              | (General or Specific)       |
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|              | Student ID #                |

If groups have members from both CENG 100 sections, please clarify in the table above which section (professor) you have!

| Problem # |  | Solution   |
|-----------|--|--|
| 1         | Hydrogen Compression: Work & Final Temperature | Work (kW): Temperature (K):  |
| 2         | Hydrogen Non-idealities                        | Residual 1 (J/mol):  Residual 2 (J/mol):  New Work (kW):  Ideal gas? Why or why not? |
| 3         | Toluene Heating (kW)                           | Q =  |
| 4         | Toluene Compression                            | Work (kW): Temperature (K)   |
| 5         | Toluene Vapor Non-Ideality                     | Residual 1 (J/mol):  Residual 2 (J/mol):  New Work (kW):  Ideal gas? Why or why not? |
| 6         | Mixing Temperature (K)                         | T =  |
| 7         | Pre-Reactor Compression                        | Work (kW): Temperature (K)   |
| 8         | Pre-Reactor Heating (kW)                       | Q =  |

| 9  | Reactor Heat (kW)   | Q =   |
|----|---|---|
| 10 | Adiabatic Temperature   | T =   |
| 11 | Influence on Equilibrium  | a.) K <sub>1</sub> =                            |
| 12 | Pre-Separation Pressure Reduction   | a.) T (K) =<br>b.) W (kW) =<br>T (K) =          |
| 13 | Flash I  (1) = Toluene; (2) = Hydrogen  (3) = Benzene; (4) = Methane;  (5) = Biphenyl | V (mol/s) =<br>L (mol/s) =<br>$x_1 = $ $y_1 = $ |

|    | R = recovery fraction  | x <sub>2</sub> = y <sub>2</sub> =   |
|----|--|---|
|    |  | x <sub>3</sub> = y <sub>3</sub> =   |
|    |  | x <sub>4</sub> = y <sub>4</sub> =   |
|    |  | x <sub>5</sub> = y <sub>5</sub> =   |
|    |  | $R_{2,V} = \underline{\qquad} \qquad R_{4,V} = \underline{\qquad}$  |
|    |  | $R_{1,L} = \underline{\qquad} R_{3,L} = \underline{\qquad}$   |
|    |  | $R_{5,L} = \phantom{aaaaaaaaaaaaaaaaaaaaaaaaaaaaaaaaaaa$  |
| 14 | Flash II  (1) = Toluene; (2) = Hydrogen  (3) = Benzene; (4) = Methane;  (5) = Biphenyl | $V 	ext{ (mol/s)} = $ $L 	ext{ (mol/s)} = $ $x_1 = $ $y_1 = $ $x_2 = $ $y_2 = $ $x_3 = $ $y_3 = $ $x_4 = $ $y_4 = $ $x_5 = $ $y_5 = $ Benzene Purge (mol/s) =  Value of Flash II: |

| 15 | Flash III (Ideal) (1) = Toluene; (2) = Biphenyl     | a.) $x_{1} = \underline{\qquad} y_{1} = \underline{\qquad}$ $x_{2} = \underline{\qquad} y_{2} = \underline{\qquad}$ b.) $V \text{ (mol/s)} = \underline{\qquad}$ $L \text{ (mol/s)} = \underline{\qquad}$ c.) $P \text{ (bar)} = \underline{\qquad} y_{1} = \underline{\qquad}$ $V \text{ (mol/s)} = \underline{\qquad}$ $L \text{ (mol/s)} = \underline{\qquad}$ |
|----|---|---|
| 16 | Flash III (Non-Ideal) (1) = Toluene; (2) = Biphenyl | a.) $x_{1} = \underline{\qquad} y_{1} = \underline{\qquad}$ $x_{2} = \underline{\qquad} y_{2} = \underline{\qquad}$ b.) $V \text{ (mol/s)} = \underline{\qquad}$ $L \text{ (mol/s)} = \underline{\qquad}$   |
| 17 | Final Question: Value of Flash III                  |   |

|  | $W_1 = \underline{\qquad} W_2 = \underline{\qquad}$   |
|--|---|
|  |   |
|  | $W_3 = $ $W_4 = $   |
| Extra Credit I: Compression with Inter-Stage Cooling | b.) All in K  |
|  | $T_{F1} = \underline{\hspace{1cm}} T_{F2} = \underline{\hspace{1cm}}$                                       |
|  | $T_{F3} = \underline{\hspace{1cm}} T_{F4} = \underline{\hspace{1cm}}$                                       |
|  | c.) All in kW   |
|  | $Q_1 = $ $Q_2 = $   |
|  | $Q_3 = $  |
| Extra Credit II:  Mixing Temperature with  Residuals | T (K) =   |
| Extra Credit III:<br>Non-Ideal Flash Pressure        | P (bar) = y <sub>1</sub> =<br>V (mol/s) =<br>L (mol/s) =  |
|  | Compression with Inter-Stage Cooling  Extra Credit II: Mixing Temperature with Residuals  Extra Credit III: |