Multiphase KKS model in Moose

Johan Hektor

December 5, 2017

1 Introduction

This document contain notes on the implementation of the phase field model presented in [1] in Moose. The following special notation of volume and surface integrals will be used, in accordance with the official Moose documentation;

$$\int a \cdot b \, dV = (a, b), \qquad \int a \cdot b \, dS = \langle a, b \rangle \tag{1}$$

The sets of phase field variables and phase compositions are denoted η and x, respectively. The global concentration field is denoted c and h denotes the switching functions. The phase fields, phase compositions and the global concentration are all dimensionless fields in the range [0,1].

2 Model

2.1 Free energy

The free energy is given by

$$F = f^{ch}(\boldsymbol{\eta}, \boldsymbol{x}) + f^{int}(\boldsymbol{\eta}) + f^{d}(\boldsymbol{\eta}, \dots), \tag{2} \quad \{\{eq:F\}\}\}$$

with f^{ch} and f^{int} representing the chemical and interface energies respectively. f^d represents the contribution from any other physics included in the model e.g. deformation, temperature, electric field etc.

Here we take

$$f^{ch} = \sum_{i} h_i(\boldsymbol{\eta}) f_i(x_i, \boldsymbol{\eta}), \tag{3} \quad \{\{eq:fch\}\}\}$$

with $f_i(x_i, \eta) = \frac{G_i(x_i)}{V^m}$ where G_i is a representation of the Gibbs energy of phase i and V^m denotes the molar volume which is assumed to be constant.

The interface energy is taken as

$$f^{int} = m \left(\sum_{i} \left(\frac{\eta_{i}^{4}}{4} - \frac{\eta_{i}^{2}}{2} \right) + \sum_{i} \sum_{j \neq i} \frac{\beta}{2} \eta_{i}^{2} \eta_{j}^{2} + \frac{1}{4} \right) + \frac{\alpha}{2} \sum_{i} \left(\nabla \eta_{i} \right)^{2}, \quad (4) \quad \{\{\text{eq:fint}\}\}\}$$

with m, α and β being parameters.

2.2 Governing equations

2.2.1 KKS conditions

KKS models require the chemical potential to be equal in all coexisting phases, i.e.

$$\frac{\partial F}{\partial c} = \frac{\partial f_1}{\partial x_1} + \frac{\partial f_1^d}{\partial x_1} = \dots = \frac{\partial f_n}{\partial x_n} + \frac{\partial f_n^d}{\partial x_n} = \mu_1 \dots = \mu_n. \tag{5}$$

Furthermore, mass conservation is fulfilled by

$$c = \sum_{i} h_i x_i. \tag{6} \quad \{\{\texttt{eq:mass}\}\}$$

2.2.2 Cahn-Hilliard equation

The evolution of the concentration field follows the Cahn-Hilliard equation

$$\frac{\partial c}{\partial t} = \boldsymbol{\nabla} \cdot M(\boldsymbol{\eta}, c) \boldsymbol{\nabla} \frac{\delta F}{\delta c} = \boldsymbol{\nabla} \cdot M(\boldsymbol{\eta}, c) \boldsymbol{\nabla} \left(\frac{\partial F}{\partial c} - \boldsymbol{\nabla} \cdot \frac{\partial F}{\partial \boldsymbol{\nabla} c} \right), \quad (7) \quad \{\{\text{eq:CH1}\}\}\}$$

where M is the mobility. Since there is no dependence on ∇c in the free energy the divergence term of Eq. (7) vanishes.¹

Using Eq. (2), Eq. (3) and Eq. (4) the derivative become

$$\frac{\partial F}{\partial c} = \frac{\partial f^{ch}}{\partial c} + \frac{\partial f^d}{\partial c} = \sum_i h_i \frac{\partial f_i}{\partial x_i} \frac{\partial x_i}{\partial c} + \frac{\partial h_i}{\partial c} f_i + \frac{\partial f^d}{\partial c}. \tag{8} \quad \{\{eq:dFdc1\}\}\}$$

By taking the derivative of the mass conservation Eq. (6) we get

$$\frac{\partial c}{\partial c} = \sum_{i} h_i \frac{\partial x_i}{\partial c} = 1. \tag{9}$$

Inserting into Eq. (8) and taking into account Eq. (5) we end up with

$$\frac{\partial F}{\partial c} = \mu,\tag{10}$$

where we can arbitrarily choose $\mu = \mu_i$ based on the KKS condition. With this Eq. (7) can be written as

 $\frac{\partial c}{\partial t} = \boldsymbol{\nabla} \cdot M(\boldsymbol{\eta}, c) \boldsymbol{\nabla} \mu_i \tag{11}$

The mobility M is taken as

$$M = \sum_{i} h_i \frac{D_i}{\frac{\mathrm{d}^2 f_i}{\mathrm{d}x^2}}.$$
 (12)

The units of Eq. (11) are

$$\frac{1}{s} = \frac{1}{m} \frac{\frac{m^2}{s}}{\frac{J}{m^3}} \frac{1}{m} \frac{J}{m^3} = \frac{1}{s}.$$
 (13)

2.2.3 Allen-Cahn equation

The evolution of each order parameter field follow the Allen-Cahn equation

$$\begin{split} \frac{\partial \eta_{i}}{\partial t} &= -L(\boldsymbol{\eta}) \frac{\delta F}{\delta \eta_{i}} + \xi(\boldsymbol{x}, t) = -L \left(\frac{\partial F}{\partial \eta_{i}} - \boldsymbol{\nabla} \cdot \frac{\partial F}{\partial \boldsymbol{\nabla} \eta_{i}} \right) \\ &= -L \left(\frac{\partial f^{ch}}{\partial \eta_{i}} + \frac{\partial f^{int}}{\partial \eta_{i}} + \frac{\partial f^{d}}{\partial \eta_{i}} - \boldsymbol{\nabla} \cdot \frac{\partial f^{int}}{\partial \boldsymbol{\nabla} \eta_{i}} - \boldsymbol{\nabla} \cdot \frac{\partial f^{d}}{\partial \boldsymbol{\nabla} \eta_{i}} \right). \end{split} \tag{14}$$

The derivatives of the interface energy are easy to calculate from Eq. (4)

$$\frac{\partial f^{int}}{\partial \eta_i} - \nabla \frac{\partial f^{int}}{\partial \nabla \eta_i} = m \left(\eta_i^3 - \eta_i + 2\beta \eta_i \sum_{j \neq i} \eta_j^2 \right) - \nabla \cdot \alpha \nabla \eta_i.$$
 (15)

The derivative of the chemical energy is

$$\frac{\partial f^{ch}}{\partial \eta_i} = \sum_{i} \left(\frac{\partial h_j}{\partial \eta_i} f_j + h_j \frac{\partial f_j}{\partial \eta_i} \right), \tag{16} \quad \{\{eq:dfchdeta\}\}\}$$

where

$$h_j \frac{\partial f_j}{\partial \eta_i} = h_j \underbrace{\frac{\partial f_j}{\partial G_j} \frac{\partial G_j}{\partial x_j}}_{\mu_i} \frac{\partial x_j}{\partial h_j} \frac{\partial h_j}{\partial \eta_i} = \mu_j h_j \frac{\partial x_j}{\partial h_j} \frac{\partial h_j}{\partial \eta_i}. \tag{17}$$

Using that $\frac{\partial c}{\partial \eta_i} = 0$, equation Eq. (6) then gives

This is only true for KKS models, in other multiphase models a term like $\kappa (\nabla c)^2$ is included. This term will make the Cahn-Hilliard a fourth order PDE.

$$\frac{\partial c}{\partial \eta_i} = \sum_j \left(\frac{\partial h_j}{\partial \eta_i} x_j + h_j \frac{\partial x_j}{\partial h_j} \frac{\partial h_j}{\partial \eta_i} \right) = \sum_j \frac{\partial h_j}{\partial \eta_i} \left(x_j + h_j \frac{\partial x_j}{\partial h_j} \right) = 0$$

$$\iff \sum_j h_j \frac{\partial x_j}{\partial h_j} \frac{\partial h_j}{\partial \eta_i} = -\sum_j \frac{\partial h_j}{\partial \eta_i} x_j.$$
(18)

By making use of the KKS condition Eq. (16) can then be written

$$\frac{\partial f^{ch}}{\partial \eta_i} = \sum_j \frac{\partial h_j}{\partial \eta_i} \left(f_j - \mu_j x_j \right) \tag{19}$$

Equation Eq. (14) now becomes

 $\left(egin{array}{c} ext{will} \ ext{change} \ ext{with} \ f^d \end{array}
ight)$

$$\frac{\partial \eta_i}{\partial t} = -L \left(\sum_j \frac{\partial h_j}{\partial \eta_i} \left(f_j - \mu_j x_j \right) \right)$$

$$+m\left(\eta_i^3-\eta_i+2\beta\eta_i\sum_{j\neq i}\eta_j^2
ight)-oldsymbol{
abla}\cdotlphaoldsymbol{
abla}\eta_i+rac{\partial f^d}{\partial\eta_i}-oldsymbol{
abla}\cdotrac{\partial f^d}{\partialoldsymbol{
abla}\eta_i}
ight). \quad (20) \quad ext{\{eq:AC\}}$$

The mobility L is taken as

$$L(\boldsymbol{\eta}) = \frac{\sum_{i} \sum_{j \neq i} L_{ij} \eta_i^2 \eta_j^2}{\sum_{i} \sum_{j \neq i} \eta_i^2 \eta_j^2}.$$
 (21)

 L_{ij} is taken as

$$L_{ij} = \frac{2m}{3\alpha \left(x_i^{eq} - x_i^{eq}\right)^2} \frac{M_i + M_j}{2},$$
 (22) {{eq:lab}}

where $M_i = \frac{D_i}{\frac{\mathrm{d}^2 f_i}{\mathrm{d} x_i^2}}$ and $M_j = \frac{D_j}{\frac{\mathrm{d}^2 f_j}{\mathrm{d} x_j^2}}$ are the mobilities and x_i^{eq} and x_j^{eq} are the

equilibrium molar fractions of phases i and j respectively.

The units of Eq. (20) are

$$\frac{1}{s} = \frac{\frac{J}{m^3}}{\frac{J}{m}} \frac{\frac{m^2}{s}}{\frac{J}{m^3}} \frac{J}{m^3} = \frac{1}{s}.$$
 (23)

2.3 Non-constant molar volume

I'm not sure it is possible to easily remove the assumption of constant molar volume. It is certainly not as easy as I thought before. For non-constant molar volume Eq. (6) becomes $c = \sum_i h_i \frac{x_i}{V_i^m}$ which converts c to units of

mol m⁻³. The problem is that the free energy is formulated in units of J m⁻³, which means that $\frac{\partial F}{\partial c}$ get the units J mol⁻¹. I don't think this is good neither for the KKS conditions nor for the Cahn-Hilliard equation. Perhaps we can formulate the Eq. (11) as

$$\frac{1}{V^m} \frac{\partial c}{\partial t} = \boldsymbol{\nabla} \cdot M(\boldsymbol{\eta}, c) \boldsymbol{\nabla} \mu_i \tag{24}$$

together with the mass balance in Eq. (6) and still have c dimensionless. Then the question is how to choose V^m ?

Another way is maybe to formulate the energies in J mol⁻¹ but then I guess the mesh will represent a certain number of moles instead of a certain volume?

2.4 Weak form residual equations

The weak form of the residual equation for η_i is constructed from Eq. (14) by multiplication with a test function ψ and integrating over the domain:

$$\mathbf{R}_{\eta_{i}} = \left(\frac{\partial \eta_{i}}{\partial t}, \psi\right) + \left(L\left(\frac{\partial f^{ch}}{\partial \eta_{i}} + \frac{\partial f^{int}}{\partial \eta_{i}} + \frac{\partial f^{d}}{\partial \eta_{i}}\right), \psi\right) - (L\nabla \cdot \alpha \nabla \eta_{i}, \psi)$$

$$= \left(\frac{\partial \eta_{i}}{\partial t}, \psi\right) + \left(L\left(\frac{\partial f^{ch}}{\partial \eta_{i}} + \frac{\partial f^{int}}{\partial \eta_{i}} + \frac{\partial f^{d}}{\partial \eta_{i}}\right), \psi\right) + (\alpha \nabla \eta_{i}, \nabla L\psi)$$

$$- \langle (\alpha \nabla \eta_{i}) \cdot \mathbf{n}, L\psi \rangle, \tag{25}$$

with the divergence theorem used on the last term. Inserting the derivatives calculated above gives

$$\mathbf{R}_{\eta_{i}} = \left(\frac{\partial \eta_{i}}{\partial t}, \psi\right) + \left(L \sum_{j} \frac{\partial h_{j}}{\partial \eta_{i}} f_{j}, \psi\right) - \left(L \frac{\partial h_{j}}{\partial \eta_{i}} \mu_{j} x_{j}, \psi\right)
+ \left(L m \left(\eta_{i}^{3} - \eta_{i} + 2\beta \eta_{i} \sum_{j \neq i} \eta_{j}^{2}\right), \psi\right)
+ \left(L \frac{\partial f^{d}}{\partial \eta_{i}}, \psi\right) + (\alpha \nabla \eta_{i}, \nabla L \psi) - \langle(\alpha \nabla \eta_{i}) \cdot \boldsymbol{n}, L \psi\rangle$$
(26)

 $\frac{\partial f^d}{\partial \boldsymbol{\nabla} \eta_i}$

miss-

The Cahn-Hilliard equation Eq. (11) can be solved in two ways. Either you can solve it directly using the residual

$$\mathbf{R}_{c} = \left(\frac{\partial c}{\partial t}, \psi\right) - (\mathbf{\nabla} \cdot M \mathbf{\nabla} \mu, \psi) = \left(\frac{\partial c}{\partial t}, \psi\right) + (M \mathbf{\nabla} \mu, \mathbf{\nabla} \psi) - \langle M \mathbf{\nabla} \mu \cdot \mathbf{n}, \psi \rangle. \quad (27)$$

This seems to be fairly straight forward, but for some reason it is "not fully implemented" in Moose. Instead, the equation is split into two and solved for the concentration c as well as for the chemical potential μ . The residuals for this are

$$\mathbf{R}_{\mu} = \left(\frac{\partial c}{\partial t}, \psi\right) + (M\nabla \mu, \nabla \psi) - \langle M\nabla \mu \cdot \mathbf{n}, \psi \rangle \tag{28}$$

$$\mathbf{R}_c = \left(\frac{\partial F}{\partial c} - \mu, \psi\right). \tag{29}$$

3 Implementation

This section describes the input file used to run the simulation. Moose input files consists of different blocks which together defines the model. All necessary blocks are described below.

3.1 Mesh

The mesh block can be used to create meshes of simple geometries. It can also be used to read the mesh from a file. A rectangular 2D mesh is created like this:

```
[Mesh]
  type = GeneratedMesh
  dim = 2
  nx = 100
  ny = 10
  xmax = 0.304 # Length
  ymax = 0.0257 # Height
[]
```

3.2 Variables

The Variables block declares the variables of the model. A variables is defined like this:

```
[Variables]
# concentration Sn
[./c] # Variable name
    order = FIRST
    family = LAGRANGE
[../]
```

To solve the model the following variables are needed: c,μ,x_i,η_i , i.e. a simulation with three grains of different phases contains 8 variables.

3.3 ICs and BCs

Initial conditions can be set in the ICs block. For simple initial conditions the type FunctionIC can be used. The following code will initiate the variable η_{imc} as a ring with radius 8 centered at (20, 20).

```
[ICs]
    [./eta2] #Cu6Sn5
        variable = eta_imc
        type = FunctionIC
        function = 'r:=sqrt((x-20)^2+(y-20)^2);if(r>8&r<=16,1,0)'
        [../]
[]</pre>
```

There are some more complicated initial conditions already implemented but probably I'll have to make something myself.

Boundary conditions are set in the BCs block using a very similar syntax as the ICs.

3.4 Kernels

In Moose each part of the residual equations are implemented in separate kernels. Each kernel is responsible for evaluating the residual and (optionally) calculate the Jacobian. For each of the Allen-Cahn equations the kernels in Table 1 is needed. For the Cahn-Hilliard equation and the KKS conditions the kernels in Table 2 are needed.

3.5 Materials

The free energies and the switching functions are defined in the Materials block of the input file. The chemical free energy of each phase can be described using the type DerivativeParsedMaterial. This type uses automatic differentiation to calculate the derivatives.

²This kernel includes a double well that can be use to constrain the order parameters to [0,1], turn off the double well by setting w=0.

Table 1: Kernels needed for the Allen-Cahn equation

{tab:AC}

Residual term	Parameters	Kernel name
$ \begin{pmatrix} \frac{\partial \eta_i}{\partial t}, \psi \\ L \sum_j \frac{\partial h_j}{\partial \eta_i} f_j + w \frac{\partial g}{\partial \eta_i}, \psi \end{pmatrix} $	L, w = 0	TimeDerivative KKSMultiACBulkF ²
$-\left(Lrac{\partial h_j}{\partial n_i}\mu_j x_j,\psi ight)$	$L^{'}$	KKSMultiACBulkC
$ \begin{pmatrix} L \frac{\partial f^d}{\partial \eta_i}, \psi \\ L m \left(\eta_i^3 - \eta_i + 2\beta \eta_i \sum_{j \neq i} \eta_j^2 \right), \psi \end{pmatrix} $		
$\left(Lm\left(\eta_i^3 - \eta_i + 2\beta\eta_i \sum_{j\neq i} \eta_j^2\right), \psi\right)$	m, eta	ACGrGrMulti
$(\alpha \nabla \eta_i, \nabla L \psi)$	L, α	ACInterface

Table 2: Kernels needed for the split version of the Cahn-Hilliard equation and the KKS conditions

{tab:CH}

Residual term	Parameters	Kernel name	
$ \begin{array}{l} \left(\frac{\partial c}{\partial t}, \psi\right) \\ \left(M \boldsymbol{\nabla} \mu, \boldsymbol{\nabla} \psi\right) \\ \left(\frac{\partial F}{\partial c} - \mu, \psi\right) \end{array} $	M	CoupledTimeDerivative SplitCHWRes KKSSplitCHCRes	
$\mu = \mu_i = \mu_j$ $c = \sum_i h_i x_i$		KKSPhaseChemicalPotential KKSMultiPhaseConcentration	

The same switching function can be used to describe all grain of the same phase (I think).

The materials block can also be used to define constants. For example

```
[./constants]
    type = GenericConstantMaterial
    prop_names = 'L kappa gamma mu tgrad_corr_mult'
    prop_values = '1. 0.5 0.5 1. 0.'
[../]
```

3.6 Executioner, Preconditioning and Outputs

The parameters of the solver are set in the Executioner, Preconditioning and Outputs blocks, here you can also set options for the behavior of the underlying PETSc commands. The blocks can look something like this

```
[Executioner]
  type = Transient
  solve_type = 'PJFNK'
  petsc_options_iname = '-pc_type -sub_pc_type -sub_pc_factor_shift_type'
  petsc_options_value = 'asm ilu nonzero'
  l_max_its = 30
  nl_max_its = 10
  l_tol = 1.0e-4
  nl_rel_tol = 1.0e-10
```

```
nl_abs_tol = 1.0e-11
 num_steps = 100
 dt = 0.5
[Preconditioning]
  active = 'full'
  [./full]
    type = SMP
    full = true
  [../]
  [./mydebug]
    type = FDP
    full = true
  [../]
[Outputs]
  exodus = true
```

These settings will solve the equations using the Pre-Conditioned Jacobian-Free Newton-Krylow method which is the standard way in Moose. The results will be written to a file that can be viewed in e.g. Peacock or Paraview.

References

[1] Johan Hektor, Matti Ristinmaa, Håkan Hallberg, Stephen A Hall, and Srinivasan Iyengar. Coupled diffusion-deformation multiphase field model for elastoplastic materials applied to the growth of Cu6Sn5. *Acta Materialia*, 108:98–109, 2016.