



# ***User Guide for QC-EMMS Drag Model Program***

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## 1. Brief Introduction

QC-EMMS is a gas-solid drag model that considers the remarkable effects of particle clusters during the heterogeneous flow in CFB (Circulating Fluidized Bed). It was developed based on the Energy Minimization in Multi-Scale (EMMS) theory<sup>[1]</sup>. The QC-EMMS model has shown good accuracy in CFB simulations under a wide range of flow conditions<sup>[2-5]</sup>.

To further extend the model, we uploaded this program to the open-source platform Github. Welcome worldwide scholars to download and use it !

Link: <https://github.com/CFACTsinghua/QC-EMMS>

The input parameters are limited to certain ranges in this **trial version**. Welcome to contact us for using the full version and getting more supports!

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### **References**

- [1] J. Li, M. Kwauk, Particle-Fluid Two-Phase Flow, the Energy Minimization Multi-Scale Method, Metallurgical Industry Press, Beijing (1994), ISBN 7-5024-1572-6
- [2] C. Chen, Investigation on Mesoscale Structure in Gas-Solid Fluidization and Heterogeneous Drag Model, Springer Press, (2016), ISBN 978-3-662-49371-8
- [3] C. Chen, Q. Dai, H. Qi, Improvement of EMMS drag model for heterogeneous gas-solid flows based on cluster modeling, Chem. Eng. Sci. 141 (2016) pp. 8-16.
- [4] Q. Dai, C. Chen, H. Qi, A generalized drag law for heterogeneous gas-solid flows in fluidized beds, Powder Technol. 283 (2015) pp. 120-127.
- [5] Q. Dai, Meso-scale Analysis and Improvement of Fluidized Heterogeneous Drag Model Based on EMMS Theory, Doctoral thesis, Tsinghua University (2017)

## 2. Calculation of Drag Correction Factor, $H_d$

(1) Open “ QC-EMMS Drag Model (Trial Version).exe ”.

(2) 8 parameters with limited ranges need inputting into the program:

- Gas viscosity,  $\mu_g$  (Pa·s)
- Gas density,  $\rho_g$  (kg/m<sup>3</sup>)
- Particle density,  $\rho_p$  (kg/m<sup>3</sup>)
- Particle diameter,  $d_p$  (μm)
- Minimal fluidization solid volume fraction,  $\varepsilon_{s,mf}$  (-)
- Superficial gas velocity,  $U_g$  (m/s)
- Solid mass circulation rate,  $G_s$  (kg/m<sup>2</sup>s)
- Bed-averaged solid volume fraction,  $\varepsilon_{s,bed}$  (-)

```
*****
*               QC-EMMS Drag Model               *
*               Trial Version Program              *
*   Professor QI Haiying's Lab, Tsinghua University, China   *
*****

Input parameters are limited to certain ranges in this trial version.
Welcome to contact us for using full version!
Please refer to User Guide for contact information.

Parameter input:
Gas viscosity,  $\mu_g$  (1.75e-5 ~ 1.85e-5 Pa·s)
1.8e-5
Gas density,  $\rho_g$  (1.2 ~ 1.3 kg/m3)
1.2
Particle density,  $\rho_p$  (2400 ~ 2600 kg/m3)
2500
Particle diameter,  $d_p$  (280 ~ 320 μm)
300
Minimal fluidization solid volume fraction,  $\varepsilon_{s,mf}$  (0.5 ~ 0.6)
0.5
Superficial gas velocity,  $U_g$  (7 ~ 8 m/s)
7.5
Solid mass circulation rate,  $G_s$  (130 ~ 170 kg/m2s)
150
Bed-averaged solid volume fraction,  $\varepsilon_{s,bed}$  (0.07 ~ 0.08)
0.07
```

Press “Enter” button to input the next parameter. If some parameters are out of range, please try again.

(3) After inputting parameters, it takes 1-2 hours to complete the calculation.

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Solid mass circulation rate,  $G_s$  (100 ~ 150 kg/m2s)
150
Bed-averaged solid volume fraction,  $\varepsilon_{s,bed}$  (0.07 ~ 0.08)
0.07

Properties of gas and particles:
  Gas viscosity,  $\mu_g=1.8e-005$  (Pa · s)
  Gas density,  $\rho_g=1.2$  (kg/m3)
  Particle density,  $\rho_p=2500$  (kg/m3)
  Particle diameter,  $d_p=300$  ( $\mu m$ )
  Minimal fluidization solid volume fraction,  $\varepsilon_{s,mf}=0.5$  (-)

CFB operating parameters:
  Superficial gas velocity,  $U_g=7.5$  (m/s)
  Solid mass circulation rate,  $G_s=150$  (kg/m2s)
  Bed-averaged solid volume fraction,  $\varepsilon_{s,bed}=0.07$  (-)

Program is running..... (Need 1~2 hours)

```

A “*Hd.dat*” data file containing 3 columns and 201201 rows can be created in the same folder with the program:

- First data column: Superficial gas-solid slip velocity,  $U_{slip}$  (m/s)
- Second: Local gas volume fraction,  $\varepsilon_g$  (-)
- Third: Drag correction factor,  $H_d$  (-)

Hd.dat	2021/4/21
QC-EMMS Drag Model (Trial Version...)	2021/4/21

  

79	0.001	0.694005	1
80	0.001	0.697381	1
81	0.001	0.69988	1
82	0.001	0.702378	0.870066
83	0.001	0.704877	0.722516
84	0.001	0.707375	0.598734
85	0.001	0.709874	0.496232
86	0.001	0.712372	0.412153
87	0.001	0.714871	0.343608
88	0.001	0.717369	0.287906
89	0.001	0.719868	0.242671
90	0.001	0.722366	0.205883
91	0.001	0.724865	0.175871
92	0.001	0.727363	0.151277
93	0.001	0.729862	0.121017

The drag correction factor,  $H_d$ , is the ratio of the drag function,  $\beta$ , calculated by QC-EMMS model to the  $\beta$  from Wen-Yu model:

$$H_d = \frac{\beta_{QC-EMMS}}{\beta_{WY}} \quad (1)$$

$$\beta_{WY} = \frac{3}{4} C_{D0} \frac{\varepsilon_s \varepsilon_g \rho_g |\vec{u}_g - \vec{u}_s|}{d_p} \varepsilon_g^{-2.65}, \quad C_{D0} = \begin{cases} \frac{24(1 + 0.15 \text{Re}^{0.687})}{\text{Re}}, & \text{Re} < 1000 \\ 0.44, & \text{Re} \geq 1000 \end{cases} \quad (2)$$

### 3. Coupling of QC-EMMS with CFD Platform

Here we provide the coupling method of QC-EMMS model with Fluent®.

(1) Put “*Hd.dat*” and the User Defined Function code “*drag\_qc\_emms.c*” into the same folder with the Fluent® case.

(2) Compile and load the “*drag\_qc\_emms.c*”: Define → User-Defined → Functions → Compiled → Add “*drag\_qc\_emms.c*” → Build → Load

(3) Drag modification: Phase Interaction → Drag → Wen-Yu → Select “Drag Modification” → Set “Drag Factor” to user-defined → qc\_emms\_drag

(4) Set a User Defined Memory: Define → User-Defined → Memory → Set “Number of User-Defined Memory Locations” to 1.