### **Computational Geosciences**

# Implementation and evaluation of permeability-porosity and tortuosity-porosity relationships linked to mineral dissolution-precipitation --Manuscript Draft--

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Abstract:	Changes of porosity, permeability and tortuosity due to physical and geochemical processes are of vital importance for a variety of hydrogeological systems, including passive treatment facilities for contaminated groundwater, Engineered Barrier Systems (EBS), and host rocks for high-level nuclear waste (HLW) repositories. Due to the nonlinear nature and chemical complexity of the problem, it is impossible to verify reactive transport codes analytically, and code inter-comparisons are the most suitable method to assess code capabilities and model performance. This paper summarizes model inter-comparisons for six hypothetical scenarios with generally increasing geochemical or physical complexity using the reactive transport codes CrunchFlow, HP1, MIN3P, PFlotran, and TOUGHREACT. Benchmark problems include the enhancement of porosity and permeability through mineral dissolution, as well as near complete clogging due to localized mineral precipitation, leading to the reduction of permeability and tortuosity. Processes considered in the benchmark simulations are advective-dispersive transport in saturated media, kinetically controlled mineral dissolution-precipitation, and aqueous complexation. Porosity changes are induced by mineral dissolution-precipitation reactions and the Carman-Kozeny relationship is used to describe changes in permeability as a function of porosity. Archie's law is used to update the tortuosity and the pore diffusion coefficient as a function of porosity. Results demonstrate that, generally, good agreement is reached amongst the computer models despite significant differences in model formulations. Some differences are observed, in particular for the more complex scenarios involving clogging; however,			

these differences do not affect the interpretation of system behavior and evolution.

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#### **Abstract**

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Changes of porosity, permeability and tortuosity due to physical and geochemical processes are of vital importance for a variety of hydrogeological systems, including passive treatment facilities for contaminated groundwater, Engineered Barrier Systems (EBS), and host rocks for high-level nuclear waste (HLW) repositories. Due to the non-linear nature and chemical complexity of the problem, it is impossible to verify reactive transport codes analytically, and code inter-comparisons are the most suitable method to assess code capabilities and model performance. This paper summarizes model inter-comparisons for six hypothetical scenarios with generally increasing geochemical or physical complexity using the reactive transport codes CrunchFlow, HP1, MIN3P, PFlotran, and TOUGHREACT. Benchmark problems include the enhancement of porosity and permeability through mineral dissolution, as well as near complete clogging due to localized mineral precipitation, leading to the reduction of permeability and tortuosity. Processes considered in the benchmark simulations are advective-dispersive transport in saturated media, kinetically controlled mineral dissolution-precipitation, and aqueous complexation. Porosity changes are induced by mineral dissolution-precipitation reactions and the Carman-Kozeny relationship is used to describe changes in permeability as a function of porosity. Archie's law is used to update the tortuosity and the pore diffusion coefficient as a function of porosity. Results demonstrate that, generally, good agreement is reached amongst the computer models despite significant differences in model formulations. Some differences are observed, in particular for the more complex scenarios involving clogging; however, these differences do not affect the interpretation of system behavior and evolution.

**Keywords**: Permeability-porosity relationship, tortuosity-porosity relationship, mineral dissolution-precipitation, benchmark, CrunchFlow, HP1, MIN3P, PFlotran, TOUGHREACT.

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#### 1. Introduction

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The simulation of permeability and tortuosity evolution due to porosity changes is of vital importance for the description of various hydrogeological processes, such as fluid circulation in geothermal systems (Wagner et al. 2005), acid rock drainage (ARD) attenuation and treatment (Annandale et al. 1999), well fouling due to oxide precipitation (Houben 2003), aquifer storage and recovery (ASR) (Rinck-Pfeiffer et al. 2000), and the long-term geochemical evolution of host rock considered for high-level nuclear waste (HLW) repositories (De Windt et al. 2004; Xie et al. 2011; Liu et al. 2014). Porosity changes can be the result of many processes including mechanical deformation, swelling of clay minerals (e.g. montmorillonite), dissolution/precipitation, and thermal deformation. Mineral dissolution and precipitation reactions can also have a significant effect on porous medium porosity and in turn permeability and tortuosity.

Porosity changes in natural porous media occur normally very slowly, but in the long term can be of pivotal importance for the migration of fluids and solutes. If porosity increases are substantial, preferential fluid migration pathways may develop, accelerating solute transport. On the other hand, for significant porosity decreases, nearly complete clogging may occur, substantially inhibiting fluid and solute migration. Clogging in particular is associated with numerical challenges due to the development of very small water-rock ratios, or the complete disappearance of the aqueous phase. It is therefore useful to evaluate the capabilities and performance of reactive transport codes to simulate evolving porosity and permeability, both for conditions of porosity enhancement and reduction. It is also of interest to evaluate the effect of changing tortuosity on pore diffusion, in particular for clogging-dominated problems. Considering the complex nature of reactive transport simulations, code verification through

analytical solutions is often impossible. Code inter-comparison through well-defined benchmarks is in many cases the most suitable method (Carrayrou et al. 2010).

The present paper presents and analyses the results of an inter-comparison involving five reactive transport codes (i.e. CrunchFlow, HP1, MIN3P, PFlotran, and TOUGHREACT) used for the investigation of six hypothetical scenarios to evaluate formulations and implementations for permeability-porosity and tortuosity-porosity relationships. Transport and reaction processes considered include: multicomponent aqueous complexation, kinetic surface-controlled reversible mineral dissolution and precipitation, advective and diffusive mass transport, and coupling of dissolution-precipitation induced porosity change and fluid flow processes. The Carman-Kozeny relationship was used to describe changes in permeability, and the tortuosity and pore diffusion coefficients were updated based on Archie's law, both as a function of porosity.

#### 2. Problem overview

Six benchmark levels with increasing complexity were investigated in this exercise (Table 1) — the first level (B1) considers mineral dissolution and associated permeability enhancement, the second level (B2) focuses on a precipitation-dominated (clogging) problem, and the third level (B3) extends the clogging problem of benchmark B2 by considering a significantly more complex geochemical system (e.g. inclusion of additional chemical components and minerals). Benchmarks B1-B3 have in common that advection is the only transport process considered. The fourth level (B4) is based on benchmark B3, but considers diffusive transport instead of advective transport to compare the codes under purely diffusive mass transfer conditions. The fifth level (B5) combines benchmarks B3 and B4, and includes both diffusive and advective transport. Benchmarks B1-B5 were carried out for one-dimensional flow and transport systems

with initially homogeneous medium properties. Benchmark B6 further extends B5 into a 2D heterogeneous problem with a randomly distributed conductivity field.

Benchmark B1 considers the infiltration of a sulfuric acid solution into a rock matrix containing calcite in an otherwise non-reactive (inert) rock matrix. The only mineral phase considered is calcite; four components are included (H<sup>+</sup>, Ca<sup>2+</sup>, CO<sub>3</sub><sup>2-</sup>, and SO<sub>4</sub><sup>2-</sup>), leading to the formulation of 10 aqueous complexes. Benchmark B2 also considers the infiltration of a sulfuric acid solution into a calcite-containing rock matrix. In addition to the primary mineral phase calcite, gypsum is considered as a secondary phase. The inflow solution contains a much higher SO<sub>4</sub><sup>2-</sup> concentration. Benchmark B3 is based on B2 by adding Fe(II), Fe(III), K, A1, Na, and O<sub>2</sub>(aq), thus increasing the number of aqueous components (10), secondary aqueous species (40) and mineral phases (6). Benchmarks B4 to B6 use the same reaction network as Benchmark B3. For Benchmarks B4 to B6, the chemical composition of the solution at the inflow boundary and the pore water in the domain, and the mineral composition of the domain also remain the same as those in Benchmark B3.

All simulations were conducted under standard pressure and temperature (25°C) and fully saturated conditions. The geochemical database was derived from the database of MINTEQA2 (Allison et al. 1991, see Supporting Information).

This set of benchmarks was solved by five different reactive transport codes, namely: CrunchFlow (Steefel et al. this issue; Steefel 2009), HP1 (Jacques et al. 2008a, b, restricted to B1-B5, because it is a one-dimensional transport code), MIN3P (Mayer et al. 2002; Mayer 2010; Mayer and MacQuarrie 2010), PFlotran (Lichtner et al. 2013), and TOUGHREACT (Xu et al. 2004, 2006, 2011). An overview on the formulations and capabilities of the individual codes is given in Steefel et al. (this issue).

#### 3. Theoretical background

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The generalized governing equations for multicomponent reactive transport are provided in Steefel et al. (this issue) and are therefore not repeated here. This section focuses on the formulations used to describe permeability-porosity and tortuosity-porosity relationships, which are central to this benchmark. In addition, the formulations for mineral dissolution-precipitation reactions and activity corrections are provided, considering that these relationships strongly affect the results of the benchmarks.

#### 3.1. Porosity, permeability, and tortuosity

The porosity change in each grid cell is calculated by summation over the volume fraction (φ)
changes of the minerals that occurred between the new time step (t+Δt) and that at the previous
time step (t). Assuming that porosity changes are occurring slowly, porosity (φ) in each cell is
explicitly updated after completion of each time step:

$$\phi^{t+\Delta t} = \phi^t - \sum_{i=1}^{N_m} (\varphi_i^{t+\Delta t} - \varphi_i^t)$$
 (1)

where  $N_m$  defines the number of the minerals. The hydraulic conductivity K is also updated at the end of each time step according to the Carman-Kozeny relationship (Carrier, 2003):

$$K^{t+\Delta t} = \left[ \frac{(\phi^{t+\Delta t})^3}{[1 - (\phi^{t+\Delta t})]^2} \right] \left[ \frac{(1 - \phi^t)^2}{(\phi^t)^3} \right] K^t$$
 (2)

Archie's law is used to calculate the tortuosity  $\tau$  as a function of porosity at the new time level:

$$\tau^{t+\Delta t} = [\phi^{t+\Delta t}]^{\alpha} \tag{3}$$

with the exponent  $\alpha = 1/3$ , consistent with the formulation by Millington and Quirk (1961). The pore diffusion coefficient at the new time level  $(D_p^{t+\Delta t})$  is calculated as:

$$D_p^{t+\Delta t} = \tau^{t+\Delta t} D_0 \tag{4}$$

- where  $D_0$  is the free phase diffusion coefficient in water (assumed to be identical for all species).
- The effective diffusion coefficient D<sub>e</sub> is calculated as:

$$D_e^{t+\Delta t} = \phi^{t+\Delta t} \tau^{t+\Delta t} D_0 = \phi^{t+\Delta t} D_p^{t+\Delta t}$$
(5)

#### 3.2. Mineral dissolution-precipitation reactions

- 105 Mineral dissolution-precipitation reactions are described as kinetic surface-controlled reactions
- based on the rate expression:

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$$R_i^m = -k_i^m \left[ 1 - \left( \frac{IAP_i^m}{K_i^m} \right) \right] \tag{6}$$

- where  $R_i^m$  is the reaction rate,  $IAP_i^m$  is the ion activity product,  $K_i^m$  is the equilibrium constant
- and  $k_i^m$  is the effective rate constant. The rate constants  $k_i^m$  of primary minerals vary as a
- 109 function of mineral abundance at each time step. For primary mineral phases following a two-
- third power relationship of the form

$$k_i^{m,t} = -k_i^{m,0} \left(\frac{\varphi_i^t}{\varphi_i^0}\right)^{2/3} \tag{7}$$

- 111 is used to update the effective rate constant (Lichtner, 1996). In this relationship,  $k_i^{m,t}$  and  $\varphi_i^t$
- define the effective rate constant and mineral volume fraction at time t, respectively; while  $k_i^{m,0}$
- and  $\varphi_i^0$  define the initial rate constant and mineral volume fraction, respectively. The rate
- 114 coefficients for secondary minerals are assumed to remain constant.

#### 3.3. Activity corrections

- 116 Activity coefficients  $\gamma_i^d$  for all charged dissolved species  $A_i^d$ , where  $A_i^d$  can be either a
- component as species in solution or an aqueous complex, are calculated based on the modified

Debye-<u>Hückel</u> equation if ion-specific parameters are available (Parkurst 1990; Allison et al. 1991):

$$log\gamma_i^d = \frac{-A_d Z_i^2 \sqrt{I}}{1 + B_d a_i \sqrt{I}} + b_i I \tag{8}$$

where I is the ionic strength,  $Z_i$  is the charge of the  $i^{th}$  ion,  $A_d$  and  $B_d$  are constants,  $a_i$  and  $b_i$  are ion-specific parameters. If  $a_i$  is available, but not  $b_i$ , equation (8) is used with  $b_i = 0$ . When  $a_i$  is not provided, the Davies equation is used as an approximation (Allison et al. 1991):

$$log\gamma_i^d = -A_d Z_i^2 \left[ \frac{\sqrt{I}}{1 + \sqrt{I}} - 0.24I \right] \tag{9}$$

Activity correction for neutral species excluding water is calculated as described by Allison et al.

124 (1991):

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$$log \gamma_i^d = 0.1I \tag{10}$$

125 The activity correction for water is defined by (Allison et al. 1991):

$$\gamma_{H_2O} = 1 - 0.017 \sum_{i=1}^{N_d} C_i^d \tag{11}$$

where  $C_i^d$  are the concentrations of the dissolved charged species and  $N_d$  defines the number of the dissolved charged species (Allison et al. 1991).

#### 3.4. Numerical considerations

Benchmark levels B1-B3 do neither consider diffusion, nor dispersion, in order to allow for a better evaluation of numerical dispersion and operator-splitting errors as a function of different model formulations. Because significant spatial differences develop for porosity, hydraulic

conductivity, and tortuosity, the spatial weighting of these parameters is important. Harmonic averaging of all flow and transport parameters (i.e. hydraulic conductivity and tortuosity) were adopted as the recommended default option for the simulations. For spatial weighting of the advection terms, upstream weighting was used; implicit time weighting was used for time integration.

#### 4. Benchmark definition

#### 4.1. Dimensions and spatial discretization

- 139 The 2m long 1D-domain for benchmarks B1 B5 was discretized using a discretization interval
- of  $\Delta x = 0.025$  m, corresponding to 80 cells for uniform discretization, or 81 cells with half cells
- on the boundaries. The 2D-domain (3 m in length and 2 m in height) for benchmark B6 was
- discretized into 31x41=1271 cells (Figure 1).

#### 4.2. Physical properties

For the 1D problems B1 to B5, the porous medium is initially homogeneous with an initial porosity of 0.35 and an initial hydraulic conductivity of  $1.16 \times 10^{-4}$  m s<sup>-1</sup> (10 m day<sup>-1</sup>). An average free phase diffusion coefficient of  $1.0 \times 10^{-9}$  m<sup>-2</sup> s<sup>-1</sup> for all aqueous species is considered for benchmarks B4-B6. For problems including advection, dispersion is neglected to minimize the complexity of the problem and facilitate a focused comparison of the different codes. In addition, dispersion becomes insignificant when clogging occurs, due to reduced flow velocities and the localized nature of pore clogging due to mineral precipitation. For the 2D problem B6, advective and diffusive transport is considered in a similar fashion to B5. However, the porous medium is characterized by a heterogeneous initial hydraulic conductivity field (Figure 1).

#### 4.3. **Boundary conditions for flow**

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Benchmarks B1-B4 considered constant hydraulic heads at the inflow (0.007 m) and outflow (0.00 m) boundaries. For Benchmark B4, no-flow conditions are enforced by setting equal hydraulic heads at the inflow and outflow boundaries. For benchmark B6, the hydraulic head at the inflow boundary was set at 0.0105 m to maintain the same hydraulic gradient as with all other benchmarks (except B4).

#### 4.4. Mineralogical and chemical parameters

#### 4.4.1. Aqueous components and speciation reactions

- 161 The components for benchmarks B1 and B2 are  $H^+$ ,  $CO_3^{2-}$ ,  $Ca^{2+}$ ,  $SO_4^{2-}$  and  $Na^+$ . An enhanced set
- of components is used for benchmarks  $B3 B6 (H^+, CO_3^{2-}, Ca^{2+}, SO_4^{2-}, Fe^{3+}, Fe^{2+}, Al^{3+}, K^+, K^+, CO_3^{2-}, Ca^{2+}, SO_4^{2-}, SO_4^{2-}, SO_4^{2-}, SO_4^{2-}, SO_4^{2-}, SO_4^{2-}, SO_4^{2-}, SO_4^{2-}, SO_4^{2-}, SO_4^{$
- 163 O<sub>2</sub>(aq) and Na<sup>+</sup>). Relevant aqueous complexation reactions and activity model parameters are
- tabulated in the Supporting Information.

#### 165 **4.4.2. Minerals**

- Mineral phases and their parameters are listed in Table 2 and Table 3. Benchmarks B1 and B2
- use a subset of these mineral phases. All minerals are treated as kinetic surface-controlled
- dissolution/precipitation reactions. The only exception is jarosite, which was treated as an
- equilibrium reaction by HP1 owing to numerical difficulties. The initial rate constants  $(k_i^{m,0})$  are
- shown in Table 3.

#### 171 **4.4.3.** Initial and boundary conditions for reactive transport

- Benchmark B1: The only mineral phase considered is calcite at a volume fraction of 0.30 m<sup>3</sup> m<sup>-1</sup>
- 173 <sup>3</sup>, the remaining fraction of the solid phase is assumed inert. The solution domain is initially

occupied by an alkaline solution in equilibrium with calcite. The infiltrating water is acidic with a pH of 3 and is undersaturated with respect to calcite (Table 4). A third type boundary condition (specified mass flux) is used at the inflow boundary and a free exit boundary is used at the outflow. Benchmark B2: The mineral phases considered in the system are calcite and gypsum. The domain initially includes only calcite with a volume fraction of 0.30 m<sup>3</sup> m<sup>-3</sup> (Table 5). Resident pore water is in equilibrium with calcite and undersaturated with respect to gypsum (Table 6). With the infiltration of a sulfuric acid solution (pH = 3) containing CO<sub>3</sub><sup>2-</sup>, Ca<sup>2+</sup>, SO<sub>4</sub><sup>2-</sup> and Na<sup>+</sup>, calcite dissolves and gypsum precipitates, followed by gypsum re-dissolution near the inflow boundary. The initial and boundary geochemical compositions for the aqueous phases are listed in Table 6. Boundary conditions are set as in B1. **Benchmarks B3 – B6:** The domain initially contains calcite with a volume fraction of 0.22 m<sup>3</sup> m<sup>-3</sup>), as well as gibbsite (0.05 m<sup>3</sup> m<sup>-3</sup>) and siderite (0.05 m<sup>3</sup> m<sup>-3</sup>) (Table 7). The initial and boundary total component concentrations in the aqueous phases are listed in Table 8. The incoming solution is acidic and undersaturated with respect to all minerals, except jarosite. This boundary condition was specified to induce jarosite precipitation near the inflow. The background solution is slightly alkaline and is in equilibrium with calcite, siderite, gibbsite, and ferrihydrite. The initial volume fraction of calcite (0.22 m<sup>3</sup> m<sup>-3</sup>) is lower than that in B2. The lower calcite content limits secondary gypsum formation, which is offset by additional precipitation of ferrihydrite, siderite, gibbsite and jarosite. This approach is taken to provide a suitable benchmark that evaluates system evolution under near clogging conditions. Boundary conditions are set as in B1 and B2, with the exception of Benchmark B4 which uses first type

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(Dirichlet) boundary conditions at the inflow and outflow ends of the column.

#### 5. Results

Simulated results by all codes are discussed in the following subsections. Reference model results produced by MIN3P are also provided in tabular format in the Supporting Information.

#### 5.1. B1 – Porosity & permeability change due to dissolution

Simulation results for benchmark B1 show the gradual dissolution of calcite along an initially narrow dissolution front, which widens as permeability and flow velocities increase (Figure 2). Although porosity and permeability increase substantially near the inflow end already at early time, total flow rate increases are relatively moderate during the first 100 years. However, a rapid increase in flow rate is predicted, once calcite depletion approaches the outflow end of the simulation domain. All profiles of porosity, permeability and hydraulic head at 10 and 100 years calculated by the five codes are nearly identical, demonstrating very good agreement between the models, despite different transport schemes and coupling methods. Slight differences exist for results at 120 years. This time correlates with the breakthrough of the dissolution front and is naturally most sensitive to deviations. The time curves of the flux at the outflow boundary are identical for all codes up to 120 years.

#### 5.2. **B2** – Clogging due to dissolution/precipitation (simple reaction network)

Simulation results show that the intrusion of the sulfuric acid solution causes the dissolution of calcite and formation of gypsum (Figure 3). Although gypsum re-dissolves near the inflow, a narrow region of gypsum accumulation causes clogging of the flow path. The zone of gypsum accumulation is already visible after 10 years; however, significant porosity remains at this time. After 100 years, clogging is nearly complete and flow rates are greatly reduced, resulting in negligible clogging front migration over the remaining 900 years. Simulated results show good

agreement between all codes. The maximum volume fraction of gypsum reaches 62.6% and results in the reduction of porosity with a minimum value of 0.0016 after 1000 years at x=0.425 m (MIN3P, PFlotran and TOUGHREACT), at x=0.40 m with a minimum porosity of 0.003 (HP1) and at x=0.40 m with a minimum porosity of 0.0018 (CrunchFlow). The simulated profiles of the hydraulic head show a sharp decline at the clogging point. The calculated flux at the outflow boundary decreased rapidly within the first 100 years and more gradually after 500 years (Figure 3), showing good agreement amongst all codes with small deviations by HP1 owing to the higher minimum value of porosity by HP1.

#### 5.3. **B3** – Clogging due to dissolution/precipitation (complex reaction

#### network - advection)

Simulated results (Figure 4 and Figure 5) show that with the infiltration of the acidic solution, calcite dissolves, while other minerals like gypsum, siderite, gibbsite, ferrihydrite dissolve or precipitate depending on the time and location, thus forming various porosity modifications along the flow path at different time levels (Figure 5). Jarosite precipitates near the inflow, consequently, the porosity decreases near the infiltration boundary. However, the major porosity reduction occurs due to the dissolution of calcite and precipitation of gypsum, similar to benchmark level B2. At 10 years, the minimum porosity reduces from the initial value of 0.35 to 0.05 at 0.25 m, showing a tendency for clogging (Figure 4). The "clogging point" develops and moves further downstream to 0.45 m at 100 years. Beyond 100 years, however, the clogging point moves more slowly (Figure 4 top left), as clogging is nearly complete and water and solute fluxes are greatly reduced. At 300 years, the minimum porosity reached is 0.0044 (CrunchFlow), 0.0020 (HP1), 0.0028 (MIN3P), 0.0022 (PFlotran) and 0.0048 (TOUGHREACT).

Overall, the model results compare well for all five codes; all models are in good agreement with respect to the prediction of the mineral distribution and clogging location. However, there appears to be significant differences in terms of outflux at the end of the simulation (ranging over approximately 2 orders of magnitude). On the other hand, this apparent mismatch has to be put into perspective. Comparing the residual outflux to the initial outflux at T = 0 demonstrates that all models predict a reduction of flux by greater than 99.9%, which again points to a very good agreement in terms of predicting both hydrogeologic and geochemical evolution. Reasons for residual differences are likely due to the high sensitivity of fluxes to minor variations in porosity, which in turn is affected by the formation and dissolution of multiple mineral phases. These results highlight the challenges that numerical models encounter due to clogging and phase disappearance.

#### 5.4. B4 - Clogging due to dissolution/precipitation (complex reactions

#### network - diffusion)

Diffusive transport results in a similar geochemical evolution as simulated in the advective case (B3), but with mineral dissolution/precipitation fronts that are moving more slowly. Consequently, the kinetic limitations have a smaller effect on the results, which can be seen by the comparison of the profiles for jarosite. Jarosite was treated as a kinetically controlled mineral dissolution/precipitation reaction by all codes except HP1. The simulated results at 100 and 1000 years by HP1 agree better to those by CrunchFlow, MIN3P and PFlotran in comparison to Benchmark B3 (compare Figure 7 and Figure 5). Figure 6 (left) shows a region of reduced porosity, leading to reductions in tortuosity and effective diffusion coefficients (De) (Figure 6 right). The point with minimal porosity is located at 0.325 m after 3000 years. Simulated geochemical and hydrogeological evolution (Figure 6) as well as mineralogical composition

(Figure 7) by all participating codes showed good agreement. Generally, the simulated profiles of mineral volume fractions by MIN3P, CrunchFlow and PFlotran agree very well with slight difference for ferrihydrite and jarosite. Simulated mineral composition profiles by TOUGHREACT and HP1 showed slightly faster moving fronts for all minerals, but visual agreement among all codes can be considered as good.

#### 5.5. **B5** – Clogging due to dissolution/precipitation (complex chemical

#### reactions – advection and diffusion)

Overall, the predicted geochemical and hydrogeological evolution (Figure 8), as well as mineralogical composition (Figure 9) are in agreement for all participating codes. The clogging positions of all simulations are at 0.5 m, which closely coincides with the position determined in Benchmark B3. This indicates that the clogging position is controlled by the advective mass transport for the benchmark set considered here. The distributions of most minerals in B4 resemble those of B3 with slight differences in the location of the moving fronts except jarosite simulated by HP1. This can be explained because jarosite precipitation is treated as an equilibrium phase instead of kinetic precipitation, as specified in the benchmark.

In contrast to Benchmark B3, larger differences can be seen for outflux and minimum porosity (Figure 8). The simulated fluxes are fairly close within the first 90 years. At later time, simulated fluxes by MIN3P, HP1, PFlotran and CrunchFlow decrease gradually (Figure 8), while TOUGHREACT results suggest a substantial reduction of permeability that remains constant after about 160 years. Although all fluxes are small in relation to the initial flux through the system, the final predicted outfluxes vary by more than four orders of magnitude. The predicted outfluxes by MIN3P, PFlotran and CrunchFlow vary by less than two orders of magnitude. These differences suggest that the numerical formulation of diffusion processes plays a key role

for simulating porosity evolution, despite the fact that the problem is initially advection-dominated. In comparison to B3, reduction of fluxes occurs smoothly (compare Figure 4 and Figure 8). This indicates that diffusion tends to slow down clogging in this scenario but leads to substantial reduction of the minimum porosity and flux in the long term.

#### 5.6. **B6** – Clogging due to dissolution/precipitation in heterogeneous media

Simulated porosities for the 2D heterogeneous scenario are depicted in Figure 10 for two selected observation points P1 (x = 0.1 m, z = 1.0 m) and P2 (x = 0.5 m, z = 1.0 m) for MIN3P, CrunchFlow, TOUGHREACT and PFlotran. At P2 all simulated results of porosity evolution show good agreement – with a rapid decrease during the first 20 years and a slight increase thereafter (Figure 10). At P1, the simulated porosity show the same trend for the first 10 years, but the minimum porosity values differ substantially. At later time, the porosity increases again, gently according to MIN3P and CrunchFlow results, but more strongly according to the results obtained with PFlotran and TOUGHREACT.

The simulated flux curves by MIN3P, CrunchFlow, TOUGHREACT and PFlotran show a gradually decreasing trend with good agreement (Figure 11). The flux declined very rapidly over the first 10 years, during which all simulated results are almost identical. At later times, the flux continues to decrease but at a reduced rate. These results seem to contradict the simulated porosity evolution at the observation points, which showed substantial differences at P1. However, these results also indicate that the overall permeability evolution is reproduced in a similar fashion by all codes, and that differences are local.

This observation is confirmed further by examining simulated 2D porosity distributions at 300 years. Results obtained with the different codes showed very similar pattern illustrating the effect of heterogeneity on clogging (Figure 12). The low porosity zones (in blue), distributed

between x = 0.4 and 0.7 m, tend to form a continuous low permeability belt, which prevents flow through the domain. The high porosity zones (in red) formed through the dissolution of calcite and are most prevalent in the regions of higher initial hydraulic conductivity (compare Figure 12 and Figure 1).

#### 6. Discussion

We acknowledge that the Carman-Kozeny relationship and Archie's law are not the only relationships to describe the dependency of permeability and tortuosity on porosity. Multiple alternative relationships exist to describe permeability and tortuosity evolution (e.g. Saripalli et al. 2001). The model comparison presented here showed good agreement between the five codes, but this does not imply that any of the codes – as is – is applicable to simulate permeability or tortuosity evolution at a field site or in a laboratory experiment. It needs to be evaluated whether the implemented relationships are suitable for the site or experimental conditions. However, most of the alternative relationships such as for example the Brinkmann or Fair-Hatch models for permeability will also be a function of porosity (Le Gallo et al. 1998) and the general findings of the present investigation should therefore also be relevant for other approaches. Lastly, it has to be recognized that permeability and tortuosity are not only functions of porosity, but may also depend on micro-structural transformations that are taking place, i.e. different secondary minerals may affect permeability in different ways due to their different growth habit (Gouze and Coudrain-Ribstein, 2002).

#### 7. Conclusions

A six-level benchmark problem with increasing complexity for flow, geochemical and mineralogical conditions was analysed with five different reactive transport codes (i.e.

CrunchFlow, HP1, MIN3P, PFlotran and TOUGHREACT). The purpose of the benchmarking exercise was to evaluate the robustness of various numerical implementations of permeability-porosity and tortuosity-porosity relationships to assess the feedback between flow and reactive transport with the potential for local phase disappearance, and the tendency for complete clogging due to mineral precipitation.

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Generally speaking, the simulation results appear to be robust and not dependent on the employed code. Simulating porosity enhancement due to mineral dissolution proved to be an easier task than simulating clogging. Increasing complexity due to the inclusion of additional transport mechanisms and a more complex mineralogical assemblage had an impact on the agreement of the model results obtained by the various codes. Although all codes showed good agreement of the predicted mineralogical assemblage and the clogging locations, absolute values of mass fluxes differed substantially. As discussed, these results have to be seen in perspective, considering that the results of all codes agree in the sense that flux reductions are near 100% for the clogging scenarios. Although differences exist in terms of the absolute flux values, the impact on interpretation of the results would be very limited or even negligible. Nevertheless, these results highlight the difficulties to simulate problems with pore clogging and phase disappearance. Interestingly, the 2D problem (B6) showed better agreement among the codes than the equivalent 1D problem (B5), despite the additional complexity in terms of dimensionality and heterogeneity. Although local differences in porosity and mineral assemblage were significant, agreement between overall outflow was good.

This benchmarking exercise also highlights that the implementation of the permeability-porosity and tortuosity-porosity relationships, the activity correction model, and the numerical

methods (e.g. spatial weighting schemes) can significantly affect the benchmarking results. A
consistent numerical treatment is crucial for the benchmarking of reactive transport codes.

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#### **Tables:**

#### 446 **Table 1 Overview of the benchmarks**

Benchmark Level	Description	Dimension	Processes	t <sub>Final</sub> # [years]
B1	Dissolution only		advection, kinetic dissolution	500
B2	Clogging in a simple geochemical system		advection, kinetic dissolution/ precipitation	1000
В3		1D	advection, kinetic dissolution/ precipitation, redox reactions	300
B4		homogeneous (2m in length)	Diffusion, no advection, kinetic dissolution/precipitation, redox reactions	3000
В5	Clogging in a complex geochemical system		advection, diffusion, kinetic dissolution/precipitation, redox reactions	300
В6		2D heterogeneous (3m in length and 2m in height)	advection, diffusion, kinetic dissolution/ precipitation, redox reactions	300

#- Final simulation time

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#### 449 Table 2 Reaction stoichiometries and solubility constants for minerals

Mineral	Reaction	logK <sub>25</sub>
Calcite	$Ca^{2+} + CO_3^{2-} \leftrightarrow CaCO_3$	8.4750
Gypsum	$\operatorname{Ca}^{2+} + \operatorname{SO_4^{2-}} + 2\operatorname{H_2O} \leftrightarrow \operatorname{CaSO_4} : 2\operatorname{H_2O}$	4.5800
Ferrihydrite	$Fe^{3+} + 3H_2O \leftrightarrow Fe(OH)_3 + 3H^+$	-4.8910
Jarosite	$K^{+} + 3Fe^{3+} + 2SO_{4}^{2-} + 6H_{2}O \leftrightarrow KFe_{3}(SO_{4})_{2}(OH)_{6} + 6H^{+}$	9.2100
Gibbsite	$Al^{3+} + 3H_2O \leftrightarrow Al(OH)_3 + 3H^+$	-8.1100
Siderite	$Fe^{2+} + CO_3^{2-} \leftrightarrow FeCO_3$	10.4500

#### 451 Table 3 Physical and kinetic mineral parameters

Mineral	$k_i^{m,0}$ [m <sup>2</sup> mineral L <sup>-1</sup> bulk]	Density [g cm <sup>-3</sup> ]	Mol. weight [g mol <sup>-1</sup> ]	Molar volume [cm <sup>3</sup> mol <sup>-1</sup> ]	Update type
Calcite	5×10 <sup>-8</sup>	2.71	100.09	36.93	twothird
Gypsum	5×10 <sup>-8</sup>	2.32	172.17	74.21	constant
Ferrihydrite	5×10 <sup>-9</sup>	4.37	104.87	23.99	constant
Jarosite	5×10 <sup>-9</sup>	3.20	494.81	154.63	constant
Gibbsite	5×10 <sup>-10</sup>	2.35	78.00	33.19	twothird
Siderite	5×10 <sup>-9</sup>	3.96	115.86	29.26	twothird

#### Table 4 Initial and boundary geochemical compositions in aqueous phase (B1)

Primary components	Unit	Initial condition	<b>Boundary condition</b>
рН	-	9.38	3.0
Ca <sup>2+</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	1.57×10 <sup>-4</sup>	1.00×10 <sup>-4</sup>
$CO_3^{2-}$	mol l <sup>-1</sup> H <sub>2</sub> O	2.57×10 <sup>-4</sup>	1.0×10 <sup>-2</sup>
SO <sub>4</sub> <sup>2-</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	1.00×10 <sup>-10</sup>	6.46×10 <sup>-4</sup>

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# Table 5 Initial mineral composition and saturation index (SI) in the initial and boundary solutions (B2)

Mineral	Initial volume fraction [m <sup>3</sup> m <sup>-3</sup> ]	SI (IC solution)	SI (BC solution)
Calcite	0.3	0.0	-9.1
Gypsum	0.0	-3.1	-1.9

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#### Table 6 Initial and boundary geochemical compositions in aqueous phase (B2)

Primary components	Unit	Initial condition (IC)	Boundary condition (BC)
рН	pН	9.33	3.0
Ca <sup>2+</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	1.70×10 <sup>-4</sup>	1.0×10 <sup>-4</sup>
$CO_3^{2-}$	mol l <sup>-1</sup> H <sub>2</sub> O	2.70×10 <sup>-4</sup>	1.0×10 <sup>-2</sup>
SO <sub>4</sub> <sup>2-</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	1.70×10 <sup>-4</sup>	0.2
Na <sup>+</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	3.20×10 <sup>-4</sup>	3.96×10 <sup>-1</sup>

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## Table 7 Initial mineral composition and saturation index (SI) in the initial and boundary solutions (B3-B6)

Mineral	Initial volume fraction [m³ m⁻³]	SI (IC solution)	SI (BC solution)
Calcite	0.22	0.00	-8.93
Gypsum	0.00	-2.78	-2.02
Ferrihydrite	0.00	0.00	-0.07
Jarosite	0.00	-12.97	6.66
Gibbsite	0.05	0.00	-2.94
Siderite	0.05	0.00	-10.89

Table 8 Initial and boundary geochemical compositions in aqueous phase (B3-B6)

Primary components	Unit	Initial condition (IC)	Boundary condition (BC)
рН	-	8.01	3.0
pe	-	-0.67	17.53
Ca <sup>2+</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	4.71×10 <sup>-4</sup>	1.00×10 <sup>-4</sup>
$\mathrm{CO_3}^{2\text{-}}$	mol l <sup>-1</sup> H <sub>2</sub> O	2.19×10 <sup>-3</sup>	1.00×10 <sup>-2</sup>
$SO_4^{2-}$	mol l <sup>-1</sup> H <sub>2</sub> O	1.70×10 <sup>-4</sup>	1.00×10 <sup>-1</sup>
Na <sup>+</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	$1.54 \times 10^{-3}$	$9.09 \times 10^{-2}$
$Al^{3+}$	mol l <sup>-1</sup> H <sub>2</sub> O	2.81×10 <sup>-7</sup>	1.43×10 <sup>-2</sup>
$\mathbf{K}^{+}$	mol l <sup>-1</sup> H <sub>2</sub> O	1.00×10 <sup>-5</sup>	7.67×10 <sup>-5</sup>
Fe <sup>2+</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	6.59×10 <sup>-6</sup>	1.14×10 <sup>-8</sup>
Fe <sup>3+</sup>	mol l <sup>-1</sup> H <sub>2</sub> O	2.53×10 <sup>-8</sup>	2.23×10 <sup>-2</sup>

### Figures

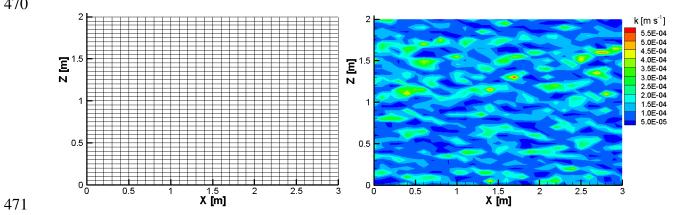


Figure 1 2D geometry (left) and initial hydraulic conductivity distribution (in [m s<sup>-1</sup>]) (right)

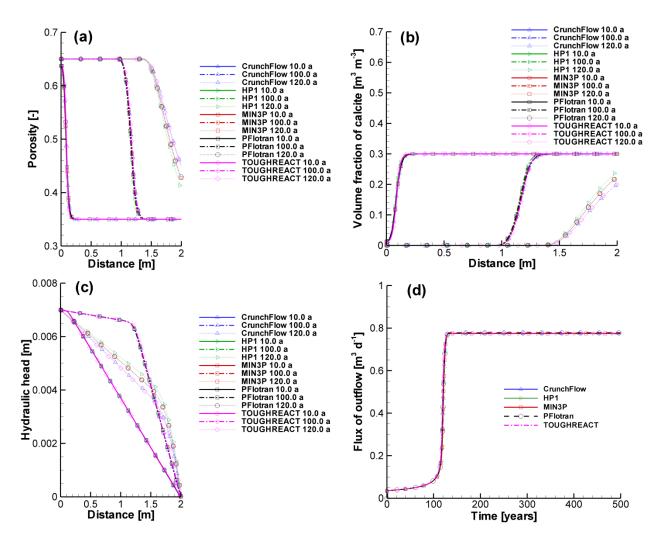


Figure 2 Profiles of porosity (a), volume fraction of calcite (b), hydraulic head (c) at 10, 100 and 120 years, and flux time curve (d) from the outflow boundary simulated by CrunchFlow, HP1, MIN3P, PFlotran and TOUGHREACT

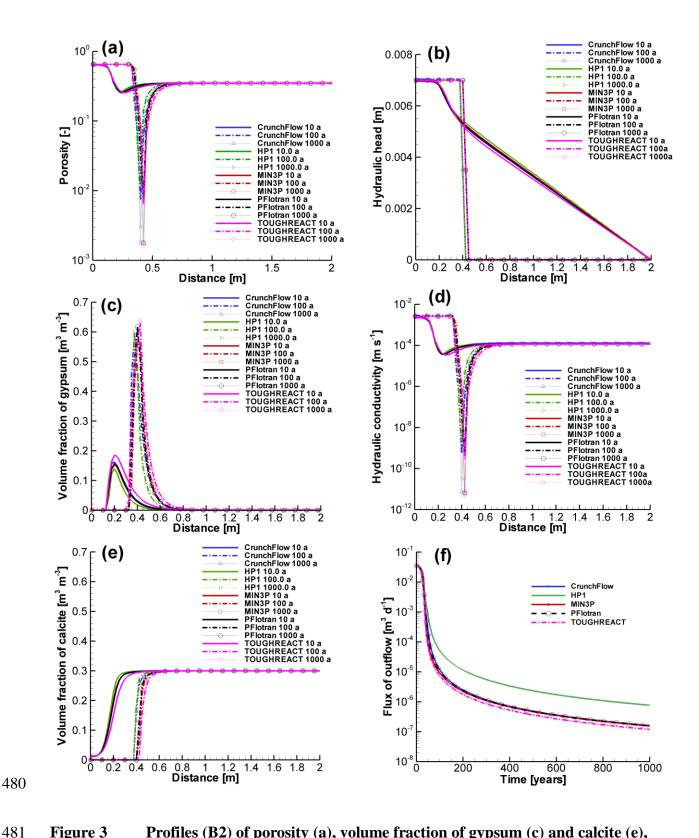


Figure 3 Profiles (B2) of porosity (a), volume fraction of gypsum (c) and calcite (e), hydraulic head (b), hydraulic conductivity (d) at 10, 100 and 120 years, and flux from the outflow boundary (f) simulated by CrunchFlow, HP1, MIN3P, PFlotran and TOUGHREACT



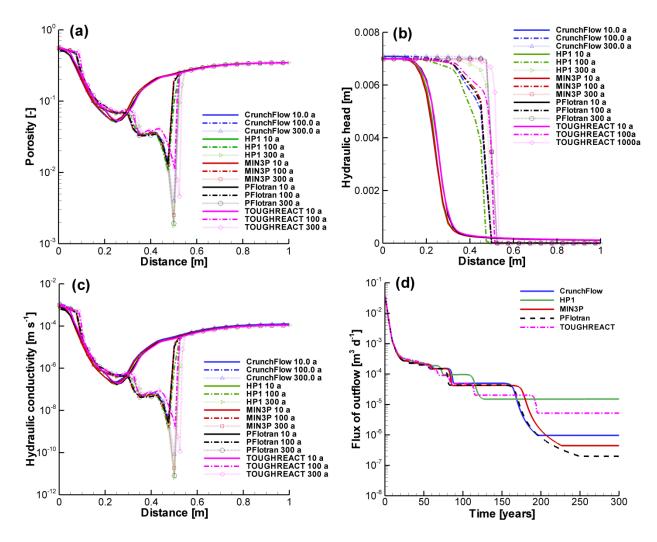


Figure 4 Comparison of profiles (B3) of porosity, hydraulic head and hydraulic conductivity at 10, 100 and 300 years, and outflux time curve from the outflow boundary simulated by CrunchFlow, HP1, MIN3P, PFlotran and TOUGHREACT

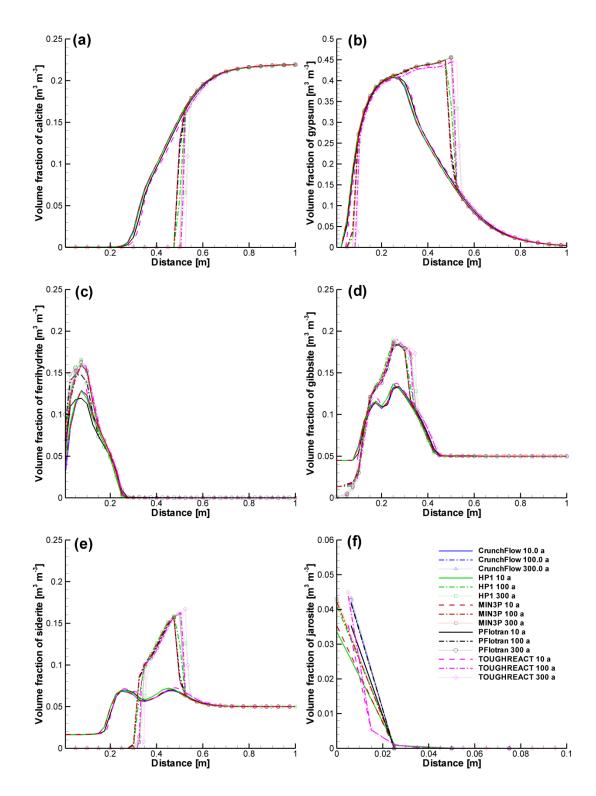


Figure 5 Comparison of volume fraction profiles (B3) of calcite (a), gypsum (b), ferrihydrite (c), gibbsite (d), siderite (e) and jarosite (f) at 10, 100 and 300 years simulated by CrunchFlow, HP1, MIN3P, PFlotran and TOUGHREACT

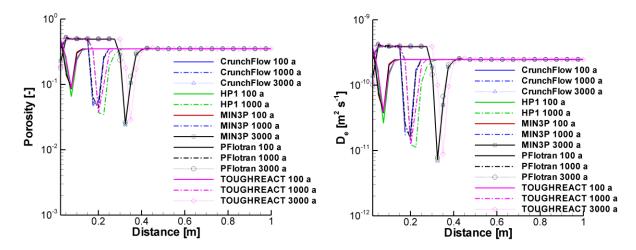


Figure 6 Comparison of profiles (B4) of porosity (left) and effective diffusion coefficient ( $D_e$ ) (right) at 100, 1000 and 3000 years simulated by CrunchFlow, MIN3P, PFlotran, TOUGHREACT and HP1 (at 100 and 1000 years)

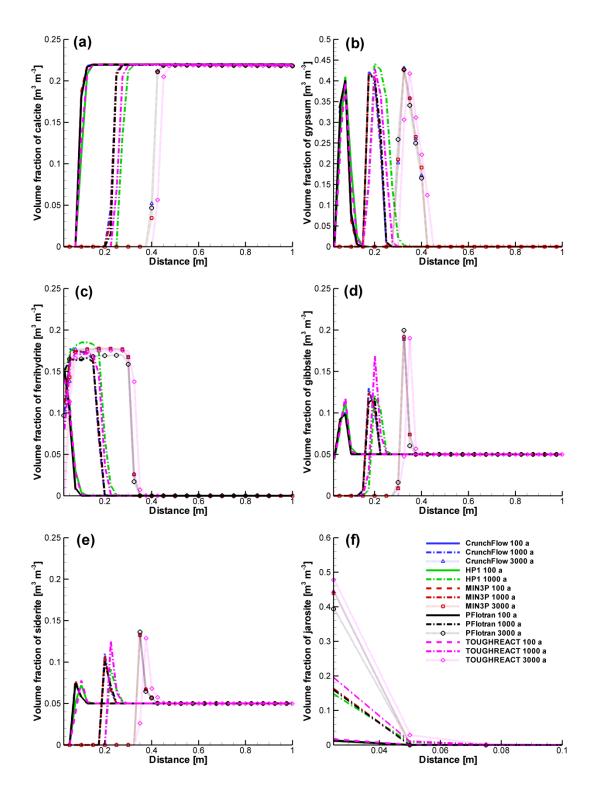


Figure 7 Comparison of mineral volume fraction profiles (B4) of calcite (a), gypsum (b), ferrihydrite (c), gibbsite (d), siderite (e) and jarosite (f) at 100, 1000 and 3000 years simulated by CrunchFlow, MIN3P, PFlotran and TOUGHREACT, and HP1 (for 100 and 1000 years)

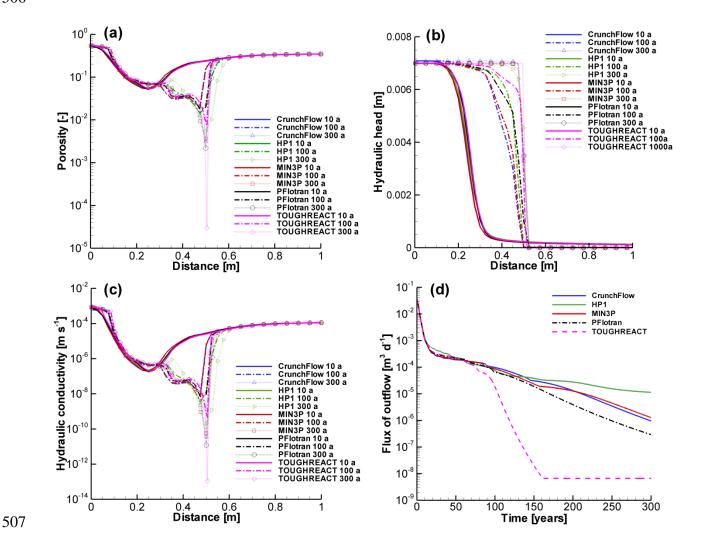


Figure 8 Comparison of profiles (B5) of porosity (a), hydraulic head (b) and hydraulic conductivity (c) at 10, 100 and 300 years, and outflux time curve from the outflow boundary (d) simulated by CrunchFlow, HP1, MIN3P, PFlotran and TOUGHREACT

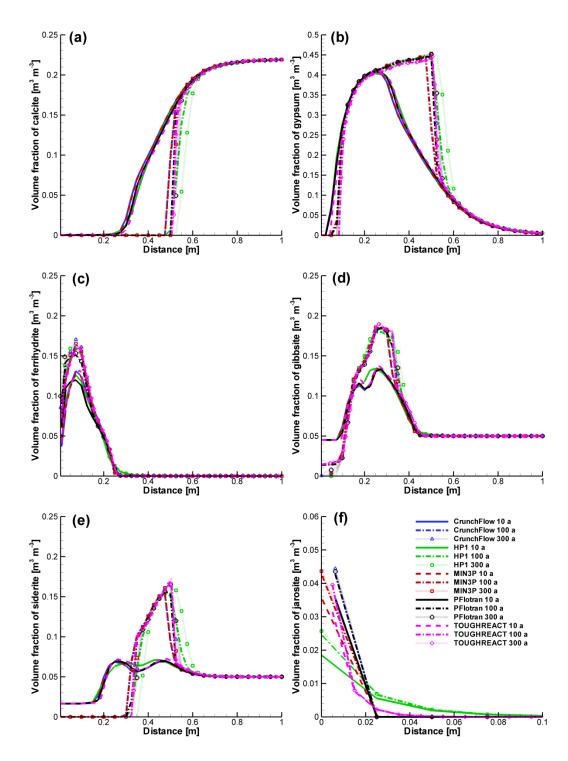


Figure 9 Comparison of volume fraction profiles (B5) of calcite (a), gypsum (b), ferrihydrite (c), gibbsite (d), siderite (e) and jarosite (f) at 10, 100 and 300 years simulated by CrunchFlow, HP1, MIN3P, PFlotran and TOUGHREACT

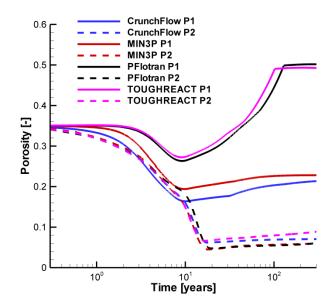


Figure 10 Comparison of porosity evolution (B6) at observation point P1 (0.1 m, 1.0 m) and P2 (0.5 m, 1.0 m) simulated by CrunchFlow, MIN3P, PFlotran and TOUGHREACT



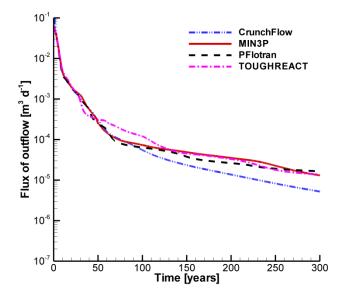


Figure 11 Comparison of flux evolution at outflow boundary (B6) simulated by CrunchFlow, MIN3P, PFlotran and TOUGHREACT

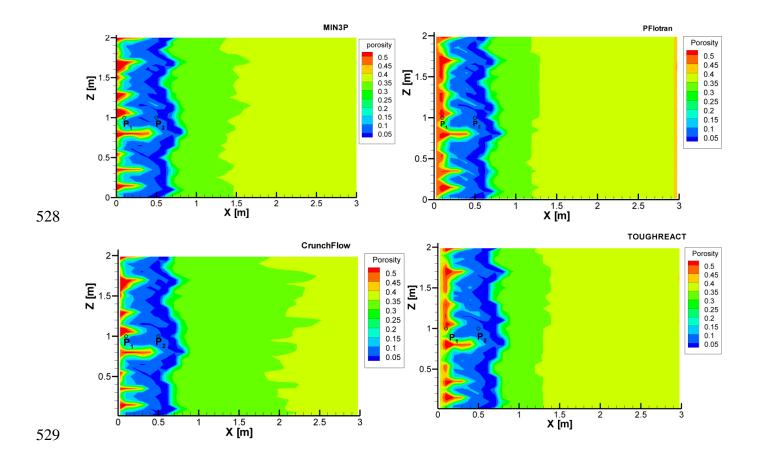


Figure 12 2D distribution of porosity (B6) simulated by MIN3P, CrunchFlow and PFlotran and TOUGHREACT at 300 years, and the positions of the observation points P1 (x = 0.1 m, z = 1.0 m) and P2 (x = 0.5 m, z = 1.0 m)

534	Supporting Information: Implementation and evaluation of
535	permeability-porosity and tortuosity-porosity relationships linked to
536	mineral dissolution-precipitation
537 538 539 540 541	Mingliang Xie <sup>1,*</sup> , K. Ulrich Mayer <sup>1</sup> , Francis Claret <sup>2</sup> , Peter Alt-Epping <sup>3</sup> , Diederik Jacques <sup>4</sup> , Carl Steefel <sup>5</sup> , Christophe Chiaberge <sup>2</sup> and Jiri Simunek <sup>6</sup>
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Table S-1 Physical and thermodynamic parameters for components

Component	Chargo	Debye-Huckel constants		Molar weight	Alkalinity
Component	Charge	a	b	[g mol <sup>-1</sup> ]	factor
O <sub>2</sub> (aq)	0.0	3.0	0	31.9998	0
H <sub>2</sub> O	0.0	0.0	0	18.0153	0
$Al^{+3}$	3.0	9.0	0	26.9815	0
CO <sub>3</sub> -2	-2.0	5.4	0	60.0094	2
Ca <sup>+2</sup>	2.0	6.0	0.17	40.08	0
Fe <sup>+2</sup>	2.0	6.0	0	55.847	0
Fe <sup>+3</sup>	3.0	9.0	0	55.847	0
$\mathbf{H}^{+}$	1.0	9.0	0	1.008	-1
K <sup>+</sup>	1.0	3.0	0.01	39.102	0
Na <sup>+</sup>	1.0	4.0	0.07	22.9898	0
$SO_4^{-2}$	-2.0	4.0	-0.04	96.0616	0

Table S-2 Geochemical reactions of aqueous species and thermodynamic parameters

$\begin{array}{llllllllllllllllllllllllllllllllllll$	Species	Mol mass	Reaction	$\log$ K <sub>25</sub>	Debye Hueckel constant	
$\begin{array}{c} H_2SO_4(aq) & 98.0776 & 2H^+ + SO_4^2 = H_2SO_4(aq) & -1.0209 & 0.00 & 0.00 \\ H_2(aq) & 2.0160 & H_2O - 0.5 O_5(aq) = H_3(aq) & -46.1070 & 0.00 & 0.00 \\ GCO_5^* & 115.8562 & Fe^{3+} + CO_3^2 = FeCO_5^* & 9.7200 & 0.00 & 0.00 \\ OH & 17.0074 & H_2O + H = OH & -13.9980 & 3.5.0 & 0.00 \\ CaOH^+ & 57.0870 & Ca^{2+} + H_2O - H^- = CaOH & -12.7800 & 6.00 & 0.00 \\ CaHCO_5^* & 101.0970 & Ca^{2+} + CO_3^2 = CaCO_3(aq) & -12.7800 & 6.00 & 0.00 \\ CaCO_3aq & 100.0890 & Ca^{3+} + CO_3^2 = CaCO_3(aq) & 3.2200 & 0.00 & 0.00 \\ CaCO_3aq & 136.1410 & Ca^{3+} + SO_4^2 = CaSO_4(aq) & 2.3090 & 0.00 & 0.00 \\ CaSO_4aq & 136.1410 & Ca^{3+} + SO_4^2 = CaSO_4(aq) & 2.3090 & 0.00 & 0.00 \\ NaCO_3^* & 82.9990 & Na^+ + CO_3^2 = NaCO_3^* & 1.2680 & 5.40 & 0.00 \\ NaCO_3^* & 82.9990 & Na^+ + CO_3^2 = NaCO_3^* & 1.2680 & 0.00 & 0.00 \\ NaBCO_3aq & 84.0070 & Na^+ + CO_3^2 + H^- = SAHCO_3(aq) & 10.0800 & 0.00 & 0.00 \\ NaSO_4^* & 119.0510 & Na^+ + SO_4^2 = NaSO_4^* & 0.7000 & 5.40 & 0.00 \\ NaSO_4^* & 119.0510 & Na^+ + SO_4^2 = NaSO_4^* & 0.8500 & 5.40 & 0.00 \\ AIOH^{2+} & 43.988 & A^{3+} + H_2O - H^- = AIOH^{2+} & 4.9900 & 5.40 & 0.00 \\ AIOH_2^* & 40.996 & A^{12} 2 + H_2O - 2 H^- = AIOH_2^{1-} & 4.9900 & 5.40 & 0.00 \\ AISO_4^* & 123.043 & AP^{1+} + SO_4^2 = AISO_4^* & 3.5000 & 4.50 & 0.00 \\ AISO_4^{12} & 124.0509 & A^{13+} + SO_4^2 = AISO_4^* & 3.5000 & 4.50 & 0.00 \\ AI(OH)_3aq & 78.030 & AP^{13} + H_2O - 3 H^- = AIIOH_3(aq) & -16.9000 & 0.00 & 0.00 \\ FeOH^- & 72.854 & Fe^{2+} + H_2O - 3 H^- = AI(OH)_3(aq) & -16.9000 & 0.00 & 0.00 \\ FeOH^{2} & 10.6869 & Fe^{2+} + 3 H_2O - 3 H^- = Fe(OH)_2^* & -3.0680 & 0.00 & 0.00 \\ FeCOH_2^3 & 15.2.9159 & Fe^{2+} + SO_4^2 = FeSO_4(aq) & -2.5700 & 0.00 & 0.00 \\ FeCOH_2^3 & 15.908 & Fe^{3+} + H_2O - H^+ = FeHSO_3^* & 4.4480 & 5.00 & 0.00 \\ FeCOH_2^3 & 15.908 & Fe^{3+} + H_2O - H^+ = FeHSO_3^* & 4.4480 & 5.00 & 0.00 \\ FeCOH_2^3 & 19.936 & Fe^{3+} + SO_4^2 = FeSO_4(aq) & -2.5700 & 5.00 & 0.00 \\ FeCOH_2^3 & 19.936 & Fe^{3+} + SO_4^2 = FeSO_4 & 4.4480 & 5.00 & 0.00 \\ FeCOH_2^3 & 19.936 & Fe^{3+} + SO_4^2 = FeSO_4 &$		[g mol <sup>-1</sup> ]			a	b
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	KHSO <sub>4</sub> (aq)	136.1716			0.00	0.00
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$H_2SO_4(aq)$	98.0776			0.00	0.00
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$		2.0160			0.00	0.00
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	FeCO <sub>3</sub> <sup>+</sup>	115.8562		9.7200	0.00	0.00
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$		17.0074			3.50	0.00
$ \begin{array}{c} CaCO_3aq & 100.0890 & Ca^{2+} + CO_3^{2-} = CaCO_3(aq) & 3.2200 & 0.00 & 0.00 \\ CaSO_3aq & 136.1410 & Ca^{2+} + SO_4^{2-} = CaSO_4(aq) & 2.3090 & 0.00 & 0.00 \\ CaHSO_4^+ & 137.1489 & Ca^{2+} + SO_4^{2-} + R^- CaHSO_4^+ & 3.0680 & 0.00 & 0.00 \\ NaCO_3^- & 82.9990 & Na^- + CO_3^{2-} + R^- CO_3^- & 1.2680 & 5.40 & 0.00 \\ NaCO_3^- & 82.9990 & Na^+ + CO_3^{2-} + R^- CO_3^- & 1.2680 & 5.40 & 0.00 \\ NaHCO_3aq & 84.0070 & Na^+ + CO_3^{2-} + R^- CO_3^- & 1.2680 & 0.00 & 0.00 \\ NaSO_4 & 119.0510 & Na^+ + SO_4^{2-} + RSO_4^- & 0.7000 & 5.40 & 0.00 \\ KSO_4 & 135.163 & K^+ + SO_4^{2-} + KSO_4^- & 0.8500 & 5.40 & 0.00 \\ AIOH^{2-} & 43.988 & AI^{3+} + H_2O - H^+ = AIOH^{2-} & -4.9900 & 5.40 & 0.00 \\ AI(OH)_2^+ & 60.996 & AI^{3+} 2 + H_2O - 2 H^+ = AI(OH)_2^+ & -10.1000 & 5.40 & 0.00 \\ AISO_4^+ & 123.043 & AI^{3+} + SO_4^{2-} + AISO_4^+ & 3.5000 & 4.50 & 0.00 \\ AISO_4^+ & 123.043 & AI^{3+} + SO_4^{2-} + AISO_4^+ & 3.5000 & 4.50 & 0.00 \\ AI(OH)_3aq & 219.104 & AI^{3+} + 2 SO_4^2 - AI(SO_4)_2 & 5.0000 & 4.50 & 0.00 \\ AI(OH)_3aq & 78.003 & AI^{3+} 3 + H_2O - 3 H^+ = AI(OH)_3 & -16.9000 & 0.00 & 0.00 \\ FeOH^+ & 72.854 & Fe^{2+} + SO_4^{2-} + FeOH^- & -9.5000 & 5.00 & 0.00 \\ FeSO_4aq & 151.908 & Fe^{2+} + SO_4^{2-} + FeOH^- & -9.5000 & 5.00 & 0.00 \\ FeSO_4aq & 151.908 & Fe^{2+} + SO_4^{2-} + FeSO_3(aq) & 2.2500 & 0.00 & 0.00 \\ FeCOH_2aq & 89.861 & Fe^{2+} + SO_4^{2-} + FeSO_3q & 4.3800 & 0.00 & 0.00 \\ FeCO_3^+ & 116.8641 & Fe^{2+} + CO_3^{2-} + FeSO_3q & 4.3800 & 0.00 & 0.00 \\ FeSO_4 & 151.908 & Fe^{3+} + SO_4^{2-} + FeSO_3q & 4.3800 & 0.00 & 0.00 \\ FeSO_4 & 151.908 & Fe^{3+} + SO_4^{2-} + FeSO_3q & 4.3800 & 0.00 & 0.00 \\ FeSO_4 & 151.908 & Fe^{3+} + SO_4^{2-} + FeSO_3q & 4.3800 & 0.00 & 0.00 \\ FeSO_4 & 151.908 & Fe^{3+} + SO_4^{2-} + FeSO_3q & 4.3800 & 0.00 & 0.00 \\ FeSO_4 & 151.908 & Fe^{3+} + SO_4^{2-} + FeSO_3q & 4.3800 & 0.00 & 0.00 \\ FeSO_4 & 151.908 & Fe^{3+} + SO_4^{2-} + FeSO_3^{4-} & 4.0400 & 5.00 & 0.00 \\ FeSO_4 & 151.908 & Fe^{3+} + SO_4^{2-} + FeSO_3^{4-} & 4.0400 & 5.00 & 0.00 \\ FeSO_4 & 151.908 & Fe^{3+} + SO$	CaOH <sup>+</sup>	57.0870		-12.7800	6.00	0.00
$ \begin{array}{c} CaSO_4aq \\ CaSO_4aq \\ CaHSO_4^+ \\ 137.1489 \\ Ca^{2+} + SO_4^{2-} + H^+ = CaHSO_4^+ \\ 3.0680 \\ 0.00 $	CaHCO <sub>3</sub> <sup>+</sup>	101.0970		11.4400	6.00	0.00
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	CaCO₃aq	100.0890	$Ca^{2+} + CO_3^{2-} = CaCO_3(aq)$	3.2200	0.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	CaSO <sub>4</sub> aq	136.1410		2.3090	0.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	CaHSO <sub>4</sub> <sup>+</sup>	137.1489		3.0680	0.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	NaCO <sub>3</sub>	82.9990	$Na^{+} + CO_{3}^{2} = NaCO_{3}^{-}$	1.2680	5.40	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	NaHCO <sub>3</sub> aq	84.0070		10.0800	0.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	NaSO <sub>4</sub>	119.0510	$Na^+ + SO_4^{2-} = NaSO_4^-$	0.7000	5.40	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		135.163	$K^{+} + SO_{4}^{2} = KSO_{4}^{-}$	0.8500	5.40	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	AlOH <sup>2+</sup>	43.988	$Al^{3+} + H_2O - H^+ = AlOH^{2+}$	-4.9900	5.40	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Al(OH) <sub>2</sub> <sup>+</sup>	60.996	$Al^{3+} 2+ H_2O - 2 H^+ = Al(OH)_2^+$	-10.1000	5.40	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Al(OH) <sub>4</sub>	95.011	$Al^{3+} + 4 H_2O - 4 H^+ = Al(OH)_4^-$	-22.7000	4.50	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	AlSO <sub>4</sub> <sup>+</sup>	123.043	$Al^{3+} + SO_4^{2-} = AlSO_4^{+}$	3.5000	4.50	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	AlHSO <sub>4</sub> <sup>2+</sup>	124.0509	$Al^{3+} + SO_4^{2-} + H^+ = AlHSO_4^{2+}$	2.4480	4.50	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$			$Al^{3+} + 2 SO_4 2 - = Al(SO_4)_2$	5.0000		
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Al(OH)3aq	78.003	$Al^{3+} 3+ H_2O - 3 H^+ = Al(OH)_3(aq)$	-16.9000	0.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	FeOH <sup>+</sup>		$Fe^{2+} + H_2O - H^+ = FeOH^+$	-9.5000	5.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Fe(OH) <sub>3</sub>	106.869	$Fe^{2+} + 3 H_2O - 3 H^+ = Fe(OH)_3^-$	-31.0000	5.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	FeSO <sub>4</sub> aq		$Fe^{2+} + SO_4^{2-} = FeSO_4(aq)$	2.2500	0.00	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	FeHSO <sub>4</sub> <sup>+</sup>	152.9159	$Fe^{2+} + SO_4^{2-} + H^+ = FeHSO_4^+$	3.0680	0.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		116.8641	$Fe^{2+} + CO_3^{2-} + H^+ = FeHCO_3^+$	12.3300	0.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	FeCO <sub>3</sub> aq		$Fe^{2+} + CO_3^{2-} = FeCO_3aq$	4.3800	0.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Fe(OH) <sub>2</sub> aq	89.861	$Fe^{2+} + 2 H_2O - 2 H^+ = Fe(OH)_2(aq)$	-20.5700		
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	FeOH <sup>2+</sup>	72.854	$Fe^{3+} + H_2O - H^+ = FeOH^{2+}$	-2.1900	5.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	FeSO <sub>4</sub> <sup>+</sup>	151.908	$Fe^{3+} + SO_4^{2-} = FeSO_4^{+}$	4.0400	5.00	0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	FeHSO <sub>4</sub> <sup>2+</sup>		$Fe^{3+} + SO_4^{2-} + H^+ = FeHSO_4^{2+}$	4.4780		
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		89.861	$Fe^{3+} + 2 H_2O - 2 H^+ = Fe(OH)_2^+$	-5.6700		0.00
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Fe(OH) <sub>3</sub> aq		$Fe^{3+} + 3 H_2O - 3 H^+ = Fe(OH)_3(aq)$	-12.5600		
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		-	$Fe^{3+} + 4 H_2O - 4 H^+ = Fe(OH)_4$	-21.6000		
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Fe(SO <sub>4</sub> ) <sub>2</sub>	1	$Fe^{3+} + 2SO_4^{2-} = Fe(SO_4)_2^{-}$	5.3800		
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	Fe <sub>2</sub> (OH) <sub>2</sub> <sup>+4</sup>					
$HCO_3^ 61.0170$ $H^+ + CO_3^{-2}$ = $HCO_3^ 10.3300$ $5.40$ $0.00$ $H_2CO_3$ aq $62.0250$ $2H^+ + CO_3^{-2}$ = $H_2CO_3$ (aq) $16.6810$ $0.00$ $0.00$	Fe <sub>3</sub> (OH) <sub>4</sub> <sup>+5</sup>			-6.3000		
$H_2CO_3aq$ 62.0250 $2H^+ + CO_3^2 = H_2CO_3(aq)$ 16.6810 0.00 0.00	HCO <sub>3</sub>		$H^{+} + CO_{3}^{2} = HCO_{3}^{-}$	10.3300		
		97.0690	$SO_4^{2-} + H^+ = HSO_4^+$		4.50	0.00

The following equilibrium redox reaction is considered for the benchmarks B3 - B6:

560

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$$Fe^{3+} \leftrightarrow Fe^{2+} + \frac{1}{4} O_2(aq) + H^+ - \frac{1}{2} H_2O$$
  $log K_{25} = -8.4725$ 

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## Reference model results produced by MIN3P were included in EXCEL files:

- 565 Figure 2: Xie-et-al-2014-B1-Fig2.xlsx
- Figure 3: Xie-et-al-2014-B2-Fig3.xlsx
- Figure 4: Xie-et-al-2014-B3-Fig4.xlsx
- Figure 5: Xie-et-al-2014-B3-Fig5.xlsx
- Figure 6: Xie-et-al-2014-B4-Fig6.xlsx
- 570 Figure 7: Xie-et-al-2014-B4-Fig7.xlsx
- 571 Figure 8: Xie-et-al-2014-B5-Fig8.xlsx
- Figure 9: Xie-et-al-2014-B5-Fig9.xlsx
- 573 Figure 10: Xie-et-al-2014-B6-Fig10.xlsx
- Figure 11: Xie-et-al-2014-B6-Fig11.xlsx
- 575 Figure 12: Xie-et-al-2014-B6-Fig12.xlsx

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