# The Trace Finite Element Method for PDEs on Surfaces

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#### 1 The Physical Problem

Consider a moving bubble of one liquid in a fluid milieu of a different liquid, with a certain concentration of some species, which adheres to the surface. Such a species is called a surfactant. An example for such a constellation would be molecules with a hydrophobic and a hydrophilic end on some bubble in water (e.g. tensides, lipids, ...).

#### 1.1 Mathematical model

Let  $\Omega \subseteq \mathbb{R}^n$  be an open domain and let  $\Omega_1$ ,  $\Omega_2 \subseteq \mathbb{R}^d$  describe the interior and exterior part of our bubble such that  $\overline{\Omega_1} \cup \overline{\Omega_2} = \Omega$ ,  $\partial \Omega_1 := \Gamma$ ,  $\Gamma \cap \partial \Omega = \emptyset$  and let n and  $\kappa$  denote the outward normal and mean curvature on  $\Gamma$  respectively.

Further we denote the densities and viscosities of our fluids by  $\rho_i$  and  $\mu_i$  respectively. Then the classical two-phase fluid dynamics model reads (cf. ??):

**Problem 1.1.** Find a velocity field u(x,t) and a pressure p(x,t), such that

$$\rho_i \left( \frac{\partial}{\partial t} u + (u \cdot \nabla) u \right) - \operatorname{div}(\mu_i D(u)) + \nabla p = \rho_i g, \quad \text{in } \Omega_i(t). \quad (1a)$$

$$\operatorname{div}(u) = 0,$$
 in  $\Omega_i(t)$ . (1b)

$$[[\sigma \cdot n]] = -\tau \kappa n, \quad \text{on } \Gamma(t).$$
 (1c)

$$[[u]] = 0,$$
 on  $\Gamma(t)$ , (1d)

where  $D(u) := \nabla u + \nabla u^T$ , [[·]] denotes the jump in normal direction,  $\tau$  is the surface tension force,  $\sigma$  the stress tensor, and g the gravitational force.

#### 1.1.1 Some remarks on differential geometry

Let  $\Gamma \subseteq \mathbb{R}^d$  be an oriented  $C^2$ -hypersurface and let n(x) denote its outward normal. For a  $C^1$ -function f on  $\Gamma$  we define its tangential derivative by

$$\nabla_{\Gamma} f := P \nabla f,\tag{2}$$

where  $P(x) := I - n(x) n(x)^T$  is the orthogonal projection on the tangential space. Further we define the tangential gradient  $\operatorname{div}_{\Gamma}$  of some vector field  $\vec{v}$  by

$$\operatorname{div}_{\Gamma}(\vec{v}) := \nabla_{\Gamma} \cdot \vec{v} = \sum_{n=1}^{d} (P\nabla)_n \, v_n = \operatorname{div}(\vec{v}) - n^T \vec{v} n. \tag{3}$$

Remark 1.2. For a differentiable scalar function f and a vector field  $\vec{g}$  on  $\Gamma$ , there holds the product rule

$$\operatorname{div}_{\Gamma}(f\vec{g}) = f \operatorname{div}_{\Gamma}(\vec{g}) + \nabla_{\Gamma} f \cdot \vec{g}. \tag{4}$$

Remark 1.3. Let  $W \subseteq \Gamma$  be an open subset and  $n_W$  denote its outward normal in the tangential plane of  $\Gamma$ . Then there holds integration of parts in  $\Gamma$ 

$$\int_{W} f \operatorname{div}_{\Gamma}(\vec{v}) ds = -\int_{W} \nabla_{\Gamma} f \cdot \vec{v} + \int_{\partial W} f \vec{v} \cdot n_{W} d\tilde{s}.$$
 (5)

**Theorem 1.4** (Reynold's transport theorem on an interface). The rate of change for a smooth function f(x,t) on  $W(t) \subseteq \Gamma$  can be described by

$$\frac{d}{dt} \int_{W(t)} f(x,t) \, ds = \int_{W(t)} \dot{f}(x,t) + f(x,t) \operatorname{div}_{\Gamma}(\vec{v}) \, ds \tag{6}$$

with the material derivative  $\dot{f}$  for a given velocity field  $\vec{v}$  defined as

$$\dot{f} := \frac{\partial f}{\partial t} + \vec{v} \cdot \nabla f \tag{7}$$

#### 1.1.2 Transport of a surfactant

Next let c(x,t) describe the concentration of the surfactant on  $\Gamma$ . Then conservation of mass in an arbitrary control volume  $W(t) \subseteq \Gamma$ , with source f yields

$$\frac{d}{dt} \int_{W(t)} c \, ds = -\int_{\partial W(t)} \vec{q} \cdot n_W \, d\tilde{s} + \int_{W(t)} f \, ds \tag{8}$$

If we assume  $\vec{q}$  to be a diffusive flux  $\vec{q} := -\alpha \nabla_{\Gamma} c$  and use integration by parts, we obtain

$$\frac{d}{dt} \int_{W(t)} c \, ds = \int_{\partial W(t)} \alpha \nabla_{\Gamma} c \cdot n_W \, d\tilde{s} + \int_{W(t)} f \, ds$$

$$= \int_{W(t)} \operatorname{div}_{\Gamma}(\alpha \nabla_{\Gamma} c) \, ds + \int_{W(t)} f \, ds. \quad (9)$$

Combined with Reynold's transport theorem we arrive at

$$\frac{d}{dt} \int_{W(t)} c \, ds = \int_{W(t)} \dot{c} + c \operatorname{div}_{\Gamma}(\vec{v}) \, ds \tag{10}$$

$$= \int_{W(t)} \frac{\partial c}{\partial t} + \vec{v} \cdot \nabla c + c \operatorname{div}_{\Gamma}(\vec{v}) ds$$
 (11)

$$= \int_{W(t)} \operatorname{div}_{\Gamma}(\alpha \nabla_{\Gamma} c) \, ds + \int_{W(t)} f \, ds. \tag{12}$$

If we assume, that the velocity  $\vec{v}$  is always tangential to the surface (i.e.  $\vec{v} \cdot n = 0$ ) there holds

$$\vec{v} \cdot \nabla c = P\vec{v} \cdot \nabla c = \vec{v} \cdot P\nabla c = \vec{v} \cdot \nabla_{\Gamma} c \tag{13}$$

and

$$\vec{v} \cdot \nabla c + c \operatorname{div}_{\Gamma}(\vec{v}) = \operatorname{div}_{\Gamma}(c\vec{v}).$$
 (14)

Our final problem for the surfactant species transport in strong form reads:

**Problem 1.5.** Given suitable boundary and initial conditions for  $\vec{v}$  and c and a source function f, find  $\vec{v}$ , p and c such that

$$\rho_i \left( \frac{\partial}{\partial t} \vec{v} + (u \cdot \nabla) \vec{v} \right) - \operatorname{div}(\mu_i D(\vec{v})) + \nabla p = \rho_i g, \quad \text{in } \Omega_i(t), \quad (15a)$$

$$\operatorname{div}(\vec{v}) = 0, \quad \text{in } \Omega_i(t), \quad (15b)$$

$$[[\sigma \cdot n]] = -\tau \kappa n, \quad \text{ on } \Gamma(t), \quad (15c)$$

$$[[\vec{v}]] = 0, \qquad \text{on } \Gamma(t), \qquad (15d)$$

$$\frac{\partial}{\partial t}c + \operatorname{div}_{\Gamma}(c\vec{v}) - \operatorname{div}_{\Gamma}(\alpha\nabla_{\Gamma}c) = f, \qquad \text{on } \Gamma(t).$$
 (15e)

In the following, we will concentrate on equation (15e) for a given velocity field  $\vec{v}$ .

Example 1.6 (Stokes flow past a sphere). Let  $\Omega_1 \subseteq \mathbb{R}^d$  (d=2,3) be a sphere (circle) with radius  $r_0$  rising with constant velocity  $v_0$ . We are interested in the resulting velocity field  $\vec{v}$  relative to the sphere. To this end we study a stationary, linearized version of (15a) and (15b), namely

$$\operatorname{div}(\vec{v}) = 0 \tag{16a}$$

$$-\nabla p + \mu_i \Delta \vec{v} = 0, \tag{16b}$$

In general an axial symmetric solution of (16) can be written in the form

$$\vec{v} = v_r \vec{e}_r + v_\theta \vec{e}_\theta = \frac{1}{r^2 \sin \theta} \frac{\partial \psi}{\partial \theta} \vec{e}_r - \frac{1}{r \sin \theta} \frac{\partial \psi}{\partial r} \vec{e}_\theta$$
 (17)

with a stream function

$$\psi(r,\theta) = r \sin^2 \theta \left( A + Br^2 + Cr^3 + Dr^5 \right). \tag{18}$$

and some coefficients A, B, C, D (r and  $\theta$  are the usual spherical coordinates). To deduce the coefficients  $A_i$ ,  $B_i$ ,  $C_i$ ,  $D_i$  for the inner and outer stream function, we need the following boundary conditions

$$\lim_{r \to \infty} v_r(r, \theta) = -v_0 \tag{19a}$$

$$\lim_{r \to 0} |v_r(r,\theta)| < \infty \tag{19b}$$

$$\lim_{r \to r_{0-}} v_{\theta}(r, \theta) = \lim_{r \to r_{0+}} v_{\theta}(r, \theta)$$
(19c)

$$\lim_{r \to r_{0-}} \sigma(r, \theta) = \lim_{r \to r_{0+}} \sigma(r, \theta)$$
 (19d)

$$\lim_{r \to r_{0-}} v_r(r, \theta) = \lim_{r \to r_{0+}} v_r(r, \theta) = 0, \tag{19e}$$

which lead to a system of linear equations

$$2C_2 = v_0 \tag{20a}$$

$$A_1 = B_1 = 0 (20b)$$

$$-A_2 + B_2 r_0^2 + v_0 r_0^3 = 2C_1 r_0^3 + 4D_1 r_0^5$$
 (20c)

$$\mu_2 A_2 = \mu_1 D_1 r_0^5 \tag{20d}$$

$$A_2 + B_2 r_0^2 + \frac{1}{2} v_0 r_0^3 = 0 (20e)$$

$$C_2 + D_2 r_0^2 = 0. (20f)$$

Solving (20) gives a stream function

$$\psi(r,\theta) = \begin{cases} \frac{v_0}{4} \sin^2 \theta \frac{1}{\mu_1 + \mu_2} \left( \frac{r_0^3}{r} \mu_2 - r_0 \left( 2\mu_2 + 3\mu_1 \right) r + 2 \left( \mu_1 + \mu_2 \right) r^2 \right), & r \ge r_0 \\ \frac{v_0}{4} \sin^2 \theta \frac{\mu_2}{\mu_1 + \mu_2} r^2 \left( \frac{r_0^2}{r_0^2} - 1 \right) & r \le r_0. \end{cases}$$

$$(21)$$

Calculating the radial and tangential component and substituting  $r=r_0$  yields the sought-after velocity field on the sphere, namely

$$\vec{v} = \vec{e}_{\theta} \frac{v_0}{2} \frac{\mu_2}{\mu_1 + \mu_2} \sin \theta. \tag{22}$$

In cartesian coordinates and two dimensions, this reads

$$\vec{v} = \frac{v_0}{2} \frac{\mu_2}{\mu_1 + \mu_2} \frac{1}{r_0^2} \begin{pmatrix} yx \\ -x^2 \end{pmatrix}. \tag{23}$$

In three dimensions we obtain

$$\vec{v} = \frac{v_0}{2} \frac{\mu_2}{\mu_1 + \mu_2} \frac{1}{r_0^2} \begin{pmatrix} zx \\ zy \\ -x^2 - y^2 \end{pmatrix}. \tag{24}$$

### 2 Discretization

## 3 Implementation

## 4 Numerical Experiments