Documentation on modelEqn

Numerical approach for a temperature distribution

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1 1D spherical equations

1.1 Basic approach and scope

- Calculate a target property field as a function of time and physical space in a spherical particle
- Discretization for various boundary conditions

1.2 Overview of the Problem

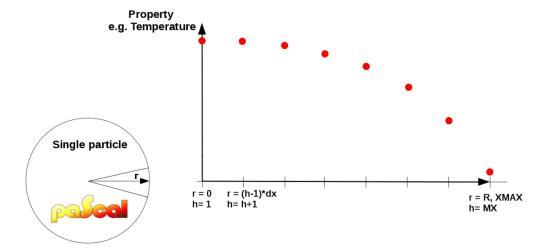


Figure 1: Overview

- Half of particle is discretized starting at r = 0, h = 1
- Every point coordinate until h=MX (MX= number of grid points to be set in input script using e.g. particle_mesh nGridPoints 20) can be obtained using $r=(h-1)\cdot \triangle r$ with $\triangle r=\frac{XMAX}{MX-1}$ with XMAX to be set in input script using e.g. xmax 1.e-3
- Value of target properties (e.g. temperature) obtained from discretization in physical space and integrating governing equations over time

1.3 Numerical approach and governing equations

- Fourier differential equation in spherical coordinates with $\lambda_{eff} = const.$ and no inner heat sources
- Eqn. (2) to Eqn. (3): transport of thermal energy in nothing but radial direction

$$\rho c_p \frac{\partial T}{\partial t} = div(\lambda_{eff} \operatorname{grad} T) + \dot{q}$$
 (1)

$$\rho c_p \frac{\partial T}{\partial t} = \frac{1}{r^2} \frac{\partial}{\partial r} \left(\lambda_{eff} r^2 \frac{\partial T}{\partial r} \right) + \frac{1}{r^2 \sin^2 \varphi} \frac{\partial}{\partial \psi} \left(\lambda_{eff} \frac{\partial T}{\partial \psi} \right) + \frac{1}{r^2 \sin^2 \varphi} \frac{\partial}{\partial \varphi} \left(\lambda_{eff} \frac{\partial T}{\partial \varphi} \right) + \dot{q}$$
(2)

$$\rho c_p \frac{\partial T}{\partial t} = \lambda_{eff} \left(\frac{\partial^2 T}{\partial r^2} + \frac{2}{r} \frac{\partial T}{\partial r} \right)$$
 (3)

with thermal diffusivity

$$a = \frac{\lambda_{eff}}{\rho \, c_p} \tag{4}$$

$$\frac{\partial T}{\partial t} = a \cdot \left(\frac{\partial^2 T}{\partial r^2} + \frac{2}{r} \frac{\partial T}{\partial r} \right) \tag{5}$$

1.4 Discretization in physical space

 \bullet CDS - second order scheme

$$\frac{\partial T}{\partial r} = \frac{T_{h+1} - T_{h-1}}{2 \triangle r} + O(\triangle r^2) \tag{6}$$

$$\frac{\partial^2 T}{\partial r^2} = \frac{T_{h+1} + T_{h-1} - 2T_h}{\Delta r^2} + O(\Delta r^2) \tag{7}$$

1.5 **Boundary conditions**

Middle of sphere 1.5.1

- Singularity in spherical coordinates at r = 0, symmetry
- First derivative of temperature after radius divided by radius is replaced by second derivative of temperature after radius (L'hopital)

$$\frac{\partial T}{\partial t} = 3 a \frac{\partial^2 T}{\partial r^2} \tag{8}$$

with:

$$\frac{\partial^2 T}{\partial r^2} = \frac{T_{h+1} + T_{h-1} - 2T_h}{\triangle r^2} + O(\triangle r^2) \tag{9}$$

and T_{0-1} results of auxiliary point method and boundary condition second order at r= $0, h = 1 \text{ with } T_{0-1} = T_{0+1}$

$$\frac{\partial T}{\partial t} = 6 a \frac{T_{0+1} - T_0}{\Delta r^2} \tag{10}$$

Surface of sphere, r = XMAX

1.5.3 **NEUMANN**

• Fixed heat flux

$$\dot{q} = -\lambda_{eff} \frac{\partial T}{\partial r} \tag{11}$$

$$\dot{q} = -\lambda_{eff} \frac{T_{h+1} - T_{h-1}}{2 \triangle r} \tag{12}$$

$$T_{h+1} = T_{h-1} - \frac{2\dot{q} \triangle r}{\lambda_{eff}} \tag{13}$$

$$\frac{\partial^2 T}{\partial r^2} = \frac{T_{h-1} - \frac{2 \dot{q} \triangle r}{\lambda_{eff}} + T_{h-1} - 2Th}{\triangle r^2}$$

$$= \frac{2 \left(T_{h-1} - \frac{\dot{q} \triangle r}{\lambda_{eff}} - T_h \right)}{\triangle r^2}$$
(14)

$$= \frac{2\left(T_{h-1} - \frac{\dot{q} \triangle r}{\lambda_{eff}} - T_h\right)}{\triangle r^2} \tag{15}$$

$$\frac{\partial T}{\partial r} = \frac{T_{h+1} - \frac{2\dot{q} \triangle r}{\lambda_{eff}} - Th - 1}{2 \triangle r} \tag{16}$$

$$= -\frac{2\,\dot{q}\,\triangle\,r}{2\,\triangle\,r\lambda_{eff}}\tag{17}$$

$$= -\frac{\dot{q}}{\lambda_{eff}} \tag{18}$$

$$\frac{\partial T}{\partial t} = \frac{2\left(T_{h-1} - \frac{\dot{q} \triangle r}{\lambda_{eff}} - T_h\right)}{\triangle r^2} - \frac{2\dot{q}}{R\lambda_{eff}} \tag{19}$$

1.5.4 DIRICHLET

• Fixed wall temperature T_w

$$T_h = T_{wall} (20)$$

1.5.5 CONVECTIVE

• Convective heat transfer at the surface of the particle

$$\alpha \cdot (T_h - T_{enviro}) = -\lambda_{eff} \frac{\partial T}{\partial r}$$
 (21)

• Calculation of auxiliary point

$$\alpha \cdot (T_h - T_{enviro}) = -\lambda_{eff} \frac{T_{h+1} - T_{h-1}}{2 \triangle r}$$
(22)

with Biot number

$$Bi = \frac{\alpha \triangle r}{\lambda_{eff}} \tag{23}$$

$$T_{h+1} = -2 Bi (T_h - T_{enviro}) + T_{h-1}$$
 (24)

with T_{h+1} at x = R, XMAX

$$\frac{\partial T}{\partial t} = a \cdot \left(\frac{\partial^2 T}{\partial r^2} + \frac{2}{R} \frac{\partial T}{\partial r} \right) \tag{25}$$

results in

$$\frac{\partial T}{\partial t} = \frac{a}{\Delta r^2} \left(-2 Bi \left(T_h - T_{enviro} \right) + T_{h-1} + T_{h-1} - 2 T_h \right) + \frac{2 a}{2 R \Delta r} \left(-2 Bi \left(T_h - T_{enviro} \right) + T_{h-1} - T_{h-1} \right) \tag{26}$$

$$\frac{\partial T}{\partial t} = \frac{2a}{\Delta r^2} \left(-Bi \left(T_h - T_{enviro} \right) + T_{h-1} - T_h \right) + \frac{a}{R \wedge r} \left(-2Bi \left(T_h - T_{enviro} \right) \right) = f(RHS - RightHandSide)$$
(27)

If a heat flux from LIGGGHTS is pulled trough a coupling model it acts as a thermal source term and is added for the outer grid point which results in

$$\frac{\partial T}{\partial t} = \frac{2a}{\Delta r^2} \left(-Bi \left(T_h - T_{enviro} \right) + T_{h-1} - T_h \right) + \frac{a}{R \Delta r} \left(-2Bi \left(T_h - T_{enviro} \right) \right) + \frac{\dot{q}}{\rho_{eff} c_{p,eff}} = f(\text{RHS - Right Hand Side})$$
(28)

1.6 Jacobian matrix coefficients

- Function returnJac in modeleqn1Dspherical
- Represents the derivation of RHS by every single component (e.g. $T_h, T_{h+1}, ...$)

1.6.1 Middle of sphere

based on Eqn. (10)

$$\frac{\partial f}{\partial T_0} = -\frac{6a}{\Delta r^2} \tag{29}$$

$$\frac{\partial f}{\partial T_{0+1}} = \frac{6 a}{\triangle r^2} \tag{30}$$

1.6.2 Between middle and surface

- Used for 1 < h < MX
- Based on Eqn. (6), (7) and (5)

$$\frac{\partial f}{\partial T_h} = -\frac{2a}{\Delta r^2} \tag{31}$$

$$\frac{\partial f}{\partial T_{h-1}} = \frac{a}{\triangle r} \left(\frac{1}{\triangle r} - \frac{1}{x} \right) \tag{32}$$

$$\frac{\partial f}{\partial T_{h+1}} = \frac{a}{\Delta r} \left(\frac{1}{\Delta r} + \frac{1}{x} \right) \tag{33}$$

1.6.3 Surface of sphere, r = XMAX

1.6.4 DIRICHLET

based on Eqn. (20)

$$\frac{\partial f}{\partial T_h} = 0 \tag{34}$$

1.6.5 NEUMANN

based on Eqn. (19)

$$\frac{\partial f}{\partial T_h} = -\frac{2}{\triangle r^2} \tag{35}$$

$$\frac{\partial f}{\partial T_{h-1}} = \frac{2}{\triangle r^2} \tag{36}$$

1.6.6 CONVECTIVE

based on Eqn. (27)

$$\frac{\partial f}{\partial T_h} = -\frac{2a}{\Delta r} \left(\frac{Bi}{R} + \frac{Bi}{\Delta r} - \frac{1}{\Delta r} \right) \tag{37}$$

$$\frac{\partial f}{\partial T_{h-1}} = \frac{2a}{\Delta r^2} \tag{38}$$

1.7 Calculating of average values

- Need to compute volume averaged particle properties
- Volume shells defined at every location i with r ranging from $0 \le i < MX$

$$\overline{y} = \frac{\sum_{i=0}^{i} \triangle V \, y_i}{\sum_{i=0}^{i} \triangle V} \tag{39}$$

with

$$\Delta V = \frac{\pi}{6} \left(r_a^3 - r_i^3 \right) \tag{40}$$

$$= \frac{\pi dx^3}{6} \left[(i+0.5)^3 - (i-0.5)^3 \right]$$
 (41)

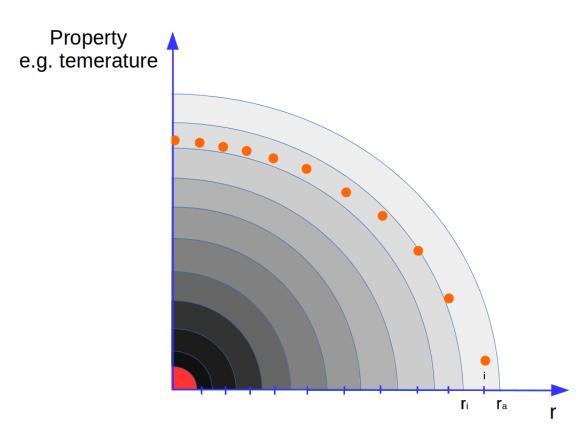


Figure 2: Averaging shells with $r_a = i + 0.5$ and $r_i = i - 0.5$ and $0 \le i < MX$