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**TABLE A-1** Atomic or Molecular Weights and Critical Properties of Selected Elements and Compounds

Substance	Chemical Formula	M (kg/kmol)	<i>T</i> <sub>c</sub> (K)	p <sub>c</sub> (bar)	$Z_{\rm c} = \frac{p_{\rm c}v_{\rm c}}{RT_{\rm c}}$
Acetylene	C <sub>2</sub> H <sub>2</sub>	26.04	309	62.8	0.274
Air (equivalent)	—	28.97	133	37.7	0.284
Ammonia	NH <sub>3</sub>	17.03	406	112.8	0.242
Argon	$\begin{array}{c} Ar \\ C_6H_6 \\ C_4H_{10} \end{array}$	39.94	151	48.6	0.290
Benzene		78.11	563	49.3	0.274
Butane		58.12	425	38.0	0.274
Carbon dioxide Carbon monoxide	$\begin{array}{c} {\sf C} \\ {\sf CO}_2 \\ {\sf CO} \end{array}$	12.01 44.01 28.01	304 133	73.9 35.0	 0.276 0.294
Copper Ethane Ethyl alcohol	$Cu$ $C_2H_6$ $C_2H_5OH$	63.54 30.07 46.07	305 516	 48.8 63.8	0.285 0.249
Ethylene	${ m C_2H_4}$	28.05	283	51.2	0.270
Helium	He	4.003	5.2	2.3	0.300
Hydrogen	${ m H_2}$	2.016	33.2	13.0	0.304
Methane	$\mathrm{CH_4} \ \mathrm{CH_3OH} \ \mathrm{N_2}$	16.04	191	46.4	0.290
Methyl alcohol		32.04	513	79.5	0.220
Nitrogen		28.01	126	33.9	0.291
Octane	$egin{array}{c} C_8H_{18} \ O_2 \ C_3H_8 \end{array}$	114.22	569	24.9	0.258
Oxygen		32.00	154	50.5	0.290
Propane		44.09	370	42.7	0.276
Propylene	C <sub>3</sub> H <sub>6</sub>	42.08	365	46.2	0.276
Refrigerant 12	CCl <sub>2</sub> F <sub>2</sub>	120.92	385	41.2	0.278
Refrigerant 22	CHClF <sub>2</sub>	86.48	369	49.8	0.267
Refrigerant 134a	CF <sub>3</sub> CH <sub>2</sub> F	102.03	374	40.7	0.260
Sulfur dioxide	SO <sub>2</sub>	64.06	431	78.7	0.268
Water	H <sub>2</sub> O	18.02	647.3	220.9	0.233

Sources: Adapted from International Critical Tables and L. C. Nelson and E. F. Obert, Generalized Compressibility Charts, Chem. Eng., 61: 203 (1954).

 TABLE A-2
 Properties of Saturated Water (Liquid–Vapor): Temperature Table

			c Volume	Internal kJ/			Enthalpy kJ/kg		Entı kJ/k	opy g·K	
Temp. °C	Press. bar	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{\rm g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor $u_{\rm g}$	Sat. Liquid $h_{\rm f}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid	Sat. Vapor	Temp.
.01	0.00611	1.0002	206.136	0.00	2375.3	0.01	2501.3	2501.4	0.0000	9.1562	.01
4	0.00813	1.0001	157.232	16.77	2380.9	16.78	2491.9	2508.7	0.0610	9.0514	4
5	0.00872	1.0001	147.120	20.97	2382.3	20.98	2489.6	2510.6	0.0761	9.0257	5
6	0.00935	1.0001	137.734	25.19	2383.6	25.20	2487.2	2512.4	0.0912	9.0003	6
8	0.01072	1.0002	120.917	33.59	2386.4	33.60	2482.5	2516.1	0.1212	8.9501	8
10	0.01228	1.0004	106.379	42.00	2389.2	42.01	2477.7	2519.8	0.1510	8.9008	10
11	0.01312	1.0004	99.857	46.20	2390.5	46.20	2475.4	2521.6	0.1658	8.8765	11
12	0.01402	1.0005	93.784	50.41	2391.9	50.41	2473.0	2523.4	0.1806	8.8524	12
13	0.01497	1.0007	88.124	54.60	2393.3	54.60	2470.7	2525.3	0.1953	8.8285	13
14	0.01598	1.0008	82.848	58.79	2394.7	58.80	2468.3	2527.1	0.2099	8.8048	14
15	0.01705	1.0009	77.926	62.99	2396.1	62.99	2465.9	2528.9	0.2245	8.7814	15
16	0.01818	1.0011	73.333	67.18	2397.4	67.19	2463.6	2530.8	0.2390	8.7582	16
17	0.01938	1.0012	69.044	71.38	2398.8	71.38	2461.2	2532.6	0.2535	8.7351	17
18	0.02064	1.0014	65.038	75.57	2400.2	75.58	2458.8	2534.4	0.2679	8.7123	18
19	0.02198	1.0016	61.293	79.76	2401.6	79.77	2456.5	2536.2	0.2823	8.6897	19
20	0.02339	1.0018	57.791	83.95	2402.9	83.96	2454.1	2538.1	0.2966	8.6672	20
21	0.02487	1.0020	54.514	88.14	2404.3	88.14	2451.8	2539.9	0.3109	8.6450	21
22	0.02645	1.0022	51.447	92.32	2405.7	92.33	2449.4	2541.7	0.3251	8.6229	22
23	0.02810	1.0024	48.574	96.51	2407.0	96.52	2447.0	2543.5	0.3393	8.6011	23
24	0.02985	1.0027	45.883	100.70	2408.4	100.70	2444.7	2545.4	0.3534	8.5794	24
25	0.03169	1.0029	43.360	104.88	2409.8	104.89	2442.3	2547.2	0.3674	8.5580	25
26	0.03363	1.0032	40.994	109.06	2411.1	109.07	2439.9	2549.0	0.3814	8.5367	26
27	0.03567	1.0035	38.774	113.25	2412.5	113.25	2437.6	2550.8	0.3954	8.5156	27
28	0.03782	1.0037	36.690	117.42	2413.9	117.43	2435.2	2552.6	0.4093	8.4946	28
29	0.04008	1.0040	34.733	121.60	2415.2	121.61	2432.8	2554.5	0.4231	8.4739	29
30	0.04246	1.0043	32.894	125.78	2416.6	125.79	2430.5	2556.3	0.4369	8.4533	30
31	0.04496	1.0046	31.165	129.96	2418.0	129.97	2428.1	2558.1	0.4507	8.4329	31
32	0.04759	1.0050	29.540	134.14	2419.3	134.15	2425.7	2559.9	0.4644	8.4127	32
33	0.05034	1.0053	28.011	138.32	2420.7	138.33	2423.4	2561.7	0.4781	8.3927	33
34	0.05324	1.0056	26.571	142.50	2422.0	142.50	2421.0	2563.5	0.4917	8.3728	34
35	0.05628	1.0060	25.216	146.67	2423.4	146.68	2418.6	2565.3	0.5053	8.3531	35
36	0.05947	1.0063	23.940	150.85	2424.7	150.86	2416.2	2567.1	0.5188	8.3336	36
38	0.06632	1.0071	21.602	159.20	2427.4	159.21	2411.5	2570.7	0.5458	8.2950	38
40	0.07384	1.0078	19.523	167.56	2430.1	167.57	2406.7	2574.3	0.5725	8.2570	40
45	0.09593	1.0099	15.258	188.44	2436.8	188.45	2394.8	2583.2	0.6387	8.1648	45

**TABLE A-2** (Continued)

			c Volume <sup>3</sup> /kg	Internal kJ/			Enthalpy kJ/kg		Enti kJ/k	ropy g·K	
Temp. °C	Press. bar	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{\rm g}$	Sat. Liquid $u_{\rm f}$	Sat. Vapor $u_{\rm g}$	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid $s_{\rm f}$	Sat. Vapor	Temp. °C
50	.1235	1.0121	12.032	209.32	2443.5	209.33	2382.7	2592.1	.7038	8.0763	50
55	.1576	1.0146	9.568	230.21	2450.1	230.23	2370.7	2600.9	.7679	7.9913	55
60	.1994	1.0172	7.671	251.11	2456.6	251.13	2358.5	2609.6	.8312	7.9096	60
65	.2503	1.0199	6.197	272.02	2463.1	272.06	2346.2	2618.3	.8935	7.8310	65
70	.3119	1.0228	5.042	292.95	2469.6	292.98	2333.8	2626.8	.9549	7.7553	70
75	.3858	1.0259	4.131	313.90	2475.9	313.93	2321.4	2635.3	1.0155	7.6824	75
80	.4739	1.0291	3.407	334.86	2482.2	334.91	2308.8	2643.7	1.0753	7.6122	80
85	.5783	1.0325	2.828	355.84	2488.4	355.90	2296.0	2651.9	1.1343	7.5445	85
90	.7014	1.0360	2.361	376.85	2494.5	376.92	2283.2	2660.1	1.1925	7.4791	90
95	.8455	1.0397	1.982	397.88	2500.6	397.96	2270.2	2668.1	1.2500	7.4159	95
100	1.014	1.0435	1.673	418.94	2506.5	419.04	2257.0	2676.1	1.3069	7.3549	100
110	1.433	1.0516	1.210	461.14	2518.1	461.30	2230.2	2691.5	1.4185	7.2387	110
120	1.985	1.0603	0.8919	503.50	2529.3	503.71	2202.6	2706.3	1.5276	7.1296	120
130	2.701	1.0697	0.6685	546.02	2539.9	546.31	2174.2	2720.5	1.6344	7.0269	130
140	3.613	1.0797	0.5089	588.74	2550.0	589.13	2144.7	2733.9	1.7391	6.9299	140
150	4.758	1.0905	0.3928	631.68	2559.5	632.20	2114.3	2746.5	1.8418	6.8379	150
160	6.178	1.1020	0.3071	674.86	2568.4	675.55	2082.6	2758.1	1.9427	6.7502	160
170	7.917	1.1143	0.2428	718.33	2576.5	719.21	2049.5	2768.7	2.0419	6.6663	170
180	10.02	1.1274	0.1941	762.09	2583.7	763.22	2015.0	2778.2	2.1396	6.5857	180
190	12.54	1.1414	0.1565	806.19	2590.0	807.62	1978.8	2786.4	2.2359	6.5079	190
200	15.54	1.1565	0.1274	850.65	2595.3	852.45	1940.7	2793.2	2.3309	6.4323	200
210	19.06	1.1726	0.1044	895.53	2599.5	897.76	1900.7	2798.5	2.4248	6.3585	210
220	23.18	1.1900	0.08619	940.87	2602.4	943.62	1858.5	2802.1	2.5178	6.2861	220
230	27.95	1.2088	0.07158	986.74	2603.9	990.12	1813.8	2804.0	2.6099	6.2146	230
240	33.44	1.2291	0.05976	1033.2	2604.0	1037.3	1766.5	2803.8	2.7015	6.1437	240
250	39.73	1.2512	0.05013	1080.4	2602.4	1085.4	1716.2	2801.5	2.7927	6.0730	250
260	46.88	1.2755	0.04221	1128.4	2599.0	1134.4	1662.5	2796.6	2.8838	6.0019	260
270	54.99	1.3023	0.03564	1177.4	2593.7	1184.5	1605.2	2789.7	2.9751	5.9301	270
280	64.12	1.3321	0.03017	1227.5	2586.1	1236.0	1543.6	2779.6	3.0668	5.8571	280
290	74.36	1.3656	0.02557	1278.9	2576.0	1289.1	1477.1	2766.2	3.1594	5.7821	290
300	85.81	1.4036	0.02167	1332.0	2563.0	1344.0	1404.9	2749.0	3.2534	5.7045	300
320	112.7	1.4988	0.01549	1444.6	2525.5	1461.5	1238.6	2700.1	3.4480	5.5362	320
340	145.9	1.6379	0.01080	1570.3	2464.6	1594.2	1027.9	2622.0	3.6594	5.3357	340
360	186.5	1.8925	0.006945	1725.2	2351.5	1760.5	720.5	2481.0	3.9147	5.0526	360
374.14	220.9	3.155	0.003155	2029.6	2029.6	2099.3	0	2099.3	4.4298	4.4298	374.14

Source: Tables A-2 through A-5 are extracted from J. H. Keenan, F. G. Keyes, P. G. Hill, and J. G. Moore, Steam Tables, Wiley, New York, 1969.

**TABLE A-3** Properties of Saturated Water (Liquid–Vapor): Pressure Table

			Volume /kg		Energy 'kg		Enthalpy kJ/kg		Entı kJ/k	ropy g·K	
D		Sat.	Sat.	Sat.	Sat.	Sat.	F.	Sat.	Sat.	Sat.	D.
Press. bar	Temp. °C	Liquid $v_{\rm f} \times 10^3$	$v_{ m g}$	Liquid $u_{\rm f}$	Vapor $u_{\rm g}$	Liquid $h_{ m f}$	Evap. $h_{\mathrm{fg}}$	Vapor $h_{\rm g}$	Liquid $s_{\rm f}$	Vapor $s_{\rm g}$	Press. bar
0.04	28.96	1.0040	34.800	121.45	2415.2	121.46	2432.9	2554.4	0.4226	8.4746	0.04
0.06	36.16	1.0064	23.739	151.53	2425.0	151.53	2415.9	2567.4	0.5210	8.3304	0.06
0.08	41.51	1.0084	18.103	173.87	2432.2	173.88	2403.1	2577.0	0.5926	8.2287	0.08
0.10	45.81	1.0102	14.674	191.82	2437.9	191.83	2392.8	2584.7	0.6493	8.1502	0.10
0.20	60.06	1.0172	7.649	251.38	2456.7	251.40	2358.3	2609.7	0.8320	7.9085	0.20
0.30	69.10	1.0223	5.229	289.20	2468.4	289.23	2336.1	2625.3	0.9439	7.7686	0.30
0.40	75.87	1.0265	3.993	317.53	2477.0	317.58	2319.2	2636.8	1.0259	7.6700	0.40
0.50 0.60	81.33 85.94	1.0300 1.0331	3.240 2.732	340.44 359.79	2483.9 2489.6	340.49 359.86	2305.4 2293.6	2645.9 2653.5	1.0910 1.1453	7.5939 7.5320	0.50 0.60
0.70	89.95	1.0360	2.365	376.63	2494.5	376.70	2283.3	2660.0	1.1919	7.4797	0.70
0.80	93.50	1.0380	2.087	391.58	2498.8	391.66	2274.1	2665.8	1.2329	7.4346	0.80
0.90	96.71	1.0410	1.869	405.06	2502.6	405.15	2265.7	2670.9	1.2695	7.3949	0.90
1.00	99.63	1.0432	1.694	417.36	2506.1	417.46	2258.0	2675.5	1.3026	7.3594	1.00
1.50	111.4	1.0528	1.159	466.94	2519.7	467.11	2226.5	2693.6	1.4336	7.2233	1.50
2.00	120.2	1.0605	0.8857	504.49	2529.5	504.70	2201.9	2706.7	1.5301	7.1271	2.00
2.50	127.4	1.0672	0.7187	535.10	2537.2	535.37	2181.5	2716.9	1.6072	7.0527	2.50
3.00	133.6	1.0732	0.6058	561.15	2543.6	561.47	2163.8	2725.3	1.6718	6.9919	3.00
3.50 4.00	138.9 143.6	1.0786 1.0836	0.5243 0.4625	583.95 604.31	2546.9 2553.6	584.33 604.74	2148.1 2133.8	2732.4 2738.6	1.7275 1.7766	6.9405 6.8959	3.50 4.00
4.50	147.9	1.0882	0.4140	622.25	2557.6	623.25	2120.7	2743.9	1.8207	6.8565	4.50
5.00	151.9	1.0926	0.3749	639.68	2561.2	640.23	2108.5	2748.7	1.8607	6.8212	5.00
6.00	158.9	1.1006	0.3157	669.90	2567.4	670.56	2086.3	2756.8	1.9312	6.7600	6.00
7.00	165.0	1.1080	0.2729	696.44	2572.5	697.22	2066.3	2763.5	1.9922	6.7080	7.00
8.00	170.4	1.1148	0.2404	720.22	2576.8	721.11	2048.0	2769.1	2.0462	6.6628	8.00
9.00	175.4	1.1212	0.2150	741.83	2580.5	742.83	2031.1	2773.9	2.0946	6.6226	9.00
10.0	179.9	1.1273	0.1944	761.68	2583.6	762.81	2015.3	2778.1	2.1387	6.5863	10.0
15.0	198.3	1.1539	0.1318	843.16	2594.5	844.84	1947.3	2792.2 2799.5	2.3150	6.4448	15.0
20.0 25.0	212.4 224.0	1.1767 1.1973	0.09963 0.07998	906.44 959.11	2600.3 2603.1	908.79 962.11	1890.7 1841.0	2/99.5	2.4474 2.5547	6.3409 6.2575	20.0 25.0
30.0	233.9	1.2165	0.06668	1004.8	2604.1	1008.4	1795.7	2804.2	2.6457	6.1869	30.0
35.0	242.6	1.2347	0.05707	1045.4	2603.7	1049.8	1753.7	2803.4	2.7253	6.1253	35.0
40.0	250.4	1.2522	0.04978	1082.3	2602.3	1087.3	1714.1	2801.4	2.7964	6.0701	40.0
45.0	257.5	1.2692	0.04406	1116.2	2600.1	1121.9	1676.4	2798.3	2.8610	6.0199	45.0
50.0	264.0	1.2859	0.03944	1147.8	2597.1	1154.2	1640.1	2794.3	2.9202	5.9734	50.0
60.0	275.6	1.3187	0.03244	1205.4	2589.7	1213.4	1571.0	2784.3	3.0267	5.8892	60.0
70.0	285.9	1.3513	0.02737	1257.6	2580.5	1267.0	1505.1	2772.1	3.1211	5.8133	70.0
80.0	295.1	1.3842	0.02352 0.02048	1305.6	2569.8 2557.8	1316.6	1441.3	2758.0	3.2068	5.7432 5.6772	80.0
90.0 100.	303.4 311.1	1.4178 1.4524	0.02048	1350.5 1393.0	2544.4	1363.3 1407.6	1378.9 1317.1	2742.1 2724.7	3.2858 3.3596	5.6141	90.0 100.
110.	318.2	1.4886	0.01599	1433.7	2529.8	1450.1	1255.5	2705.6	3.4295	5.5527	110.

**TABLE A-3** (Continued)

			Volume /kg		Energy /kg		Enthalpy kJ/kg		Entı kJ/k	opy g·K	
Press.	Temp. °C	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{ m g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor u <sub>g</sub>	Sat. Liquid h <sub>f</sub>	Evap. $h_{ m fg}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid s <sub>f</sub>	Sat. Vapor s <sub>g</sub>	Press.
120.	324.8	1.5267	0.01426	1473.0	2513.7	1491.3	1193.6	2684.9	3.4962	5.4924	120.
130.	330.9	1.5671	0.01278	1511.1	2496.1	1531.5	1130.7	2662.2	3.5606	5.4323	130.
140.	336.8	1.6107	0.01149	1548.6	2476.8	1571.1	1066.5	2637.6	3.6232	5.3717	140.
150.	342.2	1.6581	0.01034	1585.6	2455.5	1610.5	1000.0	2610.5	3.6848	5.3098	150.
160.	347.4	1.7107	0.009306	1622.7	2431.7	1650.1	930.6	2580.6	3.7461	5.2455	160.
170. 180.	352.4 357.1	1.7702 1.8397	0.008364 0.007489	1660.2 1698.9	2405.0 2374.3	1690.3 1732.0	856.9 777.1	2547.2 2509.1	3.8079 3.8715	5.1777 5.1044	170. 180.
180. 190.	361.5	1.9243	0.007489	1739.9	2374.3	1776.5	688.0	2464.5	3.9388	5.0228	190.
200.	365.8	2.036	0.005834	1785.6	2293.0	1826.3	583.4	2409.7	4.0139	4.9269	200.
220.9	374.1	3.155	0.003155	2029.6	2029.6	2099.3	0	2099.3	4.4298	4.4298	220.9

**TABLE A-4** Properties of Superheated Water Vapor

IABL	E A-4	rioperties	or Superii	eated water	vapoi				
<i>T</i> °C	v m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K		<i>v</i> m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K
		= 0.06 bar	= 0.006					r = 0.035	
		$(T_{\rm sat} =$	36.16°C)				$(T_{\rm sat} =$	72.69°C)	
Sat.	23.739	2425.0	2567.4	8.3304		4.526	2473.0	2631.4	7.7158
80	27.132	2487.3	2650.1	8.5804		4.625	2483.7	2645.6	7.7564
120	30.219	2544.7	2726.0	8.7840		5.163	2542.4	2723.1	7.9644
160	33.302	2602.7	2802.5	8.9693		5.696	2601.2	2800.6	8.1519
200	36.383	2661.4	2879.7	9.1398		6.228	2660.4	2878.4	8.3237
240	39.462	2721.0	2957.8	9.2982		6.758	2720.3	2956.8	8.4828
280	42.540	2781.5	3036.8	9.4464		7.287	2780.9	3036.0	8.6314
320	45.618	2843.0	3116.7	9.5859		7.815	2842.5	3116.1	8.7712
360	48.696	2905.5	3197.7	9.7180		8.344	2905.1	3197.1	8.9034
400	51.774	2969.0	3279.6	9.8435		8.872	2968.6	3279.2	9.0291
440	54.851	3033.5	3362.6	9.9633		9.400	3033.2	3362.2	9.1490
500	59.467	3132.3	3489.1	10.1336		10.192	3132.1	3488.8	9.3194
	p	= 0.70 ba	r = 0.07	MPa		р	= 1.0 ba	r = 0.10  N	<b>М</b> Ра
	•		89.95°C)					99.63°C)	
Sat.	2.365	2494.5	2660.0	7.4797		1.694	2506.1	2675.5	7.3594
100	2.434	2509.7	2680.0	7.5341		1.696	2506.7	2676.2	7.3614
120	2.571	2539.7	2719.6	7.6375		1.793	2537.3	2716.6	7.4668
160	2.841	2599.4	2798.2	7.8279		1.984	2597.8	2796.2	7.6597
200	3.108	2659.1	2876.7	8.0012		2.172	2658.1	2875.3	7.8343
240	3.374	2719.3	2955.5	8.1611		2.359	2718.5	2954.5	7.9949
280	3.640	2780.2	3035.0	8.3162		2.546	2779.6	3034.2	8.1445
320	3.905	2842.0	3115.3	8.4504		2.732	2841.5	3114.6	8.2849
360	4.170	2904.6	3196.5	8.5828		2.917	2904.2	3195.9	8.4175
400	4.434	2968.2	3278.6	8.7086		3.103	2967.9	3278.2	8.5435
440	4.698	3032.9	3361.8	8.8286		3.288	3032.6	3361.4	8.6636
500	5.095	3131.8	3488.5	8.9991		3.565	3131.6	3488.1	8.8342
	p	= 1.5 bar	r = 0.15  N	л Ра		р	= 3.0 ba	r = 0.30  N	м Ра
	1		111.37°C)					133.55°C)	
Sat.	1.159	2519.7	2693.6	7.2233		0.606	2543.6	2725.3	6.9919
120	1.188	2533.3	2711.4	7.2693					
160	1.317	2595.2	2792.8	7.4665		0.651	2587.1	2782.3	7.1276
200	1.444	2656.2	2872.9	7.6433		0.716	2650.7	2865.5	7.3115
240	1.570	2717.2	2952.7	7.8052		0.781	2713.1	2947.3	7.4774
280	1.695	2778.6	3032.8	7.9555		0.844	2775.4	3028.6	7.6299
320	1.819	2840.6	3113.5	8.0964		0.907	2838.1	3110.1	7.7722
360	1.943	2903.5	3195.0	8.2293		0.969	2901.4	3192.2	7.9061
400	2.067	2967.3	3277.4	8.3555		1.032	2965.6	3275.0	8.0330
440	2.191	3032.1	3360.7	8.4757		1.094	3030.6	3358.7	8.1538
500	2.376	3131.2	3487.6	8.6466		1.187	3130.0	3486.0	8.3251
600	2.685	3301.7	3704.3	8.9101		1.341	3300.8	3703.2	8.5892
					· ·				

**TABLE A-4** (Continued)

TABI	.E A-4	(Continued	1)					
T	v	и	h	S	v	и	h	S
°C	m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg · K	m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg · K
	р	= 5.0 bar	= 0.50  M	[Pa	р	= 7.0  bas	= 0.70  N	1Pa
	•		151.86°C)		•		164.97°C)	
Sat.	0.3749	2561.2	2748.7	6.8213	0.2729	2572.5	2763.5	6.7080
180	0.4045	2609.7	2812.0	6.9656	0.2847	2599.8	2799.1	6.7880
200	0.4249	2642.9	2855.4	7.0592	0.2999	2634.8	2844.8	6.8865
	0.4646		2939.9			2701.8		
240 280	0.4046	2707.6 2771.2	3022.9	7.2307 7.3865	0.3292 0.3574	2766.9	2932.2 3017.1	7.0641 7.2233
320	0.5416	2834.7	3105.6	7.5308	0.3852	2831.3	3100.9	7.2233
360	0.5796	2898.7	3188.4	7.6660	0.4126	2895.8	3184.7	7.5063
400 440	0.6173 0.6548	2963.2 3028.6	3271.9 3356.0	7.7938 7.9152	0.4397 0.4667	2960.9 3026.6	3268.7 3353.3	7.6350 7.7571
500	0.7109	3128.4	3483.9	8.0873	0.5070	3126.8	3481.7	7.9299
600	0.8041	3299.6	3701.7	8.3522	0.5738	3298.5	3700.2	8.1956
700	0.8969	3477.5	3925.9	8.5952	0.6403	3476.6	3924.8	8.4391
	p	= 10.0 ba	ar = 1.0 M	Pa		b = 15.0  b	ar = 1.5 N	1Pa
			179.91°C)				198.32°C)	
Sat.	0.1944	2583.6	2778.1	6.5865	0.1318	2594.5	2792.2	6.4448
200	0.2060	2621.9	2827.9	6.6940	0.1325	2598.1	2796.8	6.4546
240	0.2275	2692.9	2920.4	6.8817	0.1483	2676.9	2899.3	6.6628
280	0.2480	2760.2	3008.2	7.0465	0.1627	2748.6	2992.7	6.8381
320	0.2678	2826.1	3093.9	7.1962	0.1765	2817.1	3081.9	6.9938
360	0.2873	2891.6	3178.9	7.3349	0.1899	2884.4	3169.2	7.1363
400	0.3066	2957.3	3263.9	7.4651	0.2030	2951.3	3255.8	7.2690
440	0.3257	3023.6	3349.3	7.5883	0.2160	3018.5	3342.5	7.3940
500	0.3541	3124.4	3478.5	7.7622	0.2352	3120.3	3473.1	7.5698
540	0.3729	3192.6	3565.6	7.8720	0.2478	3189.1	3560.9	7.6805
600	0.4011	3296.8	3697.9	8.0290	0.2668	3293.9	3694.0	7.8385
640	0.4198	3367.4	3787.2	8.1290	0.2793	3364.8	3783.8	7.9391
	p	= 20.0 ba	ar = 2.0 M	Pa .	p	0 = 30.0  b	ar = 3.0 N	1Pa
	1		212.42°C)		1		233.90°C)	
Sat.	0.0996	2600.3	2799.5	6.3409	0.0667	2604.1	2804.2	6.1869
240	0.1085	2659.6	2876.5	6.4952	0.0682	2619.7	2824.3	6.2265
280	0.1200	2736.4	2976.4	6.6828	0.0771	2709.9	2941.3	6.4462
320	0.1308	2807.9	3069.5	6.8452	0.0850	2788.4	3043.4	6.6245
360	0.1411	2877.0	3159.3	6.9917	0.0923	2861.7	3138.7	6.7801
400	0.1512	2945.2	3247.6	7.1271	0.0994	2932.8	3230.9	6.9212
440	0.1611	3013.4	3335.5	7.2540	0.1062	3002.9	3321.5	7.0520
500	0.1757	3116.2	3467.6	7.4317	0.1162	3108.0	3456.5	7.2338
540	0.1853	3185.6	3556.1	7.5434	0.1227	3178.4	3546.6	7.3474
600	0.1996	3290.9	3690.1	7.7024	0.1324	3285.0	3682.3	7.5085
640	0.2091	3362.2	3780.4	7.8035	0.1321	3357.0	3773.5	7.6106
700	0.2232	3470.9	3917.4	7.9487	0.1484	3466.5	3911.7	7.7571
	-	1	1			l .		

 TABLE A-4 (Continued)

IADI	LE A-4 (	Continuea)	)					
<i>T</i>	v	u	<i>h</i>	s	<i>v</i>	u	<i>h</i>	s
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	kJ/kg	kJ/kg	kJ/kg · K
	р	t = 40  bar $(T_{\text{sat}} = 2)$	= 4.0 MI 250.4°C)	Pa	p		c = 6.0  M 275.64°C)	Pa
Sat.	0.04978	2602.3	2801.4	6.0701	0.03244	2589.7	2784.3	5.8892
280	0.05546	2680.0	2901.8	6.2568	0.03317	2605.2	2804.2	5.9252
320	0.06199	2767.4	3015.4	6.4553	0.03876	2720.0	2952.6	6.1846
360	0.06788	2845.7	3117.2	6.6215	0.04331	2811.2	3071.1	6.3782
400	0.07341	2919.9	3213.6	6.7690	0.04739	2892.9	3177.2	6.5408
440	0.07872	2992.2	3307.1	6.9041	0.05122	2970.0	3277.3	6.6853
500	0.08643	3099.5	3445.3	7.0901	0.05665	3082.2	3422.2	6.8803
540	0.09145	3171.1	3536.9	7.2056	0.06015	3156.1	3517.0	6.9999
600	0.09885	3279.1	3674.4	7.3688	0.06525	3266.9	3658.4	7.1677
640	0.1037	3351.8	3766.6	7.4720	0.06859	3341.0	3752.6	7.2731
700	0.1110	3462.1	3905.9	7.6198	0.07352	3453.1	3894.1	7.4234
740	0.1157	3536.6	3999.6	7.7141	0.07677	3528.3	3989.2	7.5190
		$t = 80 \text{ bar}$ $(T_{\text{sat}} = 2)$	= 8.0 MI 95.06°C)	Pa	<i>p</i>		r = 10.0  N 311.06°C)	⁄IPa
Sat.	0.02352	2569.8	2758.0	5.7432	0.01803	2544.4	2724.7	5.6141
320	0.02682	2662.7	2877.2	5.9489	0.01925	2588.8	2781.3	5.7103
360	0.03089	2772.7	3019.8	6.1819	0.02331	2729.1	2962.1	6.0060
400	0.03432	2863.8	3138.3	6.3634	0.02641	2832.4	3096.5	6.2120
440	0.03742	2946.7	3246.1	6.5190	0.02911	2922.1	3213.2	6.3805
480	0.04034	3025.7	3348.4	6.6586	0.03160	3005.4	3321.4	6.5282
520	0.04313	3102.7	3447.7	6.7871	0.03394	3085.6	3425.1	6.6622
560	0.04582	3178.7	3545.3	6.9072	0.03619	3164.1	3526.0	6.7864
600	0.04845	3254.4	3642.0	7.0206	0.03837	3241.7	3625.3	6.9029
640	0.05102	3330.1	3738.3	7.1283	0.04048	3318.9	3723.7	7.0131
700	0.05481	3443.9	3882.4	7.2812	0.04358	3434.7	3870.5	7.1687
740	0.05729	3520.4	3978.7	7.3782	0.04560	3512.1	3968.1	7.2670
	p	$= 120 \text{ bar}$ $(T_{\text{sat}} = 3)$	= 12.0 M 24.75°C)	IPa	<i>p</i>		r = 14.0  N336.75°C)	<b>Л</b> Ра
Sat.	0.01426	2513.7	2684.9	5.4924	0.01149	2476.8	2637.6	5.3717
360	0.01811	2678.4	2895.7	5.8361	0.01422	2617.4	2816.5	5.6602
400	0.02108	2798.3	3051.3	6.0747	0.01722	2760.9	3001.9	5.9448
440	0.02355	2896.1	3178.7	6.2586	0.01954	2868.6	3142.2	6.1474
480	0.02576	2984.4	3293.5	6.4154	0.02157	2962.5	3264.5	6.3143
520	0.02781	3068.0	3401.8	6.5555	0.02343	3049.8	3377.8	6.4610
560	0.02977	3149.0	3506.2	6.6840	0.02517	3133.6	3486.0	6.5941
600	0.03164	3228.7	3608.3	6.8037	0.02683	3215.4	3591.1	6.7172
640	0.03345	3307.5	3709.0	6.9164	0.02843	3296.0	3694.1	6.8326
700	0.03610	3425.2	3858.4	7.0749	0.03075	3415.7	3846.2	6.9939
740	0.03781	3503.7	3957.4	7.1746	0.03225	3495.2	3946.7	7.0952

TABI	LE A-4 (	Continued)	)						
<i>T</i> °C	v m³/kg	u kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K		v m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K
	p :	$= 160 \text{ bar}$ $(T_{\text{sat}} = 3$	= 16.0 M 47.44°C)	IPa		p		r = 18.0  N 357.06°C)	<b>Л</b> Ра
Sat. 360 400	0.00931 0.01105 0.01426	2431.7 2539.0 2719.4	2580.6 2715.8 2947.6	5.2455 5.4614 5.8175	(	0.00749 0.00809 0.01190	2374.3 2418.9 2672.8	2509.1 2564.5 2887.0	5.1044 5.1922 5.6887
440 480 520	0.01652 0.01842 0.02013	2839.4 2939.7 3031.1	3103.7 3234.4 3353.3	6.0429 6.2215 6.3752	(	0.01414 0.01596 0.01757	2808.2 2915.9 3011.8	3062.8 3203.2 3378.0	5.9428 6.1345 6.2960
560 600 640	0.02172 0.02323 0.02467	3117.8 3201.8 3284.2	3465.4 3573.5 3678.9	6.5132 6.6399 6.7580	(	0.01904 0.02042 0.02174	3101.7 3188.0 3272.3	3444.4 3555.6 3663.6	6.4392 6.5696 6.6905
700 740	0.02674 0.02808	3406.0 3486.7	3833.9 3935.9	6.9224 7.0251		0.02362	3396.3 3478.0	3821.5 3925.0	6.8580 6.9623
	<i>p</i> :	$= 200 \text{ bar}$ $(T_{\text{sat}} = 3)$	= 20.0 M 65.81°C)	IPa	-	p	= 240 bar	r = 24.0  N	ЛРа
Sat. 400 440	0.00583 0.00994 0.01222	2293.0 2619.3 2774.9	2409.7 2818.1 3019.4	4.9269 5.5540 5.8450		0.00673	2477.8 2700.6	2639.4 2923.4	5.2393 5.6506
480 520 560	0.01222     2774.9     3019.4     5       0.01399     2891.2     3170.8     6       0.01551     2992.0     3302.2     6       0.01689     3085.2     3423.0     6       0.01818     3174.0     3537.6     6       0.01940     3260.2     3648.1     6		6.0518 6.2218 6.3705	(	0.01100 0.01241 0.01366	2838.3 2950.5 3051.1	3102.3 3248.5 3379.0	5.8950 6.0842 6.2448	
600 640 700				6.5048 6.6286 6.7993	(	0.01481 0.01588 0.01739	3145.2 3235.5 3366.4	3500.7 3616.7 3783.8	6.3875 6.5174 6.6947
740 800	0.02224 0.02385	3469.3 3592.7	3914.1 4069.7	6.9052 7.0544		).01835 ).01974	3451.7 3578.0	3892.1 4051.6	6.8038 6.9567
	p	= 280 bar	= 28.0  M	IPa	-	p	= 320 bar	= 32.0  N	<b>1</b> Ра
400 440 480	0.00383 0.00712 0.00885	2223.5 2613.2 2780.8	2330.7 2812.6 3028.5	4.7494 5.4494 5.7446	(	0.00236 0.00544 0.00722	1980.4 2509.0 2718.1	2055.9 2683.0 2949.2	4.3239 5.2327 5.5968
520 560 600	0.01020 0.01136 0.01241	2906.8 3015.7 3115.6	3192.3 3333.7 3463.0	5.9566 6.1307 6.2823	(	0.00853 0.00963 0.01061	2860.7 2979.0 3085.3	3133.7 3287.2 3424.6	5.8357 6.0246 6.1858
640 700 740	0.01338 0.01473 0.01558	3210.3 3346.1 3433.9	3584.8 3758.4 3870.0	6.4187 6.6029 6.7153	(	0.01150 0.01273 0.01350	3184.5 3325.4 3415.9	3552.5 3732.8 3847.8	6.3290 6.5203 6.6361
800 900	0.01680 0.01873	3563.1 3774.3	4033.4 4298.8	6.8720 7.1084		0.01460	3548.0 3762.7	4015.1 4285.1	6.7966 7.0372

**TABLE A-5** Properties of Compressed Liquid Water

TABL	<b>.E A-5</b> P	roperties of	Compresse	d Liquid W	ater				
T	$v \times 10^3$	и	h	S		$v \times 10^3$	и	h	S
°C	m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg · K		m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg · K
		$p = 25 \text{ bar}$ $(T_{\text{sat}} = 2$	r = 2.5  MP 223.99°C)	a				r = 5.0 MP 263.99°C)	a
20	1.0006	83.80	86.30	.2961		.9995	83.65	88.65	.2956
40	1.0067	167.25	169.77	.5715		1.0056	166.95	171.97	.5705
80	1.0280	334.29	336.86	1.0737		1.0268	333.72	338.85	1.0720
100	1.0423	418.24	420.85	1.3050		1.0410	417.52	422.72	1.3030
140	1.0784	587.82	590.52	1.7369		1.0768	586.76	592.15	1.7343
180	1.1261	761.16	763.97	2.1375		1.1240	759.63	765.25	2.1341
200	1.1555	849.9	852.8	2.3294		1.1530	848.1	853.9	2.3255
220	1.1898	940.7	943.7	2.5174		1.1866	938.4	944.4	2.5128
Sat.	1.1973	959.1	962.1	2.5546		1.2859	1147.8	1154.2	2.9202
		p = 75  bar	r = 7.5  MP	a		1	p = 100  bar	r = 10.0 M	Pa
		$(T_{\rm sat}=2$	290.59°C)				$(T_{\rm sat} = 1)$	311.06°C)	
20	.9984	83.50	90.99	.2950		.9972	83.36	93.33	.2945
40	1.0045	166.64	174.18	.5696		1.0034	166.35	176.38	.5686
80	1.0256	333.15	340.84	1.0704		1.0245	332.59	342.83	1.0688
100	1.0397	416.81	424.62	1.3011		1.0385	416.12	426.50	1.2992
140	1.0752	585.72	593.78	1.7317		1.0737	584.68	595.42	1.7292
180	1.1219	758.13	766.55	2.1308		1.1199	756.65	767.84	2.1275
220	1.1835	936.2	945.1	2.5083		1.1805	934.1	945.9	2.5039
260	1.2696	1124.4	1134.0	2.8763		1.2645	1121.1	1133.7	2.8699
Sat.	1.3677	1282.0	1292.2	3.1649		1.4524	1393.0	1407.6	3.3596
		p = 150  bar		Pa			o = 200  bas	r = 20.0 M	Pa
		$(T_{\rm sat}=3)$	342.24°C)				$(T_{\rm sat} = 1)$	365.81°C)	
20	.9950	83.06	97.99	.2934		.9928	82.77	102.62	.2923
40	1.0013	165.76	180.78	.5666		.9992	165.17	185.16	.5646
80	1.0222	331.48	346.81	1.0656		1.0199	330.40	350.80	1.0624
100	1.0361	414.74	430.28	1.2955		1.0337	413.39	434.06	1.2917
140	1.0707	582.66	598.72	1.7242		1.0678	580.69	602.04	1.7193
180	1.1159	753.76	770.50	2.1210		1.1120	750.95	773.20	2.1147
220	1.1748	929.9	947.5	2.4953		1.1693	925.9	949.3	2.4870
260	1.2550	1114.6	1133.4	2.8576		1.2462	1108.6	1133.5	2.8459
300	1.3770	1316.6	1337.3	3.2260		1.3596	1306.1	1333.3	3.2071
Sat.	1.6581	1585.6	1610.5	3.6848		2.036	1785.6	1826.3	4.0139
		p = 250  ba	ar = 25 MP	a —		1	p = 300  bas	r = 30.0  M	Pa
20	.9907	82.47	107.24	.2911		.9886	82.17	111.84	.2899
40	.9971	164.60	189.52	.5626		.9951	164.04	193.89	.5607
100	1.0313	412.08	437.85	1.2881		1.0290	410.78	441.66	1.2844
200	1.1344	834.5	862.8	2.2961		1.1302	831.4	865.3	2.2893
300	1.3442	1296.6	1330.2	3.1900		1.3304	1287.9	1327.8	3.1741

 TABLE A-6
 Properties of Saturated Water (Solid-Vapor): Temperature Table

	in de la constant de			abor), roughous								
		Specific Volume m <sup>3</sup> /kg	Volume kg	In	Internal Energy kJ/kg			Enthalpy kJ/kg			Entropy kJ/kg·K	
Temp. °C	Pressure kPa	Sat. Solid $v_{\rm i} \times 10^3$	Sat. Vapor <i>v</i> g	Sat. Solid u <sub>i</sub>	Subl. u <sub>ig</sub>	Sat. Vapor ug	Sat. Solid h <sub>i</sub>	Subl. h <sub>ig</sub>	Sat. Vapor h <sub>g</sub>	Sat. Solid s <sub>i</sub>	Subl.	Sat. Vapor
.01	.6113	1.0908	206.1	-333.40	2708.7	2375.3	-333.40	2834.8	2501.4	-1.221	10.378	9.156
	.6108	1.0908	206.3	-333.43	2708.8	2375.3	-333.43	2834.8	2501.3	-1.221	10.378	9.157
	.5176	1.0904	241.7	-337.62	2710.2	2372.6	-337.62	2835.3	2497.7	-1.237	10.456	9.219
4 - 1 - 8 - 8 - 8 - 8 - 8 - 8 - 8 - 8 - 8	.4375	1.0901	283.8	-341.78	2711.6	2369.8	-341.78	2835.7	2494.0	-1.253	10.536	9.283
	.3689	1.0898	334.2	-345.91	2712.9	2367.0	-345.91	2836.2	2490.3	-1.268	10.616	9.348
	.3102	1.0894	394.4	-350.02	2714.2	2364.2	-350.02	2836.6	2486.6	-1.284	10.698	9.414
-10	.2602	1.0891	466.7	-354.09	2715.5	2361.4	-354.09	2837.0	2482.9	-1.299	10.781	9.481
-12	.2176	1.0888	553.7	-358.14	2716.8	2358.7	-358.14	2837.3	2479.2	-1.315	10.865	9.550
-14	.1815	1.0884	658.8	-362.15	2718.0	2355.9	-362.15	2837.6	2475.5	-1.331	10.950	9.619
-16	.1510	1.0881	786.0	-366.14	2719.2	2353.1	-366.14	2837.9	2471.8	-1.346	11.036	9.690
-18	.1252	1.0878	940.5	-370.10	2720.4	2350.3	-370.10	2838.2	2468.1	-1.362	11.123	9.762
-20	.1035	1.0874	1128.6	-374.03	2721.6	2347.5	-374.03	2838.4	2464.3	-1.377	11.212	9.835
-22	.0853	1.0871	1358.4	-377.93	2722.7	2344.7	-377.93	2838.6	2460.6	-1.393	11.302	9.909
-24	.0701	1.0868	1640.1	-381.80	2723.7	2342.0	-381.80	2838.7	2456.9	-1.408	11.394	9.985
-26	.0574	1.0864	1986.4	-385.64	2724.8	2339.2	-385.64	2838.9	2453.2	-1.424	11.486	10.062
-28	.0469	1.0861	2413.7	-389.45	2725.8	2336.4	-389.45	2839.0	2449.5	-1.439	11.580	10.141
-30	.0381	1.0858	2943	-393.23	2726.8	2333.6	-393.23	2839.0	2445.8	-1.455	11.676	10.221
-32	.0309	1.0854	3600	-396.98	2727.8	2330.8	-396.98	2839.1	2442.1	-1.471	11.773	10.303
-34	.0250	1.0851	4419	-400.71	2728.7	2328.0	-400.71	2839.1	2438.4	$\begin{array}{c} -1.486 \\ -1.501 \\ -1.517 \\ -1.532 \end{array}$	11.872	10.386
-36	.0201	1.0848	5444	-404.40	2729.6	2325.2	-404.40	2839.1	2434.7		11.972	10.470
-38	.0161	1.0844	6731	-408.06	2730.5	2322.4	-408.06	2839.0	2430.9		12.073	10.556
-40	.0129	1.0841	8354	-411.70	2731.3	2319.6	-411.70	2838.9	2427.2		12.176	10.644
,		,	,									

Source: J. H. Keenan, F. G. Keyes, P. G. Hill, and J. G. Moore, Steam Tables, Wiley, New York, 1978.

**TABLE A-7** Properties of Saturated Refrigerant 22 (Liquid–Vapor): Temperature Table

		Specific m <sup>3</sup> /		Internal kJ/			Enthalpy kJ/kg		Entro kJ/kg		
Temp. °C	Press.	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{\rm g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor $u_{\rm g}$	Sat. Liquid $h_{ m f}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid $s_{\rm f}$	Sat. Vapor	Temp.
-60	0.3749	0.6833	0.5370	-21.57	203.67	-21.55	245.35	223.81	-0.0964	1.0547	-60
-50	0.6451	0.6966	0.3239	-10.89	207.70	-10.85	239.44	228.60	-0.0474	1.0256	-50
-45	0.8290	0.7037	0.2564	-5.50	209.70	-5.44	236.39	230.95	-0.0235	1.0126	-45
-40	1.0522	0.7109	0.2052	-0.07	211.68	0.00	233.27	233.27	0.0000	1.0005	-40
-36	1.2627	0.7169	0.1730	4.29	213.25	4.38	230.71	235.09	0.0186	0.9914	-36
-32	1.5049	0.7231	0.1468	8.68	214.80	8.79	228.10	236.89	0.0369	0.9828	-32
-30	1.6389	0.7262	0.1355	10.88	215.58	11.00	226.77	237.78	0.0460	0.9787	-30
-28	1.7819	0.7294	0.1252	13.09	216.34	13.22	225.43	238.66	0.0551	0.9746	-28
-26	1.9345	0.7327	0.1159	15.31	217.11	15.45	224.08	239.53	0.0641	0.9707	-26
-22	2.2698	0.7393	0.0997	19.76	218.62	19.92	221.32	241.24	0.0819	0.9631	-22
-20	2.4534	0.7427	0.0926	21.99	219.37	22.17	219.91	242.09	0.0908	0.9595	-20
-18	2.6482	0.7462	0.0861	24.23	220.11	24.43	218.49	242.92	0.0996	0.9559	-18
-16	2.8547	0.7497	0.0802	26.48	220.85	26.69	217.05	243.74	0.1084	0.9525	-16
-14	3.0733	0.7533	0.0748	28.73	221.58	28.97	215.59	244.56	0.1171	0.9490	-14
-12	3.3044	0.7569	0.0698	31.00	222.30	31.25	214.11	245.36	0.1258	0.9457	-12
-10	3.5485	0.7606	0.0652	33.27	223.02	33.54	212.62	246.15	0.1345	0.9424	-10
-8	3.8062	0.7644	0.0610	35.54	223.73	35.83	211.10	246.93	0.1431	0.9392	$ \begin{array}{c c} -8 \\ -6 \\ -4 \\ -2 \\ 0 \end{array} $
-6	4.0777	0.7683	0.0571	37.83	224.43	38.14	209.56	247.70	0.1517	0.9361	
-4	4.3638	0.7722	0.0535	40.12	225.13	40.46	208.00	248.45	0.1602	0.9330	
-2	4.6647	0.7762	0.0501	42.42	225.82	42.78	206.41	249.20	0.1688	0.9300	
0	4.9811	0.7803	0.0470	44.73	226.50	45.12	204.81	249.92	0.1773	0.9271	
2	5.3133	0.7844	0.0442	47.04	227.17	47.46	203.18	250.64	0.1857	0.9241	2
4	5.6619	0.7887	0.0415	49.37	227.83	49.82	201.52	251.34	0.1941	0.9213	4
6	6.0275	0.7930	0.0391	51.71	228.48	52.18	199.84	252.03	0.2025	0.9184	6
8	6.4105	0.7974	0.0368	54.05	229.13	54.56	198.14	252.70	0.2109	0.9157	8
10	6.8113	0.8020	0.0346	56.40	229.76	56.95	196.40	253.35	0.2193	0.9129	10
12	7.2307	0.8066	0.0326	58.77	230.38	59.35	194.64	253.99	0.2276	0.9102	12
16	8.1268	0.8162	0.0291	63.53	231.59	64.19	191.02	255.21	0.2442	0.9048	16
20	9.1030	0.8263	0.0259	68.33	232.76	69.09	187.28	256.37	0.2607	0.8996	20
24	10.164	0.8369	0.0232	73.19	233.87	74.04	183.40	257.44	0.2772	0.8944	24
28	11.313	0.8480	0.0208	78.09	234.92	79.05	179.37	258.43	0.2936	0.8893	28
32	12.556	0.8599	0.0186	83.06	235.91	84.14	175.18	259.32	0.3101	0.8842	32
36	13.897	0.8724	0.0168	88.08	236.83	89.29	170.82	260.11	0.3265	0.8790	36
40	15.341	0.8858	0.0151	93.18	237.66	94.53	166.25	260.79	0.3429	0.8738	40
45	17.298	0.9039	0.0132	99.65	238.59	101.21	160.24	261.46	0.3635	0.8672	45
50	19.433	0.9238	0.0116	106.26	239.34	108.06	153.84	261.90	0.3842	0.8603	50
60	24.281	0.9705	0.0089	120.00	240.24	122.35	139.61	261.96	0.4264	0.8455	60

Source: Tables A-7 through A-9 are calculated based on equations from A. Kamei and S. W. Beyerlein, "A Fundamental Equation for Chlorodifluoromethane (R-22)," Fluid Phase Equilibria, Vol. 80, No. 11, 1992, pp. 71–86.

**TABLE A-8** Properties of Saturated Refrigerant 22 (Liquid–Vapor): Pressure Table

	Specific m <sup>3</sup> .			Internal kJ/			Enthalpy kJ/kg		Entro kJ/kg		
Press.	Temp. °C	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{ m g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor u <sub>g</sub>	Sat. Liquid $h_{ m f}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid s <sub>f</sub>	Sat. Vapor $s_{\rm g}$	Press.
0.40	-58.86	0.6847	0.5056	-20.36	204.13	-20.34	244.69	224.36	-0.0907	1.0512	0.40
0.50	-54.83	0.6901	0.4107	-16.07	205.76	-16.03	242.33	226.30	-0.0709	1.0391	0.50
0.60	-51.40	0.6947	0.3466	-12.39	207.14	-12.35	240.28	227.93	-0.0542	1.0294	0.60
0.70	-48.40	0.6989	0.3002	-9.17	208.34	-9.12	238.47	229.35	-0.0397	1.0213	0.70
0.80	-45.73	0.7026	0.2650	-6.28	209.41	-6.23	236.84	230.61	-0.0270	1.0144	0.80
0.90	-43.30	0.7061	0.2374	-3.66	210.37	-3.60	235.34	231.74	-0.0155	1.0084	0.90
1.00	-41.09	0.7093	0.2152	-1.26	211.25	-1.19	233.95	232.77	-0.0051	1.0031	1.00
1.25	-36.23	0.7166	0.1746	4.04	213.16	4.13	230.86	234.99	0.0175	0.9919	1.25
1.50	-32.08	0.7230	0.1472	8.60	214.77	8.70	228.15	236.86	0.0366	0.9830	1.50
1.75	-28.44	0.7287	0.1274	12.61	216.18	12.74	225.73	238.47	0.0531	0.9755	1.75
2.00	-25.18	0.7340	0.1123	16.22	217.42	16.37	223.52	239.88	0.0678	0.9691	2.00
2.25	-22.22	0.7389	0.1005	19.51	218.53	19.67	221.47	241.15	0.0809	0.9636	2.25
2.50	-19.51	0.7436	0.0910	22.54	219.55	22.72	219.57	242.29	0.0930	0.9586	2.50
2.75	-17.00	0.7479	0.0831	25.36	220.48	25.56	217.77	243.33	0.1040	0.9542	2.75
3.00	-14.66	0.7521	0.0765	27.99	221.34	28.22	216.07	244.29	0.1143	0.9502	3.00
3.25	-12.46	0.7561	0.0709	30.47	222.13	30.72	214.46	245.18	0.1238	0.9465	3.25
3.50	-10.39	0.7599	0.0661	32.82	222.88	33.09	212.91	246.00	0.1328	0.9431	3.50
3.75	-8.43	0.7636	0.0618	35.06	223.58	35.34	211.42	246.77	0.1413	0.9399	3.75
4.00	-6.56	0.7672	0.0581	37.18	224.24	37.49	209.99	247.48	0.1493	0.9370	4.00
4.25	-4.78	0.7706	0.0548	39.22	224.86	39.55	208.61	248.16	0.1569	0.9342	4.25
4.50	-3.08	0.7740	0.0519	41.17	225.45	41.52	207.27	248.80	0.1642	0.9316	4.50
4.75	-1.45	0.7773	0.0492	43.05	226.00	43.42	205.98	249.40	0.1711	0.9292	4.75
5.00	0.12	0.7805	0.0469	44.86	226.54	45.25	204.71	249.97	0.1777	0.9269	5.00
5.25	1.63	0.7836	0.0447	46.61	227.04	47.02	203.48	250.51	0.1841	0.9247	5.25
5.50	3.08	0.7867	0.0427	48.30	227.53	48.74	202.28	251.02	0.1903	0.9226	5.50
5.75	4.49	0.7897	0.0409	49.94	227.99	50.40	201.11	251.51	0.1962	0.9206	5.75
6.00	5.85	0.7927	0.0392	51.53	228.44	52.01	199.97	251.98	0.2019	0.9186	6.00
7.00	10.91	0.8041	0.0337	57.48	230.04	58.04	195.60	253.64	0.2231	0.9117	7.00
8.00	15.45	0.8149	0.0295	62.88	231.43	63.53	191.52	255.05	0.2419	0.9056	8.00
9.00	19.59	0.8252	0.0262	67.84	232.64	68.59	187.67	256.25	0.2591	0.9001	9.00
10.00	23.40	0.8352	0.0236	72.46	233.71	73.30	183.99	257.28	0.2748	0.8952	10.00
12.00	30.25	0.8546	0.0195	80.87	235.48	81.90	177.04	258.94	0.3029	0.8864	12.00
14.00	36.29	0.8734	0.0166	88.45	236.89	89.68	170.49	260.16	0.3277	0.8786	14.00
16.00	41.73	0.8919	0.0144	95.41	238.00	96.83	164.21	261.04	0.3500	0.8715	16.00
18.00	46.69	0.9104	0.0127	101.87	238.86	103.51	158.13	261.64	0.3705	0.8649	18.00
20.00	51.26	0.9291	0.0112	107.95	239.51	109.81	152.17	261.98	0.3895	0.8586	20.00
24.00	59.46	0.9677	0.0091	119.24	240.22	121.56	140.43	261.99	0.4241	0.8463	24.00

 TABLE A-9
 Properties of Superheated Refrigerant 22 Vapor

TABL	ABLE A-9 Properties of Superheated Refrigerant 22 Vapor								
T	v	и	h	S	v	и	h	S	
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	kJ/kg	kJ/kg	kJ/kg · K	
	p	$= 0.4 \text{ bar}$ $(T_{\text{sat}} = -$		Pa	p		r = 0.06  M -51.40°C)	<b>I</b> Pa	
Sat55	0.50559 0.51532	204.13 205.92	224.36 226.53	1.0512 1.0612	0.34656	207.14	227.93	1.0294	
-50	0.52787	208.26	229.38	1.0741	0.34895	207.80	228.74	1.0330	
-45 -40 -35	0.54037 0.55284 0.56526	210.63 213.02 215.43	232.24 235.13 238.05	1.0868 1.0993 1.1117	0.35747 0.36594 0.37437	210.20 212.62 215.06	231.65 234.58 237.52	1.0459 1.0586 1.0711	
-30 -25 -20	0.57766 0.59002 0.60236	217.88 220.35 222.85	240.99 243.95 246.95	1.1239 1.1360 1.1479	0.38277 0.39114 0.39948	217.53 220.02 222.54	240.49 243.49 246.51	1.0835 1.0956 1.1077	
-15 -10 -5 0	0.61468 0.62697 0.63925 0.65151	225.38 227.93 230.52 233.13	249.97 253.01 256.09 259.19	1.1597 1.1714 1.1830 1.1944	0.40779 0.41608 0.42436 0.43261	225.08 227.65 230.25 232.88	249.55 252.62 255.71 258.83	1.1196 1.1314 1.1430 1.1545	
	p	$= 0.8 \text{ bar}$ $(T_{\text{sat}} = -$	= 0.08  M -45.73°C)	Pa	<i>p</i>		v = 0.10  M $-41.09^{\circ}\text{C}$	¶Pa	
Sat45	0.26503 0.26597	209.41 209.76	230.61 231.04	1.0144 1.0163	0.21518	211.25	232.77	1.0031	
-40	0.27245	212.21	234.01	1.0292	0.21633	211.79	233.42	1.0059	
$-35 \\ -30$	0.27890 0.28530	214.68 217.17	236.99 239.99	1.0418 1.0543	0.22158 0.22679	214.29 216.80	236.44 239.48	1.0187 1.0313	
-25	0.29167	219.68	243.02	1.0666	0.23197	219.34	242.54	1.0438	
-20	0.29801	222.22	246.06	1.0788	0.23712	221.90	245.61	1.0560	
-15	0.30433	224.78	249.13	1.0908	0.24224	224.48	248.70	1.0681	
-10	0.31062	227.37	252.22	1.1026	0.24734	227.08	251.82	1.0801	
$-5 \\ 0$	0.31690 0.32315	229.98 232.62	255.34 258.47	1.1143 1.1259	0.25241 0.25747	229.71 232.36	254.95 258.11	1.0919 1.1035	
5	0.32313	232.02	261.64	1.1239	0.26251	232.30	261.29	1.1055	
10	0.33561	237.98	264.83	1.1488	0.26753	237.74	264.50	1.1265	
	p	$= 1.5 \text{ bar}$ $(T_{\text{sat}} = -$	= 0.15  M $-32.08^{\circ}\text{C}$	Pa	p		= 0.20  N $-25.18^{\circ}\text{C}$		
Sat30	0.14721 0.14872	214.77 215.85	236.86 238.16	0.9830 0.9883	0.11232	217.42	239.88	0.9691	
-25	0.15232	218.45	241.30	1.0011	0.11242	217.51	240.00	0.9696	
$-20 \\ -15$	0.15588	221.07	244.45	1.0137	0.11520	220.19	243.23	0.9825	
-13 $-10$	0.15941 0.16292	223.70 226.35	247.61 250.78	1.0260 1.0382	0.11795 0.12067	222.88 225.58	246.47 249.72	0.9952 1.0076	
<b>-5</b>	0.16640	229.02	253.98	1.0502	0.12336	228.30	252.97	1.0199	
0	0.16987	231.70	257.18	1.0621	0.12603	231.03	256.23	1.0310	
5	0.17331	234.42	260.41	1.0738	0.12868	233.78	259.51	1.0438	
10	0.17674	237.15	263.66	1.0854	0.13132	236.54	262.81	1.0555	
15	0.18015	239.91	266.93	1.0968	0.13393	239.33	266.12	1.0671	
20 25	0.18355 0.18693	242.69 245.49	270.22 273.53	1.1081 1.1193	0.13653 0.13912	242.14 244.97	269.44 272.79	1.0786 1.0899	
23		5		1.11/3	0.13712			1.00//	

**TABLE A-9** (Continued)

TABL	<b>.E A-9</b> ( <i>C</i>	ontinued)						
T	v	и	h	S	v	и	h	S
°C	m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	g kJ/kg	kJ/kg	kJ/kg · K
	p	= 2.5 bar	= 0.25  M	Pa		p = 3.0  bas	r = 0.30  N	<b>Л</b> Ра
		$(T_{\rm sat} = -$	-19.51°C)			$(T_{\rm sat} = $	-14.66°C)	
Sat.	0.09097	219.55	242.29	0.9586	0.0765	51 221.34	244.29	0.9502
-15	0.09303	222.03	245.29	0.9703				
-10	0.09528	224.79	248.61	0.9831	0.0783	33 223.96	247.46	0.9623
-5	0.09751	227.55	251.93	0.9956	0.0802	25 226.78	250.86	0.9751
0	0.09971	230.33	255.26	1.0078	0.0821		254.25	0.9876
5	0.10189	233.12	258.59	1.0199	0.0840	00   232.44	257.64	0.9999
10	0.10405	235.92	261.93	1.0318	0.0858		261.04	1.0120
15	0.10619	238.74	265.29	1.0436	0.0876		264.44	1.0239
20	0.10831	241.58	268.66	1.0552	0.0894	19 241.01	267.85	1.0357
25	0.11043	244.44	272.04	1.0666	0.0912		271.28	1.0472
30	0.11253	247.31	275.44	1.0779	0.0930		274.72	1.0587
35	0.11461	250.21	278.86	1.0891	0.0948		278.17	1.0700
40	0.11669	253.13	282.30	1.1002	0.0966	50 252.66	281.64	1.0811
	p		= 0.35  M	Pa		p = 4.0  bas		⁄IРа
		$(T_{\rm sat} = -$	-10.39°C)			$(T_{\rm sat} =$	-6.56°C)	
Sat.	0.06605	222.88	246.00	0.9431	0.0581	2 224.24	247.48	0.9370
-10	0.06619	223.10	246.27	0.9441				
-5	0.06789	225.99	249.75	0.9572	0.0586	50 225.16	248.60	0.9411
0	0.06956	228.86	253.21	0.9700	0.0601	1 228.09	252.14	0.9542
5	0.07121	231.74	256.67	0.9825	0.0616		225.66	0.9670
10	0.07284	234.63	260.12	0.9948	0.0630	06 233.95	259.18	0.9795
15	0.07444	237.52	263.57	1.0069	0.0645	50 236.89	262.69	0.9918
20	0.07603	240.42	267.03	1.0188	0.0659		266.19	1.0039
25	0.07760	243.34	270.50	1.0305	0.0673	33 242.77	269.71	1.0158
30	0.07916	246.27	273.97	1.0421	0.0687		273.22	1.0274
35	0.08070	249.22	227.46	1.0535	0.0701		276.75	1.0390
40	0.08224	252.18	280.97	1.0648	0.0714		280.28	1.0504
45	0.08376	255.17	284.48	1.0759	0.0728	32   254.70	283.83	1.0616
	p		= 0.45  M	Pa		p = 5.0  bar		<b>Л</b> Ра
		$(T_{\rm sat} = -$	-3.08°C)			$(T_{\rm sat} =$	0.12°C)	
Sat.	0.05189	225.45	248.80	0.9316	0.0468	36 226.54	249.97	0.9269
0	0.05275	227.29	251.03	0.9399				
5	0.05411	230.28	254.63	0.9529	0.0481	0 229.52	253.57	0.9399
10	0.05545	233.26	258.21	0.9657	0.0493		257.22	0.9530
15	0.05676	236.24	261.78	0.9782	0.0505		260.85	0.9657
20	0.05805	239.22	265.34	0.9904	0.0517		264.47	0.9781
25	0.05933	242.20	268.90	1.0025	0.0529		268.07	0.9903
30	0.06059	245.19	272.46	1.0143	0.0540		271.68	1.0023
35	0.06184	248.19	276.02	1.0259	0.0552		275.28	1.0141
40	0.06308	251.20	279.59	1.0374	0.0563		278.89	1.0257
45 50	0.06430	254.23	283.17	1.0488	0.0574		282.50	1.0371
50 55	0.06552 0.06672	257.28 260.34	286.76 290.36	1.0600 1.0710	0.0585 0.0596		286.12 289.75	1.0484 1.0595
33	0.00072	200.34	290.30	1.0/10	0.0390	233.30	209.13	1.0373

 TABLE A-9 (Continued)

TABL	<b>E A-9</b> (C	ontinued)						
T	υ	и	h	S	v	и	h	S
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	kJ/kg	kJ/kg	kJ/kg · K
	p		= 0.55  M $3.08^{\circ}\text{C}$	Pa	p		c = 0.60  M 5.85°C)	1Pa
Sat. 5	0.04271 0.04317	227.53 228.72	251.02 252.46	0.9226 0.9278	0.03923	228.44	251.98	0.9186
10	0.04317	231.81	256.20	0.9278	0.04015	231.05	255.14	0.9299
15	0.04547	234.89	259.90	0.9540	0.04122	234.18	258.91	0.9431
20 25	0.04658 0.04768	237.95 241.01	263.57 267.23	0.9667 0.9790	0.04227 0.04330	237.29 240.39	262.65 266.37	0.9560 0.9685
30	0.04708	244.07	270.88	0.9790	0.04330	243.49	270.07	0.9808
35	0.04982	247.13	274.53	1.0031	0.04530	246.58	273.76	0.9929
40	0.05086	250.20	278.17	1.0148	0.04628	249.68	277.45	1.0048
45 50	0.05190 0.05293	253.27 256.36	281.82 285.47	1.0264 1.0378	0.04724 0.04820	252.78 255.90	281.13 284.82	1.0164 1.0279
55	0.05293	259.46	289.13	1.0378	0.04820	259.02	288.51	1.0279
60	0.05495	262.58	292.80	1.0601	0.05008	262.15	292.20	1.0504
		7.01	0.70 M	D		0.0.1	0.00.1	TD.
	p		= 0.70  M $10.91^{\circ}\text{C}$	Pa	p		t = 0.80  M 15.45°C)	тРа
Sat.	0.03371	230.04	253.64	0.9117	0.02953	231.43	255.05	0.9056
15	0.03451	232.70	256.86	0.9229	0.02733	231.13	233.03	0.7030
20	0.03547	235.92	260.75	0.9363	0.03033	234.47	258.74	0.9182
25	0.03639	239.12	264.59	0.9493	0.03118	237.76	262.70	0.9315
30 35	0.03730 0.03819	242.29 245.46	268.40 272.19	0.9619 0.9743	0.03202 0.03283	241.04 244.28	266.66 270.54	0.9448 0.9574
40	0.03906	248.62	275.96	0.9865	0.03363	247.52	274.42	0.9700
45	0.03992	251.78	279.72	0.9984	0.03440	250.74	278.26	0.9821
50	0.04076	254.94	283.48	1.0101	0.03517	253.96	282.10	0.9941
55	0.04160	258.11	287.23	1.0216	0.03592	257.18	285.92	1.0058
60 65	0.04242 0.04324	261.29 264.48	290.99 294.75	1.0330 1.0442	0.03667 0.03741	260.40 263.64	289.74 293.56	1.0174 1.0287
70	0.04405	267.68	298.51	1.0552	0.03814	266.87	297.38	1.0400
	p		= 0.90 M 19.59°C)	Pa	p		r = 1.00  M 23.40°C)	MPa
Sat.	0.02623	232.64	256.25	0.9001	0.02358	233.71	257.28	0.8952
20 30	0.02630 0.02789	232.92 239.73	256.59 264.83	0.9013 0.9289	0.02457	238.34	262.91	0.9139
40	0.02939	246.37	272.82	0.9549	0.02598	245.18	271.17	0.9407
50	0.03082	252.95	280.68	0.9795	0.02732	251.90	279.22	0.9660
60	0.03219	259.49	288.46	1.0033	0.02860	258.56	287.15	0.9902
70	0.03353	266.04	296.21	1.0262	0.02984	265.19	295.03	1.0135
80 90	0.03483 0.03611	272.62 279.23	303.96 311.73	1.0484 1.0701	0.03104 0.03221	271.84 278.52	302.88 310.74	1.0361 1.0580
100	0.03736	285.90	319.53	1.0913	0.03337	285.24	318.61	1.0794
110	0.03860	292.63	327.37	1.1120	0.03450	292.02	326.52	1.1003
120	0.03982	299.42	335.26	1.1323	0.03562	298.85	334.46	1.1207
130	0.04103	306.28	343.21	1.1523	0.03672	305.74	342.46	1.1408
140 150	0.04223 0.04342	313.21 320.21	351.22 359.29	1.1719 1.1912	0.03781 0.03889	312.70 319.74	350.51 358.63	1.1605 1.1790

**TABLE A-9** (Continued)

	•	опиниеа)						
<i>T</i> °C	<i>v</i> m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K	<i>v</i> m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K
	<i>p</i> =		t = 1.20  M $30.25^{\circ}\text{C}$	1Pa	p		r = 1.40  M 36.29°C)	MPa
Sat.	0.01955	235.48	258.94	0.8864	0.01662	236.89	260.16	0.8786
40	0.02083	242.63	267.62	0.9146	0.01708	239.78	263.70	0.8900
50	0.02204	249.69	276.14	0.9413	0.01823	247.29	272.81	0.9186
60	0.02319	256.60	284.43	0.9666	0.01929	254.52	281.53	0.9452
70	0.02428	263.44	292.58	0.9907	0.02029	261.60	290.01	0.9703
80	0.02534	270.25	300.66	1.0139	0.02125	268.60	298.34	0.9942
90	0.02636	277.07	308.70	1.0363	0.02217	275.56	306.60	1.0172
100	0.02736	283.90	316.73	1.0582	0.02306	282.52	314.80	1.0395
110	0.02834	290.77	324.78	1.0794	0.02393	289.49	323.00	1.0612
120	0.02930	297.69	332.85	1.1002	0.02478	296.50	331.19	1.0823
130 140	0.03024 0.03118	304.65 311.68	340.95 349.09	1.1205 1.1405	0.02562 0.02644	303.55 310.64	339.41 347.65	1.1029 1.1231
150	0.03118	318.77		1.1403		317.79	355.94	1.1231
160	0.03210	325.92	357.29 365.54	1.1793	0.02725 0.02805	324.99	364.26	1.1429
170	0.03301	333.14	373.84	1.1793	0.02884	332.26	372.64	1.1024
170	0.03372	333.11	373.01	1.1703	0.02001	332.20	372.01	1.1015
		- 16 O hom	= 1.60  M	/Do		_ 10 0 ha	r = 1.80  N	MD <sub>o</sub>
	<i>p</i> =		41.73°C)	ТРа	<i>p</i> 		r = 1.80 r 46.69°C)	viPa
Sat.	0.01440	238.00	261.04	0.8715	0.01265	238.86	261.64	0.8649
50	0.01533	244.66	269.18	0.8971	0.01301	241.72	265.14	0.8758
60	0.01634	252.29	278.43	0.9252	0.01401	249.86	275.09	0.9061
70	0.01728	259.65	287.30	0.9515	0.01492	257.57	284.43	0.9337
80	0.01817	266.86	295.93	0.9762	0.01576	265.04	293.40	0.9595
90	0.01901	274.00	304.42	0.9999	0.01655	272.37	302.16	0.9839
100	0.01983	281.09	312.82	1.0228	0.01731	279.62	310.77	1.0073
110	0.02062	288.18	321.17	1.0448	0.01804	286.83	319.30	1.0299
120	0.02139	295.28	329.51	1.0663	0.01874	294.04	327.78	1.0517
130 140	0.02214	302.41	337.84 346.19	1.0872	0.01943	301.26 308.50	336.24	1.0730
150	0.02288 0.02361	309.58 316.79	354.56	1.1077 1.1277	0.02011 0.02077	315.78	344.70 353.17	1.0937 1.1139
160	0.02301	324.05	362.97	1.1473	0.02142	323.10	361.66	1.1133
170	0.02432	331.37	371.42	1.1473	0.02142	330.47	370.19	1.1538
170	0.02505	331.37	371.12	1.1000	0.02207	330.17	370.17	1.1332
		- 20.0 bar	= 2.00  N	/IDo	n	- 24 0 b	ar = 2.4  N	/IDo
	<i>p</i> -		= 2.00 N 51.26°C)	n a	<i>p</i>		59.46°C)	11 a
Sat.	0.01124	239.51	261.98	0.8586	0.00907	240.22	261.99	0.8463
60	0.01212	247.20	271.43	0.8873	0.00913	240.78	262.68	0.8484
70	0.01300	255.35	281.36	0.9167	0.01006	250.30	274.43	0.8831
80	0.01381	263.12	290.74	0.9436	0.01085	258.89	284.93	0.9133
90	0.01457	270.67	299.80	0.9689	0.01156	267.01	294.75	0.9407
100	0.01528	278.09	308.65	0.9929	0.01222	274.85	304.18	0.9663
110	0.01596	285.44	317.37	1.0160	0.01284	282.53	313.35	0.9906
120	0.01663	292.76	326.01	1.0383	0.01343	290.11	322.35	1.0137
130	0.01727	300.08	334.61	1.0598	0.01400	297.64	331.25	1.0361
140	0.01789	307.40	343.19	1.0808	0.01456	305.14	340.08	1.0577
150	0.01850	314.75	351.76	1.1013	0.01509	312.64	348.87	1.0787
160	0.01910	322.14	360.34	1.1214	0.01562	320.16	357.64	1.0992
170	0.01969	329.56	368.95	1.1410	0.01613	327.70	366.41	1.1192
180	0.02027	337.03	377.58	1.1603	0.01663	335.27	375.20	1.1388

**TABLE A-10** Properties of Saturated Refrigerant 134a (Liquid–Vapor): Temperature Table

		Specific m <sup>3</sup> /			Energy /kg		Enthalpy kJ/kg			ropy g·K	
Temp.	Press. bar	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{ m g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor u <sub>g</sub>	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor h <sub>g</sub>	Sat. Liquid $s_{\rm f}$	Sat. Vapor	Temp.
-40 -36 -32 -28 -26	0.5164 0.6332 0.7704 0.9305 1.0199	0.7055 0.7113 0.7172 0.7233 0.7265 0.7296	0.3569 0.2947 0.2451 0.2052 0.1882 0.1728	-0.04 4.68 9.47 14.31 16.75	204.45 206.73 209.01 211.29 212.43 213.57	0.00 4.73 9.52 14.37 16.82	222.88 220.67 218.37 216.01 214.80 213.57	222.88 225.40 227.90 230.38 231.62 232.85	0.0000 0.0201 0.0401 0.0600 0.0699	0.9560 0.9506 0.9456 0.9411 0.9390 0.9370	-40 -36 -32 -28 -26 -24
-22 -20 -18 -16	1.2192 1.3299 1.4483 1.5748	0.7328 0.7361 0.7395 0.7428	0.1590 0.1464 0.1350 0.1247 0.1068	21.68 24.17 26.67 29.18 34.25	214.70 215.84 216.97 218.10 220.36	21.77 24.26 26.77 29.30 34.39	212.32 211.05 209.76 208.45 205.77	234.08 235.31 236.53 237.74 240.15	0.0897 0.0996 0.1094 0.1192 0.1388	0.9351 0.9332 0.9315 0.9298	-22 -20 -18 -16
-8	2.1704	0.7569	0.0919	39.38	222.60	39.54	203.00	242.54	0.1583	0.9239	-8
-4	2.5274	0.7644	0.0794	44.56	224.84	44.75	200.15	244.90	0.1777	0.9213	-4
0	2.9282	0.7721	0.0689	49.79	227.06	50.02	197.21	247.23	0.1970	0.9190	0
4	3.3765	0.7801	0.0600	55.08	229.27	55.35	194.19	249.53	0.2162	0.9169	4
8	3.8756	0.7884	0.0525	60.43	231.46	60.73	191.07	251.80	0.2354	0.9150	8
12	4.4294	0.7971	0.0460	65.83	233.63	66.18	187.85	254.03	0.2545	0.9132	12
16	5.0416	0.8062	0.0405	71.29	235.78	71.69	184.52	256.22	0.2735	0.9116	16
20	5.7160	0.8157	0.0358	76.80	237.91	77.26	181.09	258.36	0.2924	0.9102	20
24	6.4566	0.8257	0.0317	82.37	240.01	82.90	177.55	260.45	0.3113	0.9089	24
26	6.8530	0.8309	0.0298	85.18	241.05	85.75	175.73	261.48	0.3208	0.9082	26
28	7.2675	0.8362	0.0281	88.00	242.08	88.61	173.89	262.50	0.3302	0.9076	28
30	7.7006	0.8417	0.0265	90.84	243.10	91.49	172.00	263.50	0.3396	0.9070	30
32	8.1528	0.8473	0.0250	93.70	244.12	94.39	170.09	264.48	0.3490	0.9064	32
34	8.6247	0.8530	0.0236	96.58	245.12	97.31	168.14	265.45	0.3584	0.9058	34
36	9.1168	0.8590	0.0223	99.47	246.11	100.25	166.15	266.40	0.3678	0.9053	36
38	9.6298	0.8651	0.0210	102.38	247.09	103.21	164.12	267.33	0.3772	0.9047	38
40	10.164	0.8714	0.0199	105.30	248.06	106.19	162.05	268.24	0.3866	0.9041	40
42	10.720	0.8780	0.0188	108.25	249.02	109.19	159.94	269.14	0.3960	0.9035	42
44	11.299	0.8847	0.0177	111.22	249.96	112.22	157.79	270.01	0.4054	0.9030	44
48	12.526	0.8989	0.0159	117.22	251.79	118.35	153.33	271.68	0.4243	0.9017	48
52	13.851	0.9142	0.0142	123.31	253.55	124.58	148.66	273.24	0.4432	0.9004	52
56	15.278	0.9308	0.0127	129.51	255.23	130.93	143.75	274.68	0.4622	0.8990	56
60	16.813	0.9488	0.0114	135.82	256.81	137.42	138.57	275.99	0.4814	0.8973	60
70	21.162	1.0027	0.0086	152.22	260.15	154.34	124.08	278.43	0.5302	0.8918	70
80	26.324	1.0766	0.0064	169.88	262.14	172.71	106.41	279.12	0.5814	0.8827	80
90	32.435	1.1949	0.0046	189.82	261.34	193.69	82.63	276.32	0.6380	0.8655	90
100	39.742	1.5443	0.0027	218.60	248.49	224.74	34.40	259.13	0.7196	0.8117	100

Source: Tables A-10 through A-12 are calculated based on equations from D. P. Wilson and R. S. Basu, "Thermodynamic Properties of a New Stratospherically Safe Working Fluid—Refrigerant 134a," ASHRAE Trans., Vol. 94, Pt. 2, 1988, pp. 2095–2118.

**TABLE A-11** Properties of Saturated Refrigerant 134a (Liquid–Vapor): Pressure Table

		Specific V m <sup>3</sup> /k			Energy /kg		Enthalpy kJ/kg			ropy g·K	
Press.	Temp. °C	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{\rm g}$	Sat. Liquid $u_{\rm f}$	Sat. Vapor $u_{\rm g}$	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\mathrm{g}}$	Sat. Liquid s <sub>f</sub>	Sat. Vapor	Press.
0.6	-37.07	0.7097	0.3100	3.41	206.12	3.46	221.27	224.72	0.0147	0.9520	0.6
0.8	-31.21	0.7184	0.2366	10.41	209.46	10.47	217.92	228.39	0.0440	0.9447	0.8
1.0	-26.43	0.7258	0.1917	16.22	212.18	16.29	215.06	231.35	0.0678	0.9395	1.0
1.2	-22.36	0.7323	0.1614	21.23	214.50	21.32	212.54	233.86	0.0879	0.9354	1.2
1.4	-18.80	0.7381	0.1395	25.66	216.52	25.77	210.27	236.04	0.1055	0.9322	1.4
1.6	-15.62	0.7435	0.1229	29.66	218.32	29.78	208.19	237.97	0.1211	0.9295	1.6
1.8	-12.73	0.7485	0.1098	33.31	219.94	33.45	206.26	239.71	0.1352	0.9273	1.8
2.0	-10.09	0.7532	0.0993	36.69	221.43	36.84	204.46	241.30	0.1481	0.9253	2.0
2.4	-5.37	0.7618	0.0834	42.77	224.07	42.95	201.14	244.09	0.1710	0.9222	2.4
2.8	-1.23	0.7697	0.0719	48.18	226.38	48.39	198.13	246.52	0.1911	0.9197	2.8
3.2	2.48	0.7770	0.0632	53.06	228.43	53.31	195.35	248.66	0.2089	0.9177	3.2
3.6	5.84	0.7839	0.0564	57.54	230.28	57.82	192.76	250.58	0.2251	0.9160	3.6
4.0	8.93	0.7904	0.0509	61.69	231.97	62.00	190.32	252.32	0.2399	0.9145	4.0
5.0	15.74	0.8056	0.0409	70.93	235.64	71.33	184.74	256.07	0.2723	0.9117	5.0
6.0	21.58	0.8196	0.0341	78.99	238.74	79.48	179.71	259.19	0.2999	0.9097	6.0
7.0	26.72	0.8328	0.0292	86.19	241.42	86.78	175.07	261.85	0.3242	0.9080	7.0
8.0	31.33	0.8454	0.0255	92.75	243.78	93.42	170.73	264.15	0.3459	0.9066	8.0
9.0	35.53	0.8576	0.0226	98.79	245.88	99.56	166.62	266.18	0.3656	0.9054	9.0
10.0	39.39	0.8695	0.0202	104.42	247.77	105.29	162.68	267.97	0.3838	0.9043	10.0
12.0	46.32	0.8928	0.0166	114.69	251.03	115.76	155.23	270.99	0.4164	0.9023	12.0
14.0	52.43	0.9159	0.0140	123.98	253.74	125.26	148.14	273.40	0.4453	0.9003	14.0
16.0	57.92	0.9392	0.0121	132.52	256.00	134.02	141.31	275.33	0.4714	0.8982	16.0
18.0	62.91	0.9631	0.0105	140.49	257.88	142.22	134.60	276.83	0.4954	0.8959	18.0
20.0	67.49	0.9878	0.0093	148.02	259.41	149.99	127.95	277.94	0.5178	0.8934	20.0
25.0	77.59	1.0562	0.0069	165.48	261.84	168.12	111.06	279.17	0.5687	0.8854	25.0
30.0	86.22	1.1416	0.0053	181.88	262.16	185.30	92.71	278.01	0.6156	0.8735	30.0

**TABLE A-12** Properties of Superheated Refrigerant 134a Vapor

TABL	E A-12	roperties (	of Superhe	eated Refrig	gerant 134a	Vapor			
<i>T</i>	v	и	<i>h</i>	s		v	и	<i>h</i>	s
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K		m³/kg	kJ/kg	kJ/kg	kJ/kg · K
		0.6  bar = 0.6  bar = 0.6  bar		<b>'</b> a			$1.0 \text{ bar} = T_{\text{sat}} = -26$	0.10 MPa 5.43°C)	
Sat20 -10	0.31003 0.33536 0.34992	206.12 217.86 224.97	224.72 237.98 245.96	0.9520 1.0062 1.0371		0.19170 0.19770 0.20686	212.18 216.77 224.01	231.35 236.54 244.70	0.9395 0.9602 0.9918
0	0.36433	232.24	254.10	1.0675		0.21587	231.41	252.99	1.0227
10	0.37861	239.69	262.41	1.0973		0.22473	238.96	261.43	1.0531
20	0.39279	247.32	270.89	1.1267		0.23349	246.67	270.02	1.0829
30	0.40688	255.12	279.53	1.1557		0.24216	254.54	278.76	1.1122
40	0.42091	263.10	288.35	1.1844		0.25076	262.58	287.66	1.1411
50	0.43487	271.25	297.34	1.2126		0.25930	270.79	296.72	1.1696
60	0.44879	279.58	306.51	1.2405		0.26779	279.16	305.94	1.1977
70	0.46266	288.08	315.84	1.2681		0.27623	287.70	315.32	1.2254
80	0.47650	296.75	325.34	1.2954		0.28464	296.40	324.87	1.2528
90	0.49031	305.58	335.00	1.3224		0.29302	305.27	334.57	1.2799
		: 1.4 bar =		<b>'</b> a		p =	1.8 bar =	0.18 MPa	
<b>G</b> .		$T_{\text{sat}} = -1$		0.0222			$T_{\text{sat}} = -12$		0.0252
Sat.	0.13945	216.52	236.04	0.9322		0.10983	219.94	239.71	0.9273
-10	0.14549	223.03	243.40	0.9606		0.11135	222.02	242.06	0.9362
0	0.15219	230.55	251.86	0.9922		0.11678	229.67	250.69	0.9684
10	0.15875	238.21	260.43	1.0230		0.12207	237.44	259.41	0.9998
20	0.16520	246.01	269.13	1.0532		0.12723	245.33	268.23	1.0304
30	0.17155	253.96	277.97	1.0828		0.13230	253.36	277.17	1.0604
40	0.17783	262.06	286.96	1.1120		0.13730	261.53	286.24	1.0898
50	0.18404	270.32	296.09	1.1407		0.14222	269.85	295.45	1.1187
60	0.19020	278.74	305.37	1.1690		0.14710	278.31	304.79	1.1472
70	0.19633	287.32	314.80	1.1969		0.15193	286.93	314.28	1.1753
80	0.20241	296.06	324.39	1.2244		0.15672	295.71	323.92	1.2030
90	0.20846	304.95	334.14	1.2516		0.16148	304.63	333.70	1.2303
100	0.21449	314.01	344.04	1.2785		0.16622	313.72	343.63	1.2573
		$2.0 \text{ bar} = (T_{\text{sat}} = -1)$		Pa			$2.4 \text{ bar} = T_{\text{sat}} = -5$	0.24 MPa .37°C)	
Sat10 0	0.09933 0.09938 0.10438	221.43 221.50 229.23	241.30 241.38 250.10	0.9253 0.9256 0.9582		0.08343	224.07 228.31	244.09 248.89	0.9222 0.9399
10	0.10922	237.05	258.89	0.9898		0.08993	236.26	257.84	0.9721
20	0.11394	244.99	267.78	1.0206		0.09399	244.30	266.85	1.0034
30	0.11856	253.06	276.77	1.0508		0.09794	252.45	275.95	1.0339
40	0.12311	261.26	285.88	1.0804		0.10181	260.72	285.16	1.0637
50	0.12758	269.61	295.12	1.1094		0.10562	269.12	294.47	1.0930
60	0.13201	278.10	304.50	1.1380		0.10937	277.67	303.91	1.1218
70	0.13639	286.74	314.02	1.1661		0.11307	286.35	313.49	1.1501
80	0.14073	295.53	323.68	1.1939		0.11674	295.18	323.19	1.1780
90	0.14504	304.47	333.48	1.2212		0.12037	304.15	333.04	1.2055
100	0.14932	313.57	343.43	1.2483		0.12398	313.27	343.03	1.2326

**TABLE A-12** (Continued)

IABL	E A-12 (	Continuea	!)					
<i>T</i> °C	v m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg⋅K	v m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K
	<i>p</i> =	$= 2.8 \text{ bar} = $ $(T_{\text{sat}} = -$		'a	<i>p</i> =	$3.2 \text{ bar} = (T_{\text{sat}} = 2.4)$	0.32 MPa 48°C)	
Sat.	0.07193 0.07240	226.38 227.37	246.52 247.64	0.9197 0.9238	0.06322	228.43	248.66	0.9177
10	0.07240	235.44	256.76	0.9566	0.06576	234.61	255.65	0.9427
20 30	0.07972 0.08320	243.59 251.83	265.91 275.12	0.9883 1.0192	0.06901 0.07214	242.87 251.19	264.95 274.28	0.9749 1.0062
40	0.08520	260.17	284.42	1.0494	0.07518	259.61	283.67	1.0367
50 60	0.08992 0.09319	268.64 277.23	293.81 303.32	1.0789 1.1079	0.07815 0.08106	268.14 276.79	293.15 302.72	1.0665 1.0957
70	0.09519	285.96	312.95	1.1364	0.08100	285.56	312.41	1.1243
80 90	0.09960 0.10275	294.82 303.83	322.71 332.60	1.1644 1.1920	0.08674 0.08953	294.46 303.50	322.22 332.15	1.1525 1.1802
100	0.10273	312.98	342.62	1.1920	0.08933	312.68	342.21	1.1802
110 120	0.10897 0.11205	322.27 331.71	352.78 363.08	1.2461 1.2727	0.09503 0.09774	322.00 331.45	352.40 362.73	1.2345 1.2611
		,	,	<u> </u>				
	p =	$4.0 \text{ bar} = (T_{\text{sat}} = 8)$		Pa .		$5.0 \text{ bar} = (T_{\text{sat}} = 15.$	0.50 MPa 74°C)	
Sat.	0.05089 0.05119	231.97 232.87	252.32 253.35	0.9145 0.9182	0.04086	235.64	256.07	0.9117
20	0.05397	241.37	262.96	0.9515	0.04188	239.40	260.34	0.9264
30 40	0.05662 0.05917	249.89 258.47	272.54 282.14	0.9837 1.0148	0.04416 0.04633	248.20 256.99	270.28 280.16	0.9597 0.9918
50	0.06164	267.13	291.79	1.0452	0.04842	265.83	290.04	1.0229
60 70	0.06405 0.06641	275.89 284.75	301.51 311.32	1.0748 1.1038	0.05043 0.05240	274.73 283.72	299.95 309.92	1.0531 1.0825
80	0.06873	293.73	321.23	1.1322	0.05432	292.80	319.96	1.1114
90 100	0.07102 0.07327	302.84 312.07	331.25 341.38	1.1602 1.1878	0.05620 0.05805	302.00 311.31	330.10 340.33	1.1397 1.1675
110	0.07550	321.44	351.64	1.2149	0.05988	320.74	350.68	1.1949
120	0.07771 0.07991	330.94	362.03	1.2417	0.06168	330.30	361.14	1.2218
130 140	0.07991	340.58 350.35	372.54 383.18	1.2681 1.2941	0.06347 0.06524	339.98 349.79	371.72 382.42	1.2484 1.2746
	<i>p</i> =	$6.0 \text{ bar} = (T_{\text{sat}} = 2)$	= 0.60 MF 1.58°C)	a		$7.0 \text{ bar} = T_{\text{sat}} = 26.$	0.70 MPa 72°C)	
Sat.	0.03408	238.74	259.19	0.9097	0.02918	241.42	261.85	0.9080
30 40	0.03581 0.03774	246.41 255.45	267.89 278.09	0.9388 0.9719	0.02979 0.03157	244.51 253.83	265.37 275.93	0.9197 0.9539
50	0.03958	264.48	288.23	1.0037	0.03324	263.08	286.35	0.9867
60 70	0.04134 0.04304	273.54 282.66	298.35 308.48	1.0346 1.0645	0.03482 0.03634	272.31 281.57	296.69 307.01	1.0182 1.0487
80	0.04469	291.86	318.67	1.0938	0.03781	290.88	317.35	1.0784
90 100	0.04631 0.04790	301.14 310.53	328.93 339.27	1.1225 1.1505	0.03924 0.04064	300.27 309.74	327.74 338.19	1.1074 1.1358
110	0.04946	320.03	349.70	1.1781	0.04201	319.31	348.71	1.1637
120 130	0.05099 0.05251	329.64 339.38	360.24 370.88	1.2053 1.2320	0.04335 0.04468	328.98 338.76	359.33 370.04	1.1910 1.2179
140	0.05402	349.23	381.64	1.2584	0.04599	348.66	380.86	1.2444
150 160	0.05550 0.05698	359.21 369.32	392.52 403.51	1.2844 1.3100	0.04729 0.04857	358.68 368.82	391.79 402.82	1.2706 1.2963
		•	•					

 TABLE A-12 (Continued)

IABL	E A-12 (	Continuea	:)					
<i>T</i> °C	v m³/kg	<i>u</i>	h	S 1-1/1 · W	<i>U</i> 3 <i>n</i>	<i>u</i>	h	S 1-1/1
		kJ/kg	kJ/kg	kJ/kg·K	m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg · K
	<i>p</i> =	$8.0 \text{ bar} = (T_{\text{sat}} = 3)$		'a		9.0 bar = $(T_{\text{sat}} = 35)$	0.90 MPa .53°C)	
Sat.	0.02547	243.78	264.15	0.9066	0.02255	245.88	266.18	0.9054
40 50	0.02691 0.02846	252.13 261.62	273.66 284.39	0.9374 0.9711	0.02325 0.02472	250.32 260.09	271.25 282.34	0.9217 0.9566
60	0.02992	271.04	294.98	1.0034	0.02472	269.72	293.21	0.9897
70	0.02332	280.45	305.50	1.0345	0.02738	279.30	303.94	1.0214
80	0.03264	289.89	316.00	1.0647	0.02861	288.87	314.62	1.0521
90	0.03393	299.37	326.52	1.0940	0.02980	298.46	325.28	1.0819
100	0.03519	308.93	337.08	1.1227	0.03095	308.11	335.96	1.1109
110	0.03642	318.57	347.71	1.1508	0.03207	317.82	346.68	1.1392
120 130	0.03762 0.03881	328.31 338.14	358.40 369.19	1.1784 1.2055	0.03316 0.03423	327.62 337.52	357.47 368.33	1.1670 1.1943
140	0.03997	348.09	380.07	1.2321	0.03529	347.51	379.27	1.2211
150	0.04113	358.15	391.05	1.2584	0.03633	357.61	390.31	1.2475
160	0.04227	368.32	402.14	1.2843	0.03736	367.82	401.44	1.2735
170	0.04340	378.61	413.33	1.3098	0.03838	378.14	412.68	1.2992
180	0.04452	389.02	424.63	1.3351	0.03939	388.57	424.02	1.3245
		10.0 bar	= 1.00 M	Pa			1.20 MP	a
		$(T_{\rm sat} = 39)$	9.39°C)			$T_{\rm sat} = 46$	.32°C)	
Sat. 40	0.02020 0.02029	247.77 248.39	267.97 268.68	0.9043 0.9066	0.01663	251.03	270.99	0.9023
50	0.02171	258.48	280.19	0.9428	0.01712	254.98	275.52	0.9164
60	0.02301	268.35	291.36	0.9768	0.01835	265.42	287.44	0.9527
70 80	0.02423 0.02538	278.11 287.82	302.34 313.20	1.0093 1.0405	0.01947 0.02051	275.59 285.62	298.96 310.24	0.9868 1.0192
90	0.02538	297.53	324.01	1.0707	0.02051	295.59	321.39	1.0503
100	0.02755	307.27	334.82	1.1000	0.02244	305.54	332.47	1.0804
110	0.02858	317.06	345.65	1.1286	0.02335	315.50	343.52	1.1096
120	0.02959	326.93	356.52	1.1567	0.02423	325.51	354.58	1.1381
130 140	0.03058 0.03154	336.88 346.92	367.46 378.46	1.1841 1.2111	0.02508 0.02592	335.58 345.73	365.68 376.83	1.1660 1.1933
150	0.03154	357.06	389.56	1.2111	0.02592	355.95	388.04	1.1933
160	0.03230	367.31	400.74	1.2638	0.02754	366.27	399.33	1.2465
170	0.03436	377.66	412.02	1.2895	0.02834	376.69	410.70	1.2724
180	0.03528	388.12	423.40	1.3149	0.02912	387.21	422.16	1.2980
		14.0 bar	= 1.40 M		n = 1	16 0 bar =	1.60 MP	a
		$(T_{\rm sat} = 52)$	2.43°C)			$T_{\rm sat} = 57$	.92°C)	
Sat.	0.01405	253.74	273.40	0.9003	0.01208	256.00	275.33	0.8982
60 70	0.01495 0.01603	262.17 272.87	283.10 295.31	0.9297 0.9658	0.01233 0.01340	258.48 269.89	278.20 291.33	0.9069 0.9457
80	0.01701	283.29	307.10	0.9997	0.01340	280.78	303.74	0.9437
90	0.01792	293.55	318.63	1.0319	0.01521	291.39	315.72	1.0148
100	0.01878	303.73	330.02	1.0628	0.01601	301.84	327.46	1.0467
110	0.01960	313.88	341.32	1.0927	0.01677	312.20	339.04	1.0773
120 130	0.02039 0.02115	324.05 334.25	352.59 363.86	1.1218 1.1501	0.01750 0.01820	322.53 332.87	350.53 361.99	1.1069 1.1357
140	0.02189	344.50	375.15	1.1777	0.01887	343.24	373.44	1.1638
150 160	0.02262 0.02333	354.82 365.22	386.49 397.89	1.2048 1.2315	0.01953 0.02017	353.66 364.15	384.91 396.43	1.1912 1.2181
170	0.02333	375.71	409.36	1.2576	0.02017	374.71	407.99	1.2445
180	0.02403	386.29	420.90	1.2834	0.02142	385.35	419.62	1.2704
190	0.02541	396.96	432.53	1.3088	0.02203	396.08	431.33	1.2960
200	0.02608	407.73	444.24	1.3338	0.02263	406.90	443.11	1.3212

**TABLE A-13** Properties of Saturated Ammonia (Liquid–Vapor): Temperature Table

		Specific m <sup>3</sup> /l			l Energy /kg		Enthalpy kJ/kg		Entro kJ/kg		
Temp. °C	Press. bar	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{\rm g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor u <sub>g</sub>	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{ m fg}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid s <sub>f</sub>	Sat. Vapor	Temp. °C
-50	0.4086	1.4245	2.6265	-43.94	1264.99	-43.88	1416.20	1372.32	-0.1922	6.1543	-50
-45	0.5453	1.4367	2.0060	-22.03	1271.19	-21.95	1402.52	1380.57	-0.0951	6.0523	-45
-40	0.7174	1.4493	1.5524	-0.10	1277.20	0.00	1388.56	1388.56	0.0000	5.9557	-40
-36	0.8850	1.4597	1.2757	17.47	1281.87	17.60	1377.17	1394.77	0.0747	5.8819	-36
-32	1.0832	1.4703	1.0561	35.09	1286.41	35.25	1365.55	1400.81	0.1484	5.8111	-32
-30	1.1950	1.4757	0.9634	43.93	1288.63	44.10	1359.65	1403.75	0.1849	5.7767	-30
-28	1.3159	1.4812	0.8803	52.78	1290.82	52.97	1353.68	1406.66	0.2212	5.7430	-28
-26	1.4465	1.4867	0.8056	61.65	1292.97	61.86	1347.65	1409.51	0.2572	5.7100	-26
-22	1.7390	1.4980	0.6780	79.46	1297.18	79.72	1335.36	1415.08	0.3287	5.6457	-22
-20	1.9019	1.5038	0.6233	88.40	1299.23	88.68	1329.10	1417.79	0.3642	5.6144	-20
-18	2.0769	1.5096	0.5739	97.36	1301.25	97.68	1322.77	1420.45	0.3994	5.5837	-18
-16	2.2644	1.5155	0.5291	106.36	1303.23	106.70	1316.35	1423.05	0.4346	5.5536	-16
-14	2.4652	1.5215	0.4885	115.37	1305.17	115.75	1309.86	1425.61	0.4695	5.5239	-14
-12	2.6798	1.5276	0.4516	124.42	1307.08	124.83	1303.28	1428.11	0.5043	5.4948	-12
-10	2.9089	1.5338	0.4180	133.50	1308.95	133.94	1296.61	1430.55	0.5389	5.4662	-10
-8	3.1532	1.5400	0.3874	142.60	1310.78	143.09	1289.86	1432.95	0.5734	5.4380	-8
-6	3.4134	1.5464	0.3595	151.74	1312.57	152.26	1283.02	1435.28	0.6077	5.4103	-6
-4	3.6901	1.5528	0.3340	160.88	1314.32	161.46	1276.10	1437.56	0.6418	5.3831	-4
-2	3.9842	1.5594	0.3106	170.07	1316.04	170.69	1269.08	1439.78	0.6759	5.3562	-2
0	4.2962	1.5660	0.2892	179.29	1317.71	179.96	1261.97	1441.94	0.7097	5.3298	0
2	4.6270	1.5727	0.2695	188.53	1319.34	189.26	1254.77	1444.03	0.7435	5.3038	2
4	4.9773	1.5796	0.2514	197.80	1320.92	198.59	1247.48	1446.07	0.7770	5.2781	4
6	5.3479	1.5866	0.2348	207.10	1322.47	207.95	1240.09	1448.04	0.8105	5.2529	6
8	5.7395	1.5936	0.2195	216.42	1323.96	217.34	1232.61	1449.94	0.8438	5.2279	8
10	6.1529	1.6008	0.2054	225.77	1325.42	226.75	1225.03	1451.78	0.8769	5.2033	10
12	6.5890	1.6081	0.1923	235.14	1326.82	236.20	1217.35	1453.55	0.9099	5.1791	12
16	7.5324	1.6231	0.1691	253.95	1329.48	255.18	1201.70	1456.87	0.9755	5.1314	16
20	8.5762	1.6386	0.1492	272.86	1331.94	274.26	1185.64	1459.90	1.0404	5.0849	20
24	9.7274	1.6547	0.1320	291.84	1334.19	293.45	1169.16	1462.61	1.1048	5.0394	24
28	10.993	1.6714	0.1172	310.92	1336.20	312.75	1152.24	1465.00	1.1686	4.9948	28
32	12.380	1.6887	0.1043	330.07	1337.97	332.17	1134.87	1467.03	1.2319	4.9509	32
36	13.896	1.7068	0.0930	349.32	1339.47	351.69	1117.00	1468.70	1.2946	4.9078	36
40	15.549	1.7256	0.0831	368.67	1340.70	371.35	1098.62	1469.97	1.3569	4.8652	40
45	17.819	1.7503	0.0725	393.01	1341.81	396.13	1074.84	1470.96	1.4341	4.8125	45
50	20.331	1.7765	0.0634	417.56	1342.42	421.17	1050.09	1471.26	1.5109	4.7604	50

Source: Tables A-13 through A-15 are calculated based on equations from L. Haar and J. S. Gallagher, "Thermodynamic Properties of Ammonia," J. Phys. Chem. Reference Data, Vol. 7, 1978, pp. 635–792.

**TABLE A-14** Properties of Saturated Ammonia (Liquid–Vapor): Pressure Table

		Specific m <sup>3</sup> /			l Energy /kg	Enthalpy kJ/kg			Entro kJ/kg		
Press.	Temp. °C	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{ m g}$	Sat. Liquid $u_{\rm f}$	Sat. Vapor u <sub>g</sub>	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{ m fg}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid s <sub>f</sub>	Sat. Vapor	Press. bar
0.40	-50.36	1.4236	2.6795	-45.52	1264.54	-45.46	1417.18	1371.72	-0.1992	6.1618	0.40
0.50	-46.53	1.4330	2.1752	-28.73	1269.31	-28.66	1406.73	1378.07	-0.1245	6.0829	0.50
0.60	-43.28	1.4410	1.8345	-14.51	1273.27	-14.42	1397.76	1383.34	-0.0622	6.0186	0.60
0.70	-40.46	1.4482	1.5884	-2.11	1276.66	-2.01	1389.85	1387.84	-0.0086	5.9643	0.70
0.80	-37.94	1.4546	1.4020	8.93	1279.61	9.04	1382.73	1391.78	0.0386	5.9174	0.80
0.90	-35.67	1.4605	1.2559	18.91	1282.24	19.04	1376.23	1395.27	0.0808	5.8760	0.90
1.00	-33.60	1.4660	1.1381	28.03	1284.61	28.18	1370.23	1398.41	0.1191	5.8391	1.00
1.25	-29.07	1.4782	0.9237	48.03	1289.65	48.22	1356.89	1405.11	0.2018	5.7610	1.25
1.50	-25.22	1.4889	0.7787	65.10	1293.80	65.32	1345.28	1410.61	0.2712	5.6973	1.50
1.75	-21.86	1.4984	0.6740	80.08	1297.33	80.35	1334.92	1415.27	0.3312	5.6435	1.75
2.00	-18.86	1.5071	0.5946	93.50	1300.39	93.80	1325.51	1419.31	0.3843	5.5969	2.00
2.25	-16.15	1.5151	0.5323	105.68	1303.08	106.03	1316.83	1422.86	0.4319	5.5558	2.25
2.50	-13.67	1.5225	0.4821	116.88	1305.49	117.26	1308.76	1426.03	0.4753	5.5190	2.50
2.75	-11.37	1.5295	0.4408	127.26	1307.67	127.68	1301.20	1428.88	0.5152	5.4858	2.75
3.00	-9.24	1.5361	0.4061	136.96	1309.65	137.42	1294.05	1431.47	0.5520	5.4554	3.00
3.25	-7.24	1.5424	0.3765	146.06	1311.46	146.57	1287.27	1433.84	0.5864	5.4275	3.25
3.50	-5.36	1.5484	0.3511	154.66	1313.14	155.20	1280.81	1436.01	0.6186	5.4016	3.50
3.75	-3.58	1.5542	0.3289	162.80	1314.68	163.38	1274.64	1438.03	0.6489	5.3774	3.75
4.00	-1.90	1.5597	0.3094	170.55	1316.12	171.18	1268.71	1439.89	0.6776	5.3548	4.00
4.25	-0.29	1.5650	0.2921	177.96	1317.47	178.62	1263.01	1441.63	0.7048	5.3336	4.25
4.50	1.25	1.5702	0.2767	185.04	1318.73	185.75	1257.50	1443.25	0.7308	5.3135	4.50
4.75	2.72	1.5752	0.2629	191.84	1319.91	192.59	1252.18	1444.77	0.7555	5.2946	4.75
5.00	4.13	1.5800	0.2503	198.39	1321.02	199.18	1247.02	1446.19	0.7791	5.2765	5.00
5.25	5.48	1.5847	0.2390	204.69	1322.07	205.52	1242.01	1447.53	0.8018	5.2594	5.25
5.50	6.79	1.5893	0.2286	210.78	1323.06	211.65	1237.15	1448.80	0.8236	5.2430	5.50
5.75	8.05	1.5938	0.2191	216.66	1324.00	217.58	1232.41	1449.99	0.8446	5.2273	5.75
6.00	9.27	1.5982	0.2104	222.37	1324.89	223.32	1227.79	1451.12	0.8649	5.2122	6.00
7.00	13.79	1.6148	0.1815	243.56	1328.04	244.69	1210.38	1455.07	0.9394	5.1576	7.00
8.00	17.84	1.6302	0.1596	262.64	1330.64	263.95	1194.36	1458.30	1.0054	5.1099	8.00
9.00	21.52	1.6446	0.1424	280.05	1332.82	281.53	1179.44	1460.97	1.0649	5.0675	9.00
10.00	24.89	1.6584	0.1285	296.10	1334.66	297.76	1165.42	1463.18	1.1191	5.0294	10.00
12.00	30.94	1.6841	0.1075	324.99	1337.52	327.01	1139.52	1466.53	1.2152	4.9625	12.00
14.00	36.26	1.7080	0.0923	350.58	1339.56	352.97	1115.82	1468.79	1.2987	4.9050	14.00
16.00	41.03	1.7306	0.0808	373.69	1340.97	376.46	1093.77	1470.23	1.3729	4.8542	16.00
18.00	45.38	1.7522	0.0717	394.85	1341.88	398.00	1073.01	1471.01	1.4399	4.8086	18.00
20.00	49.37	1.7731	0.0644	414.44	1342.37	417.99	1053.27	1471.26	1.5012	4.7670	20.00

**TABLE A-15** Properties of Superheated Ammonia Vapor

IADL	110peries of Superiested Aminonia Vapor									
T	<i>U</i>	и	h	S	<i>U</i>	и	h	S		
°C	m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	kJ/kg	kJ/kg	kJ/kg · K		
		$p = 0.4 \text{ bar}$ $(T_{\text{sat}} = -$		a	Į		= 0.06  MI $-43.28^{\circ}\text{C}$	Pa		
Sat.	2.6795	1264.54	1371.72	6.1618	1.8345	1273.27	1383.34	6.0186		
-50	2.6841	1265.11	1372.48	6.1652						
-45	2.7481	1273.05	1382.98	6.2118						
-40	2.8118	1281.01	1393.48	6.2573	1.8630	1278.62	1390.40	6.0490		
$-35 \\ -30$	2.8753 2.9385	1288.96 1296.93	1403.98 1414.47	6.3018 6.3455	1.9061 1.9491	1286.75 1294.88	1401.12 1411.83	6.0946 6.1390		
$-25 \\ -20$	3.0015 3.0644	1304.90 1312.88	1424.96 1435.46	6.3882 6.4300	1.9918 2.0343	1303.01 1311.13	1422.52 1433.19	6.1826 6.2251		
-15	3.1271	1320.87	1445.95	6.4711	2.0766	1311.13	1443.85	6.2668		
-10	3.1896	1328.87	1456.45	6.5114	2.1188	1327.37	1454.50	6.3077		
-5	3.2520	1336.88	1466.95	6.5509	2.1609	1335.49	1465.14	6.3478		
0	3.3142	1344.90	1477.47	6.5898	2.2028	1343.61	1475.78	6.3871		
5	3.3764	1352.95	1488.00	6.6280	2.2446	1351.75	1486.43	6.4257		
		p = 0.8  bar	= 0.08 MP			a = 1.0  bar	= 0.10 MI	D <sub>0</sub>		
		$T_{\text{sat}} = -$					-33.60°C)	. a		
Sat.	1.4021	1279.61	1391.78	5.9174	1.1381	1284.61	1398.41	5.8391		
$-35 \\ -30$	1.4215 1.4543	1284.51 1292.81	1398.23 1409.15	5.9446 5.9900	1.1573	1290.71	1406.44	5.8723		
		1301.09	1420.04			1299.15		5.9175		
$-25 \\ -20$	1.4868 1.5192	1301.09	1420.04	6.0343 6.0777	1.1838 1.2101	1299.13	1417.53 1428.58	5.9616		
-15	1.5514	1317.61	1441.72	6.1200	1.2362	1315.96	1439.58	6.0046		
-10	1.5834	1325.85	1452.53	6.1615	1.2621	1324.33	1450.54	6.0467		
-5	1.6153	1334.09	1463.31	6.2021	1.2880	1332.67	1461.47	6.0878		
0	1.6471	1342.31	1474.08	6.2419	1.3136	1341.00	1472.37	6.1281		
5	1.6788	1350.54	1484.84	6.2809	1.3392	1349.33	1483.25	6.1676		
10	1.7103	1358.77	1495.60	6.3192	1.3647	1357.64	1494.11	6.2063		
15 20	1.7418 1.7732	1367.01 1375.25	1506.35 1517.10	6.3568 6.3939	1.3900 1.4153	1365.95 1374.27	1504.96 1515.80	6.2442 6.2816		
20	1.7732	1373.23	1317.10	0.5757	1.1133	1371.27	1313.00	0.2010		
		p = 1.5  bar		a			= 0.20  M	Pa		
		$(T_{\rm sat} = -$	25.22°C)			$(T_{\rm sat} = -$	-18.86°C)			
Sat.	0.7787	1293.80	1410.61	5.6973	0.59460	1300.39	1419.31	5.5969		
-25	0.7795	1294.20	1411.13	5.6994						
-20	0.7978	1303.00	1422.67	5.7454						
-15	0.8158	1311.75	1434.12	5.7902	0.60542	1307.43	1428.51	5.6328		
$-10 \\ -5$	0.8336 0.8514	1320.44 1329.08	1445.49 1456.79	5.8338 5.8764	0.61926 0.63294	1316.46 1325.41	1440.31 1452.00	5.6781 5.7221		
0 5	0.8689 0.8864	1337.68 1346.25	1468.02 1479.20	5.9179 5.9585	0.64648 0.65989	1334.29 1343.11	1463.59 1475.09	5.7649 5.8066		
10	0.9037	1354.78	1490.34	5.9981	0.67320	1351.87	1486.51	5.8473		
15	0.9210	1363.29	1501.44	6.0370	0.68640	1360.59	1497.87	5.8871		
20	0.9382	1371.79	1512.51	6.0751	0.69952	1369.28	1509.18	5.9260		
25	0.9553	1380.28	1523.56	6.1125	0.71256	1377.93	1520.44	5.9641		
30	0.9723	1388.76	1534.60	6.1492	0.72553	1386.56	1531.67	6.0014		

**TABLE A-15** (Continued)

TABL	E A-15 (	Continued)						
T	<i>U</i>	и	h	S	<i>v</i>	и	h	S
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	kJ/kg	kJ/kg	kJ/kg · K
	<i>p</i>	$= 2.5 \text{ bar}$ $(T_{\text{sat}} = -$	= 0.25 MP 13.67°C)	a	1		= 0.30  M $-9.24^{\circ}\text{C}$	Pa 
Sat10	0.48213 0.49051	1305.49 1312.37	1426.03 1435.00	5.5190 5.5534	0.40607	1309.65	1431.47	5.4554
-5	0.50180	1321.65	1447.10	5.5989	0.41428	1317.80	1442.08	5.4953
0	0.51293	1330.83	1459.06	5.6431	0.42382	1327.28	1454.43	5.5409
5	0.52393	1339.91	1470.89	5.6860	0.43323	1336.64	1466.61	5.5851
10	0.53482	1348.91	1482.61	5.7278	0.44251	1345.89	1478.65	5.6280
15	0.54560	1357.84	1494.25	5.7685	0.45169	1355.05	1490.56	5.6697
20	0.55630	1366.72	1505.80	5.8083	0.46078	1364.13	1502.36	5.7103
25	0.56691	1375.55	1517.28	5.8471	0.46978	1373.14	1514.07	5.7499
30	0.57745	1384.34	1528.70	5.8851	0.47870	1382.09	1525.70	5.7886
35	0.58793	1393.10	1540.08	5.9223	0.48756	1391.00	1537.26	5.8264
40	0.59835	1401.84	1551.42	5.9589	0.49637	1399.86	1548.77	5.8635
45	0.60872	1410.56	1562.74	5.9947	0.50512	1408.70	1560.24	5.8998
	p	$= 3.5 \text{ bar}$ $(T_{\text{sat}} = -$	= 0.35 MP -5.36°C)	a	I		$= 0.40 \text{ M}$ $-1.90^{\circ}\text{C}$	Pa
Sat.	0.35108	1313.14	1436.01	5.4016	0.30942	1316.12	1439.89	5.3548
0	0.36011	1323.66	1449.70	5.4522	0.31227	1319.95	1444.86	5.3731
10	0.37654	1342.82	1474.61	5.5417	0.32701	1339.68	1470.49	5.4652
20	0.39251	1361.49	1498.87	5.6259	0.34129	1358.81	1495.33	5.5515
30	0.40814	1379.81	1522.66	5.7057	0.35520	1377.49	1519.57	5.6328
40	0.42350	1397.87	1546.09	5.7818	0.36884	1395.85	1543.38	5.7101
60	0.45363	1433.55	1592.32	5.9249	0.39550	1431.97	1590.17	5.8549
80	0.48320	1469.06	1638.18	6.0586	0.42160	1467.77	1636.41	5.9897
100	0.51240	1504.73	1684.07	6.1850	0.44733	1503.64	1682.58	6.1169
120	0.54136	1540.79	1730.26	6.3056	0.47280	1539.85	1728.97	6.2380
140	0.57013	1577.38	1776.92	6.4213	0.49808	1576.55	1775.79	6.3541
160	0.59876	1614.60	1824.16	6.5330	0.52323	1613.86	1823.16	6.4661
180	0.62728	1652.51	1872.06	6.6411	0.54827	1651.85	1871.16	6.5744
200	0.65572	1691.15	1920.65	6.7460	0.57322	1690.56	1919.85	6.6796
	p	$= 4.5 \text{ bar}$ $(T_{\text{sat}} =$	= 0.45 MP 1.25°C)	'a			= 0.50  M $4.13^{\circ}\text{C})$	Pa
Sat.	0.27671	1318.73	1443.25	5.3135	0.25034	1321.02	1446.19	5.2765
10	0.28846	1336.48	1466.29	5.3962	0.25757	1333.22	1462.00	5.3330
20	0.30142	1356.09	1491.72	5.4845	0.26949	1353.32	1488.06	5.4234
30	0.31401	1375.15	1516.45	5.5674	0.28103	1372.76	1513.28	5.5080
40	0.32631	1393.80	1540.64	5.6460	0.29227	1391.74	1537.87	5.5878
60	0.35029	1430.37	1588.00	5.7926	0.31410	1428.76	1585.81	5.7362
80	0.37369	1466.47	1634.63	5.9285	0.33535	1465.16	1632.84	5.8733
100	0.39671	1502.55	1681.07	6.0564	0.35621	1501.46	1679.56	6.0020
120	0.41947	1538.91	1727.67	6.1781	0.37681	1537.97	1726.37	6.1242
140	0.44205	1575.73	1774.65	6.2946	0.39722	1574.90	1773.51	6.2412
160	0.46448	1613.13	1822.15	6.4069	0.41749	1612.40	1821.14	6.3537
180	0.48681	1651.20	1870.26	6.5155	0.43765	1650.54	1869.36	6.4626
200	0.50905	1689.97	1919.04	6.6208	0.45771	1689.38	1918.24	6.5681

**TABLE A-15** (Continued)

	E A-15 (	Continuea)								
<i>T</i>	<i>v</i>	u	<i>h</i>	s	v	и	<i>h</i>	s		
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	kJ/kg	kJ/kg	kJ/kg · K		
	p	$= 5.5 \text{ bar}$ $(T_{\text{sat}} =$		a	p = 6.0  bar = 0.60  MPa $(T_{\text{sat}} = 9.27^{\circ}\text{C})$					
Sat.	0.22861	1323.06	1448.80	5.2430	0.21038	1324.89	1451.12	5.2122		
10	0.23227	1329.88	1457.63	5.2743	0.21115	1326.47	1453.16	5.2195		
20	0.24335	1350.50	1484.34	5.3671	0.22155	1347.62	1480.55	5.3145		
30	0.25403	1370.35	1510.07	5.4534	0.23152	1367.90	1506.81	5.4026		
40	0.26441	1389.64	1535.07	5.5345	0.24118	1387.52	1532.23	5.4851		
50	0.27454	1408.53	1559.53	5.6114	0.25059	1406.67	1557.03	5.5631		
60	0.28449	1427.13	1583.60	5.6848	0.25981	1425.49	1581.38	5.6373		
80	0.30398	1463.85	1631.04	5.8230	0.27783	1462.52	1629.22	5.7768		
100	0.32307	1500.36	1678.05	5.9525	0.29546	1499.25	1676.52	5.9071		
120	0.34190	1537.02	1725.07	6.0753	0.31281	1536.07	1723.76	6.0304		
140	0.36054	1574.07	1772.37	6.1926	0.32997	1573.24	1771.22	6.1481		
160	0.37903	1611.66	1820.13	6.3055	0.34699	1610.92	1819.12	6.2613		
180	0.39742	1649.88	1868.46	6.4146	0.36390	1649.22	1867.56	6.3707		
200	0.41571	1688.79	1917.43	6.5203	0.38071	1688.20	1916.63	6.4766		
	p	$= 7.0 \text{ bar}$ $(T_{\text{sat}} = 1)$		'a	p = 8.0  bar = 0.80  MPa $(T_{\text{sat}} = 17.84^{\circ}\text{C})$					
Sat. 20 30	0.18148	1328.04	1455.07	5.1576	0.15958	1330.64	1458.30	5.1099		
	0.18721	1341.72	1472.77	5.2186	0.16138	1335.59	1464.70	5.1318		
	0.19610	1362.88	1500.15	5.3104	0.16948	1357.71	1493.29	5.2277		
40	0.20464	1383.20	1526.45	5.3958	0.17720	1378.77	1520.53	5.3161		
50	0.21293	1402.90	1551.95	5.4760	0.18465	1399.05	1546.77	5.3986		
60	0.22101	1422.16	1576.87	5.5519	0.19189	1418.77	1572.28	5.4763		
80	0.23674	1459.85	1625.56	5.6939	0.20590	1457.14	1621.86	5.6209		
100	0.25205	1497.02	1673.46	5.8258	0.21949	1494.77	1670.37	5.7545		
120	0.26709	1534.16	1721.12	5.9502	0.23280	1532.24	1718.48	5.8801		
140	0.28193	1571.57	1768.92	6.0688	0.24590	1569.89	1766.61	5.9995		
160	0.29663	1609.44	1817.08	6.1826	0.25886	1607.96	1815.04	6.1140		
180	0.31121	1647.90	1865.75	6.2925	0.27170	1646.57	1863.94	6.2243		
200	0.32571	1687.02	1915.01	6.3988	0.28445	1685.83	1913.39	6.3311		
	p	$= 9.0 \text{ bar}$ $(T_{\text{sat}} = 2$		a	p		r = 1.00 M 24.89°C)	Pa		
Sat. 30 40	0.14239	1332.82	1460.97	5.0675	0.12852	1334.66	1463.18	5.0294		
	0.14872	1352.36	1486.20	5.1520	0.13206	1346.82	1478.88	5.0816		
	0.15582	1374.21	1514.45	5.2436	0.13868	1369.52	1508.20	5.1768		
50	0.16263	1395.11	1541.47	5.3286	0.14499	1391.07	1536.06	5.2644		
60	0.16922	1415.32	1567.61	5.4083	0.15106	1411.79	1562.86	5.3460		
80	0.18191	1454.39	1618.11	5.5555	0.16270	1451.60	1614.31	5.4960		
100	0.19416	1492.50	1667.24	5.6908	0.17389	1490.20	1664.10	5.6332		
120	0.20612	1530.30	1715.81	5.8176	0.18478	1528.35	1713.13	5.7612		
140	0.21788	1568.20	1764.29	5.9379	0.19545	1566.51	1761.96	5.8823		
160	0.22948	1606.46	1813.00	6.0530	0.20598	1604.97	1810.94	5.9981		
180	0.24097	1645.24	1862.12	6.1639	0.21638	1643.91	1860.29	6.1095		
200	0.25237	1684.64	1911.77	6.2711	0.22670	1683.44	1910.14	6.2171		

TABLE A-15(Continued)

280 0.13224 1841.03 2105.50

TABL	.E A-15 (	Continued)						
T °C	<i>v</i> m³/kg	и 1-1/1-с	h 1-1/1-2	S Ir I / Iron V	<i>v</i> m³/kg	и 1-1/1-с	h	S la I / la a a I /
		kJ/kg	kJ/kg	kJ/kg·K		kJ/kg	kJ/kg	kJ/kg·K
	<i>p</i>	= 12.0  bar $(T_{\text{sat}} = 3)$	$= 1.20 \text{ MI}$ $30.94^{\circ}\text{C}$	-a 			r = 1.40 M 36.26°C)	.———
Sat.	0.10751	1337.52	1466.53	4.9625	0.09231	1339.56	1468.79	4.9050
40	0.11287	1359.73	1495.18	5.0553	0.09432	1349.29	1481.33	4.9453
60	0.12378	1404.54	1553.07	5.2347	0.10423	1396.97	1542.89	5.1360
80	0.13387	1445.91	1606.56	5.3906	0.11324	1440.06	1598.59	5.2984
100 120	0.14347 0.15275	1485.55 1524.41	1657.71 1707.71	5.5315 5.6620	0.12172 0.12986	1480.79 1520.41	1651.20 1702.21	5.4433 5.5765
140	0.16181	1563.09	1757.26	5.7850	0.13777	1559.63	1752.52	5.7013
160 180	0.17072 0.17950	1601.95 1641.23	1806.81 1856.63	5.9021 6.0145	0.14552 0.15315	1598.92 1638.53	1802.65 1852.94	5.8198 5.9333
200	0.18819	1681.05	1906.87	6.1230	0.16068	1678.64	1903.59	6.0427
220	0.18819	1721.50	1900.87	6.1230	0.16813	1719.35	1903.39	6.1485
240	0.20534	1762.63	2009.04	6.3303	0.17551	1760.72	2006.43	6.2513
260	0.21382	1804.48	2061.06	6.4297	0.18283	1802.78	2058.75	6.3513
280	0.22225	1847.04	2113.74	6.5267	0.19010	1845.55	2111.69	6.4488
		l						
	p		= 1.60  MI	Pa	p		r = 1.80  M	Pa
		$(T_{\rm sat} = 4)$	41.03°C)			$(T_{\rm sat} =$	45.38°C)	
Sat.	0.08079	1340.97	1470.23	4.8542	0.07174	1341.88	1471.01	4.8086
60	0.08951	1389.06	1532.28	5.0461	0.07801	1380.77	1521.19	4.9627
80	0.09774	1434.02	1590.40	5.2156	0.08565	1427.79	1581.97	5.1399
100	0.10539	1475.93	1644.56	5.3648	0.09267	1470.97	1637.78	5.2937
120	0.11268	1516.34	1696.64	5.5008	0.09931	1512.22	1690.98	5.4326
140	0.11974	1556.14	1747.72	5.6276	0.10570	1552.61	1742.88	5.5614
160	0.12663	1595.85	1798.45	5.7475	0.11192	1592.76	1794.23	5.6828
180 200	0.13339 0.14005	1635.81 1676.21	1849.23 1900.29	5.8621 5.9723	0.11801 0.12400	1633.08 1673.78	1845.50 1896.98	5.7985 5.9096
220 240	0.14663 0.15314	1717.18 1758.79	1951.79 2003.81	6.0789 6.1823	0.12991 0.13574	1715.00 1756.85	1948.83 2001.18	6.0170 6.1210
260	0.15959	1801.07	2056.42	6.2829	0.13374	1799.35	2054.08	6.2222
280	0.16599	1844.05	2109.64	6.3809	0.14724	1842.55	2107.58	6.3207
	p		= 2.00  MI	Pa				
		$(T_{\rm sat} = 4)$	19.37°C)					
Sat.	0.06445	1342.37	1471.26	4.7670				
60	0.06875	1372.05	1509.54	4.8838				
80	0.07596	1421.36	1573.27	5.0696				
100	0.08248	1465.89	1630.86	5.2283				
120	0.08861	1508.03	1685.24	5.3703				
140	0.09447	1549.03	1737.98	5.5012				
160	0.10016	1589.65	1789.97	5.6241				
180 200	0.10571 0.11116	1630.32 1671.33	1841.74 1893.64	5.7409 5.8530				
220 240	0.11652 0.12182	1712.82 1754.90	1945.87 1998.54	5.9611 6.0658				
260	0.12182	1797.63	2051.74	6.1675				
• • • •	0.1000:	1041.03	2105.50					

6.2665

 TABLE A-16
 Properties of Saturated Propane (Liquid–Vapor): Temperature Table

			Volume /kg	Internal kJ/l		]	Enthalpy kJ/kg		Entro kJ/kg		
Temp. °C	Press.	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{\rm g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor u <sub>g</sub>	Sat. Liquid $h_{ m f}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid $s_{\rm f}$	Sat. Vapor	Temp.
-100	0.02888	1.553	11.27	-128.4	319.5	-128.4	480.4	352.0	-0.634	2.140	-100
-90	0.06426	1.578	5.345	-107.8	329.3	-107.8	471.4	363.6	-0.519	2.055	-90
-80	0.1301	1.605	2.774	-87.0	339.3	-87.0	462.4	375.4	-0.408	1.986	-80
-70	0.2434	1.633	1.551	-65.8	349.5	-65.8	453.1	387.3	-0.301	1.929	-70
-60	0.4261	1.663	0.9234	-44.4	359.9	-44.3	443.5	399.2	-0.198	1.883	-60
-50	0.7046	1.694	0.5793	-22.5	370.4	-22.4	433.6	411.2	-0.098	1.845	-50
-40	1.110	1.728	0.3798	-0.2	381.0	0.0	423.2	423.2	0.000	1.815	-40
-30	1.677	1.763	0.2585	22.6	391.6	22.9	412.1	435.0	0.096	1.791	-30
-20	2.444	1.802	0.1815	45.9	402.4	46.3	400.5	446.8	0.190	1.772	-20
-10	3.451	1.844	0.1309	69.8	413.2	70.4	388.0	458.4	0.282	1.757	-10
0	4.743	1.890	0.09653	94.2	423.8	95.1	374.5	469.6	0.374	1.745	0
4	5.349	1.910	0.08591	104.2	428.1	105.3	368.8	474.1	0.410	1.741	4
8	6.011	1.931	0.07666	114.3	432.3	115.5	362.9	478.4	0.446	1.737	8
12	6.732	1.952	0.06858	124.6	436.5	125.9	356.8	482.7	0.482	1.734	12
16	7.515	1.975	0.06149	135.0	440.7	136.4	350.5	486.9	0.519	1.731	16
20	8.362	1.999	0.05525	145.4	444.8	147.1	343.9	491.0	0.555	1.728	20
24	9.278	2.024	0.04973	156.1	448.9	158.0	337.0	495.0	0.591	1.725	24
28	10.27	2.050	0.04483	166.9	452.9	169.0	329.9	498.9	0.627	1.722	28
32	11.33	2.078	0.04048	177.8	456.7	180.2	322.4	502.6	0.663	1.720	32
36	12.47	2.108	0.03659	188.9	460.6	191.6	314.6	506.2	0.699	1.717	36
40	13.69	2.140	0.03310	200.2	464.3	203.1	306.5	509.6	0.736	1.715	40
44	15.00	2.174	0.02997	211.7	467.9	214.9	298.0	512.9	0.772	1.712	44
48	16.40	2.211	0.02714	223.4	471.4	227.0	288.9	515.9	0.809	1.709	48
52	17.89	2.250	0.02459	235.3	474.6	239.3	279.3	518.6	0.846	1.705	52
56	19.47	2.293	0.02227	247.4	477.7	251.9	269.2	521.1	0.884	1.701	56
60	21.16	2.340	0.02015	259.8	480.6	264.8	258.4	523.2	0.921	1.697	60
65	23.42	2.406	0.01776	275.7	483.6	281.4	243.8	525.2	0.969	1.690	65
70	25.86	2.483	0.01560	292.3	486.1	298.7	227.7	526.4	1.018	1.682	70
75	28.49	2.573	0.01363	309.5	487.8	316.8	209.8	526.6	1.069	1.671	75
80	31.31	2.683	0.01182	327.6	488.2	336.0	189.2	525.2	1.122	1.657	80
85	34.36	2.827	0.01011	347.2	486.9	356.9	164.7	521.6	1.178	1.638	85
90	37.64	3.038	0.008415	369.4	482.2	380.8	133.1	513.9	1.242	1.608	90
95	41.19	3.488	0.006395	399.8	467.4	414.2	79.5	493.7	1.330	1.546	95
96.7	42.48	4.535	0.004535	434.9	434.9	454.2	0.0	457.2	1.437	1.437	96.7

Source: Tables A-16 through A-18 are calculated based on B. A. Younglove and J. F. Ely, "Thermophysical Properties of Fluids. II. Methane, Ethane, Propane, Isobutane and Normal Butane," J. Phys. Chem. Ref. Data, Vol. 16, No. 4, 1987, pp. 577–598.

 TABLE A-17
 Properties of Saturated Propane (Liquid-Vapor): Pressure Table

			Specific Volume Internal Energy Enthalpy m³/kg kJ/kg kJ/kg						Entro kJ/kg		
Press.	Temp. °C	Sat. Liquid $v_{\rm f} \times 10^3$	Sat. Vapor $v_{\rm g}$	Sat. Liquid $u_{\rm f}$	Sat. Vapor $u_{\rm g}$	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid $s_{\rm f}$	Sat. Vapor	Press.
0.05	-93.28	1.570	6.752	-114.6	326.0	-114.6	474.4	359.8	-0.556	2.081	0.05
0.10	-83.87	1.594	3.542	-95.1	335.4	-95.1	465.9	370.8	-0.450	2.011	0.10
0.25	-69.55	1.634	1.513	-64.9	350.0	-64.9	452.7	387.8	-0.297	1.927	0.25
0.50	-56.93	1.672	0.7962	-37.7	363.1	-37.6	440.5	402.9	-0.167	1.871	0.50
0.75	-48.68	1.698	0.5467	-19.6	371.8	-19.5	432.3	412.8	-0.085	1.841	0.75
1.00	-42.38	1.719	0.4185	-5.6	378.5	-5.4	425.7	420.3	-0.023	1.822	1.00
2.00	-25.43	1.781	0.2192	33.1	396.6	33.5	406.9	440.4	0.139	1.782	2.00
3.00	-14.16	1.826	0.1496	59.8	408.7	60.3	393.3	453.6	0.244	1.762	3.00
4.00	-5.46	1.865	0.1137	80.8	418.0	81.5	382.0	463.5	0.324	1.751	4.00
5.00	1.74	1.899	0.09172	98.6	425.7	99.5	372.1	471.6	0.389	1.743	5.00
6.00	7.93	1.931	0.07680	114.2	432.2	115.3	363.0	478.3	0.446	1.737	6.00
7.00	13.41	1.960	0.06598	128.2	438.0	129.6	354.6	484.2	0.495	1.733	7.00
8.00	18.33	1.989	0.05776	141.0	443.1	142.6	346.7	489.3	0.540	1.729	8.00
9.00	22.82	2.016	0.05129	152.9	447.6	154.7	339.1	493.8	0.580	1.726	9.00
10.00	26.95	2.043	0.04606	164.0	451.8	166.1	331.8	497.9	0.618	1.723	10.00
11.00	30.80	2.070	0.04174	174.5	455.6	176.8	324.7	501.5	0.652	1.721	11.00
12.00	34.39	2.096	0.03810	184.4	459.1	187.0	317.8	504.8	0.685	1.718	12.00
13.00	37.77	2.122	0.03499	193.9	462.2	196.7	311.0	507.7	0.716	1.716	13.00
14.00	40.97	2.148	0.03231	203.0	465.2	206.0	304.4	510.4	0.745	1.714	14.00
15.00	44.01	2.174	0.02997	211.7	467.9	215.0	297.9	512.9	0.772	1.712	15.00
16.00	46.89	2.200	0.02790	220.1	470.4	223.6	291.4	515.0	0.799	1.710	16.00
17.00	49.65	2.227	0.02606	228.3	472.7	232.0	285.0	517.0	0.824	1.707	17.00
18.00	52.30	2.253	0.02441	236.2	474.9	240.2	278.6	518.8	0.849	1.705	18.00
19.00	54.83	2.280	0.02292	243.8	476.9	248.2	272.2	520.4	0.873	1.703	19.00
20.00	57.27	2.308	0.02157	251.3	478.7	255.9	265.9	521.8	0.896	1.700	20.00
22.00	61.90	2.364	0.01921	265.8	481.7	271.0	253.0	524.0	0.939	1.695	22.00
24.00	66.21	2.424	0.01721	279.7	484.3	285.5	240.1	525.6	0.981	1.688	24.00
26.00	70.27	2.487	0.01549	293.1	486.2	299.6	226.9	526.5	1.021	1.681	26.00
28.00	74.10	2.555	0.01398	306.2	487.5	313.4	213.2	526.6	1.060	1.673	28.00
30.00	77.72	2.630	0.01263	319.2	488.1	327.1	198.9	526.0	1.097	1.664	30.00
35.00	86.01	2.862	0.009771	351.4	486.3	361.4	159.1	520.5	1.190	1.633	35.00
40.00	93.38	3.279	0.007151	387.9	474.7	401.0	102.3	503.3	1.295	1.574	40.00
42.48	96.70	4.535	0.004535	434.9	434.9	454.2	0.0	454.2	1.437	1.437	42.48

**TABLE A-18** Properties of Superheated Propane

		operties	or Superi	icaicu i rop	·une				
T	<i>U</i>	и	h	S		v	и	h	S
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K		m³/kg	kJ/kg	kJ/kg	kJ/kg · K
		0.05  bar $(T_{\text{sat}} = -$						= 0.01 -83.87°C	
Sat.	6.752	326.0	359.8	2.081	3	3.542	367.3	370.8	2.011
-90 -80	6.877 7.258	329.4 339.8	363.8 376.1	2.103 2.169	<u> </u>	3.617	339.5	375.7	2.037
-70 -60 -50	7.639 8.018 8.397	350.6 361.8 373.3	388.8 401.9 415.3	2.233 2.296 2.357	3	3.808 3.999 4.190	350.3 361.5 373.1	388.4 401.5 415.0	2.101 2.164 2.226
-40 -30	8.776 9.155	385.1 397.4	429.0 443.2	2.418 2.477	4	4.380 4.570	385.0 397.3	428.8 443.0	2.286 2.346
-20	9.533	410.1	457.8	2.536	4	4.760	410.0	457.6	2.405
-10 0 10 20	9.911 10.29 10.67 11.05	423.2 436.8 450.8 270.6	472.8 488.2 504.1 520.4	2.594 2.652 2.709 2.765	<u>:</u>	4.950 5.139 5.329 5.518	423.1 436.7 450.6 465.1	472.6 488.1 503.9 520.3	2.463 2.520 2.578 2.634
		= 0.5 bar						r = 0.1  N	
		$(T_{\rm sat} = -$			-			-42.38°C	(1)
Sat50 -40	0.796 0.824 0.863	363.1 371.3 383.4	402.9 412.5 426.6	1.871 1.914 1.976		0.4185	378.5 381.5	420.3 423.8	1.822 1.837
-30 $-20$ $-10$	0.903 0.942 0.981	396.0 408.8 422.1	441.1 455.9 471.1	2.037 2.096 2.155	(	0.4439 0.4641 0.4842	394.2 407.3 420.7	438.6 453.7 469.1	1.899 1.960 2.019
0 10 20	1.019 1.058 1.096	435.8 449.8 464.3	486.7 502.7 519.1	2.213 2.271 2.328	(	0.5040 0.5238 0.5434	434.4 448.6 463.3	484.8 501.0 517.6	2.078 2.136 2.194
30 40 50 60	1.135 1.173 1.211 1.249	479.2 494.6 510.4 526.7	535.9 553.2 570.9 589.1	2.384 2.440 2.496 2.551	(	0.5629 0.5824 0.6018 0.6211	478.2 493.7 509.5 525.8	534.5 551.9 569.7 587.9	2.251 2.307 2.363 2.419
		$= 2.0 \text{ bar}$ $(T_{\text{sat}} = -$			-			r = 0.3 N -14.16°C	
Sat20	0.2192 0.2251	396.6 404.0	440.4 449.0	1.782 1.816	- (	0.1496	408.7	453.6	1.762
-10	0.2358	417.7	464.9	1.877	(	0.1527	414.7	460.5	1.789
0 10 20	0.2463 0.2566 0.2669	431.8 446.3 461.1	481.1 497.6 514.5	1.938 1.997 2.056	(	0.1602 0.1674 0.1746	429.0 443.8 458.8	477.1 494.0 511.2	1.851 1.912 1.971
30 40 50	0.2770 0.2871 0.2970	476.3 491.9 507.9	531.7 549.3 567.3	2.113 2.170 2.227	(	0.1816 0.1885 0.1954	474.2 490.1 506.2	528.7 546.6 564.8	2.030 2.088 2.145
60 70 80 90	0.3070 0.3169 0.3267 0.3365	524.3 541.1 558.4 576.1	585.7 604.5 623.7 643.4	2.283 2.339 2.394 2.449	(	0.2022 0.2090 0.2157 0.2223	522.7 539.6 557.0 574.8	583.4 602.3 621.7 641.5	2.202 2.258 2.314 2.369

 TABLE A-18 (Continued)

TABLI	<b>E A-18</b> ( <i>C</i>	Continued	)		
<i>T</i>	v	и	<i>h</i>	s	<i>v u h s</i>
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg kJ/kg kJ/kg kJ/kg·K
	<i>p</i> =	$= 4.0 \text{ bar}$ $(T_{\text{sat}} = -$			p = 5.0  bar = 0.5  MPa $(T_{\text{sat}} = 1.74^{\circ}\text{C})$
Sat.	0.1137 0.1169	418.0 426.1	463.5 472.9	1.751 1.786	0.09172   425.7   471.6   1.743
10	0.1227	441.2	490.3	1.848	0.09577     438.4     486.3     1.796       0.1005     454.1     504.3     1.858
20	0.1283	456.6	507.9	1.909	
30	0.1338	472.2	525.7	1.969	0.1051     470.0     522.5     1.919       0.1096     486.1     540.9     1.979
40	0.1392	488.1	543.8	2.027	
50	0.1445	504.4	562.2	2.085	0.1140     502.5     559.5     2.038       0.1183     519.4     578.5     2.095       0.1226     536.6     597.9     2.153
60	0.1498	521.1	581.0	2.143	
70	0.1550	538.1	600.1	2.199	
80	0.1601	555.7	619.7	2.255	0.1268     554.1     617.5     2.209       0.1310     572.1     637.6     2.265       0.1351     590.5     658.0     2.321       0.1392     609.3     678.9     2.376
90	0.1652	573.5	639.6	2.311	
100	0.1703	591.8	659.9	2.366	
110	0.1754	610.4	680.6	2.421	
	p =	$= 6.0 \text{ bar}$ $(T_{\text{sat}} =$	= 0.6  N 7.93°C)	<b>Л</b> Ра	p = 7.0  bar = 0.7  MPa $(T_{\text{sat}} = 13.41^{\circ}\text{C})$
Sat.	0.07680	432.2	478.3	1.737	0.06598     438.0     484.2     1.733       0.06847     448.8     496.7     1.776
10	0.07769	435.6	482.2	1.751	
20	0.08187	451.5	500.6	1.815	
30	0.08588	467.7	519.2	1.877	0.07210     465.2     515.7     1.840       0.07558     481.9     534.8     1.901       0.07896     498.7     554.0     1.962
40	0.08978	484.0	537.9	1.938	
50	0.09357	500.7	556.8	1.997	
60	0.09729	517.6	576.0	2.056	0.08225     515.9     573.5     2.021       0.08547     533.4     593.2     2.079       0.08863     551.2     613.2     2.137
70	0.1009	535.0	595.5	2.113	
80	0.1045	552.7	615.4	2.170	
90	0.1081	570.7	635.6	2.227	0.09175     569.4     633.6     2.194       0.09482     587.9     654.3     2.250       0.09786     606.8     675.3     2.306       0.1009     626.2     696.8     2.361
100	0.1116	589.2	656.2	2.283	
110	0.1151	608.0	677.1	2.338	
120	0.1185	627.3	698.4	2.393	
		$= 8.0 \text{ bar}$ $(T_{\text{sat}} = 1)$	= 0.8  M $18.33^{\circ}\text{C}$	⁄IPa	p = 9.0  bar = 0.9  MPa $(T_{\text{sat}} = 22.82^{\circ}\text{C})$
Sat. 20	0.05776 0.05834	443.1 445.9	489.3 492.6	1.729 1.740	0.05129 447.2 493.8 1.726
30	0.06170	462.7	512.1	1.806	0.05355     460.0     508.2     1.774       0.05653     477.2     528.1     1.839
40	0.06489	479.6	531.5	1.869	
50	0.06796	496.7	551.1	1.930	0.05938     494.7     548.1     1.901       0.06213     512.2     568.1     1.962
60	0.07094	514.0	570.8	1.990	
70	0.07385	531.6	590.7	2.049	0.06479     530.0     588.3     2.022       0.06738     548.1     608.7     2.081       0.06992     566.5     629.4     2.138
80	0.07669	549.6	611.0	2.107	
90	0.07948	567.9	631.5	2.165	
100	0.08222	586.5	652.3	2.221	0.07241     585.2     650.4     2.195       0.07487     604.3     671.7     2.252       0.07729     623.7     693.3     2.307
110	0.08493	605.6	673.5	2.277	
120	0.08761	625.0	695.1	2.333	
130	0.09026	644.8	717.0	2.388	0.07969     643.6     715.3     2.363       0.08206     663.8     737.7     2.418
140	0.09289	665.0	739.3	2.442	

 TABLE A-18 (Continued)

IABLI	E A-18 (C	onunuea	)					
<i>T</i>	v	и	<i>h</i>	s	<i>v</i>	и	<i>h</i>	s
°C	m³/kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	kJ/kg	kJ/kg	kJ/kg · K
	<i>p</i> =	= 10.0 ba $(T_{\text{sat}} = 2)$	r = 1.0 M 26.95°C)	MPa	-		ur = 1.2 (34.39°C)	
Sat. 30	0.04606 0.04696	451.8 457.1	497.9 504.1	1.723 1.744	0.03810	459.1	504.8	1.718
40	0.04980	474.8	524.6	1.810	0.03957	469.4	516.9	1.757
50	0.05248	492.4	544.9	1.874	0.04204	487.8	538.2	1.824
60	0.05505	510.2	565.2	1.936	0.04436	506.1	559.3	1.889
70	0.05752	528.2	585.7	1.997	0.04657	524.4	580.3	1.951
80	0.05992	546.4	606.3	2.056	0.04869	543.1	601.5	2.012
90	0.06226	564.9	627.2	2.114	0.05075	561.8	622.7	2.071
100	0.06456	583.7	648.3	2.172	0.05275	580.9	644.2	2.129
110	0.06681	603.0	669.8	2.228	0.05470	600.4	666.0	2.187
120	0.06903	622.6	691.6	2.284	0.05662	620.1	688.0	2.244
130	0.07122	642.5	713.7	2.340	0.05851	640.1	710.3	2.300
140	0.07338	662.8	736.2	2.395	0.06037	660.6	733.0	2.355
	p =	$= 14.0 \text{ ba}$ $(T_{\text{sat}} = 4)$	r = 1.4 M 40.97°C)	MPa			ur = 1.6 (46.89°C)	
Sat.	0.03231	465.2	510.4	1.714	0.02790	470.4	515.0	1.710
50	0.03446	482.6	530.8	1.778	0.02861	476.7	522.5	1.733
60	0.03664	501.6	552.9	1.845	0.03075	496.6	545.8	1.804
70	0.03869	520.4	574.6	1.909	0.03270	516.2	568.5	1.871
80	0.04063	539.4	596.3	1.972	0.03453	535.7	590.9	1.935
90	0.04249	558.6	618.1	2.033	0.03626	555.2	613.2	1.997
100	0.04429	577.9	639.9	2.092	0.03792	574.8	635.5	2.058
110	0.04604	597.5	662.0	2.150	0.03952	594.7	657.9	2.117
120	0.04774	617.5	684.3	2.208	0.04107	614.8	680.5	2.176
130	0.04942	637.7	706.9	2.265	0.04259	635.3	703.4	2.233
140	0.05106	658.3	729.8	2.321	0.04407	656.0	726.5	2.290
150	0.05268	679.2	753.0	2.376	0.04553	677.1	749.9	2.346
160	0.05428	700.5	776.5	2.431	0.04696	698.5	773.6	2.401
	<i>p</i> =	= 18.0 ba $(T_{\text{sat}} = 3.0)$	$r = 1.8 \text{ M}$ $52.30^{\circ}\text{C}$	MPa			$ar = 2.0^{\circ}$ 57.27°C)	
Sat. 60 70	0.02441 0.02606 0.02798	474.9 491.1 511.4	518.8 538.0 561.8	1.705 1.763 1.834	0.02157 0.02216 0.02412	478.7 484.8 506.3	521.8 529.1 554.5	1.700 1.722 1.797
80	0.02974	531.6	585.1	1.901	0.02585	527.1	578.8	1.867
90	0.03138	551.5	608.0	1.965	0.02744	547.6	602.5	1.933
100	0.03293	571.5	630.8	2.027	0.02892	568.1	625.9	1.997
110	0.03443	591.7	653.7	2.087	0.03033	588.5	649.2	2.059
120	0.03586	612.1	676.6	2.146	0.03169	609.2	672.6	2.119
130	0.03726	632.7	699.8	2.204	0.03299	630.0	696.0	2.178
140	0.03863	653.6	723.1	2.262	0.03426	651.2	719.7	2.236
150	0.03996	674.8	746.7	2.318	0.03550	672.5	743.5	2.293
160	0.04127	696.3	770.6	2.374	0.03671	694.2	767.6	2.349
170	0.04256	718.2	794.8	2.429	0.03790	716.2	792.0	2.404
180	0.04383	740.4	819.3	2.484	0.03907	738.5	816.6	2.459

 TABLE A-18 (Continued)

IABLI	E A-18 (C	опппиеа	()						
<i>T</i> °C	v m³/kg	и kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K	v m³/k	g k	и J/kg	<i>h</i> kJ/kg	s kJ/kg · K
	<i>p</i> =	= 22.0  ba $(T_{\text{sat}} = 0.0)$	r = 2.2 M 61.90°C)	MPa		•		ar = 2.4 66.21°C)	
Sat. 70 80	0.01921 0.02086 0.02261	481.8 500.5 522.4	524.0 546.4 572.1	1.695 1.761 1.834	0.017 0.018 0.019	02 4	84.3 93.7 17.0	525.6 536.9 564.6	1.688 1.722 1.801
90 100 110	0.02417 0.02561 0.02697	543.5 564.5 585.3	596.7 620.8 644.6	1.903 1.969 2.032	0.021 0.022 0.024	83 5	39.0 60.6 81.9	590.4 615.4 639.8	1.873 1.941 2.006
120 130 140	0.02826 0.02949 0.03069	606.2 627.3 648.6	668.4 692.2 716.1	2.093 2.153 2.211	0.025 0.026 0.027	56 6	03.2 24.6 46.0	664.1 688.3 712.5	2.068 2.129 2.188
150 160 170 180	0.03185 0.03298 0.03409 0.03517	670.1 691.9 714.1 736.5	740.2 764.5 789.1 813.9	2.269 2.326 2.382 2.437	0.028 0.029 0.030 0.031	86   6 91   7	67.8 89.7 11.9 34.5	736.9 761.4 786.1 811.1	2.247 2.304 2.360 2.416
	<i>p</i> =	$= 26.0 \text{ ba}$ $(T_{\text{sat}} = 7)$	r = 2.6  M $70.27^{\circ}\text{C}$	MPa				ar = 3.0 77.72°C)	
Sat. 80 90	0.01549 0.01742 0.01903	486.2 511.0 534.2	526.5 556.3 583.7	1.681 1.767 1.844	0.012 0.013 0.015	18 4	88.2 95.4 22.8	526.0 534.9 568.0	1.664 1.689 1.782
100 110 120	0.02045 0.02174 0.02294	556.4 578.3 600.0	609.6 634.8 659.6	1.914 1.981 2.045	0.016 0.017 0.018	83 5	47.2 70.4 93.0	596.8 623.9 650.0	1.860 1.932 1.999
130 140 150	0.02408 0.02516 0.02621	621.6 643.4 665.3	684.2 708.8 733.4	2.106 2.167 2.226	0.020 0.021 0.022	09 6	15.4 37.7 60.1	675.6 701.0 726.3	2.063 2.126 2.186
160 170 180 190	0.02723 0.02821 0.02918 0.03012	687.4 709.9 732.5 755.5	758.2 783.2 808.4 833.8	2.283 2.340 2.397 2.452	0.023 0.023 0.024 0.025	90   79 78   73	82.6 05.4 28.3 51.5	751.6 777.1 802.6 828.4	2.245 2.303 2.360 2.417
	<i>p</i> =	$35.0 \text{ ba}$ $(T_{\text{sat}} = 8)$	r = 3.5 M 86.01°C)	MPa				ar = 4.0 93.38°C)	
Sat. 90 100	0.00977 0.01086 0.01270	486.3 502.4 532.9	520.5 540.5 577.3	1.633 1.688 1.788	0.007		74.7 12.1	503.3 549.7	1.574 1.700
110 120 130	0.01270 0.01408 0.01526 0.01631	558.9 583.4 607.0	608.2 636.8 664.1	1.870 1.944 2.012	0.012 0.013	10 5 37 5	44.7 72.1 97.4	589.1 621.6 651.2	1.804 1.887 1.962
140 150 160	0.01728 0.01819 0.01906	630.2 653.3 676.4	690.7 717.0 743.1	2.077 2.140 2.201	0.014 0.015 0.016	27   6-	21.9 45.9 69.7	679.5 707.0 734.1	2.031 2.097 2.160
170 180 190 200	0.01989 0.02068 0.02146 0.02221	699.6 722.9 746.5 770.3	769.2 795.3 821.6 848.0	2.261 2.319 2.376 2.433	0.016 0.017 0.018 0.019	61 7 33 7	93.4 17.3 41.2 65.3	760.9 787.7 814.5 841.4	2.222 2.281 2.340 2.397

**TABLE A-19** Properties of Selected Solids and Liquids:  $c_p$ ,  $\rho$ , and  $\kappa$ 

	Specific	Density,	Thermal
	Heat, $c_p$	ρ	Conductivity, κ
Substance	(kJ/kg·K)	$(kg/m^3)$	$(W/m \cdot K)$
Selected Solids, 300K			
Aluminium	0.903	2700	237
Coal, anthracite	1.260	1350	0.26
Copper	0.385	8930	401
Granite	0.775	2630	2.79
Iron	0.447	7870	80.2
Lead	0.129	11300	35.3
Sand	0.800	1520	0.27
Silver	0.235	10500	429
Soil	1.840	2050	0.52
Steel (AISI 302)	0.480	8060	15.1
Tin	0.227	7310	66.6
Building Materials, 300K			
Brick, common	0.835	1920	0.72
Concrete (stone mix)	0.880	2300	1.4
Glass, plate	0.750	2500	1.4
Hardboard, siding	1.170	640	0.094
Limestone	0.810	2320	2.15
Plywood	1.220	545	0.12
Softwoods (fir, pine)	1.380	510	0.12
Insulating Materials, 300K			
Blanket (glass fiber)	<u> </u>	16	0.046
Cork	1.800	120	0.039
Duct liner (glass fiber, coated)	0.835	32	0.038
Polystyrene (extruded)	1.210	55	0.027
Vermiculite fill (flakes)	0.835	80	0.068
Saturated Liquids			
Ammonia, 300K	4.818	599.8	0.465
Mercury, 300K	0.139	13529	8.540
Refrigerant 22, 300K	1.267	1183.1	0.085
Refrigerant 134a, 300K	1.434	1199.7	0.081
Unused Engine Oil, 300K	1.909	884.1	0.145
Water, 275K	4.211	999.9	0.574
300K	4.179	996.5	0.613
325K	4.182	987.1	0.645
350K	4.195	973.5	0.668
375K	4.220	956.8	0.681
400K	4.256	937.4	0.688

*Source:* Drawn from several sources, these data are only representative. Values can vary depending on temperature, purity, moisture content, and other factors.

 Cable A-20

**TABLE A-20** Ideal Gas Specific Heats of Some Common Gases  $(kJ/kg \cdot K)$ 

	A 20 .	dear Gas	Specific	ricats or	Joine Co.	iiiiiioii G	ises (KJ/Kg	IX)		
	$c_p$	$c_v$	k	$c_p$	$c_v$	k	$c_p$	$c_v$	k	
Temp.										Temp.
K		Air		N	itrogen, I	$N_2$	C	Oxygen, O <sub>2</sub>		K
250	1.003	0.716	1.401	1.039	0.742	1.400	0.913	0.653	1.398	250
300	1.005	0.718	1.400	1.039	0.743	1.400	0.918	0.658	1.395	300
350	1.008	0.721	1.398	1.041	0.744	1.399	0.928	0.668	1.389	350
400	1.013	0.726	1.395	1.044	0.747	1.397	0.941	0.681	1.382	400
450 500	1.020 1.029	0.733 0.742	1.391 1.387	1.049 1.056	0.752 0.759	1.395 1.391	0.956 0.972	0.696 0.712	1.373 1.365	450 500
550 600	1.040 1.051	0.753 0.764	1.381 1.376	1.065 1.075	0.768 0.778	1.387 1.382	0.988 1.003	0.728 0.743	1.358 1.350	550 600
650	1.063	0.764	1.370	1.075	0.778	1.376	1.003	0.743	1.343	650
700	1.075	0.788	1.364	1.098	0.801	1.371	1.031	0.771	1.337	700
750 750	1.073	0.788	1.354	1.110	0.801	1.365	1.031	0.771	1.337	750
800	1.099	0.812	1.354	1.121	0.825	1.360	1.054	0.794	1.327	800
900	1.121	0.834	1.344	1.145	0.849	1.349	1.074	0.814	1.319	900
1000	1.142	0.855	1.336	1.167	0.870	1.341	1.090	0.830	1.313	1000
Temp.		Carbon	1		Carbon					Temp.
K	D	ioxide, C	$O_2$	Mo	onoxide, (	CO	H	ydrogen, H	$\mathbb{I}_2$	K
250	0.791	0.602	1.314	1.039	0.743	1.400	14.051	9.927	1.416	250
300	0.846	0.657	1.288	1.040	0.744	1.399	14.307	10.183	1.405	300
350	0.895	0.706	1.268	1.043	0.746	1.398	14.427	10.302	1.400	350
400	0.939	0.750	1.252	1.047	0.751	1.395	14.476	10.352	1.398	400
450	0.978	0.790	1.239	1.054	0.757	1.392	14.501	10.377	1.398	450
500	1.014	0.825	1.229	1.063	0.767	1.387	14.513	10.389	1.397	500
550	1.046	0.857	1.220	1.075	0.778	1.382	14.530	10.405	1.396	550
600 650	1.075 1.102	0.886 0.913	1.213 1.207	1.087 1.100	0.790 0.803	1.376 1.370	14.546 14.571	10.422 10.447	1.396 1.395	600 650
700 750	1.126	0.937	1.202	1.113	0.816	1.364	14.604	10.480	1.394	700
800	1.148 1.169	0.959 0.980	1.197 1.193	1.126 1.139	0.829 0.842	1.358 1.353	14.645 14.695	10.521 10.570	1.392 1.390	750 800
900 1000	1.204 1.234	1.015 1.045	1.186 1.181	1.163 1.185	0.866 0.888	1.343 1.335	14.822 14.983	10.698 10.859	1.385 1.380	900 1000
1000	1.237	1.043	1.101	1.105	0.000	1.555	11.703	10.057	1.500	1000

Source: Adapted from K. Wark, Thermodynamics, 4th ed., McGraw-Hill, New York, 1983, as based on "Tables of Thermal Properties of Gases," NBS Circular 564, 1955.

**TABLE A-21** Variation of  $\bar{c}_p$  with Temperature for Selected Ideal Gases

$$\frac{\overline{c}_p}{\overline{R}} = \alpha + \beta T + \gamma T^2 + \delta T^3 + \varepsilon T^4$$

T is in K, equations valid from 300 to 1000 K

Gas	$\alpha$	$eta  imes 10^3$	$\gamma  imes 10^6$	$\delta  imes 10^9$	$\varepsilon \times 10^{12}$
CO	3.710	-1.619	3.692	-2.032	0.240
$CO_2$	2.401	8.735	-6.607	2.002	0
$H_2$	3.057	2.677	-5.810	5.521	-1.812
$H_2O$	4.070	-1.108	4.152	-2.964	0.807
$O_2$	3.626	-1.878	7.055	-6.764	2.156
$N_2$	3.675	-1.208	2.324	-0.632	-0.226
Air	3.653	-1.337	3.294	-1.913	0.2763
$SO_2$	3.267	5.324	0.684	-5.281	2.559
$CH_4$	3.826	-3.979	24.558	-22.733	6.963
$C_2H_2$	1.410	19.057	-24.501	16.391	-4.135
$C_2H_4$	1.426	11.383	7.989	-16.254	6.749
Monatomic					
gases <sup>a</sup>	2.5	0	0	0	0

 $<sup>^</sup>a$ For monatomic gases, such as He, Ne, and Ar,  $\bar{c}_p$  is constant over a wide temperature range and is very nearly equal to  $5/2 \overline{R}$ .

Source: Adapted from K. Wark, Thermodynamics, 4th ed., McGraw-Hill, New York, 1983, as based on NASA SP-273, U.S. Government Printing Office, Washington, DC, 1971.

## 756 Tables in SI Units

**TABLE A-22** Ideal Gas Properties of Air

T(K), h and u(kJ/kg),  $s^{\circ}(kJ/kg \cdot K)$ 

				I(K)	n and $u(KJ)$	kg), s (k	J/Kg K)				
				when A	$\Delta s = 0^1$					when $\Delta$	$\Delta s = 0$
T	h	и	$s^{\circ}$	$p_{ m r}$	$v_{\mathrm{r}}$	T	h	и	$s^{\circ}$	$p_{ m r}$	$v_{\mathrm{r}}$
200	199.97	142.56	1.29559	0.3363	1707.	450	451.80	322.62	2.11161	5.775	223.6
210	209.97	149.69	1.34444	0.3987	1512.	460	462.02	329.97	2.13407	6.245	211.4
220	219.97	156.82	1.39105	0.4690	1346.	470	472.24	337.32	2.15604	6.742	200.1
230	230.02	164.00	1.43557	0.5477	1205.	480	482.49	344.70	2.17760	7.268	189.5
240	240.02	171.13	1.47824	0.6355	1084.	490	492.74	352.08	2.19876	7.824	179.7
250	250.05	178.28	1.51917	0.7329	979.	500	503.02	359.49	2.21952	8.411	170.6
260	260.09	185.45	1.55848	0.8405	887.8	510	513.32	366.92	2.23993	9.031	162.1
270	270.11	192.60	1.59634	0.9590	808.0	520	523.63	374.36	2.25997	9.684	154.1
280	280.13	199.75	1.63279	1.0889	738.0	530	533.98	381.84	2.27967	10.37	146.7
285	285.14	203.33	1.65055	1.1584	706.1	540	544.35	389.34	2.29906	11.10	139.7
290	290.16	206.91	1.66802	1.2311	676.1	550	554.74	396.86	2.31809	11.86	133.1
295	295.17	210.49	1.68515	1.3068	647.9	560	565.17	404.42	2.33685	12.66	127.0
300	300.19	214.07	1.70203	1.3860	621.2	570	575.59	411.97	2.35531	13.50	121.2
305	305.22	217.67	1.71865	1.4686	596.0	580	586.04	419.55	2.37348	14.38	115.7
310	310.24	221.25	1.73498	1.5546	572.3	590	596.52	427.15	2.39140	15.31	110.6
315	315.27	224.85	1.75106	1.6442	549.8	600	607.02	434.78	2.40902	16.28	105.8
320	320.29	228.42	1.76690	1.7375	528.6	610	617.53	442.42	2.42644	17.30	101.2
325	325.31	232.02	1.78249	1.8345	508.4	620	628.07	450.09	2.44356	18.36	96.92
330	330.34	235.61	1.79783	1.9352	489.4	630	638.63	457.78	2.46048	19.84	92.84
340	340.42	242.82	1.82790	2.149	454.1	640	649.22	465.50	2.47716	20.64	88.99
350	350.49	250.02	1.85708	2.379	422.2	650	659.84	473.25	2.49364	21.86	85.34
360	360.58	257.24	1.88543	2.626	393.4	660	670.47	481.01	2.50985	23.13	81.89
370	370.67	264.46	1.91313	2.892	367.2	670	681.14	488.81	2.52589	24.46	78.61
380	380.77	271.69	1.94001	3.176	343.4	680	691.82	496.62	2.54175	25.85	75.50
390	390.88	278.93	1.96633	3.481	321.5	690	702.52	504.45	2.55731	27.29	72.56
400	400.98	286.16	1.99194	3.806	301.6	700	713.27	512.33	2.57277	28.80	69.76
410	411.12	293.43	2.01699	4.153	283.3	710	724.04	520.23	2.58810	30.38	67.07
420	421.26	300.69	2.04142	4.522	266.6	720	734.82	528.14	2.60319	32.02	64.53
430	431.43	307.99	2.06533	4.915	251.1	730	745.62	536.07	2.61803	33.72	62.13
440	441.61	315.30	2.08870	5.332	236.8	740	756.44	544.02	2.63280	35.50	59.82

<sup>1.</sup>  $p_{\rm r}$  and  $v_{\rm r}$  data for use with Eqs. 6.43 and 6.44, respectively.

**TABLE A-22** (Continued)

	E A-22 (C	Continuea)		T(V)	1 d/1-I/	1> -9 (1	-I/I IZ)				
					), $h$ and $u(kJ/$	Kg), s' (F	(J/Kg·K)			<u> </u>	
				when	$\Delta s = 0^1$					when	$\Delta s = 0$
T	h	и	$s^{\circ}$	$p_{ m r}$	$v_{\rm r}$	T	h	и	$s^{\circ}$	$p_{ m r}$	$v_{\rm r}$
750 760 770 780 790 800 820	767.29 778.18 789.11 800.03 810.99 821.95 843.98	551.99 560.01 568.07 576.12 584.21 592.30 608.59	2.64737 2.66176 2.67595 2.69013 2.70400 2.71787 2.74504	37.35 39.27 41.31 43.35 45.55 47.75 52.59	57.63 55.54 53.39 51.64 49.86 48.08 44.84	1300 1320 1340 1360 1380 1400 1420	1395.97 1419.76 1443.60 1467.49 1491.44 1515.42 1539.44	1022.82 1040.88 1058.94 1077.10 1095.26 1113.52 1131.77	3.27345 3.29160 3.30959 3.32724 3.34474 3.36200 3.37901	330.9 352.5 375.3 399.1 424.2 450.5 478.0	11.275 10.747 10.247 9.780 9.337 8.919 8.526
840 860 880	866.08 888.27 910.56	624.95 641.40 657.95	2.77170 2.79783 2.82344	57.60 63.09 68.98	41.85 39.12 36.61	1440 1460 1480	1563.51 1587.63 1611.79	1150.13 1168.49 1186.95	3.39586 3.41247 3.42892	506.9 537.1 568.8	8.153 7.801 7.468 7.152
900 920 940 960 980	932.93 955.38 977.92 1000.55 1023.25	674.58 691.28 708.08 725.02 741.98	2.84856 2.87324 2.89748 2.92128 2.94468	75.29 82.05 89.28 97.00 105.2	34.31 32.18 30.22 28.40 26.73	1500 1520 1540 1560 1580	1635.97 1660.23 1684.51 1708.82 1733.17	1205.41 1223.87 1242.43 1260.99 1279.65	3.44516 3.46120 3.47712 3.49276 3.50829	601.9 636.5 672.8 710.5 750.0	6.854 6.569 6.301 6.046
1000 1020 1040 1060 1080	1046.04 1068.89 1091.85 1114.86 1137.89	758.94 776.10 793.36 810.62 827.88	2.96770 2.99034 3.01260 3.03449 3.05608	114.0 123.4 133.3 143.9 155.2	25.17 23.72 22.39 21.14 19.98	1600 1620 1640 1660 1680	1757.57 1782.00 1806.46 1830.96 1855.50	1298.30 1316.96 1335.72 1354.48 1373.24	3.52364 3.53879 3.55381 3.56867 3.58335	791.2 834.1 878.9 925.6 974.2	5.804 5.574 5.355 5.147 4.949
1100 1120 1140 1160 1180	1161.07 1184.28 1207.57 1230.92 1254.34	845.33 862.79 880.35 897.91 915.57	3.07732 3.09825 3.11883 3.13916 3.15916	167.1 179.7 193.1 207.2 222.2	18.896 17.886 16.946 16.064 15.241	1700 1750 1800 1850 1900	1880.1 1941.6 2003.3 2065.3 2127.4	1392.7 1439.8 1487.2 1534.9 1582.6	3.5979 3.6336 3.6684 3.7023 3.7354	1025 1161 1310 1475 1655	4.761 4.328 3.944 3.601 3.295
1200 1220 1240 1260 1280	1277.79 1301.31 1324.93 1348.55 1372.24	933.33 951.09 968.95 986.90 1004.76	3.17888 3.19834 3.21751 3.23638 3.25510	238.0 254.7 272.3 290.8 310.4	14.470 13.747 13.069 12.435 11.835	1950 2000 2050 2100 2150 2200 2250	2189.7 2252.1 2314.6 2377.4 2440.3 2503.2 2566.4	1630.6 1678.7 1726.8 1775.3 1823.8 1872.4 1921.3	3.7677 3.7994 3.8303 3.8605 3.8901 3.9191 3.9474	1852 2068 2303 2559 2837 3138 3464	3.022 2.776 2.555 2.356 2.175 2.012 1.864

Source: Tables A-22 are based on J. H. Keenan and J. Kaye, Gas Tables, Wiley, New York, 1945.

TABLE A-23 Ideal Gas Properties of Selected Gases

		T	0	220	240	250	260	270	280	290 298	300	310	320	330	340	350	360	370	380	390	400	410 420	430	440	450	460	4/0 480	490	500	$\frac{510}{1}$	520	540	550	260	570	580 590
	l <sub>2</sub> nol)	S <sub>o</sub>	0	182.638	185.180	186.370	187.514	188.614	189.673	190.695	191 682	192,638	193.562	194.459	195.328	196.173	196.995	197.794	198.572	199.551	200.071	201,794	202.189	202.863	203.523	204.170	204.803	206.033	206.630	207.216	207.792	208.338	209.461	209.999	210.528	211.049 211.562
	Nitrogen, N <sub>2</sub> $(\bar{h}_{\rm f}^{\circ} = 0 \text{ kJ/kmol})$	<u>n</u>	0	4,562	4,770	5,188	5,396	5,604	5,813	6,021	6779	6.437	6,645	6,853	7,061	7,270	7,478	7,687	7,895	8,104	8,314	8,523	8,943	9,153	9,363	9,574	9,780	10,210	10,423	10,635	10,848	11,062	11,492	11,707	11,923	12,139 12,356
	$(\overline{h}_{\mathrm{f}}^{\circ})$	$\bar{h}$	0	6,391	6.975	7,266	7,558	7,849	8,141	8,432	8 773	9.014	9,306	9,597	9,888	10,180	10,471	10,763	11,055	11,347	11,640	11,932	12,518	12,811	13,105	13,399	13,093	14,285	14,581	14,876	15,172	15,469	16,064	16,363	16,662	16,962 17,262
	lol)	$\bar{s}$	0	196.171	198.696	199.885	201.027	202.128	203.191	204.218	202.232	206.177	207.112	208.020	208.904	209.765	210.604	211.423	212.222	213.002	213.765	215.241	215.955	216.656	217.342	218.016	218.070	219.963	220.589	221.206	221.812	222.997	223.576	224.146	224.708	225.262
	Oxygen, O <sub>2</sub> $(\bar{h}_{\rm f}^{\circ} = 0 \text{ kJ/kmol})$	<u>u</u>	0	4,575	4,782	5,197	5,405	5,613	5,822	6,032	6 242	6.453	6,664	6,877	7,090	7,303	7,518	7,733	7,949	8,166	8,384	8,822	9,043	9,264	9,487	9,710	10.160	10,386	10,614	10,842	11,071	11,501	11,765	11,998	12,232	12,467 12,703
Q	$O \over (\overline{h}_{\mathrm{f}}^{\circ} : \overline{h})$	$\bar{h}$	0	6,404	6,034	7,275	7,566	7,858	8,150	8,443	8 736	9.030	9,325	9,620	9,916	10,213	10,511	10,809	11,109	11,409	11,711	12,012	12,618	12,923	13,228	13,535	13,842	14,460	14,770	15,082	15,395	15,708	16,338	16,654	16,971	17,609
$T(K)$ , $\overline{h}$ and $\overline{u}(kJ/\text{kmol})$ , $\overline{s}^{\circ}(kJ/\text{kmol} \cdot K)$	2O /kmol)	<u>S</u> o	0	178.576	181.471	182.831	184.139	185.399	186.616	187.791	188 928	190.030	191.098	192.136	193.144	194.125	195.081	196.012	196.920	197.807	198.673	200.350	201.160	201.955	202.734	203.497	204.247	205.705	206.413	207.112	207.799	208.475	209.795	210.440	211.075	211.702
$I/\text{kmol}), \overline{s}^{\circ}$	Water Vapor, $H_2O$ $= -241,820 \text{ kJ/kmol})$	<u>n</u>	0	5,466	5,965	6,215	6,466	6,716	6,968	7,219	7 472	7.725	7,978	8,232	8,487	8,742	8,66,8	9,255	9,513	9,771	10,030	10,290	10,813	11,075	11,339	11,603	11,869	12,403	12,671	12,940	13,211	13,482	14,028	14,303	14,579	14,856 15,134
$\overline{h}$ and $\overline{u}(k)$	$\widehat{(\bar{h}_{\rm f}^{\circ} = -}$	$\bar{h}$	0	7,295	7,961	8,294	8,627	8,961	9,296	9,631	9966	10,302	10,639	10,976	11,314	11,652	11,992	12,331	12,672	13,014	13,356	15,099	14,388	14,734	15,080	15,428	16.126	16,477	16,828	17,181	17,534	18,245	18,601	18,959	19,318	19.678
$T(\mathbf{K})$	e, CO I/kmol)	$s_{\circ}$	0	188.683	191,221	192.411	193.554	194.654	195.173	196.735	107 773	198.678	199.603	200.500	201.371	202.217	203.040	203.842	204.622	205.583	206.125	202.830	208.252	208.929	209.593	210.243	210.880	212.117	212.719	213.310	213.890	215.020	215.572	216.115	216.649	217.175
	Carbon Monoxide, CO $\bar{t}_i^{\circ} = -110,530 \text{ kJ/kmol}$	<u>n</u>	0	4,562	4,771	5,188	5,396	5,604	5,812	6,020	6226	6.437	6,645	6,854	7,062	7,271	7,480	7,689	7,899	8,108	8,319	8,329	8,951	9,163	9,375	9,587	9,800	10,228	10,443	10,658	10,874	11,090	11,524	11,743	11,961	12,181
	Carbon $(\overline{h}_{\mathrm{f}}^{\circ} = -$	<u>h</u>	0	6,391	6.975	7,266	7,558	7,849	8,140	8,432	8 773	9,014	9,306	9,597	688,6	10,181	10,473	10,765	11,058	165,11	11,644	12,232	12,526	12,821	13,116	13,412	13,708	14,302	14,600	14,898	15,197	15,497	16,097	16,399	16,701	17,003
	CO <sub>2</sub> //kmol)	$\bar{s}$	0	202.966	205.920	207.337	208.717	210.062	211.376	212.660	213.002	215.146	216.351	217.534	218.694	219.831	220.948	222.044	223.122	281.477	225.225	227.258	228.252	229.230	230.194	231.144	232.080	233.916	234.814	235.700	236.575	238.292	239.135	239.962	240.789	241.602 242.405
	Carbon Dioxide, $CO_2$ f = -393,520  kJ/kmol	<u>u</u>	0	4,772	5.285	5,548	5,817	6,091	6,369	6,651	66030	7.230	7,526	7,826	8,131	8,439	8,752	890'6	9,392	9,718	10,046	10,378	11,053	11,393	11,742	12,091	12,444	13,158	13,521	13,885	14,253	14,622	15,372	15,751	16,131	16,515
	Carbon $(\bar{h}_{\mathrm{f}}^{\circ} = -$	$\bar{h}$	0	6,601	7.280	7,627	7,979	8,335	8,697	9,063	0.73	9.807	10,186	10,570	10,959	11,351	11,748	12,148	12,552	09671	13,372	13,787	14,628	15,054	15,483	15,916	16,331	17,232	17,678	18,126	18,576	19,029	19,945	20,407	20,870	21,337
		T	0	220	240	250	260	270	280	290	300	310	320	330	340	350	360	370	380	390	400	410	430	440	450	460	0/4	490	200	510	520	540 540	550	260	570	280

 TABLE A-23
 (Continued)

		T	009	610	020	640	650	099	029	089	700	710	720	730	/40	750	09/	780	790	800	810	820	840	850	860	0/8	890	006	910	076	940	950	096	970	086 080
	V <sub>2</sub> nod)	S	212.066	212.564	213.541	214.018	214.489	214.954	215.413	215.866 216.314	216.756	217.192	217.624	218.059	218.472	218.889	219.301	219.709	220.512	220.907	221.298	221.684	222.447	222.822	223.194	223.927	224.288	224.647	225.002	225.555	226.047	226.389	226.728	227.064	227.728
	Nitrogen, N <sub>2</sub> $(\bar{h}_{\rm f}^{\circ} = 0 \text{ kJ/kmol})$	<u>n</u>	12,574	12,792	13,011	13,450	13,671	13,892	14,114	14,337 14,560	14.784	15,008	15,234	15,460	15,686	15,913	16,141	16,570	16,830	17,061	17,292	17,524	17,990	18,224	18,459	18,093	19,168	19,407	19,644	19,883	20,122	20,603	20,844	21,086	21,328
	$N_{ m f}$	$\overline{h}$	17,563	17,864	18,100	18,772	19,075	19,380	19,685	19,991 20,297	20.604	20,912	21,220	21,529	21,839	22,149	22,460	23.085	23,398	23,714	24,027	24,342	24,036	25,292	25,610	26.248	26,568	26,890	27,210	750,17	28,178	28,501	28,826	29,151	29,476
	ol)	So	226.346	226.877	227.918	228.429	228.932	229.430	229.920	230.405	231.358	231.827	232.291	232.748	233.201	233.649	234.091	234.328	235.387	235.810	236.230	236.644	237.462	237.864	238.264	239.051	239.439	239.823	240.203	240.580	241.323	241.689	242.052	242.411	242.768 243.120
	Oxygen, O <sub>2</sub> $(\bar{h}_{\rm f}^{\circ} = 0 \text{ kJ/kmol})$	n I	12,940	13,178	13,417	13,898	14,140	14,383	14,626	14,8/1	15.364	15,611	15,859	16,107	16,357	16,607	16,859	17,111	17,618	17,872	18,126	18,382	18,893	19,150	19,408	19,000	20,185	20,445	20,706	70,767	21,491	21,754	22,017	22,280	22,809
\S	$(\overline{h}_{ ext{f}}^{\circ})$	$\bar{h}$	17,929	18,250	18,895	19,219	19,544	19,870	20,197	20,524	21.184	21,514	21,845	22,177	22,510	22,844	23,1/8	23,515	24,186	24,523	24,861	25,199	25,877	26,218	26,559	27.242	27,584	27,928	28,272	28,616	29,306	29,652	29,999	30,345	30,692 31.041
$T({ m K}),  \overline{h}   { m and}   \overline{u}({ m kJ/kmol}),  \overline{s}^{\circ}({ m kJ/kmol} \cdot { m K})$	2O /kmol)	$\bar{s}$	212.920	213.529	214.122	215.285	215.856	216.419	216.976	217.527	218.610	219.142	219.668	220.189	750.707	221.215	221.720	222.221	223.207	223.693	224.174	224.651	225.592	226.057	226.517	227.426	227.875	228.321	228.763	207.677	230.070	230.499	230.924	231.347	232.184
$I/\text{kmol}), \overline{s}^{\circ}$	Water Vapor, $H_2O$ = $-241,820$ kJ/kmol)	<u>u</u>	15,413	15,693	16.257	16,541	16,826	17,112	17,399	17,688	18,268	18,561	18,854	19,148	19,444	19,741	20,039	20,539	20,937	21,245	21,549	21,855	22,470	22,779	23,090	23,402	24,029	24,345	24,662	24,980	25,621	25,943	26,265	26,588	26,913 27,240
, $\overline{h}$ and $\overline{u}(\mathbf{k}$	$\overline{(\bar{h}_{\rm f}^{\circ} = -}$	$\bar{h}$	20,402	20,765	21,130	21,862	22,230	22,600	22,970	23,342	24.088	24,464	24,840	25,218	7,65,52	25,977	26,338	20,741	27,510	27,896	28,284	28,672	29,002	29,846	30,240	30,033	31,429	31,828	32,228	32,029	33,436	33,841	34,247	34,653	35,061 35,472
T(K)	e, CO //kmol)	S <sub>o</sub>	218.204	218.708	219.695	220.179	220.656	221.127	221.592	222.052	222.953	223.396	223.833	224.265	274.692	225.115	225.533	223.947	226.762	227.162	227.559	227.922	228.724	229,106	229,482	230.227	230.593	230.957	231.317	231.074	232.379	232.727	233.072	233.413	234.088
	Carbon Monoxide, CO $\bar{i}_i^\circ = -110,530 \text{ kJ/kmol}$	n _	12,622	12,843	13,289	13,512	13,736	13,962	14,187	14,414 14,641	14.870	15,099	15,328	15,558	15,789	16,022	16,255	16,468	16,957	17,193	17,429	17,665	18,140	18,379	18,617	19.099	19,341	19,583	19,826	20,070	20,559	20,805	21,051	21,298	21,345
	Carbon $(\bar{h}_{\mathrm{f}}^{\circ} = -$	$\overline{h}$	17,611	17,915	18,527	18,833	19,141	19,449	19,758	20,068	20.690	21,002	21,315	21,628	21,943	22,258	22,573	23.208	23,526	23,844	24,164	24,483	25,124	25,446	25,768	26.415	26,740	27,066	27,392	21,119	28,375	28,703	29,033	29,362	29,693 30,024
	CO <sub>2</sub> /kmol)	S	243.199	243.983	245.524	246.282	247.032	247,773	248.507	249.233 249.952	250.663	251.368	252.065	252.755	253.439	254.117	254.787	253,432	256.762	257.408	258.048	258.682	259.934	260.551	261.164	262.371	262.968	263.559	264.146	264.728	265.877	266.444	267.007	267.566	268.119
	Carbon Dioxide, $CO_2$ $f_1^0 = -393,520 \text{ kJ/kmol}$	п	17,291	17,683	18,471	18,869	19,270	19,672	20,078	20,484	21.305	21,719	22,134	22,552	77,677	23,393	718,57	24,242	25,097	25,527	25,959	26,394	27,267	27,706	28,125	29,031	29,476	29,922	30,369	30,818	31,719	32,171	32,625	33,081	33,995
	Carboi $(\overline{h}_{\mathrm{f}}^{\circ} = -$	$\bar{h}$	22,280	22,754	23,709	24,190	24,674	25,160	25,648	26,138	27.125	27,622	28,121	28,622	29,124	29,629	30,135	31 154	31,665	32,179	32,694	33,212	34,251	34,773	35,296	36.347	36,876	37,405	37,935	30,000	39,535	40,070	40,607	41,145	41,685 42,226
		T	009	610	070	640	650	099	670	089	700	710	720	730	/40	750	09/	0//	790	008	810	820	840	850	098	0/8	890	006	910	076	940	950	096	970	086

 TABLE A-23
 (Continued)

						T(K)	), $\overline{h}$ and $\overline{u}(\overline{h})$	$\overline{s}$ (J/kmol), $\overline{s}$	$T(\mathrm{K}), \ \overline{h} \ \mathrm{and} \ \overline{u}(\mathrm{kJ/kmol}), \ \overline{s}^{\circ}(\mathrm{kJ/kmol} \cdot \mathrm{K})$	K)						
	$ \begin{array}{c} \text{Carbc} \\ (\overline{h}_{\mathbf{f}}^{\circ} = - \end{array} $	Carbon Dioxide, $CO_2$ f = -393,520  kJ/kmol	, CO <sub>2</sub> J/kmol)	Carbor $(\overline{h}_{\mathrm{f}}^{\circ} = -$	Carbon Monoxide, CO $\bar{t}_{\rm f}^{\circ} = -110,530 \text{ kJ/kmol})$	le, CO :J/kmol)		Water Vapor, $H_2O$ = $-241,820 \text{ kJ/kmol}$	H <sub>2</sub> O J/kmol)	$(\overline{h}_{\mathrm{f}}^{\circ})$	Oxygen, $O_2$ = 0 kJ/kmol)	(lot	$N_{ m f}$	Nitrogen, $N_2$ $(\overline{h}_{\rm f}^{\circ} = 0 \text{ kJ/kmol})$	t <sub>2</sub> nol)	
T	$\bar{h}$	n .	$\overline{s}_{\circ}$	$\bar{h}$	<u>n</u>	S <sub>o</sub>	$\overline{h}$	_n	$\overline{s}_{\circ}$	$\bar{h}$	n _	So	$\bar{h}$	n n	So	T
1000	42,769	34,455	269.215	30,355	22,041	234.421	35,882	27,568	232.597	31,389	23,075	243.471	30,129	21,815	228.057	1000
1020	43,859	35,378	270.293	31,020	22,540	235.079	36,709	28,228	233.415	32,088	23,607	244.164	30,784	22,304	228.706	1020
1040	44,953	36,306	271.354	31,688	23,041	235.728	37,542	28,895	234.223	32,789	24,142	244.844	31,442	22,795	229.344	1040
1080	47,153	38,174	273.430	33,029	24,049	236.992	39,223	30,243	235.806	34,194	25,214	246.171	32,762	23,782	230.591	1080
1100	48,258	39,112	274.445	33,702	24,557	237.609	40,071	30,925	236.584	34,899	25,753	246.818	33,426	24,280	231.199	1100
1120	49,369	40,057	275.444	34,377	25,065	238.217	40,923	31,611	237.352	35,606	26,294	247.454	34,092	24,780	231.799	1120
1140	50,484	41,006	276.430	35,054	25,575	238.817	41,780	32,301	238.110	36,314	26,836	248.081	34,760	25,282	232.391	1140
1180	52,724	42,913	278.362	36,406	26,602	239.989	43,509	33,698	239.600	37,734	27,923	249.307	36,104	26,291	233.549	1180
1200	53,848	43,871	279.307	37,095	27,118	240.663	44,380	34,403	240.333	38,447	28,469	249.906	36,777	26,799	234.115	1200
1220	54,977	44,834	280.238	37,780	27,637	241.128	45,256	35,112	241.057	39,162	29,018	250.497	37,452	27,308	234.673	1220
1240	50,108	45,799	281.128	38,466	28,420	241.080	46,137 47,032	35,821	241.773	1/8,87	20,268	251.079	38,129	27,819	235.223	1240
1280	58,381	40,708	282.962	39,884	29,201	242.780	47,912	37,270	242.482	40,394	30,670	252.219	39,488	28,845	236.302	1280
1300	59.522	48.713	283.847	40.534	29.725	243.316	48.807	38.000	243.877	42.033	31.224	252.776	40.170	29.361	236.831	1300
1320	999,09	49,691	284.722	41,266	30,251	243.844	49,707	38,732	244.564	42,753	31,778	253.325	40,853	29,878	237.353	1320
1340	61,813	50,672	285.586	41,919	30,778	244.366	50,612	39,470	245.243	43,475	32,334	253.868	41,539	30,398	237.867	1340
1380	62,963 64.116	52.643	286.439	42,613	31,306	244.880	52,434	40,213	245.915	44,198	33,449	254.404 254.932	42,227	30,919	238.878	1360 1380
1400	65.271	53,631	288 106	44.007	32,367	245 889	53,351	41.711	247,241	45.648	34.008	255.454	43.605	31.964	239.375	1400
1420	66,427	54,621	288.934	44,707	32,900	246.385	54,273	42,466	247.895	46,374	34,567	255.968	44,295	32,489	239.865	1420
1440	67,586	55,614	289.743	45,408	33,434	246.876	55,198	43,226	248.543	47,102	35,129	256.475	44,988	33,014	240.350	1440
1460 1480	68,748	56,609	290.542	46,110	33,971 34 508	247.360	56,128	43,989	249.185	47,831	35,692	256.978	45,682	33,543	240.827	1460
1500	71.078	58,606	292.114	47,517	35.046	248.312	57,999	45,528	250.450	49.292	36.821	596.750	47.073	34.601	241.768	1500
1520	72,246	59,609	292.888	48,222	35,584	248.778	58,942	46,304	251.074	50,024	37,387	258.450	47,771	35,133	242.228	1520
1540	73,417	60,613	292.654	48,928	36,124	249.240	59,888	47,084	251.693	50,756	37,952	258.928	48,470	35,665	242.685	1540
1580	76,767	62,630	294.411	49,033 50,344	37,207	249.693 250.147	61,792	47,808	252.303 252.912	52,224	39,088	259.870	49,168	36,197	243.137	1580
1600	76,944	63,741	295.901	51,053	37,750	250.592	62,748	49,445	253.513	52,961	39,658	260.333	50,571	37,268	244.028	1600
1620	78,123	64,653	296.632	51,763	38,293	251.033	63,709	52,240	254.111	53,696	40,227	260.791	51,275	37,806	244.464	1620
1660	80.486	66.592	298.072	53.184	39.382	251.901	04,073 65,643	51.841	255.290	55.172	40,799	261.690	52,686	38.884	245.324	1660
1680	81,670	67,702	298.781	53,895	39,927	252.329	66,614	52,646	255.873	55,912	41,944	262.132	53,393	39,424	245.747	1680
1700	82,856	68,721	299.482	54,609	40,474	252.751	62,589	53,455	256.450	56,652	42,517	262.571	54,099	39,965	246.166	1700
1720 1740	84,043   85,231	69,742   70,764	300.177	55,323 56,039	41,023 41,572	253.169 253.582	68,567 69,550	54,267 55,083	257.022   257.589	57,394 58,136	43,093 43,669	263.005 263.435	54,807 55,516	40,507 41,049	246.580 246.990	1720 1740

 TABLE A-23 (Continued)

	T	1760	1780	1800	1820	1860	1880	1900	1920 1940	1960	1980	2000	2050	2100	2150	2200	2250	2300	2350	2400	2450	2500	2550	2650	2700	2750	2800	2850	2900	2950	3000	3050	3100	3150	3200 3250
[2] (Jon Jon Jon Jon Jon Jon Jon Jon Jon Jon	<u>S</u> 0	247.396	247.798	248.195	248.589	249.365	249.748	250.128	250.502 250.874	251 242	251.607	251.969	252.858	253.726	254.578	255.412	256.227	257.027	257.810	258.580	259.332	260.073	260.799	21222	262.902	263.577	264.241	264.895	265.538	266.170	266.793	267.404	700.897	268.601	269.186 269.763
Nitrogen, N <sub>2</sub>	<u>n</u>	41,594	42,139	42,685	43,231	44,324	44,873	45,423	45,973 46.524	47.075	47,627	48,181	49,567	50,957	52,351	53,749	55,149	56,553	57,958	59,366	60,779	62,195	63,613	66,455	67,880	69,306	70,734	72,163	73,593	75,028	76,464	77,902	/9,341	80,782	82,224 83,668
$(\overline{h}_{\mathrm{f}}^{\circ})$	$\overline{h}$	56,227	56,938	57,651	58,363 59,075	59,790	60,504	61,220	61,936 62.654	63 381	64.090	64,810	66,612	68,417	70,226	72,040	73,856	75,676	77,496	79,320	81,149	82,981	84,814	88 488	90,328	92,171	94,014	95,859	97,705	99,556	101,407	103,260	105,115	106,972	108,830 110,690
ol)	So	263.861	264.283	264.701	265.113	265.925	266.326	266.722	267.115	168 297	268.275	268.655	269.588	270.504	271.399	272.278	273.136	273.981	274.809	275.625	276.424	277.207	277.979	270.72	280.219	280.942	281.654	282.357	283.048	283.728	284.399	285.060	285.713	286.355	286.989 287.614
Oxygen, $O_2$ = 0 kJ/kmol)	n	44,247	44,825	45,405	45,986 46,568	47,151	47,734	48,319	48,904	50.078	50,665	51,253	52,727	54,208	55,697	57,192	58,690	60,193	61,704	63,219	64,742	66,271	67,802	70.883	72,433	73,987	75,546	77,112	78,682	80,258	81,837	83,419	82,009	86,601	88,203 89,804
$(\overline{h}_{\mathrm{f}}^{\circ})$	$\bar{h}$	58,800	59,624	60,371	61,118	62,616	63,365	64,116	64,868	66 374	67.127	67,881	69,772	71,668	73,573	75,484	77,397	79,316	81,243	83,174	85,112	87,057	89,004	97 916	94.881	96,852	98,856	100,808	102,793	104,785	106,780	108,778	110,784	112,795	114,809
(kJ/kmol · ] [20] [7] [7]	So	258.151	258.708	259.262	259.811	260.898	261.436	261.969	262.497 263.022	263 542	264.059	264.571	265.838	267.081	268.301	269.500	270.679	271.839	272.978	274.098	275.201	276.286	277.354	279.107	280,462	281.464	282.453	283.429	284.390	285.338	286.273	287.194	701.887	288.999	289.884 290.756
$\overline{u}$ (kJ/kmol), $\overline{s}$ °(kJ/km) Water Vapor, H <sub>2</sub> O = -241,820 kJ/kmol)	<u>n</u>	55,902	56,723	57,547	58,375	60,042	60,880	61,720	62,564	64 259	65.111	65,965	68,111	70,275	72,454	74,649	76,855	79,076	81,308	83,553	85,811	88,082	90,364	94 958	97.269	99,588	101,917	104,256	106,605	108,959	111,321	113,692	116,072	118,458	120,851 123,250
$T(K)$ , $\overline{h}$ and $\overline{u}(kJ/kmol)$ , $\overline{s}^{\circ}(kJ/kmol \cdot K)$ Water Vapor, $H_2O$ $(\overline{h}_{\mathfrak{f}}^{\circ} = -241,820 \ kJ/kmol)$	$\overline{h}$	70,535	71,523	72,513	74,506	75,506	76,511	77,517	78,527	80 555	81.573	82,593	85,156	87,735	90,330	92,940	95,562	98,199	100,846	103,508	106,183	108,868	111,565	116 991	119,717	122,453	125,198	127,952	130,717	133,486	136,264	139,051	141,846	144,648	147,457 150,272
`` <del>`</del>	<u>S</u> 0	253.991	254.398	254.797	255.194	255.976	256.361	256.743	257.122 257.497	257.868	258.236	258.600	259.494	260.370	261.226	262.065	262.887	263.692	264.480	265.253	266.012	266.755	267.485	202:002	269.596	270.285	270.943	271.602	272.249	272.884	273.508	274.123	2/4.730	275.326	275.914 276.494
Carbon Monoxide, CO $\hat{t}_i^c = -110,530 \text{ kJ/kmo}$	n I	42,123	42,673	43,225	43,778	44,886	45,441	45,997	46,552	47 665	48.221	48,780	50,179	51,584	52,988	54,396	55,809	57,222	58,640	090,09	61,482	62,906	64,335	67,197	68.628	70,066	71,504	72,945	74,383	75,825	77,267	78,715	80,164	81,612	83,061 84,513
$\frac{\text{Carbor}}{(\overline{h}_{\mathbf{f}}^{\circ} = -}$	$\overline{h}$	56,756	57,473	58,191	58,910 59,629	60,351	61,072	61,794	62,516 63,238	63 961	64,684	65,408	67,224	69,044	70,864	72,688	74,516	76,345	78,178	80,015	81,852	83,692	85,537	89.730	91,077	92,930	94,784	96,639	98,495	100,352	102,210	104,073	105,939	107,802	109,667 111,534
CO <sub>2</sub> /kmol)	$\overline{s}$	301.543	302.271	302.884	303.544 304.198	304.845	305.487	306.122	306.751	307 992	308.604	309.210	310.701	312.160	313.589	314.988	316.356	317.695	319.011	320.302	321.566	322.808	324.026	308 308	327.549	328.684	329.800	330.896	331.975	333.037	334.084	335.114	336.126	337.124	338.109 339.069
Carbon Dioxide, CO <sub>2</sub> $\frac{1}{10}$ = -393,520 kJ/kmol)	n I	71,787	72,812	73,840	75,897	76,929	77,962	78,996	80,031	82 105	83.144	84,185	86,791	89,404	92,023	94,648	97,277	99,912	102,552	105,197	107,849	110,504	113,166	118 500	121.172	123,849	126,528	129,212	131,898	134,589	137,283	139,982	147,681	145,385	148,089 150,801
$\operatorname*{Carbo}_{(\overline{h}_{\mathrm{f}}^{\circ}=-}$	$\bar{h}$	86,420	87,612	88,806	90,000	92,394	93,593	94,793	95,995	98 401	90,606	100,804	103,835	106,864	109,898	112,939	115,984	119,035	122,091	125,152	128,219	131,290	134,368	140 533	143,620	146,713	149,808	152,908	156,009	159,117	162,226	165,341	168,456	171,576	174,695
	T	1760	1780	1800	1820	1860	1880	1900	1920	1960	1980	2000	2050	2100	2150	2200	2250	2300	2350	2400	2450	2500	2550	2650	2700	2750	2800	2850	2900	2950	3000	3050	3100	3150	3200 3250

Source: Tables A-23 are based on the JANAF Thermochemical Tables, NSRDS-NBS-37, 1971.

#### 762 Tables in SI Units

TABLE A-24 Constants for the van der Waals, Redlich-Kwong, and Benedict-Webb-Rubin Equations of State

1. van der Waals and Redlich-Kwong: Constants for pressure in bar, specific volume in m³/kmol, and temperature in K

	van der W	/aals	Redlich-Kw	ong
Substance	$\operatorname{bar}\left(\frac{a}{\operatorname{kmol}}\right)^{2}$	$\frac{b}{\text{m}^3}$ kmol	$\operatorname{bar}\left(\frac{a}{\operatorname{m}^{3}}\right)^{2} \operatorname{K}^{1/2}$	$\frac{b}{\text{m}^3}$ kmol
Air	1.368	0.0367	15.989	0.02541
Butane $(C_4H_{10})$	13.86	0.1162	289.55	0.08060
Carbon dioxide (CO <sub>2</sub> )	3.647	0.0428	64.43	0.02963
Carbon monoxide (CO) Methane (CH <sub>4</sub> ) Nitrogen (N <sub>2</sub> )	1.474 2.293 1.366	0.0395 0.0428 0.0386	17.22 32.11 15.53	0.02737 0.02965 0.02677
Oxygen (O <sub>2</sub> )	1.369	0.0317	17.22	0.02197
Propane $(C_3H_8)$	9.349	0.0901	182.23	0.06242
Refrigerant 12	10.49	0.0971	208.59	0.06731
Sulfur dioxide (SO <sub>2</sub> ) Water (H <sub>2</sub> O)	6.883 5.531	0.0569 0.0305	144.80 142.59	0.03945 0.02111

Source: Calculated from critical data.

2. Benedict-Webb-Rubin: Constants for pressure in bar, specific volume in m³/kmol, and temperature in K

Substance	a	A	b	B	c	C	$\alpha$	γ
$C_4H_{10}$	1.9073	10.218	0.039998	0.12436	$3.206 \times 10^{5}$	$1.006 \times 10^{6}$	$1.101 \times 10^{-3}$	0.0340
$CO_2$	0.1386	2.7737	0.007210	0.04991	$1.512 \times 10^4$	$1.404 \times 10^{5}$	$8.47 \times 10^{-5}$	0.00539
CO	0.0371	1.3590	0.002632	0.05454	$1.054 \times 10^{3}$	$8.676 \times 10^{3}$	$1.350 \times 10^{-4}$	0.0060
$CH_4$	0.0501	1.8796	0.003380	0.04260	$2.579 \times 10^{3}$	$2.287 \times 10^{4}$	$1.244 \times 10^{-4}$	0.0060
$N_2$	0.0254	1.0676	0.002328	0.04074	$7.381 \times 10^{2}$	$8.166 \times 10^{3}$	$1.272 \times 10^{-4}$	0.0053

Source: H. W. Cooper and J. C. Goldfrank, Hydrocarbon Processing, 46 (12): 141 (1967).

**TABLE A-25** Thermochemical Properties of Selected Substances at 298K and 1 atm

						Heating	Values
Substance	Formula	Molar Mass, <i>M</i> (kg/kmol)	Enthalpy of Formation, $\bar{h}_{\mathrm{f}}^{\circ}$ (kJ/kmol)	Gibbs Function of Formation, $\overline{g}_{f}^{\circ}$ (kJ/kmol)	Absolute Entropy, $\bar{s}^{\circ}$ (kJ/kmol·K)	Higher, HHV (kJ/kg)	Lower, LHV (kJ/kg)
Carbon Hydrogen Nitrogen Oxygen	$C(s) \\ H_2(g) \\ N_2(g) \\ O_2(g)$	12.01 2.016 28.01 32.00	0 0 0 0	0 0 0 0	5.74 130.57 191.50 205.03	32,770 141,780 —	32,770 119,950 —
Carbon monoxide	$CO(g)$ $CO_2(g)$ $H_2O(g)$ $H_2O(l)$	28.01	-110,530	-137,150	197.54	_	_
Carbon dioxide		44.01	-393,520	-394,380	213.69	_	_
Water		18.02	-241,820	-228,590	188.72	_	_
Water		18.02	-285,830	-237,180	69.95	_	_
Hydrogen peroxide	H <sub>2</sub> O <sub>2</sub> (g)	34.02	-136,310	-105,600	232.63	_	_
Ammonia	NH <sub>3</sub> (g)	17.03	-46,190	-16,590	192.33	_	_
Oxygen	O(g)	16.00	249,170	231,770	160.95	_	_
Hydrogen	H(g)	1.008	218,000	203,290	114.61	_	_
Nitrogen Hydroxyl Methane Acetylene	$N(g)$ $OH(g)$ $CH_4(g)$ $C_2H_2(g)$	14.01 17.01 16.04 26.04	472,680 39,460 -74,850 226,730	455,510 34,280 -50,790 209,170	153.19 183.75 186.16 200.85	  55,510 49,910	50,020 48,220
Ethylene	$C_2H_2(g)$	28.05	52,280	68,120	219.83	50,300	47,160
Ethane	$C_2H_6(g)$	30.07	-84,680	-32,890	229.49	51,870	47,480
Propylene	$C_3H_6(g)$	42.08	20,410	62,720	266.94	48,920	45,780
Propane	$C_3H_8(g)$	44.09	-103,850	-23,490	269.91	50,350	46,360
Butane	$C_4H_{10}(g) \\ C_5H_{12}(g) \\ C_8H_{18}(g) \\ C_8H_{18}(l) \\ C_6H_6(g)$	58.12	-126,150	-15,710	310.03	49,500	45,720
Pentane		72.15	-146,440	-8,200	348.40	49,010	45,350
Octane		114.22	-208,450	17,320	463.67	48,260	44,790
Octane		114.22	-249,910	6,610	360.79	47,900	44,430
Benzene		78.11	82,930	129,660	269.20	42,270	40,580
Methyl alcohol	$CH_3OH(g)$ $CH_3OH(l)$ $C_2H_5OH(g)$ $C_2H_5OH(l)$	32.04	-200,890	-162,140	239.70	23,850	21,110
Methyl alcohol		32.04	-238,810	-166,290	126.80	22,670	19,920
Ethyl alcohol		46.07	-235,310	-168,570	282.59	30,590	27,720
Ethyl alcohol		46.07	-277,690	174,890	160.70	29,670	26,800

Source: Based on JANAF Thermochemical Tables, NSRDS-NBS-37, 1971; Selected Values of Chemical Thermodynamic Properties, NBS Tech. Note 270-3, 1968; and API Research Project 44, Carnegie Press, 1953. Heating values calculated.

**TABLE A-26** Standard Molar Chemical Exergy,  $\overline{\mathbf{e}}^{\,\mathrm{ch}}$  (kJ/kmol), of Selected Substances at 298 K and  $p_0$ 

	1 0		
Substance	Formula	Model I <sup>a</sup>	Model II <sup>b</sup>
Nitrogen	$N_2(g)$	640	720
Oxygen	$O_2(g)$	3,950	3,970
Carbon dioxide	$CO_2(g)$	14,175	19,870
Water	$H_2O(g)$	8,635	9,500
Water	$H_2O(1)$	45	900
Carbon (graphite)	C(s)	404,590	410,260
Hydrogen	$H_2(g)$	235,250	236,100
Sulfur	S(s)	598,160	609,600
Carbon monoxide	CO(g)	269,410	275,100
Sulfur dioxide	$SO_2(g)$	301,940	313,400
Nitrogen monoxide	NO(g)	88,850	88,900
Nitrogen dioxide	$NO_2(g)$	55,565	55,600
Hydrogen sulfide	$H_2S(g)$	799,890	812,000
Ammonia	$NH_3(g)$	336,685	337,900
Methane	$CH_4(g)$	824,350	831,650
Ethane	$C_2H_6(g)$	1,482,035	1,495,840
Methyl alcohol	CH <sub>3</sub> OH(g)	715,070	722,300
Methyl alcohol	CH <sub>3</sub> OH(l)	710,745	718,000
Ethyl alcohol	$C_2H_5OH(g)$	1,348,330	1,363,900
Ethyl alcohol	$C_2H_5OH(1)$	1,342,085	1,357,700

<sup>°</sup>J. Ahrendts, "Die Exergie Chemisch Reaktionsfähiger Systeme," VDI-Forschungsheft, VDI-Verlag, Dusseldorf, 579, 1977. Also see "Reference States," Energy—The International Journal, 5: 667–677, 1980. In Model I,  $p_0=1.019$  atm. This model attempts to impose a criterion that the reference environment be in equilibrium. The reference substances are determined assuming restricted chemical equilibrium for nitric acid and nitrates and unrestricted thermodynamic equilibrium for all other chemical components of the atmosphere, the oceans, and a portion of the Earth's crust. The chemical composition of the gas phase of this model approximates the composition of the natural atmosphere.

 $<sup>^</sup>b$ J. Szargut, D. R. Morris, and F. R. Steward, *Exergy Analysis of Thermal, Chemical, and Metallurgical Processes*, Hemisphere, New York, 1988. In Model II,  $p_0 = 1.0$  atm. In developing this model a reference substance is selected for each chemical element from among substances that contain the element being considered and that are abundantly present in the natural environment, even though the substances are not in completely mutual stable equilibrium. An underlying rationale for this approach is that substances found abundantly in nature have little economic value. On an overall basis, the chemical composition of the exergy reference environment of Model II is closer than Model I to the composition of the natural environment, but the equilibrium criterion is not always satisfied.

**TABLE A-27** Logarithms to the Base 10 of the Equilibrium Constant K

	Degariams to the Base 10 of the Equinorian Constant N										
				lo	$\log_{10} K$						
Temp.				$\frac{1}{2}O_2 + \frac{1}{2}N_2$	$H_2O \leftrightharpoons$	$H_2O \leftrightharpoons$	$CO_2 \leftrightharpoons$	$CO_2 + H_2 \leftrightharpoons$	Temp.		
K	$H_2 \leftrightharpoons 2H$	$O_2 \leftrightharpoons 2O$	$N_2 \leftrightharpoons 2N$	≒ NO	$H_2 + \frac{1}{2}O_2$	$OH + \frac{1}{2}H_2$	$CO + \frac{1}{2}O_2$	$CO + H_2O$	°R		
298	-71.224	-81.208	-159.600	-15.171	-40.048	-46.054	-45.066	-5.018	537		
500	-40.316	-45.880	-92.672	-8.783	-22.886	-26.130	-25.025	-2.139	900		
1000	-17.292	-19.614	-43.056	-4.062	-10.062	-11.280	-10.221	-0.159	1800		
1200	-13.414	-15.208	-34.754	-3.275	-7.899	-8.811	-7.764	+0.135	2160		
1400	-10.630	-12.054	-28.812	-2.712	-6.347	-7.021	-6.014	+0.333	2520		
1600	-8.532	-9.684	-24.350	-2.290	-5.180	-5.677	-4.706	+0.474	2880		
1700	-7.666	-8.706	-22.512	-2.116	-4.699	-5.124	-4.169	+0.530	3060		
1800	-6.896	-7.836	-20.874	-1.962	-4.270	-4.613	-3.693	+0.577	3240		
1900	-6.204	-7.058	-19.410	-1.823	-3.886	-4.190	-3.267	+0.619	3420		
2000	-5.580	-6.356	-18.092	-1.699	-3.540	-3.776	-2.884	+0.656	3600		
2100	-5.016	-5.720	-16.898	-1.586	-3.227	-3.434	-2.539	+0.688	3780		
2200	-4.502	-5.142	-15.810	-1.484	-2.942	-3.091	-2.226	+0.716	3960		
2300	-4.032	-4.614	-14.818	-1.391	-2.682	-2.809	-1.940	+0.742	4140		
2400	-3.600	-4.130	-13.908	-1.305	-2.443	-2.520	-1.679	+0.764	4320		
2500	-3.202	-3.684	-13.070	-1.227	-2.224	-2.270	-1.440	+0.784	4500		
2600	-2.836	-3.272	-12.298	-1.154	-2.021	-2.038	-1.219	+0.802	4680		
2700	-2.494	-2.892	-11.580	-1.087	-1.833	-1.823	-1.015	+0.818	4860		
2800	-2.178	-2.536	-10.914	-1.025	-1.658	-1.624	-0.825	+0.833	5040		
2900	-1.882	-2.206	-10.294	-0.967	-1.495	-1.438	-0.649	+0.846	5220		
3000	-1.606	-1.898	-9.716	-0.913	-1.343	-1.265	-0.485	+0.858	5400		
3100	-1.348	-1.610	-9.174	-0.863	-1.201	-1.103	-0.332	+0.869	5580		
3200	-1.106	-1.340	-8.664	-0.815	-1.067	-0.951	-0.189	+0.878	5760		
3300	-0.878	-1.086	-8.186	-0.771	-0.942	-0.809	-0.054	+0.888	5940		
3400	-0.664	-0.846	-7.736	-0.729	-0.824	-0.674	+0.071	+0.895	6120		
3500	-0.462	-0.620	-7.312	-0.690	-0.712	-0.547	+0.190	+0.902	6300		

Source: Based on data from the JANAF Thermochemical Tables, NSRDS-NBS-37, 1971.

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**TABLE A-1E** Atomic or Molecular Weights and Critical Properties of Some Selected Elements and Compounds

Substance	Chemical Formula	M (lb/lbmol)	<i>T</i> <sub>c</sub> (°R)	p <sub>c</sub> (atm)	$Z_{\rm c} = \frac{p_{\rm c} v_{\rm c}}{RT_{\rm c}}$
Acetylene	C <sub>2</sub> H <sub>2</sub>	26.04	556	62	0.274
Air (equivalent)	—	28.97	239	37.2	0.284
Ammonia	NH <sub>3</sub>	17.03	730	111.3	0.242
Argon	$\begin{array}{c} Ar \\ C_6H_6 \\ C_4H_{10} \end{array}$	39.94	272	47.97	0.290
Benzene		78.11	1013	48.7	0.274
Butane		58.12	765	37.5	0.274
Carbon Carbon dioxide Carbon monoxide	C CO <sub>2</sub> CO	12.01 44.01 28.01	548 239	72.9 34.5	0.276 0.294
Copper Ethane Ethyl alcohol	$Cu \\ C_2H_6 \\ C_2H_5OH$	63.54 30.07 46.07	549 929	48.2 63.0	0.285 0.249
Ethylene	$C_2H_4$ He $H_2$	28.05	510	50.5	0.270
Helium		4.003	9.33	2.26	0.300
Hydrogen		2.016	59.8	12.8	0.304
Methane	$\mathrm{CH_4}$ $\mathrm{CH_3OH}$ $\mathrm{N_2}$	16.04	344	45.8	0.290
Methyl alcohol		32.04	924	78.5	0.220
Nitrogen		28.01	227	33.5	0.291
Octane	$C_8H_{18}$ $O_2$ $C_3H_8$	114.22	1025	24.6	0.258
Oxygen		32.00	278	49.8	0.290
Propane		44.09	666	42.1	0.276
Propylene	C <sub>3</sub> H <sub>6</sub>	42.08	657	45.6	0.276
Refrigerant 12	CCl <sub>2</sub> F <sub>2</sub>	120.92	693	40.6	0.278
Refrigerant 22	CHClF <sub>2</sub>	86.48	665	49.1	0.267
Refrigerant 134a	CF <sub>3</sub> CH <sub>2</sub> F	102.03	673	40.2	0.260
Sulfur dioxide	SO <sub>2</sub>	64.06	775	77.7	0.268
Water	H <sub>2</sub> O	18.02	1165	218.0	0.233

Sources: Adapted from International Critical Tables and L. C. Nelson and E. F. Obert, Generalized Compressibility Charts, Chem. Eng., 617: 203 (1954).

**TABLE A-2E** Properties of Saturated Water (Liquid–Vapor): Temperature Table

		Specific ft <sup>3</sup> /			Energy ı/lb	Btu/lb			Entro Btu/lb		
		Sat.	Sat.	Sat.	Sat.	Sat.		Sat.	Sat.	Sat.	
Temp.	Press.	Liquid	Vapor	Liquid	Vapor	Liquid	Evap.	Vapor	Liquid	Vapor	Temp.
°F	lbf/in. <sup>2</sup>	$v_{ m f}$	$v_{\mathrm{g}}$	$u_{ m f}$	$u_{\rm g}$	$h_{ m f}$	$h_{ m fg}$	$h_{ m g}$	$s_{ m f}$	$s_{\mathrm{g}}$	°F
32	0.0886	0.01602	3305	01	1021.2	01	1075.4	1075.4	00003	2.1870	32
35	0.0999	0.01602	2948	2.99	1022.2	3.00	1073.7	1076.7	0.00607	2.1764	35
40	0.1217	0.01602	2445	8.02	1023.9	8.02	1070.9	1078.9	0.01617	2.1592	40
45	0.1475	0.01602	2037	13.04	1025.5	13.04	1068.1	1081.1	0.02618	2.1423	45
50	0.1780	0.01602	1704	18.06	1027.2	18.06	1065.2	1083.3	0.03607	2.1259	50
52	0.1917	0.01603	1589	20.06	1027.8	20.07	1064.1	1084.2	0.04000	2.1195	52
54	0.2064	0.01603	1482	22.07	1028.5	22.07	1063.0	1085.1	0.04391	2.1131	54
56	0.2219	0.01603	1383	24.08	1029.1	24.08	1061.9	1085.9	0.04781	2.1068	56
58	0.2386	0.01603	1292	26.08	1029.8	26.08	1060.7	1086.8	0.05159	2.1005	58
60	0.2563	0.01604	1207	28.08	1030.4	28.08	1059.6	1087.7	0.05555	2.0943	60
62	0.2751	0.01604	1129	30.09	1031.1	30.09	1058.5	1088.6	0.05940	2.0882	62
64	0.2952	0.01604	1056	32.09	1031.8	32.09	1057.3	1089.4	0.06323	2.0821	64
66	0.3165	0.01604	988.4	34.09	1032.4	34.09	1056.2	1090.3	0.06704	2.0761	66
68	0.3391	0.01605	925.8	36.09	1033.1	36.09	1055.1	1091.2	0.07084	2.0701	68
70	0.3632	0.01605	867.7	38.09	1033.7	38.09	1054.0	1092.0	0.07463	2.0642	70
72	0.3887	0.01606	813.7	40.09	1034.4	40.09	1052.8	1092.9	0.07839	2.0584	72
74	0.4158	0.01606	763.5	42.09	1035.0	42.09	1051.7	1093.8	0.08215	2.0526	74
76	0.4446	0.01606	716.8	44.09	1035.7	44.09	1050.6	1094.7	0.08589	2.0469	76
78	0.4750	0.01607	673.3	46.09	1036.3	46.09	1049.4	1095.5	0.08961	2.0412	78
80	0.5073	0.01607	632.8	48.08	1037.0	48.09	1048.3	1096.4	0.09332	2.0356	80
82	0.5414	0.01608	595.0	50.08	1037.6	50.08	1047.2	1097.3	0.09701	2.0300	82
84	0.5776	0.01608	559.8	52.08	1038.3	52.08	1046.0	1098.1	0.1007	2.0245	84
86	0.6158	0.01609	527.0	54.08	1038.9	54.08	1044.9	1099.0	0.1044	2.0190	86
88	0.6562	0.01609	496.3	56.07	1039.6	56.07	1043.8	1099.9	0.1080	2.0136	88
90	0.6988	0.01610	467.7	58.07	1040.2	58.07	1042.7	1100.7	0.1117	2.0083	90
92	0.7439	0.01611	440.9	60.06	1040.9	60.06	1041.5	1101.6	0.1153	2.0030	92
94	0.7914	0.01611	415.9	62.06	1041.5	62.06	1040.4	1102.4	0.1189	1.9977	94
96	0.8416	0.01612	392.4	64.05	1041.2	64.06	1039.2	1103.3	0.1225	1.9925	96
98	0.8945	0.01612	370.5	66.05	1042.8	66.05	1038.1	1104.2	0.1261	1.9874	98
100	0.9503	0.01613	350.0	68.04	1043.5	68.05	1037.0	1105.0	0.1296	1.9822	100
110	1.276	0.01617	265.1	78.02	1046.7	78.02	1031.3	1109.3	0.1473	1.9574	110
120	1.695	0.01621	203.0	87.99	1049.9	88.00	1025.5	1113.5	0.1647	1.9336	120
130	2.225	0.01625	157.2	97.97	1053.0	97.98	1019.8	1117.8	0.1817	1.9109	130
140	2.892	0.01629	122.9	107.95	1056.2	107.96	1014.0	1121.9	0.1985	1.8892	140
150	3.722	0.01634	97.0	117.95	1059.3	117.96	1008.1	1126.1	0.2150	1.8684	150
160	4.745	0.01640	77.2	127.94	1062.3	127.96	1002.2	1130.1	0.2313	1.8484	160
170	5.996	0.01645	62.0	137.95	1065.4	137.97	996.2	1134.2	0.2473	1.8293	170
180	7.515	0.01651	50.2	147.97	1068.3	147.99	990.2	1138.2	0.2631	1.8109	180
190	9.343	0.01657	41.0	158.00	1071.3	158.03	984.1	1142.1	0.2787	1.7932	190
200	11.529	0.01663	33.6	168.04	1074.2	168.07	977.9	1145.9	0.2940	1.7762	200

**TABLE A-2E** (Continued)

		Specific Volume ft <sup>3</sup> /lb			Energy 1/lb		Enthalpy Btu/lb		Entı Btu/l		
		Sat.	Sat.	Sat.	Sat.	Sat.		Sat.	Sat.	Sat.	
Temp.	Press.	Liquid	Vapor	Liquid	Vapor	Liquid	Evap.	Vapor	Liquid	Vapor	Temp.
°F	lbf/in. <sup>2</sup>	$v_{ m f}$	$v_{\mathrm{g}}$	$u_{ m f}$	$u_{\rm g}$	$h_{ m f}$	$h_{ m fg}$	$h_{\mathrm{g}}$	$s_{ m f}$	$s_{ m g}$	°F
210	14.13	0.01670	27.82	178.1	1077.0	178.1	971.6	1149.7	0.3091	1.7599	210
212	14.70	0.01672	26.80	180.1	1077.6	180.2	970.3	1150.5	0.3121	1.7567	212
220	17.19	0.01677	23.15	188.2	1079.8	188.2	965.3	1153.5	0.3241	1.7441	220
230	20.78	0.01685	19.39	198.3	1082.6	198.3	958.8	1157.1	0.3388	1.7289	230
240	24.97	0.01692	16.33	208.4	1085.3	208.4	952.3	1160.7	0.3534	1.7143	240
250	29.82	0.01700	13.83	218.5	1087.9	218.6	945.6	1164.2	0.3677	1.7001	250
260	35.42	0.01708	11.77	228.6	1090.5	228.8	938.8	1167.6	0.3819	1.6864	260
270	41.85	0.01717	10.07	238.8	1093.0	239.0	932.0	1170.9	0.3960	1.6731	270
280	49.18	0.01726	8.65	249.0	1095.4	249.2	924.9	1174.1	0.4099	1.6602	280
290	57.53	0.01735	7.47	259.3	1097.7	259.4	917.8	1177.2	0.4236	1.6477	290
300	66.98	0.01745	6.472	269.5	1100.0	269.7	910.4	1180.2	0.4372	1.6356	300
310	77.64	0.01745	5.632	279.8	1100.0	280.1	903.0	1183.0	0.4507	1.6238	310
320	89.60	0.01765	4.919	290.1	1104.2	290.4	895.3	1185.8	0.4640	1.6123	320
330	103.00	0.01776	4.312	300.5	1106.2	300.8	887.5	1188.4	0.4772	1.6010	330
340	117.93	0.01787	3.792	310.9	1108.0	311.3	879.5	1190.8	0.4903	1.5901	340
350	134.53	0.01799	3.346	321.4	1109.8	321.8	871.3	1193.1	0.5033	1.5793	350
360	152.92	0.01799	2.961	331.8	1111.4	332.4	862.9	1195.1	0.5162	1.5688	360
370	173.23	0.01811	2.628	342.4	1112.9	343.0	854.2	1193.2	0.5102	1.5585	370
380	195.60	0.01826	2.339	353.0	1114.3	353.6	845.4	1199.0	0.5416	1.5483	380
390	220.2	0.01850	2.087	363.6	1115.6	364.3	836.2	1200.6	0.5542	1.5383	390
400	247.1	0.01864	1.866	374.3	1116.6	375.1	826.8	1202.0	0.5667	1.5284	400
410 420	276.5 308.5	0.01878 0.01894	1.673 1.502	385.0 395.8	1117.6 1118.3	386.0 396.9	817.2	1203.1 1204.1	0.5792 0.5915	1.5187	410 420
430	343.3	0.01894	1.302	406.7	1118.5	407.9	807.2 796.9	1204.1	0.5913	1.5091 1.4995	430
440	381.2	0.01909	1.219	417.6	1119.3	419.0	786.3	1204.8	0.6161	1.4900	440
450	422.1	0.01943	1.1011	428.6	1119.5	430.2	775.4	1205.6	0.6282	1.4806	450
460	466.3	0.01961	0.9961	439.7	1119.6	441.4	764.1	1205.5	0.6404	1.4712	460
470	514.1	0.01980	0.9025	450.9	1119.4	452.8	752.4	1205.2	0.6525	1.4618	470
480 490	565.5 620.7	0.02000 0.02021	0.8187 0.7436	462.2 473.6	1118.9 1118.3	464.3 475.9	740.3 727.8	1204.6 1203.7	0.6646 0.6767	1.4524 1.4430	480 490
490					1110.3						
500	680.0	0.02043	0.6761	485.1	1117.4	487.7	714.8	1202.5	0.6888	1.4335	500
520	811.4	0.02091	0.5605	508.5	1114.8	511.7	687.3	1198.9	0.7130	1.4145	520
540	961.5	0.02145	0.4658	532.6	1111.0	536.4	657.5	1193.8	0.7374	1.3950	540
560	1131.8	0.02207	0.3877	548.4	1105.8	562.0	625.0	1187.0	0.7620	1.3749	560
580	1324.3	0.02278	0.3225	583.1	1098.9	588.6	589.3	1178.0	0.7872	1.3540	580
600	1541.0	0.02363	0.2677	609.9	1090.0	616.7	549.7	1166.4	0.8130	1.3317	600
620	1784.4	0.02465	0.2209	638.3	1078.5	646.4	505.0	1151.4	0.8398	1.3075	620
640	2057.1	0.02593	0.1805	668.7	1063.2	678.6	453.4	1131.9	0.8681	1.2803	640
660	2362	0.02767	0.1446	702.3	1042.3	714.4	391.1	1105.5	0.8990	1.2483	660
680	2705	0.03032	0.1113	741.7	1011.0	756.9	309.8	1066.7	0.9350	1.2068	680
700	3090	0.03666	0.0744	801.7	947.7	822.7	167.5	990.2	0.9902	1.1346	700
705.4	3204	0.05053	0.05053	872.6	872.6	902.5	0	902.5	1.0580	1.0580	705.4

Source: Tables A-2E through A-6E are extracted from J. H. Keenan, F. G. Keyes, P. G. Hill, and J. G. Moore, Steam Tables, Wiley, New York, 1969.

**TABLE A-3E** Properties of Saturated Water (Liquid-Vapor): Pressure Table

			e Volume <sup>3</sup> /lb	Internal Btu	Energy ı/lb		Enthalpy Btu/lb		]	Entropy Btu/lb·°R	1	
Press. lbf/in. <sup>2</sup>	Temp.	Sat. Liquid $v_{ m f}$	Sat. Vapor $v_{\rm g}$	Sat. Liquid $u_{\rm f}$	Sat. Vapor $u_g$	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid $s_{\rm f}$	Evap. $s_{\rm fg}$	Sat. Vapor	Press. lbf/in. <sup>2</sup>
0.4	72.84	0.01606	792.0	40.94	1034.7	40.94	1052.3	1093.3	0.0800	1.9760	2.0559	0.4
0.6	85.19	0.01609	540.0	53.26	1038.7	53.27	1045.4	1098.6	0.1029	1.9184	2.0213	0.6
0.8	94.35	0.01611	411.7	62.41	1041.7	62.41	1040.2	1102.6	0.1195	1.8773	1.9968	0.8
1.0	101.70	0.01614	333.6	69.74	1044.0	69.74	1036.0	1105.8	0.1327	1.8453	1.9779	1.0
1.2	107.88	0.01616	280.9	75.90	1046.0	75.90	1032.5	1108.4	0.1436	1.8190	1.9626	1.2
1.5	115.65	0.01619	227.7	83.65	1048.5	83.65	1028.0	1111.7	0.1571	1.7867	1.9438	1.5
2.0	126.04	0.01623	173.75	94.02	1051.8	94.02	1022.1	1116.1	0.1750	1.7448	1.9198	2.0
3.0	141.43	0.01630	118.72	109.38	1056.6	109.39	1013.1	1122.5	0.2009	1.6852	1.8861	3.0
4.0	152.93	0.01636	90.64	120.88	1060.2	120.89	1006.4	1127.3	0.2198	1.6426	1.8624	4.0
5.0	162.21	0.01641	73.53	130.15	1063.0	130.17	1000.9	1131.0	0.2349	1.6093	1.8441	5.0
6.0 7.0 8.0 9.0	170.03 176.82 182.84 188.26 193.19	0.01645 0.01649 0.01653 0.01656 0.01659	61.98 53.65 47.35 42.41 38.42	137.98 144.78 150.81 156.25 161.20	1065.4 1067.4 1069.2 1070.8 1072.2	138.00 144.80 150.84 156.27 161.23	996.2 992.1 988.4 985.1 982.1	1134.2 1136.9 1139.3 1141.4 1143.3	0.2474 0.2581 0.2675 0.2760 0.2836	1.5819 1.5585 1.5383 1.5203 1.5041	1.8292 1.8167 1.8058 1.7963 1.7877	6.0 7.0 8.0 9.0
14.696	211.99	0.01672	26.80	180.10	1077.6	180.15	970.4	1150.5	0.3121	1.4446	1.7567	14.696
15	213.03	0.01672	26.29	181.14	1077.9	181.19	969.7	1150.9	0.3137	1.4414	1.7551	15
20	227.96	0.01683	20.09	196.19	1082.0	196.26	960.1	1156.4	0.3358	1.3962	1.7320	20
25	240.08	0.01692	16.31	208.44	1085.3	208.52	952.2	1160.7	0.3535	1.3607	1.7142	25
30	250.34	0.01700	13.75	218.84	1088.0	218.93	945.4	1164.3	0.3682	1.3314	1.6996	30
35	259.30	0.01708	11.90	227.93	1090.3	228.04	939.3	1167.4	0.3809	1.3064	1.6873	35
40	267.26	0.01715	10.50	236.03	1092.3	236.16	933.8	1170.0	0.3921	1.2845	1.6767	40
45	274.46	0.01721	9.40	243.37	1094.0	243.51	928.8	1172.3	0.4022	1.2651	1.6673	45
50	281.03	0.01727	8.52	250.08	1095.6	250.24	924.2	1174.4	0.4113	1.2476	1.6589	50
55	287.10	0.01733	7.79	256.28	1097.0	256.46	919.9	1176.3	0.4196	1.2317	1.6513	55
60	292.73	0.01738	7.177	262.1	1098.3	262.2	915.8	1178.0	0.4273	1.2170	1.6443	60
65	298.00	0.01743	6.647	267.5	1099.5	267.7	911.9	1179.6	0.4345	1.2035	1.6380	65
70	302.96	0.01748	6.209	272.6	1100.6	272.8	908.3	1181.0	0.4412	1.1909	1.6321	70
75	307.63	0.01752	5.818	277.4	1101.6	277.6	904.8	1182.4	0.4475	1.1790	1.6265	75
80	312.07	0.01757	5.474	282.0	1102.6	282.2	901.4	1183.6	0.4534	1.1679	1.6213	80
85	316.29	0.01761	5.170	286.3	1103.5	286.6	898.2	1184.8	0.4591	1.1574	1.6165	85
90	320.31	0.01766	4.898	290.5	1104.3	290.8	895.1	1185.9	0.4644	1.1475	1.6119	90
95	324.16	0.01770	4.654	294.5	1105.0	294.8	892.1	1186.9	0.4695	1.1380	1.6075	95
100	327.86	0.01774	4.434	298.3	1105.8	298.6	889.2	1187.8	0.4744	1.1290	1.6034	100
110	334.82	0.01781	4.051	305.5	1107.1	305.9	883.7	1189.6	0.4836	1.1122	1.5958	110
120	341.30	0.01789	3.730	312.3	1108.3	312.7	878.5	1191.1	0.4920	1.0966	1.5886	120
130	347.37	0.01796	3.457	318.6	1109.4	319.0	873.5	1192.5	0.4999	1.0822	1.5821	130
140	353.08	0.01802	3.221	324.6	1110.3	325.1	868.7	1193.8	0.5073	1.0688	1.5761	140
150	358.48	0.01809	3.016	330.2	1111.2	330.8	864.2	1194.9	0.5142	1.0562	1.5704	150
160	363.60	0.01815	2.836	335.6	1112.0	336.2	859.8	1196.0	0.5208	1.0443	1.5651	160

**TABLE A-3E** (Continued)

		Specific ft <sup>3</sup> /		l .	Energy 1/lb		Enthalpy Btu/lb			Entropy Btu/lb·°R		
Press. lbf/in. <sup>2</sup>	Temp.	Sat. Liquid $v_{ m f}$	Sat. Vapor $v_{\rm g}$	Sat. Liquid $u_{\rm f}$	Sat. Vapor $u_{\rm g}$	Sat. Liquid $h_{ m f}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid $s_{\rm f}$	Evap. $s_{\rm fg}$	Sat. Vapor	Press. lbf/in. <sup>2</sup>
170	368.47	0.01821	2.676	340.8	1112.7	341.3	855.6	1196.9	0.5270	1.0330	1.5600	170
180	373.13	0.01827	2.553	345.7	1113.4	346.3	851.5	1197.8	0.5329	1.0223	1.5552	180
190	377.59	0.01833	2.405	350.4	1114.0	351.0	847.5	1198.6	0.5386	1.0122	1.5508	190
200	381.86	0.01839	2.289	354.9	1114.6	355.6	843.7	1199.3	0.5440	1.0025	1.5465	200
250	401.04	0.01865	1.845	375.4	1116.7	376.2	825.8	1202.1	0.5680	0.9594	1.5274	250
300	417.43	0.01890	1.544	393.0	1118.2	394.1	809.8	1203.9	0.5883	0.9232	1.5115	300
350	431.82	0.01912	1.327	408.7	1119.0	409.9	795.0	1204.9	0.6060	0.8917	1.4977	350
400	444.70	0.01934	1.162	422.8	1119.5	424.2	781.2	1205.5	0.6218	0.8638	1.4856	400
450	456.39	0.01955	1.033	435.7	1119.6	437.4	768.2	1205.6	0.6360	0.8385	1.4745	450
500	467.13	0.01975	0.928	447.7	1119.4	449.5	755.8	1205.3	0.6490	0.8154	1.4644	500
550	477.07	0.01994	0.842	458.9	1119.1	460.9	743.9	1204.8	0.6611	0.7941	1.4451	550
600	486.33	0.02013	0.770	469.4	1118.6	471.7	732.4	1204.1	0.6723	0.7742	1.4464	600
700	503.23	0.02051	0.656	488.9	1117.0	491.5	710.5	1202.0	0.6927	0.7378	1.4305	700
800	518.36	0.02087	0.569	506.6	1115.0	509.7	689.6	1199.3	0.7110	0.7050	1.4160	800
900	532.12	0.02123	0.501	523.0	1112.6	526.6	669.5	1196.0	0.7277	0.6750	1.4027	900
1000	544.75	0.02159	0.446	538.4	1109.9	542.4	650.0	1192.4	0.7432	0.6471	1.3903	1000
1100	556.45	0.02195	0.401	552.9	1106.8	557.4	631.0	1188.3	0.7576	0.6209	1.3786	1100
1200	567.37	0.02232	0.362	566.7	1103.5	571.7	612.3	1183.9	0.7712	0.5961	1.3673	1200
1300	577.60	0.02269	0.330	579.9	1099.8	585.4	593.8	1179.2	0.7841	0.5724	1.3565	1300
1400	587.25	0.02307	0.302	592.7	1096.0	598.6	575.5	1174.1	0.7964	0.5497	1.3461	1400
1500	596.39	0.02346	0.277	605.0	1091.8	611.5	557.2	1168.7	0.8082	0.5276	1.3359	1500
1600	605.06	0.02386	0.255	616.9	1087.4	624.0	538.9	1162.9	0.8196	0.5062	1.3258	1600
1700	613.32	0.02428	0.236	628.6	1082.7	636.2	520.6	1156.9	0.8307	0.4852	1.3159	1700
1800	621.21	0.02472	0.218	640.0	1077.7	648.3	502.1	1150.4	0.8414	0.4645	1.3060	1800
1900	628.76	0.02517	0.203	651.3	1072.3	660.1	483.4	1143.5	0.8519	0.4441	1.2961	1900
2000 2250 2500 2750 3000 3203.6	636.00 652.90 668.31 682.46 695.52	0.02565 0.02698 0.02860 0.03077 0.03431 0.05053	0.188 0.157 0.131 0.107 0.084	662.4 689.9 717.7 747.3 783.4 872.6	1066.6 1050.6 1031.0 1005.9 968.8 872.6	671.9 701.1 730.9 763.0 802.5	464.4 414.8 360.5 297.4 213.0	1136.3 1115.9 1091.4 1060.4 1015.5	0.8623 0.8876 0.9131 0.9401 0.9732	0.4238 0.3728 0.3196 0.2604 0.1843	1.2861 1.2604 1.2327 1.2005 1.1575	2000 2250 2500 2750 3000 3203.6

**TABLE A-4E** Properties of Superheated Water Vapor

TABLI	E A-4E	Properties	of Superh	neated Water	Vapor				
<i>T</i> °F	<i>v</i> ft³/lb	u Btu/lb	<i>h</i> Btu/lb	s Btu/lb·°R	f	<i>v</i> t³/lb	и Btu/lb	<i>h</i> Btu/lb	s Btu/lb·°R
		p =	1 lbf/in. <sup>2</sup> = 101.7°F)				p = 1	5 lbf/in. <sup>2</sup> = 162.2°F)	
Sat. 150	333.6 362.6	1044.0 1060.4	1105.8 1127.5	1.9779 2.0151	,	73.53	1063.0	1131.0	1.8441
200	392.5	1077.5	1150.1	2.0508	7	78.15	1076.0	1148.6	1.8715
250 300 400	422.4 452.3 511.9	1094.7 1112.0 1147.0	1172.8 1195.7 1241.8	2.0839 2.1150 2.1720	Ģ	84.21 90.24 02.24	1093.8 1111.3 1146.6	1171.7 1194.8 1241.2	1.9052 1.9367 1.9941
500 600 700	571.5 631.1 690.7	1182.8 1219.3 1256.7	1288.5 1336.1 1384.5	2.2235 2.2706 2.3142	12	14.20 26.15 38.08	1182.5 1219.1 1256.5	1288.2 1335.8 1384.3	2.0458 2.0930 2.1367
800 900 1000	750.3 809.9 869.5	1294.4 1333.9 1373.9	1433.7 1483.8 1534.8	2.3550 2.3932 2.4294	10	50.01 61.94 73.86	1294.7 1333.8 1373.9	1433.5 1483.7 1534.7	2.1775 2.2158 2.2520
					_				
			10 lbf/in. <sup>2</sup> = 193.2°F)					4.7 lbf/in. <sup>2</sup> = 212.0°F)	
Sat. 200	38.42 38.85	1072.2 1074.7	1143.3 1146.6	1.7877 1.7927	-	26.80	1077.6	1150.5	1.7567
250	41.95	1092.6	1170.2	1.8272		28.42	1091.5	1168.8	1.7832
300 400 500	44.99 51.03 57.04	1110.4 1146.1 1182.2	1193.7 1240.5 1287.7	1.8592 1.9171 1.9690	3	30.52 34.67 38.77	1109.6 1145.6 1181.8	1192.6 1239.9 1287.3	1.8157 1.8741 1.9263
600 700 800	63.03 69.01 74.98	1218.9 1256.3 1294.6	1335.5 1384.0 1433.3	2.0164 2.0601 2.1009	4	42.86 46.93 51.00	1218.6 1256.1 1294.4	1335.2 1383.8 1433.1	1.9737 2.0175 2.0584
900 1000 1100	80.95 86.91 92.88	1333.7 1373.8 1414.7	1483.5 1534.6 1586.6	2.1393 2.1755 2.2099		55.07 59.13 63.19	1333.6 1373.7 1414.6	1483.4 1534.5 1586.4	2.0967 2.1330 2.1674
		(	20.11-6/: 2		_		/	10.11-6/: 2	
		$p-2$ $(T_{\text{sat}} =$	20 lbf/in. <sup>2</sup> = 228.0°F)		_		$p = 2$ $(T_{\text{sat}} =$	10 lbf/in. <sup>2</sup> = 267.3°F)	
Sat. 250 300	20.09 20.79 22.36	1082.0 1090.3 1108.7	1156.4 1167.2 1191.5	1.7320 1.7475 1.7805		10.50 11.04	1093.3 1105.1	1170.0 1186.8	1.6767 1.6993
350	23.90	1126.9	1215.4	1.8110		11.84	1124.2	1211.8	1.7312
400 500	25.43 28.46	1145.1 1181.5	1239.2 1286.8	1.8395 1.8919		12.62 14.16	1143.0 1180.1	1236.4 1284.9	1.7606 1.8140
600 700 800	31.47 34.47 37.46	1218.4 1255.9 1294.3	1334.8 1383.5 1432.9	1.9395 1.9834 2.0243		15.69 17.20 18.70	1217.3 1255.1 1293.7	1333.4 1382.4 1432.1	1.8621 1.9063 1.9474
900 1000 1100	40.45 43.44 46.42	1333.5 1373.5 1414.5	1483.2 1534.3 1586.3	2.0627 2.0989 2.1334	2	20.20 21.70 23.20	1333.0 1373.1 1414.2	1482.5 1533.8 1585.9	1.9859 2.0223 2.0568

**TABLE A-4E** (Continued)

IADLE	: A-4E	(Continuea	()					
<i>T</i> °F	<i>v</i> ft³/lb	u Btu/lb	h Btu/lb	s Btu/lb · °R	<i>v</i> ft³/lb	u Btu/lb	<i>h</i> Btu/lb	s Btu/lb · °R
	11 /10		60 lbf/in. <sup>2</sup>	Dtu/10 K	11 /10		30 lbf/in. <sup>2</sup>	Dtu/10 K
			= 292.7°F)				312.1°F)	
Sat.	7.17	1098.3	1178.0	1.6444	5.47	1102.6	1183.6	1.6214
300 350	7.26 7.82	1101.3 1121.4	1181.9 1208.2	1.6496 1.6830	5.80	1118.5	1204.3	1.6476
400	8.35	1140.8	1233.5	1.7134	6.22	1138.5	1230.6	1.6790
500	9.40	1178.6	1283.0	1.7678	7.02	1177.2	1281.1	1.7346
600	10.43	1216.3	1332.1	1.8165	7.79	1215.3	1330.7	1.7838
700 800	11.44 12.45	1254.4 1293.0	1381.4 1431.2	1.8609 1.9022	8.56 9.32	1253.6 1292.4	1380.3 1430.4	1.8285 1.8700
900	13.45	1332.5	1481.8	1.9408	10.08	1332.0	1481.2	1.9087
1000	14.45	1372.7	1533.2	1.9773	10.83	1372.3	1532.6	1.9453
1100 1200	15.45 16.45	1413.8 1455.8	1585.4 1638.5	2.0119 2.0448	11.58 12.33	1413.5 1455.5	1584.9 1638.1	1.9799 2.0130
			<u> </u>	I		l	l	L
			00 lbf/in. <sup>2</sup>				20 lbf/in. <sup>2</sup>	
			= 327.8°F)				341.3°F)	
Sat. 350	4.434 4.592	1105.8 1115.4	1187.8 1200.4	1.6034 1.6191	3.730 3.783	1108.3 1112.2	1191.1 1196.2	1.5886 1.5950
400	4.934	1136.2	1227.5	1.6517	4.079	1133.8	1224.4	1.6288
450	5.265	1156.2	1253.6	1.6812	4.360	1154.3	1251.2	1.6590
500 600	5.587 6.216	1175.7 1214.2	1279.1 1329.3	1.7085 1.7582	4.633 5.164	1174.2 1213.2	1277.1 1327.8	1.6868 1.7371
700	6.834	1252.8	1379.2	1.8033	5.682	1252.0	1378.2	1.7825
800	7.445	1291.8	1429.6	1.8449	6.195	1291.2	1428.7	1.8243
900	8.053	1331.5	1480.5	1.8838	6.703	1330.9	1479.8	1.8633
1000 1100	8.657 9.260	1371.9 1413.1	1532.1 1584.5	1.9204 1.9551	7.208 7.711	1371.5 1412.8	1531.5 1584.0	1.9000 1.9348
1200	9.861	1455.2	1637.7	1.9882	8.213	1454.9	1637.3	1.9679
		$p = 1$ $(T_{\text{sat}} =$	40 lbf/in. <sup>2</sup> = 353.1°F)				60 lbf/in. <sup>2</sup> = 363.6°F)	
Sat.	3.221	1110.3	1193.8	1.5761	2.836	1112.0	1196.0	1.5651
400 450	3.466 3.713	1131.4 1152.4	1221.2 1248.6	1.6088 1.6399	3.007 3.228	1128.8 1150.5	1217.8 1246.1	1.5911 1.6230
500	3.952	1172.7	1275.1	1.6682	3.440	1171.2	1273.0	1.6518
550	4.184	1192.5	1300.9	1.6945	3.646	1191.3	1299.2	1.6785
600	4.412	1212.1	1326.4	1.7191	3.848	1211.1	1325.0	1.7034
700 800	4.860 5.301	1251.2 1290.5	1377.1 1427.9	1.7648 1.8068	4.243 4.631	1250.4 1289.9	1376.0 1427.0	1.7494 1.7916
900	5.739	1330.4	1479.1	1.8459	5.015	1329.9	1478.4	1.8308
1000	6.173	1371.0	1531.0	1.8827	5.397	1370.6	1530.4	1.8677
1100 1200	6.605 7.036	1412.4 1454.6	1583.6 1636.9	1.9176 1.9507	5.776 6.154	1412.1 1454.3	1583.1 1636.5	1.9026 1.9358
1_00		1 .5	1000.7	1.,,,,,	0.10	1 .55	1000.0	1.,,,,,,

 TABLE A-4E
 (Continued)

		Commi	1				1	
<i>T</i> °F	v ft³/lb	и Btu/lb	<i>h</i> Btu/lb	s Btu/lb · °R	v ft³/lb	и Btu/lb	h Btu/lb	s Btu/lb · °R
		p = 1	180 lbf/in. <sup>2</sup>	2		p = 2	200 lbf/in. <sup>2</sup>	2
		$(T_{\rm sat} =$	= 373.1°F	)		(T <sub>sat</sub> =	= 381.8°F	)
Sat.	2.533	1113.4	1197.8	1.5553	2.289	1114.6	1199.3	1.5464
400 450	2.648 2.850	1126.2 1148.5	1214.4 1243.4	1.5749 1.6078	2.361 2.548	1123.5 1146.4	1210.8 1240.7	1.5600 1.5938
500	3.042	1169.6	1270.9	1.6372	2.724	1168.0	1268.8	1.6239
550	3.228	1190.0	1270.9	1.6642	2.724	1188.7	1208.8	1.6512
600	3.409	1210.0	1323.5	1.6893	3.058	1208.9	1322.1	1.6767
700	3.763	1249.6	1374.9	1.7357	3.379	1248.8	1373.8	1.7234
800	4.110	1289.3	1426.2	1.7781	3.693	1288.6	1425.3	1.7660
900	4.453	1329.4	1477.7	1.8174	4.003	1328.9	1477.1	1.8055
1000	4.793	1370.2	1529.8	1.8545	4.310	1369.8	1529.3	1.8425
1100 1200	5.131 5.467	1411.7 1454.0	1582.6 1636.1	1.8894 1.9227	4.615 4.918	1411.4 1453.7	1582.2 1635.7	1.8776 1.9109
1200	3.407	1434.0	1030.1	1.9227	4.710	1433.7	1033.7	1.9109
				,				,
			250 lbf/in. <sup>2</sup> = 401.0°F				300 lbf/in. = 417.4°F	
Sat.	1.845	1116.7	1202.1	1.5274	1.544	1118.2	1203.9	1.5115
450 500	2.002 2.150	1141.1 1163.8	1233.7 1263.3	1.5632 1.5948	1.636 1.766	1135.4 1159.5	1226.2 1257.5	1.5365 1.5701
550 600	2.290 2.426	1185.3 1206.1	1291.3 1318.3	1.6233 1.6494	1.888 2.004	1181.9 1203.2	1286.7 1314.5	1.5997 1.6266
700	2.688	1246.7	1371.1	1.6970	2.227	1244.0	1368.3	1.6751
800	2.943	1287.0	1423.2	1.7301	2.442	1285.4	1421.0	1.7187
900	3.193	1327.6	1475.3	1.7799	2.653	1326.3	1473.6	1.7589
1000	3.440	1368.7	1527.9	1.8172	2.860	1367.7	1526.5	1.7964
1100	3.685	1410.5	1581.0	1.8524	3.066	1409.6	1579.8	1.8317
1200 1300	3.929 4.172	1453.0 1496.3	1634.8 1689.3	1.8858 1.9177	3.270 3.473	1452.2 1495.6	1633.8 1688.4	1.8653 1.8973
				21, 21,		- 13-13		
		n = 3	350 lbf/in. <sup>2</sup>	2		n = /	400 lbf/in. <sup>2</sup>	2
		-	= 431.8°F			1	= 444.7°F	
Sat.	1.327	1119.0	1204.9	1.4978	1.162	1119.5	1205.5	1.4856
450 500	1.373 1.491	1129.2 1154.9	1218.2 1251.5	1.5125 1.5482	1.175 1.284	1122.6 1150.1	1209.5 1245.2	1.4901 1.5282
550 600	1.600 1.703	1178.3 1200.3	1281.9 1310.6	1.5790 1.6068	1.383 1.476	1174.6 1197.3	1277.0 1306.6	1.5605 1.5892
700	1.898	1242.5	1365.4	1.6562	1.650	1240.4	1362.5	1.6397
800	2.085	1283.8	1418.8	1.7004	1.816	1282.1	1416.6	1.6844
900	2.267	1325.0	1471.8	1.7409	1.978	1323.7	1470.1	1.7252
1000	2.446	1366.6	1525.0	1.7787	2.136	1365.5	1523.6	1.7632
1100	2.624	1408.7	1578.6	1.8142	2.292	1407.8	1577.4	1.7989
1200	2.799	1451.5	1632.8	1.8478	2.446	1450.7	1621.8	1.8327
1300	2.974	1495.0	1687.6	1.8799	2.599	1494.3	1686.8	1.8648

**TABLE A-4E** (Continued)

IABLI	E A-4E	(Continu	ea)					
<i>T</i> °F	<i>v</i> ft <sup>3</sup> /lb	u Btu/lb	<i>h</i> Btu/lb	s Btu/lb·°R	<i>v</i> ft <sup>3</sup> /lb	u Btu/lb	<i>h</i> Btu/lb	s Btu/lb·°R
	11 /10		450 lbf/in. <sup>2</sup>		11 / 10		500 lbf/in.	
		$(T_{\rm sat} =$	= 456.4°F)	)		$(T_{\rm sat} =$	= 467.1°F	)
Sat.	1.033	1119.6	1205.6	1.4746	0.928 0.992	1119.4	1205.3	1.4645
500 550	1.123 1.215	1145.1 1170.7	1238.5 1271.9	1.5097 1.5436	1.079	1139.7 1166.7	1231.5 1266.6	1.4923 1.5279
600	1.300	1194.3	1302.5	1.5732	1.158	1191.1	1298.3	1.5585
700 800	1.458 1.608	1238.2 1280.5	1359.6 1414.4	1.6248 1.6701	1.304 1.441	1236.0 1278.8	1356.7 1412.1	1.6112 1.6571
900	1.752	1322.4	1468.3	1.7113	1.572	1321.0	1466.5	1.6987
1000	1.732	1364.4	1522.2	1.7495	1.701	1363.3	1520.7	1.7371
1100	2.034	1406.9	1576.3	1.7853	1.827	1406.0	1575.1	1.7731
1200 1300	2.172 2.308	1450.0 1493.7	1630.8 1685.9	1.8192 1.8515	1.952 2.075	1449.2 1493.1	1629.8 1685.1	1.8072 1.8395
1400	2.444	1538.1	1741.7	1.8823	2.198	1537.6	1741.0	1.8704
		•						
			600 lbf/in. <sup>2</sup> = 486.3°F)				700 lbf/in. = 503.2°F	
Sat.	0.770	1118.6	1204.1	1.4464	0.656	1117.0	1202.0	1.4305
500 550	0.795 0.875	1128.0 1158.2	1216.2 1255.4	1.4592 1.4990	0.728	1149.0	1243.2	1.4723
600	0.946	1184.5	1289.5	1.5320	0.793	1177.5	1280.2	1.5081
700 800	1.073 1.190	1231.5 1275.4	1350.6 1407.6	1.5872 1.6343	0.907 1.011	1226.9 1272.0	1344.4 1402.9	1.5661 1.6145
900	1.302	1318.4	1462.9	1.6766	1.109	1315.6	1402.9	1.6576
1000	1.411	1361.2	1517.8	1.7155	1.204	1358.9	1514.9	1.6970
1100	1.517	1404.2	1572.7	1.7519	1.296	1402.4	1570.2	1.7337
1200 1300	1.622 1.726	1447.7 1491.7	1627.8 1683.4	1.7861 1.8186	1.387 1.476	1446.2 1490.4	1625.8 1681.7	1.7682 1.8009
1400	1.829	1536.5	1739.5	1.8497	1.565	1535.3	1738.1	1.8321
			300 lbf/in. <sup>2</sup> = 518.3°F)				000 lbf/in. <sup>2</sup> = 532.1°F	
Sat.	0.569	1115.0	1199.3	1.4160	0.501	1112.6	1196.0	1.4027
550 600	0.615 0.677	1138.8 1170.1	1229.9 1270.4	1.4469 1.4861	0.527 0.587	1127.5 1162.2	1215.2 1260.0	1.4219 1.4652
650	0.732	1197.2	1305.6	1.5186	0.639	1191.1	1297.5	1.4999
700	0.783	1222.1	1338.0	1.5471	0.686	1217.1	1331.4	1.5297
800	0.876	1268.5	1398.2	1.5969	0.772	1264.9	1393.4	1.5810
900 1000	0.964 1.048	1312.9 1356.7	1455.6 1511.9	1.6408 1.6807	0.851 0.927	1310.1 1354.5	1451.9 1508.9	1.6257 1.6662
1100	1.130	1400.5	1567.8	1.7178	1.001	1398.7	1565.4	1.7036
1200	1.210	1444.6	1623.8	1.7526	1.073	1443.0	1621.7	1.7386
1300 1400	1.289 1.367	1489.1 1534.2	1680.0 1736.6	1.7854 1.8167	1.144 1.214	1487.8 1533.0	1687.3 1735.1	1.7717 1.8031
1.00	1.507	1 1002	1.55.0	1.5107		1000.0	1.55.1	1.0001

 TABLE A-4E
 (Continued)

			1				1	
<i>T</i> °F	<i>v</i> ft³/lb	u Btu/lb	<i>h</i> Btu/lb	s Btu/lb · °R	<i>v</i> ft³/lb	u Btu/lb	h Btu/lb	s Btu/lb · °R
			000 lbf/in.				200 lbf/in	
			= 544.7°F)				= 567.4°F	
Sat.	0.446	1109.0	1192.4	1.3903	0.362	1103.5	1183.9	1.3673
600	0.514	1153.7	1248.8	1.4450	0.402	1134.4	1223.6	1.4054
650	0.564	1184.7	1289.1	1.4822	0.450	1170.9	1270.8	1.4490
700	0.608	1212.0	1324.6	1.5135	0.491	1201.3	1310.2	1.4837
800 900	0.688 0.761	1261.2 1307.3	1388.5 1448.1	1.5665 1.6120	0.562 0.626	1253.7 1301.5	1378.4 1440.4	1.5402 1.5876
1000 1100	0.831 0.898	1352.2 1396.8	1505.9 1562.9	1.6530 1.6908	0.685 0.743	1347.5 1393.0	1499.7 1557.9	1.6297 1.6682
1200	0.898	1441.5	1619.7	1.7261	0.743	1438.3	1615.5	1.7040
1300	1.027	1486.5	1676.5	1.7593	0.853	1483.8	1673.1	1.7377
1400	1.027	1531.9	1733.7	1.7909	0.833	1529.6	1730.7	1.7696
1600	1.215	1624.4	1849.3	1.8499	1.011	1622.6	1847.1	1.8290
		n = 1	400 lbf/in.	2		n = 1	600 lbf/in	2
			= 587.2°F)				= 605.1°F	
Sat.	0.302	1096.0	1174.1	1.3461	0.255	1087.4	1162.9	1.3258
600	0.318	1110.9	1193.1	1.3641				
650	0.367	1155.5	1250.5	1.4171	0.303	1137.8	1227.4	1.3852
700	0.406	1189.6	1294.8	1.4562	0.342	1177.0	1278.1	1.4299
800 900	0.471 0.529	1245.8 1295.6	1367.9 1432.5	1.5168 1.5661	0.403 0.466	1237.7 1289.5	1357.0 1424.4	1.4953 1.5468
1000 1100	0.582 0.632	1342.8 1389.1	1493.5 1552.8	1.6094 1.6487	0.504 0.549	1338.0 1385.2	1487.1 1547.7	1.5913 1.6315
1200	0.681	1435.1	1611.4	1.6851	0.592	1431.8	1607.1	1.6684
1300	0.728	1481.1	1669.6	1.7192	0.634	1478.3	1666.1	1.7029
1400	0.774	1527.2	1727.8	1.7513	0.675	1524.9	1724.8	1.7354
1600	0.865	1620.8	1844.8	1.8111	0.755	1619.0	1842.6	1.7955
		p = 1	800 lbf/in.	2		p = 2	000 lbf/in	2
		-	= 621.2°F)			$(T_{\rm sat} =$	$= 636.0^{\circ} F$	)
Sat.	0.218	1077.7	1150.4	1.3060	0.188	1066.6	1136.3	1.2861
650	0.251	1117.0	1200.4	1.3517	0.206	1091.1	1167.2	1.3141
700	0.291	1163.1	1259.9	1.4042	0.249	1147.7	1239.8	1.3782
750	0.322	1198.6	1305.9	1.4430	0.280	1187.3	1291.1	1.4216
800 900	0.350	1229.1	1345.7	1.4753	0.307	1220.1	1333.8	1.4562
	0.399	1283.2	1416.1	1.5291	0.353	1276.8	1407.6	1.5126
1000	0.443	1333.1	1480.7	1.5749	0.395	1328.1	1474.1	1.5598
1100 1200	0.484 0.524	1381.2 1428.5	1542.5 1602.9	1.6159 1.6534	0.433 0.469	1377.2 1425.2	1537.2 1598.6	1.6017 1.6398
1300	0.561	1475.5	1662.5	1.6883	0.503	1472.7	1659.0	1.6751
1400	0.598	1522.5	1721.8	1.7211	0.503	1520.2	1718.8	1.0731
1600	0.670	1617.2	1840.4	1.7817	0.602	1615.4	1838.2	1.7692

**TABLE A-4E** (Continued)

$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	IABL	E A-4E	(Continue	ι)					
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$									
Sat. 0.1306   1031.0   1091.4   1.2327   0.0840   968.8   1015.5   1.1575   1.700   0.1684   1098.7   1176.6   1.3073   0.0907   1003.9   1058.1   1.1944   1.700   1.1684   1098.7   1176.6   1.3073   0.0907   1003.9   1058.1   1.1944   1.700   0.200   1.15.2   1249.1   1.3686   0.1483   1114.7   1197.1   1.3122   1.300   0.2291   1195.7   1301.7   1.4112   0.1757   1167.6   1265.2   1.3675   1.000   0.309   1315.2   1457.2   1.5262   0.2485   1301.7   1439.6   1.4967   1.4010   0.3090   1315.2   1457.2   1.5262   0.2485   1301.7   1439.6   1.4967   1.100   0.3393   1366.8   1523.8   1.5704   0.2772   1356.2   1510.1   1.5434   1200   0.3696   1416.7   1587.7   1.6101   0.3086   1408.0   1576.6   1.5848   1300   0.3984   1465.7   1650.0   1.6465   0.3285   1458.5   1640.9   1.6224   1400   0.4261   1514.2   1711.3   1.6804   0.3524   1508.1   1703.7   1.6571   1500   0.4531   1562.5   1772.1   1.7123   0.3754   1557.3   1765.7   1.6896   1600   0.4795   1610.8   1832.6   1.7424   0.3978   1606.3   1827.1   1.7201		10,10				10,10			
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$							$(T_{\rm sat} =$	695.5°F)	
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$									
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$									
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	800		1195.7	1301.7	1.4112	0.1757	1167.6	1265.2	1.3675
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	900	0.2712	1259.9	1385.4	1.4752				
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$									
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$									
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$									
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	1400	0.4261	1514.2	1711.3	1.6804	0.3524	1508.1	1703.7	1.6571
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$									
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	1000	0.4793	1010.8	1832.0	1.7424	0.3978	1000.3	1827.1	1.7201
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$									
700         0.0306         759.5         779.3         0.9506         0.0287         742.1         763.4         0.9345           750         0.1046         1058.4         1126.1         1.2440         0.0633         960.7         1007.5         1.1395           800         0.1363         1134.7         1223.0         1.3226         0.1052         1095.0         1172.9         1.2740           900         0.1763         1222.4         1336.5         1.4096         0.1462         1201.5         1309.7         1.3789           1000         0.2066         1287.6         1421.4         1.4699         0.1752         1272.9         1402.6         1.4449           1100         0.2328         1345.2         1496.0         1.5193         0.1995         1333.9         1481.6         1.4973           1200         0.2566         1399.2         1565.3         1.5624         0.2213         1390.1         1553.9         1.5423           1300         0.2787         1451.1         1631.7         1.6012         0.2414         1443.7         1622.4         1.5823           1400         0.2997         1501.9         1696.1         1.6368         0.2603         1495.7         16			p = 35	500 lbf/in. <sup>2</sup>	!		p = 40	000 lbf/in. <sup>2</sup>	2
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$				679.7	0.8630				0.8574
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$									
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$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	1000								1.4449
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$									
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$\begin{array}{c ccccccccccccccccccccccccccccccccccc$									
650         0.0242         653.6         673.3         0.8535         0.0237         649.8         671.0         0.8499           700         0.0278         732.7         755.3         0.9257         0.0271         725.1         749.1         0.9187           750         0.0415         870.8         904.6         1.0513         0.0352         832.6         863.9         1.0154           800         0.0844         1056.5         1125.3         1.2306         0.0668         1011.2         1070.5         1.1827           900         0.1270         1183.7         1287.1         1.3548         0.1109         1164.8         1263.4         1.3310           1000         0.1552         1260.8         1387.2         1.4260         0.1385         1248.3         1317.4         1.4078           1100         0.1784         1324.7         1469.9         1.4809         0.1608         1315.3         1458.1         1.4653           1200         0.1989         1382.8         1544.7         1.5274         0.1802         1375.4         1535.4         1.5133           1300         0.2176         1437.7         1614.9         1.5685         0.1979         1431.7         1607.4 <td>1600</td> <td>0.3395</td> <td>1601.7</td> <td>1831.6</td> <td>1.7010</td> <td>0.2959</td> <td>1597.1</td> <td>1816.1</td> <td>1.6841</td>	1600	0.3395	1601.7	1831.6	1.7010	0.2959	1597.1	1816.1	1.6841
650         0.0242         653.6         673.3         0.8535         0.0237         649.8         671.0         0.8499           700         0.0278         732.7         755.3         0.9257         0.0271         725.1         749.1         0.9187           750         0.0415         870.8         904.6         1.0513         0.0352         832.6         863.9         1.0154           800         0.0844         1056.5         1125.3         1.2306         0.0668         1011.2         1070.5         1.1827           900         0.1270         1183.7         1287.1         1.3548         0.1109         1164.8         1263.4         1.3310           1000         0.1552         1260.8         1387.2         1.4260         0.1385         1248.3         1317.4         1.4078           1100         0.1784         1324.7         1469.9         1.4809         0.1608         1315.3         1458.1         1.4653           1200         0.1989         1382.8         1544.7         1.5274         0.1802         1375.4         1535.4         1.5133           1300         0.2176         1437.7         1614.9         1.5685         0.1979         1431.7         1607.4 <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td>									
700         0.0278         732.7         755.3         0.9257         0.0271         725.1         749.1         0.9187           750         0.0415         870.8         904.6         1.0513         0.0352         832.6         863.9         1.0154           800         0.0844         1056.5         1125.3         1.2306         0.0668         1011.2         1070.5         1.1827           900         0.1270         1183.7         1287.1         1.3548         0.1109         1164.8         1263.4         1.3310           1000         0.1552         1260.8         1387.2         1.4260         0.1385         1248.3         1317.4         1.4078           1100         0.1784         1324.7         1469.9         1.4809         0.1608         1315.3         1458.1         1.4653           1200         0.1989         1382.8         1544.7         1.5274         0.1802         1375.4         1535.4         1.5133           1300         0.2176         1437.7         1614.9         1.5685         0.1979         1431.7         1607.4         1.5555           1400         0.2352         1490.7         1682.3         1.6057         0.2143         1485.7         1676.			p = 44	00 lbf/in. <sup>2</sup>	!		p = 48	300 lbf/in. <sup>2</sup>	2
750         0.0415         870.8         904.6         1.0513         0.0352         832.6         863.9         1.0154           800         0.0844         1056.5         1125.3         1.2306         0.0668         1011.2         1070.5         1.1827           900         0.1270         1183.7         1287.1         1.3548         0.1109         1164.8         1263.4         1.3310           1000         0.1552         1260.8         1387.2         1.4260         0.1385         1248.3         1317.4         1.4078           1100         0.1784         1324.7         1469.9         1.4809         0.1608         1315.3         1458.1         1.4653           1200         0.1989         1382.8         1544.7         1.5274         0.1802         1375.4         1535.4         1.5133           1300         0.2176         1437.7         1614.9         1.5685         0.1979         1431.7         1607.4         1.5555           1400         0.2352         1490.7         1682.3         1.6057         0.2143         1485.7         1676.1         1.5934           1500         0.2520         1542.7         1747.6         1.6399         0.2300         1538.2	650	0.0242	653.6	673.3	0.8535	0.0237	649.8	671.0	0.8499
800         0.0844         1056.5         1125.3         1.2306         0.0668         1011.2         1070.5         1.1827           900         0.1270         1183.7         1287.1         1.3548         0.1109         1164.8         1263.4         1.3310           1000         0.1552         1260.8         1387.2         1.4260         0.1385         1248.3         1317.4         1.4078           1100         0.1784         1324.7         1469.9         1.4809         0.1608         1315.3         1458.1         1.4653           1200         0.1989         1382.8         1544.7         1.5274         0.1802         1375.4         1535.4         1.5133           1300         0.2176         1437.7         1614.9         1.5685         0.1979         1431.7         1607.4         1.5555           1400         0.2352         1490.7         1682.3         1.6057         0.2143         1485.7         1676.1         1.5934           1500         0.2520         1542.7         1747.6         1.6399         0.2300         1538.2         1742.5         1.6282									
900         0.1270         1183.7         1287.1         1.3548         0.1109         1164.8         1263.4         1.3310           1000         0.1552         1260.8         1387.2         1.4260         0.1385         1248.3         1317.4         1.4078           1100         0.1784         1324.7         1469.9         1.4809         0.1608         1315.3         1458.1         1.4653           1200         0.1989         1382.8         1544.7         1.5274         0.1802         1375.4         1535.4         1.5133           1300         0.2176         1437.7         1614.9         1.5685         0.1979         1431.7         1607.4         1.5555           1400         0.2352         1490.7         1682.3         1.6057         0.2143         1485.7         1676.1         1.5934           1500         0.2520         1542.7         1747.6         1.6399         0.2300         1538.2         1742.5         1.6282									
1000         0.1552         1260.8         1387.2         1.4260         0.1385         1248.3         1317.4         1.4078           1100         0.1784         1324.7         1469.9         1.4809         0.1608         1315.3         1458.1         1.4653           1200         0.1989         1382.8         1544.7         1.5274         0.1802         1375.4         1535.4         1.5133           1300         0.2176         1437.7         1614.9         1.5685         0.1979         1431.7         1607.4         1.5555           1400         0.2352         1490.7         1682.3         1.6057         0.2143         1485.7         1676.1         1.5934           1500         0.2520         1542.7         1747.6         1.6399         0.2300         1538.2         1742.5         1.6282									
1200     0.1989     1382.8     1544.7     1.5274     0.1802     1375.4     1535.4     1.5133       1300     0.2176     1437.7     1614.9     1.5685     0.1979     1431.7     1607.4     1.5555       1400     0.2352     1490.7     1682.3     1.6057     0.2143     1485.7     1676.1     1.5934       1500     0.2520     1542.7     1747.6     1.6399     0.2300     1538.2     1742.5     1.6282									
1300     0.2176     1437.7     1614.9     1.5685     0.1979     1431.7     1607.4     1.5555       1400     0.2352     1490.7     1682.3     1.6057     0.2143     1485.7     1676.1     1.5934       1500     0.2520     1542.7     1747.6     1.6399     0.2300     1538.2     1742.5     1.6282									
1400     0.2352     1490.7     1682.3     1.6057     0.2143     1485.7     1676.1     1.5934       1500     0.2520     1542.7     1747.6     1.6399     0.2300     1538.2     1742.5     1.6282									
1500 0.2520 1542.7 1747.6 1.6399 0.2300 1538.2 1742.5 1.6282									

**TABLE A-5E** Properties of Compressed Liquid Water

<i>T</i>	<i>v</i>	u	h	s	<i>v</i>	u	h	s			
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R	ft³∕lb	Btu/lb	Btu/lb	Btu/lb·°R			
	11710	p = 50	0 lbf/in. <sup>2</sup> 467.1°F)	Burio R	11710	$p = 1000 \text{ lbf/in.}^2$ ( $T_{\text{sat}} = 544.7^{\circ}\text{F}$ )					
32	0.015994	0.00	1.49	0.00000	0.015967	0.03	2.99	0.00005			
50	0.015998	18.02	19.50	0.03599	0.015972	17.99	20.94	0.03592			
100	0.016106	67.87	69.36	0.12932	0.016082	67.70	70.68	0.12901			
150	0.016318	117.66	119.17	0.21457	0.016293	117.38	120.40	0.21410			
200	0.016608	167.65	169.19	0.29341	0.016580	167.26	170.32	0.29281			
300	0.017416	268.92	270.53	0.43641	0.017379	268.24	271.46	0.43552			
400 Sat.	0.017410 0.018608 0.019748	373.68 447.70	375.40 449.53	0.56604 0.64904	0.017579 0.018550 0.021591	372.55 538.39	375.98 542.38	0.56472 0.74320			
			00 lbf/in. <sup>2</sup> 596.4°F)				00 lbf/in. <sup>2</sup> 636.0°F)				
32	0.015939	0.05	4.47	0.00007	0.015912	0.06	5.95	0.00008			
50	0.015946	17.95	22.38	0.03584	0.015920	17.91	23.81	0.03575			
100	0.016058	67.53	71.99	0.12870	0.016034	67.37	73.30	0.12839			
150	0.016268	117.10	121.62	0.21364	0.016244	116.83	122.84	0.21318			
200	0.016554	166.87	171.46	0.29221	0.016527	166.49	172.60	0.29162			
300	0.017343	267.58	272.39	0.43463	0.017308	266.93	273.33	0.43376			
400	0.018493	371.45	376.59	0.56343	0.018439	370.38	377.21	0.56216			
500	0.02024	481.8	487.4	0.6853	0.02014	479.8	487.3	0.6832			
Sat.	0.02346	605.0	611.5	0.8082	0.02565	662.4	671.9	0.8623			
			00 lbf/in. <sup>2</sup> 695.5°F)			p = 400	00 lbf/in. <sup>2</sup>				
32	0.015859	0.09	8.90	0.00009	0.015807	0.10	11.80	0.00005			
50	0.015870	17.84	26.65	0.03555	0.015821	17.76	29.47	0.03534			
100	0.015987	67.04	75.91	0.12777	0.015942	66.72	78.52	0.12714			
150	0.016196	116.30	125.29	0.21226	0.016150	115.77	127.73	0.21136			
200	0.016476	165.74	174.89	0.29046	0.016425	165.02	177.18	0.28931			
300	0.017240	265.66	275.23	0.43205	0.017174	264.43	277.15	0.43038			
400 500 Sat.	0.018334 0.019944 0.034310	368.32 476.2 783.5	378.50 487.3 802.5	0.55970 0.6794 0.9732	0.018235 0.019766	366.35 472.9	379.85 487.5	0.55734 0.6758			

 TABLE A-6E
 Properties of Saturated Water (Solid–Vapor): Temperature Table

		Specific Volume ft <sup>3</sup> /lb		Internal Energy Btu/lb			Enthalpy Btu/lb			Entropy Btu/lb·°R		
Temp. °F	Press. lbf/in. <sup>2</sup>	Sat. Solid $v_{\rm i}$	Sat. Vapor $v_{\rm g} \times 10^{-3}$	Sat. Solid $u_{\rm i}$	Subl.	Sat. Vapor $u_{\rm g}$	Sat. Solid $h_{\rm i}$	Subl. $h_{\rm ig}$	Sat. Vapor $h_{\rm g}$	Sat. Solid	Subl.	Sat. Vapor
32.018	.0887	.01747	3.302	-143.34	1164.6	1021.2	-143.34	1218.7	1075.4	292	2.479	2.187
32	.0886	.01747	3.305	-143.35	1164.6	1021.2	-143.35	1218.7	1075.4	292	2.479	2.187
30	.0808	.01747	3.607	-144.35	1164.9	1020.5	-144.35	1218.9	1074.5	294	2.489	2.195
25	.0641	.01746	4.506	-146.84	1165.7	1018.9	-146.84	1219.1	1072.3	299	2.515	2.216
20	.0505	.01745	5.655	-149.31	1166.5	1017.2	-149.31	1219.4	1070.1	304	2.542	2.238
15	.0396	.01745	7.13	-151.75	1167.3	1015.5	-151.75	1219.7	1067.9	309	2.569	2.260
10	.0309	.01744	9.04	-154.17	1168.1	1013.9	-154.17	1219.9	1065.7	314	2.597	2.283
5	.0240	.01743	11.52	-156.56	1168.8	1012.2	-156.56	1220.1	1063.5	320	2.626	2.306
0	.0185	.01743	14.77	-158.93	1169.5	1010.6	-158.93	1220.2	1061.2	325	2.655	2.330
-5	.0142	.01742	19.03	-161.27	1170.2	1008.9	-161.27	1220.3	1059.0	330	2.684	2.354
-10	.0109	.01741	24.66	-163.59	1170.9	1007.3	-163.59	1220.4	1056.8	335	2.714	2.379
-15	.0082	.01740	32.2	-165.89	1171.5	1005.6	-165.89	1220.5	1054.6	340	2.745	2.405
-20	.0062	.01740	42.2	-168.16	1172.1	1003.9	-168.16	1220.6	1052.4	345	2.776	2.431
-25	.0046	.01739	55.7	-170.40	1172.7	1002.3	-170.40	1220.6	1050.2	351	2.808	2.457
-30	.0035	.01738	74.1	-172.63	1173.2	1000.6	-172.63	1220.6	1048.0	356	2.841	2.485
-35 -40	.0026 .0019	.01737 .01737	99.2 133.8	-174.82 $-177.00$	1173.8 1174.3	998.9 997.3	-174.82 $-177.00$	1220.6 1220.6	1045.8 1043.6	361 366	2.874 2.908	2.513 2.542

**TABLE A-7E** Properties of Saturated Refrigerant 22 (Liquid–Vapor): Temperature Table

		Specific ft <sup>3</sup> /		Internal Btu			Enthalpy Btu/lb		Entro Btu/lb		
		Sat.	Sat.	Sat.	Sat.	Sat.		Sat.	Sat.	Sat.	
Temp.	Press.	Liquid	Vapor	Liquid	Vapor	Liquid	Evap.	Vapor	Liquid	Vapor	Temp.
°F	lbf/in. <sup>2</sup>	$v_{ m f}$	$v_{\mathrm{g}}$	$u_{\mathrm{f}}$	$u_{\mathrm{g}}$	$h_{ m f}$	$h_{ m fg}$	$h_{ m g}$	$s_{ m f}$	$s_{\mathrm{g}}$	°F
-80	4.781	0.01090	9.6984	-10.30	87.24	-10.29	106.11	95.82	-0.0257	0.2538	-80
-60	8.834	0.01113	5.4744	-5.20	89.16	-5.18	103.30	98.12	-0.0126	0.2458	-60
-55	10.187	0.01120	4.7933	-3.91	89.64	-3.89	102.58	98.68	-0.0094	0.2441	-55
-50	11.701	0.01126	4.2123	-2.62	90.12	-2.60	101.84	99.24	-0.0063	0.2424	-50
-45	13.387	0.01132	3.7147	-1.33	90.59	-1.30	101.10	99.80	-0.0031	0.2407	-45
-40	15.261	0.01139	3.2869	-0.03	91.07	0.00	100.35	100.35	0.0000	0.2391	-40
-35	17.335	0.01145	2.9176	1.27	91.54	1.31	99.59	100.90	0.0031	0.2376	-35
-30	19.624	0.01152	2.5976	2.58	92.00	2.62	98.82	101.44	0.0061	0.2361	-30
-25	22.142	0.01159	2.3195	3.89	92.47	3.94	98.04	101.98	0.0092	0.2347	-25
-20	24.906	0.01166	2.0768	5.21	92.93	5.26	97.24	102.50	0.0122	0.2334	-20
-15	27.931	0.01173	1.8644	6.53	93.38	6.59	96.43	103.03	0.0152	0.2321	-15
-10	31.233	0.01181	1.6780	7.86	93.84	7.93	95.61	103.54	0.0182	0.2308	-10
-5	34.829	0.01188	1.5138	9.19	94.28	9.27	94.78	104.05	0.0211	0.2296	-5
0	38.734	0.01196	1.3688	10.53	94.73	10.62	93.93	104.55	0.0240	0.2284	0
5	42.967	0.01204	1.2404	11.88	95.17	11.97	93.06	105.04	0.0270	0.2272	5
10	47.545	0.01212	1.1264	13.23	95.60	13.33	92.18	105.52	0.0298	0.2261	10
15	52.486	0.01220	1.0248	14.58	96.03	14.70	91.29	105.99	0.0327	0.2250	15
20	57.808	0.01229	0.9342	15.95	96.45	16.08	90.38	106.45	0.0356	0.2240	20
25	63.529	0.01237	0.8531	17.31	96.87	17.46	89.45	106.90	0.0384	0.2230	25
30	69.668	0.01246	0.7804	18.69	97.28	18.85	88.50	107.35	0.0412	0.2220	30
35	76.245	0.01255	0.7150	20.07	97.68	20.25	87.53	107.78	0.0441	0.2210	35
40	83.278	0.01265	0.6561	21.46	98.08	21.66	86.54	108.20	0.0468	0.2200	40
45	90.787	0.01275	0.6029	22.86	98.47	23.07	85.53	108.60	0.0496	0.2191	45
50	98.792	0.01285	0.5548	24.27	98.84	24.50	84.49	108.99	0.0524	0.2182	50
55	107.31	0.01295	0.5112	25.68	99.22	25.94	83.44	109.37	0.0552	0.2173	55
60	116.37	0.01306	0.4716	27.10	99.58	27.38	82.36	109.74	0.0579	0.2164	60
65	125.98	0.01317	0.4355	28.53	99.93	28.84	81.25	110.09	0.0607	0.2155	65
70	136.18	0.01328	0.4027	29.98	100.27	30.31	80.11	110.42	0.0634	0.2147	70
75	146.97	0.01340	0.3726	31.43	100.60	31.79	78.95	110.74	0.0661	0.2138	75
80	158.38	0.01352	0.3452	32.89	100.92	33.29	77.75	111.04	0.0689	0.2130	80
85	170.44	0.01365	0.3200	34.36	101.22	34.80	76.53	111.32	0.0716	0.2121	85
90	183.16	0.01378	0.2969	35.85	101.51	36.32	75.26	111.58	0.0743	0.2113	90
95	196.57	0.01392	0.2756	37.35	101.79	37.86	73.96	111.82	0.0771	0.2104	95
100	210.69	0.01407	0.2560	38.86	102.05	39.41	72.63	112.04	0.0798	0.2095	100
105	225.54	0.01422	0.2379	40.39	102.29	40.99	71.24	112.23	0.0825	0.2087	105
110	241.15	0.01438	0.2212	41.94	102.52	42.58	69.82	112.40	0.0852	0.2078	110
115	257.55	0.01455	0.2058	43.50	102.72	44.19	68.34	112.53	0.0880	0.2069	115
120	274.75	0.01472	0.1914	45.08	102.90	45.83	66.81	112.64	0.0907	0.2060	120
140	352.17	0.01555	0.1433	51.62	103.36	52.64	60.06	112.70	0.1019	0.2021	140

Source: Tables A-7E through A-9E are calculated based on equations from A. Kamei and S. W. Beyerlein, "A Fundamental Equation for Chlorodifluoromethane (R-22)," *Fluid Phase Equilibria*, Vol. 80, No. 11, 1992, pp. 71–86.

**TABLE A-8E** Properties of Saturated Refrigerant 22 (Liquid–Vapor): Pressure Table

	Specific V ft <sup>3</sup> /lt Sat.			lb Btu/lb			Enthalpy Btu/lb		Entropy Btu/lb·°R		
Press. lbf/in. <sup>2</sup>	Temp. °F	Sat. Liquid $v_{ m f}$	Sat. Vapor $v_{\rm g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor $u_{\rm g}$	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{ m fg}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid s <sub>f</sub>	Sat. Vapor $s_{ m g}$	Press. lbf/in. <sup>2</sup>
5	-78.62	0.01091	9.3014	-9.95	87.37	-9.93	105.92	95.98	-0.0248	0.2532	5
10	-55.66	0.01119	4.8769	-4.08	89.58	-4.06	102.67	98.61	-0.0098	0.2443	10
15	-40.67	0.01138	3.3402	-0.21	91.00	-0.17	100.45	100.28	-0.0004	0.2393	15
20	-29.22	0.01153	2.5518	2.78	92.07	2.83	98.70	101.52	0.0066	0.2359	20
25	-19.84	0.01166	2.0695	5.25	92.94	5.31	97.22	102.52	0.0123	0.2333	25
30	-11.82	0.01178	1.7430	7.38	93.67	7.44	95.91	103.35	0.0171	0.2313	30
35	-4.77	0.01189	1.5068	9.25	94.30	9.33	94.74	104.07	0.0212	0.2295	35
40	1.54	0.01198	1.3277	10.94	94.86	11.03	93.66	104.70	0.0249	0.2280	40
45	7.27	0.01207	1.1870	12.49	95.37	12.59	92.67	105.26	0.0283	0.2267	45
50	12.53	0.01216	1.0735	13.91	95.82	14.03	91.73	105.76	0.0313	0.2256	50
55	17.41	0.01224	0.9799	15.24	96.23	15.36	90.85	106.21	0.0341	0.2245	55
60	21.96	0.01232	0.9014	16.48	96.62	16.62	90.01	106.63	0.0367	0.2236	60
65	26.23	0.01239	0.8345	17.65	96.97	17.80	89.21	107.01	0.0391	0.2227	65
70	30.26	0.01247	0.7768	18.76	97.30	18.92	88.45	107.37	0.0414	0.2219	70
75	34.08	0.01254	0.7265	19.82	97.61	19.99	87.71	107.70	0.0435	0.2212	75
80	37.71	0.01260	0.6823	20.83	97.90	21.01	86.99	108.00	0.0456	0.2205	80
85	41.18	0.01267	0.6431	21.79	98.17	21.99	86.30	108.29	0.0475	0.2198	85
90	44.49	0.01274	0.6081	22.72	98.43	22.93	85.63	108.56	0.0494	0.2192	90
95	47.67	0.01280	0.5766	23.61	98.67	23.84	84.98	108.81	0.0511	0.2186	95
100	50.73	0.01286	0.5482	24.47	98.90	24.71	84.34	109.05	0.0528	0.2181	100
110	56.52	0.01298	0.4988	26.11	99.33	26.37	83.11	109.49	0.0560	0.2170	110
120	61.92	0.01310	0.4573	27.65	99.71	27.94	81.93	109.88	0.0590	0.2161	120
130	67.00	0.01321	0.4220	29.11	100.07	29.43	80.80	110.22	0.0618	0.2152	130
140	71.80	0.01332	0.3915	30.50	100.39	30.84	79.70	110.54	0.0644	0.2144	140
150	76.36	0.01343	0.3649	31.82	100.69	32.20	78.63	110.82	0.0669	0.2136	150
160	80.69	0.01354	0.3416	33.09	100.96	33.49	77.59	111.08	0.0693	0.2128	160
170	84.82	0.01365	0.3208	34.31	101.21	34.74	76.57	111.31	0.0715	0.2121	170
180	88.78	0.01375	0.3023	35.49	101.44	35.95	75.57	111.52	0.0737	0.2115	180
190	92.58	0.01386	0.2857	36.62	101.66	37.11	74.60	111.71	0.0757	0.2108	190
200	96.24	0.01396	0.2706	37.72	101.86	38.24	73.64	111.88	0.0777	0.2102	200
225	104.82	0.01422	0.2386	40.34	102.28	40.93	71.29	112.22	0.0824	0.2087	225
250	112.73	0.01447	0.2126	42.79	102.63	43.46	69.02	112.47	0.0867	0.2073	250
275	120.07	0.01473	0.1912	45.10	102.91	45.85	66.79	112.64	0.0908	0.2060	275
300	126.94	0.01499	0.1732	47.30	103.11	48.14	64.60	112.73	0.0946	0.2047	300
325	133.39	0.01525	0.1577	49.42	103.26	50.33	62.42	112.75	0.0982	0.2034	325
350	139.49	0.01552	0.1444	51.45	103.35	52.46	60.25	112.71	0.1016	0.2022	350

**TABLE A-9E** Properties of Superheated Refrigerant 22 Vapor

	v	и	h	s	v	и	h	S
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R
			5 lbf/in. <sup>2</sup> -78.62°F	)			10 lbf/in. <sup>2</sup> -55.66°F	')
Sat. -70 -60	9.3014 9.5244 9.7823	87.37 88.31 89.43	95.98 97.13 98.48	0.2532 0.2562 0.2596	4.8769	89.58	98.61	0.2443
-50	10.0391	90.55	99.84	0.2630	4.9522	90.23	99.40	0.2462
-40	10.2952	91.69	101.22	0.2663	5.0846	91.39	100.81	0.2496
-30	10.5506	92.84	102.61	0.2696	5.2163	92.57	102.23	0.2530
$-20 \\ -10 \\ 0$	10.8054	94.01	104.01	0.2728	5.3472	93.75	103.65	0.2563
	11.0596	95.19	105.43	0.2760	5.4775	94.95	105.09	0.2595
	11.3133	96.39	106.87	0.2791	5.6073	96.16	106.55	0.2627
10	11.5666	97.60	108.31	0.2822	5.7366	97.39	108.01	0.2658
20	11.8195	98.83	109.77	0.2853	5.8655	98.63	109.49	0.2690
30	12.0720	100.07	111.25	0.2884	5.9941	99.88	110.98	0.2720
40	12.3242	101.33	112.74	0.2914	6.1223	101.15	112.49	0.2751
			5 lbf/in. <sup>2</sup> -40.67°F	)		$p = C$ $(T_{\text{sat}} = C)$	20 lbf/in. <sup>2</sup> -29.22°F	······································
Sat40 -30	3.3402 3.3463 3.4370	91.00 91.08 92.28	100.28 100.38 101.83	0.2393 0.2396 0.2430	2.5518	92.07	101.52	0.2359
$-20 \\ -10 \\ 0$	3.5268	93.49	103.28	0.2463	2.6158	93.21	102.90	0.2391
	3.6160	94.70	104.75	0.2496	2.6846	94.45	104.39	0.2424
	3.7046	95.93	106.22	0.2529	2.7528	95.69	105.89	0.2457
10	3.7927	97.17	107.71	0.2561	2.8204	96.95	107.39	0.2490
20	3.8804	98.43	109.20	0.2592	2.8875	98.22	108.91	0.2522
30	3.9677	99.69	110.71	0.2623	2.9542	99.49	110.43	0.2553
40	4.0546	100.97	112.23	0.2654	3.0205	100.78	111.97	0.2584
50	4.1412	102.26	113.76	0.2684	3.0865	102.09	113.52	0.2615
60	4.2275	103.57	115.31	0.2714	3.1522	103.40	115.08	0.2645
70	4.3136	104.89	116.87	0.2744	3.2176	104.73	116.65	0.2675
			5 lbf/in. <sup>2</sup> -19.84°F	)	_	-	30 lbf/in. <sup>2</sup> -11.82°F	······································
Sat10 0	2.0695	92.94	102.52	0.2333	1.7430	93.67	103.35	0.2313
	2.1252	94.18	104.02	0.2367	1.7518	93.91	103.64	0.2319
	2.1812	95.45	105.54	0.2400	1.7997	95.19	105.19	0.2353
10	2.2365	96.72	107.07	0.2433	1.8470	96.48	106.74	0.2386
20	2.2914	98.00	108.61	0.2466	1.8937	97.78	108.30	0.2419
30	2.3458	99.29	110.15	0.2498	1.9400	99.09	109.86	0.2451
40	2.3998	100.59	111.70	0.2529	1.9858	100.40	111.43	0.2483
50	2.4535	101.91	113.27	0.2560	2.0313	101.73	113.01	0.2514
60	2.5068	103.23	114.84	0.2590	2.0764	103.06	114.60	0.2545
70	2.5599	104.57	116.42	0.2621	2.1213	104.41	116.19	0.2576
80	2.6127	105.92	118.01	0.2650	2.1659	105.77	117.80	0.2606
90	2.6654	107.28	119.62	0.2680	2.2103	107.13	119.41	0.2635
100	2.7178	108.65	121.24	0.2709	2.2545	108.52	121.04	0.2665

**TABLE A-9E** (Continued)

T	υ	и	h	S	υ	и	h	S
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R	ft <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb · °R
			0 lbf/in. <sup>2</sup> = 1.54°F)				50 lbf/in. <sup>2</sup> = 12.53°F)	)
Sat.	1.3277 1.3593	94.86 95.99	104.70 106.06	0.2280 0.2310	1.0735	95.82	105.76	0.2256
20	1.3960	97.33	107.67	0.2343	1.0965	96.85	107.00	0.2282
30	1.4321	98.66	109.27	0.2376	1.1268	98.22	108.65	0.2316
40 50	1.4678 1.5032	100.01 101.35	110.88 112.49	0.2409 0.2441	1.1565 1.1858	99.59 100.97	110.30 111.95	0.2349 0.2382
60	1.5381	102.71	114.10	0.2472	1.2147	102.35	113.60	0.2414
70 80	1.5728 1.6071	104.08 105.45	115.73 117.36	0.2503 0.2534	1.2433 1.2716	103.74 105.13	115.25 116.90	0.2445 0.2476
90	1.6413	106.84	118.99	0.2564	1.2996	106.53	118.57	0.2507
100	1.6752	108.23	120.64	0.2593	1.3274	107.95	120.24	0.2537
110 120	1.7089 1.7424	109.64 111.06	122.30 123.97	0.2623 0.2652	1.3549 1.3823	109.37 110.80	121.91 123.60	0.2567 0.2596
120	1.7424	111.00	123.91	0.2032	1.3623	110.00	123.00	0.2390
			0 lbf/in. <sup>2</sup> 21.96°F)				70 lbf/in. <sup>2</sup> = 30.26°F)	)
Sat.	0.9014	96.62	106.63	0.2236	0.7768	97.30	107.37	0.2219
30 40	0.9226 0.9485	97.75 99.16	108.00 109.70	0.2264 0.2298	0.7994	98.71	109.07	0.2254
50	0.9739	100.57	111.39	0.2332	0.8221	100.15	110.81	0.2288
60	0.9988	101.98	113.07	0.2365	0.8443	101.59	112.53	0.2321
70	1.0234	103.39	114.76	0.2397	0.8660	103.03	114.25	0.2354
80	1.0476	104.80	116.44	0.2428	0.8874	104.46	115.97	0.2386
90 100	1.0716 1.0953	106.22 107.65	118.13 119.82	0.2459 0.2490	0.9086 0.9294	105.90 107.35	117.68 119.40	0.2418 0.2449
110	1.1188	107.03	121.52	0.2490	0.9294	107.33	121.12	0.2449
120	1.1421	110.53	123.22	0.2520	0.9704	110.26	121.12	0.2479
130	1.1653	111.99	124.93	0.2579	0.9907	111.73	124.57	0.2539
140	1.1883	113.45	126.65	0.2608	1.0107	113.21	126.31	0.2568
			0 lbf/in. <sup>2</sup>				90 lbf/in. <sup>2</sup>	
			37.71°F)				= 44.49°F)	
Sat.	0.6823 0.6871	97.90 98.24	108.00 108.42	0.2205 0.2213	0.6081	98.43	108.56	0.2192
50	0.7079	99.72	110.20	0.2248	0.6186	99.26	109.57	0.2212
60	0.7280	101.19	111.97	0.2283	0.6373	100.77	111.39	0.2247
70	0.7478	102.65	113.73	0.2316	0.6555	102.27	113.19	0.2282
80	0.7671	104.11	115.48	0.2349	0.6733	103.76	114.98	0.2315
90 100	0.7861 0.8048	105.58 107.04	117.22 118.97	0.2381 0.2412	0.6907 0.7078	105.24 106.73	116.75 118.52	0.2348 0.2380
110	0.8233	108.51	120.71	0.2443	0.7246	108.22	120.29	0.2411
120	0.8416	109.99	122.45	0.2474	0.7412	109.71	122.06	0.2442
130	0.8596	111.47	124.20	0.2504	0.7576	111.20	123.83	0.2472
140	0.8775	112.96	125.96	0.2533	0.7739	112.71	125.60	0.2502
150	0.8953	114.46	127.72	0.2562	0.7899	114.22	127.38	0.2531

**TABLE A-9E** (Continued)

<i>T</i> °F	<i>v</i>	<i>u</i>	h Dr. //I	S D4 /II °D	<i>v</i>	<i>u</i>	h D. //I	S D. /II. °D
-F	ft <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb · °R	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R
			00 lbf/in. <sup>2</sup> 50.73°F)				20 lbf/in. <sup>2</sup> = 61.92°F)	
Sat.	0.5482 0.5645	98.90 100.33	109.05 110.79	0.2181 0.2214	0.4573	99.71	109.88	0.2161
80	0.5980	100.33	114.46	0.2214	0.4846	102.60	113.37	0.2227
100	0.6300	106.40	118.07	0.2349	0.5130	105.73	117.13	0.2295
120	0.6609	109.42	121.66	0.2412	0.5400	108.83	120.83	0.2360
140	0.6908	112.45	125.24	0.2473	0.5661	111.92	124.50	0.2422
160	0.7201	115.50	128.83	0.2532	0.5914	115.02	128.16	0.2482
180	0.7489	118.58	132.45	0.2589	0.6161	118.15	131.84	0.2541
200	0.7771	121.69	136.08	0.2645	0.6404	121.30	135.53	0.2597
220	0.8051	124.84	139.75	0.2700	0.6642	124.48	139.24	0.2653
240	0.8327	128.04	143.45	0.2754	0.6878	127.69	142.98	0.2707
260	0.8600	131.27	147.19	0.2806	0.7110	130.95	146.75	0.2760
280	0.8871	134.54	150.97	0.2858	0.7340	134.24	150.55	0.2812
300	0.9140	137.85	154.78	0.2909	0.7568	137.57	154.39	0.2863
		1	40 lbf/in. <sup>2</sup>				60 lbf/in. <sup>2</sup>	
		$(T_{\rm sat} =$	71.80°F)			$(T_{\rm sat} =$	= 80.69°F)	
Sat.	0.3915	100.39	110.54	0.2144	0.3416	100.96	111.08	0.2128
80	0.4028	101.76	112.20	0.2175				
100	0.4289	105.02	116.14	0.2246	0.3653	104.26	115.08	0.2201
120	0.4534	108.21	119.96	0.2313	0.3881	107.56	119.06	0.2271
140	0.4768	111.37	123.73	0.2377	0.4095	110.81	122.94	0.2337
160	0.4993	114.53	127.48	0.2439	0.4301	114.03	126.77	0.2400
180	0.5212	117.70	131.21	0.2498	0.4499	117.25	130.57	0.2460
200	0.5426	120.89	134.96	0.2556	0.4692	120.47	134.37	0.2518
220	0.5636	124.10	138.71	0.2612	0.4880	123.72	138.18	0.2575
240	0.5842	127.35	142.49	0.2666	0.5065	126.99	142.00	0.2631
260 280	0.6045	130.62 133.94	146.30 150.13	0.2720	0.5246 0.5425	130.30 133.63	145.84 149.70	0.2685 0.2738
	0.6246			0.2773				
300 320	0.6445 0.6642	137.29 140.68	154.00 157.89	0.2824 0.2875	0.5602 0.5777	137.00 140.41	153.60 157.62	0.2790 0.2841
320	0.0042	140.08	137.69	0.2673	0.3777	140.41	137.02	0.2041
			80 lbf/in. <sup>2</sup> 88.78°F)				00 lbf/in. <sup>2</sup> = 96.24°F)	
C-4	0.2022		ı	0.2115	0.2706			
Sat. 100	0.3023 0.3154	101.44	111.52	0.2115	0.2706	101.86	111.88 112.73	0.2102
120	0.3134	103.44 106.88	113.95 118.11	0.2159 0.2231	0.2748 0.2957	102.56 106.15	117.10	0.2117 0.2194
			122.11					
140 160	0.3570 0.3761	110.21 113.50	122.11	0.2299 0.2364	0.3148 0.3327	109.59 112.96	121.25 125.28	0.2264 0.2330
180	0.3761	116.78	120.04	0.2304	0.3327	116.29	129.25	0.2393
200	0.4120	120.05	133.78	0.2485	0.3661	119.61	133.17	0.2454
220	0.4120	123.33	137.64	0.2463	0.3820	122.94	137.08	0.2434
240	0.4459	126.64	141.50	0.2598	0.3975	126.27	140.99	0.2569
260	0.4624	129.96	145.38	0.2653	0.4126	129.63	144.91	0.2624
280	0.4786	133.32	149.28	0.2706	0.4275	133.01	148.84	0.2678
300	0.4946	136.71	153.20	0.2759	0.4422	136.42	152.79	0.2731
320	0.5104	140.13	157.15	0.2810	0.4566	139.86	156.77	0.2782
340	0.5260	143.59	161.12	0.2860	0.4709	143.33	160.77	0.2833

**TABLE A-9E** (Continued)

TABLE	<b>A-9E</b> (	Continued	()					
T	<i>U</i>	и	h	<i>S</i>	<i>v</i>	и	h	S
°F	ft <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb · °R	ft <sup>3</sup> /1		Btu/lb	Btu/lb · °R
			25 lbf/in. <sup>2</sup> 104.82°F)				250 lbf/in. <sup>2</sup> = 112.73°F	
Sat.	0.2386	102.28	112.22	0.2087	0.212		112.47	0.2073
120	0.2539	105.17	115.75	0.2149	0.219		114.27	0.2104
140	0.2722	108.78	120.12	0.2223	0.237		118.91	0.2183
160	0.2891 0.3050	112.26 115.67	124.30 128.38	0.2291 0.2356	0.254		123.27	0.2255
180 200	0.3202	119.06	132.40	0.2330	0.269 0.283		127.48 131.59	0.2321 0.2385
220	0.3348	122.43	136.38	0.2477	0.296		135.66	0.2445
240	0.3490	125.81	140.35	0.2535	0.310	125.33	139.69	0.2504
260	0.3628	129.20	144.32	0.2591	0.322		143.71	0.2560
280	0.3764	132.61	148.29	0.2645	0.335		147.73	0.2616
300 320	0.3896 0.4027	136.05 139.51	152.28 156.29	0.2699 0.2751	0.347 0.359		151.76 155.81	0.2669 0.2722
340	0.4156	143.00	160.32	0.2802	0.371		159.87	0.2773
360	0.4284	146.33	164.38	0.2852	0.383		163.95	0.2824
		n - 27	75 lbf/in. <sup>2</sup>			n = '	300 lbf/in. <sup>2</sup>	2
		•	120.07°F)				= 126.94°F	
Sat.	0.1912	102.91	112.64	0.2060	0.173		112.73	0.2047
140 160	0.2092 0.2250	106.96 110.73	117.61 122.19	0.2144 0.2219	0.18 <sup>2</sup> 0.200		116.20 121.04	0.2105 0.2185
180	0.2395	144.35	126.54	0.2219	0.214		125.56	0.2163
200	0.2530	117.88	130.77	0.2353	0.22		129.91	0.2324
220	0.2659	121.38	134.91	0.2415	0.239	99   120.83	134.15	0.2387
240	0.2782	124.85	139.02	0.2475	0.251		138.33	0.2447
260	0.2902	128.32	143.10	0.2532	0.262		142.47	0.2506
280 300	0.3018 0.3132	131.80 135.29	147.17 151.24	0.2588 0.2642	0.273 0.284		146.59 150.71	0.2562 0.2617
320	0.3132	133.29	151.24	0.2695	0.284		154.83	0.2671
340	0.3353	142.34	159.41	0.2747	0.305		158.95	0.2723
360	0.3461	145.90	163.53	0.2798	0.315	52   145.58	163.09	0.2774
		$p = 32$ $(T_{\text{sat}} =$	25 lbf/in. <sup>2</sup> 133.39°F)			$p = 1$ $(T_{\text{sat}} =$	350 lbf/in. <sup>2</sup> = 139.49°F	2)
Sat.	0.1577	103.26	112.75	0.2034	0.144	14 103.35	112.71	0.2022
140	0.1637	104.78	114.63	0.2066	0.144		112.86	0.2024
160	0.1796	109.00	119.81	0.2151	0.160		118.30	0.2113
180	0.1934	112.89	124.53	0.2226	0.174	I	123.38	0.2194
200 220	0.2061 0.2179	116.62 120.26	129.02 133.37	0.2295 0.2360	0.187 0.198		128.10 132.53	0.2267 0.2333
240	0.2291	123.84	137.63	0.2422	0.209		136.89	0.2396
260	0.2398	127.40	141.83	0.2481	0.219	99   126.93	141.18	0.2457
280	0.2501	130.96	146.01	0.2538	0.229		145.41	0.2514
300	0.2602	134.51	150.17	0.2593	0.239	I	149.62	0.2571
320 340	0.2700 0.2796	138.08 141.66	154.33 158.49	0.2647 0.2700	0.248 0.257	I	153.82 158.02	0.2626 0.2679
360	0.2891	145.26	162.66	0.2752	0.266		162.23	0.2730
380	0.2983	148.89	166.85	0.2802	0.275		166.43	0.2781

**TABLE A-10E** Properties of Saturated Refrigerant 134a (Liquid–Vapor): Temperature Table

		Specific ft <sup>3</sup> /			Energy ı/lb		Enthalpy Btu/lb			ropy b·°R	
Temp. °F	Press.	Sat. Liquid $v_{\mathrm{f}}$	Sat. Vapor $v_{\rm g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor u <sub>g</sub>	Sat. Liquid $h_{\mathrm{f}}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid s <sub>f</sub>	Sat. Vapor	Temp.
	101/111.		-	-	-	_					1
-40	7.490	0.01130	5.7173	-0.02	87.90	0.00	95.82	95.82	0.0000	0.2283	-40
-30	9.920	0.01143	4.3911	2.81	89.26	2.83	94.49	97.32	0.0067	0.2266	-30
-20	12.949	0.01156	3.4173	5.69	90.62	5.71	93.10	98.81	0.0133	0.2250	-20
-15	14.718	0.01163	3.0286	7.14	91.30	7.17	92.38	99.55	0.0166	0.2243	-15
-10	16.674	0.01170	2.6918	8.61	91.98	8.65	91.64	100.29	0.0199	0.2236	-10
-5	18.831	0.01178	2.3992	10.09	92.66	10.13	90.89	101.02	0.0231	0.2230	-5
0	21.203	0.01185	2.1440	11.58	93.33	11.63	90.12	101.75	0.0264	0.2224	0
5	23.805	0.01193	1.9208	13.09	94.01	13.14	89.33	102.47	0.0296	0.2219	5
10	26.651	0.01200	1.7251	14.60	94.68	14.66	88.53	103.19	0.0329	0.2214	10
15	29.756	0.01208	1.5529	16.13	95.35	16.20	87.71	103.90	0.0361	0.2209	15
20	33.137	0.01216	1.4009	17.67	96.02	17.74	86.87	104.61	0.0393	0.2205	20
25	36.809	0.01225	1.2666	19.22	96.69	19.30	86.02	105.32	0.0426	0.2200	25
30	40.788	0.01233	1.1474	20.78	97.35	20.87	85.14	106.01	0.0458	0.2196	30
40	49.738	0.01251	0.9470	23.94	98.67	24.05	83.34	107.39	0.0522	0.2189	40
50	60.125	0.01270	0.7871	27.14	99.98	27.28	81.46	108.74	0.0585	0.2183	50
60	72.092	0.01290	0.6584	30.39	101.27	30.56	79.49	110.05	0.0648	0.2178	60
70	85.788	0.01311	0.5538	33.68	102.54	33.89	77.44	111.33	0.0711	0.2173	70
80	101.37	0.01334	0.4682	37.02	103.78	37.27	75.29	112.56	0.0774	0.2169	80
85	109.92	0.01346	0.4312	38.72	104.39	38.99	74.17	113.16	0.0805	0.2167	85
90	118.99	0.01358	0.3975	40.42	105.00	40.72	73.03	113.75	0.0836	0.2165	90
95	128.62	0.01371	0.3668	42.14	105.60	42.47	71.86	114.33	0.0867	0.2163	95
100	138.83	0.01385	0.3388	43.87	106.18	44.23	70.66	114.89	0.0898	0.2161	100
105	149.63	0.01399	0.3131	45.62	106.76	46.01	69.42	115.43	0.0930	0.2159	105
110	161.04	0.01414	0.2896	47.39	107.33	47.81	68.15	115.96	0.0961	0.2157	110
115	173.10	0.01429	0.2680	49.17	107.88	49.63	66.84	116.47	0.0992	0.2155	115
120	185.82	0.01445	0.2481	50.97	108.42	51.47	65.48	116.95	0.1023	0.2153	120
140	243.86	0.01520	0.1827	58.39	110.41	59.08	59.57	118.65	0.1150	0.2143	140
160	314.63	0.01617	0.1341	66.26	111.97	67.20	52.58	119.78	0.1280	0.2128	160
180	400.22	0.01758	0.0964	74.83	112.77	76.13	43.78	119.91	0.1417	0.2101	180
200	503.52	0.02014	0.0647	84.90	111.66	86.77	30.92	117.69	0.1575	0.2044	200
210	563.51	0.02329	0.0476	91.84	108.48	94.27	19.18	113.45	0.1684	0.1971	210

Source: Tables A-10E through A-12E are calculated based on equations from D. P. Wilson and R. S. Basu, "Thermodynamic Properties of a New Stratospherically Safe Working Fluid—Refrigerant 134a," ASHRAE Trans., Vol. 94, Pt. 2, 1988, pp. 2095–2118.

**TABLE A-11E** Properties of Saturated Refrigerant 134a (Liquid–Vapor): Pressure Table

		Specific ft <sup>3</sup> /		Internal Btu			Enthalpy Btu/lb		Entro Btu/lb		
		Sat.	Sat.	Sat.	Sat.	Sat.		Sat.	Sat.	Sat.	
Press.	Temp.	Liquid	Vapor	Liquid	Vapor	Liquid	Evap.	Vapor	Liquid	Vapor	Press.
lbf/in. <sup>2</sup>	°F	$v_{ m f}$	$v_{\mathrm{g}}$	$u_{ m f}$	$u_{\rm g}$	$h_{ m f}$	$h_{ m fg}$	$h_{ m g}$	$s_{ m f}$	$s_{\rm g}$	lbf/in. <sup>2</sup>
5	-53.48	0.01113	8.3508	-3.74	86.07	-3.73	97.53	93.79	-0.0090	0.2311	5
10	-29.71	0.01143	4.3581	2.89	89.30	2.91	94.45	97.37	0.0068	0.2265	10
15	-14.25	0.01164	2.9747	7.36	91.40	7.40	92.27	99.66	0.0171	0.2242	15
20	-2.48	0.01181	2.2661	10.84	93.00	10.89	90.50	101.39	0.0248	0.2227	20
30	15.38	0.01209	1.5408	16.24	95.40	16.31	87.65	103.96	0.0364	0.2209	30
40	29.04	0.01232	1.1692	20.48	97.23	20.57	85.31	105.88	0.0452	0.2197	40
50	40.27	0.01252	0.9422	24.02	98.71	24.14	83.29	107.43	0.0523	0.2189	50
60	49.89	0.01270	0.7887	27.10	99.96	27.24	81.48	108.72	0.0584	0.2183	60
70	58.35	0.01286	0.6778	29.85	101.05	30.01	79.82	109.83	0.0638	0.2179	70
80	65.93	0.01302	0.5938	32.33	102.02	32.53	78.28	110.81	0.0686	0.2175	80
90	72.83	0.01317	0.5278	34.62	102.89	34.84	76.84	111.68	0.0729	0.2172	90
100	79.17	0.01332	0.4747	36.75	103.68	36.99	75.47	112.46	0.0768	0.2169	100
120	90.54	0.01360	0.3941	40.61	105.06	40.91	72.91	113.82	0.0839	0.2165	120
140	100.56	0.01386	0.3358	44.07	106.25	44.43	70.52	114.95	0.0902	0.2161	140
160	109.56	0.01412	0.2916	47.23	107.28	47.65	68.26	115.91	0.0958	0.2157	160
180	117.74	0.01438	0.2569	50.16	108.18	50.64	66.10	116.74	0.1009	0.2154	180
200	125.28	0.01463	0.2288	52.90	108.98	53.44	64.01	117.44	0.1057	0.2151	200
220	132.27	0.01489	0.2056	55.48	109.68	56.09	61.96	118.05	0.1101	0.2147	220
240	138.79	0.01515	0.1861	57.93	110.30	58.61	59.96	118.56	0.1142	0.2144	240
260	144.92	0.01541	0.1695	60.28	110.84	61.02	57.97	118.99	0.1181	0.2140	260
280	150.70	0.01568	0.1550	62.53	111.31	63.34	56.00	119.35	0.1219	0.2136	280
300	156.17	0.01596	0.1424	64.71	111.72	65.59	54.03	119.62	0.1254	0.2132	300
350	168.72	0.01671	0.1166	69.88	112.45	70.97	49.03	120.00	0.1338	0.2118	350
400	179.95	0.01758	0.0965	74.81	112.77	76.11	43.80	119.91	0.1417	0.2102	400
450	190.12	0.01863	0.0800	79.63	112.60	81.18	38.08	119.26	0.1493	0.2079	450
500	199.38	0.02002	0.0657	84.54	111.76	86.39	31.44	117.83	0.1570	0.2047	500

**TABLE A-12E** Properties of Superheated Refrigerant 134a Vapor

TABI	LE A-12E	Properti	es of Sup	erheated Refr	igerant 134	a Vapor			
<i>T</i> °F	<i>v</i> ft³/lb	и Btu/lb	<i>h</i> Btu/lb	s Btu/lb · °R		<i>v</i> ft³/lb	и Btu/lb	<i>h</i> Btu/lb	s Btu/lb·°R
	11 /10		0 lbf/in. <sup>2</sup>	Btu/10 K		11 /10		15 lbf/in. <sup>2</sup>	Btu/10 K
			−29.71°F	)				−14.25°F	)
Sat20	4.3581 4.4718	89.30 90.89	97.37 99.17	0.2265 0.2307		2.9747	91.40	99.66	0.2242
-20	4.4718	90.89	102.94	0.2391		3.0893	93.84	102.42	0.2303
20	4.9297	97.67	106.79	0.2472		3.2468	97.33	106.34	0.2386
40 60	5.1539 5.3758	101.19 104.80	110.72 114.74	0.2553 0.2632		3.4012 3.5533	100.89 104.54	110.33 114.40	0.2468 0.2548
80	5.5959	108.50	118.85	0.2709		3.7034	108.28	118.56	0.2626
100 120	5.8145 6.0318	112.29 116.18	123.05 127.34	0.2786 0.2861		3.8520 3.9993	112.10 116.01	122.79 127.11	0.2703 0.2779
140	6.2482	120.16	131.72	0.2935		4.1456	120.00	131.51	0.2854
160	6.4638	124.23	136.19	0.3009		4.2911	124.09	136.00	0.2927
180 200	6.6786 6.8929	128.38 132.63	140.74 145.39	0.3081 0.3152		4.4359 4.5801	128.26 132.52	140.57 145.23	0.3000 0.3072
									l
			20 lbf/in. <sup>2</sup>					30 lbf/in. <sup>2</sup>	
Sat.	2.2661	$(T_{\text{sat}} = 93.00)$	-2.48°F)	0.2227		1.5408	95.40	15.38°F)	0.2209
0	2.2816	93.43	101.39	0.2238		1.5406	93.40	103.90	0.2209
20	2.4046	96.98	105.88	0.2323		1.5611	96.26	104.92	0.2229
40 60	2.5244 2.6416	100.59 104.28	109.94 114.06	0.2406 0.2487		1.6465 1.7293	99.98 103.75	109.12 113.35	0.2315 0.2398
80	2.7569	108.05	118.25	0.2566		1.8098	107.59	117.63	0.2478
100 120	2.8705 2.9829	111.90 115.83	122.52 126.87	0.2644 0.2720		1.8887 1.9662	111.49 115.47	121.98 126.39	0.2558 0.2635
140	3.0942	119.85	131.30	0.2725		2.0426	119.53	130.87	0.2711
160	3.2047	123.95	135.81	0.2869		2.1181	123.66	135.42	0.2786
180 200	3.3144 3.4236	128.13 132.40	140.40 145.07	0.2922 0.3014		2.1929 2.2671	127.88 132.17	140.05 144.76	0.2859 0.2932
220	3.5323	136.76	149.83	0.3085		2.3407	136.55	149.54	0.3003
			10.11.67. 2				,	-0.11.C/. 2	
		•	10 lbf/in. <sup>2</sup> = 29.04°F)				*	50 lbf/in. <sup>2</sup> = 40.27°F)	
Sat.	1.1692	97.23	105.88	0.2197		0.9422	98.71	107.43	0.2189
40 60	1.2065 1.2723	99.33 103.20	108.26 112.62	0.2245 0.2331		0.9974	102.62	111.85	0.2276
80	1.3357	107.11	117.00	0.2414		1.0508	106.62	116.34	0.2361
100 120	1.3973 1.4575	111.08 115.11	121.42 125.90	0.2494 0.2573		1.1022 1.1520	110.65 114.74	120.85 125.39	0.2443 0.2523
140	1.5165	119.21	130.43	0.2650		1.2007	118.88	129.99	0.2601
160	1.5746	123.38	135.03	0.2725		1.2484	123.08	134.64 139.34	0.2677
180 200	1.6319 1.6887	127.62 131.94	139.70 144.44	0.2799 0.2872		1.2953 1.3415	127.36 131.71	139.34	0.2752 0.2825
220	1.7449	136.34	149.25	0.2944		1.3873	136.12	148.96	0.2897
240 260	1.8006 1.8561	140.81 145.36	154.14	0.3015 0.3085		1.4326	140.61	153.87	0.2969 0.3039
280	1.8561	145.36	159.10 164.13	0.3085		1.4775 1.5221	145.18 149.82	158.85 163.90	0.3039

 TABLE A-12E
 (Continued)

TABI	.E A-12E	(Contin	ued)						
T	v - 2 ···	и	h	S	_	v 2	и	h	S
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R	fı	t <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb · °R
$p = 60 \text{ lbf/in.}^2$ $(T_{\text{sat}} = 49.89^{\circ}\text{F})$					$p = 70 \text{ lbf/in.}^2$ ( $T_{\text{sat}} = 58.35^{\circ}\text{F}$ )				
Sat.	0.7887	99.96	108.72	0.2183	0.0	6778	101.05	109.83	0.2179
60	0.8135	102.03	111.06	0.2229	0.0	6814	101.40	110.23	0.2186
80	0.8604	106.11	115.66	0.2316	0.	7239	105.58	114.96	0.2276
100	0.9051	110.21	120.26	0.2399		7640	109.76	119.66	0.2361
120	0.9482	114.35	124.88	0.2480		8023	113.96	124.36	0.2444
140	0.9900	118.54	129.53	0.2559		8393	118.20	129.07	0.2524
160 180	1.0308 1.0707	122.79 127.10	134.23 138.98	0.2636 0.2712		8752 9103	122.49 126.83	133.82 138.62	0.2601 0.2678
200	1.1100	131.47	143.79	0.2712		9103	131.23	138.62	0.2078
220	1.1488	135.91	148.66	0.2780		9784	135.69	148.36	0.2732
240	1.1466	140.42	153.60	0.2839		0118	140.22	153.33	0.2823
260	1.2251	145.00	158.60	0.3001		0448	144.82	158.35	0.2968
280	1.2627	149.65	163.67	0.3070		0774	149.48	163.44	0.3038
300	1.3001	154.38	168.81	0.3139		1098	154.22	168.60	0.3107
$p = 80 \text{ lbf/in.}^2$ ( $T_{\text{sat}} = 65.93^{\circ}\text{F}$ )					$p = 90 \text{ lbf/in.}^2$ ( $T_{\text{sat}} = 72.83^{\circ}\text{F}$ )				
					_				
Sat.	0.5938	102.02	110.81	0.2175		5278	102.89	111.68	0.2172
80	0.6211	105.03	114.23	0.2239		5408	104.46	113.47	0.2205
100	0.6579	109.30	119.04	0.2327		5751	108.82	118.39	0.2295
120 140	0.6927	113.56	123.82 128.60	0.2411 0.2492		6073	113.15	123.27 128.12	0.2380
160	0.7261 0.7584	117.85 122.18	133.41	0.2492		6380 6675	117.50 121.87	128.12	0.2463 0.2542
180	0.7898	126.55	138.25	0.2647		6961	126.28	137.87	0.2620
200	0.8205	130.98	143.13	0.2722		7239	130.73	142.79	0.2696
220	0.8506	135.47	148.06	0.2796		7512	135.25	147.76	0.2770
240	0.8803	140.02	153.05	0.2868	0.	7779	139.82	152.77	0.2843
260	0.9095	144.63	158.10	0.2940	0.5	8043	144.45	157.84	0.2914
280	0.9384	149.32	163.21	0.3010	0.3	8303	149.15	162.97	0.2984
300	0.9671	154.06	168.38	0.3079		8561	153.91	168.16	0.3054
320	0.9955	158.88	173.62	0.3147	0.	8816	158.73	173.42	0.3122
$p = 100 \text{ lbf/in.}^2$					$p = 120 \text{ lbf/in.}^2$				
p = 100  form. $(T_{\text{sat}} = 79.17^{\circ}\text{F})$					$(T_{\text{sat}} = 90.54^{\circ}\text{F})$				
Sat.	0.4747	103.68	112.46	0.2169	0	3941	105.06	113.82	0.2165
80	0.4761	103.87	112.68	0.2173					
100	0.5086	108.32	117.73	0.2265	0.4	4080	107.26	116.32	0.2210
120	0.5388	112.73	122.70	0.2352		4355	111.84	121.52	0.2301
140	0.5674	117.13	127.63	0.2436		4610	116.37	126.61	0.2387
160	0.5947	121.55	132.55	0.2517		4852	120.89	131.66	0.2470
180	0.6210	125.99	137.49	0.2595		5082	125.42	136.70	0.2550
200 220	0.6466 0.6716	130.48 135.02	142.45 147.45	0.2671 0.2746		5305 5520	129.97 134.56	141.75 146.82	0.2628 0.2704
240	0.6710	139.61	152.49	0.2740		5731	139.20	151.92	0.2704
260	0.7201	139.01	157.59	0.2819		5937	139.20	157.07	0.2778
280	0.7438	148.98	162.74	0.2962		6140	148.63	162.26	0.2921
300	0.7672	153.75	167.95	0.3031		6339	153.43	167.51	0.2991
320	0.7904	158.59	173.21	0.3099		6537	158.29	172.81	0.3060

 TABLE A-12E
 (Continued)

TABI	.E A-12E	(Contin	ued)					
T	v	и	h	S	<i>v</i>	и	h	S
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R
			40 lbf/in. <sup>2</sup> 100.56°F				60 lbf/in. <sup>2</sup> 109.55°F	
<b>C</b> .	0.2250				0.2017			
Sat. 120	0.3358 0.3610	106.25 110.90	114.95 120.25	0.2161 0.2254	0.2916 0.3044	107.28 109.88	115.91 118.89	0.2157 0.2209
140	0.3846	115.58	120.23	0.2234	0.3269	114.73	124.41	0.2209
160	0.4066	120.21	130.74	0.2429	0.3474	119.49	129.78	0.2391
180	0.4274	124.82	135.89	0.2511	0.3666	124.20	135.06	0.2475
200	0.4474	129.44	141.03	0.2590	0.3849	128.90	140.29	0.2555
220	0.4666	134.09	146.18	0.2667	0.4023	133.61	145.52	0.2633
240	0.4852	138.77	151.34	0.2742	0.4192	138.34	150.75	0.2709
260	0.5034	143.50	156.54	0.2815	0.4356	143.11	156.00	0.2783
280	0.5212	148.28	161.78	0.2887	0.4516	147.92	161.29	0.2856
300	0.5387	153.11	167.06	0.2957	0.4672	152.78	166.61	0.2927
320	0.5559	157.99	172.39	0.3026	0.4826	157.69	171.98	0.2996
340	0.5730	162.93	177.78	0.3094	0.4978	162.65	177.39	0.3065
360	0.5898	167.93	183.21	0.3162	0.5128	167.67	182.85	0.3132
		n = 1	80 lbf/in. <sup>2</sup>			n = 2	00 lbf/in. <sup>2</sup>	
			117.74°F				125.28°F	
Sat.	0.2569	108.18	116.74	0.2154	0.2288	108.98	117.44	0.2151
120	0.2595	108.77	117.41	0.2166				
140	0.2814	113.83	123.21	0.2264	0.2446	112.87	121.92	0.2226
160	0.3011	118.74	128.77	0.2355	0.2636	117.94	127.70	0.2321
180	0.3191	123.56	134.19	0.2441	0.2809	122.88	133.28	0.2410
200	0.3361	128.34	139.53	0.2524	0.2970	127.76	138.75	0.2494
220	0.3523	133.11 137.90	144.84	0.2603	0.3121	132.60 137.44	144.15 149.53	0.2575
<ul><li>240</li><li>260</li></ul>	0.3678 0.3828	142.71	150.15 155.46	0.2680 0.2755	0.3266 0.3405	142.30	154.90	0.2653 0.2728
280	0.3974	147.55	160.79	0.2828	0.3540	147.18	160.28	0.2728
300	0.4116	152.44	166.15	0.2899	0.3671	152.10	165.69	0.2874
320	0.4256	157.38	171.55	0.2969	0.3799	157.07	171.13	0.2945
340	0.4393	162.36	177.00	0.3038	0.3926	162.07	176.60	0.3014
360	0.4529	167.40	182.49	0.3106	0.4050	167.13	182.12	0.3082
		n - 2	00 lbf/in. <sup>2</sup>			n – 1	00 lbf/in. <sup>2</sup>	
			00 161/111. 156.17°F)			p-4 $T=$	179.95°F	)
Sat.	0.1424	111.72	119.62	0.2132	0.0965	112.77	119.91	0.2102
160	0.1462	112.95	121.07	0.2155	0.0703	112.77	117.71	0.2102
180	0.1633	118.93	128.00	0.2265	0.0965	112.79	119.93	0.2102
200	0.1777	124.47	134.34	0.2363	0.1143	120.14	128.60	0.2235
220	0.1905	129.79	140.36	0.2453	0.1275	126.35	135.79	0.2343
240	0.2021	134.99	146.21	0.2537	0.1386	132.12	142.38	0.2438
260	0.2130	140.12	151.95	0.2618	0.1484	137.65	148.64	0.2527
280	0.2234	145.23	157.63	0.2696	0.1575	143.06	154.72	0.2610
300	0.2333	150.33	163.28	0.2772	0.1660	148.39	160.67	0.2689
320	0.2428	155.44	168.92	0.2845	0.1740	153.69	166.57	0.2766
340	0.2521	160.57	174.56	0.2916	0.1816	158.97	172.42	0.2840
360	0.2611	165.74	180.23	0.2986	0.1890	164.26	178.26	0.2912
380 400	0.2699 0.2786	170.94 176.18	185.92 191.64	0.3055 0.3122	0.1962 0.2032	169.57 174.90	184.09 189.94	0.2983 0.3051
<del>-100</del>	0.2700	170.10	171.07	0.5122	0.2032	177.50	107.94	0.5051

**TABLE A-13E** Properties of Saturated Ammonia (Liquid–Vapor): Temperature Table

			Volume /lb	Internal Btu/			Enthalpy Btu/lb		Entro Btu/lb		
Temp.	Press. lbf/in. <sup>2</sup>	Sat. Liquid $v_{ m f}$	Sat. Vapor $v_{ m g}$	Sat. Liquid $u_{\rm f}$	Sat. Vapor u <sub>g</sub>	Sat. Liquid $h_{ m f}$	Evap. $h_{\mathrm{fg}}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid s <sub>f</sub>	Sat. Vapor $s_{\rm g}$	Temp. °F
-60	5.548	0.02278	44.7537	-21.005	543.61	-20.97	610.56	589.58	-0.0512	1.4765	-60
-55	6.536	0.02288	38.3991	-15.765	545.11	-15.73	607.31	591.58	-0.0381	1.4627	-55
-50	7.664	0.02299	33.0880	-10.525	546.59	-10.49	604.04	593.54	-0.0253	1.4492	-50
-45	8.949	0.02310	28.6284	-5.295	548.04	-5.25	600.72	595.48	-0.0126	1.4361	-45
-40	10.405	0.02322	24.8672	-0.045	549.46	0.00	597.37	597.37	0.0000	1.4235	-40
-35	12.049	0.02333	21.6812	5.20	550.86	5.26	593.98	599.24	0.0124	1.4111	-35
-30	13.899	0.02345	18.9715	10.46	552.24	10.52	590.54	601.06	0.0247	1.3992	-30
-25	15.972	0.02357	16.6577	15.73	553.59	15.80	587.05	602.85	0.0369	1.3875	-25
-20	18.290	0.02369	14.6744	21.01	554.91	21.09	583.51	604.61	0.0490	1.3762	-20
-15	20.871	0.02381	12.9682	26.31	556.20	26.40	579.92	606.32	0.0610	1.3652	-15
-10	23.738	0.02393	11.4951	31.63	557.46	31.73	576.26	607.99	0.0729	1.3544	-10
-5	26.912	0.02406	10.2190	36.96	558.70	37.08	572.54	609.62	0.0847	1.3440	-5
0	30.416	0.02419	9.1100	42.32	559.91	42.45	568.76	611.22	0.0964	1.3338	0
5	34.275	0.02432	8.1430	47.69	561.08	47.85	564.92	612.76	0.1080	1.3238	5
10	38.512	0.02446	7.2974	53.09	562.23	53.27	561.00	614.27	0.1196	1.3141	10
15	43.153	0.02460	6.5556	58.52	563.34	58.72	557.01	615.73	0.1311	1.3046	15
20	48.224	0.02474	5.9032	63.97	564.43	64.19	552.95	617.14	0.1425	1.2953	20
25	53.752	0.02488	5.3278	69.43	565.48	69.68	548.82	618.51	0.1539	1.2862	25
30	59.765	0.02503	4.8188	74.93	566.49	75.20	544.62	619.82	0.1651	1.2774	30
35	66.291	0.02517	4.3675	80.44	567.48	80.75	540.34	621.09	0.1764	1.2687	35
40	73.359	0.02533	3.9664	85.98	568.42	86.33	535.97	622.30	0.1875	1.2602	40
45	81.000	0.02548	3.6090	91.55	569.33	91.93	531.54	623.46	0.1986	1.2518	45
50	89.242	0.02564	3.2897	97.13	570.21	97.55	527.02	624.57	0.2096	1.2436	50
55	98.118	0.02581	3.0040	102.73	571.04	103.20	522.42	625.62	0.2205	1.2356	55
60	107.66	0.02597	2.7476	108.35	571.83	108.87	517.74	626.61	0.2314	1.2277	60
65	117.90	0.02614	2.5171	113.99	572.59	114.56	512.97	627.54	0.2422	1.2199	65
70	128.87	0.02632	2.3095	119.65	573.29	120.28	508.12	628.40	0.2530	1.2123	70
75	140.60	0.02650	2.1220	125.33	573.95	126.02	503.18	629.20	0.2636	1.2048	75
80	153.13	0.02668	1.9524	131.02	574.57	131.78	498.15	629.93	0.2742	1.1973	80
85	166.50	0.02687	1.7988	136.73	575.13	137.56	493.03	630.59	0.2848	1.1900	85
90	180.73	0.02707	1.6593	142.46	575.65	143.37	487.81	631.18	0.2953	1.1827	90
95	195.87	0.02727	1.5324	148.21	576.10	149.20	482.49	631.68	0.3057	1.1756	95
100	211.96	0.02747	1.4168	153.98	576.51	155.05	477.06	632.11	0.3161	1.1685	100
105	229.02	0.02768	1.3113	159.76	576.85	160.94	471.52	632.46	0.3264	1.1614	105
110	247.10	0.02790	1.2149	165.58	577.13	166.85	465.86	632.71	0.3366	1.1544	110
115	266.24	0.02813	1.1266	171.41	577.34	172.80	460.08	632.88	0.3469	1.1475	115
120	286.47	0.02836	1.0456	177.28	577.48	178.79	454.16	632.95	0.3570	1.1405	120

Source: Tables A-13E through A-15E are calculated based on equations from L. Haar and J. S. Gallagher, "Thermodynamic Properties of Ammonia," J. Phys. Chem. Reference Data, Vol. 7, 1978, pp. 635–792.

## 792 Tables in English Units

**TABLE A-14E** Properties of Saturated Ammonia (Liquid–Vapor): Pressure Table

			Volume /lb	Internal Btu			Enthalpy Btu/lb		Entro Btu/lb		
		Sat.	Sat.	Sat.	Sat.	Sat.		Sat.	Sat.	Sat.	
Press.	Temp.	Liquid	Vapor	Liquid	Vapor	Liquid	Evap.	Vapor	Liquid	Vapor	Press.
lbf/in. <sup>2</sup>	°F	$v_{ m f}$	$v_{ m g}$	$u_{\mathrm{f}}$	$u_{\mathrm{g}}$	$h_{ m f}$	$h_{ m fg}$	$h_{ m g}$	$s_{ m f}$	$s_{\mathrm{g}}$	lbf/in. <sup>2</sup>
5	-63.10	0.02271	49.320	-24.24	542.67	-24.22	612.56	588.33	-0.0593	1.4853	5
6	-57.63	0.02283	41.594	-18.51	544.32	-18.49	609.02	590.54	-0.0450	1.4699	6
7	-52.86	0.02293	36.014	-13.52	545.74	-13.49	605.92	592.42	-0.0326	1.4569	7
8	-48.63	0.02302	31.790	-9.09	546.98	-9.06	603.13	594.08	-0.0218	1.4456	8
9	-44.81	0.02311	28.477	-5.09	548.09	-5.05	600.60	595.55	-0.0121	1.4357	9
10	-41.33	0.02319	25.807	-1.44	549.09	-1.40	598.27	596.87	-0.0033	1.4268	10
12	-35.14	0.02333	21.764	5.06	550.82	5.11	594.08	599.18	0.0121	1.4115	12
14	-29.74	0.02345	18.843	10.73	552.31	10.79	590.36	601.16	0.0254	1.3986	14
16	-24.94	0.02357	16.631	15.80	553.60	15.87	587.01	602.88	0.0371	1.3874	16
18	-20.60	0.02367	14.896	20.38	554.75	20.46	583.94	604.40	0.0476	1.3775	18
20	-16.63	0.02377	13.497	24.58	555.78	24.67	581.10	605.76	0.0571	1.3687	20
25	-7.95	0.02399	10.950	33.81	557.97	33.92	574.75	608.67	0.0777	1.3501	25
30	-0.57	0.02418	9.229	41.71	559.77	41.84	569.20	611.04	0.0951	1.3349	30
35	5.89	0.02435	7.984	48.65	561.29	48.81	564.22	613.03	0.1101	1.3221	35
40	11.65	0.02450	7.041	54.89	562.60	55.07	559.69	614.76	0.1234	1.3109	40
45	16.87	0.02465	6.302	60.56	563.75	60.76	555.50	616.26	0.1354	1.3011	45
50	21.65	0.02478	5.705	65.77	564.78	66.00	551.59	617.60	0.1463	1.2923	50
55	26.07	0.02491	5.213	70.61	565.70	70.86	547.93	618.79	0.1563	1.2843	55
60	30.19	0.02503	4.801	75.13	566.53	75.41	544.46	619.87	0.1656	1.2770	60
65	34.04	0.02515	4.450	79.39	567.29	79.69	541.16	620.85	0.1742	1.2703	65
70	37.67	0.02526	4.1473	83.40	567.99	83.73	538.01	621.74	0.1823	1.2641	70
75	41.11	0.02536	3.8837	87.21	568.63	87.57	535.00	622.56	0.1900	1.2583	75
80	44.37	0.02546	3.6520	90.84	569.22	91.22	532.10	623.32	0.1972	1.2529	80
85	47.47	0.02556	3.4466	94.30	569.77	94.71	529.31	624.02	0.2040	1.2478	85
90	50.44	0.02566	3.2632	97.62	570.28	98.05	526.62	624.66	0.2106	1.2429	90
100	56.01	0.02584	2.9497	103.87	571.21	104.35	521.48	625.82	0.2227	1.2340	100
110	61.17	0.02601	2.6913	109.68	572.01	110.20	516.63	626.83	0.2340	1.2259	110
120	65.98	0.02618	2.4745	115.11	572.73	115.69	512.02	627.71	0.2443	1.2184	120
130	70.50	0.02634	2.2899	120.21	573.36	120.85	507.64	628.48	0.2540	1.2115	130
140 150	74.75 78.78	0.02649	2.1309 1.9923	125.04 129.63	573.92	125.73 130.37	503.43 499.39	629.16 629.76	0.2631 0.2717	1.2051 1.1991	140 150
		0.02664			574.42						
175	88.02	0.02699	1.7128	140.19	575.45	141.07	489.89	630.95	0.2911	1.1856	175
200	96.31	0.02732	1.5010	149.72	576.21	150.73	481.07	631.80	0.3084	1.1737	200
225	103.85	0.02764	1.3348	158.43	576.77	159.58	472.80	632.38	0.3240	1.1630	225
250 275	110.78	0.02794 0.02823	1.2007 1.0901	166.48	577.16	167.77	464.97	632.74	0.3382	1.1533	250 275
300	117.20 123.20	0.02823	0.9974	173.99	577.41	175.43 182.63	457.49 450.31	632.92 632.94	0.3513	1.1444	300
300	123.20	0.02851	0.9974	181.05	577.54	182.03	430.31	032.94	0.3635	1.1361	300

**TABLE A-15E** Properties of Superheated Ammonia Vapor

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$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	T			h Dtu/llb			U Dtu/lb	h Dtu/lb	
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$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$						31.790	546.98	594.08	1.4456
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$						32.511	550.32	598.49	1.4562
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	-30	44.627	554.84	604.42	1.5033	33.342	554.19	603.58	1.4682
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$\begin{array}{c ccccccccccccccccccccccccccccccccccc$		46.800		614.47			561.93		
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$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$			p = 1	0 lbf/in. <sup>2</sup>			p = 1	2 lbf/in. <sup>2</sup>	
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$					)				)
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$						21.764	550.82	599.18	1.4115
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$						22.056	550.07	601.00	1 4170
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$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	70	33.127	592.66	654.01	1.5479	27.564	592.38	653.63	1.5261
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$									
Sat.         18.843         552.31         601.16         1.3986         16.631         553.60         602.88         1.3874           -20         19.321         556.24         606.33         1.4105         16.845         555.62         605.53         1.3935           -10         19.807         560.26         611.61         1.4223         17.275         559.69         610.88         1.4055           0         20.289         564.27         616.86         1.4339         17.701         563.75         616.19         1.4172           10         20.768         568.26         622.10         1.4452         18.124         567.79         621.48         1.4286           20         21.244         572.24         627.31         1.4562         18.544         571.81         626.75         1.4397           30         21.717         576.22         632.52         1.4669         18.961         575.82         632.00         1.4505           40         22.188         580.19         637.71         1.4774         19.376         579.82         637.23         1.4611           50         22.657         584.16         642.89         1.4877         19.789         583.82         642.45 </td <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>•</td> <td></td> <td></td>							•		
-20         19.321         556.24         606.33         1.4105         16.845         555.62         605.53         1.3935           -10         19.807         560.26         611.61         1.4223         17.275         559.69         610.88         1.4055           0         20.289         564.27         616.86         1.4339         17.701         563.75         616.19         1.4172           10         20.768         568.26         622.10         1.4452         18.124         567.79         621.48         1.4286           20         21.244         572.24         627.31         1.4562         18.544         571.81         626.75         1.4397           30         21.717         576.22         632.52         1.4669         18.961         575.82         632.00         1.4505           40         22.188         580.19         637.71         1.4774         19.376         579.82         637.23         1.4611           50         22.657         584.16         642.89         1.4877         19.789         583.82         642.45         1.4714           60         23.124         588.12         648.07         1.4977         20.200         587.81         647.66 <td></td> <td></td> <td><math>(T_{\rm sat} =</math></td> <td>-29.74°F</td> <td>)</td> <td></td> <td><math>(T_{\rm sat} =</math></td> <td>-24.94°F</td> <td>)</td>			$(T_{\rm sat} =$	-29.74°F	)		$(T_{\rm sat} =$	-24.94°F	)
-10         19.807         560.26         611.61         1.4223         17.275         559.69         610.88         1.4055           0         20.289         564.27         616.86         1.4339         17.701         563.75         616.19         1.4172           10         20.768         568.26         622.10         1.4452         18.124         567.79         621.48         1.4286           20         21.244         572.24         627.31         1.4562         18.544         571.81         626.75         1.4397           30         21.717         576.22         632.52         1.4669         18.961         575.82         632.00         1.4505           40         22.188         580.19         637.71         1.4774         19.376         579.82         637.23         1.4611           50         22.657         584.16         642.89         1.4877         19.789         583.82         642.45         1.4714           60         23.124         588.12         648.07         1.4977         20.200         587.81         647.66         1.4815           70         23.590         592.09         653.25         1.5076         20.609         591.80         652.86			552.31			16.631	553.60	602.88	1.3874
0         20.289         564.27         616.86         1.4339         17.701         563.75         616.19         1.4172           10         20.768         568.26         622.10         1.4452         18.124         567.79         621.48         1.4286           20         21.244         572.24         627.31         1.4562         18.544         571.81         626.75         1.4397           30         21.717         576.22         632.52         1.4669         18.961         575.82         632.00         1.4505           40         22.188         580.19         637.71         1.4774         19.376         579.82         637.23         1.4611           50         22.657         584.16         642.89         1.4877         19.789         583.82         642.45         1.4714           60         23.124         588.12         648.07         1.4977         20.200         587.81         647.66         1.4815           70         23.590         592.09         653.25         1.5076         20.609         591.80         652.86         1.4915           80         24.054         596.07         658.42         1.5173         21.017         595.80         658.07									
10     20.768     568.26     622.10     1.4452     18.124     567.79     621.48     1.4286       20     21.244     572.24     627.31     1.4562     18.544     571.81     626.75     1.4397       30     21.717     576.22     632.52     1.4669     18.961     575.82     632.00     1.4505       40     22.188     580.19     637.71     1.4774     19.376     579.82     637.23     1.4611       50     22.657     584.16     642.89     1.4877     19.789     583.82     642.45     1.4714       60     23.124     588.12     648.07     1.4977     20.200     587.81     647.66     1.4815       70     23.590     592.09     653.25     1.5076     20.609     591.80     652.86     1.4915       80     24.054     596.07     658.42     1.5173     21.017     595.80     658.07     1.5012									
20     21.244     572.24     627.31     1.4562     18.544     571.81     626.75     1.4397       30     21.717     576.22     632.52     1.4669     18.961     575.82     632.00     1.4505       40     22.188     580.19     637.71     1.4774     19.376     579.82     637.23     1.4611       50     22.657     584.16     642.89     1.4877     19.789     583.82     642.45     1.4714       60     23.124     588.12     648.07     1.4977     20.200     587.81     647.66     1.4815       70     23.590     592.09     653.25     1.5076     20.609     591.80     652.86     1.4915       80     24.054     596.07     658.42     1.5173     21.017     595.80     658.07     1.5012								l .	
30         21.717         576.22         632.52         1.4669         18.961         575.82         632.00         1.4505           40         22.188         580.19         637.71         1.4774         19.376         579.82         637.23         1.4611           50         22.657         584.16         642.89         1.4877         19.789         583.82         642.45         1.4714           60         23.124         588.12         648.07         1.4977         20.200         587.81         647.66         1.4815           70         23.590         592.09         653.25         1.5076         20.609         591.80         652.86         1.4915           80         24.054         596.07         658.42         1.5173         21.017         595.80         658.07         1.5012								1	
40     22.188     580.19     637.71     1.4774     19.376     579.82     637.23     1.4611       50     22.657     584.16     642.89     1.4877     19.789     583.82     642.45     1.4714       60     23.124     588.12     648.07     1.4977     20.200     587.81     647.66     1.4815       70     23.590     592.09     653.25     1.5076     20.609     591.80     652.86     1.4915       80     24.054     596.07     658.42     1.5173     21.017     595.80     658.07     1.5012									
50     22.657     584.16     642.89     1.4877     19.789     583.82     642.45     1.4714       60     23.124     588.12     648.07     1.4977     20.200     587.81     647.66     1.4815       70     23.590     592.09     653.25     1.5076     20.609     591.80     652.86     1.4915       80     24.054     596.07     658.42     1.5173     21.017     595.80     658.07     1.5012									
60     23.124     588.12     648.07     1.4977     20.200     587.81     647.66     1.4815       70     23.590     592.09     653.25     1.5076     20.609     591.80     652.86     1.4915       80     24.054     596.07     658.42     1.5173     21.017     595.80     658.07     1.5012									
70     23.590     592.09     653.25     1.5076     20.609     591.80     652.86     1.4915       80     24.054     596.07     658.42     1.5173     21.017     595.80     658.07     1.5012									
80 24.054 596.07 658.42 1.5173 21.017 595.80 658.07 1.5012								1	
		24.517			1.5268	21.424		663.27	1.5107

**TABLE A-15E** (Continued)

IADL	L A-IJL	Сопиние	ш)						
<i>T</i> °F	<i>v</i> ft³/lb	и Btu/lb	h Btu/lb	s Btu/lb · °R		<i>v</i> ft³/lb	u Btu/lb	h Btu/lb	s Btu/lb · °R
	11710		8 lbf/in. <sup>2</sup>	Dtu/10 K	-	10 / 10		0 lbf/in. <sup>2</sup>	Dtu/10 K
		•	-20.60°F	)				-16.63°F	)
Sat.	14.896	554.75	604.40	1.3775	-	13.497	555.78	605.76	1.3687
$-20 \\ -10$	14.919 15.306	555.00 559.13	604.72 610.14	1.3783 1.3905		13.730	558.55	609.40	1.3769
0	15.688	563.23	615.52	1.4023		14.078	562.70	614.84	1.3888
10	16.068	567.31	620.87	1.4138		14.422	566.83	620.24	1.4005
20	16.444	571.37	626.18	1.4250		14.764	570.94	625.61	1.4118
30 40	16.818 17.189	575.42 579.46	631.47 636.75	1.4359 1.4466		15.103 15.439	575.02 579.09	630.95 636.26	1.4228 1.4335
50	17.558	583.48	642.00	1.4570		15.773	583.14	641.55	1.4440
60	17.925	587.50	647.25	1.4672		16.105	587.19	646.83	1.4543
70 80	18.291 18.655	591.52 595.53	652.48 657.71	1.4772 1.4869		16.436 16.765	591.23 595.26	652.10 657.35	1.4643 1.4741
90	19.018	599.55	662.94	1.4965		17.094	599.30	662.60	1.4838
			l	l					
		•	0 lbf/in. <sup>2</sup>				•	0 lbf/in. <sup>2</sup>	
<b>G</b> .	0.2207		-0.57°F)	1 22 40				11.65°F)	1.2100
Sat.	9.2286 9.2425	559.77 560.02	611.04 611.36	1.3349 1.3356		7.0414	562.60	614.76	1.3109
10	9.4834	564.38	617.07	1.3479					
20	9.7209	568.70	622.70	1.3598		7.1965	566.39	619.69	1.3213
30 40	9.9554 10.187	572.97 577.21	628.28 633.80	1.3713 1.3824		7.3795 7.5597	570.86 575.28	625.52 631.28	1.3333 1.3450
50	10.417	581.42	639.28	1.3933		7.7376	579.65	636.96	1.3562
60	10.645	585.60	644.73	1.4039		7.9134	583.97	642.58	1.3672
70	10.871	589.76	650.15	1.4142		8.0874	588.26	648.16	1.3778
80	11.096	593.90 598.04	655.54	1.4243		8.2598	592.52	653.69	1.3881
90 100	11.319 11.541	602.16	660.91 666.27	1.4342 1.4438		8.4308 8.6006	596.75 600.97	659.20 664.67	1.3982 1.4081
110	11.762	606.28	671.62	1.4533		8.7694	605.17	670.12	1.4178
					-				
			0 lbf/in. <sup>2</sup> 21.65°F)					0 lbf/in. <sup>2</sup> 30.19°F)	
Sat.	5.7049	564.78	617.60	1.2923		4.8009	566.53	619.87	1.2770
40	5.9815	573.30	628.68	1.3149		4.9278	571.25	626.00	1.2894
60	6.2733	582.31	640.39	1.3379		5.1788	580.60	638.14	1.3133
80	6.5574	591.10	651.82	1.3595		5.4218	589.66	649.90	1.3355
100 120	6.8358 7.1097	599.75 608.30	663.04 674.13	1.3799 1.3993		5.6587 5.8910	598.52 607.23	661.39 672.68	1.3564 1.3762
140	7.3802	616.80	685.13	1.4180		6.1198	615.86	683.85	1.3951
160	7.6480	625.28	696.09	1.4360		6.3458	624.44	694.95	1.4133
200	8.1776	642.27	717.99	1.4702		6.7916	641.59	717.05	1.4479
240 280	8.7016 9.2218	659.44 676.88	740.00 762.26	1.5026 1.5336		7.2318 7.6679	658.87 676.38	739.21 761.58	1.4805 1.5116
320	9.7391	694.65	784.82	1.5633		8.1013	694.21	784.22	1.5414
360	10.254	712.79	807.73	1.5919		8.5325	712.40	807.20	1.5702

**TABLE A-15E** (Continued)

IADLL	: A-15E	(Continue	ш)					
<i>T</i>	<i>v</i>	u	<i>h</i>	s	<i>v</i>	и	<i>h</i>	s
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb·°R	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R
			0 lbf/in. <sup>2</sup> 37.67°F)			p = 8	0 lbf/in. <sup>2</sup> 44.37°F)	
Sat.	4.1473	567.99	621.74	1.2641	3.6520	569.22	623.32	1.2529
40 60	4.1739 4.3962	569.15 578.85	623.25 635.84	1.2671 1.2918	3.8084	577.06	633.48	1.2727
80	4.6100	588.19	647.95	1.3147	4.0006	586.69	645.95	1.2963
100	4.8175	597.26	659.70	1.3361	4.1862	595.98	657.99	1.3182
120	5.0202	606.14	671.22	1.3563	4.3668	605.04	669.73	1.3388
140	5.2193	614.91	682.56	1.3756	4.5436	613.94	681.25	1.3583
160	5.4154	623.60	693.79	1.3940	4.7175	622.74	692.63	1.3770
200	5.8015	640.91	716.11	1.4289	5.0589	640.22	715.16	1.4122
240	6.1818	658.29	738.42	1.4617	5.3942	657.71	737.62	1.4453
280	6.5580	675.89	760.89	1.4929	5.7256	675.39	760.20	1.4767
320	6.9314	693.78	783.62	1.5229	6.0540	693.34	783.02	1.5067
360	7.3026	712.02	806.67	1.5517	6.3802	711.63	806.15	1.5357
400	7.6721	730.63	830.08	1.5796	6.7047	730.29	829.61	1.5636
			0 lbf/in. <sup>2</sup> 50.44°F)				00 lbf/in. <sup>2</sup> 56.01°F)	
Sat. 60 80	3.2632 3.3504 3.5261	570.28 575.22 585.15	624.66 631.05 643.91	1.2429 1.2553 1.2796	2.9497 2.9832 3.1460	571.21 573.32 583.58	625.82 628.56 641.83	1.2340 1.2393 1.2644
100	3.6948	594.68	656.26	1.3021	3.3014	593.35	654.49	1.2874
120	3.8584	603.92	668.22	1.3231	3.4513	602.79	666.70	1.3088
140	4.0180	612.97	679.93	1.3430	3.5972	611.98	678.59	1.3290
160	4.1746	621.88	691.45	1.3619	3.7401	621.01	690.27	1.3481
200	4.4812	639.52	714.20	1.3974	4.0189	638.82	713.24	1.3841
240	4.7817	657.13	736.82	1.4307	4.2916	656.54	736.01	1.4176
280	5.0781	674.89	759.52	1.4623	4.5600	674.39	758.82	1.4493
320	5.3715	692.90	782.42	1.4924	4.8255	692.47	781.82	1.4796
360	5.6628	711.24	805.62	1.5214	5.0888	710.86	805.09	1.5087
400	5.9522	729.95	829.14	1.5495	5.3503	729.60	828.68	1.5368
		$p = 11$ $(T_{\text{sat}} =$	10 lbf/in. <sup>2</sup> 61.17°F)			$p = 12$ $(T_{\text{sat}} =$	20 lbf/in. <sup>2</sup> 65.98°F)	
Sat.	2.6913	572.01	626.83	1.2259	2.4745	572.73	627.71	1.2184
80	2.8344	581.97	639.71	1.2502	2.5744	580.33	637.53	1.2369
100	2.9791	592.00	652.69	1.2738	2.7102	590.63	650.85	1.2611
120	3.1181	601.63	665.14	1.2957	2.8401	600.46	663.57	1.2834
140	3.2528	610.98	677.24	1.3162	2.9657	609.97	675.86	1.3043
160	3.3844	620.13	689.07	1.3356	3.0879	619.24	687.86	1.3240
200	3.6406	638.11	712.27	1.3719	3.3254	637.40	711.29	1.3606
240	3.8905	655.96	735.20	1.4056	3.5563	655.36	734.39	1.3946
280	4.1362	673.88	758.13	1.4375	3.7829	673.37	757.43	1.4266
320	4.3788	692.02	781.22	1.4679	4.0065	691.58	780.61	1.4572
360	4.6192	710.47	804.56	1.4971	4.2278	710.08	804.02	1.4864
400	4.8578	729.26	828.21	1.5252	4.4473	728.92	827.74	1.5147

**TABLE A-15E** (Continued)

TABLE	A-15E	(Continue	2d)					
<i>T</i>	<i>v</i>	u	<i>h</i>	s	<i>v</i>	u	<i>h</i>	s
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb·°R	ft <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb·°R
	11710	p = 13	30 lbf/in. <sup>2</sup> 70.50°F)	Btu/10 K	11710	p = 14	40 lbf/in. <sup>2</sup> 74.75°F)	Btu/10 K
Sat.	2.2899	573.36	628.48	1.2115	2.1309	573.92	629.16	1.2051
80	2.3539	578.64	635.30	1.2243	2.1633	576.80	632.89	1.2119
100	2.4824	589.23	648.98	1.2492	2.2868	587.79	647.08	1.2379
120	2.6048	599.27	661.97	1.2720	2.4004	597.85	660.08	1.2604
140	2.7226	608.94	674.48	1.2932	2.5140	607.90	673.07	1.2828
160	2.8370	618.34	686.64	1.3132	2.6204	617.34	685.27	1.3025
180	2.9488	627.57	698.55	1.3321	2.7268	626.77	697.46	1.3222
200	3.0585	636.69	710.31	1.3502	2.8289	635.93	709.27	1.3401
240	3.2734	654.77	733.57	1.3844	3.0304	654.17	732.73	1.3747
280	3.4840	672.87	756.73	1.4166	3.2274	672.38	756.04	1.4071
320	3.6915	691.14	780.00	1.4472	3.4212	690.73	779.42	1.4379
360	3.8966	709.69	803.49	1.4766	3.6126	709.34	802.99	1.4674
400	4.1000	728.57	827.27	1.5049	3.8022	728.27	826.84	1.4958
			50 lbf/in. <sup>2</sup> 78.78°F)				00 lbf/in. <sup>2</sup> 96.31°F)	
Sat.	1.9923	574.42	629.76	1.1991	1.5010	576.21	631.80	1.1737
100	2.1170	586.33	645.13	1.2271	1.5190	578.52	634.77	1.1790
140	2.3332	606.84	671.65	1.2729	1.6984	601.34	664.24	1.2299
180	2.5343	625.95	696.35	1.3128	1.8599	621.77	690.65	1.2726
220	2.7268	644.43	720.17	1.3489	2.0114	641.07	715.57	1.3104
260	2.9137	662.70	743.63	1.3825	2.1569	659.90	739.78	1.3450
300	3.0968	681.02	767.04	1.4141	2.2984	678.62	763.74	1.3774
340	3.2773	699.54	790.57	1.4443	2.4371	697.44	787.70	1.4081
380	3.4558	718.35	814.34	1.4733	2.5736	716.50	811.81	1.4375
420	3.6325	737.50	838.39	1.5013	2.7085	735.86	836.17	1.4659
460	3.8079	757.01	862.78	1.5284	2.8420	755.57	860.82	1.4933
500	3.9821	776.91	887.51	1.5548	2.9742	775.65	885.80	1.5199
540	4.1553	797.19	912.60	1.5804	3.1054	796.10	911.11	1.5457
580	4.3275	817.85	938.05	1.6053	3.2357	816.94	936.77	1.5709
		$p = 25$ $(T_{\text{sat}} =$	50 lbf/in. <sup>2</sup> 110.78°F)				00 lbf/in. <sup>2</sup> 123.20°F)	
Sat.	1.2007	577.16	632.74	1.1533	0.9974	577.54	632.94	1.1361
140	1.3150	595.40	656.28	1.1936	1.0568	588.94	647.65	1.1610
180	1.4539	617.38	684.69	1.2395	1.1822	612.75	678.42	1.2107
220	1.5816	637.61	710.82	1.2791	1.2944	634.01	705.91	1.2524
260	1.7025	657.03	735.85	1.3149	1.3992	654.09	731.82	1.2895
300	1.8191	676.17	760.39	1.3481	1.4994	673.69	756.98	1.3235
340	1.9328	695.32	784.79	1.3794	1.5965	693.16	781.85	1.3554
380	2.0443	714.63	809.27	1.4093	1.6913	712.74	806.70	1.3857
420	2.1540	734.22	833.93	1.4380	1.7843	732.55	831.67	1.4148
460	2.2624	754.12	858.85	1.4657	1.8759	752.66	856.87	1.4428
500	2.3695	774.38	884.07	1.4925	1.9663	773.10	882.33	1.4699
540	2.4755	795.01	909.61	1.5186	2.0556	793.90	908.09	1.4962
580	2.5807	816.01	935.47	1.5440	2.1440	815.07	934.17	1.5218

 TABLE A-16E
 Properties of Saturated Propane (Liquid–Vapor): Temperature Table

			c Volume t³/lb	Internal Btu			Enthalpy Btu/lb		Entro Btu/lb		
Temp. °F	Press. lbf/in <sup>2</sup>	Sat. Liquid $v_{ m f}$	Sat. Vapor $v_{ m g}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor $u_{\rm g}$	Sat. Liquid $h_{ m f}$	Evap. $h_{\rm fg}$	Sat. Vapor $h_{\rm g}$	Sat. Liquid $s_{\mathrm{f}}$	Sat. Vapor s <sub>g</sub>	Temp.
-140	0.6053	0.02505	128.00	-51.33	139.22	-51.33	204.9	153.6	-0.139	0.501	-140
-120	1.394	0.02551	58.88	-41.44	143.95	-41.43	200.6	159.1	-0.109	0.481	-120
-100	2.888	0.02601	29.93	-31.34	148.80	-31.33	196.1	164.8	-0.080	0.465	-100
-80	5.485	0.02653	16.52	-21.16	153.73	-21.13	191.6	170.5	-0.053	0.452	-80
-60	9.688	0.02708	9.75	-10.73	158.74	-10.68	186.9	176.2	-0.026	0.441	-60
$     \begin{array}{r}     -40 \\     -20 \\     0 \\     10 \\     20   \end{array} $	16.1	0.02767	6.08	-0.08	163.80	0.00	181.9	181.9	0.000	0.433	-40
	25.4	0.02831	3.98	10.81	168.88	10.94	176.6	187.6	0.025	0.427	-20
	38.4	0.02901	2.70	21.98	174.01	22.19	171.0	193.2	0.050	0.422	0
	46.5	0.02939	2.25	27.69	176.61	27.94	168.0	196.0	0.063	0.420	10
	55.8	0.02978	1.89	33.47	179.15	33.78	164.9	198.7	0.074	0.418	20
30	66.5	0.03020	1.598	39.34	181.71	39.71	161.7	201.4	0.087	0.417	30
40	78.6	0.03063	1.359	45.30	184.30	45.75	158.3	204.1	0.099	0.415	40
50	92.3	0.03110	1.161	51.36	186.74	51.89	154.7	206.6	0.111	0.414	50
60	107.7	0.03160	0.9969	57.53	189.30	58.16	151.0	209.2	0.123	0.413	60
70	124.9	0.03213	0.8593	63.81	191.71	64.55	147.0	211.6	0.135	0.412	70
80	144.0	0.03270	0.7433	70.20	194.16	71.07	142.9	214.0	0.147	0.411	80
90	165.2	0.03332	0.6447	76.72	196.46	77.74	138.4	216.2	0.159	0.410	90
100	188.6	0.03399	0.5605	83.38	198.71	84.56	133.7	218.3	0.171	0.410	100
110	214.3	0.03473	0.4881	90.19	200.91	91.56	128.7	220.3	0.183	0.409	110
120	242.5	0.03555	0.4254	97.16	202.98	98.76	123.3	222.1	0.195	0.408	120
130	273.3	0.03646	0.3707	104.33	204.92	106.17	117.5	223.7	0.207	0.406	130
140	306.9	0.03749	0.3228	111.70	206.64	113.83	111.1	225.0	0.220	0.405	140
150	343.5	0.03867	0.2804	119.33	208.05	121.79	104.1	225.9	0.233	0.403	150
160	383.3	0.04006	0.2426	127.27	209.16	130.11	96.3	226.4	0.246	0.401	160
170	426.5	0.04176	0.2085	135.60	209.81	138.90	87.4	226.3	0.259	0.398	170
180	473.4	0.04392	0.1771	144.50	209.76	148.35	76.9	225.3	0.273	0.394	180
190	524.3	0.04696	0.1470	154.38	208.51	158.94	63.8	222.8	0.289	0.387	190
200	579.7	0.05246	0.1148	166.65	204.16	172.28	44.2	216.5	0.309	0.376	200
206.1	616.1	0.07265	0.07265	186.99	186.99	195.27	0.0	195.27	0.343	0.343	206.1

## 798 Tables in English Units

 TABLE A-17E
 Properties of Saturated Propane (Liquid-Vapor): Pressure Table

			ic Volume t <sup>3</sup> /lb	Internal Btu		]	Enthalpy Btu/lb		Entro Btu/lb		
		Sat.	Sat.	Sat.	Sat.	Sat.		Sat.	Sat.	Sat.	
Press.	Temp.	Liquid	Vapor	Liquid	Vapor	Liquid	Evap.	Vapor	Liquid	Vapor	Press.
lbf/in <sup>2</sup>	°F	$v_{ m f}$	$v_{ m g}$	$u_{\mathrm{f}}$	$u_{\mathrm{g}}$	$h_{ m f}$	$h_{ m fg}$	$h_{ m g}$	$s_{ m f}$	$s_{\mathrm{g}}$	lbf/in <sup>2</sup>
0.75	-135.1	0.02516	104.8	-48.93	140.36	-48.93	203.8	154.9	-0.132	0.496	0.75
1.5	-118.1	0.02556	54.99	-40.44	144.40	-40.43	200.1	159.7	-0.106	0.479	1.5
3	-98.9	0.02603	28.9	-30.84	149.06	-30.83	196.0	165.1	-0.079	0.464	3
5	-83.0	0.02644	18.00	-22.75	152.96	-22.73	192.4	169.6	-0.057	0.454	5
7.5	-69.3	0.02682	12.36	-15.60	156.40	-15.56	189.1	173.6	-0.038	0.446	7.5
10	-58.8	0.02711	9.468	-10.10	159.04	-10.05	186.6	176.6	-0.024	0.441	10
20	-30.7	0.02796	4.971	4.93	166.18	5.03	179.5	184.6	0.012	0.430	20
30	-12.1	0.02858	3.402	15.15	170.93	15.31	174.5	189.8	0.035	0.425	30
40	2.1	0.02909	2.594	23.19	174.60	23.41	170.4	193.8	0.053	0.422	40
50	13.9	0.02954	2.099	29.96	177.63	30.23	166.8	197.1	0.067	0.419	50
60	24.1	0.02995	1.764	35.86	180.23	36.19	163.6	199.8	0.079	0.418	60
70	33.0	0.03033	1.520	41.14	182.50	41.53	160.6	202.2	0.090	0.416	70
80	41.1	0.03068	1.336	45.95	184.57	46.40	157.9	204.3	0.100	0.415	80
90	48.4	0.03102	1.190	50.38	186.36	50.90	155.3	206.2	0.109	0.414	90
100	55.1	0.03135	1.073	54.52	188.07	55.10	152.8	207.9	0.117	0.414	100
120	67.2	0.03198	0.8945	62.08	191.07	62.79	148.1	210.9	0.131	0.412	120
140	78.0	0.03258	0.7650	68.91	193.68	69.75	143.7	213.5	0.144	0.412	140
160	87.6	0.03317	0.6665	75.17	195.97	76.15	139.5	215.7	0.156	0.411	160
180	96.5	0.03375	0.5890	80.99	197.97	82.12	135.5	217.6	0.166	0.410	180
200	104.6	0.03432	0.5261	86.46	199.77	87.73	131.4	219.2	0.176	0.409	200
220	112.1	0.03489	0.4741	91.64	201.37	93.06	127.6	220.7	0.185	0.408	220
240	119.2	0.03547	0.4303	96.56	202.76	98.14	123.7	221.9	0.194	0.408	240
260	125.8	0.03606	0.3928	101.29	204.07	103.0	120.0	223.0	0.202	0.407	260
280	132.1	0.03666	0.3604	105.83	205.27	107.7	116.1	223.9	0.210	0.406	280
300	138.0	0.03727	0.3319	110.21	206.27	112.3	112.4	224.7	0.217	0.405	300
320	143.7	0.03790	0.3067	114.47	207.17	116.7	108.6	225.3	0.224	0.404	320
340	149.1	0.03855	0.2842	118.60	207.96	121.0	104.7	225.8	0.231	0.403	340
360	154.2	0.03923	0.2639	122.66	208.58	125.3	100.9	226.2	0.238	0.402	360
380	159.2	0.03994	0.2455	126.61	209.07	129.4	97.0	226.4	0.245	0.401	380
400	164.0	0.04069	0.2287	130.51	209.47	133.5	93.0	226.5	0.251	0.400	400
450	175.1	0.04278	0.1921	140.07	209.87	143.6	82.2	225.9	0.266	0.396	450
500	185.3	0.04538	0.1610	149.61	209.27	153.8	70.4	224.2	0.282	0.391	500
600	203.4	0.05659	0.1003	172.85	200.27	179.1	32.2	211.4	0.319	0.367	600
616.1	206.1	0.07265	0.07265	186.99	186.99	195.3	0.0	195.3	0.343	0.343	616.1

**TABLE A-18E** Properties of Superheated Propane

IABLE	A-10E	riopeines c	or Superno	eated Propane				
<i>T</i>	<i>v</i>	<i>u</i>	<i>h</i>	s	<i>v</i>	u	<i>h</i>	s
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb·°R	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R
			75 lbf/in <sup>2</sup> -135.1°F)	)			.5 lbf/in <sup>2</sup> -118.1°F	<i>"</i> )
Sat130	104.8 106.5	140.4 141.6	154.9 156.4	0.496 0.501	54.99	144.4	159.7	0.479
-110	113.1	146.6	162.3	0.518	56.33	146.5	162.1	0.486
-90	119.6	151.8	168.4	0.535	59.63	151.7	168.2	0.503
-70	126.1	157.2	174.7	0.551	62.92	157.1	174.5	0.520
-50	132.7	162.7	181.2	0.568	66.20	162.6	181.0	0.536
-30	139.2	168.6	187.9	0.584	69.47	168.4	187.7	0.552
-10	145.7	174.4	194.7	0.599	72.74	174.4	194.6	0.568
10	152.2	180.7	201.9	0.615	76.01	180.7	201.8	0.583
30	158.7	187.1	209.2	0.630	79.27	187.1	209.1	0.599
50	165.2	193.8	216.8	0.645	82.53	193.8	216.7	0.614
70	171.7	200.7	224.6	0.660	85.79	200.7	224.5	0.629
90	178.2	207.8	232.6	0.675	89.04	207.8	232.5	0.644
			0 lbf/in <sup>2</sup> -83.0°F)				0.0 lbf/in <sup>2</sup> -58.8°F	
Sat80 -60	18.00 18.15 19.17	153.0 153.8 159.4	169.6 170.6 177.1	0.454 0.456 0.473	9.468	159.0	176.6	0.441
-40	20.17	165.1	183.8	0.489	9.957	80.9	99.3	1.388
-20	21.17	171.1	190.7	0.505	10.47	86.9	106.3	1.405
0	22.17	177.2	197.7	0.521	10.98	93.1	113.4	1.421
20	23.16	183.5	205.0	0.536	11.49	99.5	120.8	1.436
40	24.15	190.1	212.5	0.552	11.99	106.1	128.3	1.452
60	25.14	196.9	220.2	0.567	12.49	113.0	136.1	1.467
80	26.13	204.0	228.2	0.582	12.99	120.0	144.1	1.482
100	27.11	211.3	236.4	0.597	13.49	127.3	152.3	1.497
120	28.09	218.8	244.8	0.611	13.99	134.9	160.7	1.512
140	29.07	226.5	253.4	0.626	14.48	142.6	169.4	1.526
			.0 lbf/in <sup>2</sup> -30.7°F)			•	0.0 lbf/in <sup>2</sup> = 2.1°F)	
Sat20	4.971 5.117 5.385	166.2 169.5 175.8	184.6 188.5 195.8	0.430 0.439 0.455	2.594	174.6	193.8	0.422
20	5.648	182.4	203.3	0.471	2.723	180.6	200.8	0.436
40	5.909	189.1	211.0	0.487	2.864	187.6	208.8	0.453
60	6.167	195.9	218.8	0.502	3.002	194.6	216.9	0.469
80	6.424	203.1	226.9	0.518	3.137	201.8	225.1	0.484
100	6.678	210.5	235.2	0.533	3.271	209.4	233.6	0.500
120	6.932	218.0	243.7	0.548	3.403	217.0	242.2	0.515
140	7.184	225.8	252.4	0.562	3.534	224.9	251.1	0.530
160	7.435	233.9	261.4	0.577	3.664	232.9	260.1	0.545
180	7.685	242.1	270.6	0.592	3.793	241.3	269.4	0.559
200	7.935	250.6	280.0	0.606	3.921	249.8	278.9	0.574

**TABLE A-18E** (Continued)

0	<i>U</i>	u	h	S CH OD	<i>v</i>	u	h	S
°F	ft <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb·°R	ft <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb · °R
			.0 lbf/in <sup>2</sup> 24.1°F)				0.0 lbf/in <sup>2</sup> = 41.1°F)	
Sat.	1.764	180.2	199.8	0.418	1.336	184.6	204.3	0.415
30 50	1.794 1.894	182.4 189.5	202.3 210.6	0.384 0.400	1.372	187.9	208.2	0.423
70	1.992	196.9	219.0	0.417	1.450	195.4	216.9	0.440
90 110	2.087 2.179	204.4 212.1	227.6 236.3	0.432 0.448	1.526 1.599	203.1 210.9	225.7 234.6	0.456 0.472
130	2.271	220.0	245.2	0.463	1.671	218.8	243.6	0.487
150 170	2.361 2.450	228.0 236.3	254.2 263.5	0.478 0.493	1.741 1.810	227.0 235.4	252.8 262.2	0.503 0.518
190	2.539	244.8	273.0	0.508	1.879	244.0	271.8	0.533
210 230	2.626 2.713	253.5 262.3	282.7 292.5	0.523 0.537	1.946 2.013	252.7 261.7	281.5 291.5	0.548 0.562
250	2.800	271.6	302.7	0.552	2.079	270.9	301.7	0.577
		1.0	0.11.67. 2			1.	20 11 61 2	
			0 lbf/in <sup>2</sup> 55.1°F)				20 lbf/in <sup>2</sup> = 67.2°F)	
Sat.	1.073	188.1	207.9	0.414	0.8945	191.1	210.9	0.412
60 80	1.090 1.156	189.9 197.8	210.1 219.2	0.418 0.435	0.9323	196.2	216.9	0.424
100	1.219	205.7	228.3	0.452	0.9887	204.3	226.3	0.441
120	1.280	213.7	237.4	0.468	1.043	212.5	235.7	0.457
140	1.340	221.9	246.7	0.483	1.094	220.8	245.1	0.473
160 180	1.398 1.454	230.2 238.8	256.1 265.7	0.499 0.514	1.145 1.194	229.2 237.9	254.7 264.4	0.489 0.504
200	1.510	247.5	275.5	0.529	1.242	246.7	274.3	0.520
220	1.566	256.4	285.4	0.544	1.289	255.6	284.3	0.534
240	1.620	265.6	295.6	0.559	1.336	264.8	294.5	0.549
260	1.674	274.9	305.9	0.573	1.382	274.2	304.9	0.564
280	1.728	284.4	316.4	0.588	1.427	283.8	315.5	0.579
			0 lbf/in <sup>2</sup>				60 lbf/in <sup>2</sup>	
	0.7470		78.0°F)	0.442			= 87.6°F)	0.111
Sat. 80	0.7650 0.7705	193.7 213.3	213.5 214.5	0.412 0.413	0.6665	196.0	215.7	0.411
100	0.8227	222.9	224.2	0.431	0.6968	201.2	221.9	0.422
120	0.8718	232.4	233.8	0.448	0.7427	209.9	231.9	0.439
140 160	0.9185 0.9635	242.1 251.7	243.5 253.2	0.464 0.480	0.7859 0.8272	218.4 227.2	241.7 251.7	0.456 0.472
180	1.007	261.4	263.0	0.496	0.8669	235.9	261.6	0.488
200	1.050	271.4	273.0	0.511	0.9054	244.9	271.7	0.504
220	1.091	281.5	283.2	0.526	0.9430	254.0	282.0	0.519
240	1.132	291.7	293.5	0.541	0.9797	263.4	292.4	0.534
260 280	1.173	302.1 312.7	303.9 314.6	0.556 0.571	1.016 1.051	272.8 282.6	302.9 313.7	0.549 0.564
300	1.213 1.252	323.6	314.6	0.571	1.031	292.4	324.6	0.564

**TABLE A-18E** (Continued)

T	<i>U</i>	и	h	S	U o 3 m	и	h	S
°F	ft³/lb	Btu/lb	Btu/lb	Btu/lb·°R	ft³/lb	Btu/lb	Btu/lb	Btu/lb · °R
			0 lbf/in <sup>2</sup> 96.5°F)				00 lbf/in <sup>2</sup> 104.6°F)	
Sat. 100	0.5890 0.5972	198.0 199.6	217.6 219.5	0.410 0.413	0.5261	199.8	219.2	0.409
120	0.6413	208.4	229.8	0.431	0.5591	206.8	227.5	0.424
140	0.6821	217.1	239.9	0.449	0.5983	215.8	238.0	0.441
160 180	0.7206 0.7574	226.1 234.9	250.1 260.2	0.465 0.481	0.6349 0.6694	224.9 233.9	248.4 258.7	0.458 0.475
200	0.7928	244.0	270.4	0.497	0.7025	243.1	269.1	0.491
220 240	0.8273 0.8609	253.2 262.6	280.8 291.3	0.513 0.528	0.7345 0.7656	252.4 261.7	279.6 290.1	0.506 0.522
260	0.8938	272.1	301.9	0.543	0.7960	271.4	300.9	0.522
280	0.9261	281.8	312.7	0.558	0.8257	281.1	311.7	0.552
300	0.9579	291.8	323.7	0.572	0.8549	291.1	322.8	0.567
320	0.9894	301.9	334.9	0.587	0.8837	301.3	334.0	0.581
			0 lbf/in <sup>2</sup> 112.1°F)				40 lbf/in <sup>2</sup> 119.2°F)	
Cat	0.4741			0.409	0.4202			
Sat. 120	0.4741 0.4906	201.4 205.1	220.7 225.1	0.408 0.416	0.4303 0.4321	202.8 203.2	221.9 222.4	0.408 0.409
140	0.5290	214.4	236.0	0.435	0.4704	212.9	233.8	0.428
160	0.5642	223.6	246.6	0.452	0.5048	222.4	244.8	0.446
180	0.5971	232.9	257.2	0.469	0.5365	231.6	255.5	0.463
200	0.6284	242.1	267.7	0.485	0.5664	241.1	266.3	0.480
220	0.6585	251.5	278.3	0.501	0.5949	250.5	277.0	0.496
240 260	0.6875 0.7158	261.0 270.6	289.0 299.8	0.516 0.532	0.6223 0.6490	260.1 269.8	287.8 298.7	0.511 0.527
280	0.7435	280.5	310.8	0.532	0.6749	279.8	309.8	0.542
300	0.7706	290.5	321.9	0.547	0.7002	289.8	320.9	0.542
320	0.7972	300.6	333.1	0.576	0.7251	300.1	332.3	0.571
340	0.8235	311.0	344.6	0.591	0.7496	310.5	343.8	0.586
			0 lbf/in <sup>2</sup>				80 lbf/in <sup>2</sup>	
		$(T_{\rm sat} =$	125.8°F)			$(T_{\rm sat} =$	132.1°F)	
Sat.	0.3928	204.1	223.0	0.407	0.3604	205.3	223.9	0.406
130 150	0.4012 0.4374	206.3 216.1	225.6 237.2	0.411 0.431	0.3932	214.5	234.9	0.424
170	0.4697	225.8	248.4	0.449	0.4253	224.4	246.5	0.443
190	0.4995	235.2	259.3	0.466	0.4544	234.1	257.7	0.461
210	0.5275	244.8	270.2	0.482	0.4815	243.8	268.8	0.477
230 250	0.5541	254.4	281.1	0.498	0.5072	253.5	279.8	0.494
230 270	0.5798 0.6046	264.2 274.1	292.1 303.2	0.514 0.530	0.5317 0.5553	263.3 273.3	290.9 302.1	0.510 0.525
290	0.6288	284.0	314.3	0.545	0.5783	283.4	313.4	0.540
310	0.6524	294.3	325.7	0.543	0.6007	293.5	324.7	0.555
330	0.6756	304.7	337.2	0.574	0.6226	304.0	336.3	0.570
350	0.6984	315.2	348.8	0.589	0.6441	314.6	348.0	0.585

**TABLE A-18E** (Continued)

T	v 2 3 mm	и	h	S	<i>v</i>	и	h	S		
°F	ft <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb·°R	ft <sup>3</sup> /lb	Btu/lb	Btu/lb	Btu/lb · °R		
			0 lbf/in <sup>2</sup> 143.7°F)		$p = 360 \text{ lbf/in}^2$ ( $T_{\text{sat}} = 154.2^{\circ}\text{F}$ )					
Sat.	0.3067	207.2	225.3	0.404	0.2639	208.6	226.2	0.402		
150 170	0.3187 0.3517	210.7 221.4	229.6 242.3	0.412 0.432	0.2920	217.9	237.4	0.420		
190	0.3803	231.7	254.2	0.450	0.3213	228.8	250.2	0.440		
210 230	0.4063 0.4304	241.6 251.6	265.7 277.1	0.468 0.485	0.3469 0.3702	239.3 249.5	262.4 274.2	0.459 0.476		
250	0.4533	261.6	288.5	0.483	0.3702	259.8	285.9	0.470		
270	0.4751	271.7	299.9	0.517	0.4124	270.1	297.6	0.509		
290 310	0.4961	281.9 292.3	311.3 322.9	0.532 0.548	0.4320 0.4510	280.4 290.8	309.2 320.9	0.525 0.540		
330	0.5165 0.5364	302.7	322.9	0.548	0.4510	301.4	332.7	0.540		
350	0.5559	313.4	346.3	0.577	0.4872	312.2	344.7	0.570		
370	0.5750	324.2	358.3	0.592	0.5047	323.0	356.7	0.585		
			0 lbf/in <sup>2</sup>				50 lbf/in <sup>2</sup>			
			164.0°F)			$(T_{\rm sat} =$	175.1°F)			
Sat. 170	0.2287 0.2406	209.5 213.6	226.5 231.4	0.400 0.408	0.1921	209.9	225.9	0.396		
190	0.2725	225.6	245.8	0.430	0.2205	220.7	239.1	0.416		
210	0.2985	236.7	258.8	0.450	0.2486	233.0	253.7	0.439		
230 250	0.3215 0.3424	247.4 257.8	271.2 283.2	0.468 0.485	0.2719 0.2925	244.3 255.2	267.0 279.6	0.458 0.476		
270	0.3620	268.3	295.1	0.483	0.2923	266.0	292.0	0.470		
290	0.3806	278.8	307.0	0.518	0.3290	276.8	304.2	0.510		
310	0.3984	289.4	318.9	0.534	0.3457	287.6	316.4	0.526		
330	0.4156	300.1	330.9	0.549	0.3617	298.4	328.5	0.542		
350 370	0.4322 0.4484	311.0 321.9	343.0 355.1	0.564 0.579	0.3772 0.3922	309.4 320.4	340.8 353.1	0.557 0.572		
390	0.4643	333.1	367.5	0.594	0.4068	331.7	365.6	0.587		
		n = 50	0 lbf/in <sup>2</sup>			n = 6	00 lbf/in <sup>2</sup>			
			185.3°F)				203.4°F)			
Sat.	0.1610	209.3	224.2	0.391	0.1003	200.3	211.4	0.367		
190 210	0.1727 0.2066	213.8 228.6	229.8 247.7	0.399 0.426	0.1307	214.3	228.8	0.394		
230	0.2312	240.9	262.3	0.448	0.1661	232.2	250.7	0.426		
250	0.2519	252.4	275.7	0.467	0.1892	245.8	266.8	0.449		
270 290	0.2704 0.2874	263.6 274.6	288.6	0.485 0.502	0.2080 0.2245	258.1	281.2 294.8	0.469 0.487		
310	0.2874	285.6	301.2 313.7	0.502	0.2243	269.8 281.4	308.0	0.487		
330	0.3186	296.6	326.1	0.534	0.2536	292.8	321.0	0.521		
350	0.3331	307.7	338.6	0.550	0.2669	304.2	333.9	0.538		
370 390	0.3471 0.3607	318.9 330.2	351.0 363.6	0.565 0.580	0.2796 0.2917	315.7 327.3	346.8 359.7	0.553 0.569		
410	0.3740	341.7	376.3	0.580	0.2917	338.9	372.6	0.584		

**TABLE A-19E** Properties of Selected Solids and Liquids:  $c_p$ ,  $\rho$ , and  $\kappa$ 

	Specific	Density,	Thermal
	Heat, $c_p$	ho	Conductivity, $\kappa$
Substance	$(Btu/lb \cdot {}^{\circ}R)$	(lb/ft <sup>3</sup> )	$(Btu/h \cdot ft \cdot {}^{\circ}R)$
Selected Solids, 540°R			
Aluminum	0.216	169	137
Coal, anthracite	0.301	84.3	0.15
Copper	0.092	557	232
Granite	0.185	164	1.61
Iron	0.107	491	46.4
Lead	0.031	705	20.4
Sand	0.191	94.9	0.16
Silver	0.056	656	248
Soil	0.439	128	0.30
Steel (AISI 302)	0.115	503	8.7
Tin	0.054	456	38.5
Building Materials, 540°R			
Brick, common	0.199	120	0.42
Concrete (stone mix)	0.210	144	0.81
Glass, plate	0.179	156	0.81
Hardboard, siding	0.279	40	0.054
Limestone	0.193	145	1.24
Plywood	0.291	34	0.069
Softwoods (fir, pine)	0.330	31.8	0.069
Insulating Materials, 540°R			
Blanket (glass fiber)	_	1.0	0.027
Cork	0.43	7.5	0.023
Duct liner (glass fiber, coated)	0.199	2.0	0.022
Polystyrene (extruded)	0.289	3.4	0.016
Vermiculite fill (flakes)	0.199	5.0	0.039
Saturated Liquids			
Ammonia, 540°R	1.151	37.5	0.269
Mercury, 540°R	0.033	845	4.94
Refrigerant 22, 540°R	0.303	74.0	0.049
Refrigerant 134a, 540°R	0.343	75.0	0.047
Unused Engine Oil, 540°R	0.456	55.2	0.084
Water, 495°R	1.006	62.42	0.332
540°R	0.998	62.23	0.354
585°R	0.999	61.61	0.373
630°R	1.002	60.79	0.386
675°R	1.008	59.76	0.394
720°R	1.017	58.55	0.398

Source: Drawn from several sources, these data are only representative. Values can vary depending on temperature, purity, moisture content, and other factors.

**TABLE A-20E** Ideal Gas Specific Heats of Some Common Gases (Btu/lb  $\cdot$   $^{\circ}$ R)

	ideal das specific fleats of some common dases (bla/16 K)									
	$c_p$	$c_v$	k	$c_p$	$c_v$	k	$c_p$	$c_v$	k	
Temp.		Air		Nitrogen, N <sub>2</sub>			(	Temp.		
40	0.240	0.171	1.401	0.248	0.177	1.400	0.219	0.156	1.397	40
100	0.240	0.172	1.400	0.248	0.178	1.399	0.220	0.158	1.394	100
200	0.241	0.173	1.397	0.249	0.178	1.398	0.223	0.161	1.387	200
300	0.243	0.174	1.394	0.250	0.179	1.396	0.226	0.164	1.378	300
400	0.245	0.176	1.389	0.251	0.180	1.393	0.230	0.168	1.368	400
500	0.248	0.179	1.383	0.254	0.183	1.388	0.235	0.173	1.360	500
600	0.250	0.182	1.377	0.256	0.185	1.383	0.239	0.177	1.352	600
700	0.254	0.185	1.371	0.260	0.189	1.377	0.242	0.181	1.344	700
800	0.257	0.188	1.365	0.262	0.191	1.371	0.246	0.184	1.337	800
900	0.259	0.191	1.358	0.265	0.194	1.364	0.249	0.187	1.331	900
1000	0.263	0.195	1.353	0.269	0.198	1.359	0.252	0.190	1.326	1000
1500	0.276	0.208	1.330	0.283	0.212	1.334	0.263	0.201	1.309	1500
2000	0.286	0.217	1.312	0.293	0.222	1.319	0.270	0.208	1.298	2000
Temp.	Carbon Dioxide, CO <sub>2</sub>			Carbon Monoxide, CO			H	Temp.		
40	0.195	0.150	1.300	0.248	0.177	1.400	3.397	2.412	1.409	40
100	0.205	0.160	1.283	0.249	0.178	1.399	3.426	2.441	1.404	100
200	0.217	0.172	1.262	0.249	0.179	1.397	3.451	2.466	1.399	200
300	0.229	0.184	1.246	0.251	0.180	1.394	3.461	2.476	1.398	300
400	0.239	0.193	1.233	0.253	0.182	1.389	3.466	2.480	1.397	400
500	0.247	0.202	1.223	0.256	0.185	1.384	3.469	2.484	1.397	500
600	0.255	0.210	1.215	0.259	0.188	1.377	3.473	2.488	1.396	600
700	0.262	0.217	1.208	0.262	0.191	1.371	3.477	2.492	1.395	700
800	0.269	0.224	1.202	0.266	0.195	1.364	3.494	2.509	1.393	800
900	0.275	0.230	1.197	0.269	0.198	1.357	3.502	2.519	1.392	900
1000	0.280	0.235	1.192	0.273	0.202	1.351	3.513	2.528	1.390	1000
1500	0.298	0.253	1.178	0.287	0.216	1.328	3.618	2.633	1.374	1500
2000	0.312	0.267	1.169	0.297	0.226	1.314	3.758	2.773	1.355	2000

Source: Adapted from K. Wark, Thermodynamics, 4th ed., McGraw-Hill, New York, 1983, as based on "Tables of Thermal Properties of Gases," NBS Circular 564, 1955.

**TABLE A-21E** Variation of  $\overline{c}_p$  with Temperature for Selected Ideal Gases

$$\frac{\overline{c}_p}{\overline{R}} = \alpha + \beta T + \gamma T^2 + \delta T^3 + \varepsilon T^4$$

T is in °R, equations valid from 540 to 1800 °R

Gas	$\alpha$	$\beta \times 10^3$	$\gamma \times 10^6$	$\delta \times 10^9$	$\varepsilon \times 10^{12}$
CO	3.710	-0.899	1.140	-0.348	0.0228
$CO_2$	2.401	4.853	-2.039	0.343	0
$H_2$	3.057	1.487	-1.793	0.947	-0.1726
$H_2O$	4.070	-0.616	1.281	-0.508	0.0769
$O_2$	3.626	-1.043	2.178	-1.160	0.2053
$N_2$	3.675	-0.671	0.717	-0.108	-0.0215
Air	3.653	-0.7428	1.017	-0.328	0.02632
$NH_3$	3.591	0.274	2.576	-1.437	0.2601
NO	4.046	-1.899	2.464	-1.048	0.1517
$NO_2$	3.459	1.147	2.064	-1.639	0.3448
$SO_2$	3.267	2.958	0.211	-0.906	0.2438
$SO_3$	2.578	8.087	-2.832	-0.136	0.1878
$CH_4$	3.826	-2.211	7.580	-3.898	0.6633
$C_2H_2$	1.410	10.587	-7.562	2.811	-0.3939
$C_2H_4$	1.426	6.324	2.466	-2.787	0.6429
Monatomic					
gases <sup>a</sup>	2.5	0	0	0	0

 $<sup>^</sup>a$ For monatomic gases, such as He, Ne, and Ar,  $\bar{c}_p$  is constant over a wide temperature range and is very nearly equal to  $5/2 \overline{R}$ .

Source: Adapted from K. Wark, Thermodynamics, 4th ed., McGraw-Hill, New York, 1983, as based on NASA SP-273, U.S. Government Printing Office, Washington, DC, 1971.

## 806 Tables in English Units

**TABLE A-22E** Ideal Gas Properties of Air

	$T(^{\circ}R)$ , h and $u(Btu/lb)$ , $s^{\circ}(Btu/lb \cdot {^{\circ}R})$										
				when $\Delta$	$s = 0^1$					when $\Delta s$	r = 0
T	h	и	$s^{\circ}$	$p_{ m r}$	$v_{ m r}$	T	h	и	$s^{\circ}$	$p_{ m r}$	$v_{\rm r}$
360	85.97	61.29	0.50369	0.3363	396.6	940	226.11	161.68	0.73509	9.834	35.41
380	90.75	64.70	0.51663	0.4061	346.6	960	231.06	165.26	0.74030	10.61	33.52
400	95.53	68.11	0.52890	0.4858	305.0	980	236.02	168.83	0.74540	11.43	31.76
420	100.32	71.52	0.54058	0.5760	270.1	1000	240.98	172.43	0.75042	12.30	30.12
440	105.11	74.93	0.55172	0.6776	240.6	1040	250.95	179.66	0.76019	14.18	27.17
460	109.90	78.36	0.56235	0.7913	215.33	1080	260.97	186.93	0.76964	16.28	24.58
480	114.69	81.77	0.57255	0.9182	193.65	1120	271.03	194.25	0.77880	18.60	22.30
500	119.48	85.20	0.58233	1.0590	174.90	1160	281.14	201.63	0.78767	21.18	20.29
520	124.27	88.62	0.59172	1.2147	158.58	1200	291.30	209.05	0.79628	24.01	18.51
537	128.34	91.53	0.59945	1.3593	146.34	1240	301.52	216.53	0.80466	27.13	16.93
540	129.06	92.04	0.60078	1.3860	144.32	1280	311.79	224.05	0.81280	30.55	15.52
560	133.86	95.47	0.60950	1.5742	131.78	1320	322.11	231.63	0.82075	34.31	14.25
580	138.66	98.90	0.61793	1.7800	120.70	1360	332.48	239.25	0.82848	38.41	13.12
600	143.47	102.34	0.62607	2.005	110.88	1400	342.90	246.93	0.83604	42.88	12.10
620	148.28	105.78	0.63395	2.249	102.12	1440	353.37	254.66	0.84341	47.75	11.17
640	153.09	109.21	0.64159	2.514	94.30	1480	363.89	262.44	0.85062	53.04	10.34
660	157.92	112.67	0.64902	2.801	87.27	1520	374.47	270.26	0.85767	58.78	9.578
680	162.73	116.12	0.65621	3.111	80.96	1560	385.08	278.13	0.86456	65.00	8.890
700	167.56	119.58	0.66321	3.446	75.25	1600	395.74	286.06	0.87130	71.73	8.263
720	172.39	123.04	0.67002	3.806	70.07	1650	409.13	296.03	0.87954	80.89	7.556
740	177.23	126.51	0.67665	4.193	65.38	1700	422.59	306.06	0.88758	90.95	6.924
760	182.08	129.99	0.68312	4.607	61.10	1750	436.12	316.16	0.89542	101.98	6.357
780	186.94	133.47	0.68942	5.051	57.20	1800	449.71	326.32	0.90308	114.0	5.847
800	191.81	136.97	0.69558	5.526	53.63	1850	463.37	336.55	0.91056	127.2	5.388
820	196.69	140.47	0.70160	6.033	50.35	1900	477.09	346.85	0.91788	141.5	4.974
840	201.56	143.98	0.70747	6.573	47.34	1950	490.88	357.20	0.92504	157.1	4.598
860	206.46	147.50	0.71323	7.149	44.57	2000	504.71	367.61	0.93205	174.0	4.258
880	211.35	151.02	0.71886	7.761	42.01	2050	518.61	378.08	0.93891	192.3	3.949
900	216.26	154.57	0.72438	8.411	39.64	2100	532.55	388.60	0.94564	212.1	3.667
920	221.18	158.12	0.72979	9.102	37.44	2150	546.54	399.17	0.95222	233.5	3.410

<sup>1.</sup>  $p_{\rm r}$  and  $v_{\rm r}$  data for use with Eqs. 6.43 and 6.44, respectively.