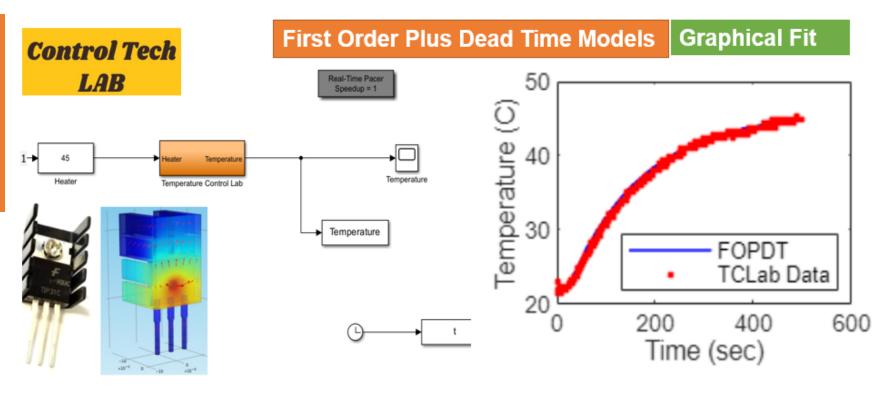
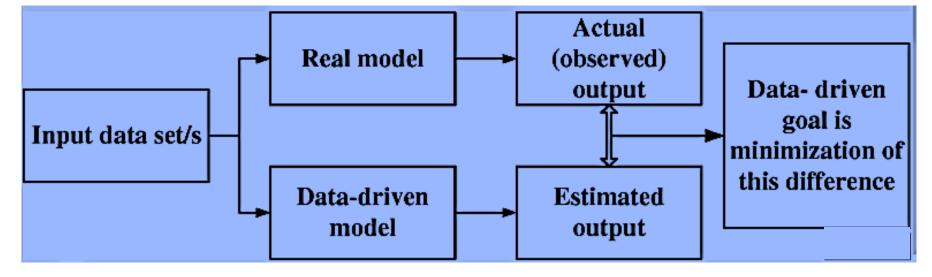
Data-Driven Modelling

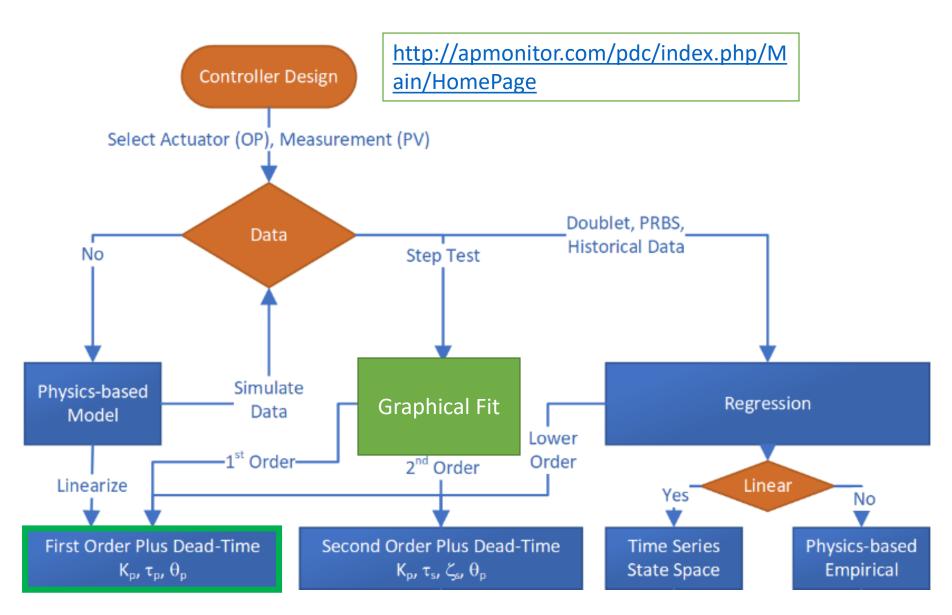






Working with:

- 1. Introduction to First Order Plus Dead Time Models with a Presentation
- 2. FOPD Temperature response to a step (A live Script that includes a video)

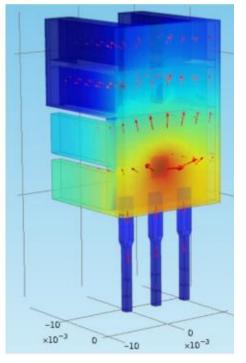


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TC Lab Dynamics:

A single heater and the total energy balance.





Quantity

Initial temperature (T_0)

Ambient temperature (T_{∞})

Heater output (Q)

Heater factor (α)

Heat capacity (C_p)

Surface Area (A)

Mass (m)

Overall Heat Transfer Coefficient (U)

Emissivity (ε)

Stefan Boltzmann Constant (σ)

$$m\,c_prac{dT}{dt}=\sum \dot{h}_{in}-\sum \dot{h}_{out}+Q$$

Q is the rate of heat transfer

$$m c_p \frac{dT}{dt} = U A \left(T_{\infty} - T \right) + \epsilon \sigma A \left(T_{\infty}^4 - T^4 \right) + \alpha Q$$

Convection

Radiation

Heater

https://apmonitor.co m/do/index.php/Mai n/AdvancedTempera tureControl

REAL TIME EXPERIMENTS - TC Lab – Dynamic model of a single heater

m = 0.001; % kg (1 gm) % mass

% heat transfer coefficient

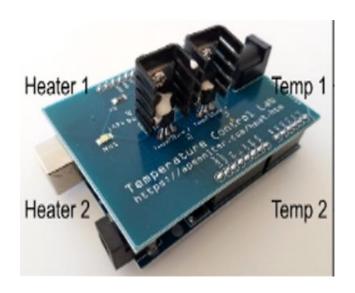
U = 200; % W/m^2-K

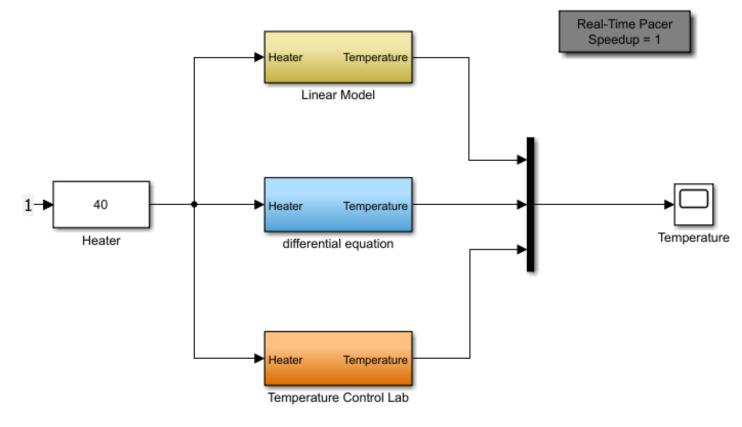
% surface area

 $A = 2 / 100^2; \% m^2$

% heat capacity

Cp = 4900.0; % J/kg-K





REAL-TIME EXPERIMENTS - TC Lab - Dynamic model of a single heater

Total Energy Balance

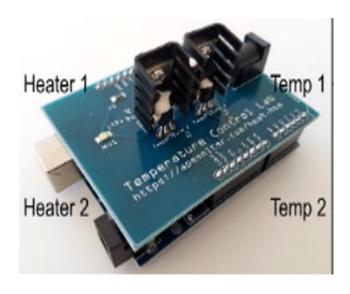
$$m(p) = MA(Tw-T) + Eb(Tw^q - T^q) + xQ$$
 T_{f} We ignore Radiation components.

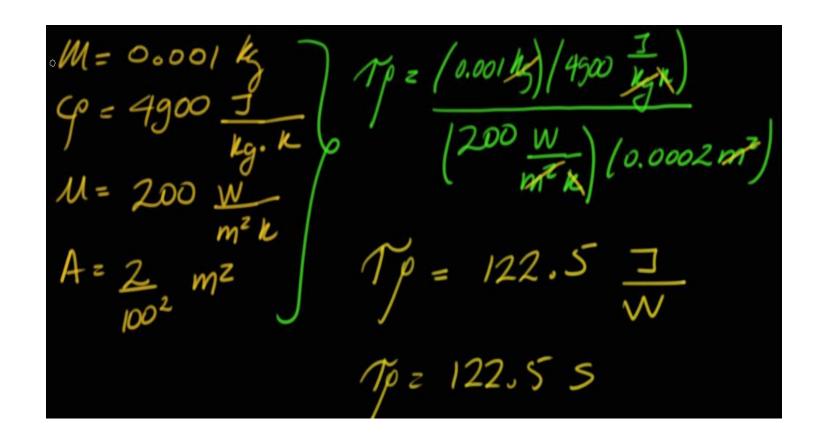
* $M(p) = MA(Tw-T) + xQ$
 T_{f} First order sufferential equation

 T_{f} at T_{f} = T_{f} $T_$

REAL-TIME EXPERIMENTS - TC Lab – Dynamic model of a single heater

m = 0.001; % kg (1 gm) % heat transfer coefficient U = 200; % W/m^2-K % surface area A = 2 / 100^2; % m^2 % heat capacity Cp = 4900.0; % J/kg-K





Temperature response to a step input and obtain the First Order Plus Dead Time FOPDT parameters

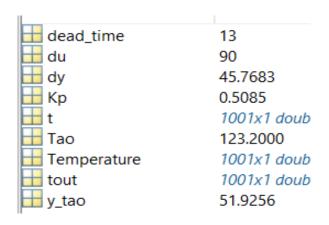


https://www.yo utube.com/wat ch?v=CJ3OD5W JUTE

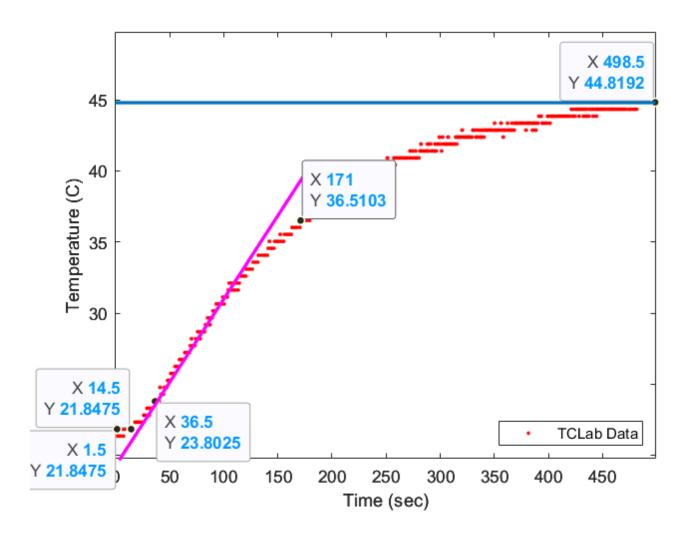
First Order Plus Dead Time Models (FOPDT) with TC lab Real Time Experiments

Temperature response to a step input and obtain the First Order Plus Dead Time FOPDT parameters

Real-Time Experiment and Graphical Fit



```
dy=Temperature(end)-Temperature(1);
du=45;
Kp=dy/du;
dead_time=22-9;
y_tao=Temperature(1)+0.632*dy;
Tao=145.2-22;
```



An Introduction to First Order Plus Dead Time Models

A first-order linear system with time delay is a common empirical description of many stable dynamic processes.

Graphical Method: FOPDT to Step Test

After gaining an intuitive understanding of the step response of a single heater model, it is important to understand the mathematical FOPDT equation

$$\tau_p \frac{dy(t)}{dt} = -y(t) + K_p u(t - \theta_p) \qquad \qquad \text{Where} \\ K_p = \text{Process gain} \\ \text{with variables} \quad y(t) \text{ and } \quad u(t) \qquad \qquad \tau_p = \text{Process time constant} \\ \theta_p = \text{Process dead time} \\$$

An Introduction to First Order Plus Dead Time Models

REAL-TIME EXPERIMENTS - TC Lab -

The Live Script will help us to see the effect of the three adjustable parameters in the FOPDT equation. The gain, time constant, and dead time. Sample data from the TC Lab is used to show how FOPDT models represent measured data.

Use the Live Script: An Introduction to

Real-Time Pacer Speedup = 1

Heater Temperature
Temperature Control Lab

Temperature
Temperature

Use the measured temperature data and see how the main dynamic parameters fit the temperature curve.

First Order Plus Dead Time Models

Obtain the gain, time constant, and dead time