# **5.1 Dehydrogenation of Propane**

- Example 4.7-2 Dehydrogenation of Propane
- Process Model
- Product Composition
- Recycle Ratio
- Single Pass Conversion
- How Does Process Performance Depend on Single Pass Conversion?

## **Process Model**

```
In [1]:
from sympy import *
# define constants
nfeed = 100.0
# define variables
var('X')
var('n1:11')
# define constants
# unit balances
mixer = [
    Eq(nfeed + n9, n1), # C3H8
                              # C3H6
    Eq(n10, n2)
reactor = [
   Eq(n3, n1 - X), # C3H8
Eq(n4, n2 + X), # C3H6
Eq(n5, X) # H2
    Eq(n5, X)
]
separator = [
                          # C3H8
# C3H6
    Eq(n3, n6 + n9),
    Eq(n4, n7 + n10),
    Eq(n5, n8)
                              # H2
]
# process specifications
specs = [
   Eq(n6, (1-0.95)*nfeed), # 95% process conversion
    Eq(n6, 0.00555*n3), # 0.555% of propane recovered in propylene product
Eq(n10, 0.05*n7) # propylene recycle is 5% of outlet flow
soln = solve(mixer + reactor + separator + specs)
soln
Out[1]:
{X: 95.0000000000000,
 n1: 995.900900900901,
 n10: 4.750000000000000,
 n2: 4.750000000000000,
n3: 900.900900900901,
 n4: 99.7500000000000,
 n5: 95.0000000000000,
 n6: 5.00000000000000,
 n7: 95.0000000000000,
n8: 95.0000000000000,
n9: 895.900900900901}
```

#### **Product Composition**

```
In [2]:
```

```
nTotal = soln[n6] + soln[n7] + soln[n8]
print('C3H8 Product = ', round(100*soln[n6]/nTotal,2), '%')
print('C3H6 Product = ', round(100*soln[n7]/nTotal,2), '%')
print(' H2 Product = ', round(100*soln[n8]/nTotal,2), '%')

C3H8 Product = 2.56 %
C3H6 Product = 48.72 %
H2 Product = 48.72 %
```

## **Recycle Ratio**

```
In [3]:
```

```
print('Recycle Ratio = ', (soln[n9] + soln[n10])/nfeed)

Recycle Ratio = 9.00650900900901
```

## **Single Pass Conversion**

```
In [4]:
```

```
print('Single Pass Conversion', (soln[n1] - soln[n3])/soln[n1])
Single Pass Conversion 0.0953910172328011
In [ ]:
```